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DOE HANDBOOK

AIRBORNE RELEASE FRACTIONS/RATES AND RESPIRABLE FRACTIONS FOR NONREACTOR NUCLEAR FACILITIES

Volume I - Analysis of Experimental Data



U.S. Department of Energy
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AREA SAFT



Computational Capability to Substantiate DOE-HDBK-3010 Data (NSRD-11) Status

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Outline

- Motivation to substantiate DOE-HDBK-3010 data
- Our approach
 - Sandia high-fidelity codes
 - Substantiate the experimental data
- Year 1 accomplishment (NSRD-6)
 - Liquid fire simulations
 - Exploratory simulations
- Year 2 progress (NSRD-11)
- Year 3 proposed research

Why Substantiate the Handbook?

- Safety analysts at DOE complex rely heavily on the data provided in this Handbook to determine the source term (ST)
- Five Factor Formula
 - $ST = MAR \cdot DR \cdot ARF \cdot RF \cdot LPF$
 - MAR - material at risk, DR – damage ratio, ARF – airborne release fraction, RF – respirable fraction & LPF – leak path factor
- More often, analysts simply take the bounding values to perform ST calculations to avoid regulatory critique
- Derived data (i.e., ARF & RF) from Handbook:
 - Very limited table-top and bench/laboratory experiments
 - Engineering judgement which may not have adequate bases
 - Actual situation may not be represented

Technical Approach/Benefits

- To leverage the state of art 3-D integrated computer codes developed at Sandia – Sierra Code Suite to substantiate the data in the Handbook:
 - Demonstrate that our codes can substantiate table-top and laboratory experiments in the Handbook, and thus justify using codes for more accurate safety analysis
 - Provide physical insights into the events that leads to the airborne release
 - Provide data assessment for the realistic accident conditions
- The goal of this approach is to ensure the accuracy and technical defensibility of the airborne release safety analyses
 - Non-conservative data – underestimates ST – safety concern
 - Over-conservative data – overestimates ST – Substantial cost to DOE/NNSA

Sandia Sierra Code Suite

- Sierra code suite includes solid mechanics (i.e., SIERRA SM, PRESTO), structural dynamics, fluid mechanics (i.e., SIERRA FM, FUEGO) and a number of utilities that can be coupled for simulating multi-physics problems
- This code suite is compliant with DOE Order 414.1D (SAND2008-5517)
- The codes are installed on supercomputing clusters at Sandia, and readily available for use within Sandia
- There is no license fee associated with the usage
- Use and information release are subject to approval

Year 1 Accomplishment

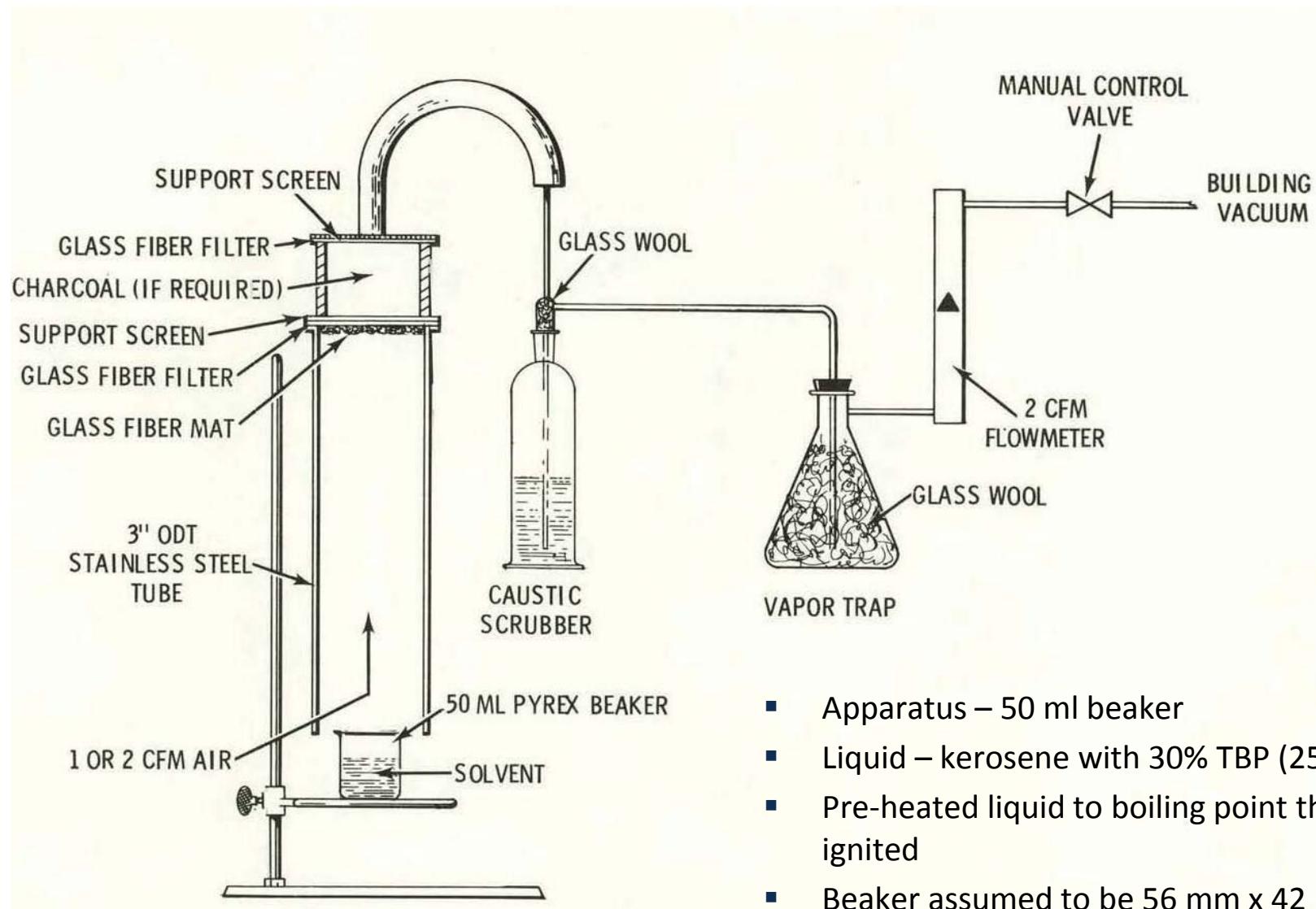
- Liquid fire experiment simulations
 - Beaker fire
 - Gasoline pool fire
 - Simulation results with experimental data
- Exploratory simulations
 - Impact on a powder can
 - Pressurized powder release
- Final report published (SAND2015-10495)
 - Recommendation for FUEGO improvement
 - Resuspension
 - Multi-component capability

Simulation of Liquid Fire using FUEGO in Year 1



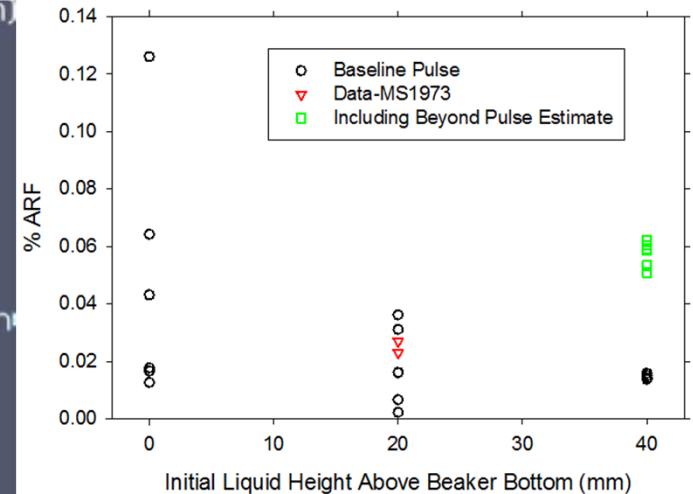
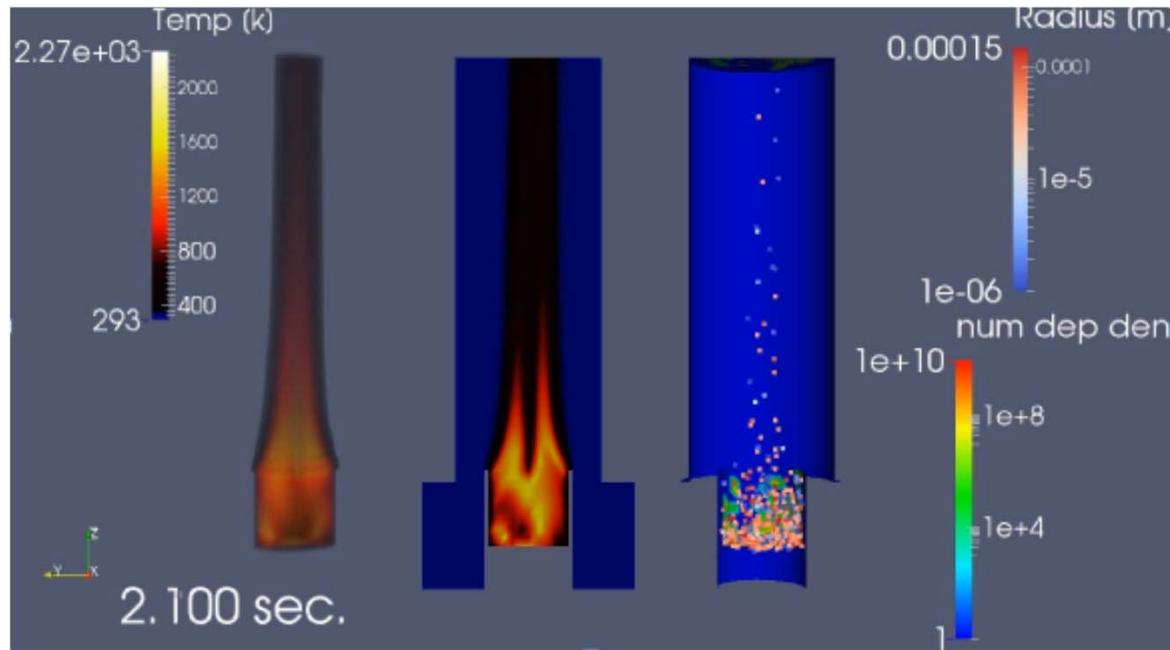
- Chapter 3 of Handbook discusses release related to liquids
- From other work, we have demonstrated that SIERRA code suite (PRESTO/FUEGO) can be used to simulate an explosion accident involving combustible liquids
 - Similarly, we believe we could simulate liquid nuclear excursion using the combination of Liquid explosion – chemical energy and by-product
 - Nuclear excursion – fission energy and fission product
- We currently simulate liquid fire experiments described in the Handbook (Section 3.3)
 - Beaker fire (BNWL-B-274)
 - Gasoline pool fire (BNWL-1732)

Beaker Fire (BNWL-B274)



- Apparatus – 50 ml beaker
- Liquid – kerosene with 30% TBP (25 ml)
- Pre-heated liquid to boiling point then ignited
- Beaker assumed to be 56 mm x 42 mm diameter

Beaker Fire FUEGO Simulation

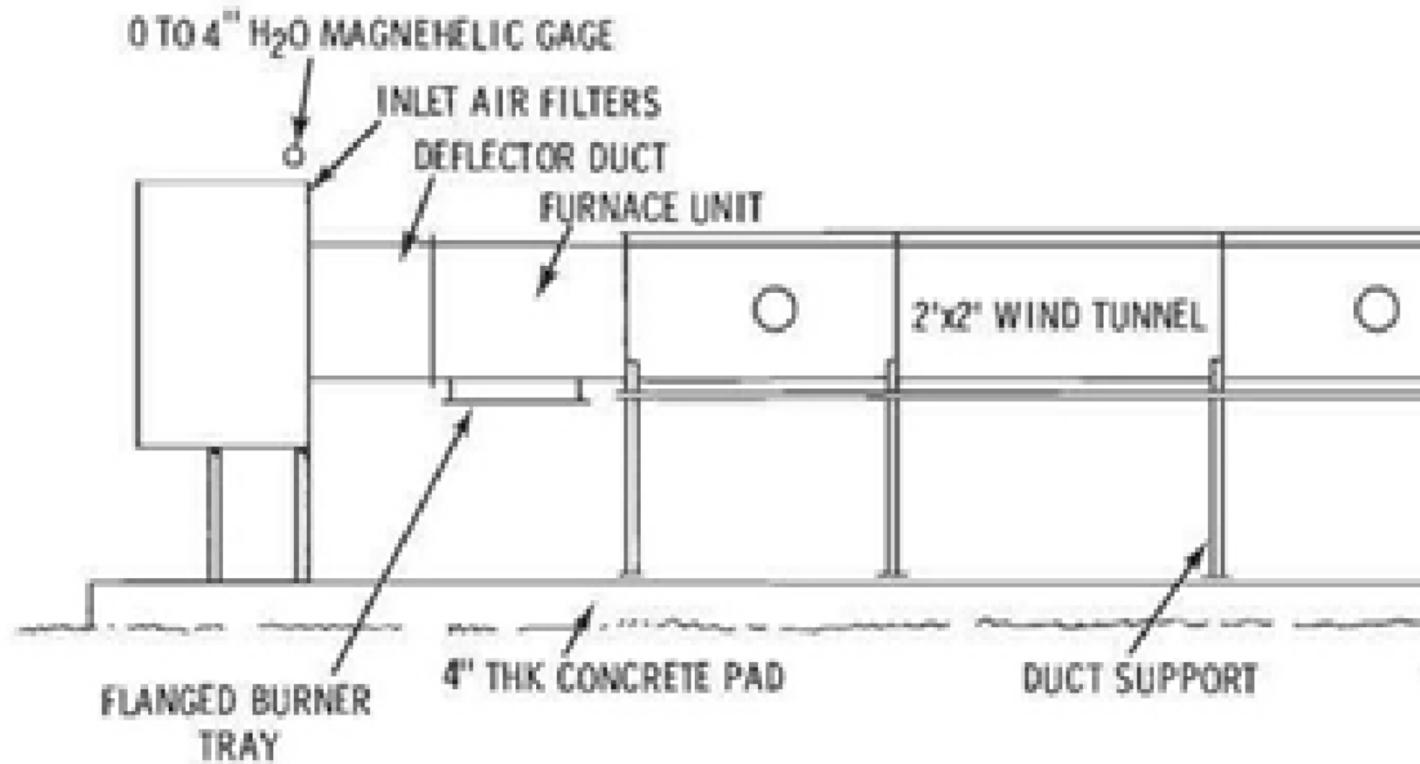


Findings:

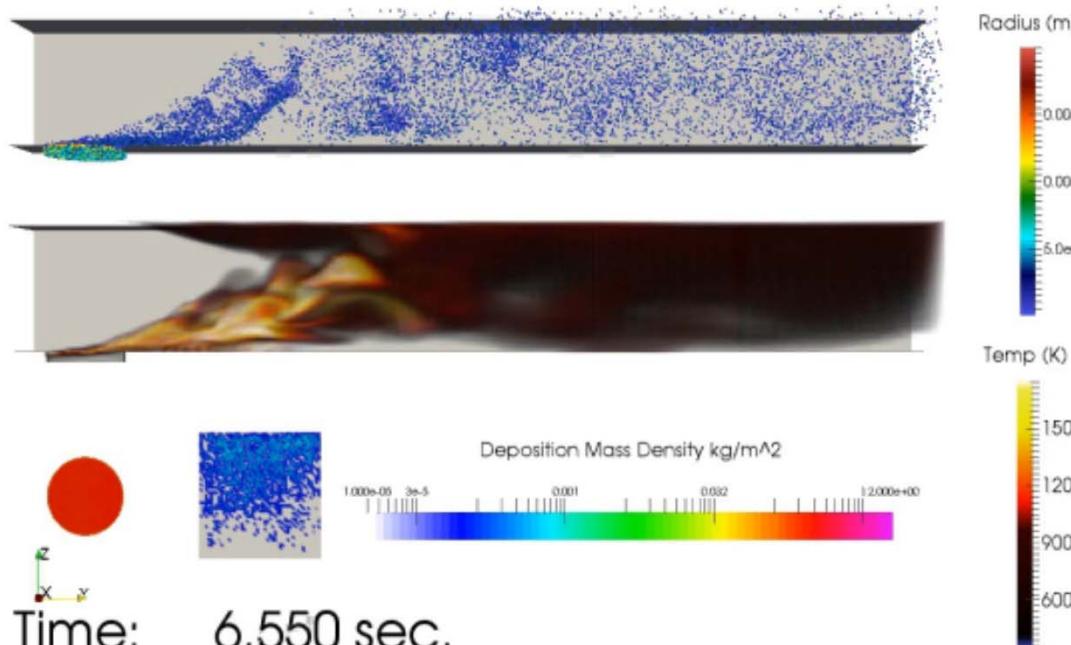
- Only a single initial liquid height was used in the experiment
- Simulation compared well with the data
- FUEGO did not have particle interaction model
- **Code results can be improved with multi-component evaporation capability**
 - Larger droplets tended to stay behind

Gasoline Pool Fire (BNWL-1732)

- 1 gallon gasoline onto pan surface
- UO_2 powder, 20-50 g poured before gasoline
- Pan size 15-inch diameter tray used

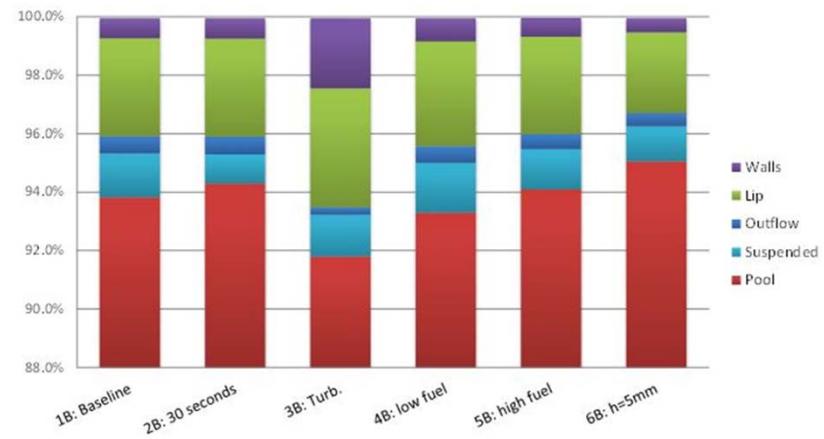
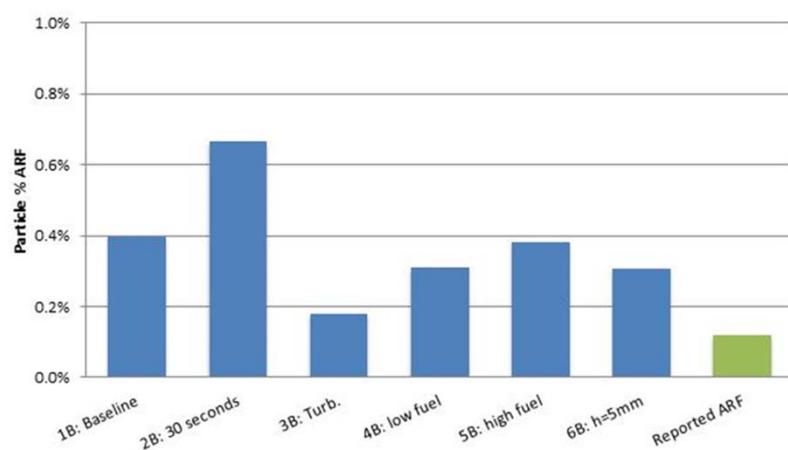


Simulation Visualization for Gasoline Pool Fire



Findings:

- Entrainment due to boiling dominates compared to the evaporation-induced in code results
- Resuspension model needs to accurately capture the residual entrainment after the fire was gone.
- FUEGO did not model particle interactions

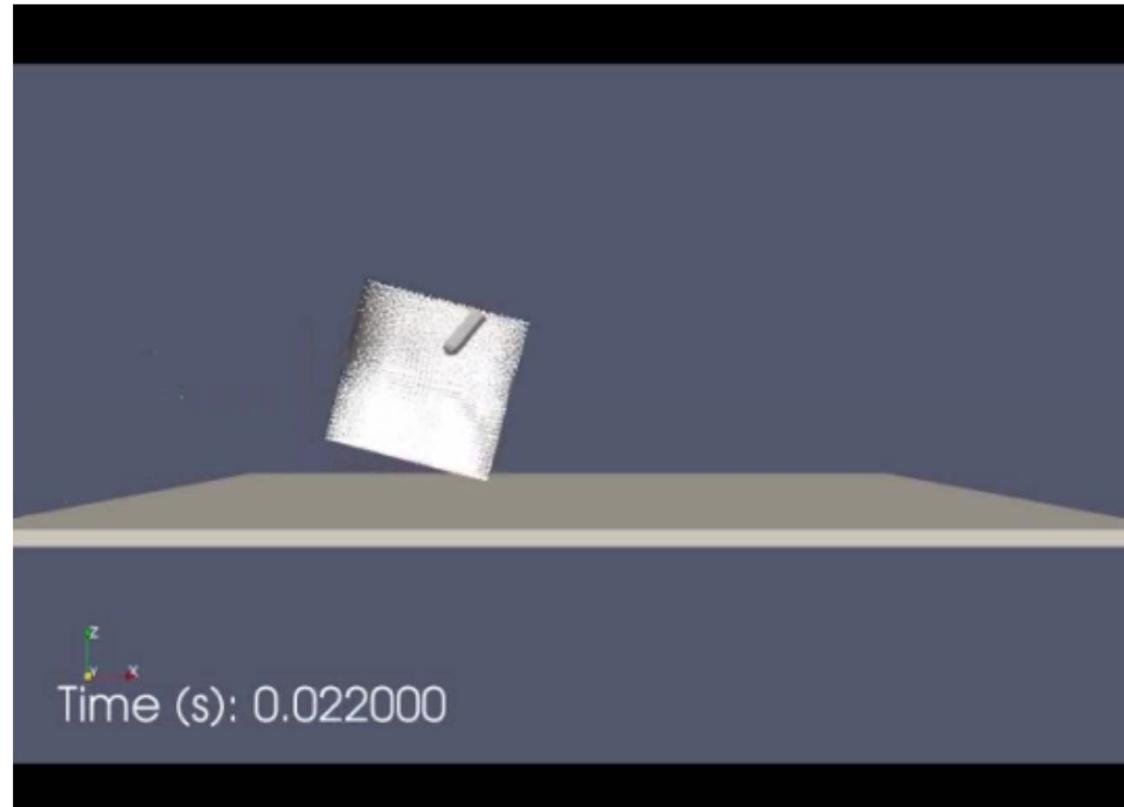
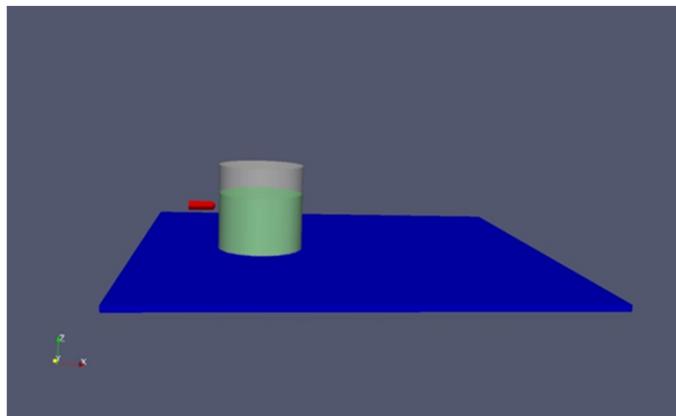


Exploratory Simulations in Year 1



- We focused on powder release in Chapter 4 of Handbook
- We selected two powder scenarios to simulate using PRESTO and FUEGO to address explosion-induced impact and pressurized dispersion
 - An object hitting a can filled with powder (Postulated)
 - PRESTO
 - A pressurized release of powder from a chamber into a containment volume (FUEGO)
 - Discussion on this simulation defers to Year 2

Projectile Impact Powder Can at 175 m/s



Simulation Results:

- PRESTO can be used to provide more realistic impact estimates compared to hand calculation using DOE/TIC-11268 "A Manual for the Prediction of Blast and Fragment Loading on Structures".
- This is a demonstration, no experiment is available.

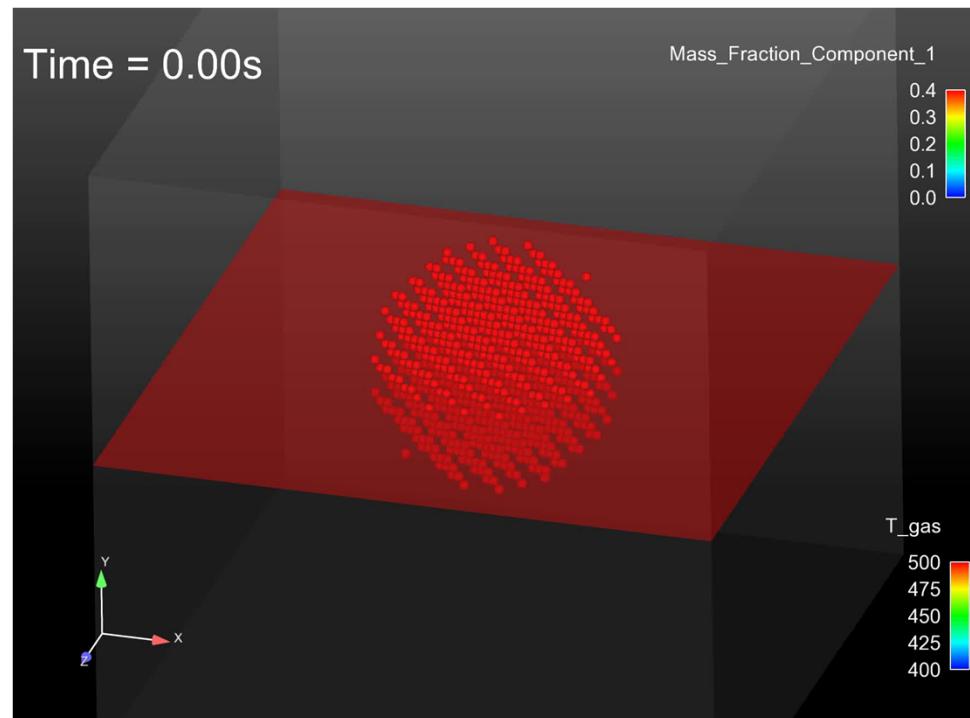
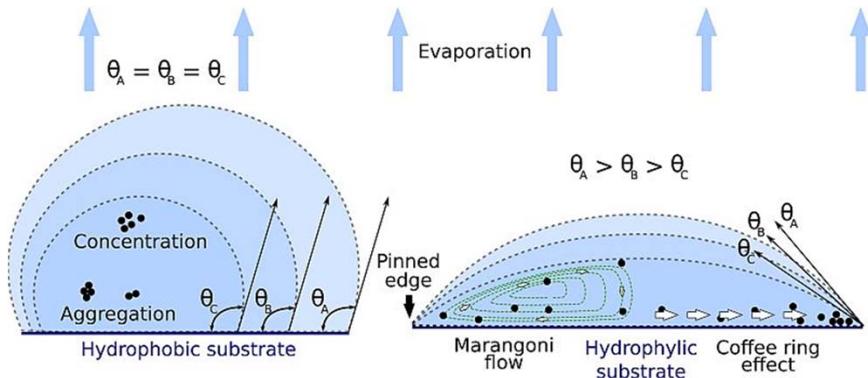
Year 2 - Progress

- Task 1 – FUEGO code improvement
 - Resuspension Model (discussed in Task 2)
 - Multi-component Model (applicable to Task 3)
- Task 2 – Validate resuspension model
 - In progress – 1967s experiment from the Handbook, and STORM experiment
- Task 3 – re-run of liquid fire simulations from Year 1
 - (not yet started)
- Task 4 – re-run the pressurized powder release simulations from Year 1
 - In progress – 50 psig case
 - Spill simulation for NSRD-10 project
- Task 5 – Fragmentation Analysis
 - In progress
- Task 6 – final report

Task 1A – Resuspension Model

- An User function was implemented into FUEGO instead of an user subroutine
- Wichner resuspension Model is based on a similar model implemented into MELCOR (SAND2015-6119)
 - The model uses the balance forces of the lift and adhesive forces at the surface.
 - Resuspension is based on the particle size, fluid velocity, wall shear stress, surface roughness
 - This model may be good for high values of Reynolds number
 - For fires, where the fluid velocity may be low, the model has not been working successful – improvement is being developed
 - See Task 2 for test cases

Multicomponent Evaporation (Task 1B)



In FUEGO, implemented multicomponent evaporating particle model

- Particle can be composed of any number of constituent materials
 - distinct (and evolving) mass fractions
 - different physical properties
 - Inert components can be included

Simulation Example:

Spherical array of 683 evaporating liquid droplets with 2 distinct components (1, 2).

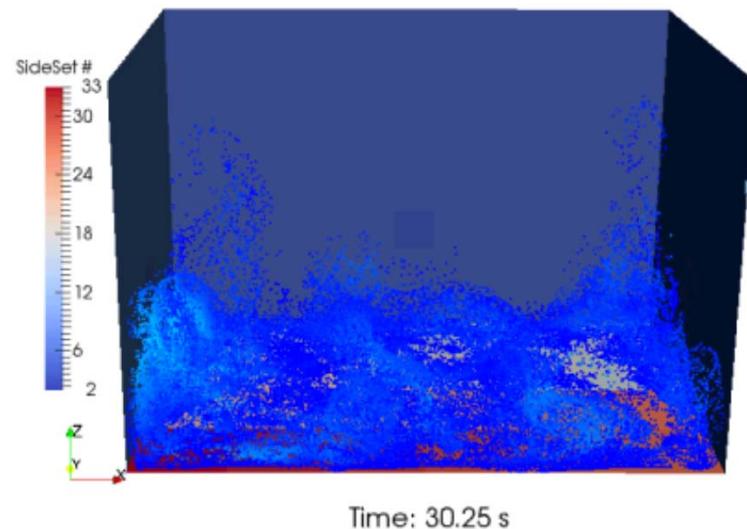
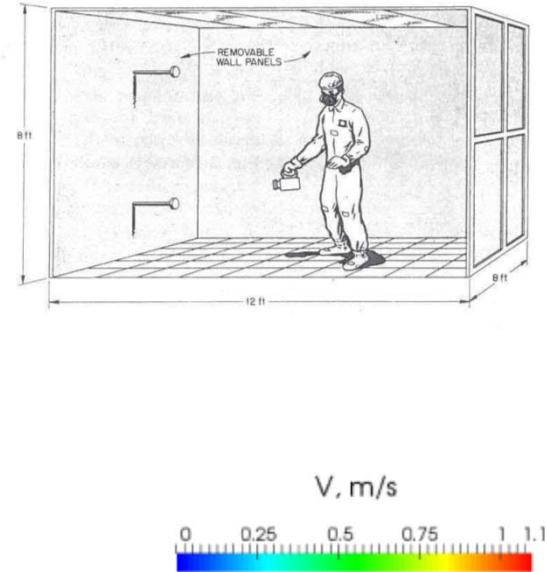
At start

- $\text{mass_fraction}(1) = 0.4$
 - $T_{\text{gas}} = 500$ (volume and boundaries)
- As droplets heat, A evaporates more quickly than B (distinct material properties)
- $\text{mass_fraction}(1) \rightarrow 0$
 - $\text{mass_fraction}(2) \rightarrow 1$

Due to evaporative cooling, T_{gas} near droplet array is lowered (thermal energy of gas is depleted to evaporate droplets)

Task 2 – 1967 Resuspension Exp.*

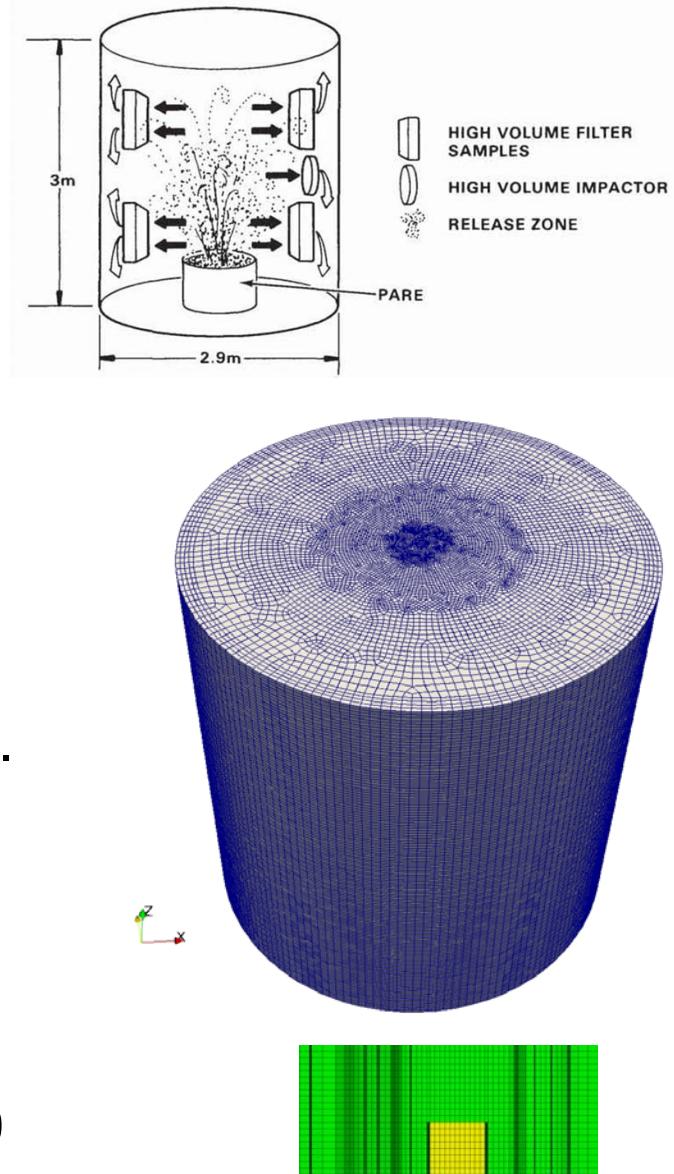
- Data used in Handbook p. 4-93 are poorly characterized
- One of the relatively better characterized experiments documented in “Redisposition of Settled Particulates,” B. R. Fish, R. L. Walker, G. W. Royster, and J. L. Thompson, 1967.
- Resuspension factor (surface concentration/atmosphere concentration, m^{-1})
 - Vigorous work-sweeping: $1.9 \times 10^{-4} \text{ m}^{-1}$
 - Walking: $3.9 \times 10^{-5} \text{ m}^{-1}$
 - Light work: $9.4 \times 10^{-6} \text{ m}^{-1}$
 - Light sweeping: $7.1 \times 10^{-4} \text{ m}^{-1}$
 - Pedestrian and equipment: $4.6 \times 10^{-3} - 5 \times 10^{-5}$
- Preliminary FUEGO Simulation
 - Element size is sufficient to capture integral/Taylor eddies.
 - Each of 24 floor sidesets (boundaries) has time-dependent x-y-z velocity components (u, v, w velocities).
 - Floor sidesets mimic walking and sweeping motion.
 - Each sideset is activated and deactivated as man walks and sweeps through room.
 - 100,000 particles are tracked; All on floor at transient initiation.
 - Used particle “stick” option for ceiling and walls.
 - Floor has Wichner resuspension model



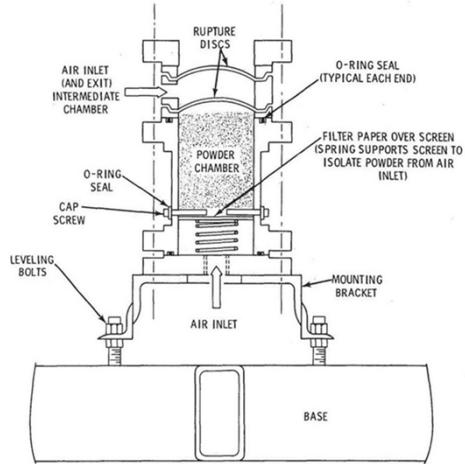
*B.R. Fish, et.al, “Redisposition of Settled Particulates,” in Surface Contamination, B.R. Fish (ed.), Pergamon Press, 1967

Task 4 - FUEGO Model

- Mesh metrics compliant with NRC, CFD journal recommendations.
- 1.03 million hexahedral elements with radial biasing near higher-velocity regions.
- Element size is sufficient to capture integral/Taylor eddies.
- Dynamic Smagorinsky LES turbulence.
- Each filter/impactor has its own time-dependent air flow boundary.
- 100,000 particles are tracked.
- Particle “stick” option for the filters and walls.
- Applications for
 - Spill case (PNL-3786)
 - Pressurized case (PNL-4566)
 - Model improved from Year 1
 - Results will also provide inputs for MELCOR model developed in NSRD-10



50 psig Pressurized Release - FUEGO (Task 4)

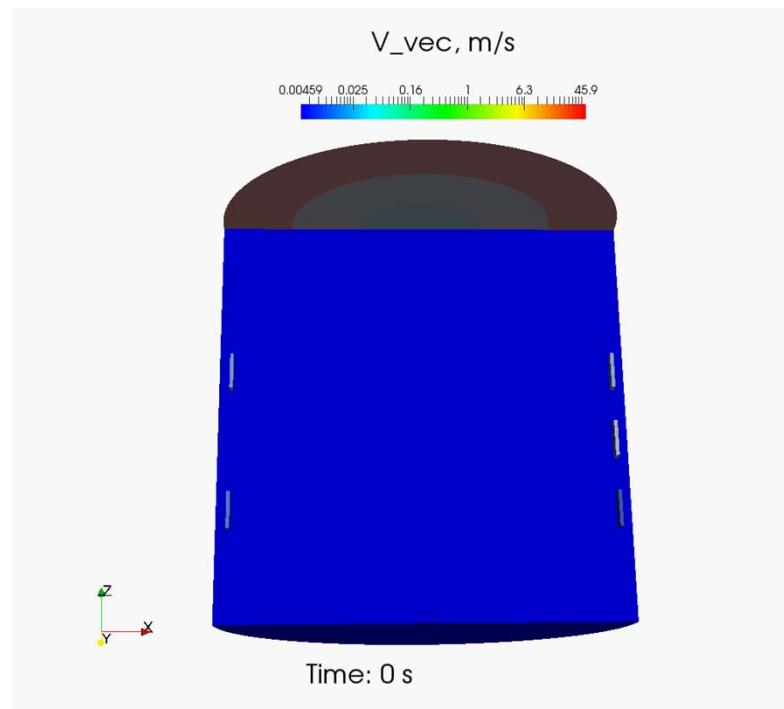
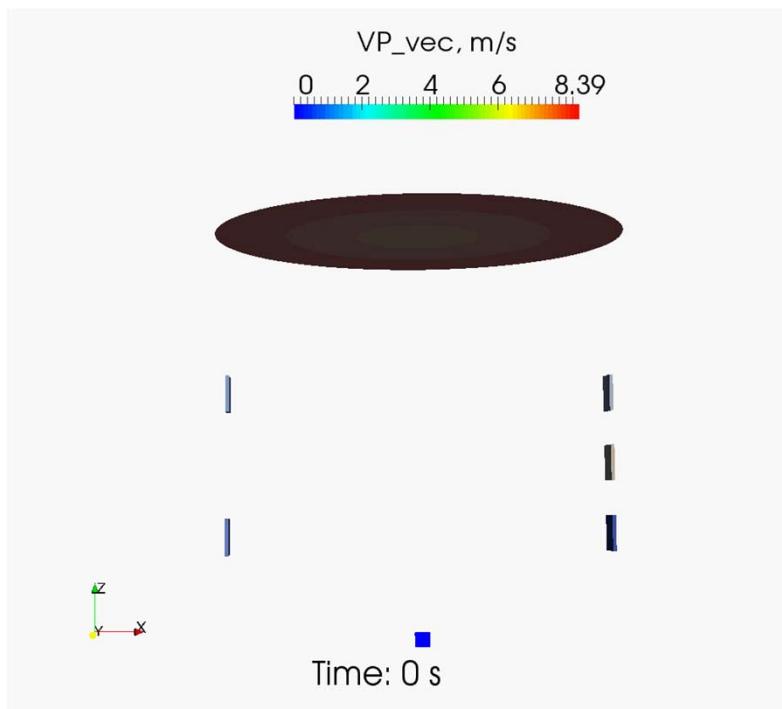


Simulation inputs:

- Rupture disk timing
 - 0 m/s @ 0.001 s
 - 643 m/s @ 0.0015 s
 - 643 m/s @ 0.015 s
 - 0 m/s @ 0.016 s

Preliminary Simulation Results

- Particle size of 1.7 μm
- Calculated fluid and particle velocity distributions (top and bottom figs., respectively).
- Ran for 100 s.
- Particles first hit top surface at 5 s.

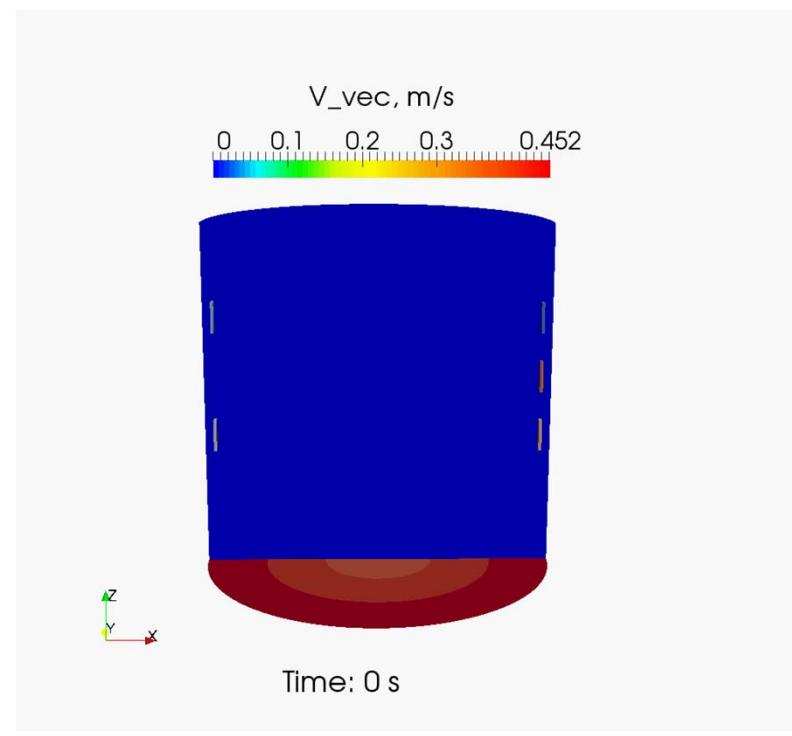
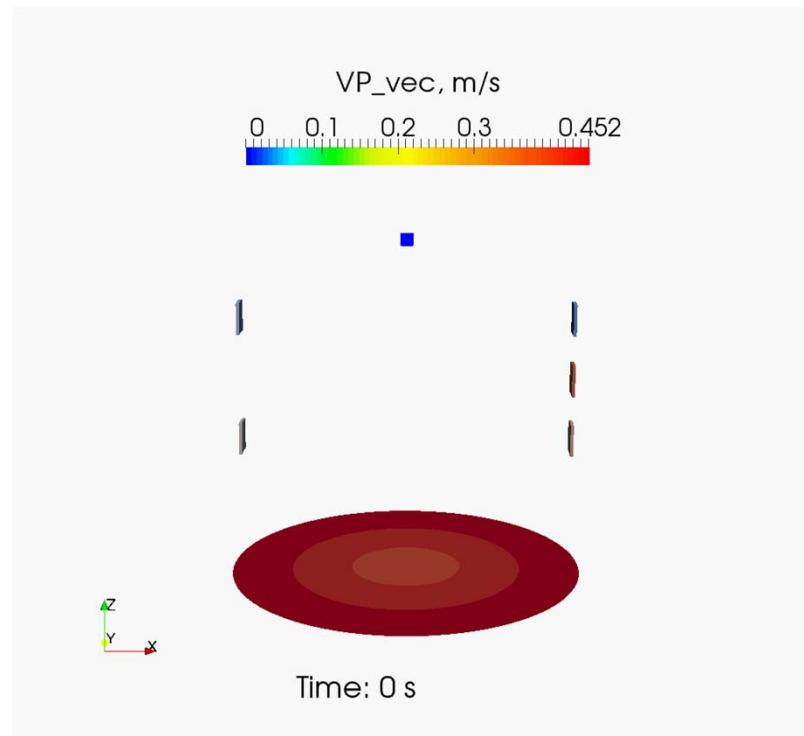
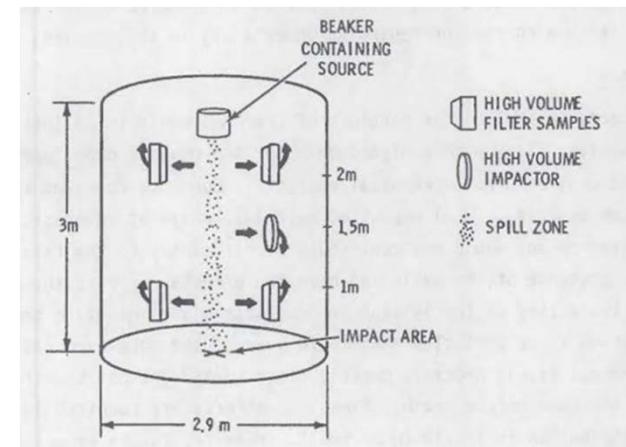


Spill Simulation – FUEGO (Task 4)

Preliminary Simulation Results:

- Particle size – $1.7 \mu\text{m}$
- Calculated fluid and particle velocity distributions (top and bottom figs., respectively).
- Simulation runs to 490 s of 30 minutes of experiment time
- The simulations show dust clusters first reached the bottom at ~ 50 s.

- Sampling has a ramp time of 1 s
- Filters @ 0.452 m/s
 - Impactor @ 0.181 m/s



Task 5 –Fragmentation Analysis

- Section 4.3.3: Non-Metallic or Composite Solids, Free-Fall Spill and Impaction Stress: ANL-82-39

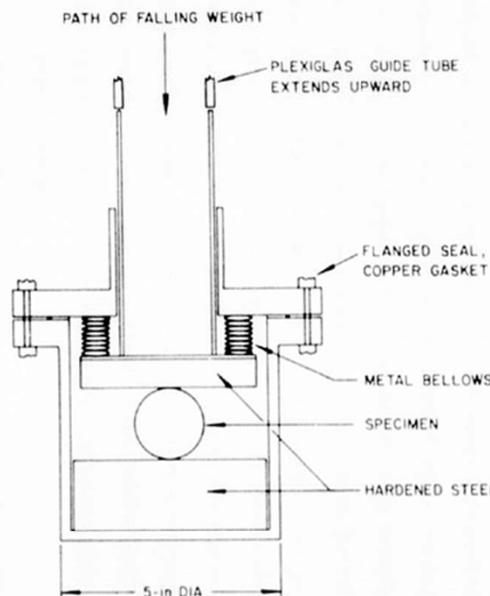
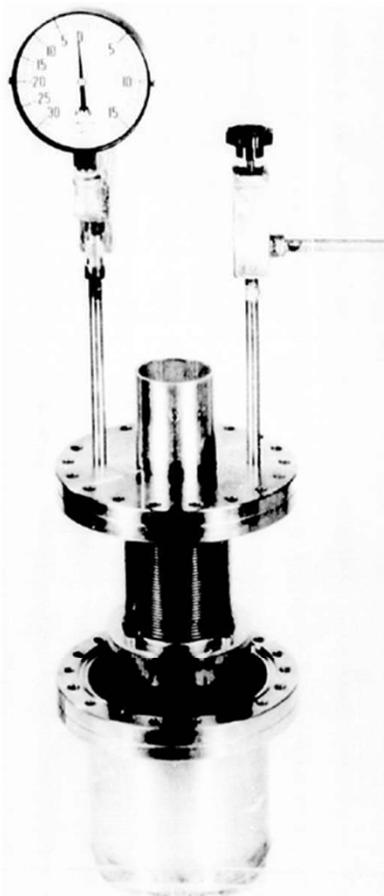


Fig. 10. Bellows Chamber for Impacting Brittle Specimens

$$ARF \times RF = (A)(P)(g)(h) \quad (4-1)$$

where: $ARF \times RF = (Airborne Release Fraction)(Respirable Fraction)$

A = empirical correlation, $2E-11 \text{ cm}^3 \text{ per g-cm}^2/\text{s}^2$
 P = specimen density, g/cm^3
 g = gravitational acceleration, 980 cm/s^2 at sea level
 h = fall height, cm.

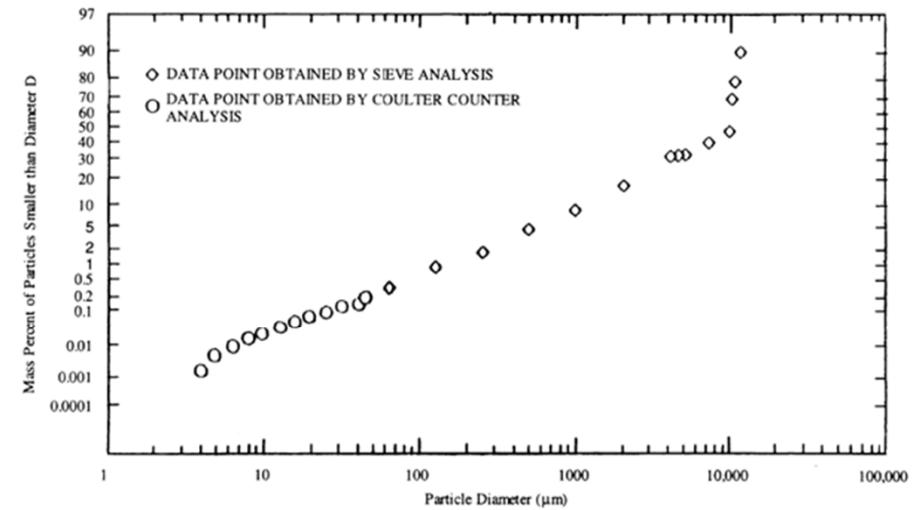


Figure 4-12. Particle Size Distribution Resulting for UO_2 -2 Pellet Impact Test
 Data for UO_2 Specimen #2 Including Mean Grain Size of Original
 Crystalline UO_2 Particles. (Size Distribution 3 Pellets 13.7-mm diameter x
 13.6-mm long; drop-weight 1.2 J.cm^3 .)
 (Jardine, et. al. 1982)

Initial Demonstration Problem

Modeling Approach

Large Range of Length Scales Involved in Problem

- Test Specimen Geometry: 0.137 m x 0.136 m
- Particle Size of Interest $< 10 \mu\text{m}$
- Disparity in Length Scales: **4+ Orders of Magnitude**

Two-Scale Model Approach

- Macro-Scale → Macro-Fragmentation & Boundary Conditions
- Micro-Scale → Micro-Fragmentation/Particle-Size-Distribution

Macro-Scale Model

SIERRA/SM (PRESTO) - Explicit Transient Dynamic FEA

Micro-Scale Model

Micromorphic Continuum Mechanics Approach
Elasto-Dynamic Model with Cohesive Zone Based
Fragmentation Model

Test Case

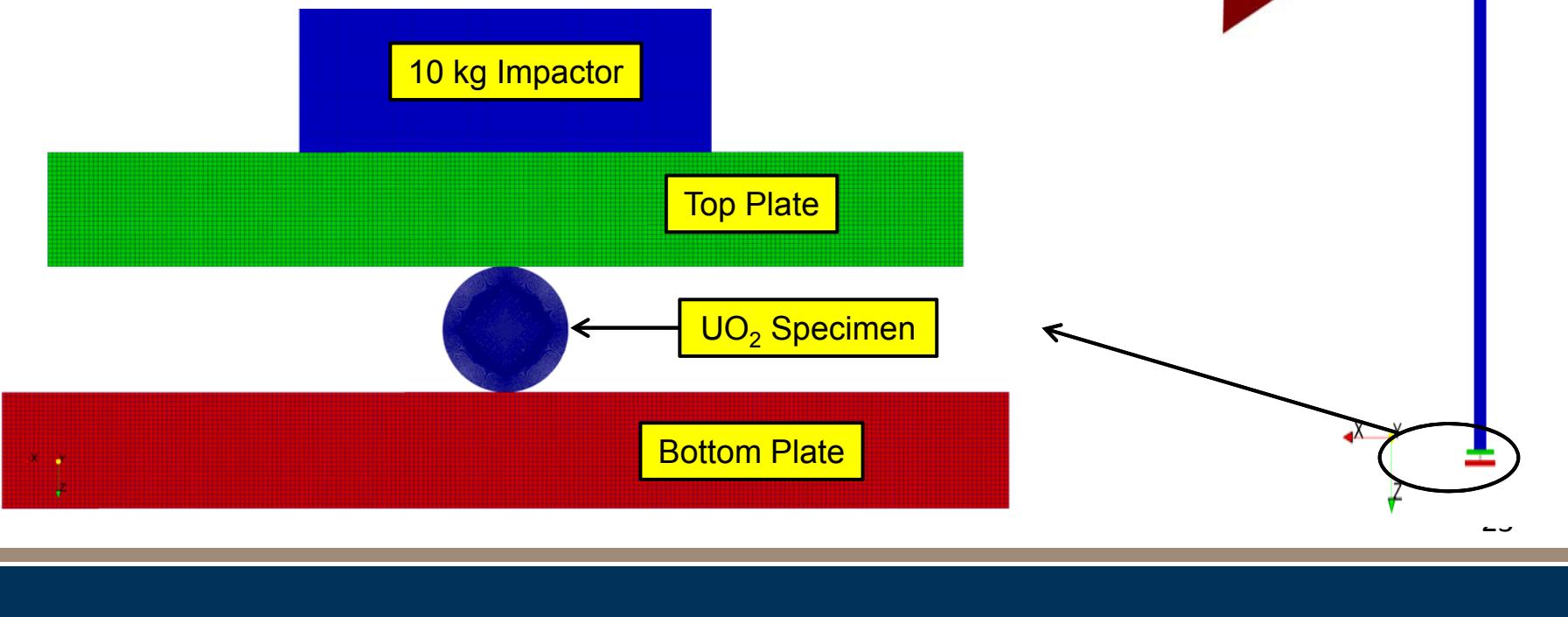
- ANL - UO₂ Diametral Impact
- 10 kg Impactor Dropped 0.0734m (1.2 J/cm³)

Macro-Scale Finite Element Model

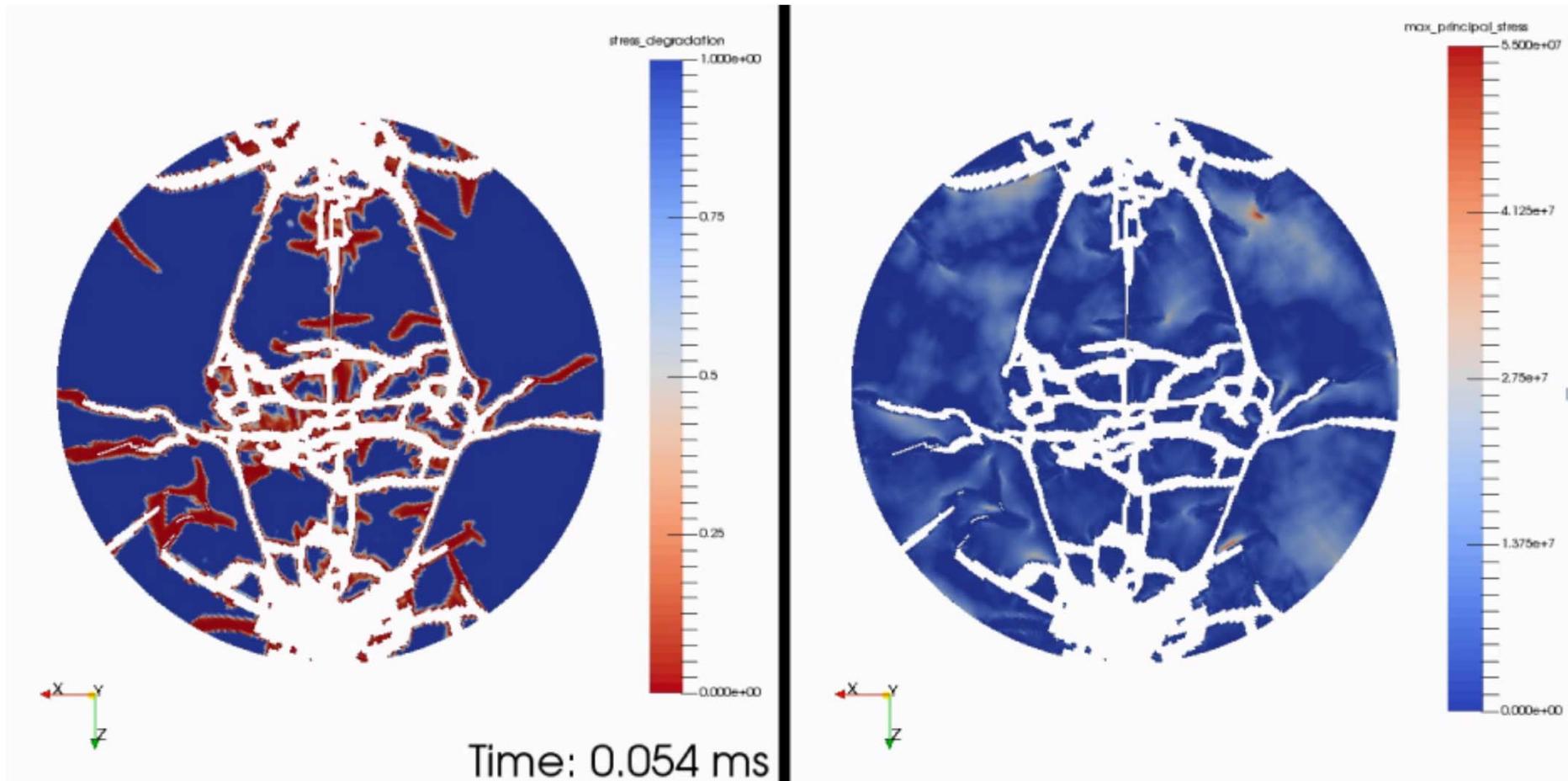
- Plane Strain "Slice" 

Micro-Scale Model

- 1-D Micromorphic Model with Fragmentation

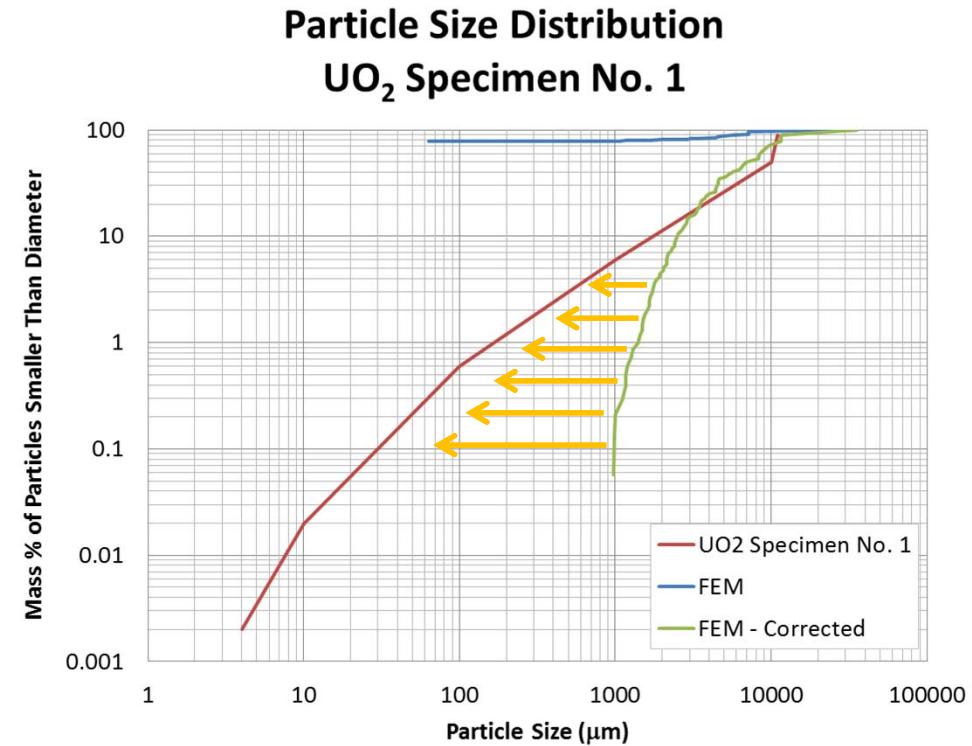


Preliminary Macro Scale Results



Micro-Scale Fragmentation

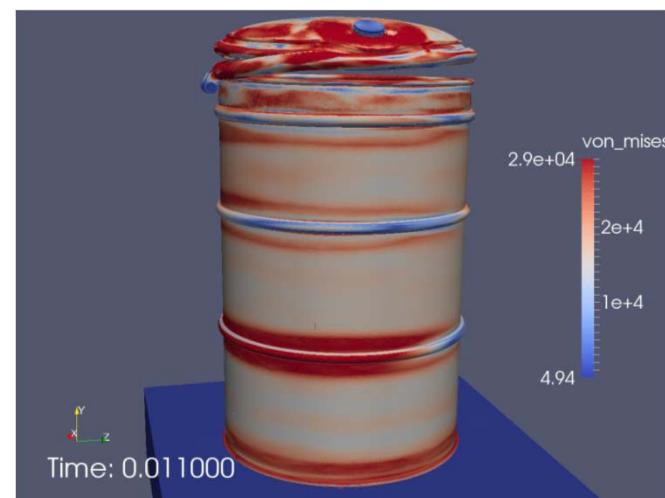
- Cohesive zone based fragmentation model to be implemented in an existing micromorphic simulation program.
- Output from the SIERRA SM (PRESTO) analyses will be used to define the boundary conditions for the micromorphic simulations.
- The particle size distribution from the macro-scale FEM will be adjusted based on the micro-fragmentation calculated by the micromorphic model simulations.



Micro-fragmentation will tend to increase the mass percentage of particles that fall below a given particle size (see arrows on plot).

Year 3 Proposed Research

- Based on the Year 1 and Year 2 research, we demonstrate the capabilities:
 - Substantiate data for liquid material (Chapter 3 of Handbook)
 - Substantiate data for solid and powder materials (Chapter 4 of Handbook).
- In Year 3, we also like to address topics in Chapter 5 and Chapter 6 of Handbook
 - As a part of continuation in Year 2, implementation of micromorphic material model into SIERRA SM (PRESTO)
 - Revise Chapter 6 (Inadvertent Nuclear Criticality)
 - Existing data is outdated, and many references used were no longer applicable, and some irrelevant data were used
 - The revision will include updating all information to latest information available, and revisit the liquid criticality release fraction, and will simulate using SIERRA codes
- Simulate a drum release during a fire to include in Chapter 5
 - Use existing 55-gal drum model from a WIPP drum release accident analysis*
 - Capitalize the on-going drum fire experiments at Sandia and recent data for fire condition to determine the opening size of the breached drum using SIERRA SM
 - Use solid combustion models from on-going DOE project to simulate the content burn in a breached drum



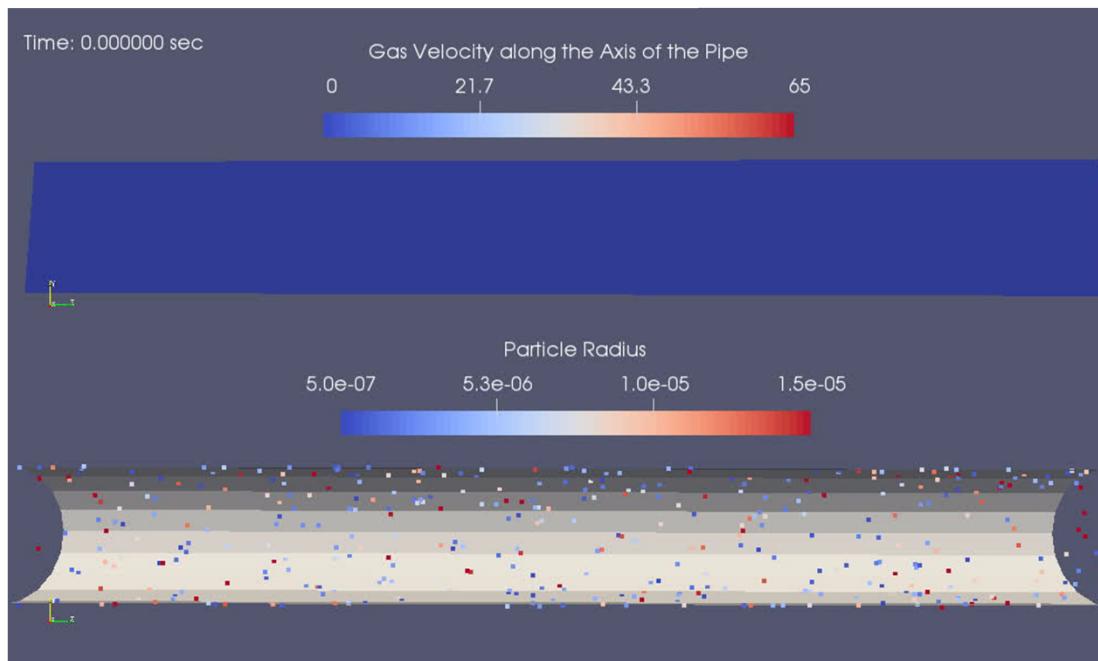
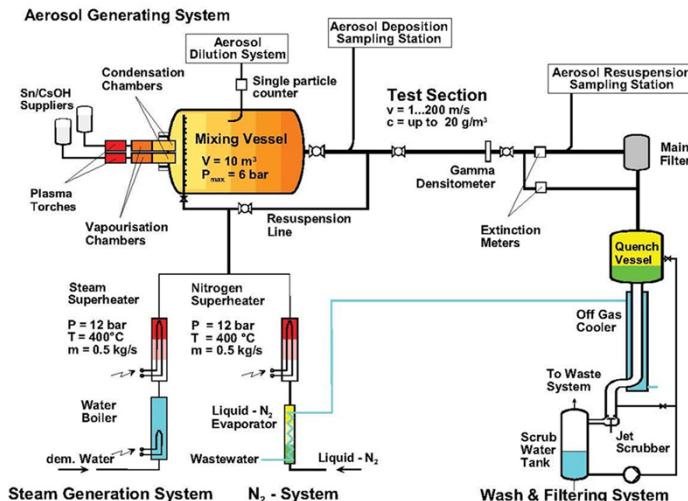
*Smith, J., Memorandum to Distribution: Mechanical Modeling of a WIPP Drum Under Pressure, Sandia National Laboratories, Albuquerque, NM, November 25, 2014

Backups

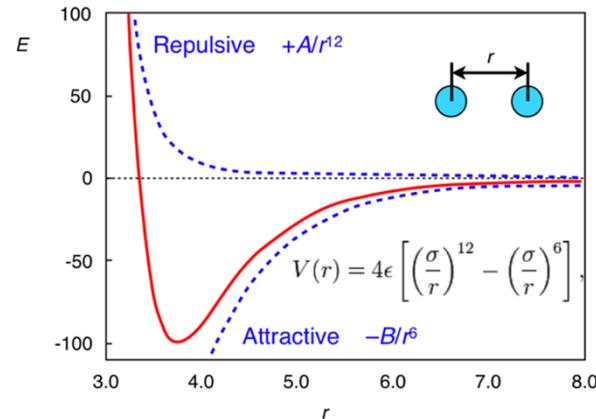


STORM SR-11 Resuspension Phase

Resuspension Model



Particle Interactions (not part of NSRD-11)



Simulation Example:

- 5 vertically suspended liquid droplets are released at start of simulation
- Lower droplet impacts rebounding surface at bottom of simulation domain
- Subsequently, other 4 droplets impact and coalesce with growing droplet
- Final agglomerate moves around on lower boundary due to velocity of immersing gas (fluid) phase
- Any number of scenarios is possible from droplet agglomeration to breakup to liquid flow

