

# Perrhenate Incorporation into Binary Mixed Sodalites: The Role of Anion Size and Implications for Technetium-99 Sequestration

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## Abstract

Perrhenate ( $\text{ReO}_4^-$ ), as a  $\text{TcO}_4^-$  analogue, was incorporated into mixed-anion sodalites from binary solutions containing  $\text{ReO}_4^-$  and a competing anion  $\text{X}^{n-}$  ( $\text{Cl}^-$ ,  $\text{CO}_3^{2-}$ ,  $\text{SO}_4^{2-}$ ,  $\text{MnO}_4^-$ , or  $\text{WO}_4^{2-}$ ). Our objective was to determine the extent of solid solution formation and the dependence of competing ion selectivity on ion size. Using equivalent aqueous concentrations of the anions ( $\text{ReO}_4^- / \text{X}^{n-}$  molar ratio = 1:1), we synthesized mixed-anion sodalites from zeolite and NaOH at 90°C for 96 h. The resulting solids were characterized by bulk chemical analysis, powder X-ray diffraction, scanning electron microscopy, and X-ray absorption near edge structure (XANES) spectroscopy to determine crystal structure, chemical composition, morphology, and rhenium (Re) oxidation state. Rhenium in the solid phase occurred predominately as  $\text{Re(VII)O}_4^-$  in the

sodalites, which have a primitive cubic pattern in the space group  $P\bar{4}3n$ . The refined unit-cell parameters of the mixed sodalites ranged from 8.88 to 9.15 Å and showed a linear dependence on the size and mole fraction of the incorporated anion(s). The  $\text{ReO}_4^-$  selectivity, represented by its distribution coefficient ( $K_d$ ), increased in the following order:  $\text{Cl}^- < \text{NO}_3^- < \text{MnO}_4^-$  and  $\text{CO}_3^{2-} < \text{SO}_4^{2-} < \text{WO}_4^{2-}$  for the monovalent and divalent anions, respectively. The relationship between the  $\text{ReO}_4^-$  distribution coefficient and competing anion size was nonlinear. When the difference in ionic radius (DIR) between  $\text{ReO}_4^-$  and  $X^{n-}$  ( $n = 1$  or  $2$ ) was greater than ~12%, then  $\text{ReO}_4^-$  incorporation into sodalite was insignificant. The results imply that anion size is the major factor that determines sodalite anion compositions. Given the similarity in chemical behavior or anion size when redox is not concerned  $\text{ReO}_4^-$  is likely to serve as a suitable analogue for  $\text{TcO}_4^-$  where Tc(VII) is the stable oxidation state.

## Highlights

- Mixed-anion sodalites were synthesized from zeolite and NaOH at 90°C
- Solid solution formation and ion selectivity were studied
- Solid phases were characterized by chemical analysis, XRD, SEM, and XANES
- Perrhenate selectivity for the mixed-anion sodalite cages increased in the following order:  $\text{Cl}^- < \text{NO}_3^- < \text{MnO}_4^-$  and  $\text{CO}_3^{2-} < \text{SO}_4^{2-} < \text{WO}_4^{2-}$
- The influence of anion size on mixed-anion sodalite compositions was documented

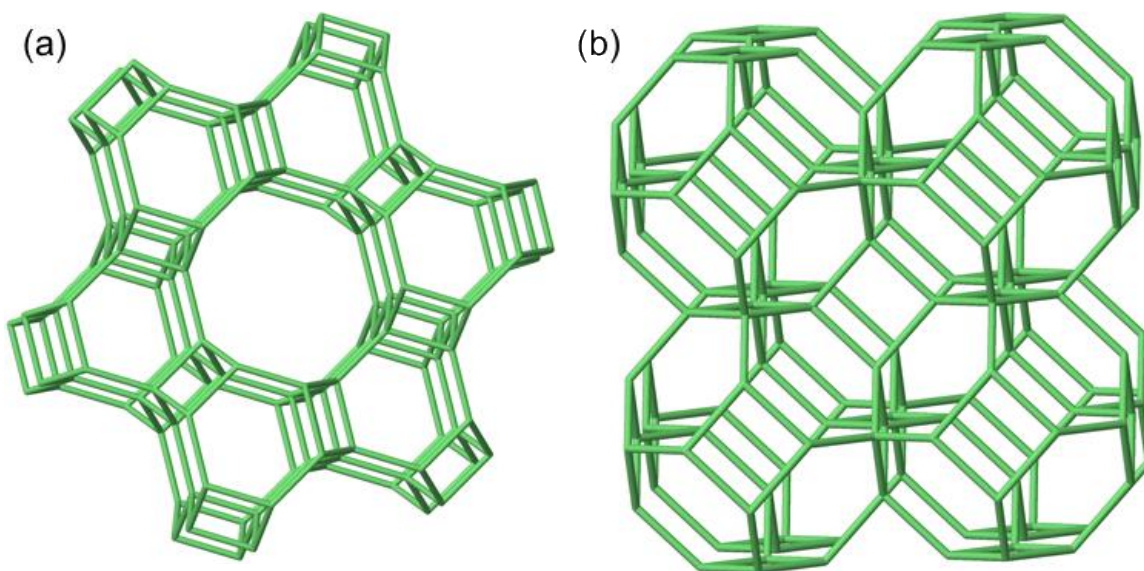
## Keywords

Mixed-anion sodalites; Anion selectivity; Distribution coefficient; Perrhenate; Pertechnetate, Technetium-99; Nuclear waste

## 1. Introduction

The safe disposal of nuclear waste generated by the nuclear fuel cycle remains one of the most challenging and potentially costly environmental endeavours facing the nuclear energy industry (Ewing, 2006). Additionally, disposal of reprocessed waste generated as a result of the Cold War legacy remains a challenge for numerous industrialized nations (Ewing, 1999). The application of versatile porous framework materials (feldspathoids) as a selective medium for sequestration of long-lived anionic radionuclides (e.g.,  $^{99}\text{TcO}_4^-$ ,  $^{129}\text{I}^-$ ,  $^{75}\text{SeO}_4^{2-}$ ) represents a key component of a closed nuclear fuel cycle. Furthermore, advanced knowledge of factors governing anion selectivity in feldspathoids is critical for their potential application in anion-sequestration processes (Custelcean and Moyer, 2007).

Feldspathoids such as cancrinite and sodalite (Fig. 1) have crystalline microporous framework structures. They can be represented by the general formula:  $\text{A}_8[\text{TO}_4]_6\text{X}_2$  where T is Al and/or Si, and A and X are monovalent or divalent cations and anions, respectively (Taylor and Henderson, 1978). Sodalite, a high-temperature, low pressure phase, consists of corner sharing  $\text{SiO}_4$  and  $\text{AlO}_4$  tetrahedra constructed into four and six-membered rings that form the cuboctahedral cages referred to as sodalite  $\beta$ -cages. The sodalite framework can be considered as a space-filling arrangement of the sodalite  $\beta$ -cages directly linked via the six-membered rings to form the semi-condensed sodalite structure. In the center of the cage is an anion that is tetrahedrally coordinated to four cations, forming  $\text{A}_4\text{X}$  clusters (Trill, 2002). Because anions are strongly trapped within the cages natural or synthetic sodalite phases constitute highly durable waste forms for immobilization of key anionic radionuclides (Maddrell et al., 2014).



**Fig. 1.** (a) Cancrinite structure (ABABAB.... stacking sequence). (b) Sodalite structure (ABCABC... stacking sequence of the six-rings)(Baerlocher and McCusker, 2014). For clarity cage oxygen, anions and cations were omitted.

Feldspathoids with guest ions in their structure have been widely studied (Johnson et al., 1999). Most studies have been devoted to mixed cation substitutions in sodalite frameworks (Brenchley and Weller, 1994; Stein et al., 1992) and to single anion sodalites (Weller and Wong, 1989; Weller et al., 1990), but the substitution of multiple guest anions in mixed sodalite phases is not well understood. Research into sodalite selectivity for anionic species of varying sizes is important for elucidating anion substitution into mixed sodalites with more complex structures, especially those sodalites containing key anionic radionuclides ( $^{99}\text{TcO}_4^-$ ,  $^{129}\text{I}^-$ ,  $^{75}\text{SeO}_4^{2-}$ ). Significant gaps exist in our current understanding of the role of sodalite selectivity as a driving force for controlling anion incorporation into the structure.

Previous work with  $\text{NO}_3/\text{ReO}_4$ -sodalites suggests that selectivity might be anion size-dependent (Dickson et al., 2014), but there is lack of experimental evidence

demonstrating the selectivity of different ions for incorporation into sodalites. Therefore, we investigated under oxidizing conditions the competitive incorporation of  $\text{ReO}_4^-$  into mixed anion-bearing sodalites in the presence of these competing anions ( $\text{X}^{n-}$ ) ranging in size and charge:  $\text{Cl}^-$ ,  $\text{CO}_3^{2-}$ ,  $\text{SO}_4^{2-}$ ,  $\text{MnO}_4^-$ , and  $\text{WO}_4^{2-}$ .

We used Re as a nonradioactive analogue for Tc because both elements occur primarily under oxidizing conditions as oxyanions ( $\text{ReO}_4^-$  and  $\text{TcO}_4^-$ ), which have similar metal oxygen bond lengths ( $\text{Tc-O} = 1.702 \text{ \AA}$ ;  $\text{Re-O} = 1.719 \text{ \AA}$ ) and ionic radii ( $\text{TcO}_4^- = 2.52 \text{ \AA}$ ;  $\text{ReO}_4^- = 2.60 \text{ \AA}$ ) (Icenhower et al., 2010; Marcus, 1991; Moyer and Bonnesen, 1979). However, in reducing environments, the redox chemistry of Re and Tc significantly differs due to the difference in standard electrode potentials ( $E_h$ ) of the two species ( $\text{ReO}_4^-/\text{ReO}_2 = 0.510 \text{ V}$  and  $\text{TcO}_4^-/\text{TcO}_2 = 0.738 \text{ V}$ ), and  $\text{ReO}_4^-$  being more difficult to reduce than  $\text{TcO}_4^-$  (Darab and Smith, 1996; Lukens et al., 2007; Wakoff and Nagy, 2004). For example, at pH 8, the  $E_h$  would have to drop below 0.25 V before  $\text{TcO}_2 \cdot 2\text{H}_2\text{O(s)}$  would form in the presence of  $10^{-8} \text{ M TcO}_4^-$  (Icenhower et al., 2010) but Re(VII) reduction would require a lower  $E_h$ . Thus, the use of Re as a Tc analogue is only applicable under aerobic conditions where both species are expected to remain as an oxyanion (+7 oxidation state).

This study highlights the dependence of selectivity on ion size and charge. Additionally, the variation of the sodalite structural parameter as a function of composition (anion mixing) will shed light on the extent of anion incorporation into mixed sodalites formed in environmentally relevant conditions such as subsurface and engineered wastes, vitrification products, and materials formed by chemical weathering.

## 2. Materials and Methods

### 2.1. Hydrothermal Mineral Synthesis

Mixed-anion sodalites with  $\text{ReO}_4^-$  and one other anion ( $\text{X}^{n-}$ ) were hydrothermally synthesized based on modification of a method previously described by Liu and Navrotsky (2007): sodium hydroxide (Alfa Aesar) was mixed with zeolite 4A ( $\text{Na}_{12}\text{Al}_{12}\text{Si}_{12}\text{O}_{48}\cdot x\text{H}_2\text{O}$ , W.R. Grace & Co.) and sodium salts of the appropriate anions. The zeolite supplied a 1:1 molar ratio of Si/Al. The mixed sodalites were synthesized in a 60-mL Teflon digestion bomb filled with 20 mL of deionized water, one gram of NaOH pellets (1.25 M NaOH) and 0.5 g of zeolite. To these basic solutions, 0.88 M of  $\text{NaReO}_4$  was added and 0.88 M of  $\text{Cl}^-$ ,  $\text{CO}_3^{2-}$ ,  $\text{SO}_4^{2-}$ ,  $\text{MnO}_4^-$ , or  $\text{WO}_4^{2-}$  was added as the competing anion. The rationale for the concentrations used in this experiment was that we wanted to produce pure sodalite phases to determine anion selectivity in a mixed system. All chemical reagents were used as received.

To perform hydrothermal syntheses, the bombs were capped, and reagents were aged for 96 h in a 90 °C oven. After decanting the basic supernatant solutions, the solid precipitates were washed three times with deionized water ( $0.054 \times 10^{-3} \text{ dSm}^{-1}$ ) by centrifugation. The solids were dialyzed in deionized water until the electrolytic conductivity was  $\leq 0.01 \text{ dSm}^{-1}$ , dried for 24 h, and weighed. Solid yield after dialysis ranged from 0.5 to 0.6 g.

### 2.2. Powder X-ray Diffraction

X-ray diffraction data were obtained with a Panalytical Xpert Pro diffractometer (XRD) scanning at 1.5 °/min over 5 – 90° 2 $\theta$ . We used  $\text{CoK}_\alpha$  radiation ( $\lambda = 1.789010 \text{ \AA}$ ) and an X'Celerator silicon strip detector equipped with an Fe filter. Scans used ¼° fixed

divergence slits and  $\frac{1}{2}^\circ$  anti-scatter slits. Jade and/or High Score Plus software, and the ICDD database were used for mineral identification (Kabekkodu, 2012). Rietveld refinements of the XRD data were performed in High Score Plus and/or GSAS with EXPGUI interface (Toby, 2001) using the reported structures of the following phases:  $\text{Na}_8(\text{AlSiO}_4)_6(\text{NO}_2)_2$ ,  $\text{Na}_8(\text{AlSiO}_4)_6(\text{ReO}_4)_2$ , and  $\text{Na}_6\text{Ca}_{1.5}(\text{AlSiO}_4)_6(\text{CO}_3)_{1.5}(\text{H}_2\text{O})_{1.75}$  (Buhl et al., 1996; Hackbarth et al., 1999; Mattigod et al., 2006). The following parameters were allowed to vary: the background (8 parameters), unit cell, Na position, peak shape (5 parameters: U, V, W, and two peak shape parameters), overall thermal parameter (B), and preferred orientation.

### 2.3. X-ray Absorption Near Edge Structure (XANES) Spectroscopy

Powdered sodalite samples were mixed with boron nitride and mounted on an aluminum holder with Kapton windows. The XANES spectra were obtained at the Stanford Synchrotron Radiation Lightsource (SSRL) using the 11-2 beamline equipped with a Si (220) double crystal monochromator ( $\Phi = 90^\circ$  crystals) detuned 50% to reduce the harmonic content of the beam. The spectra from 0.2 keV below to 10 keV above the Re  $L_2$ -edge (11.959 keV) were collected either in transmission mode using nitrogen-filled ion chambers or fluorescence mode using a 100-element Ge detector and corrected for detector dead time. We converted raw data to spectra and normalized with SixPack and Artemis (Ravel and Newville, 2005). Normalized XANES spectra were fit using standard spectra in the locally written program 'fites', which utilizes a non-linear least squares approach to fitting data (Li et al., 1995). Two reference spectra,  $\text{ReO}_2(\text{s})$ , and pure  $\text{ReO}_4$ -sodalite, were used for data fitting. The XANES spectra of the samples were allowed to vary in energy during fitting, and the spectral resolution is 7 eV based

on the width of the white line at the Re L<sub>2</sub>-edge. Henceforth, we will refer to “ReO<sub>4</sub><sup>−</sup>” in the mixed sodalites as “Re” because no other “Re” species are significant in this study.

## 2.4. Electron Microscopy

Scanning electron micrographs (SEM) were obtained with platinum-palladium sputter-coated powder sodalite samples. The coated samples were examined using a field emission scanning electron microscope (FESEM) with an accelerating voltage of 30 keV, and a resolution of 1 nm. The FESEM was equipped with a field emission gun (FEI Quanta 200F, FEI Co., Hillsboro, OR) and Everhart-Thornley detector.

## 2.5. Chemical Analysis

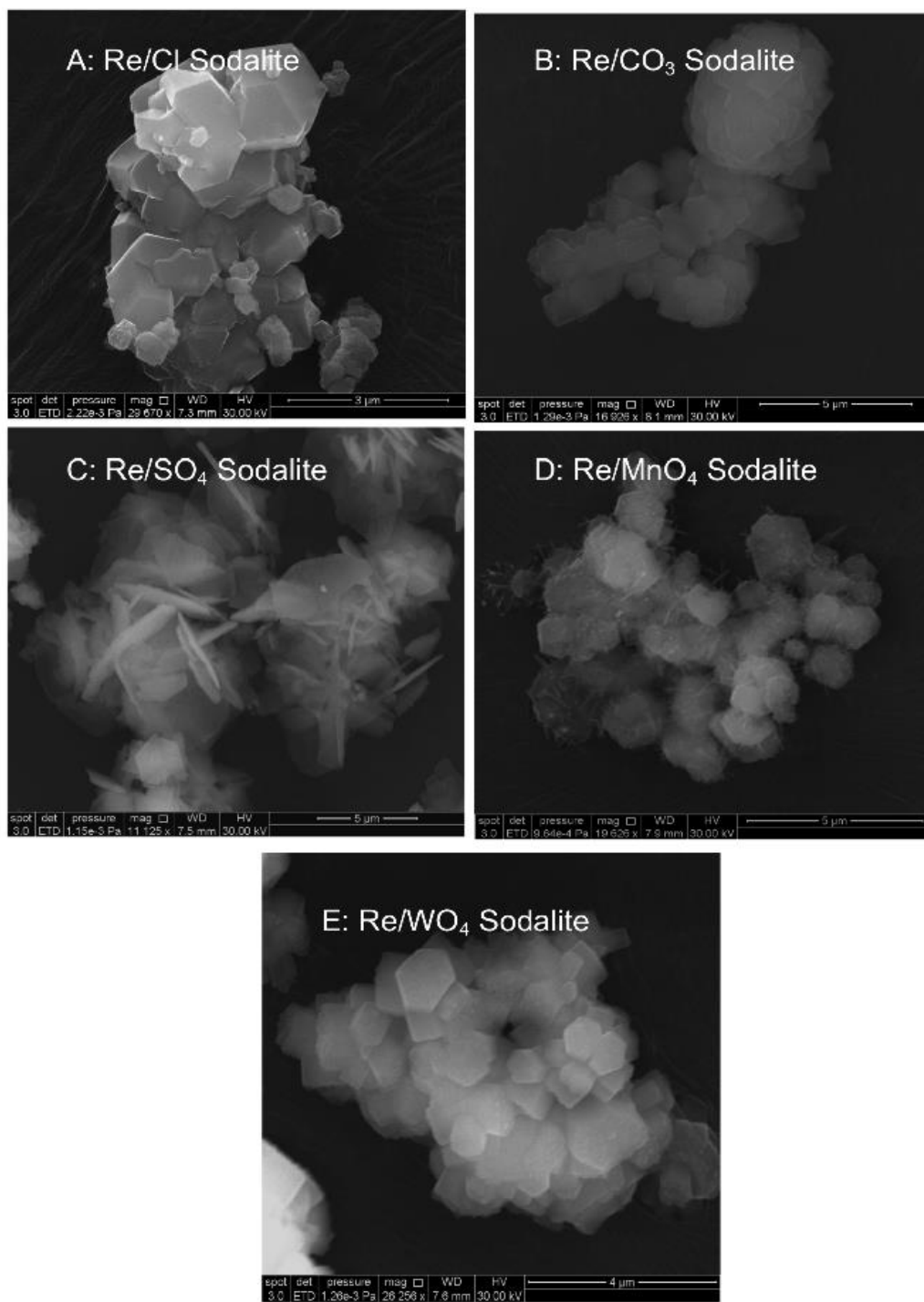
The powder sodalite samples digested in 3% nitric acid were analyzed for Na concentrations by atomic emission and absorption spectrophotometry (Varian 220 Flame Atomic Absorption Spectrometer, Varian Ltd., Mulgrave, Australia). The Si, Al, Mn, W, and Re concentrations in the solids were determined by inductively coupled plasma-mass spectrometry (Agilent 7700 ICP-MS, Santa Clara, CA), and concentrations of Cl<sup>−</sup> and, SO<sub>4</sub><sup>2−</sup> by ion chromatography (HPLC-10Ai, Shimadzu Inc., Canby, OR). Total carbon concentration was determined by dry combustion from TruSpec C/N analyzer (Leco Corporation, St. Joseph, MI) equipped with a high temperature combustion method and infrared detection technique.

## 3. Results

### 3.1. Synthesis Product Morphology

The SEM images of the mixed-anion sodalites are shown in Fig. 2. The mixed-anion sodalites formed in the presence of Cl<sup>−</sup>, CO<sub>3</sub><sup>2−</sup>, MnO<sub>4</sub><sup>−</sup> and WO<sub>4</sub><sup>2−</sup> were hexagonal crystallites (Fig. 2A-B, D-E). The observed morphology differs from the lepispheric

morphology (i.e., thin disks or blades) reported by Deng et al. (2006) for precipitates formed from simultaneous additions of two or more anions ( $\text{Cl}^-$ ,  $\text{NO}_2^-$ ,  $\text{NO}_3^-$ ,  $\text{CO}_3^{2-}$ ,  $\text{SO}_4^{2-}$ ,  $\text{PO}_4^{3-}$ ) to starting solutions of Na hydroxide, aluminate, and silicate. In contrast, our experiments used zeolite as the source for Al and Si. The crystalline solids formed in the presence of  $\text{SO}_4^{2-}$  anions were dominated by lepispheric and/or lenticular-shaped crystal structures (Fig. 2C). The observed Re/ $\text{SO}_4$ -sodalite morphology was similar to those reported by Deng et al, (2006) for precipitates formed in binary or multi-anion solutions.



**Fig. 2.** SEM images of mixed-anion sodalite formed in an equimolar  $\text{ReO}_4^-/\text{X}^{n-}$  solution. Images scale bars are between 3 – 5 μm

### 3.2. Composition Analysis

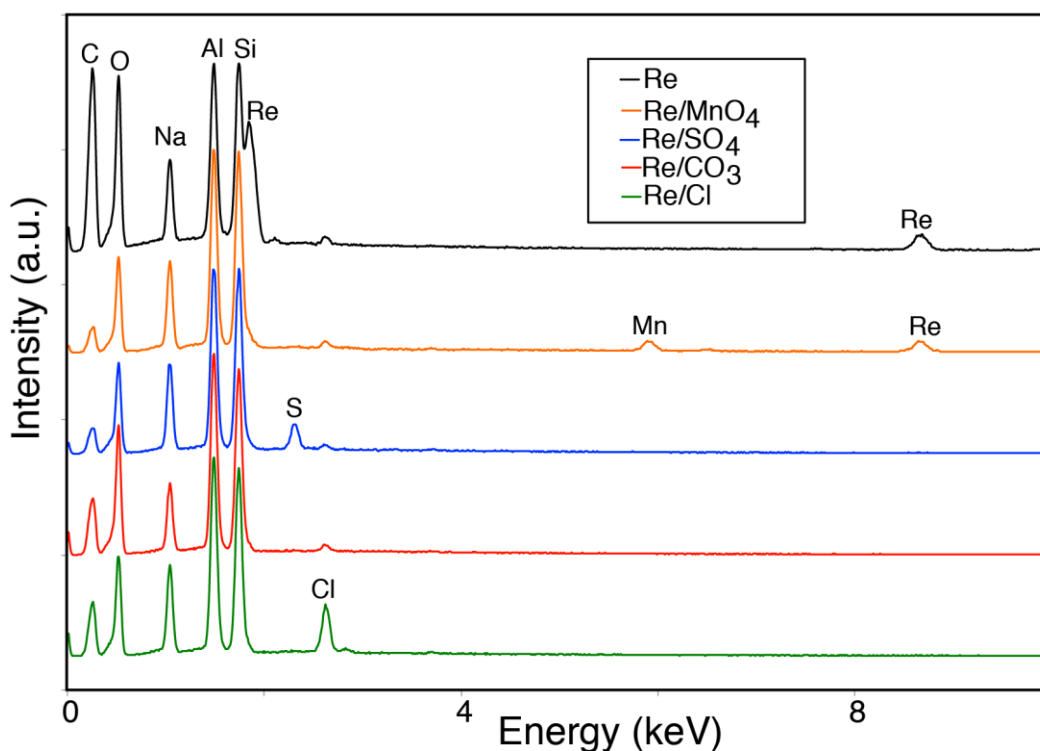
The chemical composition of the synthesized products is shown in Table 1. The mixed-anion sodalites contained from 0.02 – 1.90 moles of  $\text{ReO}_4^-$  and 0.04 – 2.10 moles of  $\text{X}^{n-}$  per formula unit. The sodalites, synthesized in the presence of  $\text{ReO}_4^-$  and  $\text{Cl}^-$ ,  $\text{CO}_3^{2-}$ , or  $\text{SO}_4^{2-}$  incorporated negligible amounts of  $\text{ReO}_4^-$ . In contrast, the sodalite cages exhibited strong preference for  $\text{ReO}_4^-$  over  $\text{WO}_4^{2-}$  with ~95%  $\text{ReO}_4^-$  occupancy of available sites. Further evidence of  $\text{ReO}_4^-$  incorporation into sodalite is shown in the energy-dispersive X-ray spectroscopy (EDS) patterns (Fig. 3). Perrhenate was best incorporated into the  $\text{Re/MnO}_4^-$  and  $\text{Re/WO}_4^-$  sodalites whereas insignificant incorporation occurred for the  $\text{Re/Cl}^-$ ,  $\text{Re/SO}_4^-$  and  $\text{Re/CO}_3^-$  sodalites.

**Table 1.**

Chemical composition data for mixed-anion sodalites (mol/formula unit).

Structural Formula	Na	Al	Si	Re/X	$\text{ReO}_4$	$\text{X}^*$
$\text{Na}_8[\text{Al}_6\text{Si}_6\text{O}_{24}](\text{Cl}_{(2.1)}\text{ReO}_{4(0.003)})$	$7.96 \pm 0.16$	$6.00 \pm 0.05$	$6.06$ $\pm 0.11$	0.00	0.003 $\pm 0.001$	2.14 $\pm 0.07$
$\text{Na}_8[\text{Al}_6\text{Si}_6\text{O}_{24}](\text{CO}_{3(1.0)}\text{ReO}_{4(0.02)})$	$8.00 \pm 0.30$	$6.01 \pm 0.11$	$6.00$ $\pm 0.10$	0.02	0.021 $\pm 0.005$	1.01 $\pm 0.10$
$\text{Na}_{7.6}[\text{Al}_6\text{Si}_6\text{O}_{24}](\text{SO}_{4(0.96)}\text{ReO}_{4(0.08)})$	$7.61 \pm 0.07$	$6.02 \pm 0.07$	$6.08$ $\pm 0.07$	0.08	0.080 $\pm 0.002$	0.958 $\pm 0.12$
$\text{Na}_8[\text{Al}_6\text{Si}_{5.9}\text{O}_{24}](\text{MnO}_{4(1.1)}\text{ReO}_{4(0.97)})$	$8.09 \pm 0.17$	$6.09 \pm 0.05$	$5.92$ $\pm 0.02$	0.89	0.965 $\pm 0.015$	1.09 $\pm 0.03$
$\text{Na}_{7.9}[\text{Al}_6\text{Si}_6\text{O}_{24}](\text{WO}_{4(0.05)}\text{ReO}_{4(1.9)})$	$7.94 \pm 0.10$	$6.02 \pm 0.08$	$6.00$ $\pm 0.17$	39.7	1.904 $\pm 0.03$	0.048 $\pm 0.004$

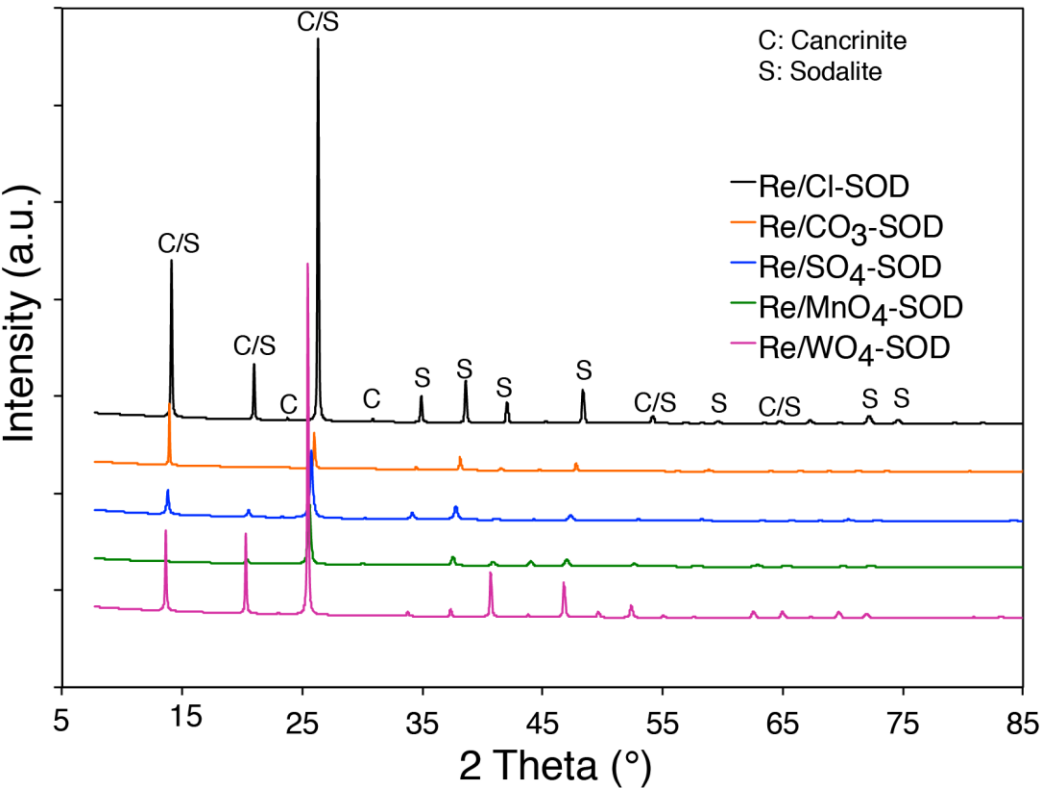
\*X: Anions ( $\text{Cl}^-$ ,  $\text{CO}_3^{2-}$ ,  $\text{SO}_4^{2-}$ ,  $\text{MnO}_4^-$ ,  $\text{WO}_4^{2-}$ ).



**Fig. 3.** EDS spectra of select mixed-anion sodalites. The Re/WO<sub>4</sub> spectrum is not shown. The additional Cl<sup>-</sup> peaks in some of the samples are from the epoxy matrix used in thin section preparation.

### 3.3. Mineral Structure

The calculated XRD patterns obtained from the Rietveld refinements of the mixed-anion sodalites are displayed in Fig. 4. The refined lattice parameter ( $a$ ) and index of agreement ( $\chi^2$ ) for the mixed-anion sodalites are shown in Table 2. The lower the  $\chi^2$  term the better the fit. The space group  $P\bar{4}3n$  was adopted for the mixed-anion sodalites with ( $a$ ) ranging from 8.8885(2) to 9.1527(1) Å. The Rietveld refinements indicate that minor amounts of cancrinite (<2 wt%) were formed along with the dominant sodalite phase(s).



**Fig. 4.** Refined (calculated) powder X-ray spectra for mixed-anion sodalites.

**Table 2.**

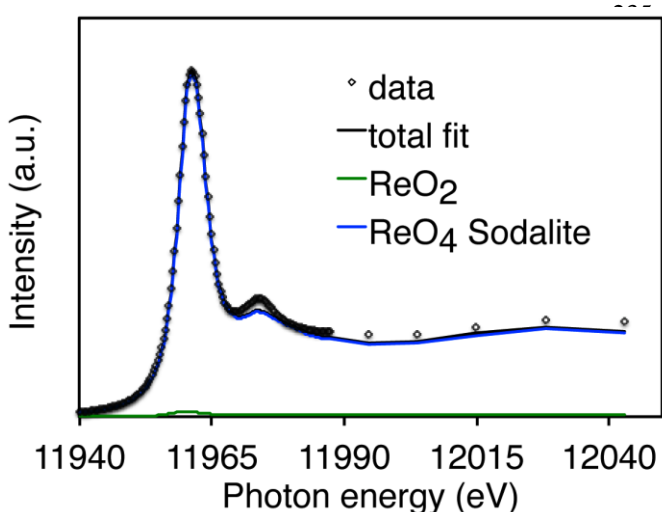
Refined powder X-ray data for mixed-anion sodalite.

Sample Type	Structural Formula	$a$ (Å)	esd	$\chi^2$
Re/Cl-SOD	$\text{Na}_8[\text{Al}_6\text{Si}_6\text{O}_{24}](\text{Cl}_{(2.1)}\text{ReO}_{4(0.003)})$	8.8885	$\pm 0.0002$	2.76
Re/CO <sub>3</sub> -SOD	$\text{Na}_8[\text{Al}_6\text{Si}_6\text{O}_{24}](\text{CO}_{3(1.0)}\text{ReO}_{4(0.02)})$	8.9691	$\pm 0.0002$	8.07
Re/SO <sub>4</sub> -SOD	$\text{Na}_{7.6}[\text{Al}_6\text{Si}_6\text{O}_{24}](\text{SO}_{4(0.96)}\text{ReO}_{4(0.08)})$	9.0785	$\pm 0.0004$	3.60
Re/MnO <sub>4</sub> -SOD	$\text{Na}_8[\text{Al}_6\text{Si}_{5.9}\text{O}_{24}](\text{MnO}_{4(1.1)}\text{ReO}_{4(0.97)})$	9.1258	$\pm 0.0005$	1.32
Re/WO <sub>4</sub> -SOD	$\text{Na}_{7.9}[\text{Al}_6\text{Si}_6\text{O}_{24}](\text{WO}_{4(0.05)}\text{ReO}_{4(1.9)})$	9.1527	$\pm 0.0002$	6.05

$a$  – unit cell parameter, esd – estimated standard deviation, and  $\chi^2$  – index of agreement.

### 3.4. Rhenium Oxidation State

The spectra fitting were performed as described by Lukens et al. (2005). The Re  $L_2$ -edge XANES data were fitted using only the spectra of  $\text{ReO}_2(\text{s})$  and  $\text{ReO}_4$ -sodalite (Pierce et al., 2014, submitted). The spectrum of  $\text{Re/MnO}_4$ -sodalite is presented in Fig. 5. In the mixed-anion sodalites, the spectrum of  $\text{ReO}_4$ -sodalite contributes significantly ( $\geq 92\%$ ) to the fit and only in the presence of  $\text{Cl}^-$  does the spectrum of  $\text{ReO}_2(\text{s})$  contribute significantly to greater than  $2\sigma$  of the fit (Table 3). Thus, the  $\text{ReO}_4^-$  species is considered the dominant rhenium species in these solid phases.



**Fig. 5.** Rhenium  $L_2$ -XANES spectral data for  $\text{Re/MnO}_4$ -sodalite; data are represented by dots, and the fit is shown by the black line. Results indicate that the  $\text{Re(VII)}$  oxidation state dominates.

**Table 3.**

Rhenium L<sub>2</sub>-edge XANES spectral fitting results for mixed-anion sodalites.

Sample	ReO <sub>2</sub> ‡	<i>p</i> <sup>*</sup>	ReO <sub>4</sub> <sup>-</sup> -sodalite‡	<i>p</i> <sup>*</sup>
Re/Cl-SOD	0.18(6) <sup>†</sup>	0.017	0.82(5)	<0.001
Re/CO <sub>3</sub> -SOD	0.08(5)	0.168	0.92(4)	<0.001
Re/SO <sub>4</sub> -SOD	0.03(5)	0.545	0.97(4)	<0.001
Re/MnO <sub>4</sub> -SOD	0.02(6)	0.828	0.98(5)	<0.001
Re/WO <sub>4</sub> -SOD	0.00(2)	1.000	1.00(1)	<0.001

‡The fractional contributions of each oxidation state to the XANES spectral.

<sup>†</sup>The number in parentheses is the standard deviation in the same decimal place as the digit preceding it.

\**p* is the usual *p*-value, which is the likelihood that the improvement to the fit due to inclusion of this component is due to random error (noise) in the data. If *p* < 0.05, then the data supports the hypothesis that a given component is present (improvement is > 2σ of the fit).

## 4. Discussion

### 4.1. Incorporation of ReO<sub>4</sub><sup>-</sup> in the Presence of Competing Anion (X<sup>n-</sup>)

Using an equimolar concentration of ReO<sub>4</sub><sup>-</sup> and X<sup>n-</sup> in the starting solutions, we synthesized five mixed-anion sodalites and tested the hypothesis that ion size and charge drive the selectivity for a given anion.

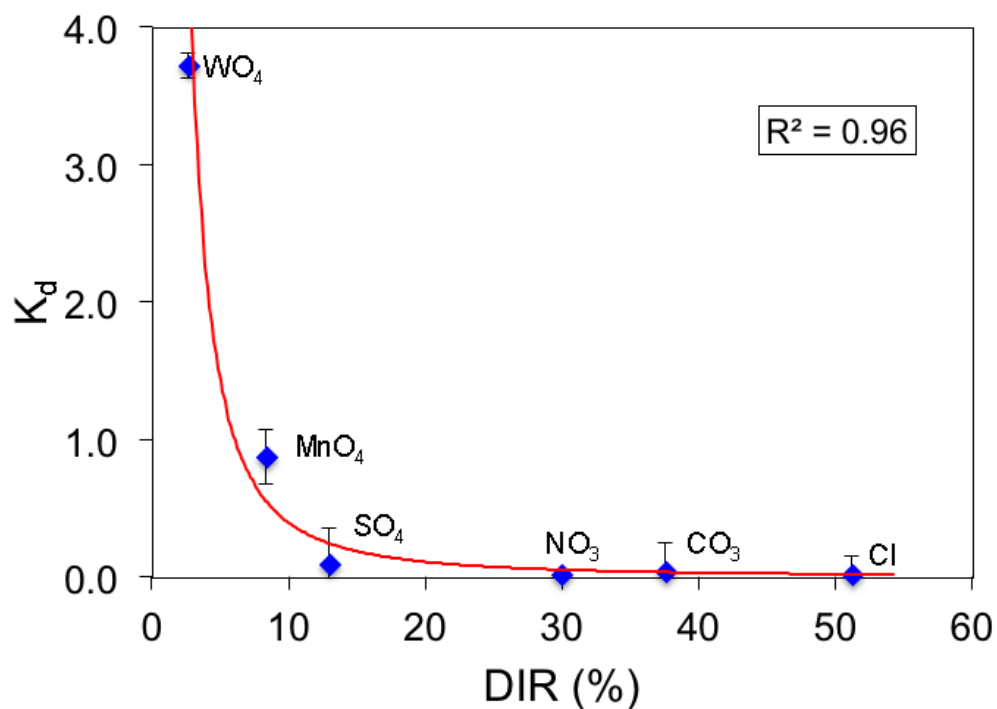
As the ionic radius increases in the following series: Cl<sup>-</sup> < CO<sub>3</sub><sup>2-</sup> < SO<sub>4</sub><sup>2-</sup> < MnO<sub>4</sub><sup>-</sup> < WO<sub>4</sub><sup>2-</sup>, the selectivity of ReO<sub>4</sub><sup>-</sup> for the mixed sodalite linearly increased, consistent with the linear expansion of the cages from the Re/Cl-sodalite to the Re/WO<sub>4</sub>-sodalite.

The inability to form mixed sodalites containing significant amounts of  $\text{ReO}_4^-$  in the presence of  $\text{Cl}^-$ ,  $\text{CO}_3^{2-}$ , and  $\text{SO}_4^{2-}$  is due the large size difference between  $\text{ReO}_4^-$  and the competing anions, and the nature of the anions. According to Hume-Rothery Rules, the following conditions favor the formation of solid solutions (e.g., metal alloys, crystallized salts): similarity in ion crystal structures, valency, electronegativity and size (Mizutani, 2010). Sodalite cages can host anions of varying size due to cooperative tilting and deformation of the frameworks up to a point. Trill et al. (2003) state that the difference in anion size may not exceed 15%, because of excessive strain imposed on the sodalite framework when anions of different size are accommodated. This behavior is confirmed in our system as shown in Fig. 6, where anion selectivity is plotted against the difference in ionic radii (DIR) of solvent A ( $r_A$ ) and solute B ( $r_B$ ) where:

$$\text{DIR (\%)} = \left( \frac{r_A - r_B}{r_B} \right) \times 100$$

As the DIR increases from 2.7% in the  $\text{Re}/\text{WO}_4$ -sodalite to 51.2% in the  $\text{Re}/\text{Cl}$ -sodalite, the  $\text{ReO}_4^-$  distribution coefficient exponentially declines from 3.73 to 0.02. When the DIR between  $\text{ReO}_4^-$  and the competing anion exceeds 15%, the concomitant inclusion of both anions would sufficiently distort the mixed-anion sodalite cages, resulting in the exclusion of the larger anion from the cages. This trend is manifested in the preferential formation of mostly  $\text{Cl}^-$ ,  $\text{CO}_3^-$  and  $\text{SO}_4$ -sodalites containing minor amounts of enclathrated  $\text{ReO}_4^-$ . Although the DIR for  $\text{Re}/\text{SO}_4$  (13%) and  $\text{Re}/\text{WO}_4$ -sodalites (2.7%) should favor the formation of mixed sodalite solid solutions, the distribution coefficient shows a clear preference for  $\text{SO}_4^{2-}$  and  $\text{ReO}_4^-$  respectively. In the case of  $\text{SO}_4^{2-}$ , the DIR is close to 15%, indicating that this difference is still large

enough to strongly favor the smaller anion. For  $\text{WO}_4^{2-}$ , the difference in charge and inability to fill all cages with either  $\text{ReO}_4^-$  or  $\text{WO}_4^{2-}$  may explain the preference for  $\text{ReO}_4^-$ .



**Fig. 6.** The distribution coefficient ( $K_d$ ) graph for  $\text{ReO}_4^-$  sequestered in mixed-anion sodalites as a function of the DIR. Generally, more than 90% of sodalite cages are filled with anions. \* $\text{NO}_3$  data point is from Dickson et al. (2014)

**Table 4.**

Ionic radii, hydration energy and ionic potential data for studied anions with respect to  $\text{ReO}_4^-$ .

Anions (X)	r (nm)	DIR (%)	Ionic Potential (Z/r)	Hydration Energies (kJmol <sup>-1</sup> )
$\text{Cl}^-$	0.172 <sup>d</sup>	51.2	0.58	-340 <sup>a</sup>
$\text{CO}_3^{2-}$	0.189 <sup>c</sup>	37.6	1.06	-1315 <sup>a</sup>
$\text{SO}_4^{2-}$	0.230 <sup>a</sup>	13.0	0.87	-1080 <sup>a</sup>
$\text{NO}_3^-$	0.200 <sup>a</sup>	30.0	0.50	-300 <sup>a</sup>
$\text{MnO}_4^-$	0.240 <sup>a</sup>	8.3	0.42	-235 <sup>a</sup>
$\text{WO}_4^{2-}$	0.267 <sup>b</sup>	2.7	0.75	-702 <sup>e</sup>
$\text{ReO}_4^-$	0.260 <sup>a</sup>	0.0	0.39	-330 <sup>a</sup>
$\text{TcO}_4^-$	0.252 <sup>d</sup>	3.2	0.40	-251 <sup>d</sup>

r represents the ionic radii of anions

<sup>a</sup> Thermodynamics of solvation of ions; Marcus et al. (1991)

<sup>b</sup> Ionic radius in aqueous solution; Marcus et al. (1988)

<sup>c</sup> Handbook of chemistry and physics; David et al. (2003)

<sup>d</sup> Physical factors in anion separation; Moyer et al. (1979)

<sup>e</sup> Hydration and extraction of oxyanion; Abramov et al. (2001)

DIR: Difference in ionic radii.

## 5. Conclusions and Implications for <sup>99</sup>Tc Immobilization

In this study, five mixed-anion sodalites containing extra-framework species were synthesized and characterized. The selectivity for intra-lattice anions of the products was highly dependent on the size and, to a lesser extent, the charge of the competing anion. The results of our study suggest that similarity in ionic radius (DIR of ≤15%) and charge (ionic potential) promote the competitive incorporation of  $\text{ReO}_4^-$  into the mixed-

anion sodalites (Fig. 6 and Table 4). Selectivity of  $\text{ReO}_4^-$  for the mixed-anion sodalites was found to increase in the series as follows:  $\text{Cl}^- < \text{CO}_3^{2-} < \text{NO}_3^- < \text{SO}_4^{2-} < \text{MnO}_4^- < \text{WO}_4^{2-}$ .

The findings in this study have implications for the fate and transport of  $^{99}\text{TcO}_4^-$  in subsurface sediments, assuming that its chemical behavior can be well approximated by  $\text{ReO}_4^-$ . Firstly, the formation of a  $\text{Re}/\text{MnO}_4$ -sodalite solid solution implies that  $\text{ReO}_4^-$  is a suitable analogue for  $\text{TcO}_4^-$ . Like  $\text{TcO}_4^-$ ,  $\text{MnO}_4^-$  shares a similar size, and ionic potential with  $\text{ReO}_4^-$  (Table 4). The distribution coefficient for  $\text{ReO}_4^-$  was unity, implying nearly equal selectivity for  $\text{MnO}_4^-$  and  $\text{ReO}_4^-$  during the formation of sodalite. The same is likely true for  $\text{TcO}_4$ -sodalite.

Secondly, our results also suggest that while neoformed feldspathoid minerals, such as sodalite, can incorporate  $^{99}\text{Tc}$  as  $\text{TcO}_4^-$ , but smaller competing anions with DIR >12% will be preferred. Unfortunately, in many instances where environmental conditions are conducive for feldspathoid formation, the waste solutions may also contain high concentrations of such competing anions.

One limitation of our results is that sodalite synthesis occurred in a closed system. In open, free-flowing systems, the smaller anions may become depleted leaving  $\text{TcO}_4^-$  to be incorporated later in the reaction sequence. Additionally, our experiments were designed specifically to form only sodalite phases because of the ability of its cages to sequester large ions such as  $\text{TcO}_4^-$ . In other systems, neoformed mineral phases could include cancrinite, zeolite, nosean, and nepheline. It has been reported that  $\text{NO}_3^-$  is sequestered by cancrinite and  $\text{SO}_4^{2-}$  by nosean, whereas  $\text{Cl}^-$  and  $\text{ReO}_4^-$  are incorporated into mixed-anion sodalites (Pierce et al., 2014). Thus, at the comparatively low concentrations of  $\text{TcO}_4^-$  ( $10^{-6}$  to  $10^{-4}$  M) expected in most nuclear waste streams,

TcO<sub>4</sub><sup>-</sup> could intercalate into the mixed-anion sodalite phases after other competing anions have been selectively sequestered into their respective neoformed mineral phases.

Additionally, to enhance ReO<sub>4</sub><sup>-</sup> (and ultimately TcO<sub>4</sub><sup>-</sup>) sequestration into mixed sodalites pre-treatment of the waste streams has been suggested to remove NO<sub>3</sub><sup>-</sup> and NO<sub>2</sub><sup>-</sup> from the wastes prior to formation of sequestering aluminosilicate phases (Pierce et al., 2014). Although mixed-anion sodalites are somewhat less durable compared to their pure phase analogues (Pierce et al., 2014), they remain an excellent waste form for the long-term disposal of key anion radionuclides in an environment where they are stable—e.g., under the alkaline conditions expected for vitrified waste disposal. For example, Pierce et al. (2014) estimated the leach rate of ReO<sub>4</sub><sup>-</sup> from Re-sodalite to be 0.0006 g m<sup>-2</sup>d<sup>-1</sup>.

Further work is needed in open systems, with a greater range of hydrothermal conditions (high temperature and dynamic flow synthesis of an array of aluminosilicate mineral phases), and at realistic <sup>99</sup>Tc concentrations, to mimic waste-impacted subsurface sediments and managed waste streams to determine if mixed-anion sodalites may be relevant sequestering phase(s).

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