

Model-free Thermodynamic Relationships for Non-stoichiometric Metal Oxides from Experimental Measurements

Anthony H. McDaniel, presenting
Sandia National Labs



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Acknowledgments to the team

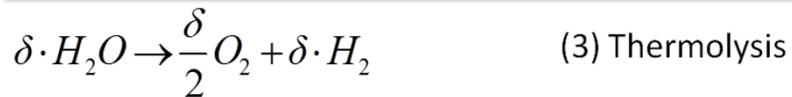
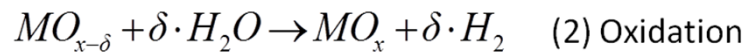
- Sandia Labs
 - Jim Miller
 - Andrea Ambrosini
 - Sean Babiniec
 - Eric Coker
- University Collaborator
 - Ellen B. Stechel (ASU)



- DOE/Fuel Cell Technologies Office
- DOE/SunShot Initiative

- Challenges for material characterization and evaluation.
 - Standard protocols for measuring data need development
 - Temperature and O_2 partial pressure ranges too narrow
 - Sample purity and experimental methods always in question
 - Benchmarked protocols for extracting properties need development
 - Thermodynamic and kinetic properties
- Extracting thermodynamic properties from (T, p_{O_2}, δ) data.
 - van't Hoff approximation with or without invoking defect models
 - Apply arbitrary or “informed” δ -dependence
 - CALPHAD (very rigorous!)
- Model-free approach to analyzing (T, p_{O_2}, δ) data.
 - $\Delta H(\delta, T)$ and $\Delta S(\delta, T)$ derived from equilibrium response surface
- US Government investments in solar H_2 production.
 - HydroGen Consortium and H2@Scale

Solar powered two-step thermochemical water-splitting cycle to produce H₂ (STCH)

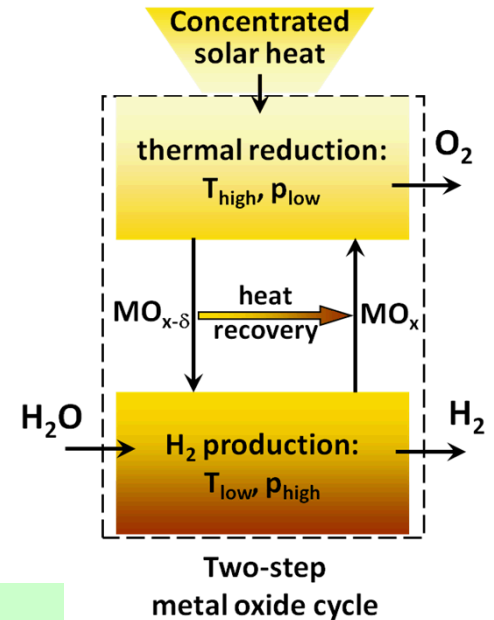


MW scale concentrating solar power facilities provide heat before making electricity



Cycle conditions and system metrics:

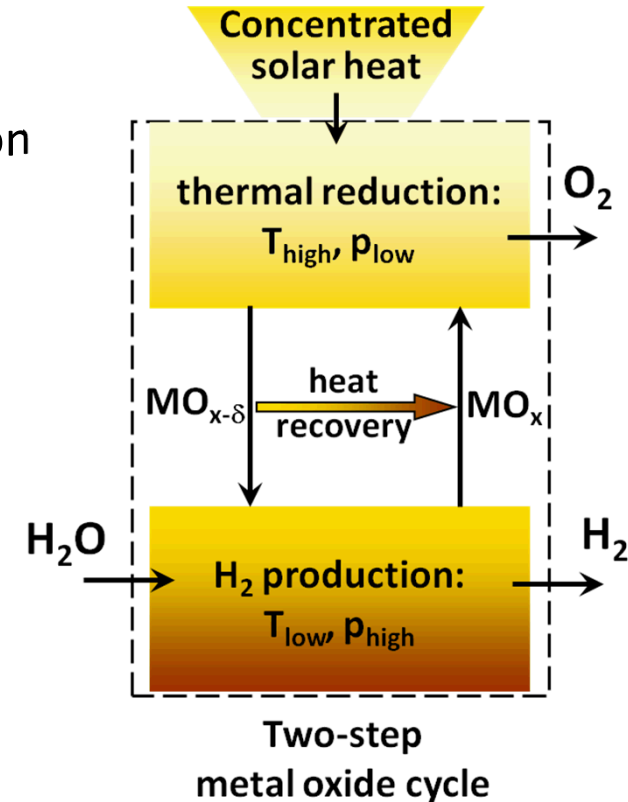
Reduction Temperature (T _{high})	<2000°C
"O" activity in reduction (p _{low})	$\mu_{gas} < \mu_{solid}$
Oxidation Temperature (T _{low})	debated
"O" activity in oxidation (p _{high})	$\mu_{gas} > \mu_{solid}$
H ₂ production rate	50-100mt/day
Solar-to-H ₂ conversion efficiency	>25%
H ₂ production cost (US DOE)	\$3/gge at plant gate



- The challenge is to develop efficient and scalable solar-powered reduction receivers and water-splitting reactors.

Miller et. al, *Advanced Energy Materials* **2013**, DOI:10.1002/aenm.201300469

- Redox thermodynamics and kinetics.
 - Critical to reactor design and efficient operation
 - Large, reversible oxygen deficiency (reduction extent)
 - Fast redox rates and matched to solar flux
- Stability and long-term durability of redox active ceramic structures.
 - Cycle life ~ 300,000 cycles (10 year life)
 - heating rates (1000°C/min)
 - Compatibility with materials of construction
- Earth abundant and easy to manufacture.



$\Delta H(\delta; T)$ to model reactor efficiency

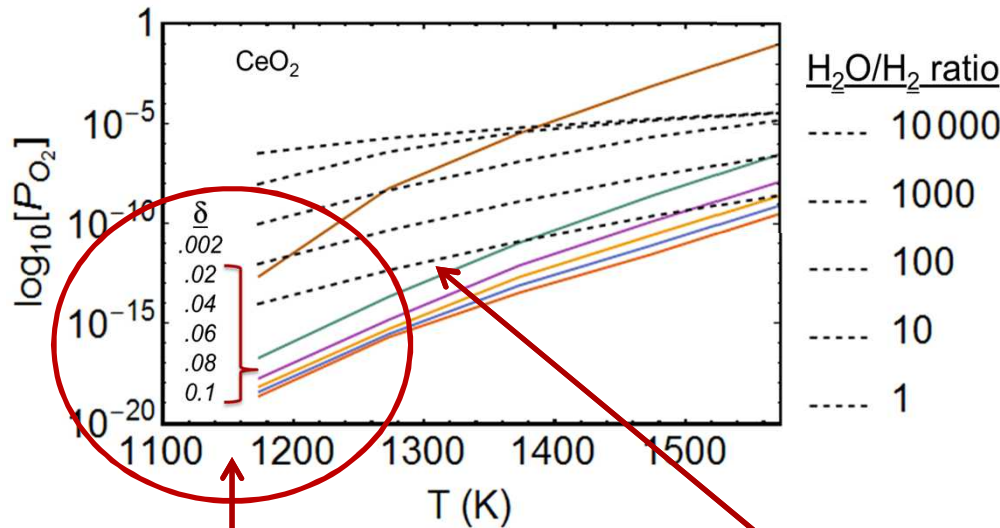
All inclusive efficiency metric

$$\eta = \left(\frac{P_{TH}}{P_S} \right) \left(\frac{LHV_{H_2}}{Q} \right) = \frac{\dot{n}_{H_2} LHV_{H_2}}{P_S} \rightarrow \dot{n}_{H_2} = \frac{P_{TH}}{Q}$$

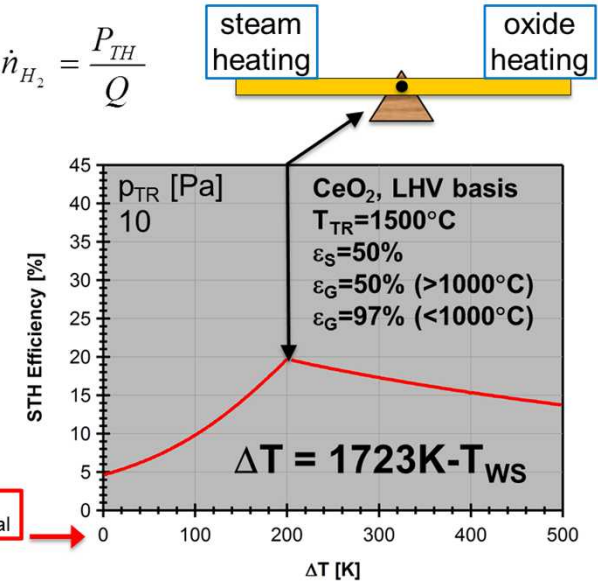
$$P_{TH} = r_{12} * r_d * t_w * A * P_S - P_{rad}$$

$$Q = Q_{TR} + Q_{SH} + Q_{AUX}$$

$\Delta H(\delta; T)$ embedded here



challenged to measure P_{O_2} - T - δ
@ low T , low P_{O_2}



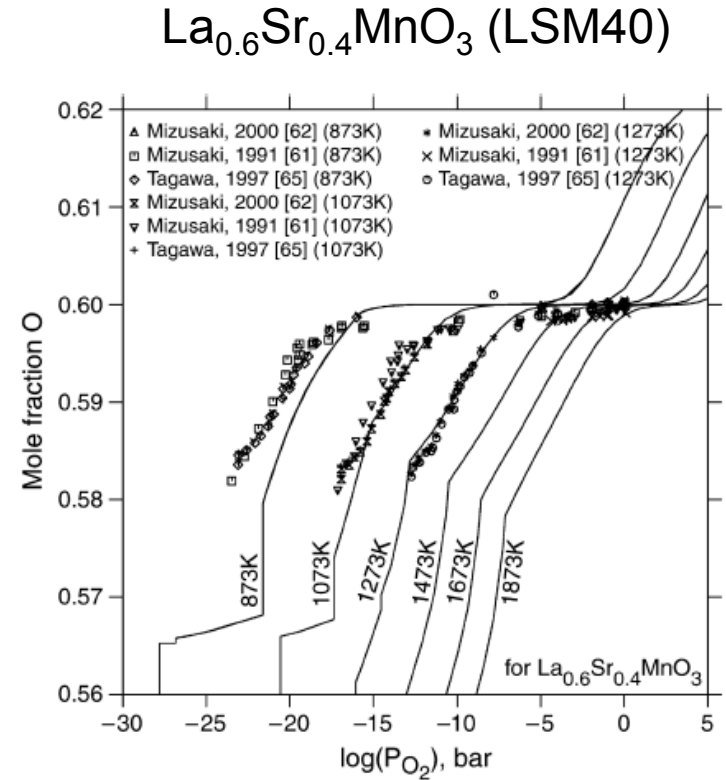
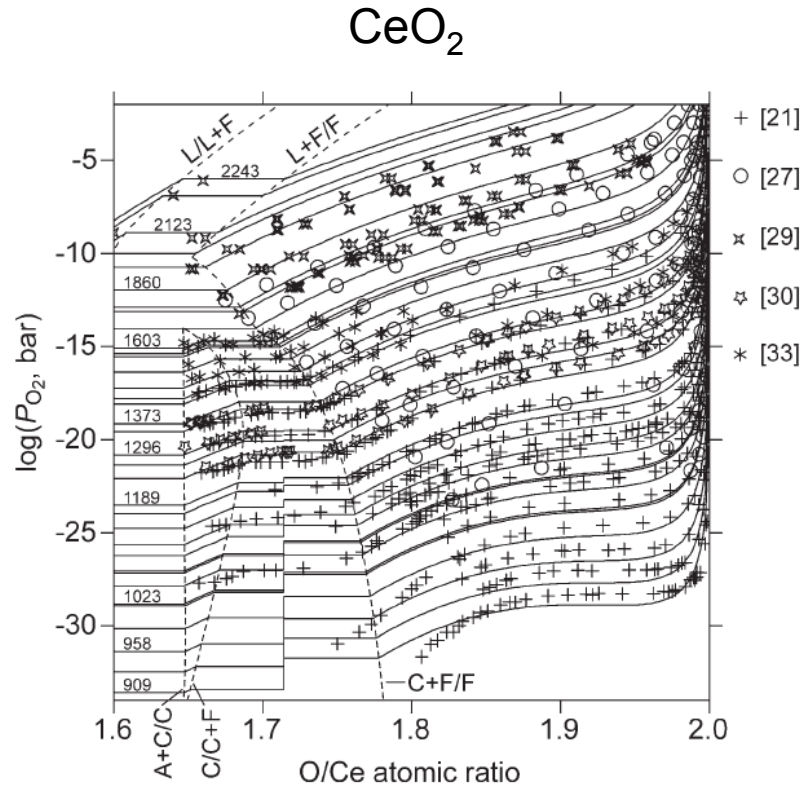
- No *a priori* assumptions about material defect behavior required to model reactor efficiency.

"O" activity in reduction (p_{low})	$\mu_{gas} < \mu_{solid}$
"O" activity in oxidation (p_{high})	$\mu_{gas} > \mu_{solid}$

Mapping the P_{O_2} -T- δ space

M. Zinkevich et al., *Solid State Ionics*. **177**, 989–1001 (2006).

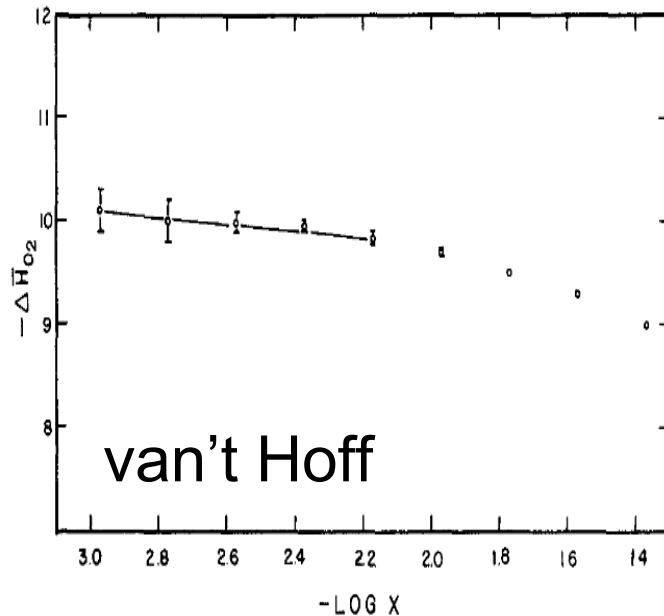
A. N. Grundy et al., *Calphad*. **28**, 191–201 (2004).



- Measure oxygen defect concentration (δ) in non-stoichiometric oxides as a function of P_{O_2} and Temperature.
 - Thermogravimetry (TGA), coulometric titration, other methods?

$\Delta H(\delta)$: from van't Hoff to CALPHAD

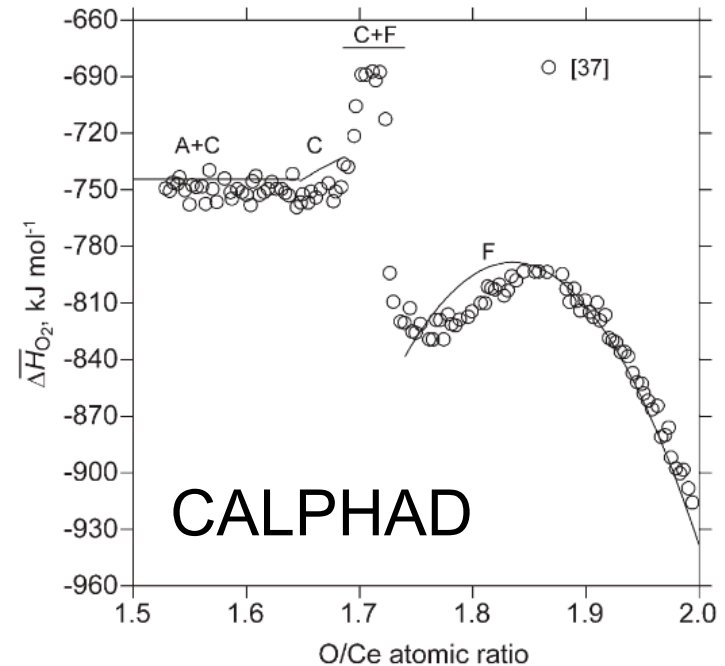
R. J. Panlener et al., *Journal of Physics and Chemistry of Solids*. **36**, 1213–1222 (1975).



- Invoke assumptions about defect behavior.
 - Species [], reactions, K_{eq} 's, etc.
- Linearize system then use slopes and/or intercepts.

M. Zinkevich et al., *Solid State Ionics*. **177**, 989–1001 (2006).

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- Combine all reported phase behavior.
 - Various approximations for phase-dependent ΔG 's
 - ΔG 's are additive

CALPHAD rigor is a lost art



M. Zinkevich et al., *Solid State Ionics*. **177**, 989–1001 (2006).

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The experimental database for Ce–O system

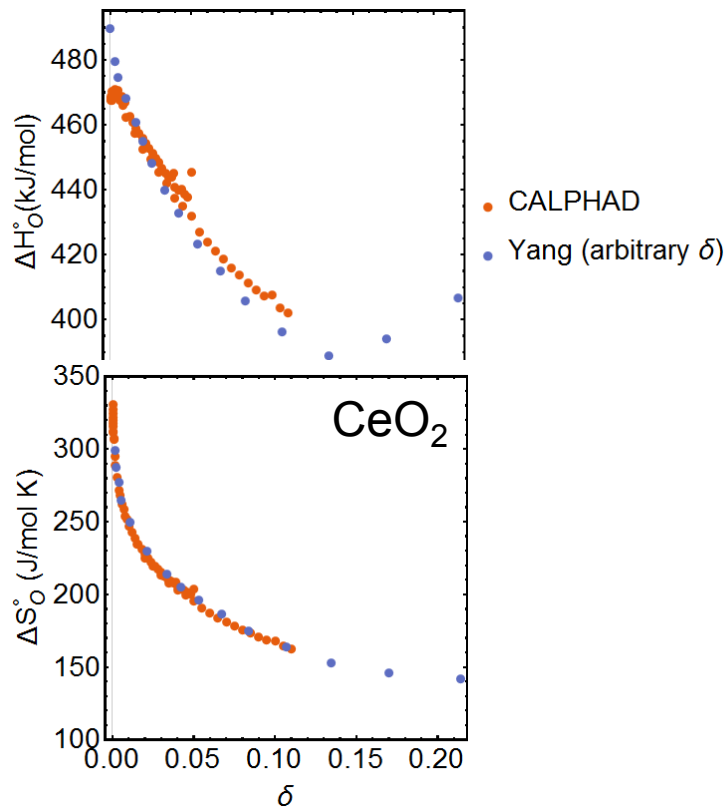
Data description	Temperature range (K)	Composition range (O/Ce)	Phases involved	Ref.
Equilibrium oxygen pressure	813–1323	1.670–1.996	F, A	[19]
Equilibrium oxygen pressure	968–1282	1.581–1.960	F, A	[20]
Equilibrium oxygen pressure	909–1442	1.500–1.997	F, C, A, Ce ₂ O ₃	[21]
Equilibrium oxygen pressure	1075–1273	1.930–1.984	F	[22]
Equilibrium oxygen pressure	1173–1573	1.727–2.000	F	[23]
Equilibrium oxygen pressure	1173–1323	1.710–2.000	F	[24]
Equilibrium oxygen pressure	1173–1823	1.723–1.992	F	[25]
Equilibrium oxygen pressure	900–1400	1.650–2.000	F, C, A, Ce ₂ O ₃	[26]
Equilibrium oxygen pressure	1023–1773	1.721–2.000	F	[27]
Equilibrium oxygen pressure	1173–1673	1.749–1.997	F	[28]
Equilibrium oxygen pressure	1750–2243	1.600–1.958	F, liquid	[29]
Equilibrium oxygen pressure	1244–1353	1.731–1.999	F, C, A, Ce ₂ O ₃	[30]
Equilibrium oxygen pressure	1273–1573	1.720–2.000	F	[31]
Equilibrium oxygen pressure	1073	1.997–2.000	F	[32]
Equilibrium oxygen pressure	1273–1603	1.647–1.994	F, C, A	[33]
Equilibrium oxygen pressure	1073–1218	1.968–1.998	F	[34]
Equilibrium oxygen pressure	1073	1.995–2.000	F	[35]
Equilibrium oxygen pressure	1073–1273	1.750–2.000	F	[36]
Partial enthalpy of oxygen dissolution	1353	1.529–1.994	F, C, A	[37]
Enthalpy of formation	298	1.500	A	[38–42]
Heat capacity	50–298	1.500	A	[43]
Heat capacity	5–300	1.500	A	[44]
Heat capacity	3–420	1.500	A	[42]
Heat capacity	578–1116	1.500	A	[45]
Heat capacity	400–1100	1.500	A	[46]
Enthalpy increment	400–1000	1.500	A	[47]
Enthalpy increment	470–883	1.500	A	[42]
Enthalpy of formation	298	2.000	F	[48,49]
Heat capacity	5–300	2.000	F	[50]
Heat capacity	608–1172	2.000	F	[51]
Heat capacity	418–758	2.000	F	[52]
Enthalpy increment	298–1800	2.000	F	[53]
Enthalpy increment	492–1141	2.000	F	[54]
Enthalpy increment	391–1624	2.000	F	[55]
Enthalpy of reaction	722	1.846	F, Ce ₁₁ O ₂₀	[56]
Enthalpy of reaction	736	1.818	F, Ce ₁₁ O ₂₀ , Ce ₂ O ₃	[56]
Enthalpy of reaction	766	1.808	F, Ce ₂ O ₃ , Ce ₂ O ₁₂	[56]
Heat capacity	348–1200	1.823–2.000	F, Ce ₁₁ O ₂₀ , Ce ₂ O ₁₂ , Ce ₂ O ₁₂	[57]
Phase diagram	293–1273	1.790–2.000	F	[58]
Phase diagram	673–901	1.800–2.000	F	[59]
Phase diagram	573–1073	1.750–1.960	F, Ce ₁₁ O ₂₀ , Ce ₂ O ₁₂ , Ce ₂ O ₁₂	[60]
Phase diagram	600–1200	1.714–2.000	F, Ce ₁₁ O ₂₀ , Ce ₂ O ₁₂ , Ce ₂ O ₁₂ , Ce ₂ O ₁₂ , Ce ₂ O ₁₂	[56,57,61]
Phase diagram	597–1064	1.698–1.800	F, Ce ₂ O ₁₂ , Ce ₂ O ₁₂ , Ce ₂ O ₁₂	[15]
Phase diagram	2123–2243	1.600–1.660	F, liquid	[29]
Phase diagram	1606–2302	1.330–1.540	A, liquid	[62]
Phase diagram	923–1386	0.002–0.008	fcc-Ce, bcc-Ce, liquid, A	[63]

~ 50 independent observations!

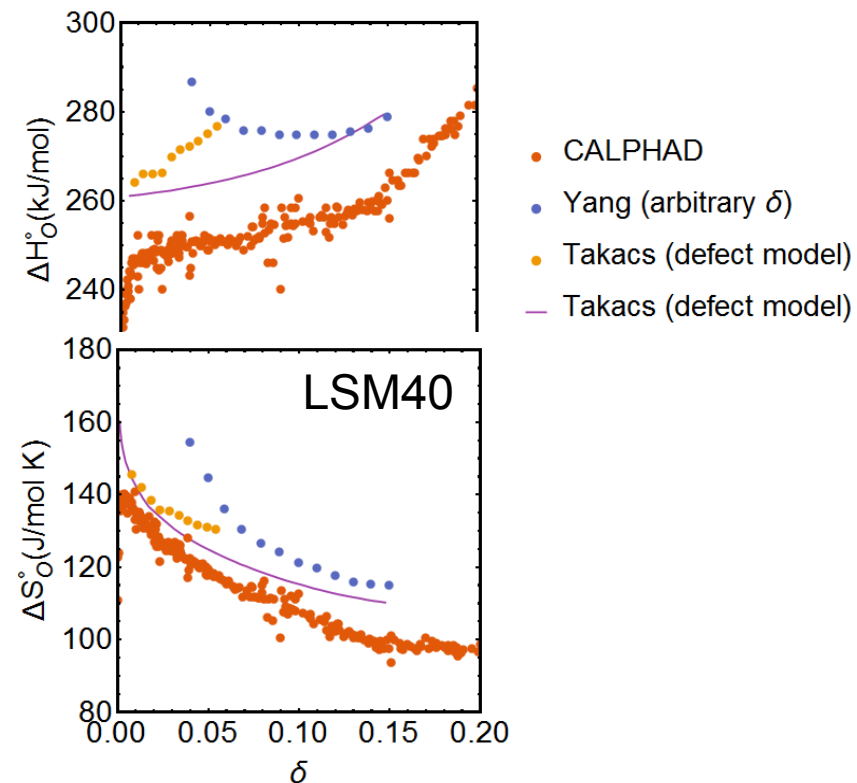
Phase, parameter	Phase, parameter
Liquid (Ce ³⁺ , Ce ⁴⁺) _l (Va ^{••} , O ²⁻) _l , Eqs. (2)–(4)	${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = -247150 - 71 T + 11 {}^{\circ}G_{\text{CeO}_2} + 4 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = 126654 - 54.4977 T + {}^{\circ}G_{\text{CeO}_2}$	${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = -488650 - 155 T + 24 {}^{\circ}G_{\text{CeO}_2} + 8 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = 87177 - 29.059 T + {}^{\circ}G_{\text{CeO}_2}$	${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = -730900 - 237.3 T + 38 {}^{\circ}G_{\text{CeO}_2} + 12 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2}$	${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = -121419 - 40.457 T + 7 {}^{\circ}G_{\text{CeO}_2} + 2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = 2 {}^{\circ}G_{\text{CeO}_2} + 3 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}} - 2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = -105398$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = -35158$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = -114250$	
fcc (bcc)-Ce (Ce) _l (O, Va) _l , Eq. (5)	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = -525009 + 67.7626 T + {}^{\circ}G_{\text{CeO}_2} + 1/2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = -521242 + 67.7626 T + {}^{\circ}G_{\text{CeO}_2} + 1/2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
A-phase (Ce ³⁺ , Ce ⁴⁺) _l (O ²⁻ , Va) _l , Eqs. (6)–(8)	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 1/2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} + 1/2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 102206$	
H-phase (Ce ³⁺ , Ce ⁴⁺) _l (O ²⁻ , Va) _l , Eqs. (6)–(8)	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 1/2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} + 1/2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 102206$	
X-phase (Ce ³⁺ , Ce ⁴⁺) _l (O ²⁻ , Va) _l , Eqs. (6)–(8)	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 1/2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} + 1/2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 102206$	
C-phase (Ce ³⁺ , Ce ⁴⁺) _l (O ²⁻ , Va) _l , Eq. (9)	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} + 1/2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = 19140 + 2 {}^{\circ}G_{\text{CeO}_2} - 1/2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = 19140 + 2 {}^{\circ}G_{\text{CeO}_2}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 17178 - 17.7264 T$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 25591 + 22.2801 T$	
F-phase (Ce ³⁺ , Ce ⁴⁺) _l (O ²⁻ , Va) _l , Eqs. (10)–(12)	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 18.702165 T$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 1.5 {}^{\circ}G_{\text{CeO}_2} + 18.702165 T$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 117572 + 25.9745 T$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = {}^{\circ}G_{\text{CeO}_2} - 115033 + 31.1026 T$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = -133719 - 11.0961 T + 3 {}^{\circ}G_{\text{CeO}_2} + 2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	
${}^{\circ}G_{\text{CeO}_2}^{\text{liq}} = -125351 - 31.333 T + 5 {}^{\circ}G_{\text{CeO}_2} + 2 {}^{\circ}G_{\text{CeO}_2}^{\text{liq}}$	

species, phases, and governing equations

Comparing analysis methods using CALPHAD as ground truth



- Good agreement for the “best-known” system.



- Poor agreement for a well-known system.

C.-K. Yang et al., *Journal of Materials Chemistry A* (2014).
M. Takacs et al., *Acta Materialia*. **103**, 700–710 (2016).

- What we refer to as $\Delta H(\delta; T)$ and $\Delta S(\delta; T)$ is really:

$$\Delta H(\delta; T) = \lim_{d\delta \rightarrow 0} \frac{H_{sol}(\delta + d\delta; T) - H_{sol}(\delta; T)}{d\delta} + \frac{1}{2} H_{O_2, g}(T)$$

$$\frac{\partial H_{sol}(\delta; T)}{\partial \delta} = \frac{RT_0 \partial \ln(p^0/p_{O_2})}{2 \partial (T_0/T)} - \frac{1}{2} H_{O_2, g}(T)$$

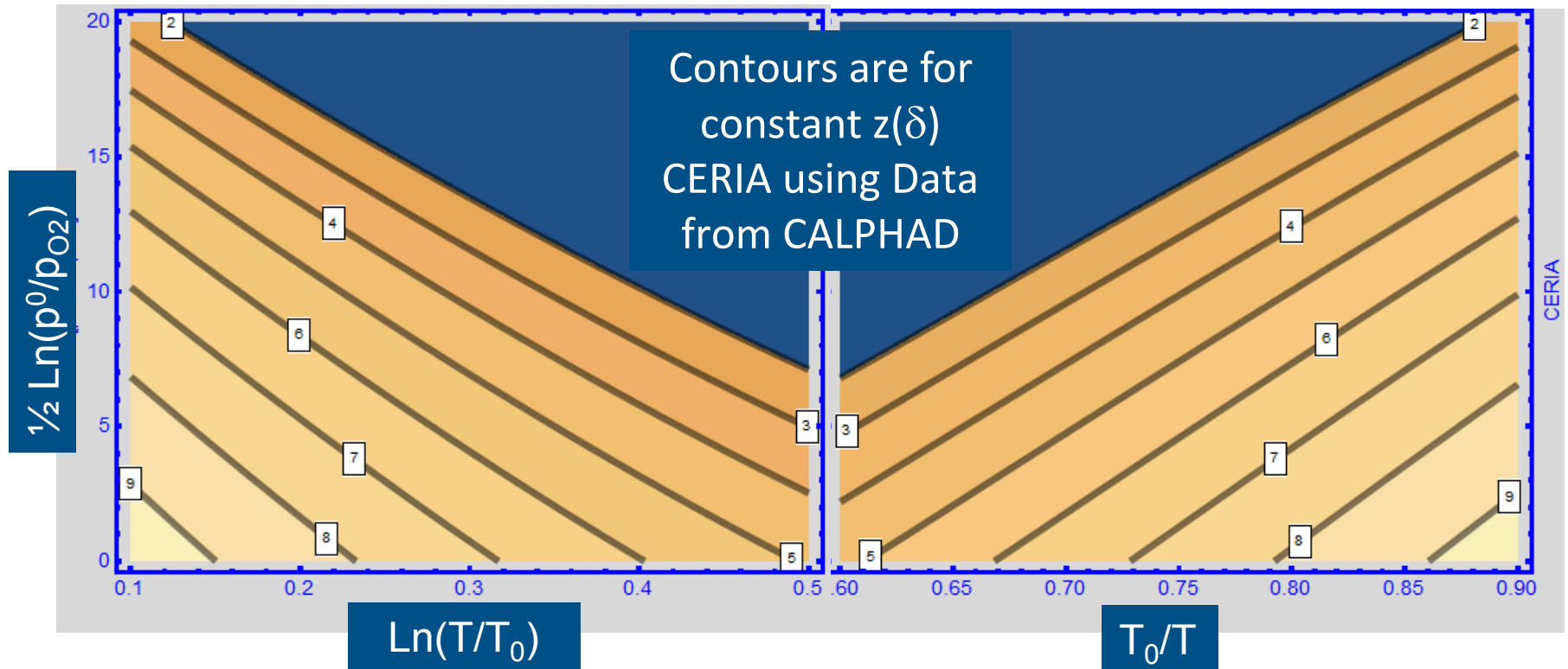
$$\Delta S(\delta; T) = \lim_{d\delta \rightarrow 0} \frac{S_{sol}(\delta + d\delta; T) - S_{sol}(\delta; T)}{d\delta} + \frac{1}{2} S_{O_2, g}(T; p_{O_2}(\delta; T))$$

$$\frac{\partial S_{sol}(\delta; T)}{\partial \delta} = \frac{-R \partial \ln(p^0/p_{O_2})}{2 \partial \ln(T/T_0)} - \frac{1}{2} S_{O_2, g}(T; p_{O_2}(\delta; T))$$

- Enthalpy and entropy of reaction (incremental change in δ) are local partial derivatives of the same function.

- Fit a two dimensional response surface given measured triplets $\{T, p_{O_2}, \delta\}$ so that:
 - $z(\delta) \equiv f\left(\ln \frac{T}{T_0}, \frac{1}{2} \ln \frac{p^0}{p_{O_2}}\right)$ and
 - $\frac{1}{2} \ln \frac{p^0}{p_{O_2}} \equiv g\left(\ln \frac{T}{T_0}, z(\delta)\right)$ - convenient if easily invertible
- Take temperature derivatives of “g” from response surface to yield incremental changes with δ in the reaction enthalpy and entropy.
- Need reliable and reproducible (T, p_{O_2}, δ) data over a relevant range of expected conditions.
 - Low T, low P_{O_2} for gas splitting
 - Avoid extrapolating outside data envelope

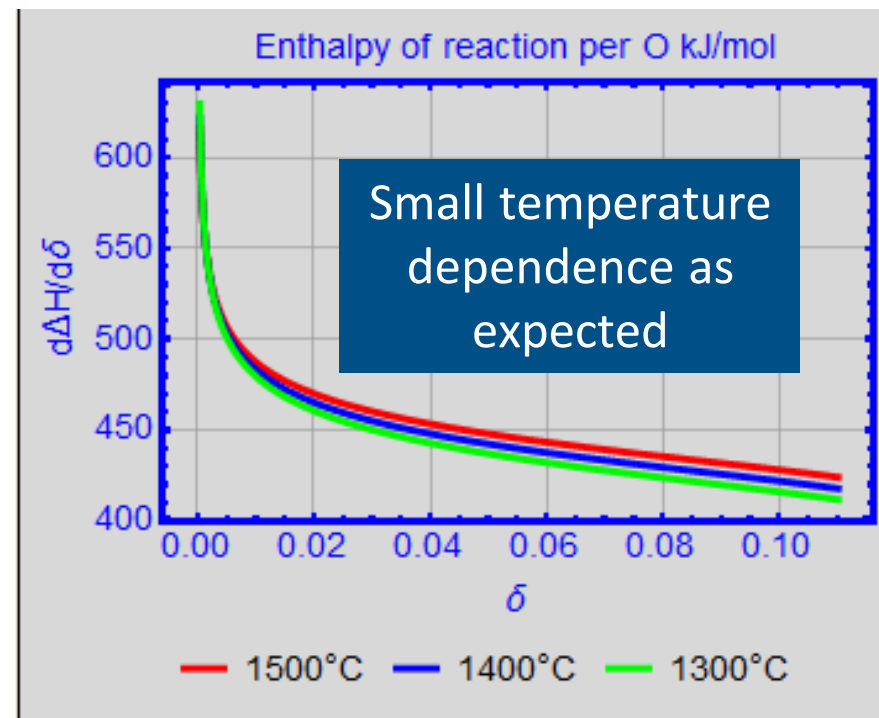
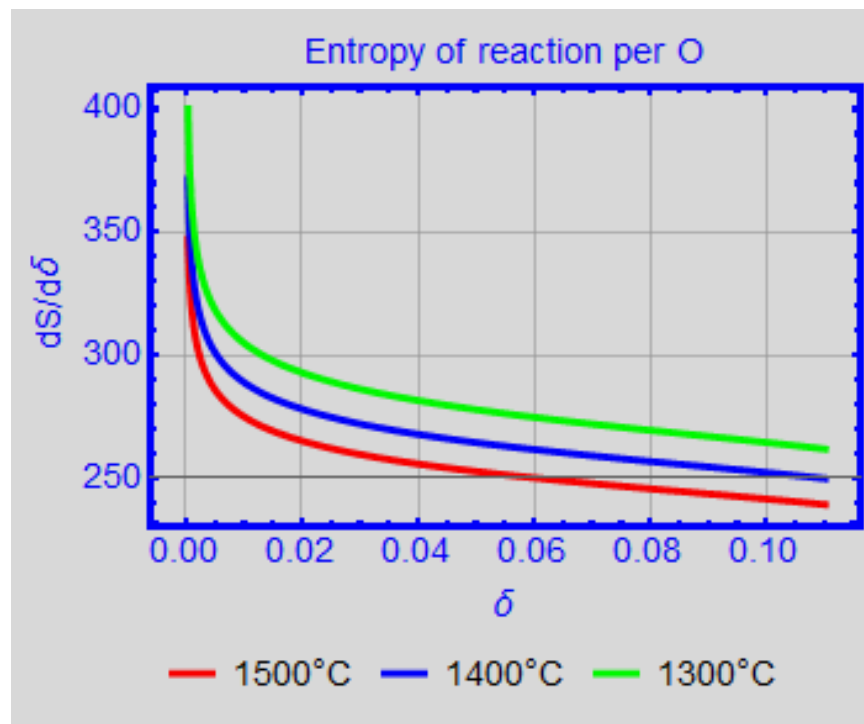
Initial response surface for Ceria



Negative of the slope
determines $\frac{\partial \Delta s(\delta; T)}{\partial \delta}$

Slope determines $\frac{\partial \Delta H(\delta; T)}{\partial \delta}$

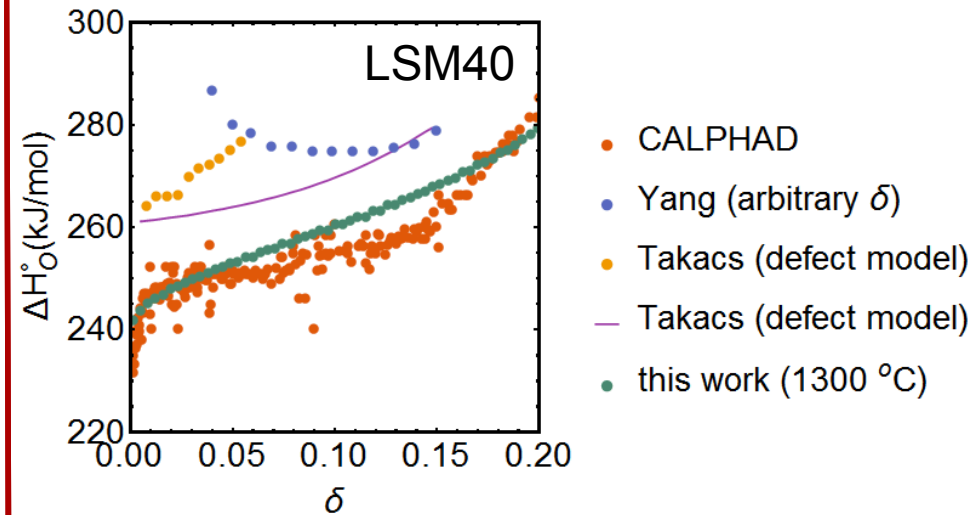
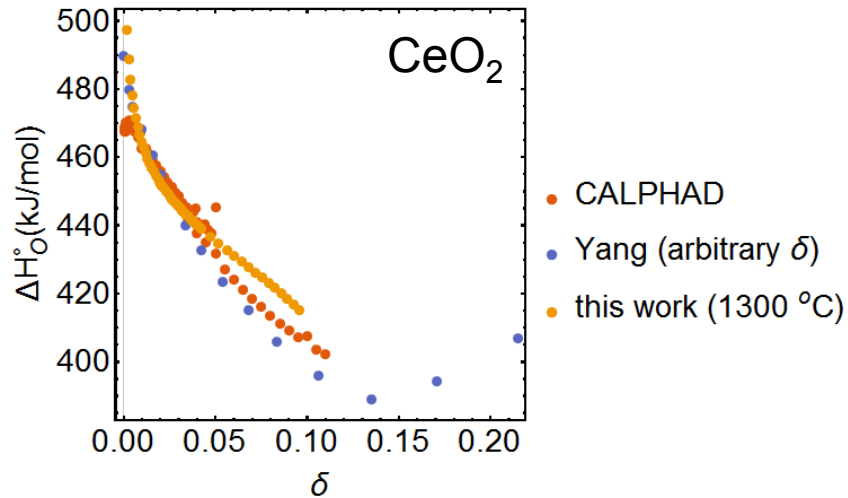
Derivatives determine enthalpy and entropy of incremental reaction for Ceria



Negative of the slope and
scaling R determined $\frac{\partial \Delta S(\delta; T)}{\partial \delta}$

Slope and scaling parameter
 RT_0 determined $\frac{\partial \Delta H(\delta; T)}{\partial \delta}$

Comparing analysis methods for $\Delta H(\delta)$



- Established a sound framework to analyze and explore material thermodynamic properties.
- Continue to refine fitting of the equilibrium response surface.

Summary and future direction

- Defect models are not needed to extract ΔH or ΔS .
 - Apply advanced surface fitting strategies to further develop method (i.e., Basis Splines).
 - Caveat: ***extrapolate*** at your own peril
 - Formulate new insights from manipulating thermodynamic equations.
 - Made possible by vetted response surface representative of equilibrium phase space
 - Rigorously evaluate the impact of uncertainties.
 - Statistically-based UA/UQ enabled by this approach
-
- Leverage ideas to build consensus around standard practices.
 - Experimental protocols and benchmarked tools

Challenged by moving beyond these popular non-stoichiometric oxide material systems

Fe²⁺/Fe³⁺ systems:

- Deep reduction at 1400 °C.
- High redox capacity ($\Delta\delta > 0.1$).
- Slow H₂O oxidation kinetics.
- YSZ, ZrO₂, Al₂O₃ matrix required.

Ce³⁺/Ce⁴⁺ systems:

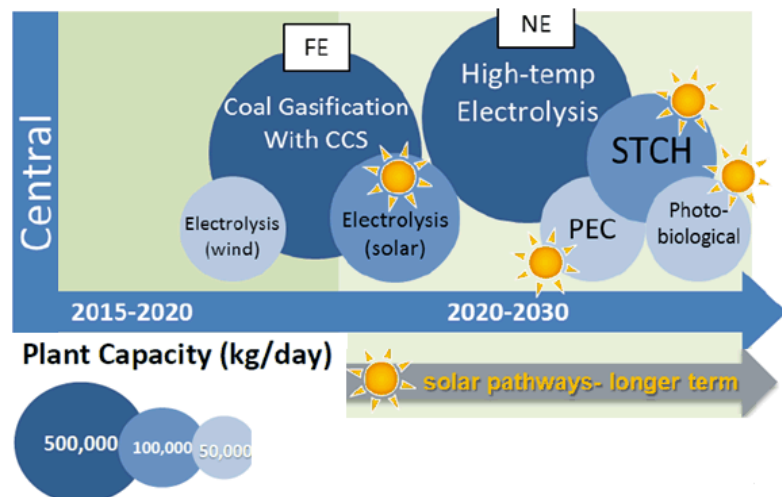
- Shallow reduction at 1500 °C.
- Low redox capacity ($\Delta\delta < 0.08$).
- Fast H₂O oxidation kinetics.
- Durable.

TM²⁺/TM³⁺/TM⁴⁺ perovskite systems:

- Deep reduction at 1400 °C.
- High redox capacity ($\Delta\delta > 0.1$).
- Promising H₂O oxidation kinetics.
- Vast material space!

PROPERTY	FERRITE (MFeO _x /ZrO ₂) (MFeO _x /Al ₂ O ₃)	CERIA (CeO ₂) Current State of the Art	PEROVSKITE (ABO ₃)	IDEAL
Redox Kinetics	SLOW	FAST	?	FAST
Capacity ($\Delta\delta$)	HIGH	LOW	HIGH	HIGH
T _{TR} @ Reduction	MED/HIGH	HIGH	LOW	LOW
H ₂ O/H ₂ @ Oxidation	MED	LOW	?	LOW
Durability	MED/HIGH	HIGH	?	HIGH
Earth Abundance	HIGH	LOW/MED	HIGH	HIGH

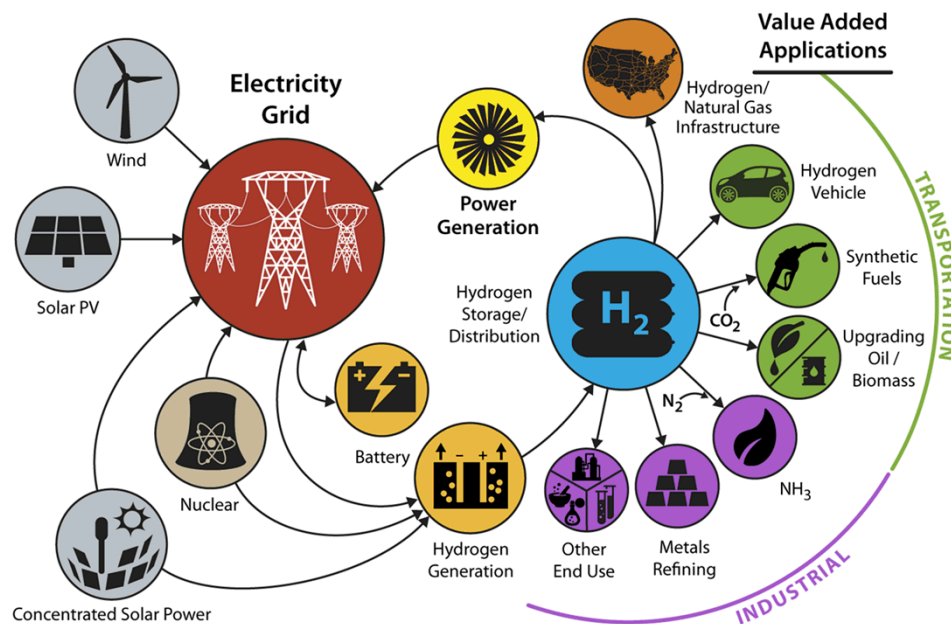
US DOE vision for H₂ production and utilization



- Multi-laboratory consortium and Energy Materials Network announced in 2016.



<http://energy.gov/eere/energy-materials-network/energy-materials-network>



H₂

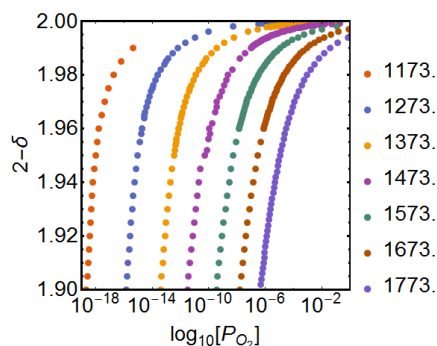
at Scale:

Deeply Decarbonizing
our Energy System

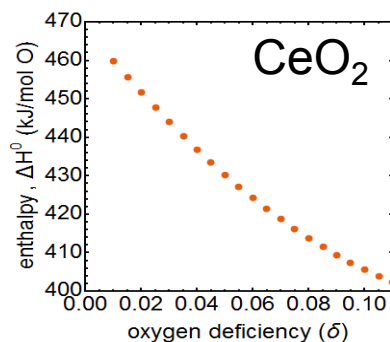
BIG IDEA

Opportunities to work with Sandia

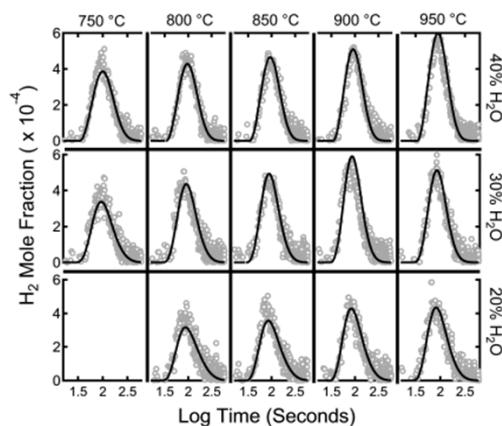
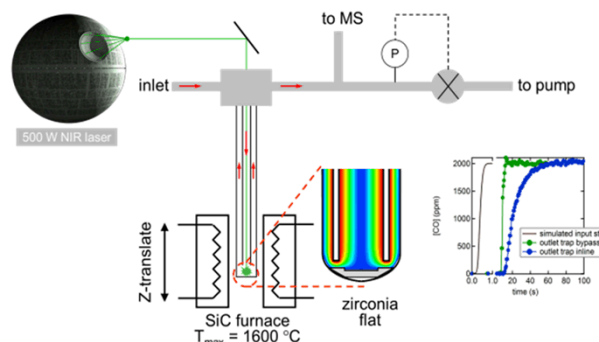
determine P_{O_2} - T - δ relation using TGA or other methods



derive thermodynamic properties for material from P_{O_2} - T - δ relation



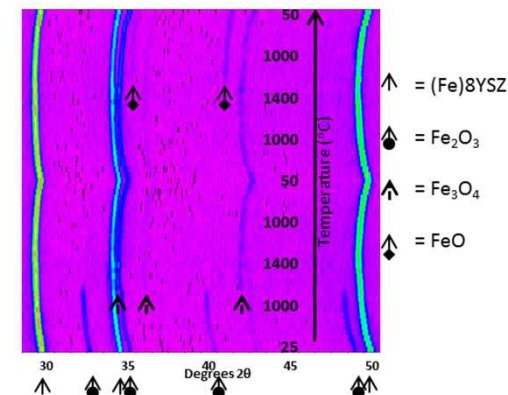
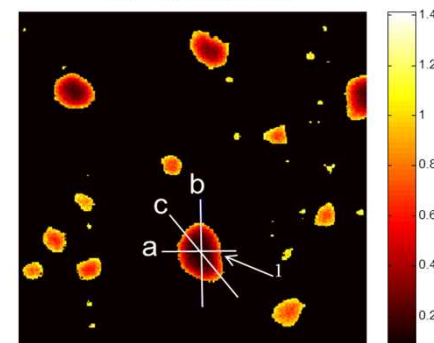
derive kinetic information at technology-specific conditions using idealized flow reactor



- Cycled under high radiative flux.
- Technology-specific operation.

derive structural and mechanistic information using advanced diagnostics (i.e., HTXRD, ToF-SIMS)

$^{18}O/^{16}O$ masked



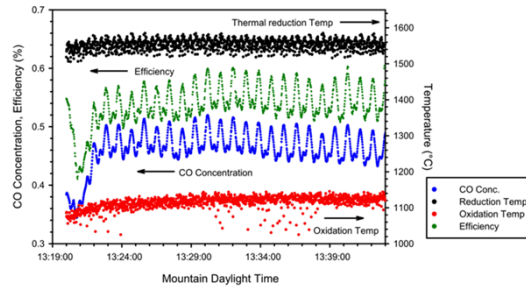
- Great potential for operando X-ray scattering.

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National Solar Thermal Test Facility

Cascading Pressure
Receiver/Reactor (CPR2)

PATHWAY FOR ADVANCING TRL...



- 16kW_{th} solar furnace.
- 6MW_{th} power tower.
- Technology-specific operation at scale.



25 ft. tall

- ~5kW_{th} system capable of producing 0.5slpm H₂.
- Derive engineering test data necessary for model validation and scale-up.

Thank you for your attention.

Questions?