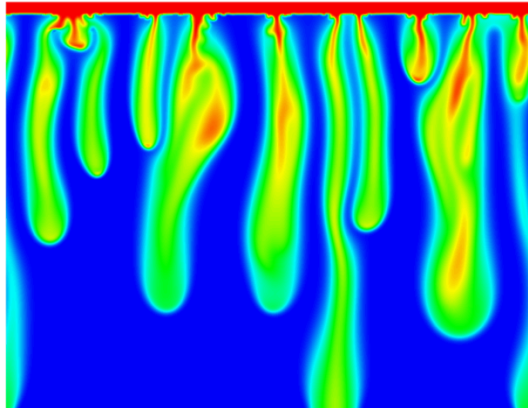


Role of the Capillary Transition Zone on the Dissolution of CO₂ into Brine in Saline Reservoirs



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Motivation:

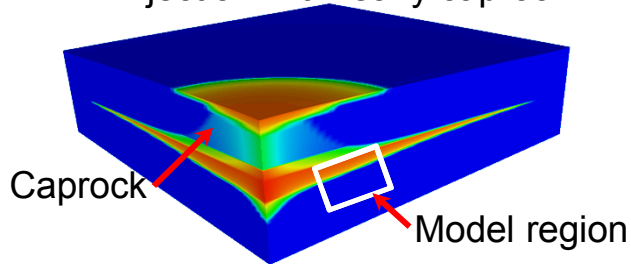
- Geologic carbon storage is a technically viable technology to reduce the impact of anthropogenic CO₂ emissions
- Solubility trapping is thought to be a critical step in geologic carbon storage
- Buoyantly driven convective dissolution can substantially enhance the rate of dissolution, but is difficult to quantify in the field
- Theory and computational models have been applied but few have included the two-phase region above the gas-water contact where dissolution actually takes place

Objectives of this research:

- We use a numerical model which includes the two-phase region to determine:
 - Impact of capillary transition zone on long-term dissolution rate
 - Role of strength of capillary forces (with entry pressure as surrogate)
 - limiting behavior

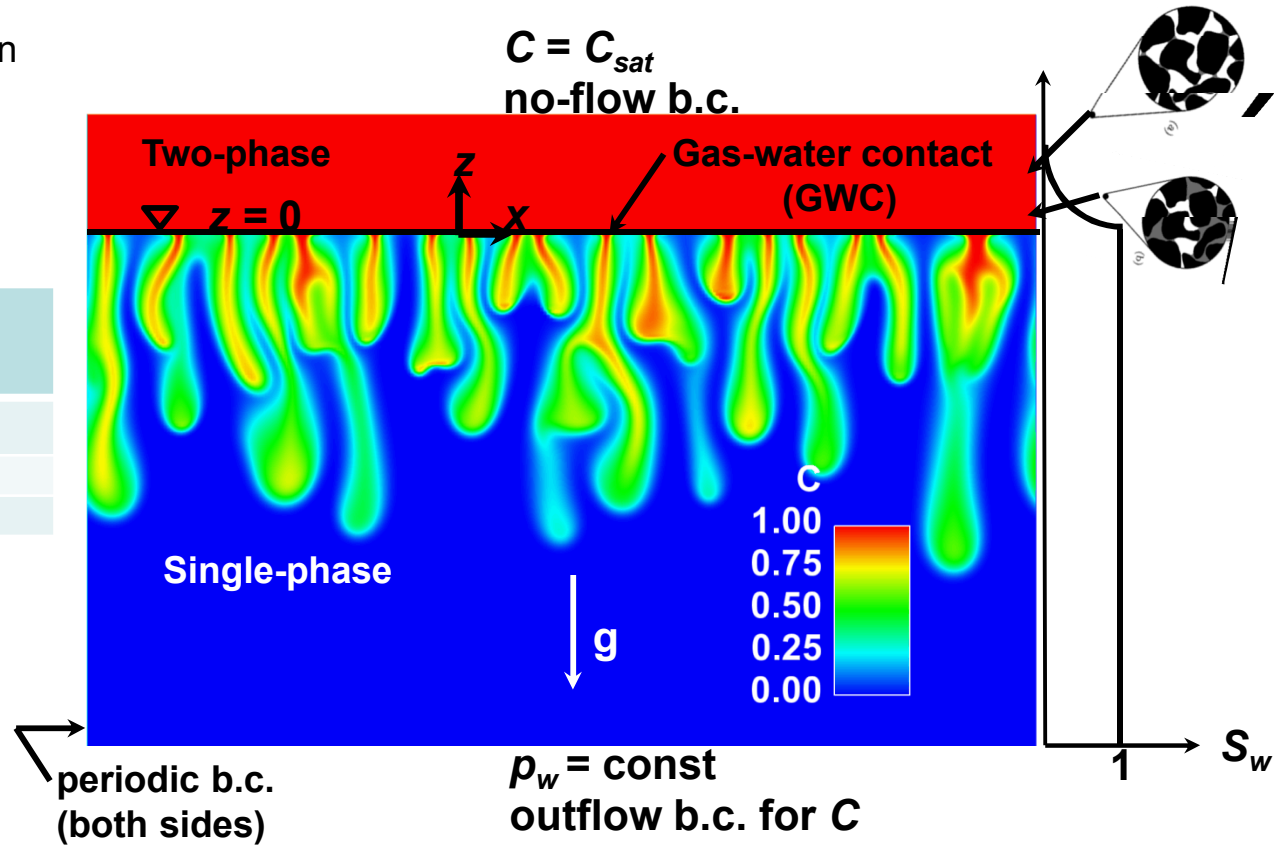
Model Problem

Injection with leaky caprock



Two reservoirs are modeled

Property	Sleipner Utsira	Bravo Dome
porosity	0.37	0.15
perm. (mD)	2000	50



- Two-phase flow :

- Brine:
$$\frac{\partial(\rho_w \phi (1 - S_n))}{\partial t} = \nabla \cdot \left(\rho_w \frac{k_{rw}}{\mu_w} \mathbf{k} \cdot (\nabla p_w - \rho_w \mathbf{g}) \right) + Q_w$$

- CO₂:
$$\frac{\partial(\rho_n \phi S_n)}{\partial t} = \nabla \cdot \left(\rho_n \frac{k_{rn}}{\mu_n} \mathbf{k} \cdot (\nabla p_w + \nabla p_c - \rho_n \mathbf{g}) \right) + Q_n$$

- Balance of dissolved CO₂:

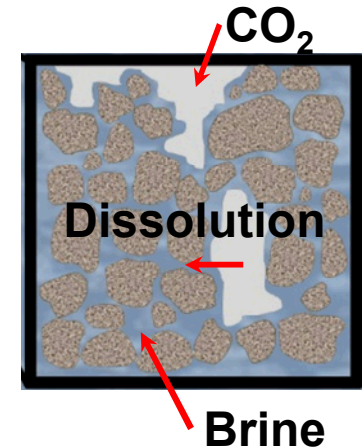
$$\frac{\partial}{\partial t} \phi (S_w C) + \nabla \cdot (\mathbf{v}_w C - \phi S_w \tau D_w^{CO_2} \nabla C) = Q_w^{CO_2}$$

- Dissolution rate:

$$Q_w^{CO_2} = \kappa S_n \phi \rho_w (x_{CO_2}^{sat} - x_{CO_2}) = -Q_n$$

- EoS:

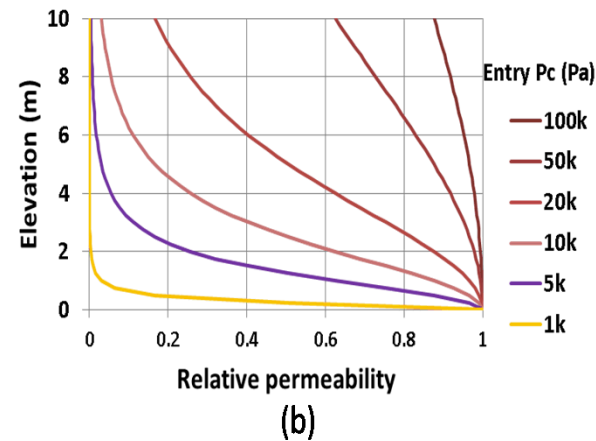
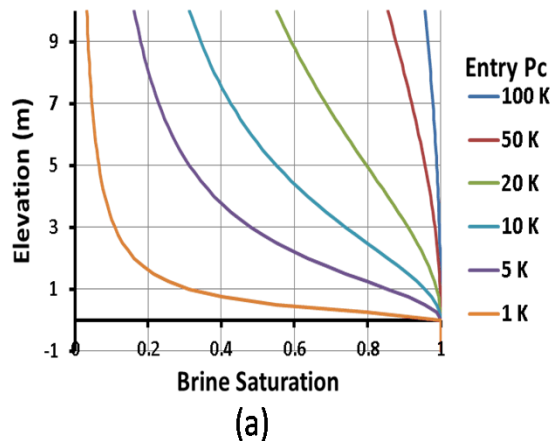
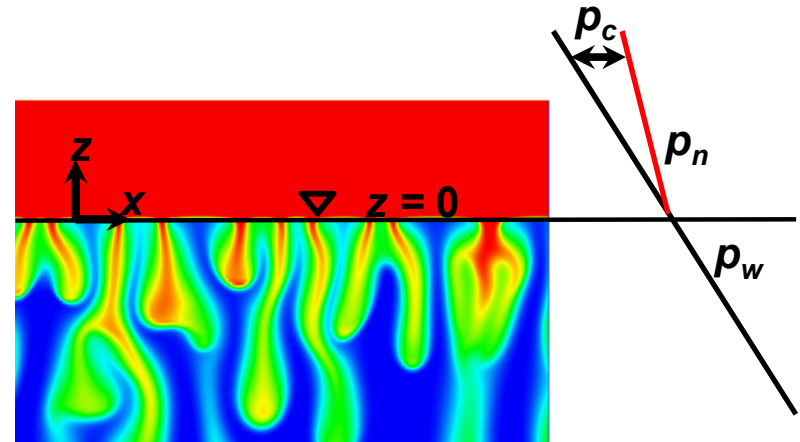
$$\rho_w = \rho_{w,ref} \left(1 + \frac{\Delta \rho_w}{\rho_{w,ref}} \frac{C}{C_{sat}} \right), \quad C \leq C_{sat}$$



Initial state and capillary model

- Hydrostatic initial condition
- Van-Genuchten Pc model plus hydrostatic:

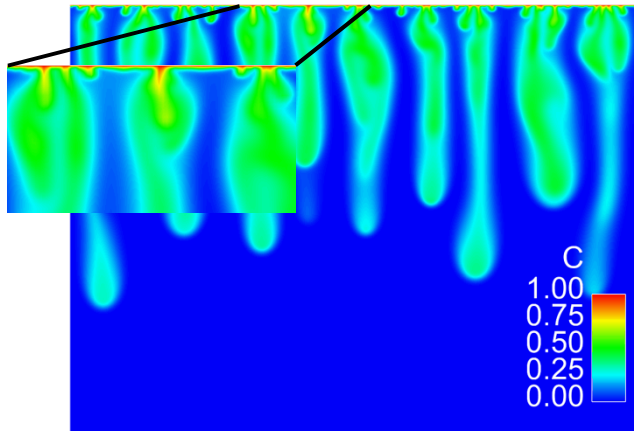
$$s_w(p_c(z)) = \left[\left(\frac{(\rho_w - \rho_n)gz}{p_{c0}} \right)^\beta + 1 \right]^{-\lambda}$$



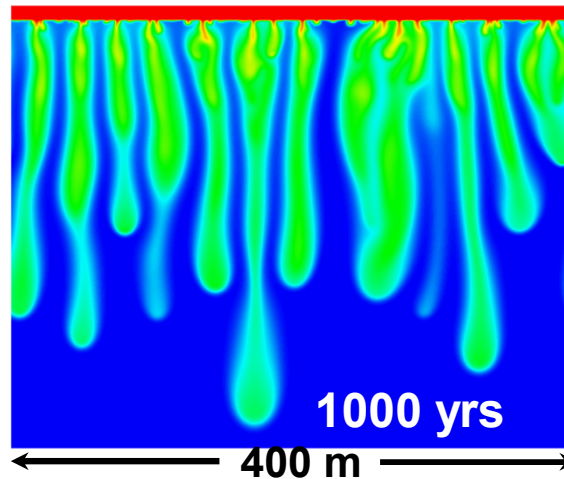
Variation of (a) brine saturation and (b) relative permeability with elevation as a function of “entry pressure,” p_{c0}

Dissolved CO₂ in Bravo Dome ($k = 50$ mD poro = 0.15) reservoir

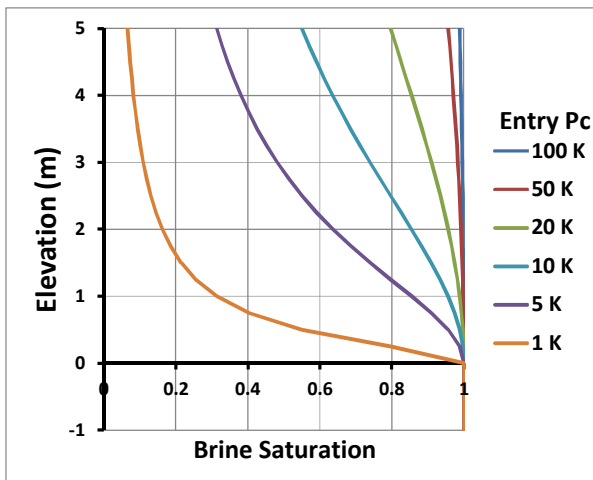
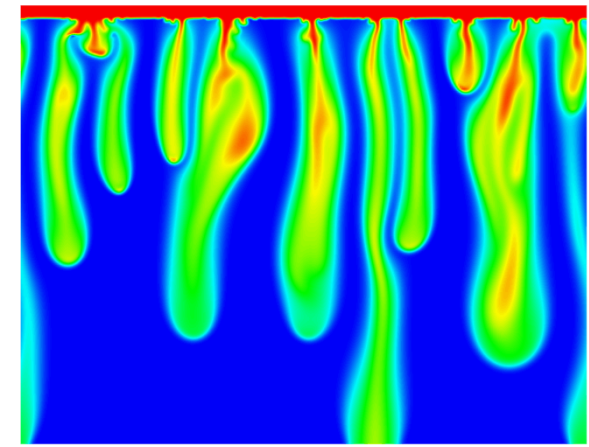
Single phase model



$P_c = 5$ K

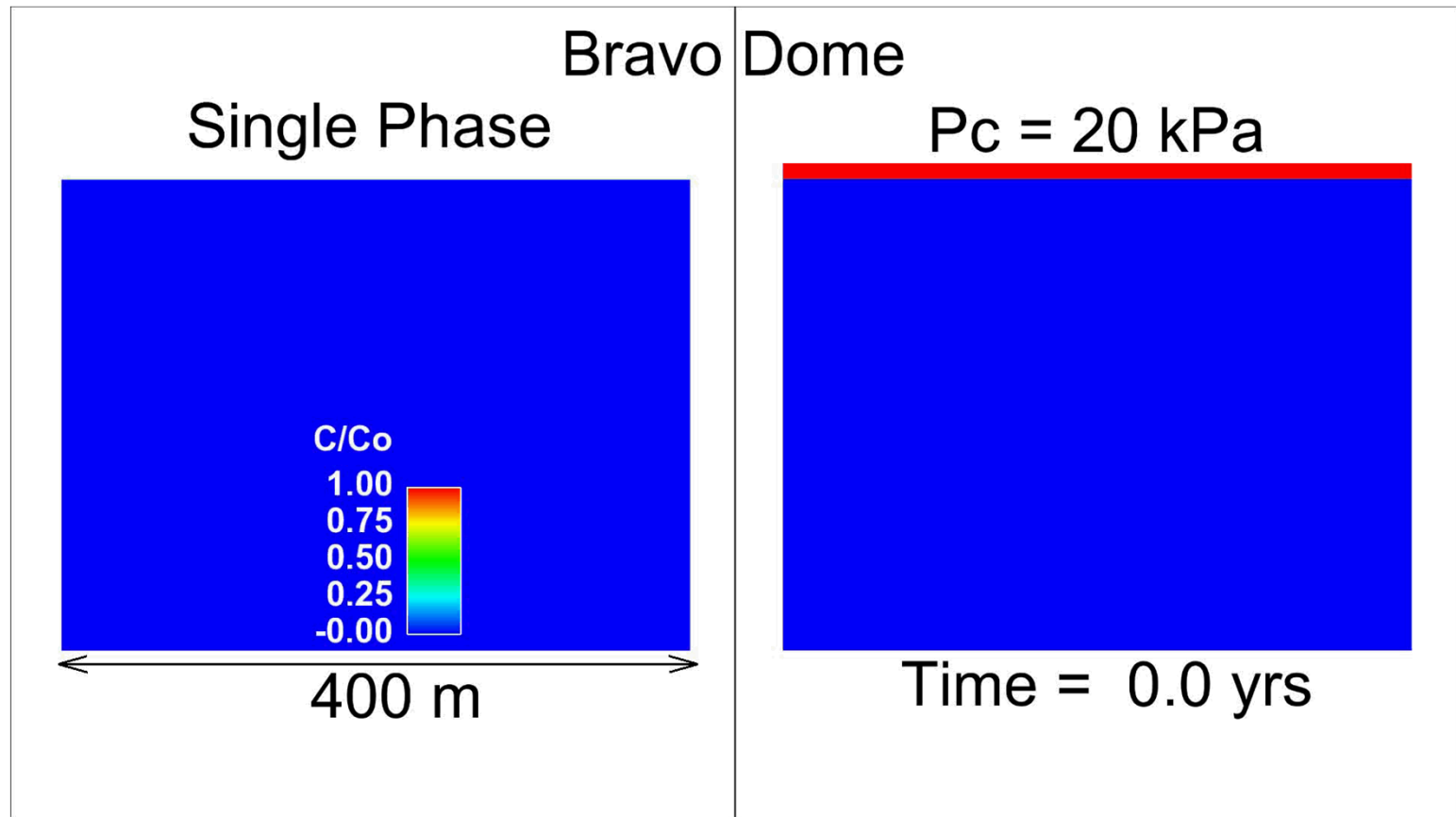


$P_c = 100$ K



- Least dissolution in single phase, closed top model
- Dissolution increases with cross-flow and entry pressure

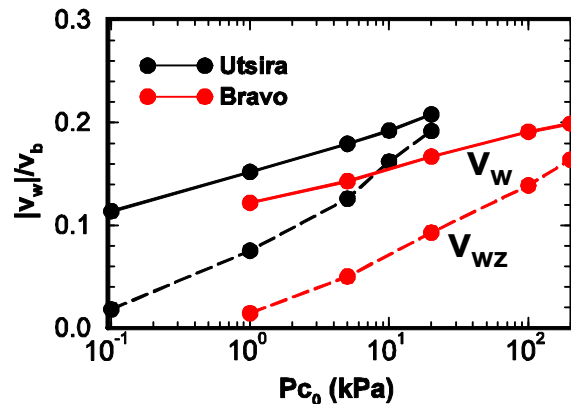
Convective dissolution in a deep reservoir with Bravo Dome properties



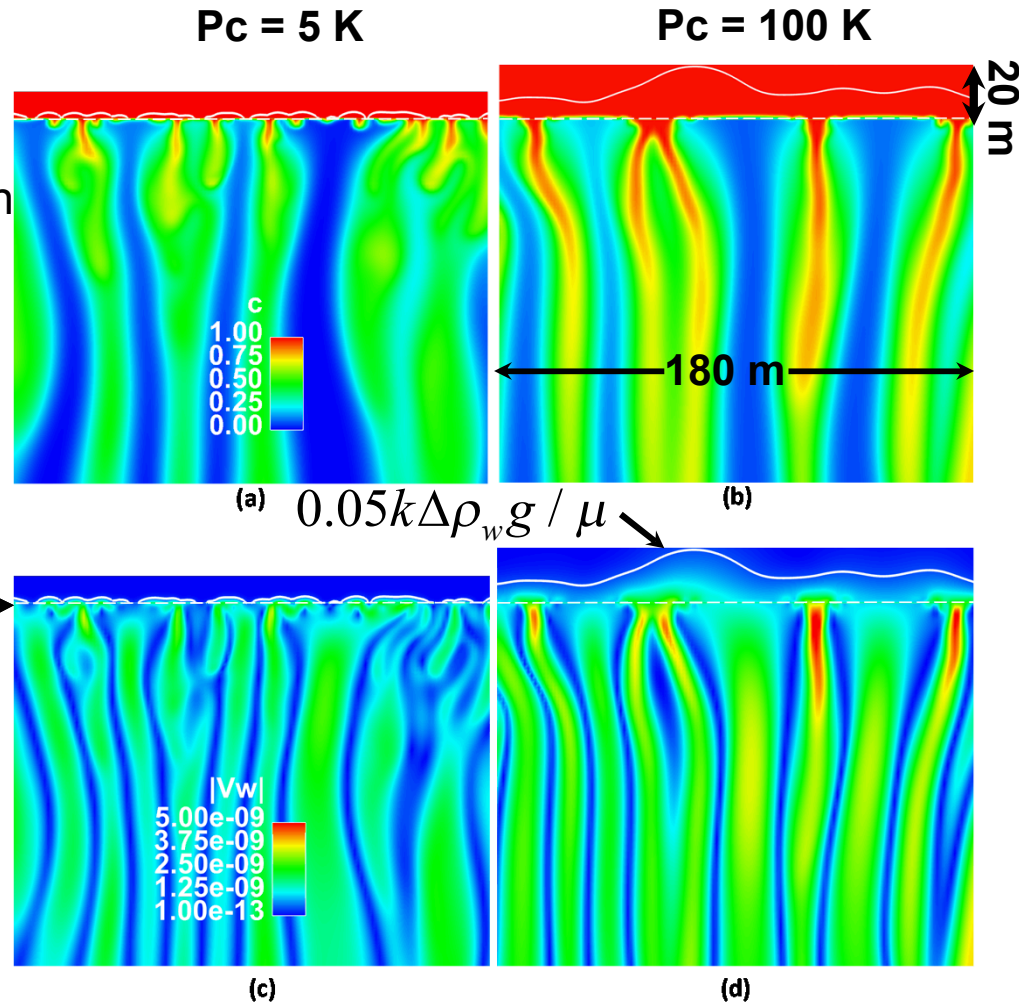
Approximate Convective Onset times: 85 (20 kPa) vs 120 (single phase) yrs

Two-phase model predicts higher dissolution

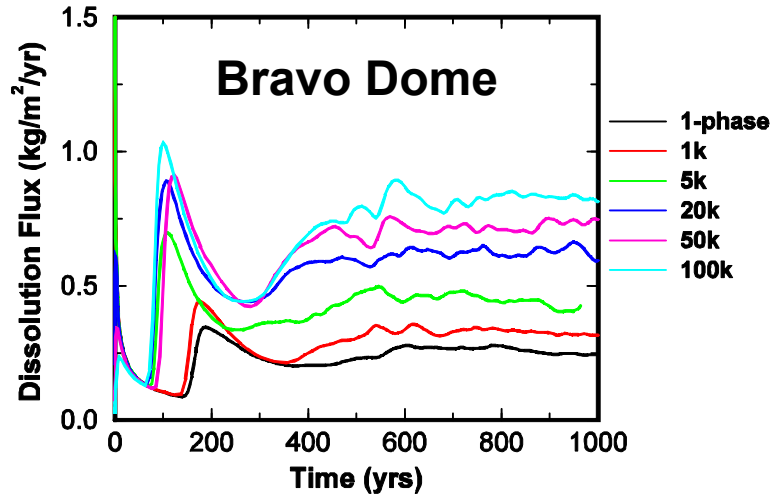
- Two phase model naturally allows currents loops above GWC
- The extent of currents increases with entry pressure (permeability stays high in two-phase region)
- Single phase, closed top:
 - boundary layer diffusion controlled
- Two-phase:
 - current loop \rightarrow convectively-enhanced transport



Convection current strength at GWC increases with entry pressure



Extent of convection currents above GWC Bravo Dome



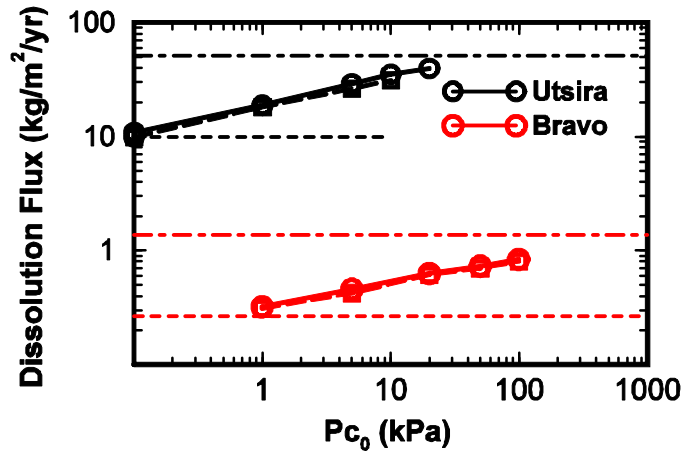
Observations:

- $F \sim 1/\sqrt{t}$ early time diffusion before onset of convective currents
- Onset time decreases with cross-flow and entry pressure
- Quasi-steady flux rate eventually established

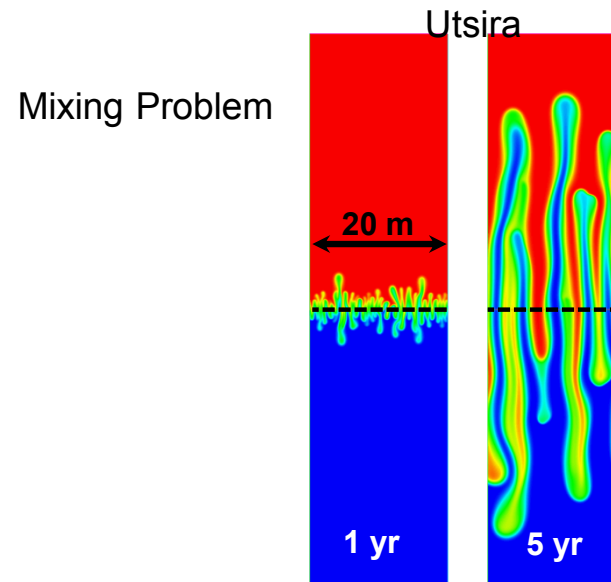
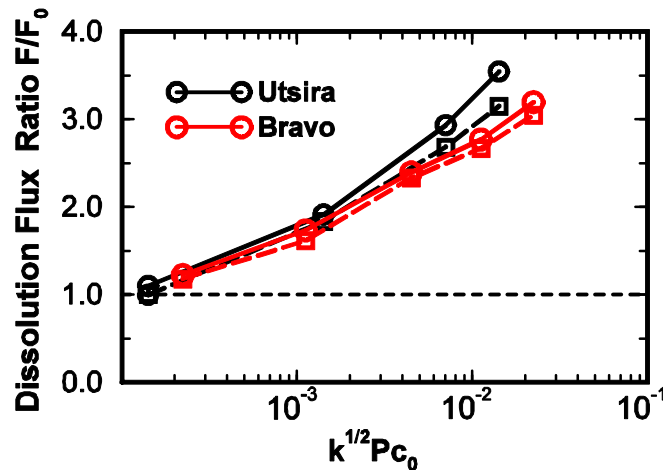
Flux calculation:

- Single phase
 - boundary flux via residual imbalance
- Two-phase

$$F(t) = \frac{1}{W} \int_{\Omega} Q_w^{CO_2} d\Omega$$



- $p_{c0} \rightarrow 0$ recovers the single-phase, closed top dissolution rate
- For “large” but feasible p_{c0} , Flux $\sim 3.5x$ single-phase fluxes
- An upper bound on flux is $\sim 5x$ single-phase value, based on a convective mixing analog



- Inclusion of the two-phase region above the GWC provides a more realistic dissolution model:
 - Allows buoyantly driven convection current loops into the two-phase region
 - Dissolution of gas-phase CO_2 into brine is convectively assisted with current loops
 - For feasible values of entry pressure, the dissolution rate can be roughly 3.5 times the rate from a single-phase representation
 - An upper bound may be 5x based on a mixing model analog
- Single-phase, closed top model:
 - Generally under-predicts dissolution rate,
 - except for a reservoir with vanishing entry pressure (sand) $p_{\text{co}} \rightarrow 0$ where the two model representations converge

