

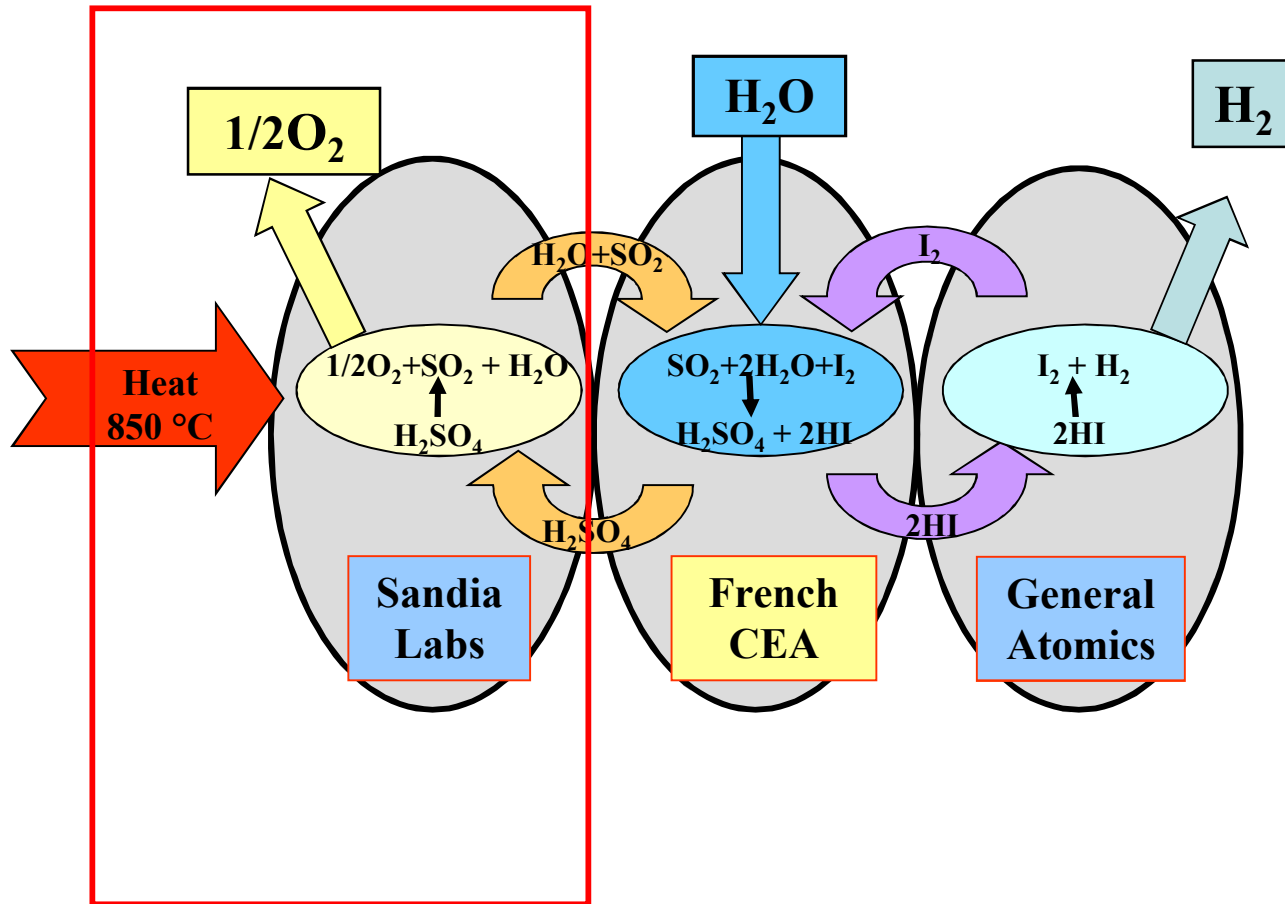


Pressurized Sulfuric Acid Decomposition Experiments for the Sulfur-Iodine Thermochemical Cycle

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Sulfur-Iodine Thermochemical Cycle

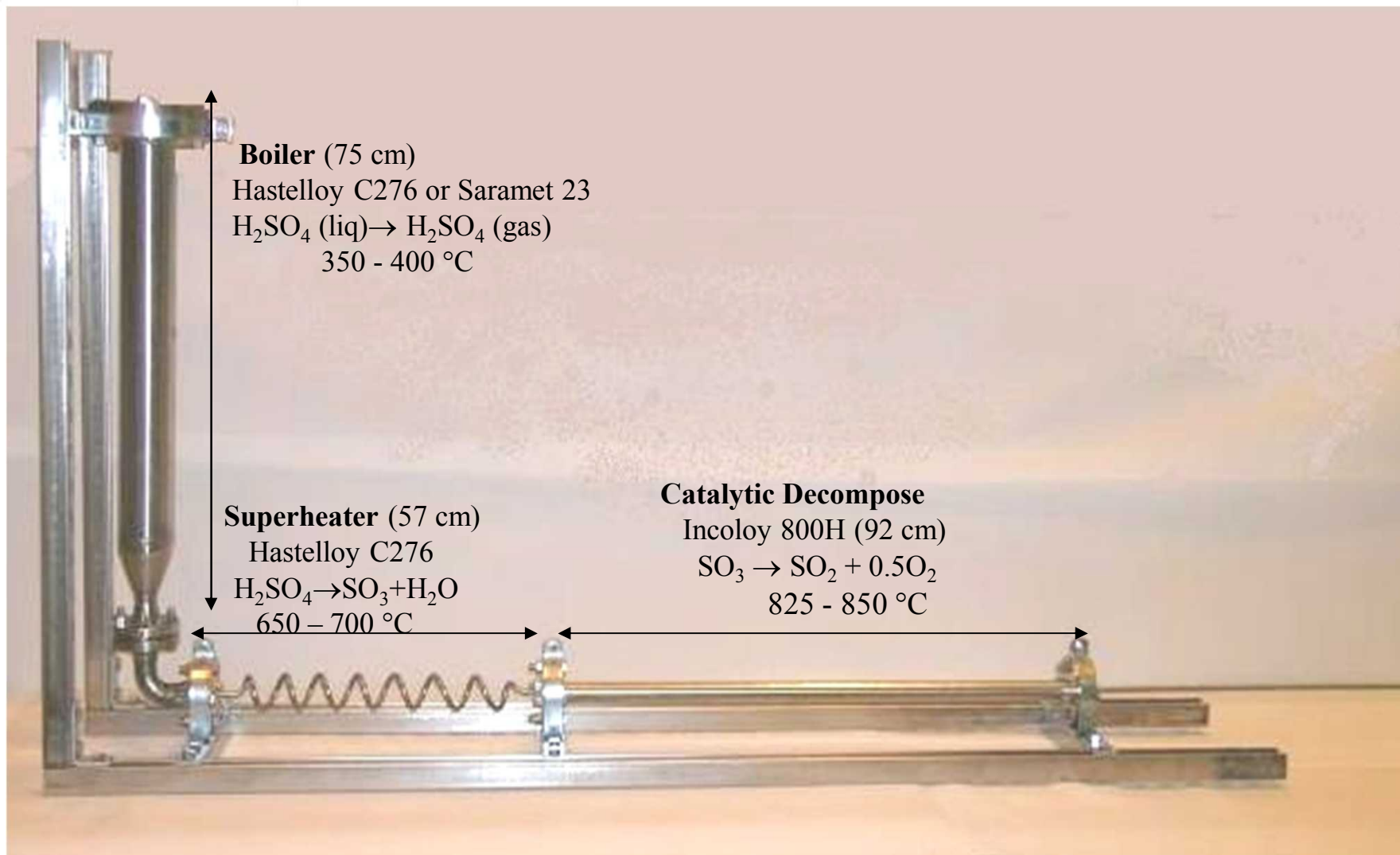




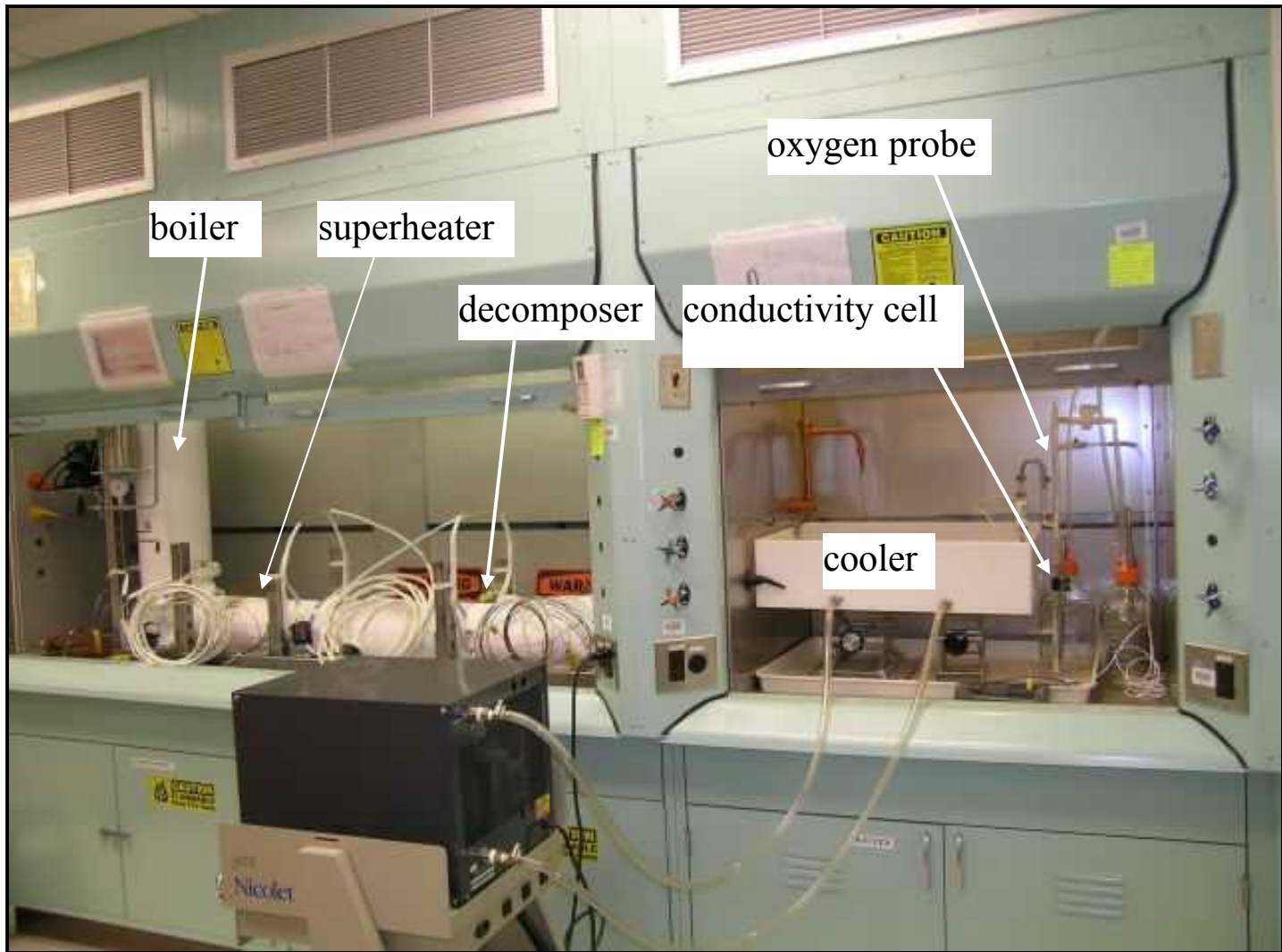
Objectives

- **Demonstrate laboratory-scale sulfuric acid decomposition process with engineering materials**
- **Assess process performance and materials**
 - Variations in acid concentration, temperature, and pressure
 - Catalyst: conversion, poisoning, acid concentration, temperature, pressure
 - Engineering materials (starting with Hastelloy, Incoloy, ceramics, and glass)
- **Integrate into a closed-loop SI cycle:
Integrated Lab-Scale (ILS) Experiments**
 - Real-time instrumentation for process control

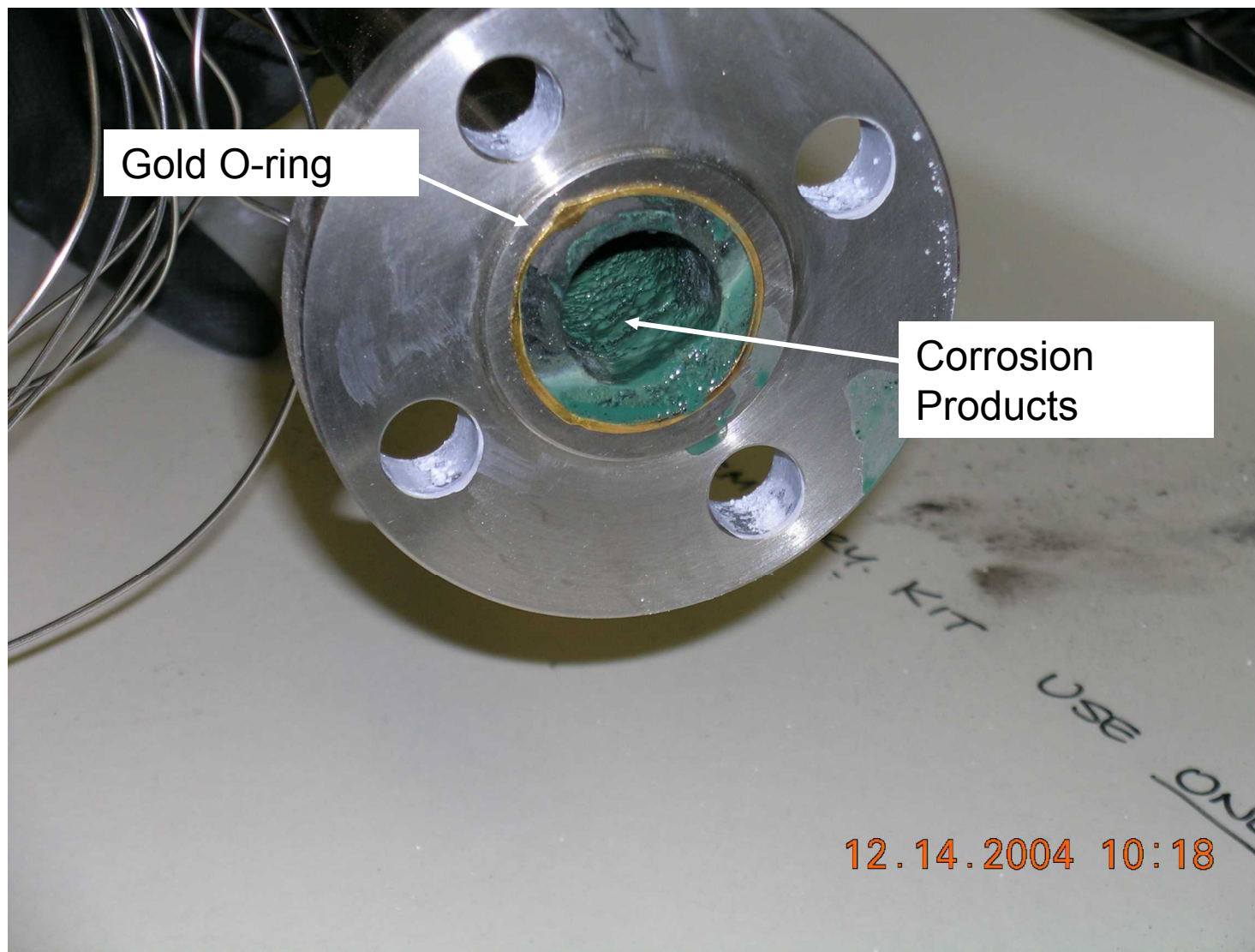
Basic Lab-Scale Units



Laboratory-Scale Acid Decomposer



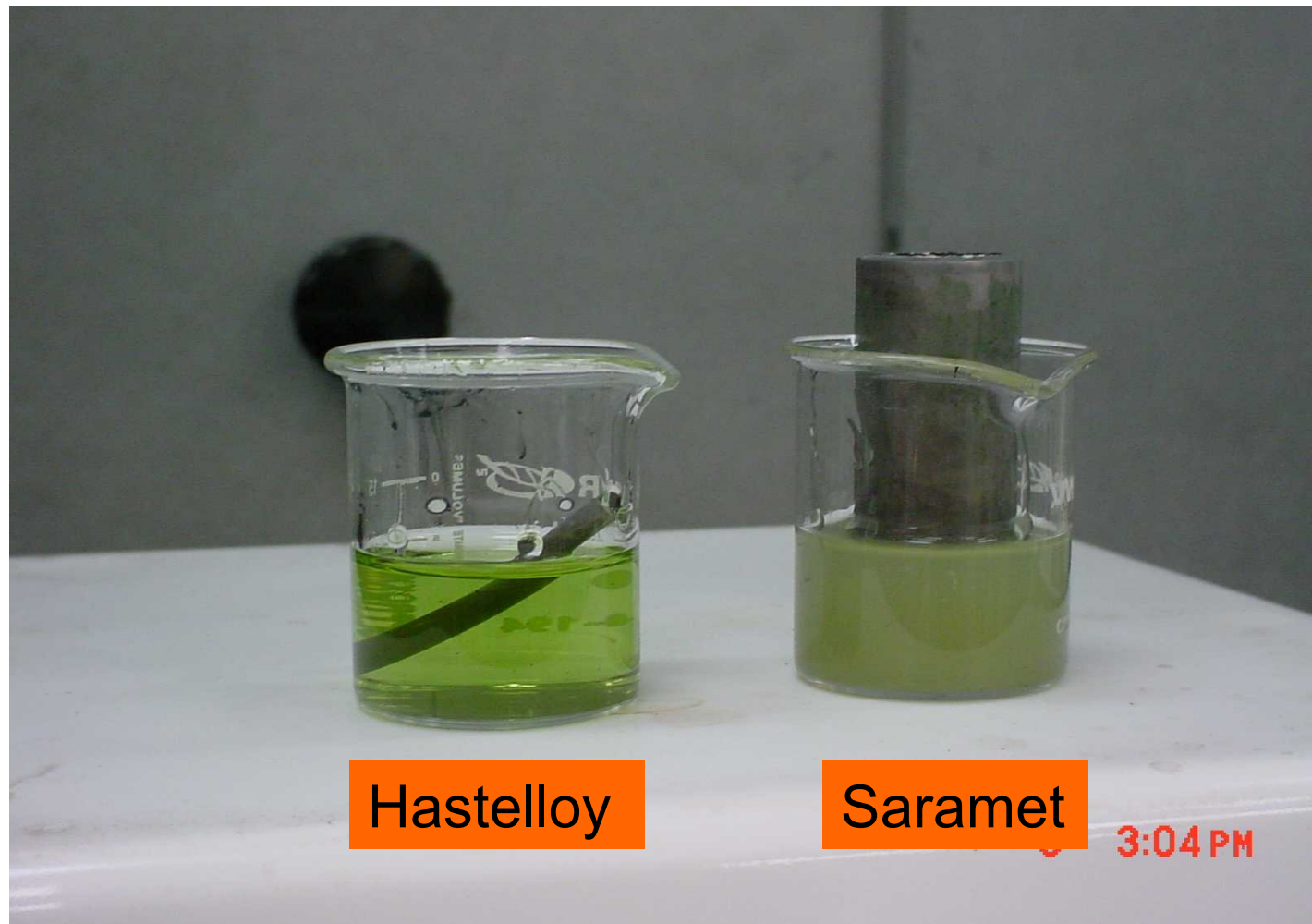
Post Decomposer



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Simple Corrosion Test

40 mol% acid after 20 minutes

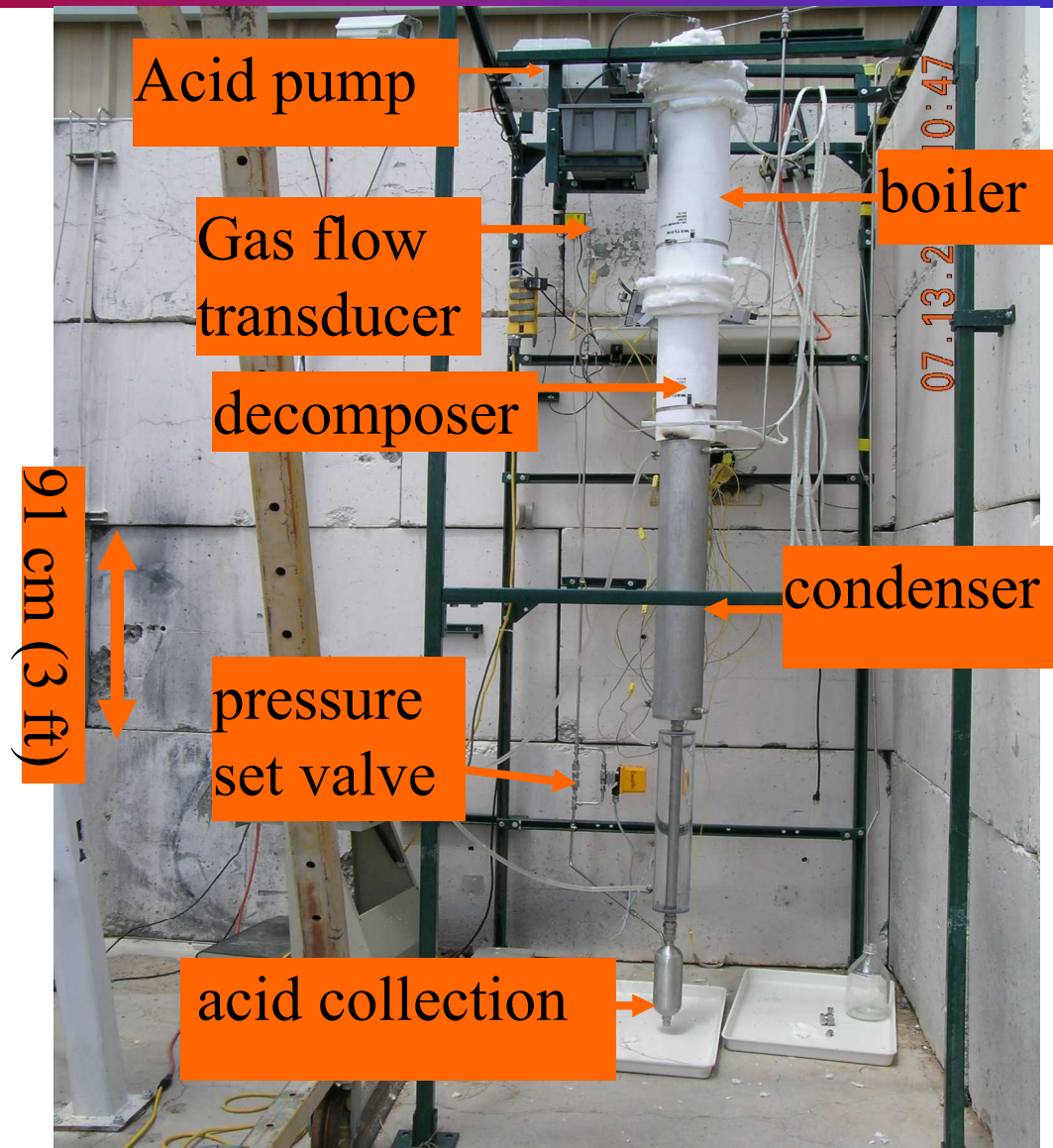




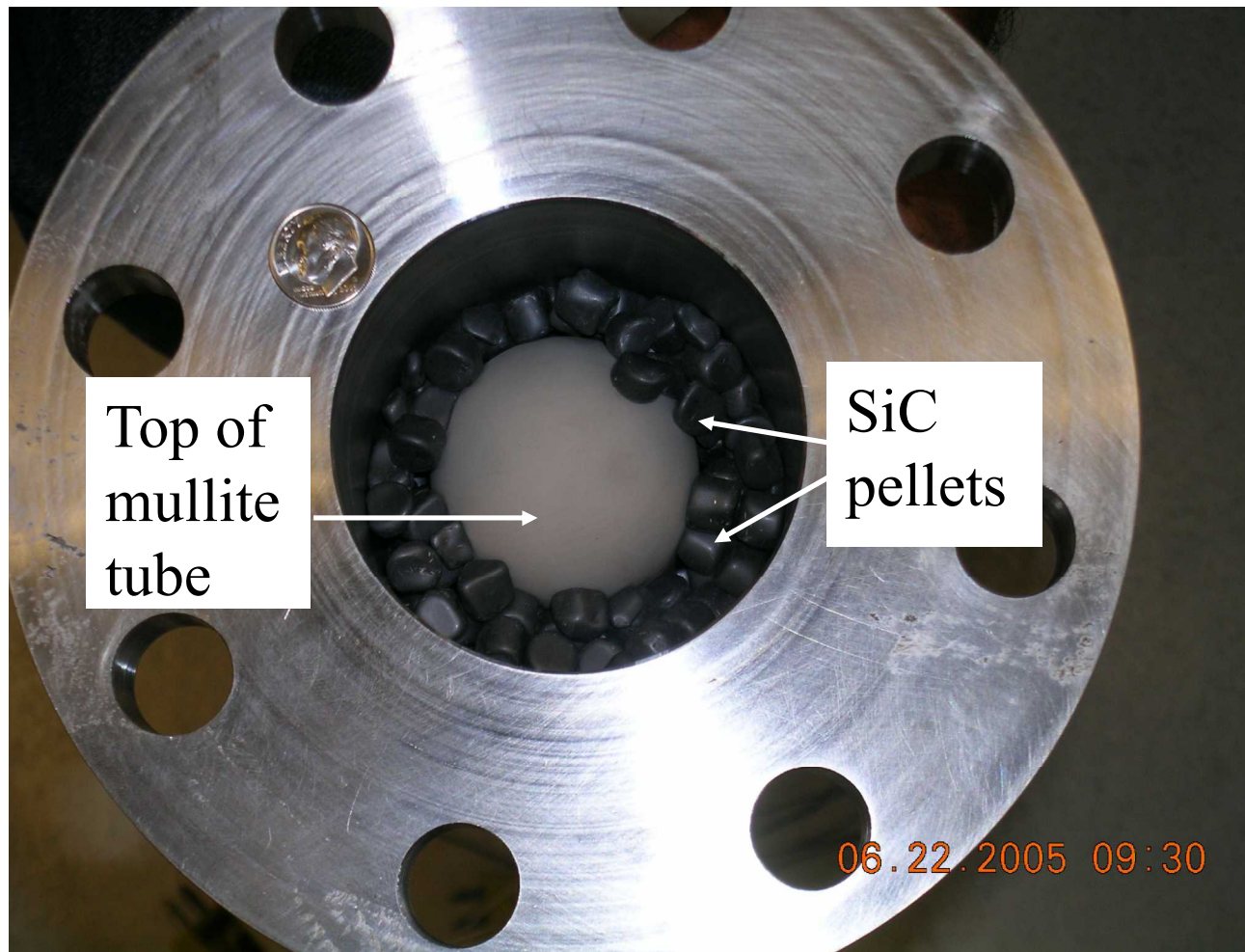
Results of First Acid Test

- **Corrosion products clogged apparatus in minutes**
 - Green deposits primarily in upper boiler and after decomposer. (Incoloy 800H flange severely corroded, ~1/2 mm).
 - Boiler thermocouple tube (Hastelloy) corroded slightly. Hastelloy flange blackened and bonded with gold O-ring.
 - Corrosion rates much higher than estimated from data with sulfuric acid coupon tests
 - Static versus flow experiments
 - SO_2 and O_2 may contribute to enhanced corrosion
 - Volume expansion: $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}/\text{Fe} = 21$
- **New Strategy Based on Test Results**
 - Keep metallic walls either very hot ($>600^\circ\text{C}$) or cold ($<20^\circ\text{C}$)
 - Ceramics/glass needed for hot liquid acid vaporizing or condensing acid vapors

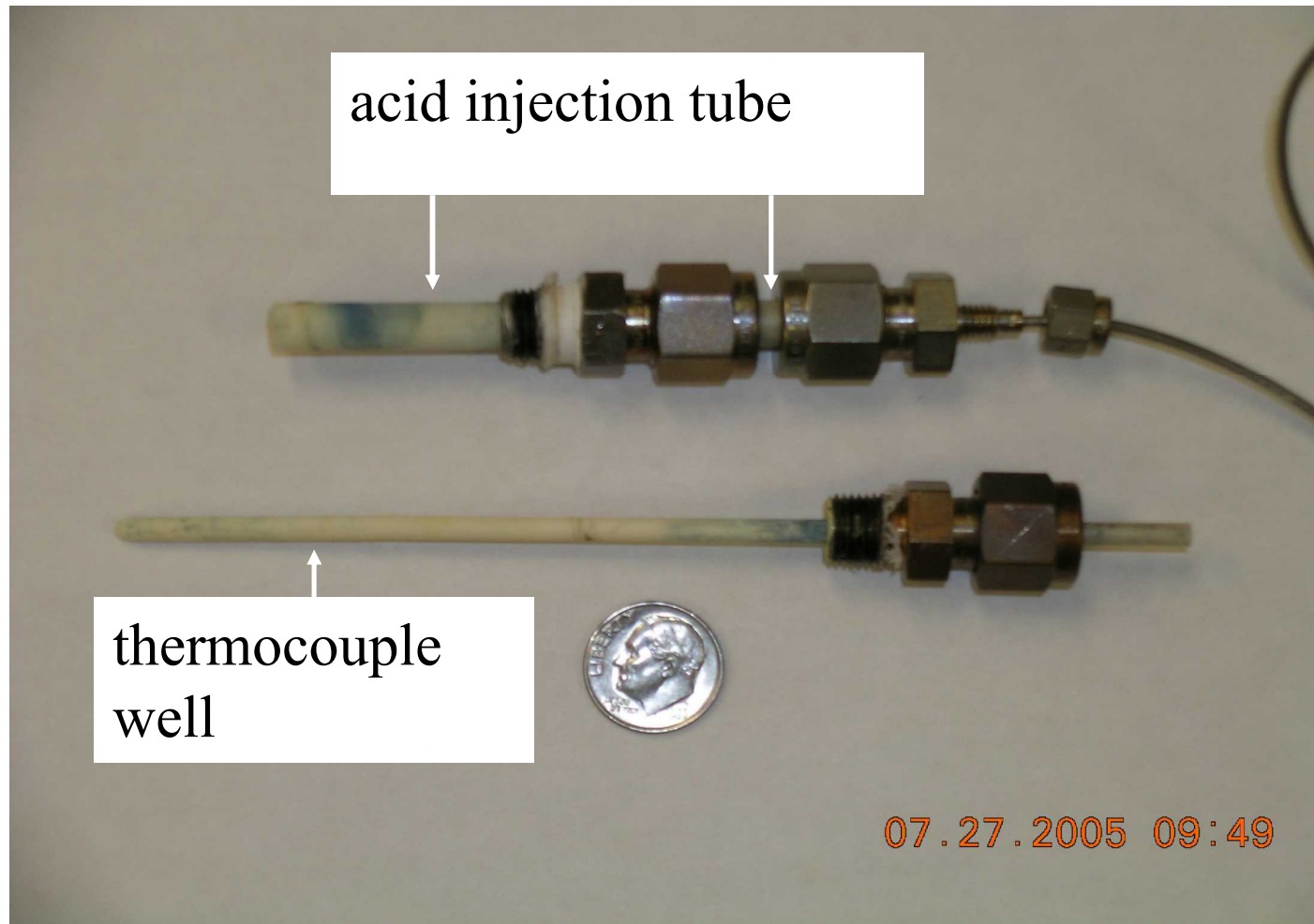
Single-Pass Sulfuric Acid Decomposition Apparatus



Top of Boiler



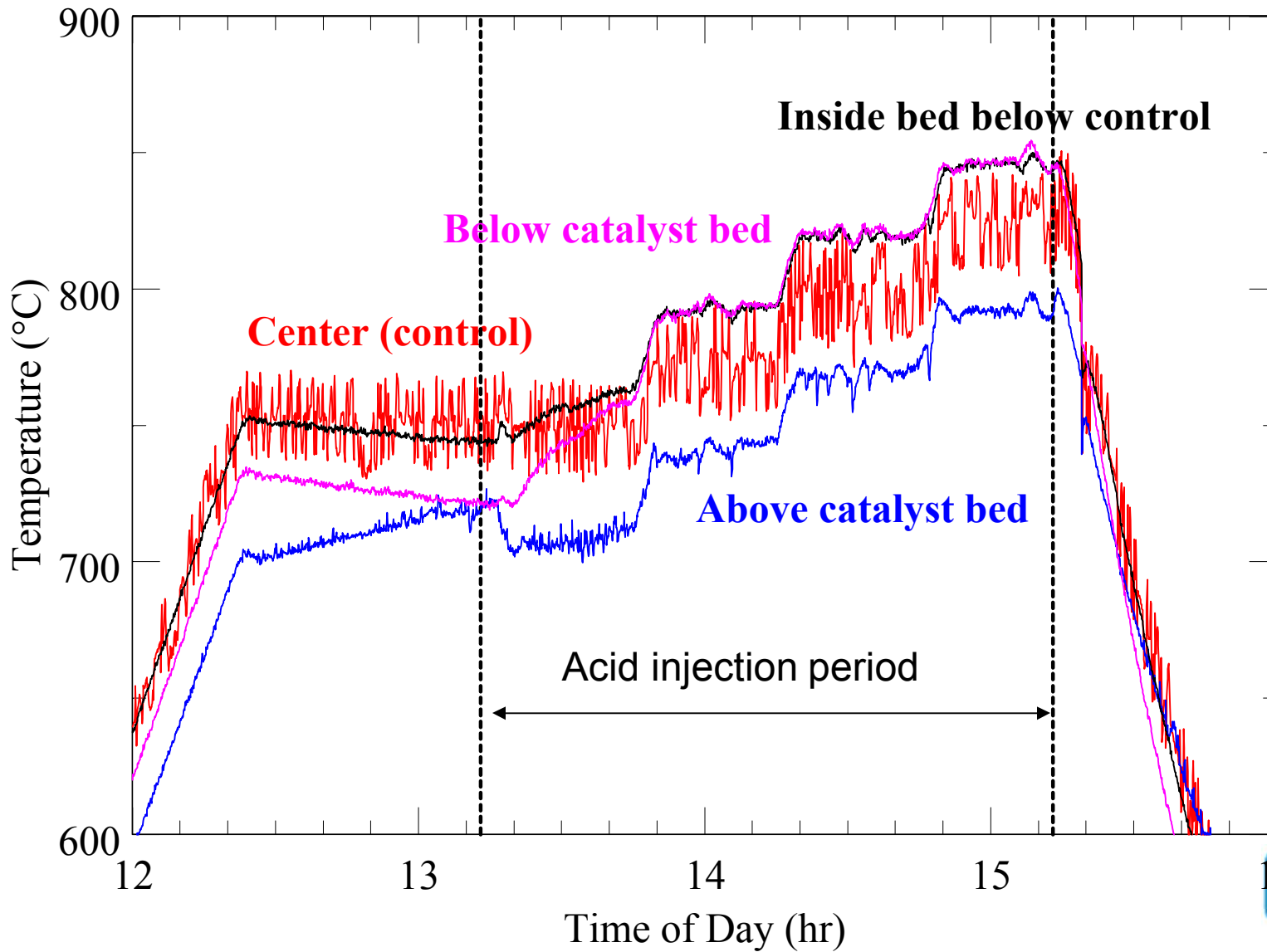
Ceramic Injector and Thermocouple Well



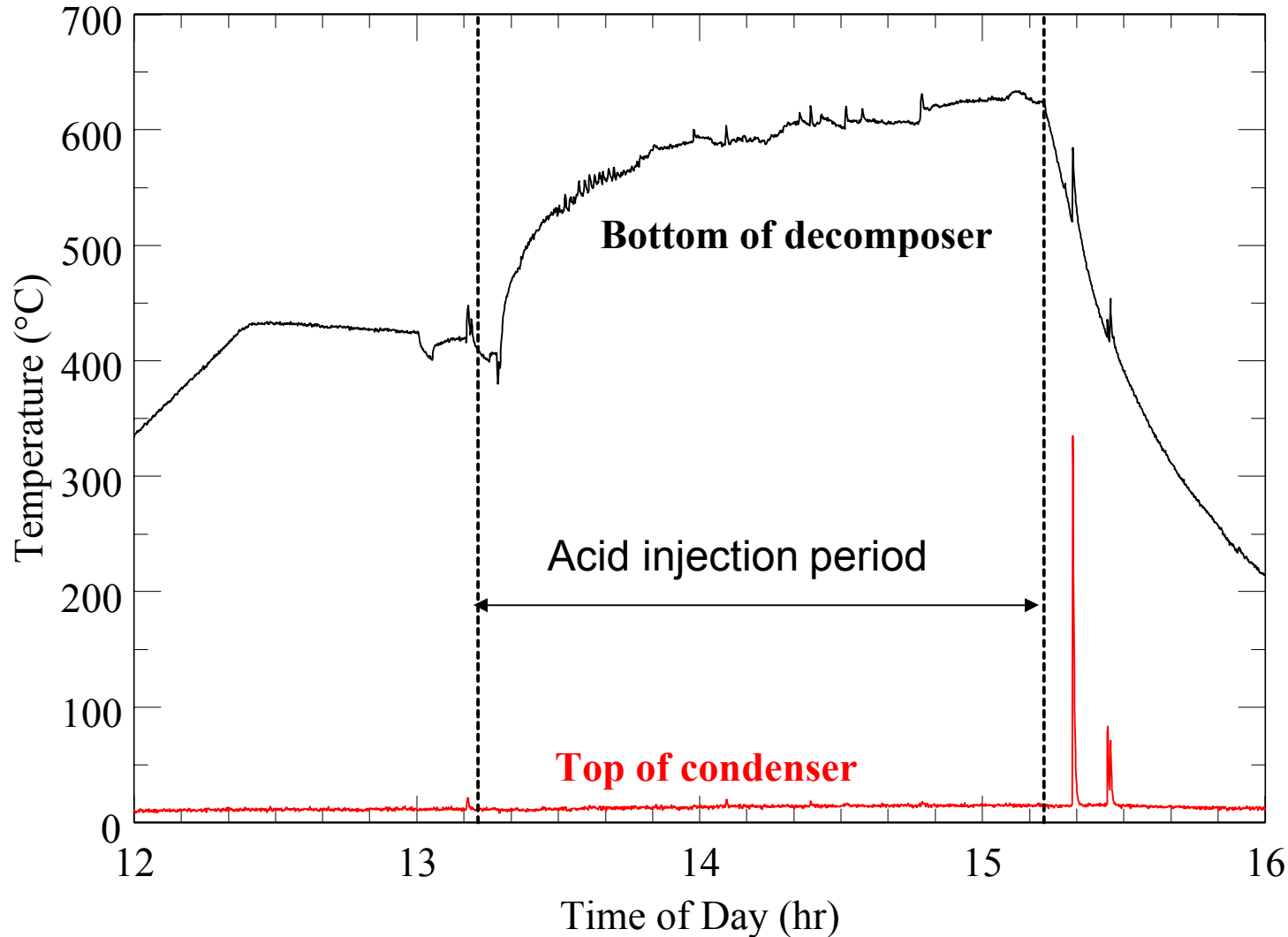
Corrosion Coupon Testing



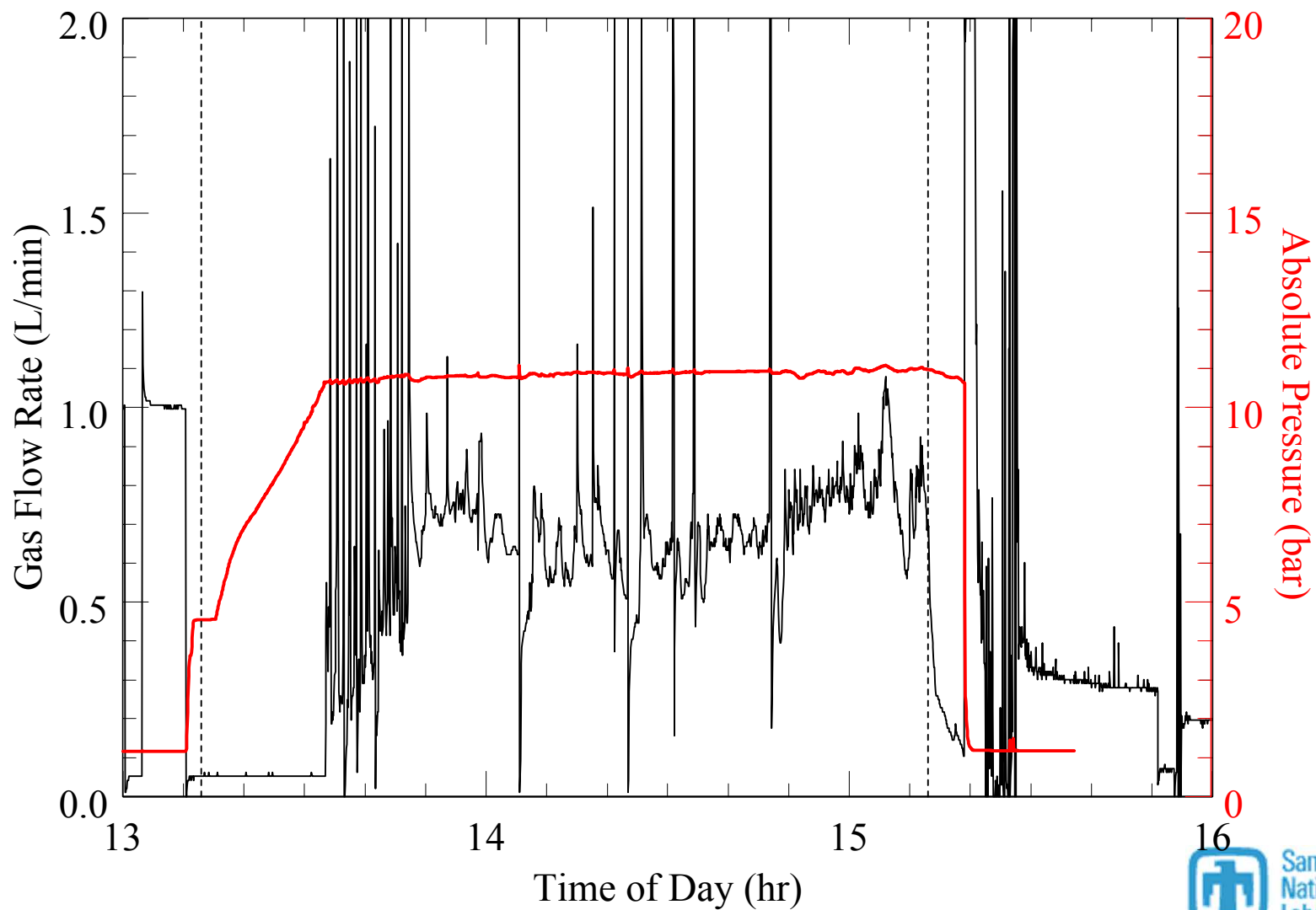
Decomposer Temperature Profile



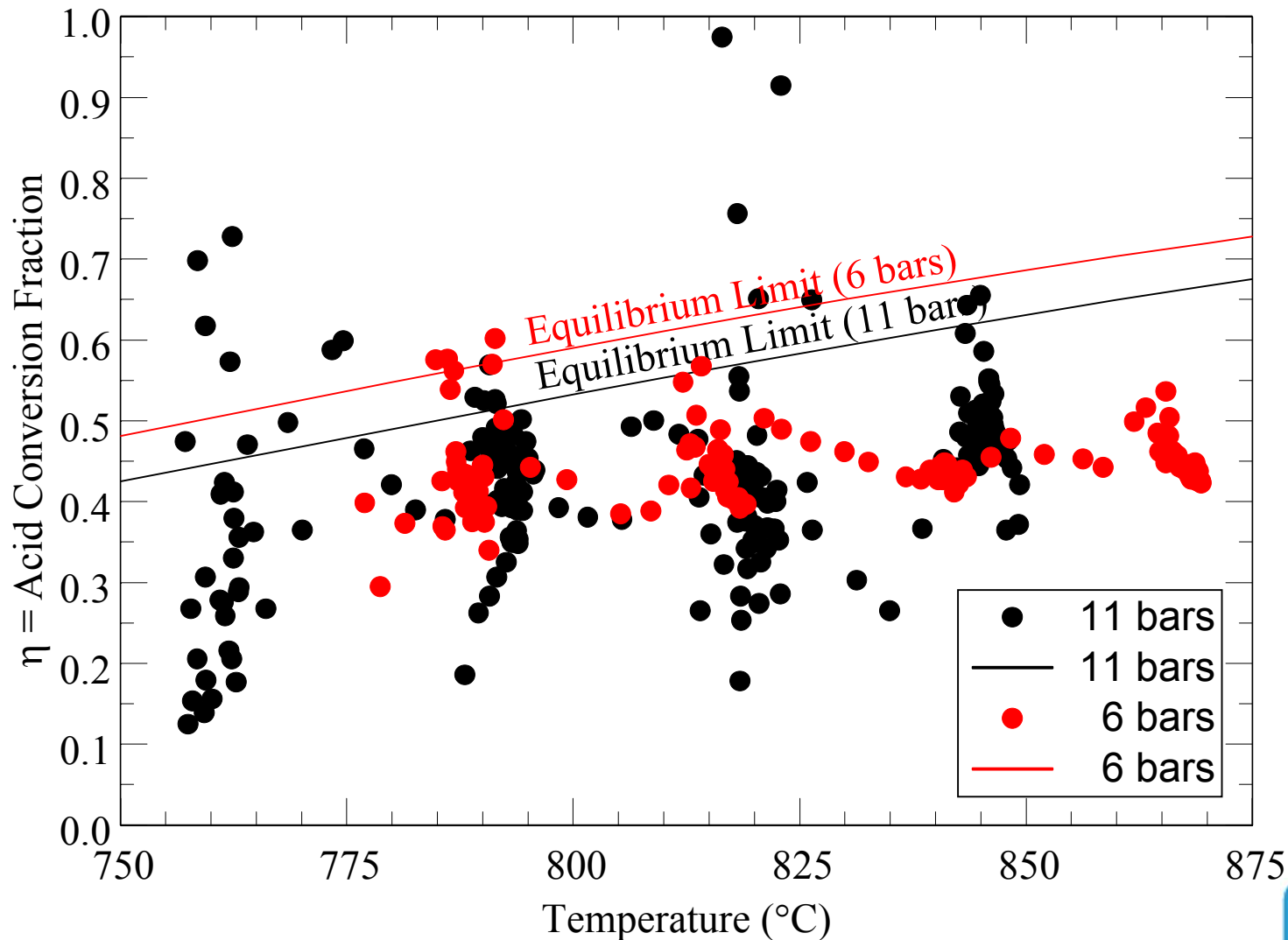
Bottom of Decomposer & Top of Condenser Temperature Profiles



Flow Rate & Pressure



Acid Conversion Fraction





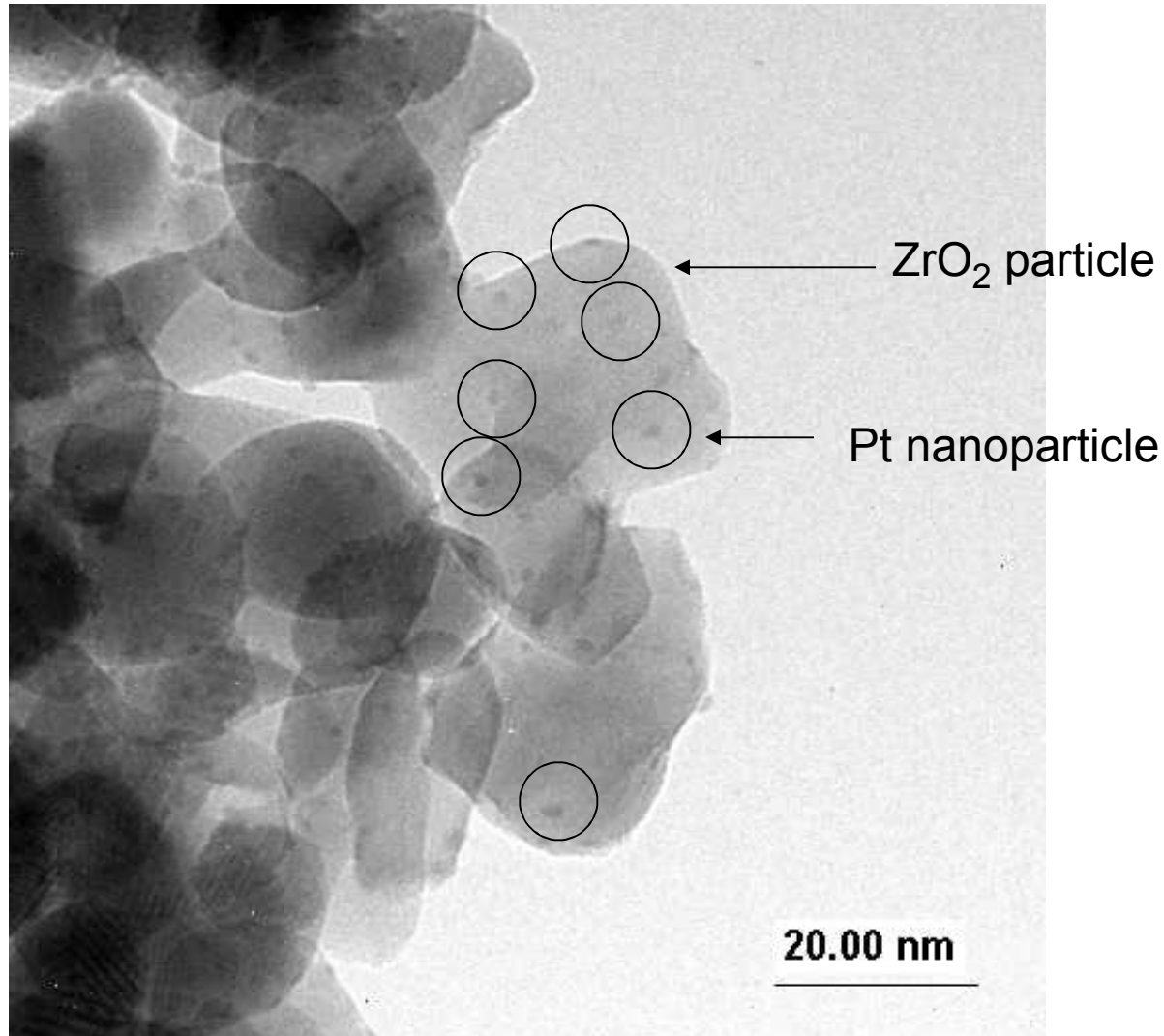
Platinum Catalyst on Zirconia



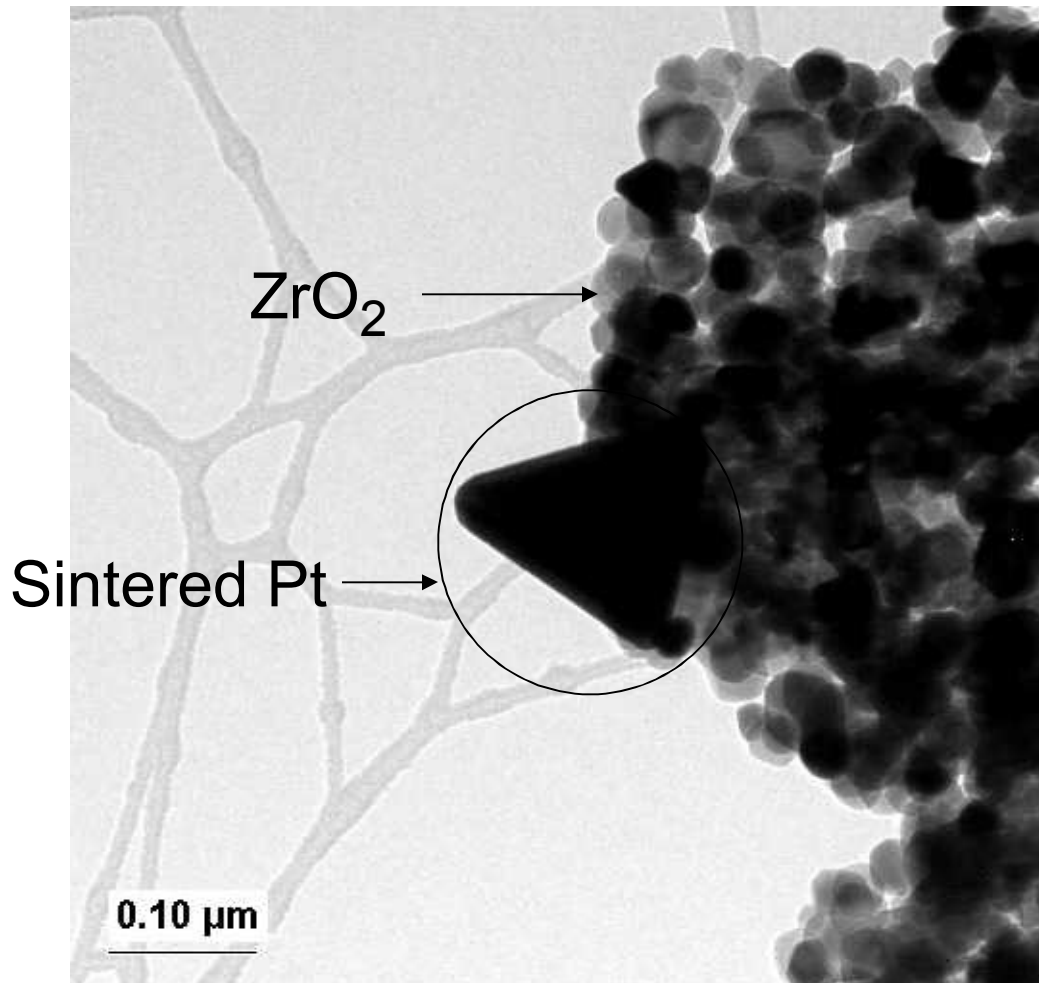
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Pretest TEM of Catalyst

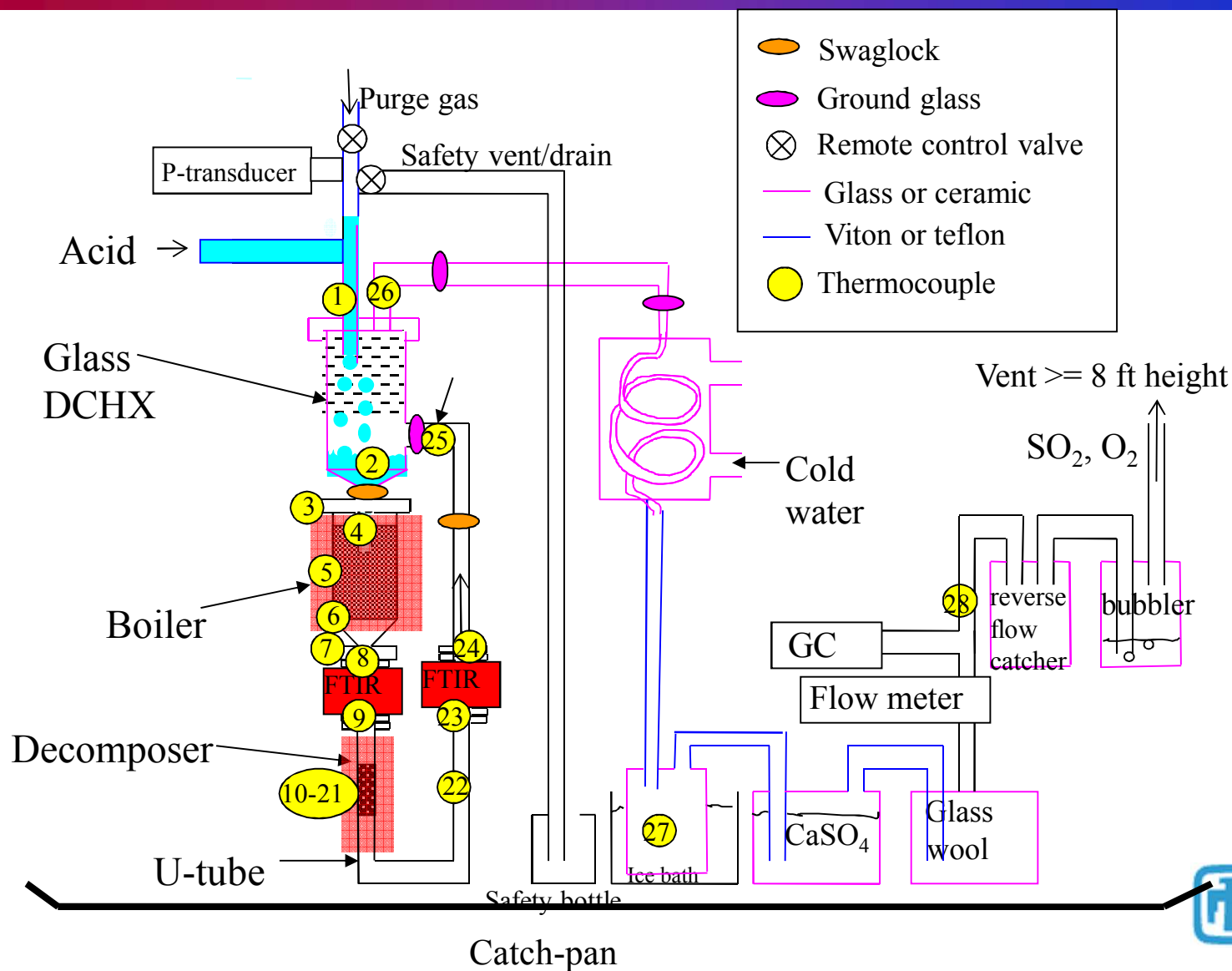
(Tom Headley, SNL)



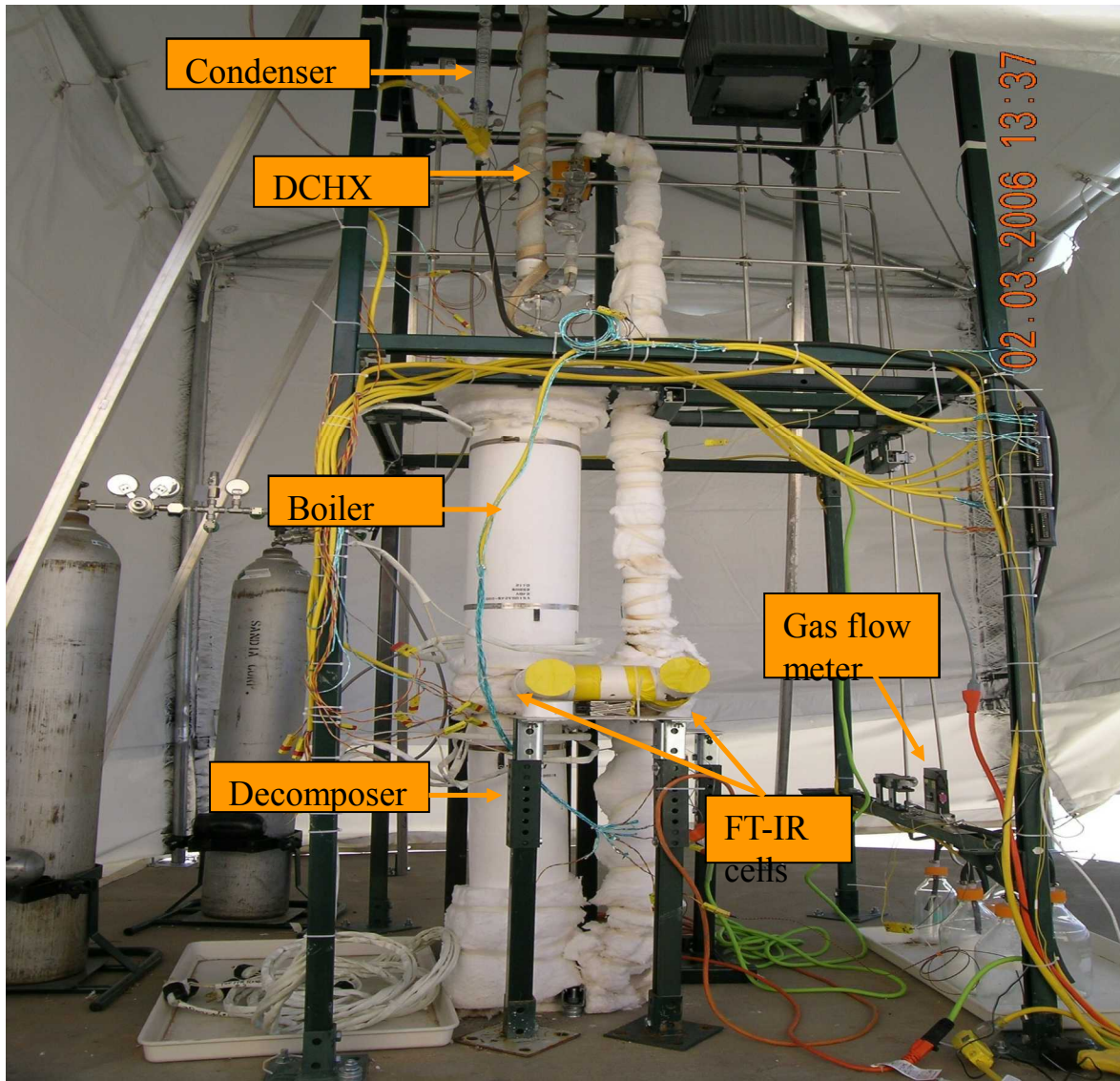
Post test TEM of Catalyst (Tom Headley, SNL)



DCHX & FT-IR



DCHX Apparatus





Recycling Undecomposed Acid

- **Direct Contact Heat Exchanger recovers heat and recycles undecomposed SO_3**
- **Corrosion for acid condensation can be greatly minimized by condensing in ceramic/glass tubes (or rapid quenching)**
- **Hardly any corrosion**
 - boiler heated to $\sim 600^\circ\text{C}$
 - glass insert at top of boiler
 - Condense into glass/ceramic DCHX



Summary

- Pressurized lab-scale apparatus fabricated, assembled, tested, and operational
 - Completed series of pressurized acid tests (2, 6, and 11 bars)
 - Demonstrated real time measurements which are needed for process control
 - Acid conversion fraction 15-20% below theoretical maximum determined by equilibrium
 - Corrosion problems resolved by either rapid quenching or condensing on ceramic/glass materials



Future Plans Leading to Integrated Lab-Scale Experiments

- Metallic components contacting acid will be removed in subsequent tests
 - All ductile metals tested corroded significantly in hot/warm liquid acid
 - Brittle ceramics or glass required for condensing unreacted acid for recycling
- Test incorporating acid concentrator planned for August 2006
- Demonstrate full Section 2 for ILS experiments Dec 2006