

# A Benign synthesis of alane by the composition controlled mechanochemical reaction of sodium hydride and aluminum chloride

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## Abstract

Solid-state mechanochemical synthesis of alane ( $\text{AlH}_3$ ) starting from sodium hydride ( $\text{NaH}$ ) and aluminum chloride ( $\text{AlCl}_3$ ) has been achieved at room temperature. The transformation pathway of this solid-state reaction was controlled by a step-wise addition of  $\text{AlCl}_3$  to the initial reaction mixture that contained sodium hydride in excess of stoichiometric amount. As in the case of previously investigated  $\text{LiH-AlCl}_3$  system, complete selectivity was achieved whereby formation of unwanted elemental aluminum was fully suppressed, and  $\text{AlH}_3$  was obtained in quantitative yield. Reaction progress during each step was investigated by means of solid-state NMR and powder X-ray diffraction, which revealed that the overall reaction proceeds through a series of intermediate alanates that may be partially chlorinated. The  $\text{NaH-AlCl}_3$  system present some subtle differences compared to  $\text{LiH-AlCl}_3$  system particularly with respect to optimal concentrations needed during one of the reaction stages. Based on the results we postulate that high local concentrations of  $\text{NaH}$  may stabilize chlorine-containing derivatives and prevent decomposition into elemental aluminum with hydrogen evolution. Complete conversion with quantitative yield of alane was confirmed both by SSNMR and hydrogen desorption analysis.

**Keywords:** alane, ball milling, hydrogen storage, mechanochemistry, metathesis, solid-state NMR

## 1. Introduction

Uncertainties associated with sustainability of the current levels of production of crude oil and the ever-rising emissions of carbon dioxide are fueling a gradual transition to clean and renewable energy technologies, including electric propulsion of vehicles. As a result, many car manufacturers have committed to development of hydrogen fuel cell-powered vehicles. This stimulated intensive research on fully reversible solid-state hydrogen storage material(s) to supply the hydrogen required to power proton exchange membrane (PEM) fuel cells [1,2]. Challenging targets set forth by the U.S. DOE [3] both limit the list of materials potentially suitable for hydrogen storage applications and place in focus several candidates that may fulfill these stringent requirements and foster a smooth transition to hydrogen as a mainstream energy carrier.

According to recommendations of the Hydrogen Storage Engineering Center of Excellence, alane ( $\text{AlH}_3$ ) is considered as one of the most prospective materials for hydrogen storage [4,5]. The compound is valued for its remarkable gravimetric and volumetric capacities of ~10 wt.% H and ~150 g H/l respectively, in addition to its low desorption onset temperature close to 100 °C and favorable and tunable kinetics [6]. Nonetheless, alane suffers from complete irreversibility at reasonably low hydrogen pressures, which remains an outstanding syntheses challenge [6]. While density functional based computational studies point to possible stabilization of alane clusters [7], and elucidate the favorable role of transition metal catalysts and vacancies in such processes [8], attempts to convert elemental Al to  $\text{AlH}_3$  in high yields at easily achievable  $\text{H}_2$  pressures have been unsuccessful. Furthermore, traditional methods for synthesis of  $\text{AlH}_3$  not only require large volumes of environmentally hazardous organic solvents during the reaction but also relatively expensive lithium-containing reactants [9–13]. Despite being abundantly

present in the Earth's crust [14], lithium is in high demand due to the rapid growth of the rechargeable lithium battery industry. Hence, it would be beneficial to develop reactions and processes to synthesize alane using cheaper, more abundant, and noncritical resources. The most likely substitutes are the sodium-based precursors. Considering all available forms, sodium is three orders of magnitude more abundant than lithium, and is produced in large quantities through the electrolysis of molten sodium chloride that is readily available from seawater, brine, or crystalline NaCl [15].

A large body of work exists that describe the synthesis of alane from the reaction between alkali-metal hydrides or alanates with aluminum halide in ether solution [9–13]. This solution based metathesis reaction, also known as Schlesinger reaction, usually yields alane in the form of an adduct that is then further processed to obtain adduct-free alane. Successful preparation of  $\text{AlH}_3$  via  $\text{NaAlH}_4\text{-AlCl}_3$  reaction in ether-toluene mixture has been accomplished via the reaction [16]:



which proved to be a lower-cost process and also much faster synthesis method in comparison to the traditional  $\text{LiAlH}_4\text{-AlCl}_3$  route [10]. Another strategy used highly active  $\text{NaAlH}_4$  together with  $\text{AlCl}_3$  in a lower alkyl-dialkyl ether solution [17]. However, despite being less expensive, both these methods involve the use of large amounts of environmentally harmful organic solvents.

Processing and chemical related challenges associated with traditional methods, such as precise temperature control, handling of volatile organic liquids and significant loss of yields have prompted development of other syntheses routes that (1) may afford adduct-free alane [18–24]

and (2) utilize small amounts solvents or are entirely solvent-free [13–17]. We and others have recently demonstrated that these shortcomings can be partly circumvented by solvent-free mechanochemical syntheses of alane at room temperature using LiH or LiAlH<sub>4</sub> and AlCl<sub>3</sub> [20–24]. Here, we describe a room temperature mechanochemical process starting from a different hydrogen-containing precursor, namely NaH, which converts the 3NaH-AlCl<sub>3</sub> system into adduct-free alane.

## 2. Experimental

### 2.1. Materials and mechanochemical processing

As-received NaH (Aldrich, 95 %) and AlCl<sub>3</sub> (Aldrich, 99.99 %) were used as starting materials without further purification. Because of the high sensitivity of the precursors and products to moist air, manipulations at all stages were carried out in an Ar-filled glove box with the O<sub>2</sub> and H<sub>2</sub>O levels controlled at less than 5 ppm. For a typical mechanochemical reaction, a total of 1–2 g of reaction mixture was weighed out in the desired molar ratio and transferred to a custom-built high-pressure milling container for use with a two-station planetary ball mill (Fritsch, Pulverisette 7). Twenty stainless steel balls (11.9 mm in dia., each weighing ~8 g) and the reaction mixture were placed into the container, which was then sealed under Ar atmosphere inside the glove box. The argon atmosphere was purged twice with zero grade H<sub>2</sub> (Linweld, 99.999%) before the container was finally pressurized to ca. 345 bar (5000 psi) H<sub>2</sub> pressure. High-energy milling was carried out for various time intervals at 300 rpm. To achieve effective milling and prevent excessive heating of the containers during milling, the milling direction was alternated every two minutes with an intermittent pause of one minute.

## 2.2. X-ray powder diffraction analysis

The progress of the reaction, as well as the yields and purity of the final products were monitored by powder X-ray diffraction (PXRD) analysis at room temperature on a PANalytical X'PERT powder diffractometer using Cu-K $\alpha_1$  radiation in the  $2\theta$  range from 10° to 80° at a step size of 0.02°. To prevent oxidation from atmospheric oxygen and moisture, a polyimide (Kapton) film was used during the data acquisition, which resulted in an amorphous-like background in the PXRD patterns most notable in the  $2\theta$  range of 13–20°.

## 2.3. Solid-state NMR spectroscopy

Solid-state (SS)NMR experiments were performed at 9.4 T using an Agilent DD2 spectrometer, equipped with a 3.2-mm magic angle spinning (MAS) probe, tuned to 104.2, 105.8, and 400.0 MHz for  $^{27}\text{Al}$ ,  $^{23}\text{Na}$ , and  $^1\text{H}$ , respectively. To maximize quantitative accuracy, direct polarization (DP)MAS spectra were collected under 16 kHz MAS, using a single, short excitation pulse of 0.15  $\mu\text{s}$  at an effective RF magnetic field strength of 150 kHz (corresponding to a flip angle of 8.1°) [25,26]. For  $^{27}\text{Al}$  experiments, 1024 scans were collected with a relaxation delay of 3 s, whereas 512 scans and a delay of 15 s were employed in  $^{23}\text{Na}$  experiments. In all cases,  $^1\text{H}$  two-pulse phase-modulation (TPPM) decoupling [27] was applied at a frequency of 64 kHz throughout acquisition. The resulting  $^{27}\text{Al}$  and  $^{23}\text{Na}$  spectra were referenced to 1.0 M aqueous solutions of  $\text{Al}(\text{NO}_3)_3$  and  $\text{NaCl}$ , respectively – both of which produce a single sharp signal at 0 ppm [28]. Finally, due to the air and/or moisture sensitivity of the materials studied, all samples were packed in MAS zirconia rotors in a glove box under argon atmosphere and sealed with gas-tight, double O-ring caps, as previously described.

## 2.4. Temperature Programmed Desorption

For thermal desorption measurements, as-prepared powder samples (~0.2 g) were pelletized and loaded in a custom-built autoclave within a glove box, followed by evacuation in an automatic Sievert's type volumetric gas sorption analyzer (PCTPro-2000, Setaram). Volume calibration of the free sample space was carried out with three helium absorption-desorption cycles over a period of 30–40 min during which time the temperature was maintained at 25 °C. During the desorption measurements, samples were heated at a rate of 4 °C/min up to 300 °C, followed by equilibration at that temperature until no further change in the pressure was noticeable. The composition of desorbed gases was analyzed by mass spectrometry using RGA100 residual gas analyzer coupled with the PCTPro-2000.

### **3. Results and Discussion**

#### **3.1. Determination of the initial reaction conditions**

Earlier studies have demonstrated that mechanochemical synthesis of alane via metathesis reaction of  $\text{AlCl}_3$  with Li precursors ( $\text{LiAlH}_4$  or  $\text{LiH}$ ) affords an easy and practical method of producing adduct-free  $\text{AlH}_3$  in large quantities [21–24]. However, each precursor presents its own peculiarities in terms of reaction temperature, pressure or the composition of the reaction mixture. For example, the 3:1 molar mixture of  $\text{LiAlH}_4$  and  $\text{AlCl}_3$  could be converted in quantitative yields to  $\text{AlH}_3$  only when the solid-state reaction was performed under gas pressure exceeding a threshold gas pressure at room temperature [21,22] or at 77 K [23,24]. Another variable is the milling energy, which unfavorably affects the time needed to complete the reaction [22]. Our systematic study of the  $\text{LiH-AlCl}_3$  system has indicated that the reaction pathway is critically dependent on the composition of the reaction mixture. Briefly, when a stoichiometric 3:1 molar mixture is used to start the reaction, elemental Al

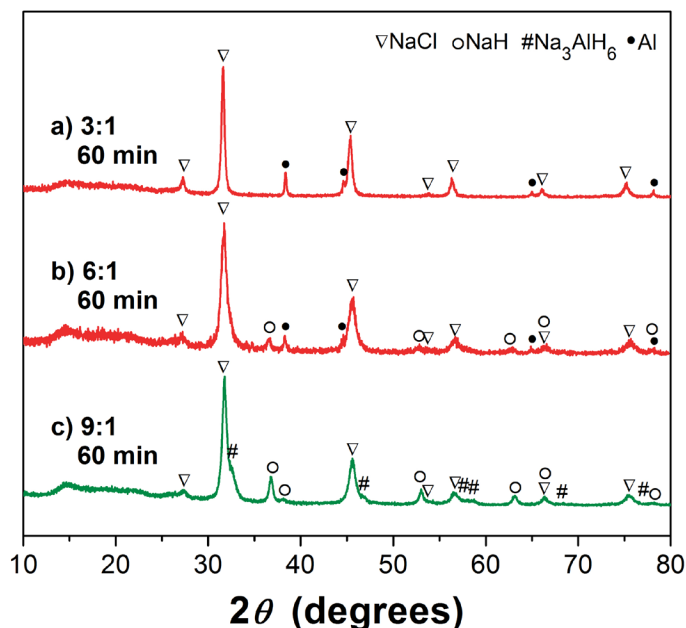
(Al<sub>M</sub>) is formed irrespective of the applied gas pressure during ball milling. However, the reaction pathway leading to AlH<sub>3</sub> is favored only when the LiH concentration in the starting mixture is 9 moles or more per mole of AlCl<sub>3</sub> and the reaction is performed above a threshold pressure [21].

The complexity of these reactions and their uniqueness with respect to the precursors, suggest that the earlier results may not be fully applicable to the NaH-AlCl<sub>3</sub> system, which motivated our present investigation. As in case of the LiH-AlCl<sub>3</sub> system, initially reactions in the NaH-AlCl<sub>3</sub> system were performed for NaH:AlCl<sub>3</sub> molar ratios varying between 3:1 to 9:1 to determine the stoichiometry necessary to completely suppress the formation of Al<sub>M</sub>. Accordingly, a 3:1 molar mixture of NaH and AlCl<sub>3</sub> was prepared and processed mechanochemically at 300 rpm under ca. 345 bar of H<sub>2</sub> pressure. After 60 min of milling (standard milling time used for all reactions unless stated otherwise) only Al<sub>M</sub> and NaCl were obtained as major products (Eq. 1), which is in agreement with the similar reaction between LiH and AlCl<sub>3</sub>.



The PXRD pattern for the corresponding reaction is shown in Fig. 1 (pattern a). As in the case of the LiH-AlCl<sub>3</sub> system, it was then reasoned that the presence of excess NaH in the starting mixture may be required to alter the reaction pathway by blocking the likely formation of unstable intermediates that immediately decompose to Al<sub>M</sub>. Thus, varying ratios of NaH and AlCl<sub>3</sub> (4:1, 6:1 and 9:1) were examined, and it was observed that the optimum composition that prevents the formation of Al<sub>M</sub> is close to 9:1 (Fig. 1, pattern c). All reactions with a lower NaH content than the determined optimum resulted in the formation of

$\text{Al}_M$  and the presence of unreacted  $\text{NaH}$ , as shown in Fig. 1 (b) for the starting mixture of 6:1. Thereafter, the sample with 9:1 composition was reexamined at various stages of milling and the products obtained after 60 min of milling were subsequently used for further mechanochemical processing with additional  $\text{AlCl}_3$  to yield  $\text{AlH}_3$  and  $\text{NaCl}$  as final products.



**Fig. 1** Powder X-ray diffraction patterns corresponding to as-milled samples with  $\text{NaH}:\text{AlCl}_3$  starting molar ratios of a) 3:1, b) 6:1 and c) 9:1 after ball milling for 60 min under 345 bar of  $\text{H}_2$  at a milling speed of 300 rpm and ball to sample mass ratio (B/S) of  $\sim 140$ .

### 3.2. The 9:1 reaction of $\text{NaH}$ and $\text{AlCl}_3$ (stage 1)

Once the optimal starting composition of  $9\text{NaH}:\text{AlCl}_3$  was determined, the progress of the reaction, the formation of the intermediate compounds and the final products were analyzed by PXRD as a function of the milling time ( $\tau_{\text{BM}}$ ). According to the PXRD pattern shown in Fig. 2 for  $\tau_{\text{BM}} = 4$  min (pattern a), four sets of Bragg peaks are identified. Two of those sets



correspond to NaCl (with the major peaks at  $2\theta \approx 32$  and  $46^\circ$ ) [29] and orthorhombic NaAlCl<sub>4</sub> (two sets of clearly identifiable Bragg peaks are at  $2\theta \approx 16\text{--}19^\circ$  and  $28\text{--}32^\circ$ ) [30,31] as the major products. The other two sets correspond to the still unreacted NaH (with the most intense Bragg peaks at  $2\theta \approx 37$  and  $53^\circ$ ) [32] and AlCl<sub>3</sub> (the major Bragg peak is at  $2\theta \approx 15^\circ$ ) [33]. Upon further milling ( $\tau_{\text{BM}} = 7$  min), the peak intensities of NaH decrease and those of AlCl<sub>3</sub> disappear completely. At  $\tau_{\text{BM}} = 10$  and 15 min, the PXRD patterns clearly show the formation of NaAlH<sub>4</sub> [34] and Na<sub>3</sub>AlH<sub>6</sub> [35] with a concomitant increase in NaCl and decrease in the NaAlCl<sub>4</sub> that was formed early in the reaction (Fig. 2, patterns c and d). Although the mechanism of formation of NaAlCl<sub>4</sub> is not currently understood, it is one of the most crystalline intermediates formed that could be easily observed by powder XRD. Its formation implies the concomitant presence of other ternary or quaternary intermediates, such as AlCl<sub>3-x</sub>H<sub>x</sub> (x=3 or less) or Na-Al-Cl-H species (designated as phase *X* Eq. 2a):

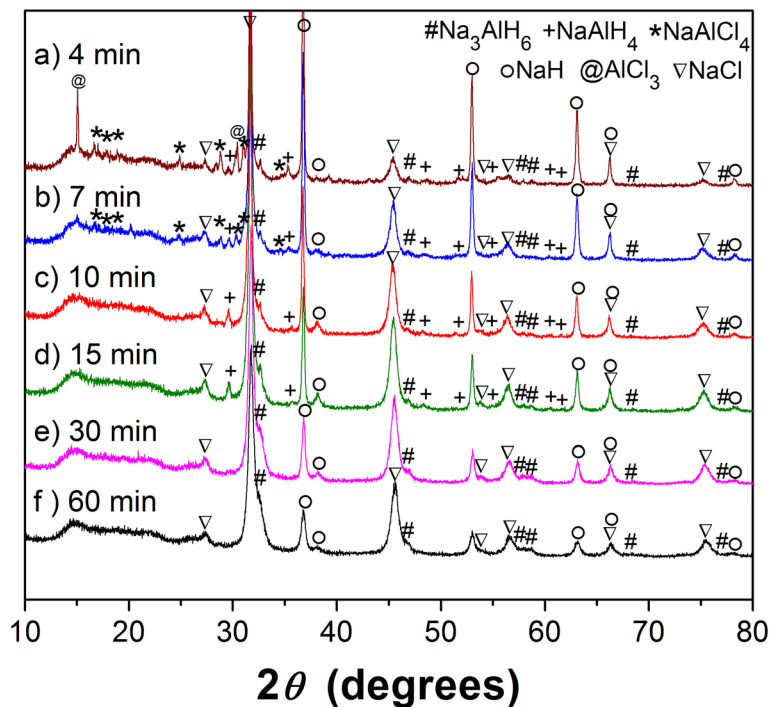


The presence of such species is difficult to confirm because of their X-ray amorphous nature, transient nature and small concentration. Identification of such species and detailed mechanistic studies require highly precise and quantitative SSNMR analysis and will be described in a separate study. Meanwhile, the presence of NaAlH<sub>4</sub> and Na<sub>3</sub>AlH<sub>6</sub> after 60 minutes of milling can be explained by the following two well-known reactions [36]:



As noted above, AlH<sub>3</sub> shown in the reaction (3a) most likely originate from a reaction shown in the reaction (2), which is not yet fully established because of lack of complete

characterization of the nature of products.

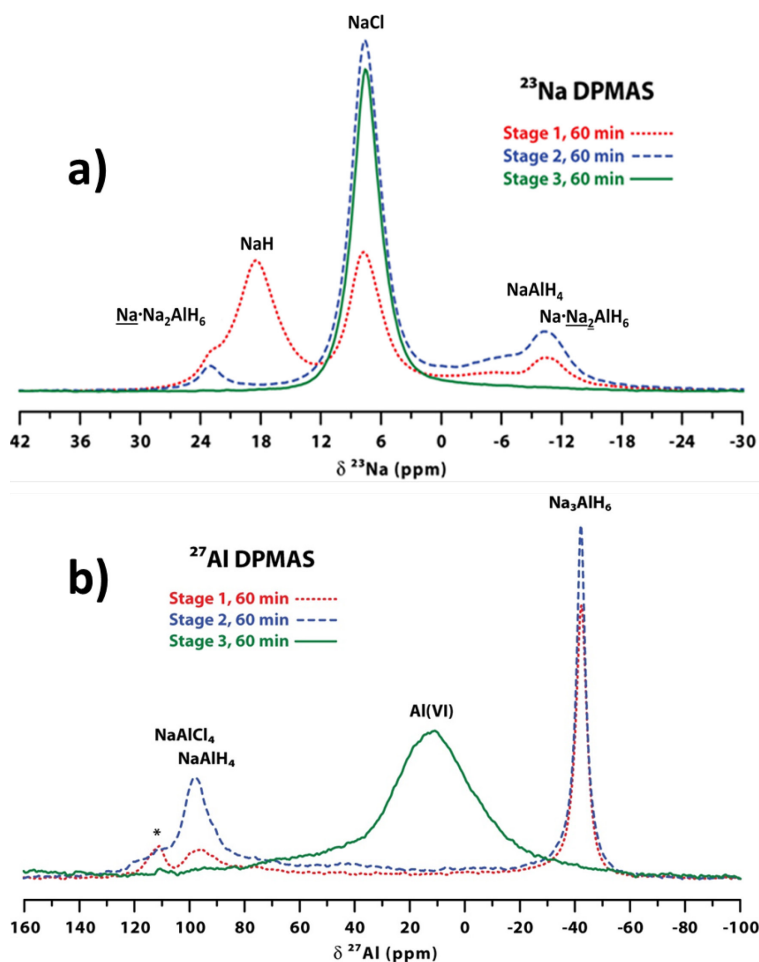


**Fig. 2** Powder X-ray diffraction patterns (a-f) of samples obtained from the 9:1 mixture of NaH and  $\text{AlCl}_3$  after ball-milling for the indicated time intervals under 350 bar  $\text{H}_2$  with a milling speed of 300 rpm and a B/S of  $\sim 140$ . Note that this reaction corresponds to the first stage of the stepwise mechanochemical synthesis of alane, as described in the text.

After further processing ( $\tau_{\text{BM}} = 30$  and 60 min), the phases detected by PXRD are  $\text{Na}_3\text{AlH}_6$ , NaCl and unreacted NaH (Fig. 2, patterns e and f), which does not change with processing beyond 60 min indicating that the reaction has reached completion. The nearly complete consumption of  $\text{NaAlH}_4$  formed early in the reaction, can likewise be understood on the basis of Eq. 3b, marking the end of stage 1.

Solid-state NMR measurements were carried out to confirm the findings from X-ray diffraction and, more importantly, to ascertain whether there were any X-ray-amorphous phase(s) are present in the sample. The  $^{23}\text{Na}$  DPMAS spectrum of the 9:1 sample at  $\tau_{\text{BM}} = 60$  min, revealed

the presence of three different Na-containing species (Fig. 3a, stage 1). These include unreacted NaH represented by the resonance centered around 19 ppm [37], a signal originating from NaCl centered around 7 ppm, and two weak resonances at approximately 23 and -10 ppm corresponding to the two  $^{23}\text{Na}$  sites of newly formed  $\text{Na}_3\text{AlH}_6$  species [38]. The  $^{27}\text{Al}$  DPMAS spectrum of the same sample (Fig. 3b, stage 1) confirms the presence of  $\text{Na}_3\text{AlH}_6$  with an intense signal centered at -42 ppm [38]. Another hydride observed at this stage is unreacted  $\text{NaAlH}_4$  (as indicated by the weak signal at ~96 ppm) [38], though this species comprises only a minor fraction of the DPMAS intensity. Thus, solid-state NMR results corroborate the PXRD analysis.



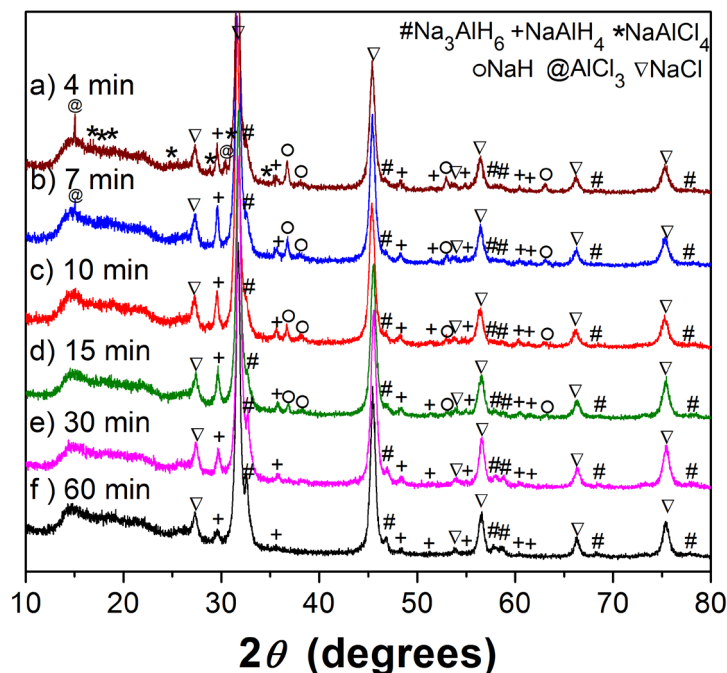
**Fig. 3**  $^{23}\text{Na}$  (a) and  $^{27}\text{Al}$  (b) DPMAS spectra of samples obtained after each stage of processing for 60 min. Stages 1, 2 and 3 denote respectively samples with 9:1, 5:1 and 3:1 ratio of  $\text{NaH}:\text{AlCl}_3$ . An asterisk (\*) in (b) marks a spinning sideband arising from  $\text{Na}_3\text{AlH}_6$ .

### 3.3. The 5:1 reaction of $\text{NaH}$ and $\text{AlCl}_3$ (stage 2)

Further, 2 molar equivalents of  $\text{AlCl}_3$  were added to the products obtained from the 9:1 reaction of  $\text{NaH}$  and  $\text{AlCl}_3$  ( $\text{Na}_3\text{AlH}_6$ ,  $\text{NaCl}$  and  $\text{NaH}$  at  $\tau_{\text{BM}} = 60$  min) to reach the desired  $\text{NaH}:\text{AlCl}_3$  ratio of 3:1. After milling for 30 min under 345 bar of  $\text{H}_2$ , a dark grey powder was obtained, again indicating the formation of  $\text{Al}_\text{M}$ , which was also confirmed by PXRD analysis (not shown). Based on the previous experience with the  $\text{LiH}-\text{AlCl}_3$  system, in a separate experiment, the amount of additional  $\text{AlCl}_3$  was then reduced to 1.25 molar equivalents instead of 2 to achieve a cumulative  $\text{NaH}:\text{AlCl}_3$  ratio of 4:1 rather than the target ratio of 3:1. However, contrary to the  $\text{LiH}-\text{AlCl}_3$  system, this mixture still did not produce the anticipated result, and instead led to  $\text{Al}_\text{M}$ . Only when the amount of  $\text{AlCl}_3$  added was reduced to 0.8 molar equivalents (resulting in an overall  $\text{NaH}:\text{AlCl}_3$  ratio of 5:1), did the reaction proceed without the formation of  $\text{Al}_\text{M}$ . The progress of the 5:1 reaction was similarly monitored at same time points using PXRD, the results of which are shown in Fig. 4 and described below.

For  $\tau_{\text{BM}} = 4$  min, the PXRD data (Fig. 4, pattern a) show the Bragg peaks corresponding to the freshly formed  $\text{NaAlCl}_4$  and  $\text{NaAlH}_4$  and the unreacted  $\text{NaH}$  and  $\text{AlCl}_3$  along with previously present  $\text{NaCl}$  and  $\text{Na}_3\text{AlH}_6$ . Upon further milling ( $\tau_{\text{BM}} = 7\text{--}30$  min), during the early period the peaks of  $\text{AlCl}_3$  disappear, while peak intensities of  $\text{NaH}$  gradually decrease with concomitant increase in those corresponding to  $\text{NaAlH}_4$ . At a later period ( $\tau_{\text{BM}} = 60$  min), the phases detected by PXRD are  $\text{NaAlH}_4$ ,  $\text{Na}_3\text{AlH}_6$  and  $\text{NaCl}$  (Fig. 4, pattern f).

According to the PXRD pattern, NaH is completely consumed to produce  $\text{Na}_3\text{AlH}_6$  according to Eq. 3b. A small portion of  $\text{NaAlH}_4$  is left in the sample as the amount of NaH is now limited compared with the 9:1 reaction.



**Fig. 4** Powder X-ray diffraction patterns (a-f) of samples obtained from the 5:1 mixture of NaH and  $\text{AlCl}_3$  after ball-milling for the indicated time intervals under 350 bar  $\text{H}_2$  with a milling speed of 300 rpm and a B/S of  $\sim 140$ . Note that this starting composition (obtained by adding 0.8 moles of  $\text{AlCl}_3$  to the as-milled 9:1 products shown in Fig. 2) corresponds to the second stage of the stepwise mechanochemical synthesis of alane, as described in the text.

For the sample with  $\tau_{\text{BM}} = 60$  min, analysis of the  $^{23}\text{Na}$  and  $^{27}\text{Al}$  SSNMR spectra (Fig. 3, stage 2) provides consistent and comparable results to the data obtained from PXRD (Fig. 4, pattern f). In the  $^{23}\text{Na}$  DPMAS spectrum, a strong presence of NaCl is observed at 8 ppm. The peak at  $\sim 23$  ppm corresponds to one of the two  $^{23}\text{Na}$  sites of  $\text{Na}_3\text{AlH}_6$  species. The second site of  $\text{Na}_3\text{AlH}_6$  at around  $-10$  ppm, however, strongly overlaps with the signal produced by  $\text{NaAlH}_4$ , the presence of which is confirmed by a signal in the  $^{27}\text{Al}$  DPMAS spectrum centered at  $\sim 96$  ppm. As expected, the only other Al-containing species observed in

the  $^{27}\text{Al}$  spectrum is  $\text{Na}_3\text{AlH}_6$ , as indicated by the intense signal at  $-42$  ppm [38]. Thus, in the second stage, the reaction progresses through a similar set of intermediates as observed for stage 1.

### 3.4. The 3:1 reaction of NaH and $\text{AlCl}_3$ (stage 3)

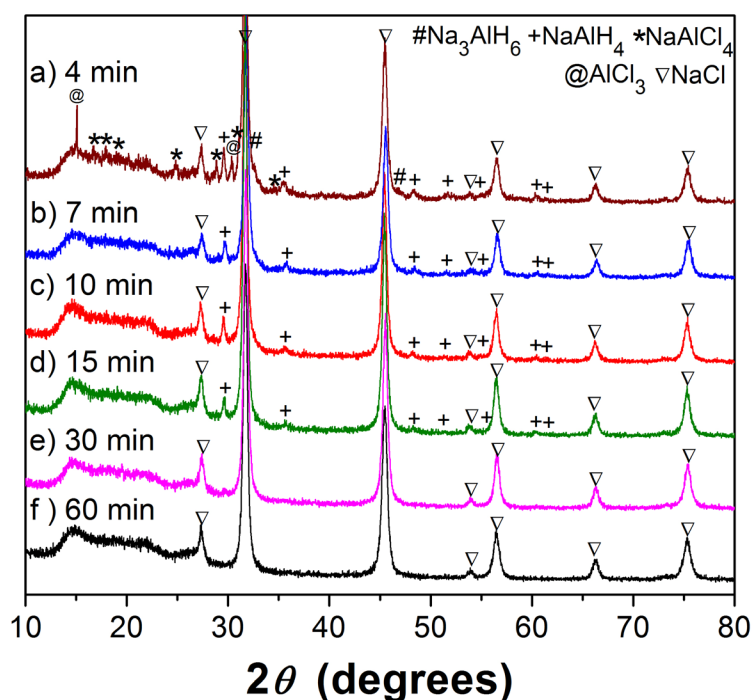
Finally, in order to obtain alane as the end product, the remaining 1.2 molar equivalent of  $\text{AlCl}_3$  was added to the mixture obtained upon completion of stage 2 of processing. Thereafter, the resulting mixture (now with what would have been a net composition of  $3\text{NaH}:1\text{AlCl}_3$ ) was processed as in the previous two stages.

Like before, the powder XRD pattern of the products at  $\tau_{\text{BM}} = 4$  min (Fig. 5, pattern a) shows Bragg peaks corresponding to  $\text{NaCl}$ ,  $\text{NaAlH}_4$ , and  $\text{Na}_3\text{AlH}_6$  present from the previous stages, partially unreacted  $\text{AlCl}_3$  and the newly formed  $\text{NaAlCl}_4$  phase. The apparently weaker Bragg peak intensities observed for  $\text{NaAlCl}_4$  in this case are because of the relatively higher concentration of  $\text{NaCl}$  now present in the sample when compared to previous stages. At  $\tau_{\text{BM}} = 7$  min (Fig. 5, pattern b), the diffraction peaks from  $\text{NaAlCl}_4$  and  $\text{Na}_3\text{AlH}_6$  vanish, whereas upon further milling ( $\tau_{\text{BM}} = 10\text{--}30$  min), the peaks corresponding to  $\text{NaAlH}_4$  start to decrease as well. Finally, at  $\tau_{\text{BM}} = 60$  min, the only phase detected by PXRD is  $\text{NaCl}$  (Fig. 5, pattern f).

Although no Bragg peaks corresponding to any of the known polymorphs of alane are observed in the diffraction patterns, the absence of elemental aluminum and any starting precursors or intermediate compounds suggest that the reaction proceeded as intended, which we further corroborated by SSNMR. Indeed, the  $^{23}\text{Na}$  DPMAS spectrum of the final product features a single peak centered at 7 ppm, representing  $\text{NaCl}$  (Fig. 3a, stage 3). A single broad

peak is also observed in the corresponding  $^{27}\text{Al}$  DPMAS spectrum (Fig. 3b, stage 3), with the shift of  $\sim 13$  ppm which is characteristic of hexa-coordinated Al. These spectra confirm that all starting precursors and intermediates have been consumed thereby unambiguously confirming the completion of the reaction. The observed  $^{27}\text{Al}$  shift centered at  $\sim 13$  ppm is broad and includes the 5.8-36.0 ppm range reported for  $\alpha$ ,  $\beta$ , and  $\gamma$  polymorphs of alane by Bowman and Hwang [39], and, within experimental error, matches the value of 14.8 ppm reported by Humphries *et al* for the  $\alpha'$  polymorph of alane ( $\alpha'$ - $\text{AlH}_3$ ) [40].

The absence of Bragg peaks attributable to  $\text{AlH}_3$  implies that it is X-ray-amorphous, or nanocrystalline in nature. It is noted that as follows from X-ray powder diffraction, the crystallinity of alane synthesized by mechanochemical metathesis at room temperature is sensitive to the milling conditions e.g. the time of milling and the process control agent(s) used during the reaction. In our previous work on  $\text{LiAlH}_4\text{-AlCl}_3$  system [22], 3:1 molar reactions carried out at room temperature under high gas pressure yield a well-crystallized  $\alpha$ -alane after 60 min. However, when the same reaction is carried out under ambient pressure, lower milling intensity required to avoid formation of metallic Al leads to a nearly 10-fold increase in the reaction time. The final product is identified as x-ray amorphous alane by SSNMR present in quantitative yield as determined by volumetric analysis during  $\text{H}_2$  desorption [22]. Further, room temperature mechanochemical reactions with excess  $\text{LiAlH}_4$  (e.g. 4:1–6:1 molar) produce a highly crystalline alane, which shows  $^{27}\text{Al}$  NMR signals [41] that are in an excellent agreement with the results reported here. Finally, similar metathesis reactions, particularly with  $\text{LiAlH}_4$  and  $\text{NaAlH}_4$  at liquid  $\text{N}_2$  temperature, yield alane with better crystallinity [23, 42] compared to room temperature milling under high gas pressure [22].

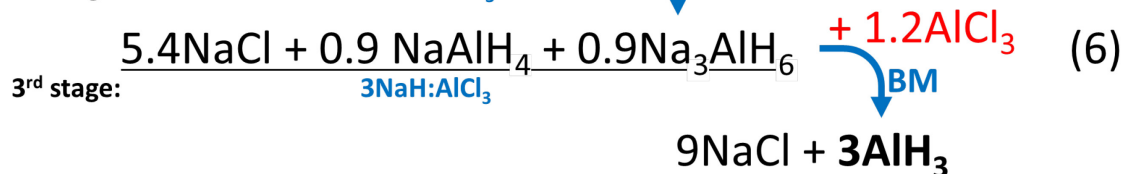
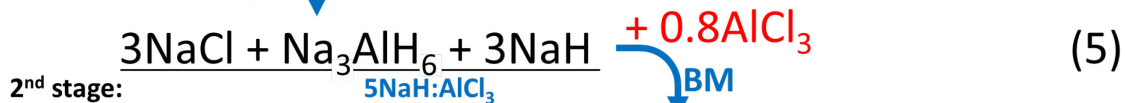


**Fig. 5** Powder X-ray diffraction patterns (a-f) of samples obtained from the 3:1 mixture of NaH and  $\text{AlCl}_3$  after ball-milling for the indicated time intervals under 350 bar  $\text{H}_2$  with a milling speed of 300 rpm and a B/S of  $\sim 140$ . Note that this starting composition (obtained by adding 1.2 moles of  $\text{AlCl}_3$  to the as-milled 5:1 products shown in Fig. 4) corresponds to the third and final stage of the stepwise mechanochemical synthesis of alane, as described in the text.

### 3.5. Overall reaction scheme

Based on the PXRD and SSNMR characterization, the reaction progress as studied for the indicated compositions (optimized for each step to prevent decomposition to elemental Al) may be summarized as follows:

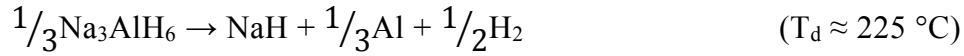
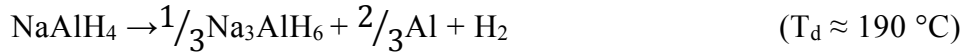




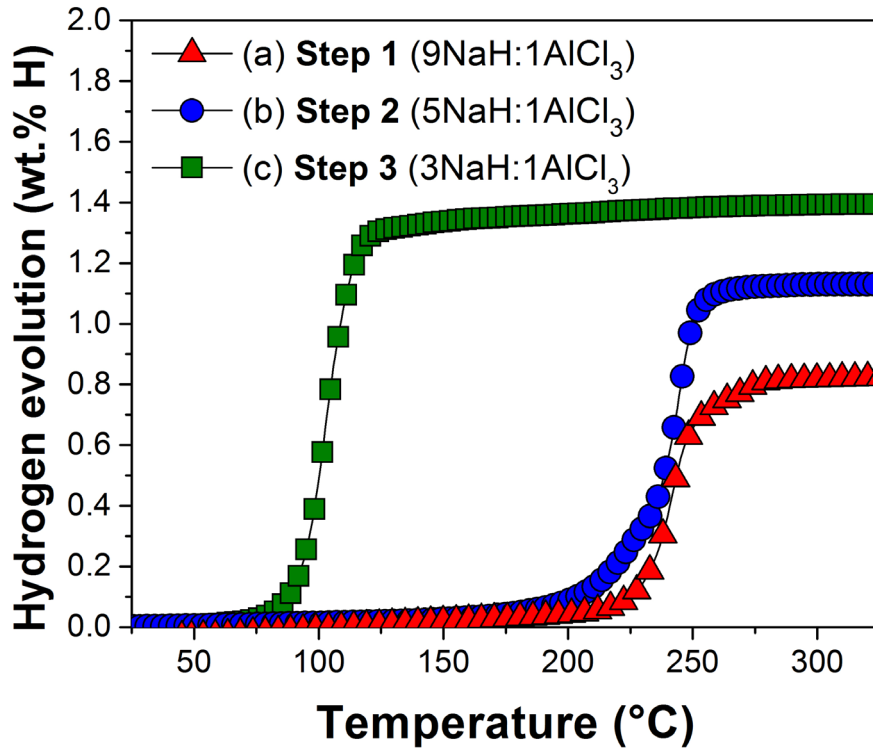
### 3.6. Temperature-programmed desorption (TPD) analysis

Judging only by the color of the sample, it is evident that all, or at least the majority of hydrogen is retained throughout the three stages of milling. As noted elsewhere [21,22], any loss of hydrogen during the solid-state metathesis reaction of an alkali metal hydride or alanate with aluminum halide salts results in the formation of elemental aluminum, which imparts dark gray color to the sample. In the present work, during the entire course of the reaction, the 9:1 and subsequent 5:1 and 3:1 reaction mixtures maintained a grayish white to light grey color indicating that very little, if any, elemental Al had formed. To further confirm the amount of hydrogen present in the sample after completion of each step, the volumetric desorption experiments were performed. Figure 6 (plots a, b and c) compares the decomposition profiles of the products obtained after each stage of processing at  $\tau_{\text{BM}} = 60$  min. For the 9:1 sample obtained after the first stage, a single-step desorption curve with an onset desorption temperature ( $T_d$ ) of  $\approx 225$  °C, is in excellent agreement with the  $T_d$  reported for pristine  $\text{Na}_3\text{AlH}_6$  [43]. The measured equilibrium hydrogen content of *ca.* 0.81 wt.% H is in nearly quantitative agreement with the ratio of the products described in Eq. 4 ( $3\text{NaCl} + \text{Na}_3\text{AlH}_6 + 3\text{NaH}$ ) that altogether are expected to release 0.85 wt.% H, considering that the decomposition of NaH can only occur at temperatures exceeding 450 °C [44].

The products obtained after the second stage of processing represented by Eq. 5 (Fig. 6 plot b) have a two-step decomposition profile with  $T_d$ 's close to 200 °C and 230 °C. This is also in an excellent agreement with the decomposition pathway of  $\text{NaAlH}_4$  which proceeds as a two-step reaction below 400 °C [45]:



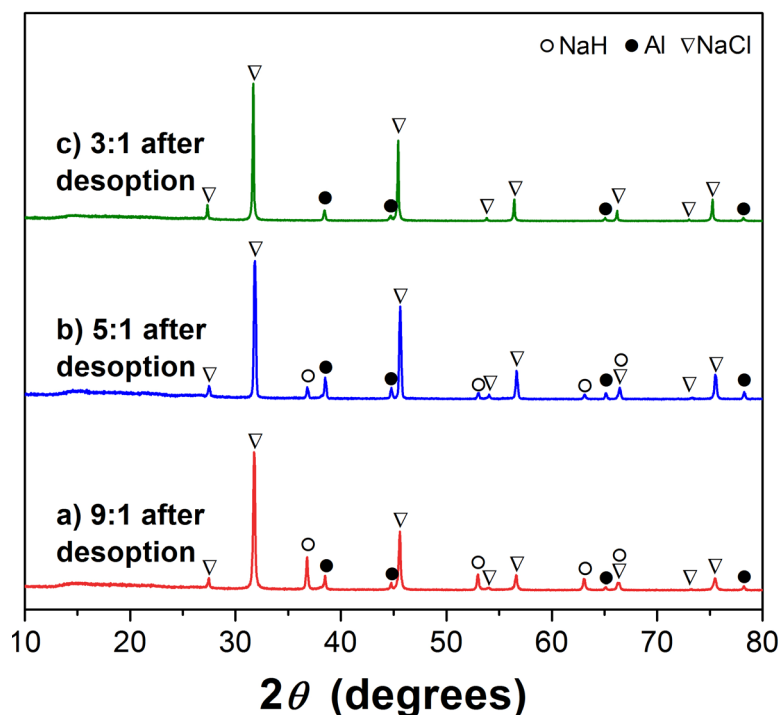
The net hydrogen evolution of 1.14 wt.% hydrogen matches the expected value of 1.19 wt.% hydrogen, assuming that the reaction described by Eq. 5 proceeds to completion ( $5.4\text{NaCl} + 0.9\text{NaAlH}_4 + 0.9\text{Na}_3\text{AlH}_6$ ). It should be noted that the first dehydrogenation step is not distinctly noticeable, mainly due to a sluggish desorption kinetics of  $\text{NaAlH}_4$  [43].



**Fig. 6** Temperature-programmed desorption profiles obtained for samples of the reaction mixtures resulting from NaH:AlCl<sub>3</sub> starting ratios of (a) 9:1 (b) 5:1, and (c) 3:1 after 60 min of ball milling under 350 bar H<sub>2</sub> with a milling speed of 300 rpm and a B/S of ~140. Samples correspond (respectively) to the final products obtained upon completion of the first, second, and final stages of the stepwise mechanochemical synthesis of alane, as described in the text and shown in Eqs 2, 3, and 4.

Finally, curve (c) in Fig. 6 represents the decomposition profile of the products from the reaction described in Eq. 6. The one-step decomposition with a T<sub>d</sub> of ca. 90 °C is as typically expected for AlH<sub>3</sub> [46], and the measured hydrogen capacity corresponding to 1.39 wt.% hydrogen is practically quantitative for the 3:1 molar mixture of NaCl and AlH<sub>3</sub> (1.46 wt. % H). Based on the desorption results and taking into account the observed evolution of the reaction products after the final addition of AlCl<sub>3</sub> (Figs. 3 and 5), which confirms the complete consumption of AlCl<sub>3</sub> between 4 and 7 min of the milling and eventual appearance and consumption of intermediate alanates, we confirm that hydrogen evolution occurs from alane formed mechanochemically rather than from possible thermally-induced reactions of alanates and AlCl<sub>3</sub> during heating. In all three cases, mass-spectroscopic analyses showed that H<sub>2</sub> constituted 99.7 % or more of the gases released, the rest being residual air.

The powder XRD analyses of desorbed samples from first and second stages of processing showed the Bragg peaks corresponding to elemental Al, NaH and NaCl (Fig. 7, patterns a and b). However, the final stage sample after desorption shows only elemental Al and NaCl (Fig. 7, pattern c), which suggests that NaH was completely consumed during the mechanochemical processing and that all of the alanates formed as intermediates during the first two stages were transformed into alane.



**Fig. 7** Powder X-ray diffraction patterns of products obtained after complete desorption (see Fig. 6) of as-synthesized samples with (a) 9:1, (b) 5:1 and (c) 3:1 molar ratio of NaH and  $\text{AlCl}_3$ .

Finally, although a nearly quantitative conversion of  $\text{AlCl}_3$  to alane can be achieved in a relatively simple solvent-free process, the product of the mechanochemical synthesis contains 75 mol. % (85.4 wt.%) of sodium chloride as a byproduct. Even though NaCl is benign, it must be separated from alane before the latter can be used as high-capacity source of hydrogen. While the separation of alane from NaCl is not the focus of this work, both chemical and physical separations should be possible. Apart from solvent-extraction of  $\text{AlH}_3$ , more benign physical separation techniques based on difference in densities of alane ( $1.49 \text{ g/cm}^3$ ) and NaCl ( $2.16 \text{ g/cm}^3$ ) should be possible.

### 3.7. Reaction mechanisms

Apparently, the presence of excess hydride source in a starting mixture can prevent decomposition to elemental Al and facilitate formation of the desired products. Similar

observations were made by Mikheeva *et al.* during their studies of the reaction between LiH and AlCl<sub>3</sub> in ethereal solution, who noticed that slow addition of AlCl<sub>3</sub> prevented decomposition of newly formed alane and improved the yield of LiAlH<sub>4</sub> [47]. Hence, similar to the previously described LiH-AlCl<sub>3</sub> system [21], the possible explanation of why the reaction between NaH and AlCl<sub>3</sub> in a 3:1 molar ratio leads to elemental Al is because of the relatively low fraction of the hydride source in the 3:1 mixture (compared to 9:1), which may not be sufficiently dispersed, leading to high local AlCl<sub>3</sub>:NaH ratios. Consequently, this may cause the decomposition of unstable chlorine-containing derivatives (*e.g.* AlCl<sub>2</sub>H and AlClH<sub>2</sub> or others that are not known) into elemental aluminum with hydrogen evolution, rather than formation of intermediate alanates NaAlH<sub>4</sub> and Na<sub>3</sub>AlH<sub>6</sub>.

#### 4. Conclusions

An efficient solvent-free mechanochemical method for the preparation of alane from NaH and AlCl<sub>3</sub> at room temperature has been developed. The reaction pathway could be altered by use of excess hydride source or in other word by limiting the concentration of AlCl<sub>3</sub> in the reaction mixture, thereby completely suppressing the decomposition to elemental Al and favoring the formation of the desired product AlH<sub>3</sub> through a series of stable alanate intermediates. Although this reaction can be carried out in organic solvents such as ether-toluene mixtures, the mechanochemical approach affords a straightforward room-temperature approach for the large-scale production of unsolvated alane. As a final note, while the concept of limiting reagent is well-known and has been widely used by chemists and biochemists to control the course of the reaction, it has not been as frequently utilized in the solid-state chemistry research. We believe this concept, as exemplified in the present work can be effectively and more generally applied to other classes of mechanochemical reactions to control pathway and alter reaction products.

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## **6. Compliance with ethical standards**

Conflict of interest

The authors declare that they have no conflict of interest.

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