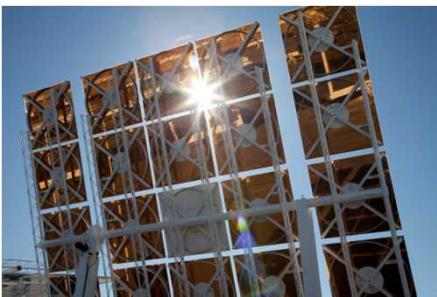


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# A Particle/sCO<sub>2</sub> Heat Exchanger Testbed and Reference Cycle Cost Analysis

M. Carlson<sup>1</sup>, B. Middleton<sup>1</sup>, C. Ho<sup>1</sup>

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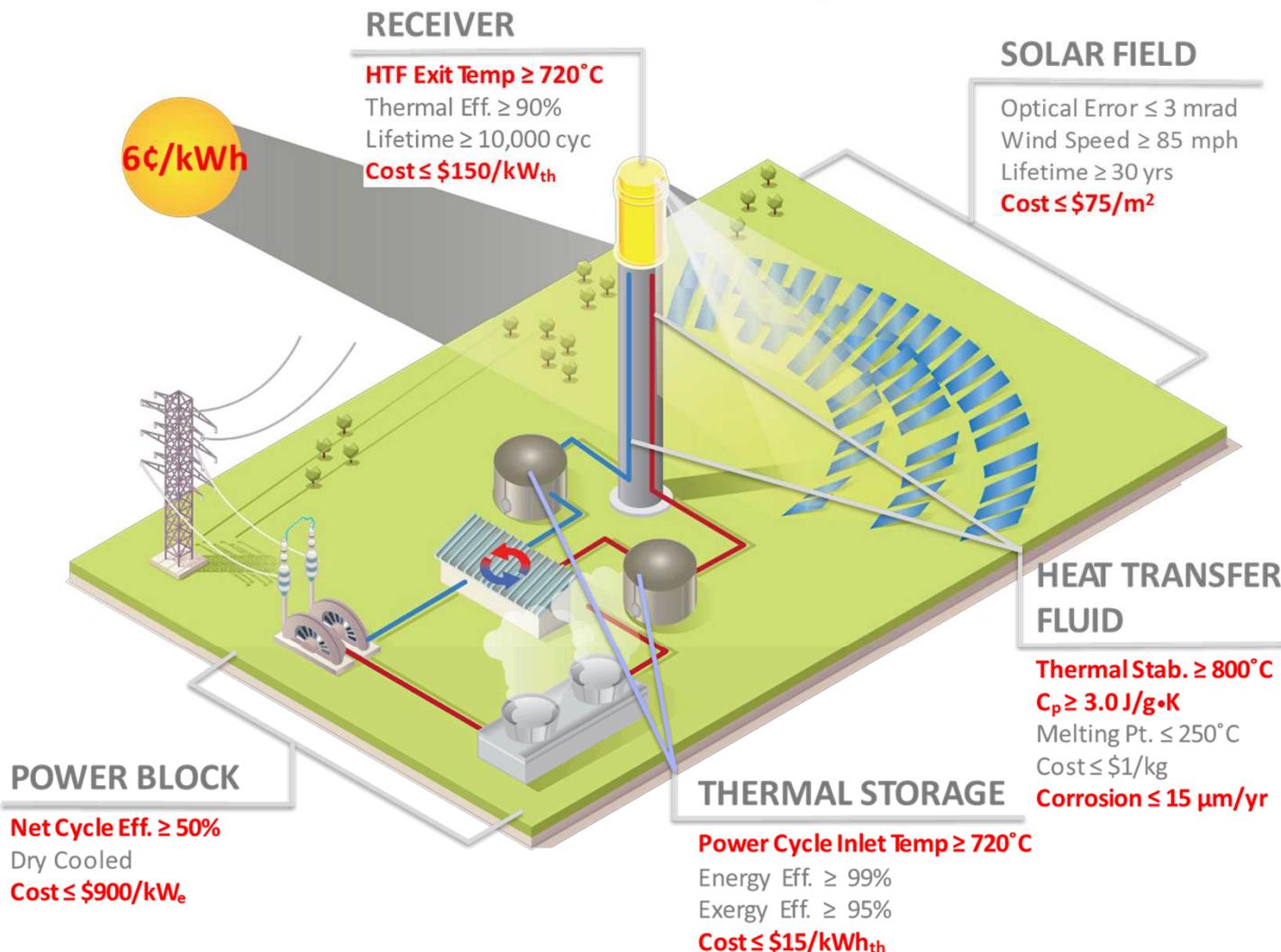


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# Overview

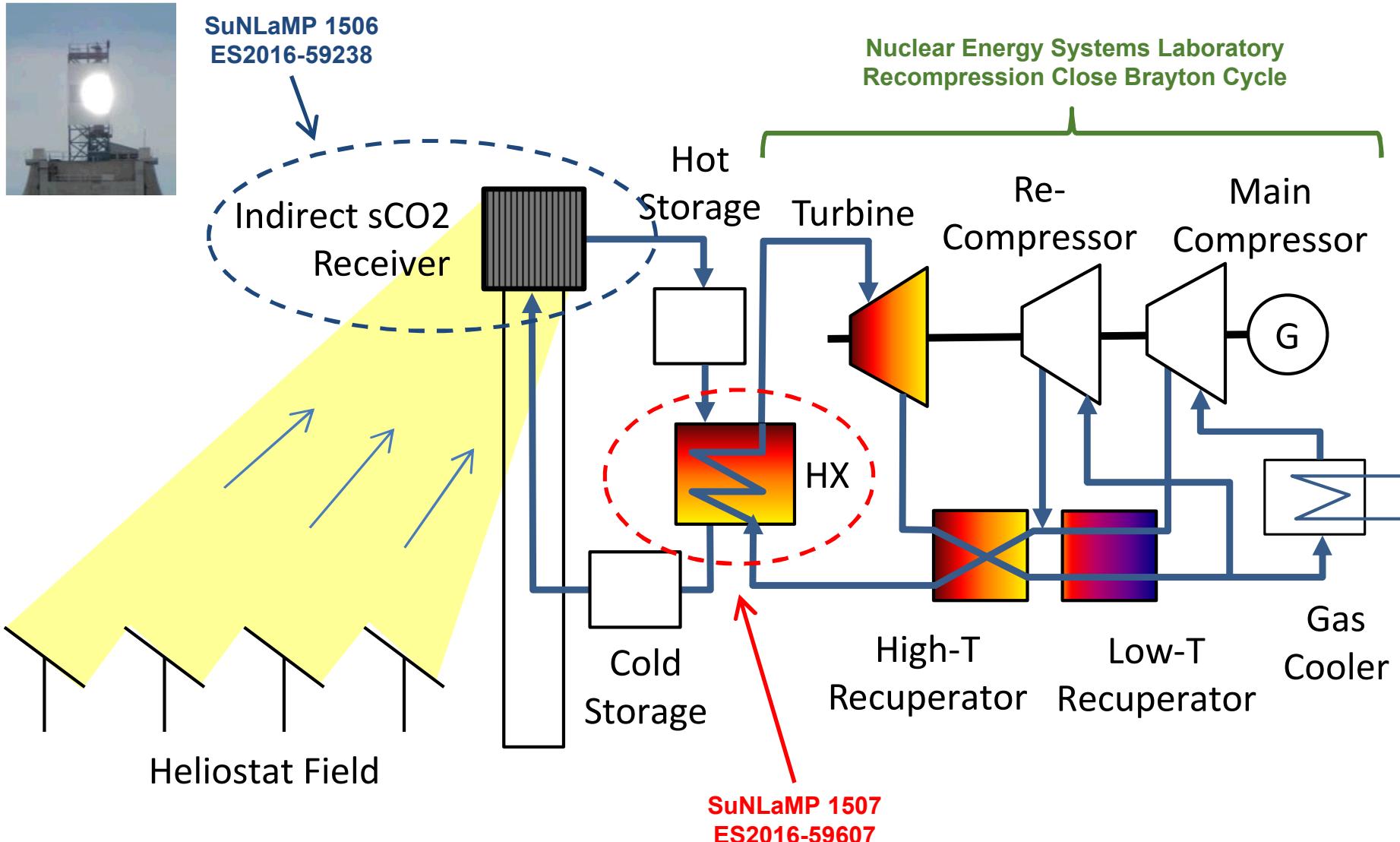
- Background and Objectives
- Particle/sCO<sub>2</sub> Heat Exchanger Testbed
- Reference Cycle Cost Analysis
- Conclusions

# SunShot CSP Tower Targets



M. Bauer, R. Vijaykumar, M. Lausten, J. Stekli, "Pathways to Cost Competitive Concentrated Solar Power Incorporating Supercritical Carbon Dioxide Power Cycles," presented at the 5<sup>th</sup> International Symposium on Supercritical CO<sub>2</sub> Power Cycles, San Antonio, TX, 2016.

# Integration with Sandia Capabilities



# sCO<sub>2</sub> Cycle Cost & Performance

	SCBC	RCBC	CCBC	CBI
<b>Net Power (MWe)</b>	100	100	100	133
<b>Efficiency (%)</b>	16	46	46	28
$\Delta T_{HTR} (C)$	540	172	170	518
$T_{max} (C)$	700	700	700	600
$P_{max} (MPa)$	20	20	20	27.6
$P_{min} (MPa)$	6.4	8.0	7.3	8.5
$T_{comp,min} (C)$	55	55	55	37
<b>Heater (\$/kWe)</b>	381	212	322	281*
<b>Recuperation (\$/kWe)</b>	0.00	243	244	122*
<b>Cooling (\$/kWe)</b>	545	85	154	574*
<b>Compression (\$/kWe)</b>	423	230	147	80*
<b>Expansion (\$/kWe)</b>	136	128	135	138*
<b>Total (\$/kWe)</b>	1,485	898	1,002	914*
				1,095

SCBC=Simple Closed Brayton Cycle

CCBC=Cascaded Closed Brayton Cycle

RCBC=Recompression Closed Brayton Cycle

CBI=Combination Bifurcation with Intercooler

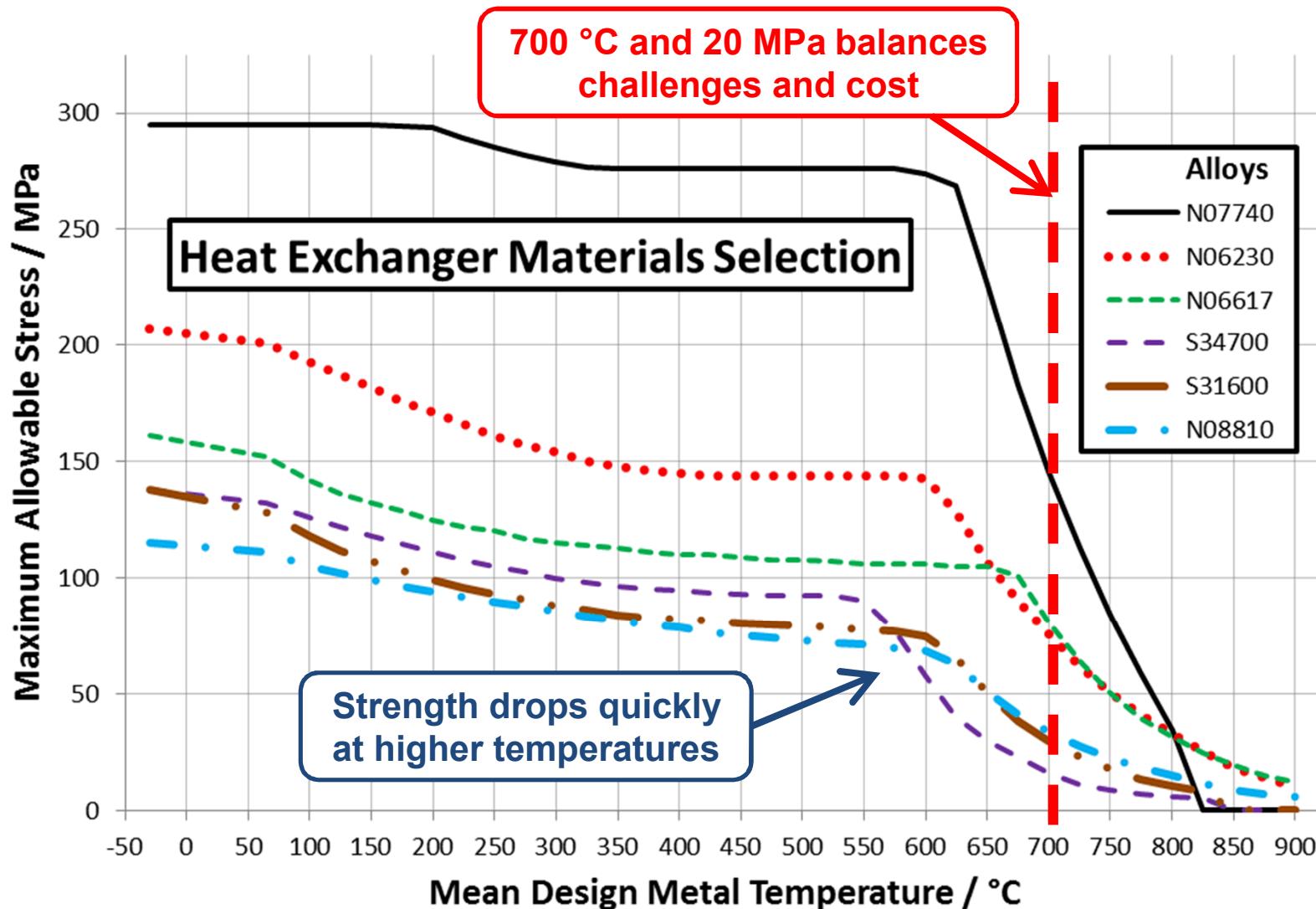
# sCO<sub>2</sub> Cycle Layout Options



Application	Size / MWe	Temp / °C	Pressure / MPa
Nuclear	10-300	350-700	20-35
Fossil (Indirect)	300-600	550-900	15-35
Fossil (Direct)	300-600	1100-1500	35
Solar	10-100	500-1000	20-35
Shipboard	<10-10	200-300	15-25
Waste Heat	1-10	<230-650	15-35
Geothermal	1-50	100-300	15

Adapted from R. Dennis, "DOE Initiative on SCO<sub>2</sub> Power Cycles (STEP) -Heat Exchangers: A Performance and Cost Challenge -," presented at the EPRI-NETL Workshop on Heat Exchangers for SCO<sub>2</sub> Power Cycles, San Diego, CA, 2015

# Materials Challenges



# Overview

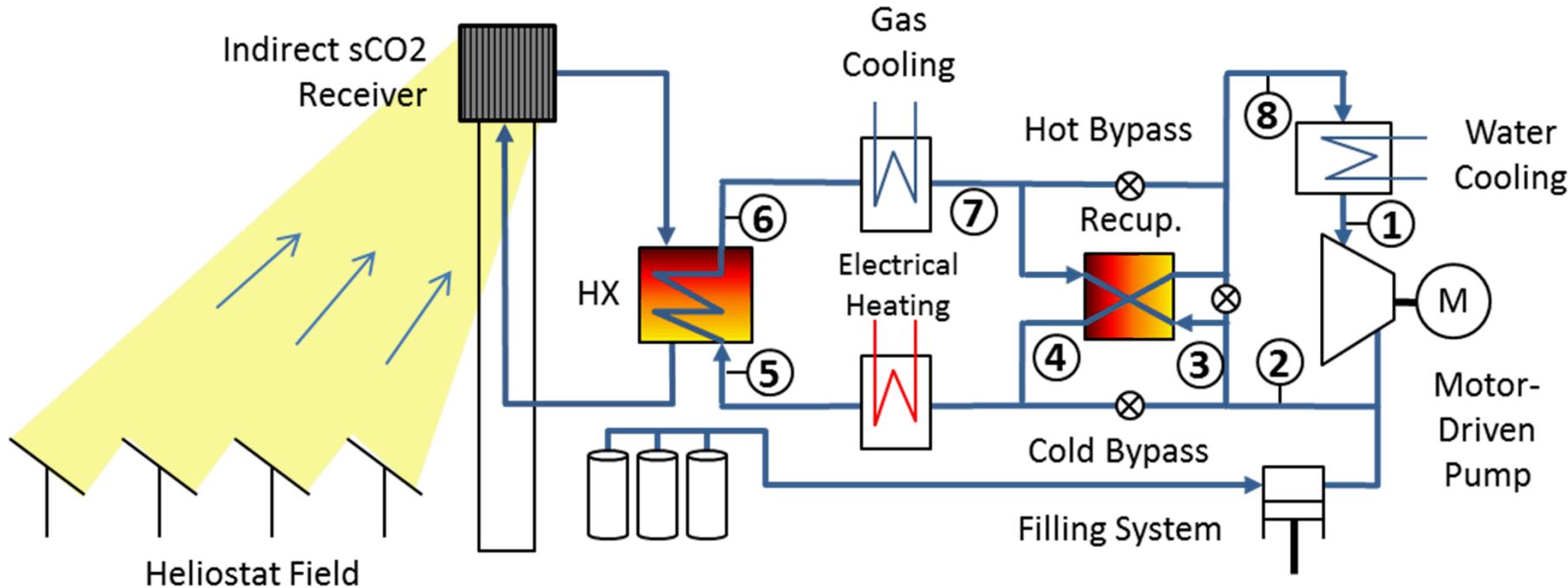
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# Preliminary Design Requirements

PERFORMANCE OF ONE UNIT							
		HOT SIDE		COLD SIDE			
STREAM NAME		PARTICLES			SCO2		
FLUID FLOW RATE (TOTAL)	kg/s	0.41			0.53		
TEMPERATURE (IN/OUT)	°C	775	570.	550.	700.		
DENSITY (VAP/FLUID)	kg/m <sup>3</sup>	Per Note 3	Per Note 3	124	103		
VISCOSITY (VAP/FLUID)	µPa-s	Per Note 4	Per Note 4	37.4	41.6		
MOLECULAR WEIGHT (VAP/FLUID)	kg/kmol	N.A.	N.A.	44	44		
SPECIFIC HEAT (VAP/FLUID)	kJ/kg-K	1.210 (Per Note 5)	1.140 (Per Note 5)	1.240	1.270		
THERMAL CONDUCTIVITY (VAP/FLUID)	W/m-K	Per Note 4	Per Note 4	0.06258	0.07207		
PRESSURE (IN)	MPa	0.101		20.0			
PRESSURE DROP (ALLOW./CALC.)	kPa	Per Note 6	Per Note 6	200	200		
FOULING RESISTANCE (MIN.)	m <sup>2</sup> -K/W	0.0 (nil)		0.000176			
HEAT EXCHANGED	100	kW	MTD (corrected)	STA	°C		
TRANSFER RATE, SERVICE	STA	W/m <sup>2</sup> -K	CLEAN	STA	W/m <sup>2</sup> -K		
CONSTRUCTION OF ONE MODULE					SKETCH OF NOZZLE ORIENTATION		
		HOT SIDE		COLD SIDE			
DESIGN/TEST PRESSURE	kPa	STA	STA	24000	STA		
DESIGN TEMP (MIN/MAX)	°C	0.00	800.	0.00	800.		
CORROSION ALLOWANCE	mm	0.0 (nil)		0.0 (nil)			
CONNECTION SIZE AND RATING	IN OUT	STA	STA	STA	STA		
MATERIAL OF CONSTRUCTION		Per Note 7		Per Note 7			
INSULATION		Per Note 8		Per Note 8			
NOTES:							
1.	NOMENCLATURE: STA = Supplier to advise; N.A. = Not Applicable						
2.	Design must satisfy ASME Boiler and Pressure Code VIII Division 1 (latest)						
3.	~2000 kg/m <sup>3</sup> ; See CARBO Accucast ID50 properties provided in Ho et al. 2015 (PowerEnergy2015-49421, pre-published)						
4.	Cliff Ho (SNL) and Zhiwen Ma (NREL) to advise on effective transport properties for particle flows depending on flow characteristics						
5.	Latest measurements suggest $0.365(T)^{0.18}$ for temperatures between 50 and 1100 °C						
6.	Must allow for gravity-driven flow of particles through the unit or include a flow system in the unit design						
7.	Material must be stainless steel or nickel alloy (i.e. UNS#s S31600/S31603, S34700, N08810, N06617, N06625, N06230, N07740)						
8.	Insulation to be provided to maintain 90% thermal efficiency (<10% or 10 kW of heat loss) with potential for 99% at a 100 MW scale						

**\*Key elements of the preliminary heat exchanger design requirements**

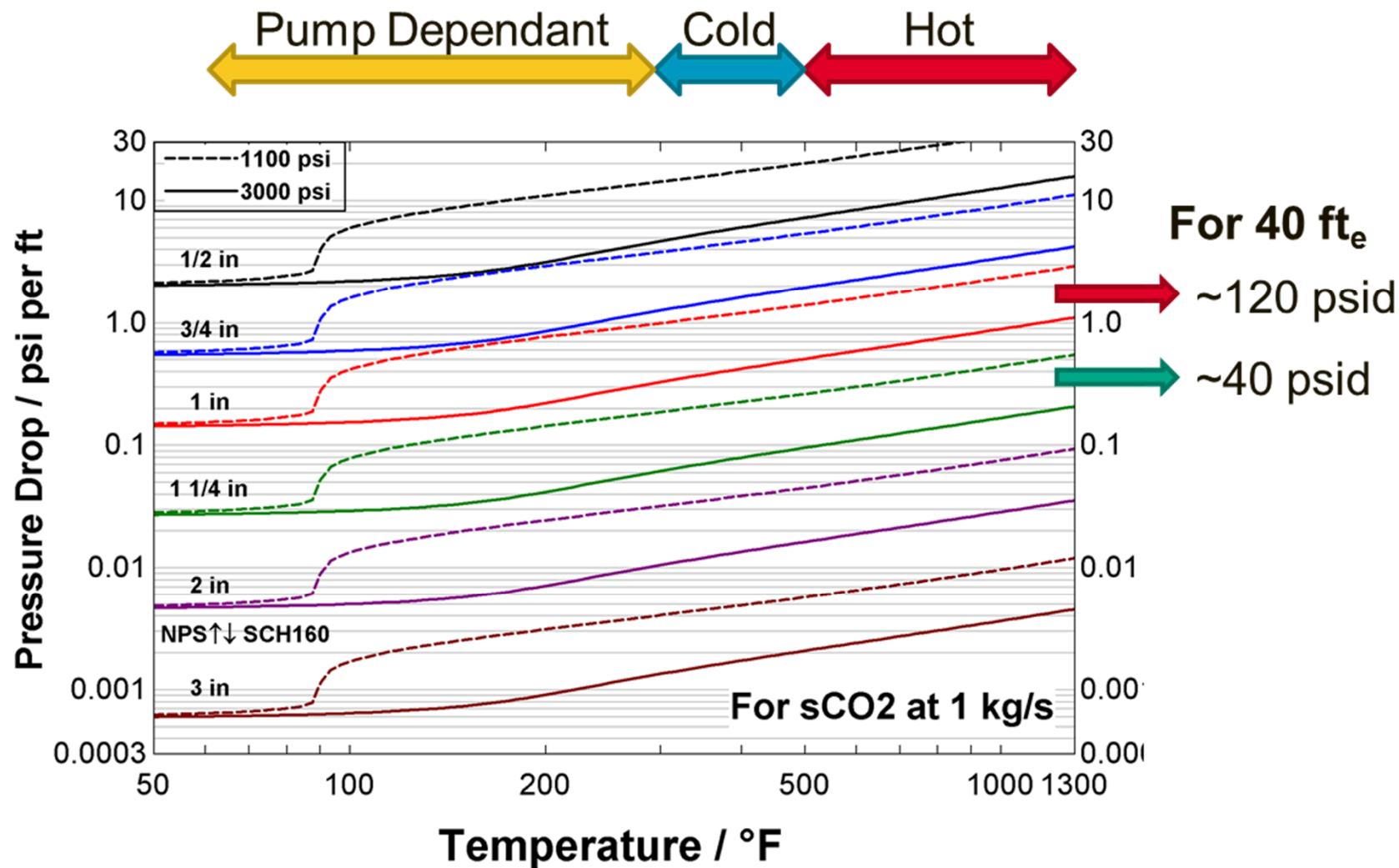
# Purpose of the sCO2 Flow System



Provide the particle/sCO<sub>2</sub> heat exchanger a supply of carbon dioxide at:

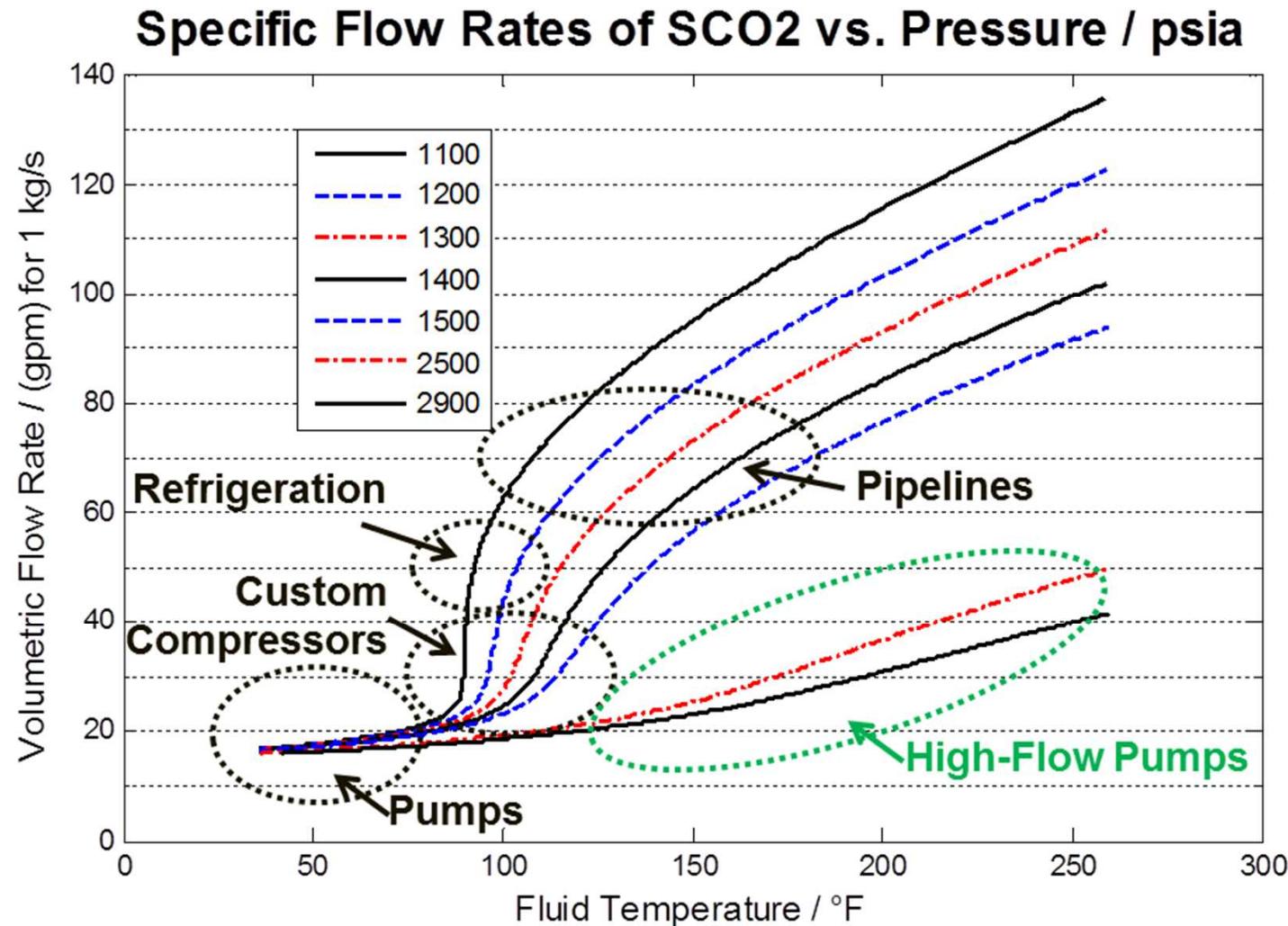
Mass Flow / kg/s	T / °C	P / MPa
0.75	550.	20.0

# sCO<sub>2</sub> Flow System Piping Losses



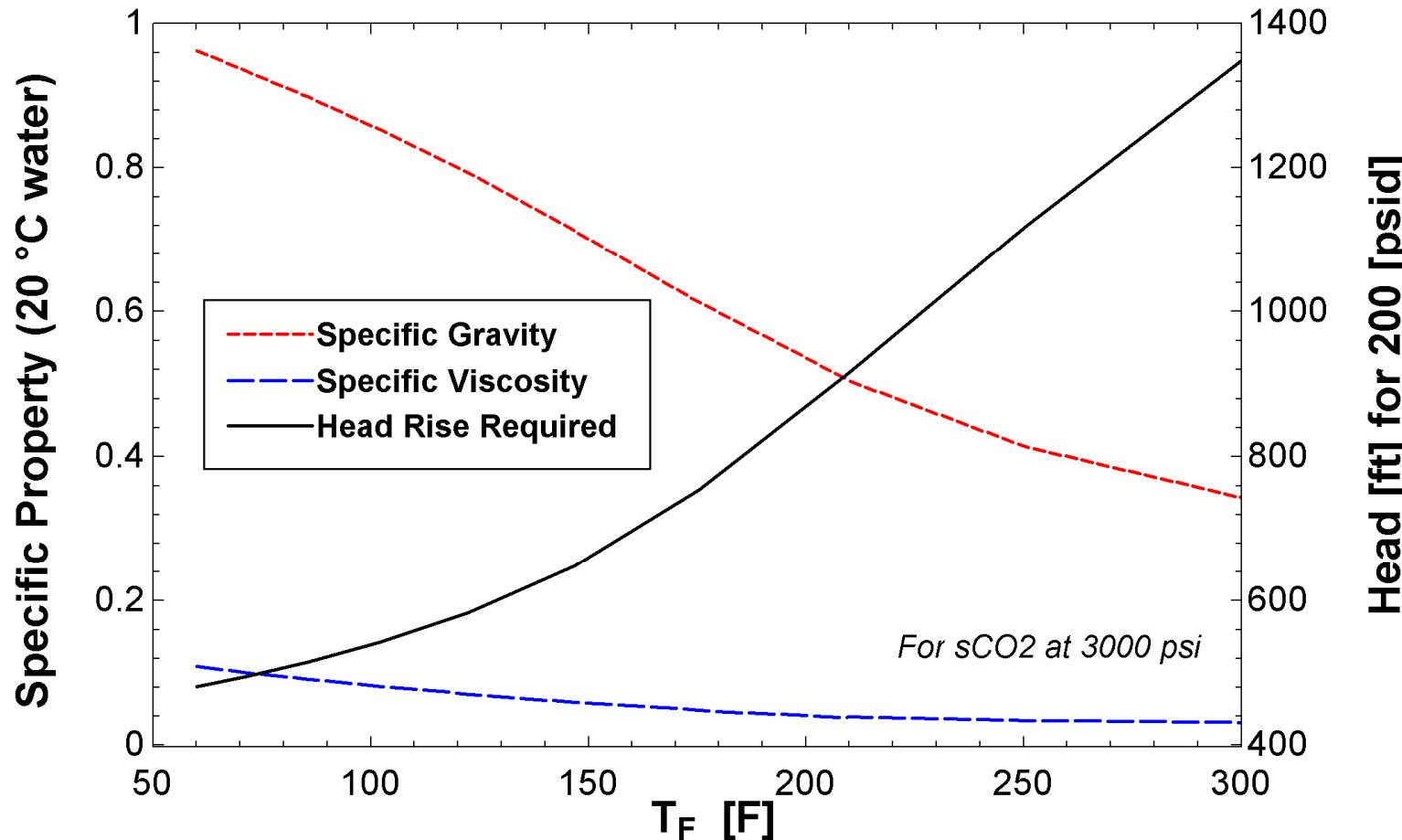
Total system pressure drop approximately 200 psid including 1% per component.

# Pump Volumetric Flow Rate



# Pump Head Rise Considerations

**Head rise increasing significantly as specific gravity (density) reduces**



# Overview

- Background and Objectives
- Particle/sCO<sub>2</sub> Heat Exchanger Testbed
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# Reference Cycle Cost Analysis

## ■ Purpose

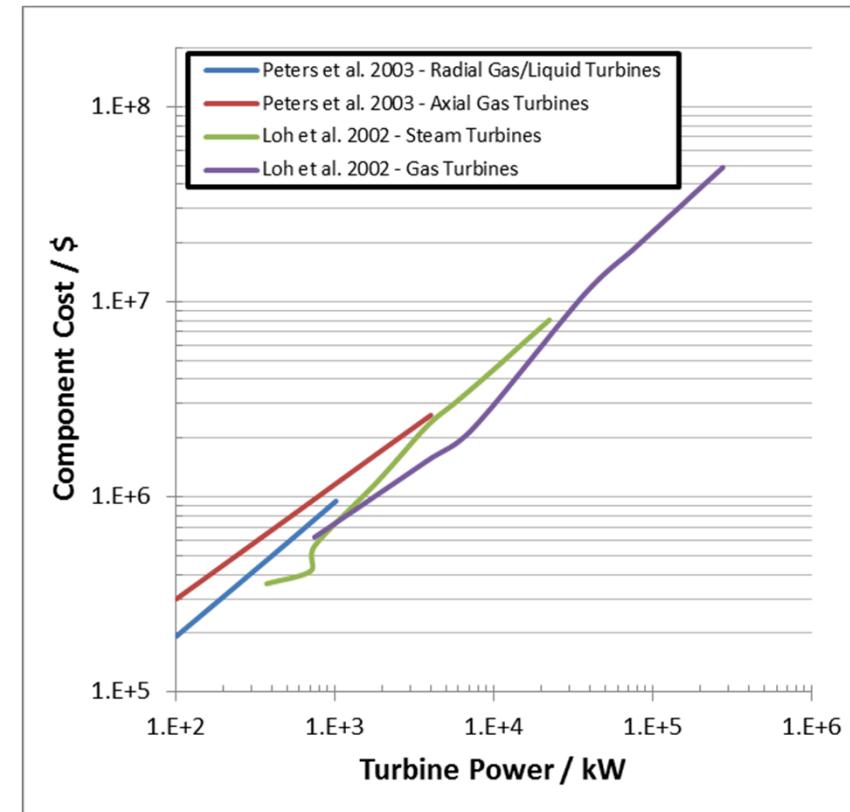
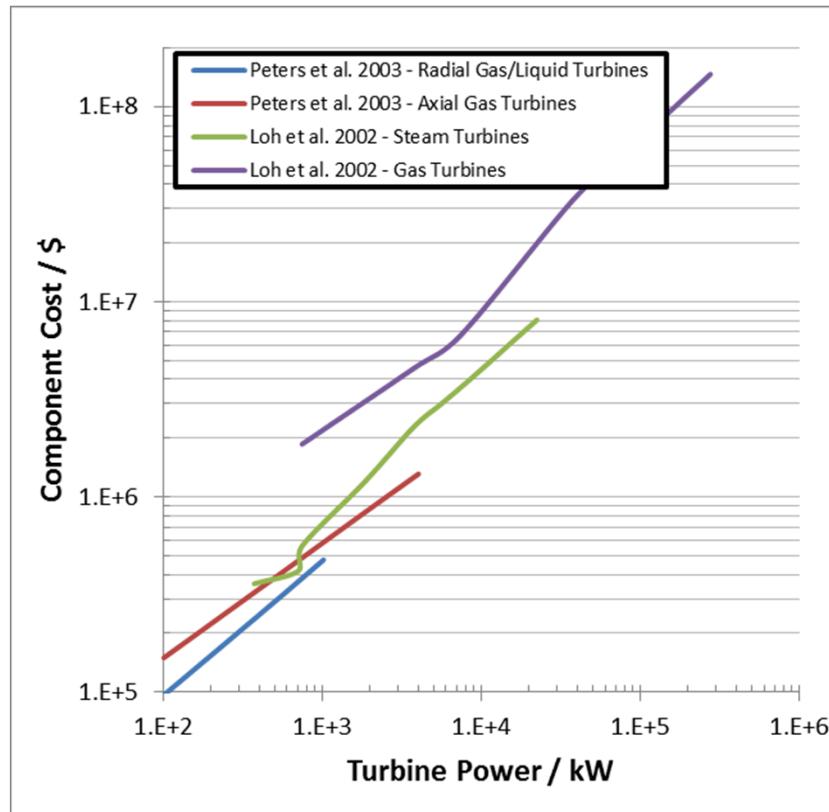
- Develop a cost metric for the particle/sCO<sub>2</sub> heat exchanger using the SunShot power block cost of 900 \$/kWe

## ■ Approach

1. Collect literature-based cost models for the major components
2. Collect sCO<sub>2</sub> Brayton cycle layout options, including CSP-optimized
  - For 1 and 2 see C. K. Ho, M. D. Carlson, P. Garg, and P. Kumar, "Cost and Performance Tradeoffs of Alternative Solar-Driven S-CO<sub>2</sub> Brayton Cycle Configurations," in Proceedings of the ASME 2015 Power and Energy Conversion Conference, San Diego, California, 2015, pp. 1–10.
3. Fit cost model trends to available and obtained vendor estimates
4. Approximate the uncertainty in cost model estimates
5. Develop a confidence range for the particle/sCO<sub>2</sub> Hxer cost

# Fit Cost Models to Vendor Data

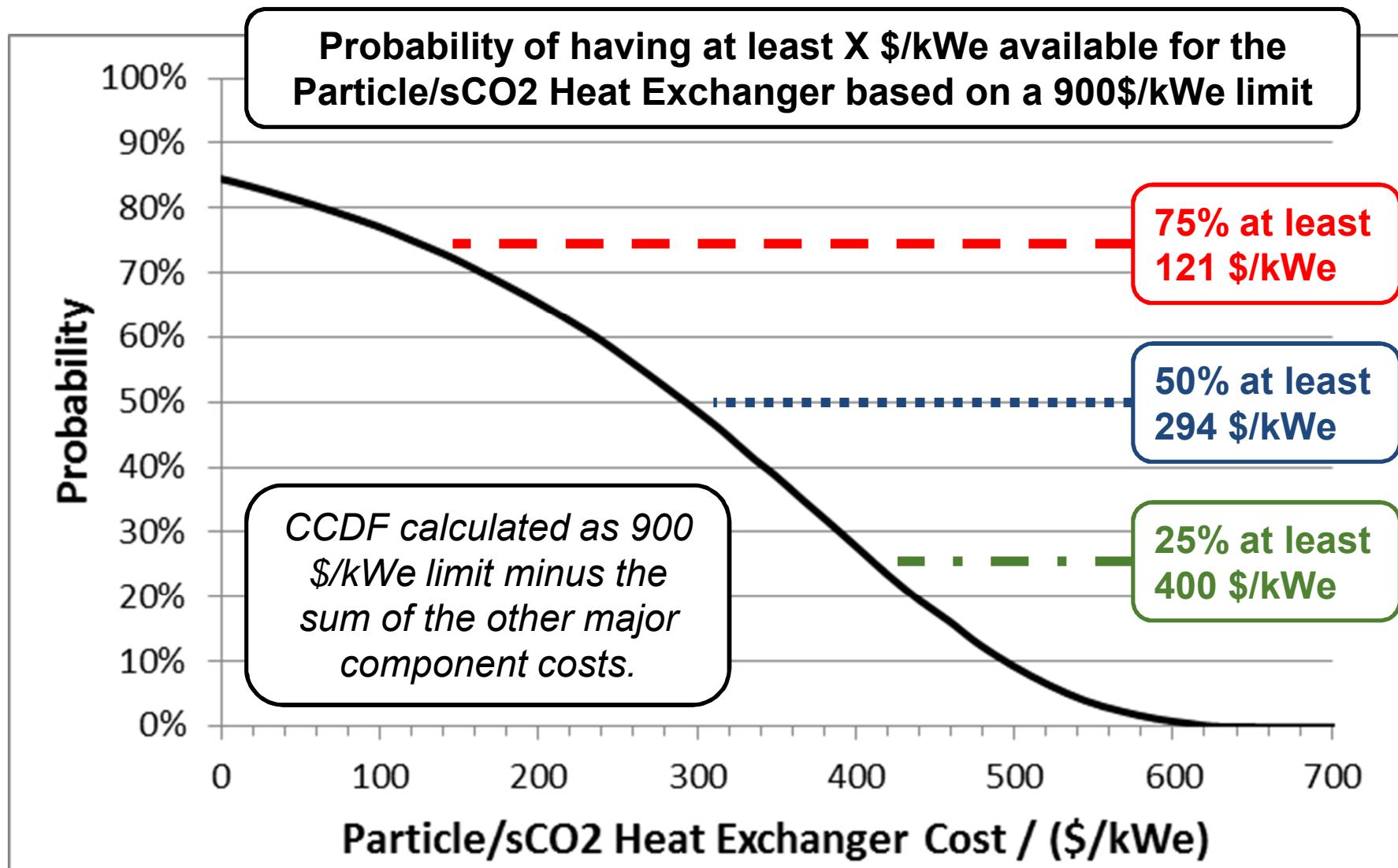
Cost models are collapsed to approximately trend with vendor data.  
\*\*Proprietary vendor data not shown\*\*



# Cost Confidence with Minimal Data

- Approaches to cycle cost estimation
  - Use specific literature cost models or vendor estimates
    - ✗ Assigning uncertainty to specific data is somewhat arbitrary
  - Weighted average of available cost data (Ho et al. 2015)
    - ✗ Propagated uncertainty still relies on assigned uncertainty data
  - Bayesian analysis of component cost data (SuNLaMP)
    - Only assumes the functional form and fit parameter distributions
- Assumption of the hierarchical Bayesian approach
  - Component cost will follow a log-normal distribution
  - Cost vs. size functional form (i.e. power-law,  $Cost = \alpha_0 Capacity^{\alpha_1}$ )
  - Fitting parameters are normally-distributed
  - Prior precision is described by a gamma distribution
  - See P. R. Garvey, S. A. Book, and R. P. Covert, *Probability methods for cost uncertainty analysis: a systems engineering perspective*. 2016.

# Heat Exchanger Cost Confidence



# Overview

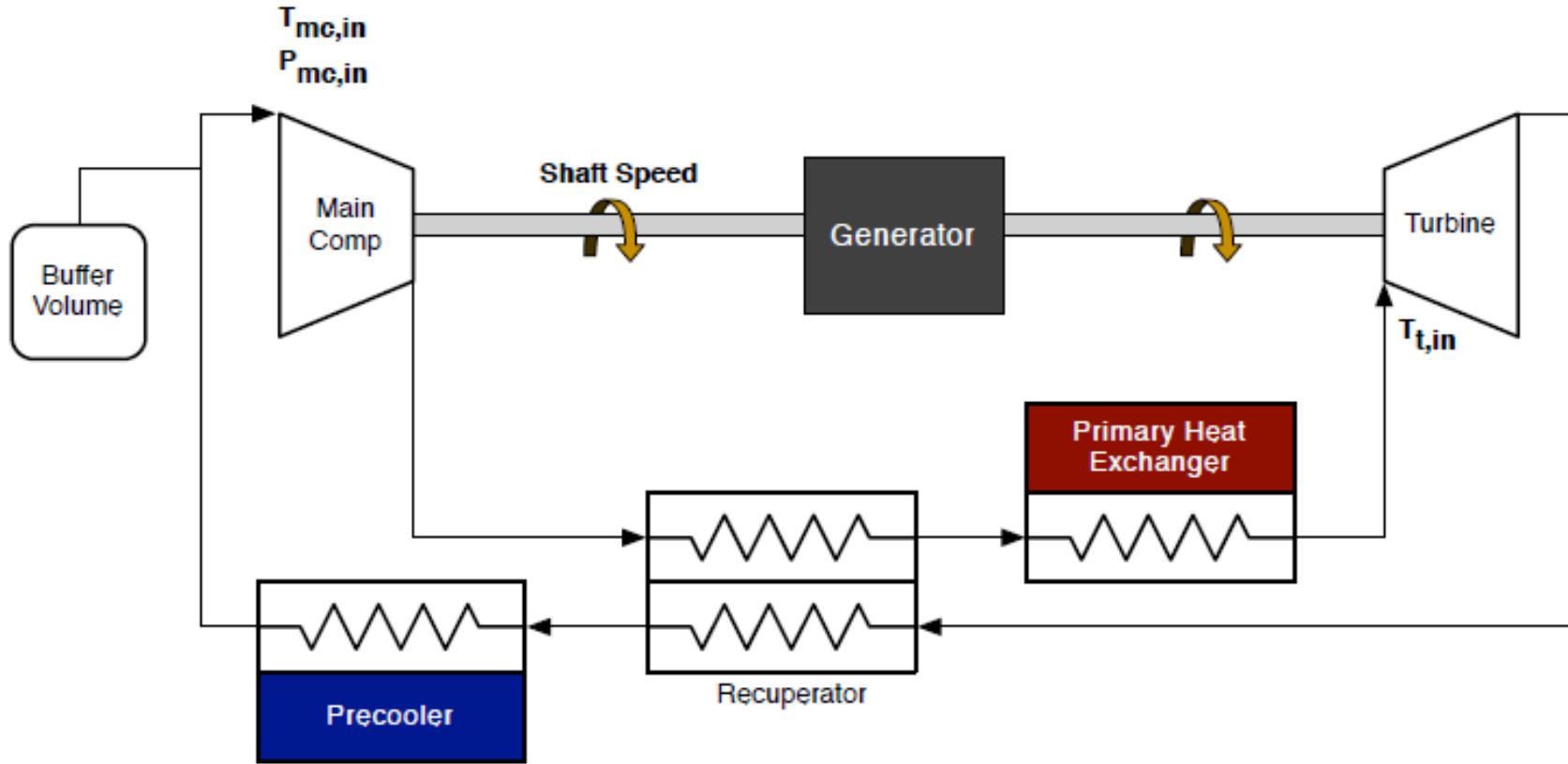
- Background and Objectives
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# Conclusions

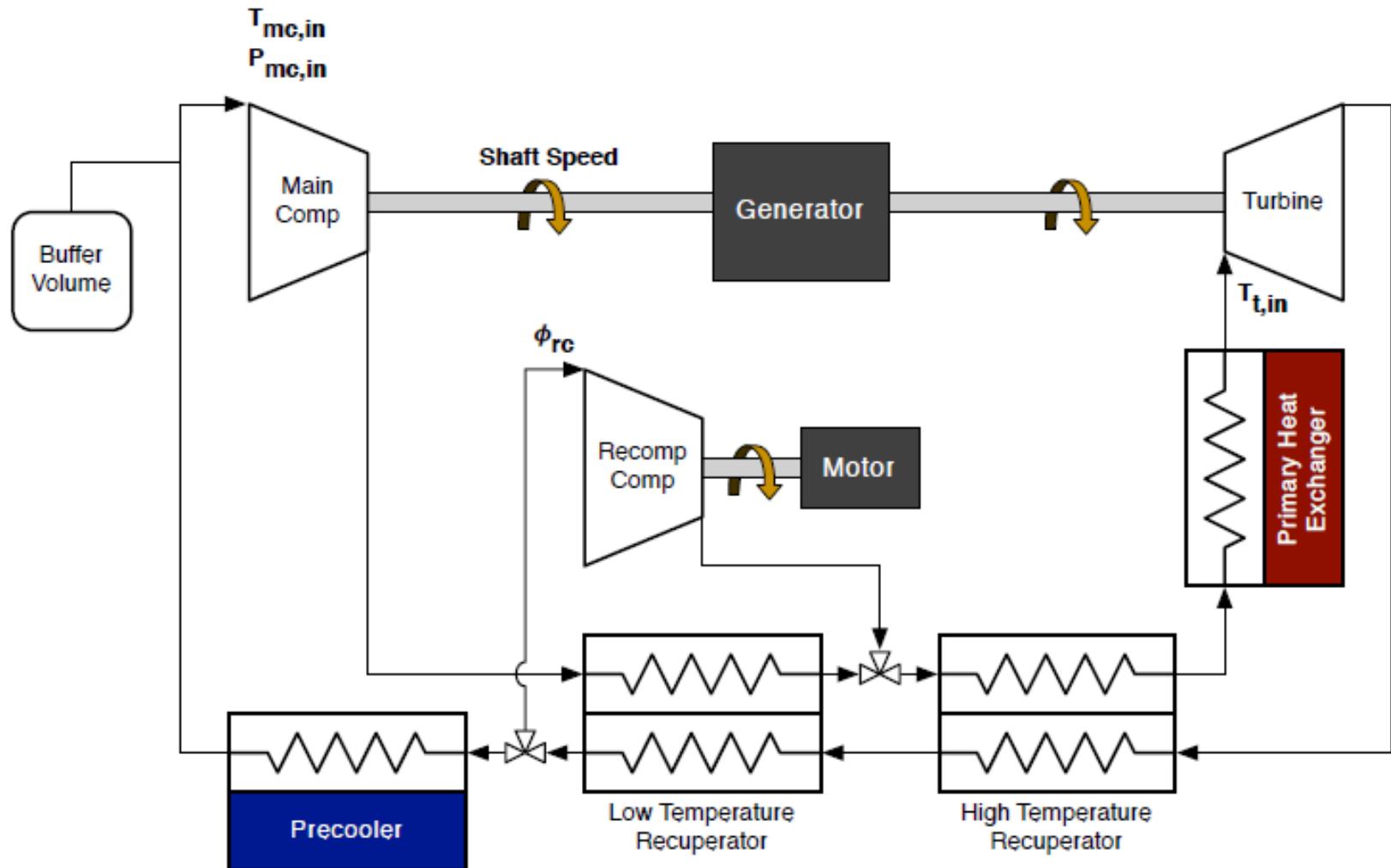
- The particle/sCO<sub>2</sub> heat exchanger test bed is a last step in an integrated solarized sCO<sub>2</sub> Brayton cycle demonstration
  - Sandia now has a falling particle receiver and RCBC equipment
  - Once tested, the SuNLaMP particle/sCO<sub>2</sub> heat exchanger could couple the falling particle receiver and RCBC system
- Hierarchical Bayesian analysis of sCO<sub>2</sub> Brayton cycle cost provides approximate confidence bounds with minimal data
  - Literature models exist for similar equipment but not for sCO<sub>2</sub>
  - Few vendor estimates or FOAK costs for sCO<sub>2</sub> designs exist
- Next steps
  - Complete final design and procurement for the sCO<sub>2</sub> support loop
  - Iterate power law fit parameter distributions in Bayesian analysis

# Backup Slides

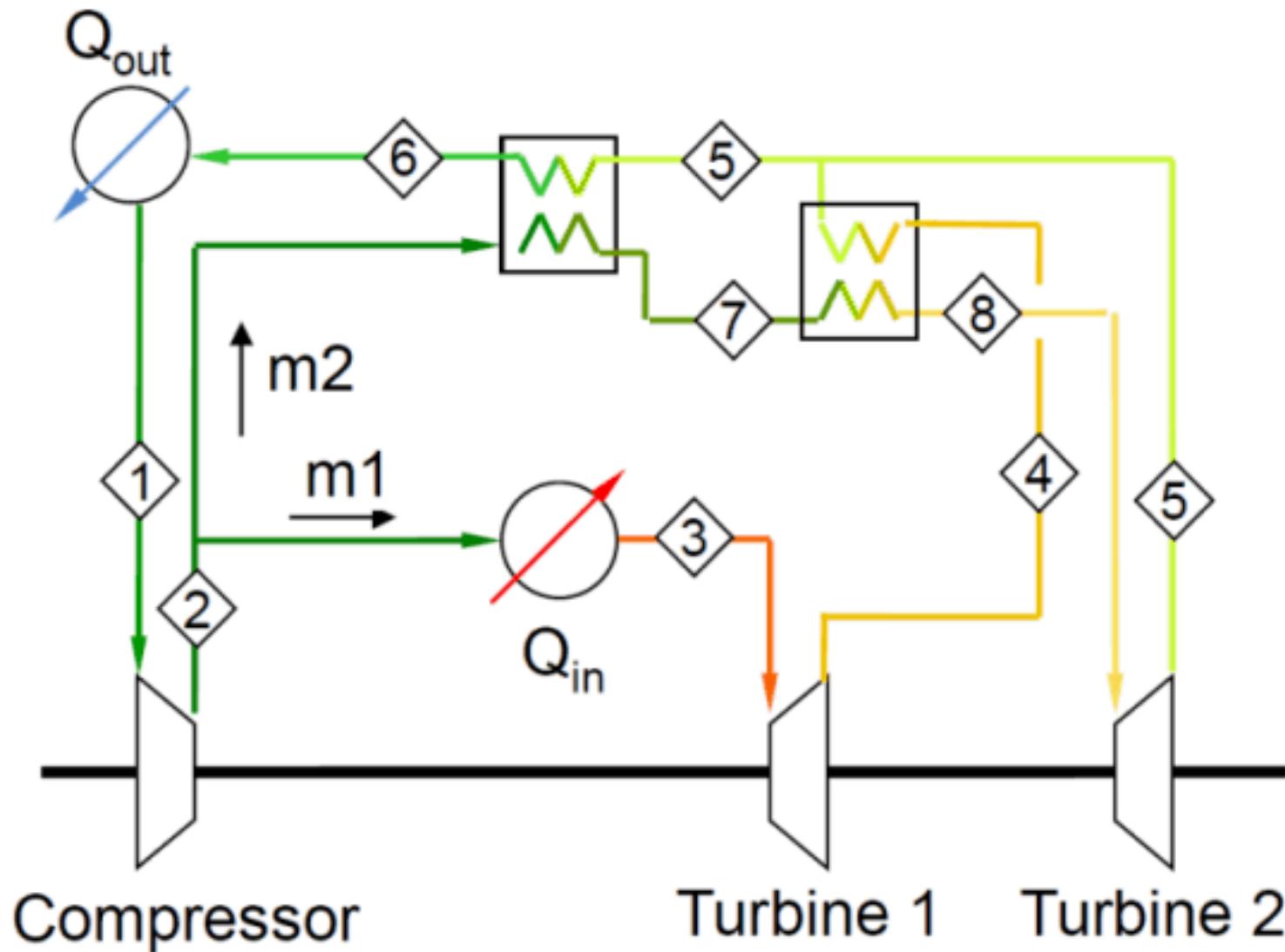
# Simple Closed Brayton Cycle (SCBC)



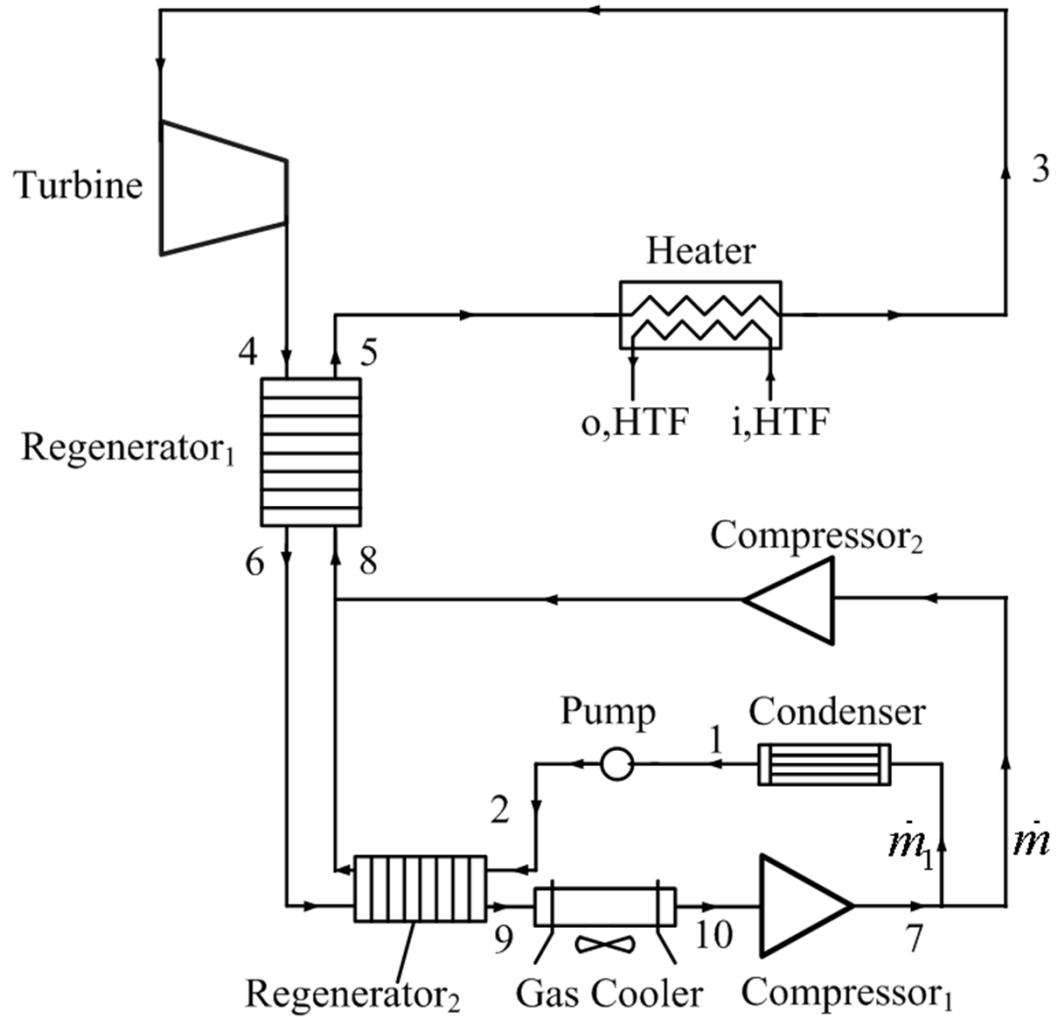
# Recompression Closed Brayton Cycle (RCBC)



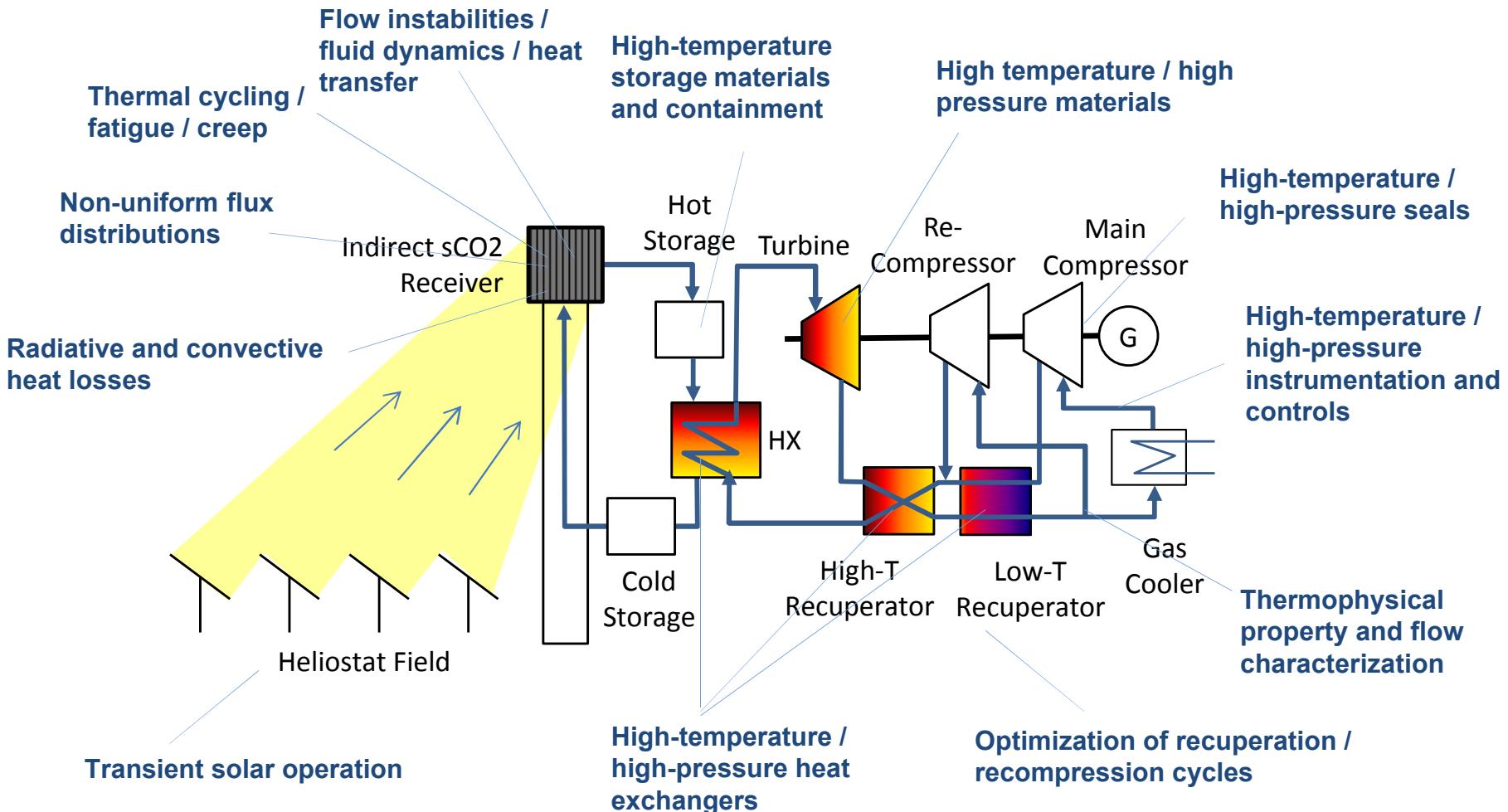
# Cascaded Closed Brayton Cycle



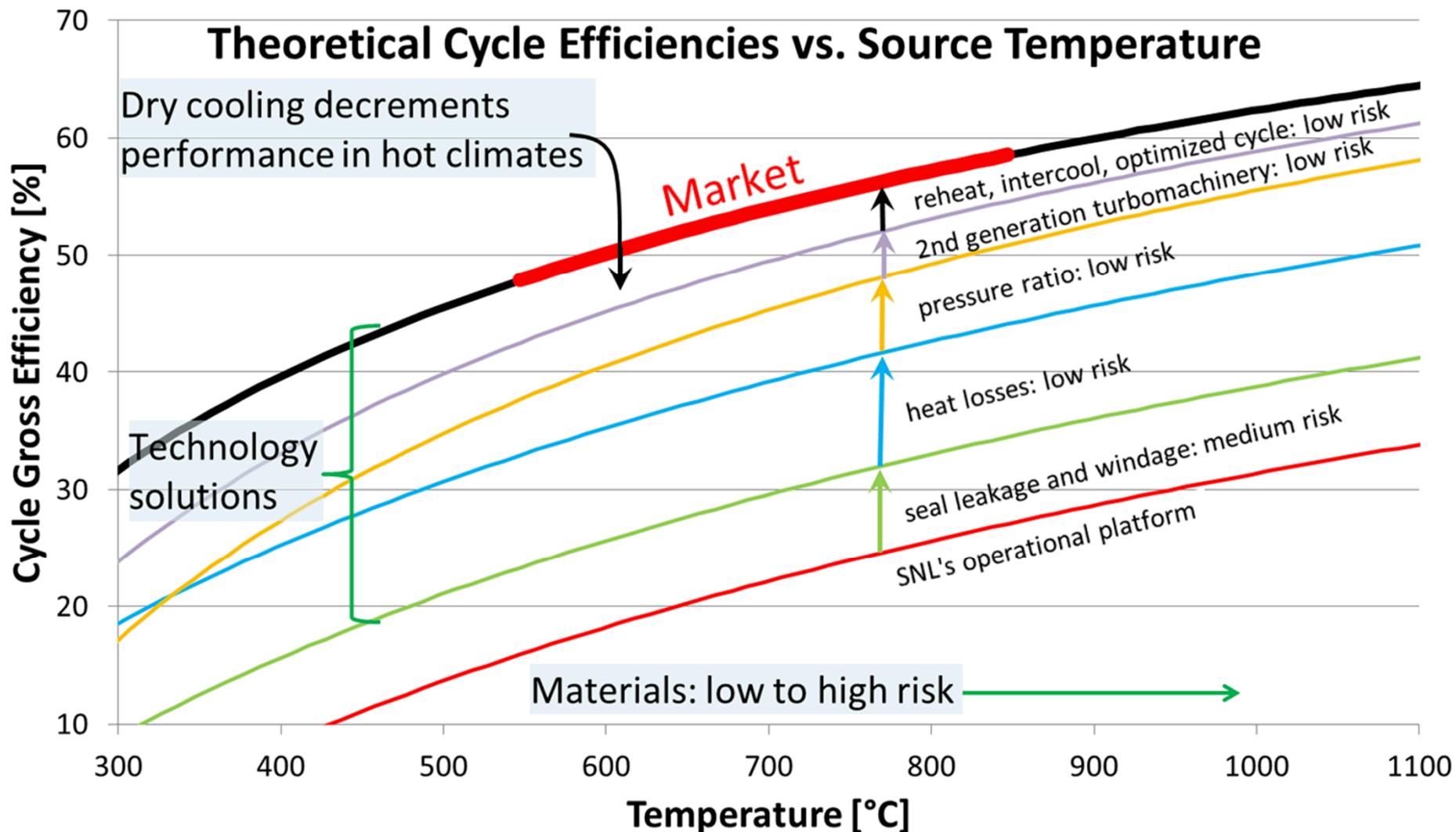
# Combination Bifurcation with Intercooler (CBI)



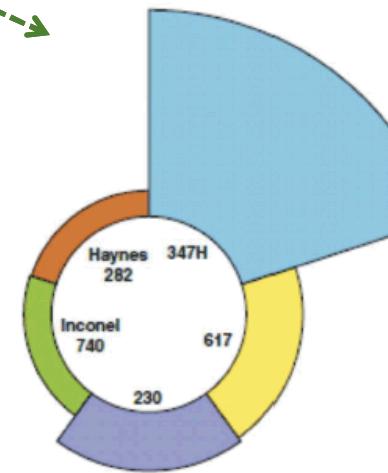
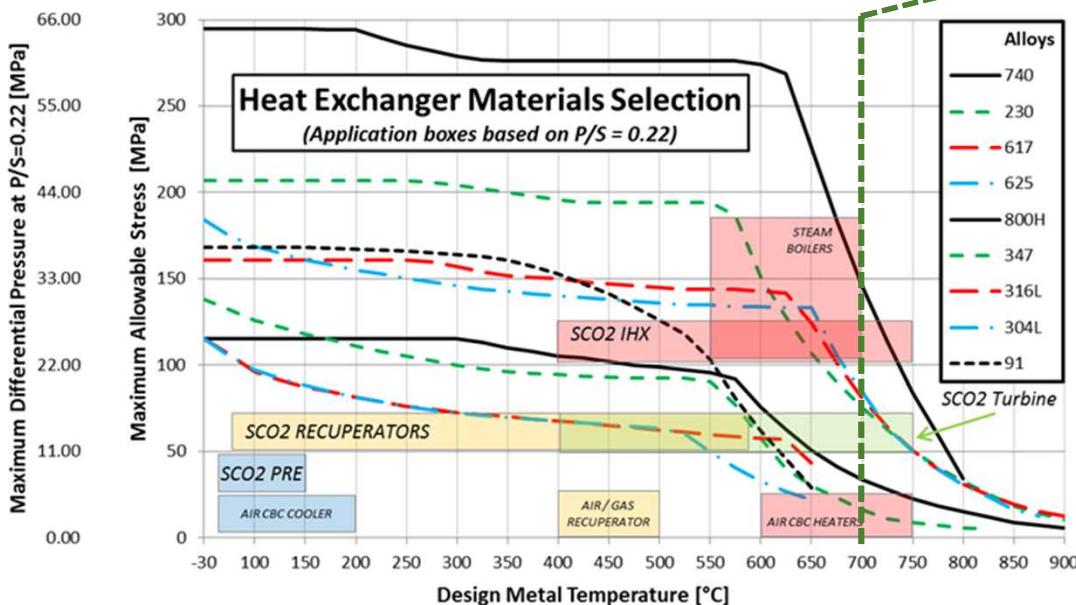
# Technical Challenges



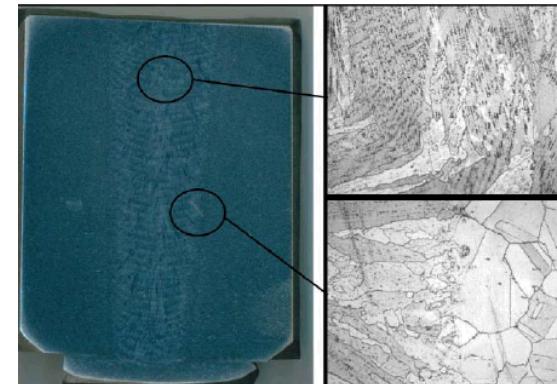
# Path to High Efficiency



# Materials are limited to <700C



Today: Repeatable 3" (75mm) thick Inconel 740 welds without cracking



- Advanced Ultrasupercritical (A-USC) research has advanced high temperature materials<sup>1</sup>
- Alloy 617 and 740 are leading candidates for such systems
  - 740 has recently been welded without cracking, more work is still needed to vet any materials issues<sup>1</sup>
- Little industrial experience exists and field testing is sparse.

1. Shingledecker, *Development of Advanced Materials for Advanced Ultrasupercritical (A-USC) Boiler Systems*, 2014

2. M. Carlson, "Options for SCO<sub>2</sub> Brayton Cycle Heat Exchangers," presented at the The 4th International Symposium on Supercritical CO<sub>2</sub> Power Cycles, Pittsburgh, PA, 2014.

# Assumptions for Centrifugal Pumps

- At any particular value of pump capacity, there is a distribution for the cost of the pump.
  - ✓ Distribution is assumed to be lognormally distributed since cost can't be less than zero, but theoretically could be as high as anyone wants to charge.
  - ✓ Garvey, et al, state that lognormal distributions can model the production costs of goods well.
- The mean values of the distributions at each capacity level are related to each other via a power law model.

$$Cost = \alpha_0 * Capacity^{\alpha_1}$$

- $\alpha_0$   $\alpha_1$  and the standard deviation ( $\sigma$ ) of the cost distributions are unknown.

# Process

- Treat unknowns as random variables.
- Assign a prior distribution to each of the unknown variables.
- Use Bayes' Theorem to update with the data.

# Bayes' Theorem

$$P(\theta|y)P(y) = P(y|\theta)\pi(\theta)$$

$$P(\theta|y) = \frac{P(y|\theta)\pi(\theta)}{P(y)} = \frac{P(y|\theta)\pi(\theta)}{\int P(y|\theta)d\theta}$$

all possible  
values of  $\theta$

$$P(\alpha_0, \alpha_1, \sigma|y) = \frac{P(y|\alpha_0, \alpha_1, \sigma)P(\alpha_0, \alpha_1, \sigma)}{P(y)}$$

$$= \frac{P(y|\alpha_0, \alpha_1, \sigma)P(\alpha_0, \alpha_1, \sigma)}{\int P(y|\alpha_0, \alpha_1, \sigma)d(\alpha_0, \alpha_1, \sigma)}$$

Using Monte Carlo simulation, the posterior distribution for the parameters can immediately be found. However, this involves sampling from a 3-dimensional distribution.

Instead, we can rewrite in such a way that we can sample from 3 one-dimensional distributions.

- $\theta$  represents a vector of unknowns ( $\alpha_0, \alpha_1, \sigma$ ).
- $\Pi$  represents the joint prior distribution for  $\theta$ .
- $y$  represents an observed data point (in our case, this would be a single cost/capacity observation for a centrifugal pump).
- $P(y|\theta)$  represents the assumed form of the distribution for data (lognormally distributed cost for a given mean and SD, which are determined by the triplet of  $(\alpha_0, \alpha_1, \sigma)$ ).

# Sampling Technique

$$P(\alpha_0^{t_1} | \alpha_1^{t_0}, \sigma^{t_0}, y^{t_0}) = \frac{P(\alpha_1^{t_0}, \sigma^{t_0}, y^{t_0} | \alpha_0^{t_0}) P(\alpha_0^{t_0})}{\int P(\alpha_1^{t_0}, \sigma^{t_0}, y^{t_0} | \alpha_0^{t_0}) d\alpha_0^{t_0}}$$

$$P(\alpha_1^{t_1} | \alpha_0^{t_0}, \sigma^{t_0}, y^{t_0}) = \frac{P(\alpha_0^{t_0}, \sigma^{t_0}, y^{t_0} | \alpha_1^{t_0}) P(\alpha_1^{t_0})}{\int P(\alpha_0^{t_0}, \sigma^{t_0}, y^{t_0} | \alpha_1^{t_0}) d\alpha_1^{t_0}}$$

$$P(\sigma^{t_1} | \alpha_0^{t_0}, \alpha_1^{t_0}, y^{t_0}) = \frac{P(\alpha_0^{t_0}, \alpha_1^{t_0}, y^{t_0} | \sigma^{t_0}) P(\sigma^{t_0})}{\int P(\alpha_0^{t_0}, \alpha_1^{t_0}, y^{t_0} | \sigma^{t_0}) d\sigma^{t_0}}$$

- This represents a single iteration of the MCMC process.
- The process is repeated thousands of time until the posterior distribution changes very little.
- At this point, it is assumed that the distribution has converged to a point that is very close to the stationary distribution.

# Monte Carlo Simulation

- Monte Carlo – a numerical technique based on probability theory which is used for calculating the value of an integral
- Define:  $I \equiv \int h(x)dx = \int \frac{h(x)}{\omega(x)}\omega(x)dx$
- Now, suppose  $\omega(x)$  is a probability density function. Then, the integral,  $I$ , is the expected value of  $\frac{h(x)}{\omega(x)}$  which, according to the Law of Large Numbers, can be approximated by

$$I \approx I_N \equiv \frac{1}{N} \sum_{t=0}^{N-1} \frac{h(x_t)}{\omega(x_t)}$$

- Note that the number of samples,  $N$ , required for a good approximation, can be reduced by choosing the appropriate function  $\omega(x)$  .

# Markov Chains

- Markov Chain – A model of a system in which the state of a system (including all associated probabilities) at time  $t+dt$  depends only upon the state of the system at time  $t$  (i.e., times prior to the present do not influence the future).

$$\vec{P}(t_{i+1}) = T \vec{P}(t_i)$$

- In this expression,  $\vec{P}(t)$  is a vector representing the probabilities of various states at time  $t$  and  $T$  is the transition matrix, which contains the probabilities of transitioning from state to state.

# Markov Chains, cont.

- Stationary Distribution – The limiting distribution of a Markov process. A stationary distribution will exist if:
  - The transition matrix,  $T$ , is time homogeneous
  - It is possible to transition from any state to any other state, given enough time (this property is called irreducibility)
  - Given any current state, there is a finite expected time to return to that state (i.e., all states are positive recurrent)

# Markov Chain Monte Carlo

- Markov Chain Monte Carlo is a technique by which an approximate distribution is sampled and successively updated until the distribution is deemed to be “close enough” to the desired stationary distribution.
- The stationary distribution is the desired state.
- For our system, a state is defined by a particular set of values for the five parameters of the release model and the data that we have.