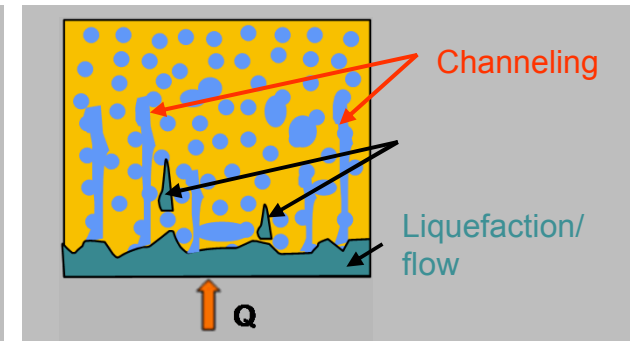
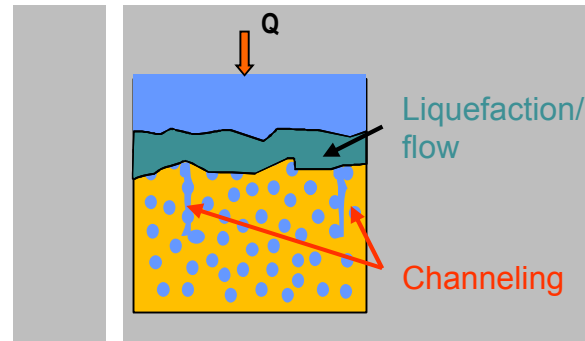
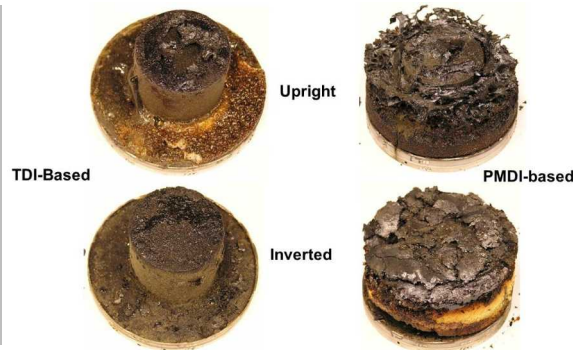


Exceptional service in the national interest



Interface Tracking For Modeling Thermal Decomposition of Polymer Foams

Victor E. Brunini

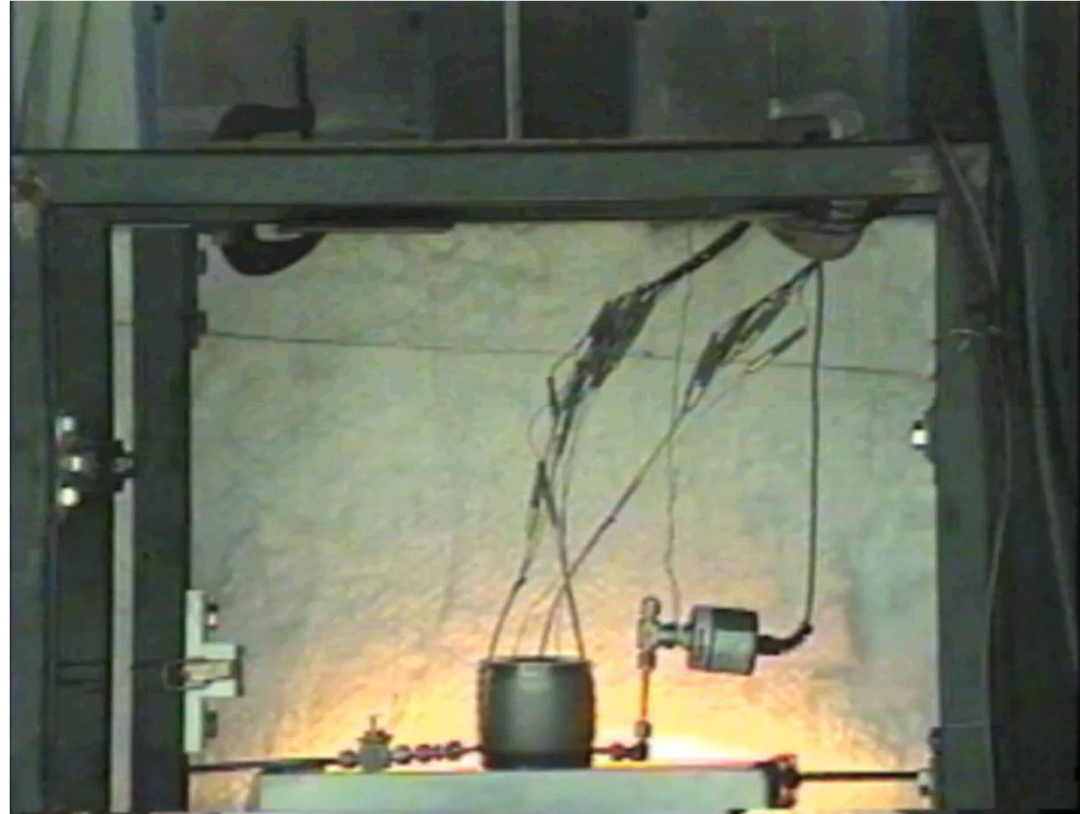
Ryan Keedy, Sarah Scott, David Noble, Amanda Dodd

Outline

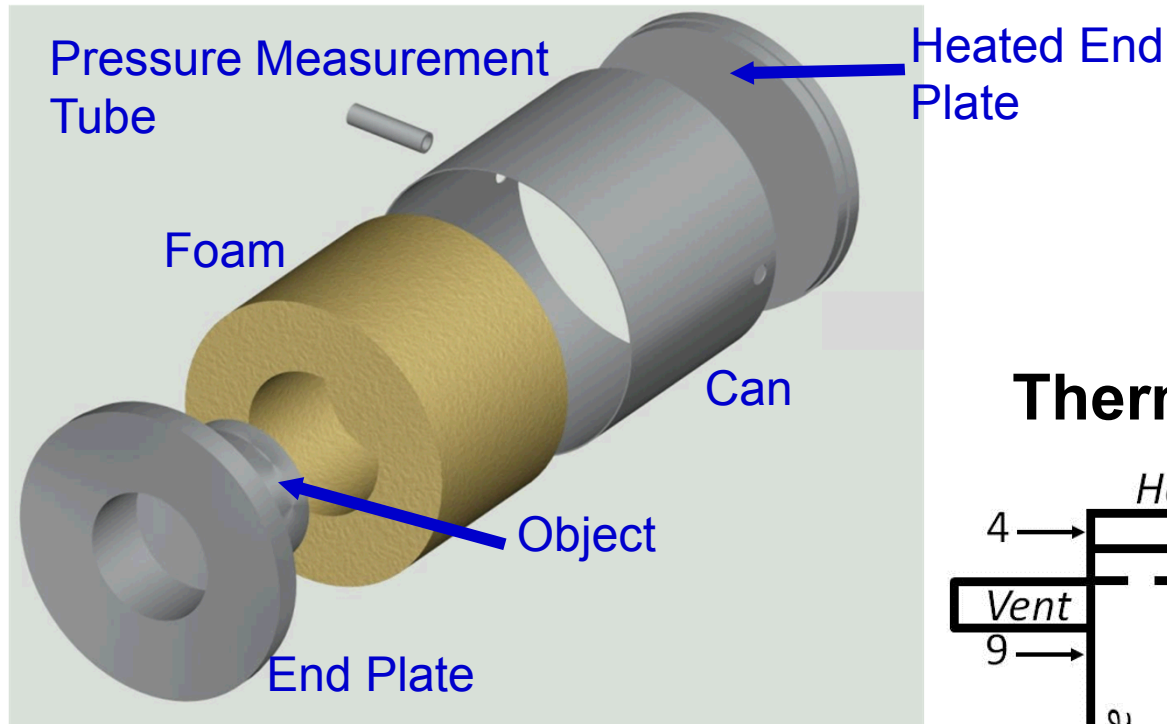
1. Motivation
2. Background and experimental understanding
3. Modeling approach
4. Preliminary model results
5. Conclusions + Future work

Foam Behavior in Fire Environments

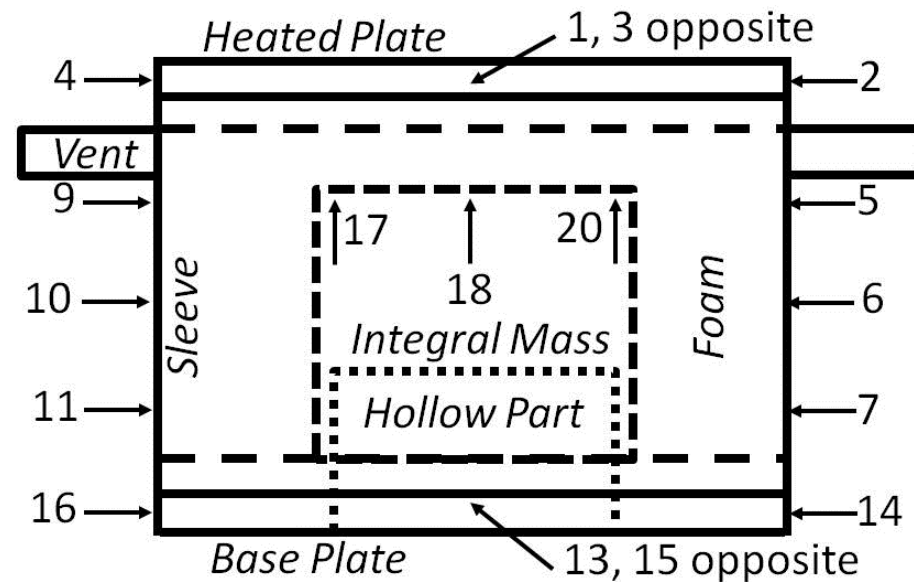
- Polymer foams provide thermal, mechanical, & electrical isolation in engineered systems
- In a fire foam decomposes and loses effectiveness as insulator
- Modeling techniques also applicable to other problems like ablation, carbon composite fires, etc.



Foam in a Can (FIC) Geometry

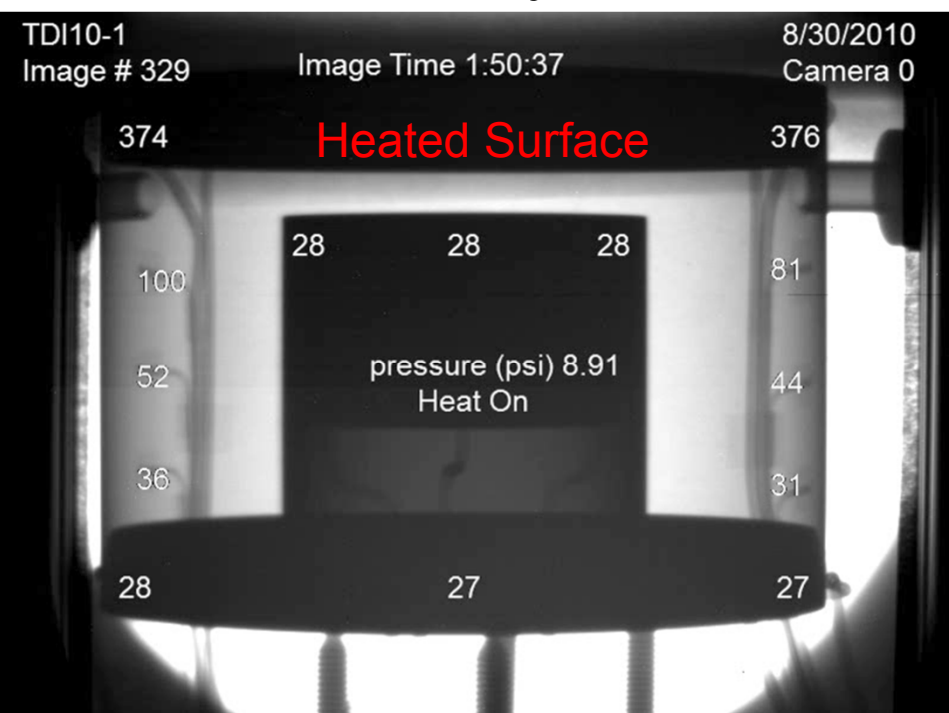


Thermocouple Locations

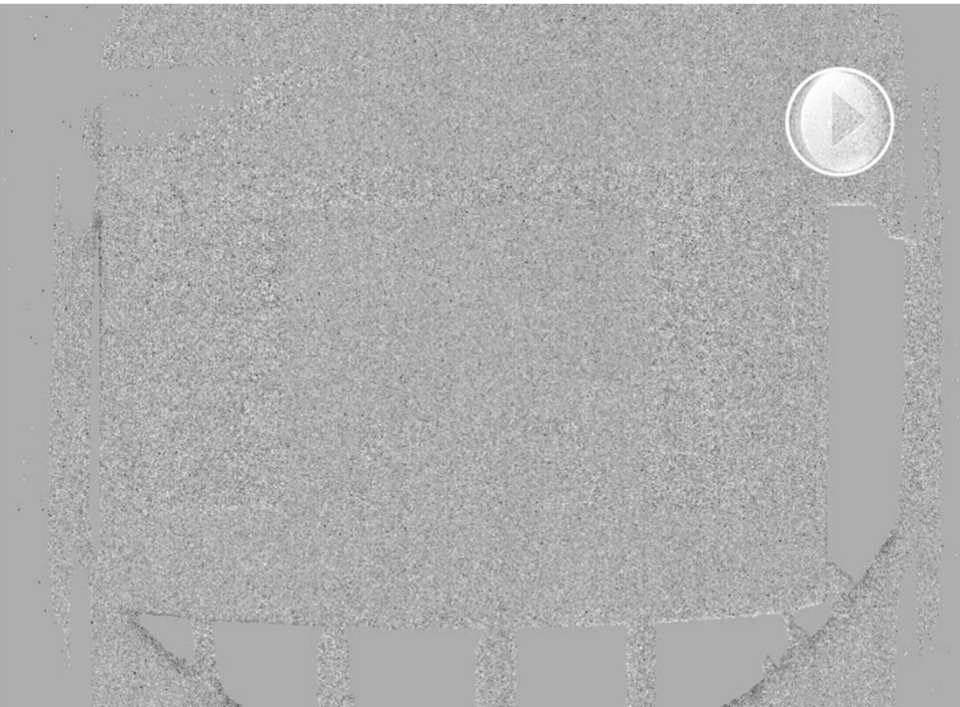


X-ray Video Captures Foam Decomposition Front

X-ray

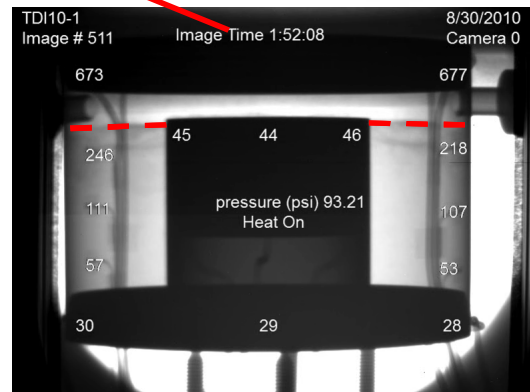
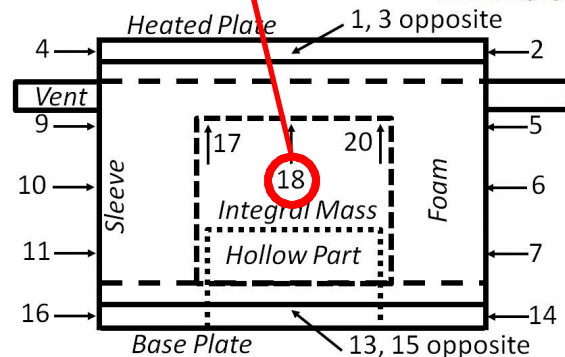
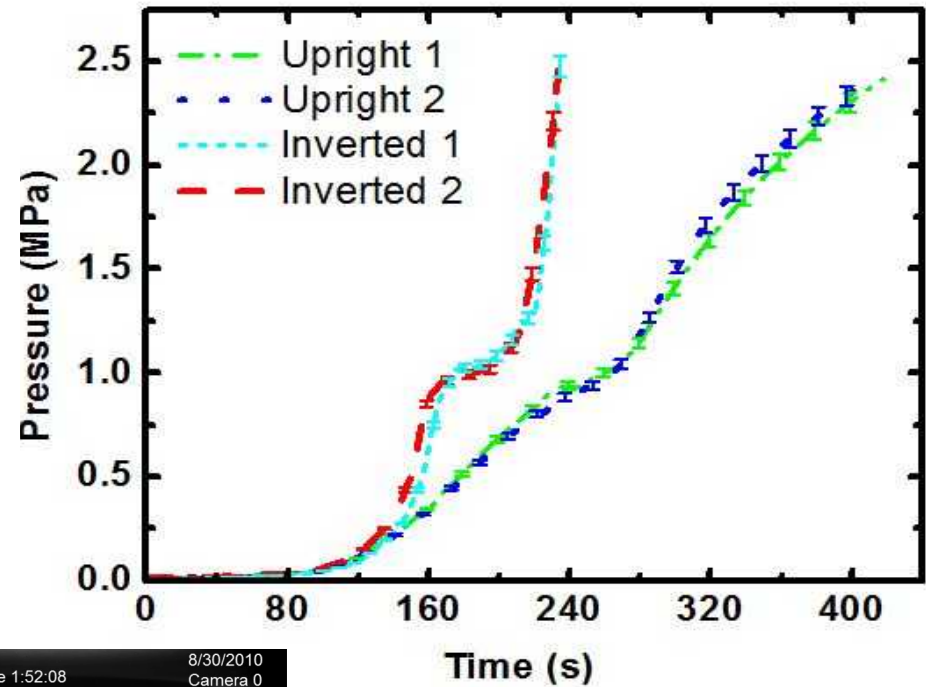
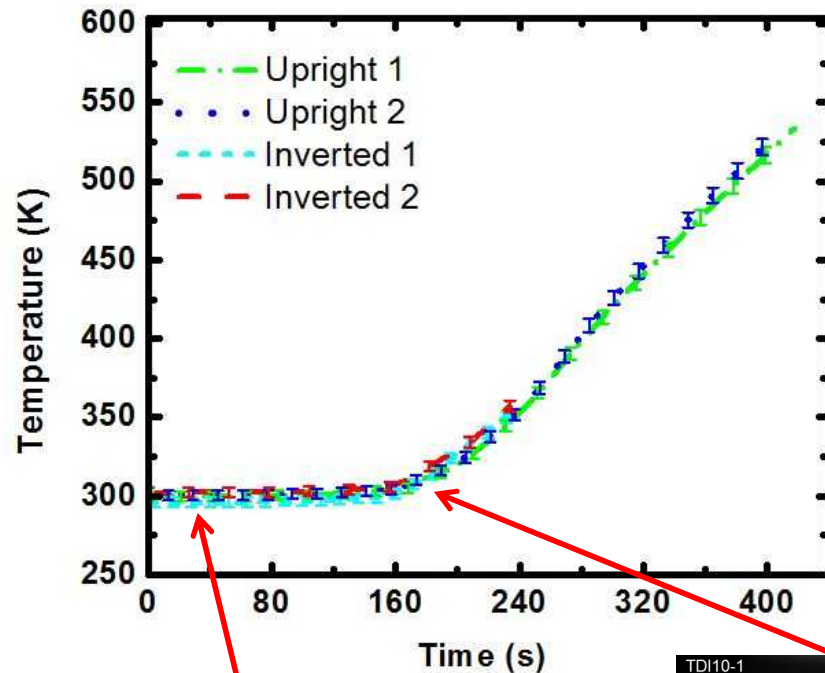


X-ray Frame Difference

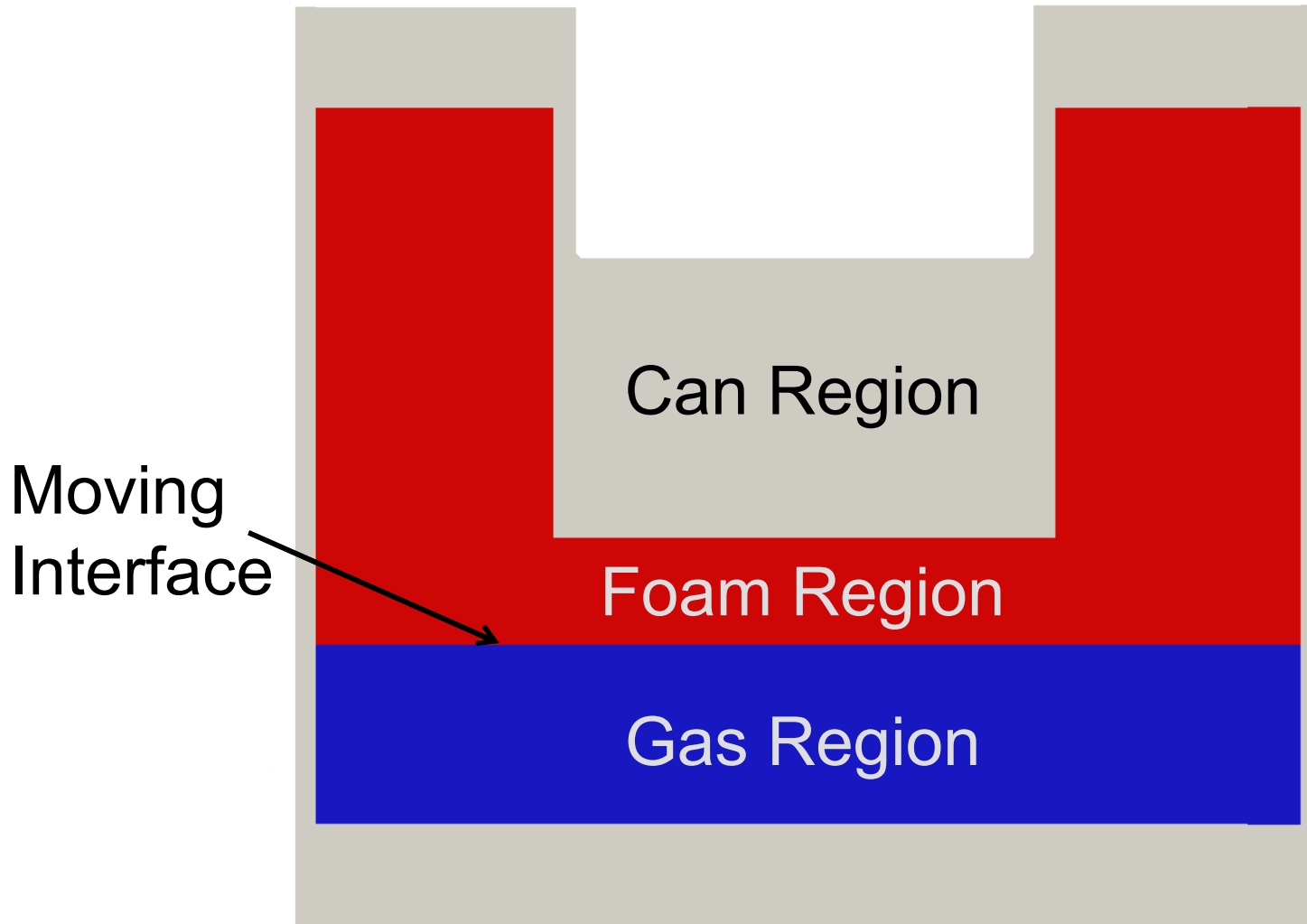


Upright 160 kg/m^3 TDI polyurethane foam
Heated at $150^\circ\text{C}/\text{minute}$

Orientation and Front Regression Important for Pressure and Temperature Response



Model Domain Split Into 3 Regions



Modeled Physics

■ Gas Region

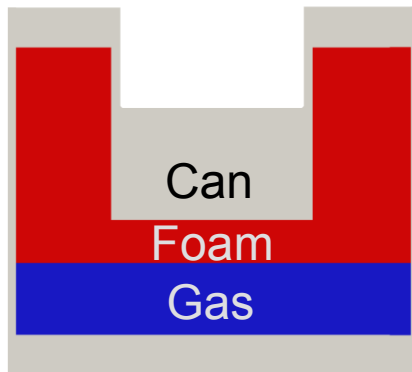
- Continuity
- Momentum
- Species
- Energy
- Enclosure radiation

■ Can Region

- Energy

■ Foam Region

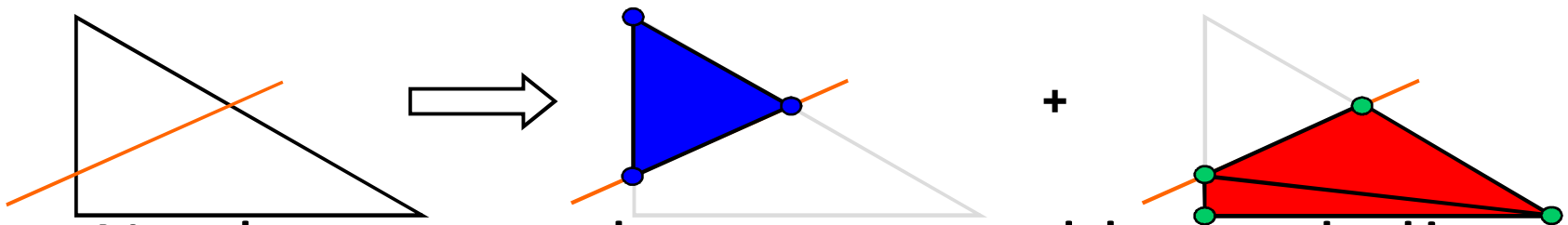
- Gas Phase
- Darcy Mass Balance
- Species
- Energy
- Solid Phase
- Energy
- Mass balance
- Species



- All solved using SIERRA Multiphysics Module – Aria, implicit finite element code.
- Gas region uses control volume finite element method (CVFEM), remainder is Galerkin FEM.

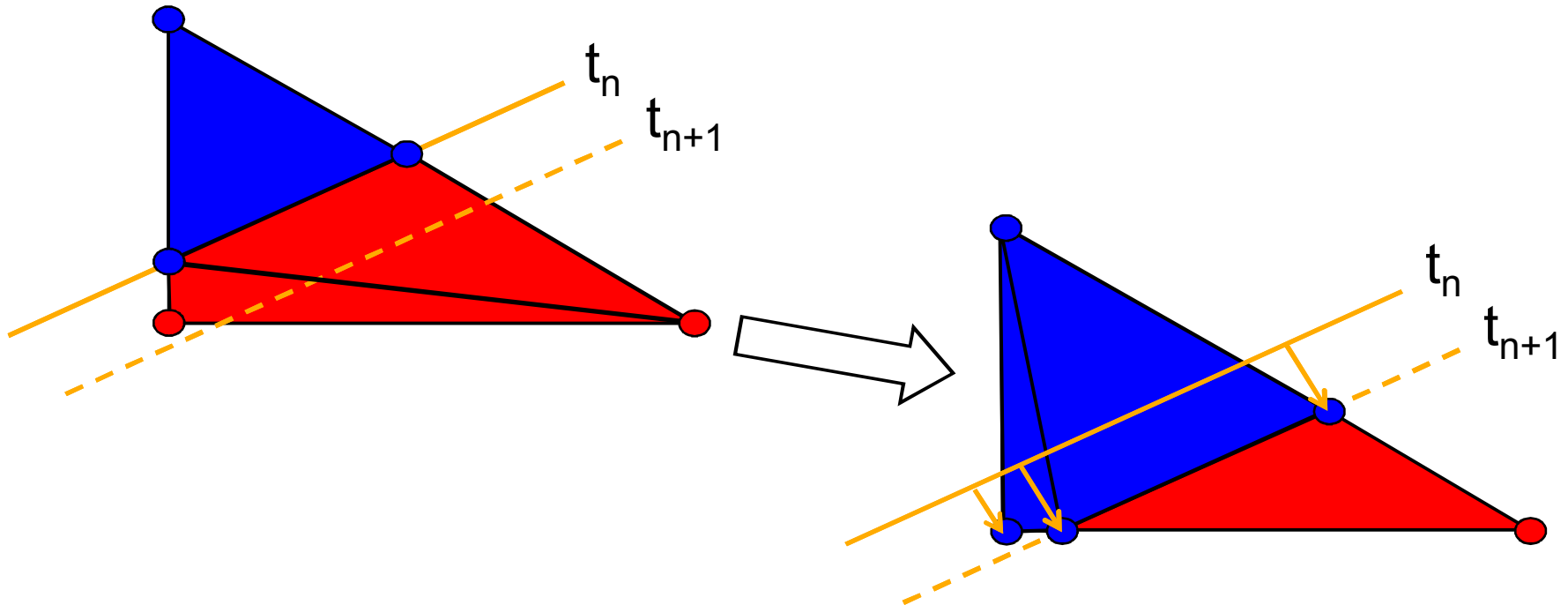
Interface Motion

- Conformal Decomposition Finite Element Method (CDFEM)¹



- No changes to element assembly needed!
- Supports different physics on either side of interface.
- Convert **Foam** -> **Gas** as it decomposes
 - Interface tracks 99% mass fraction isosurface of decomposition product

A note on prolongation



- At each time step newly created nodes and nodes that have moved or changed phase prolong their field values from the nearest interface location at the last time step.
- Time derivatives are adjusted appropriately using an ALE approach.¹

How can we solve this robustly and efficiently?

1. Fully monolithic Newton iteration

- Excellent nonlinear convergence... if linear solves are successful
- Poor scalability

2. Segregated solution scheme

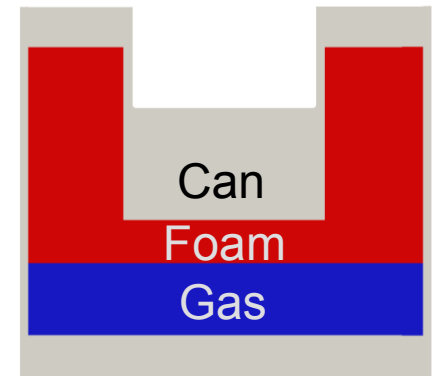
- How to split up equations?
- Smaller matrices with fewer off-diagonal terms
- Nonlinear convergence more challenging – Lots of trial + error to find usable set of equation systems

Segregated Solution Scheme

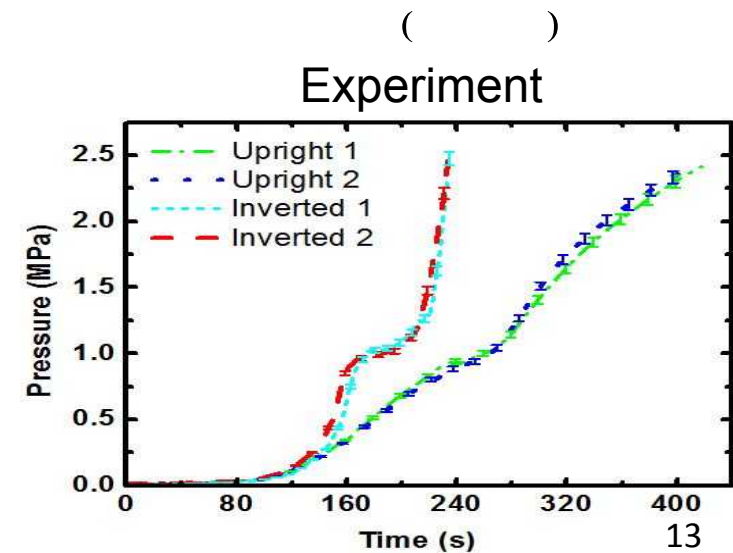
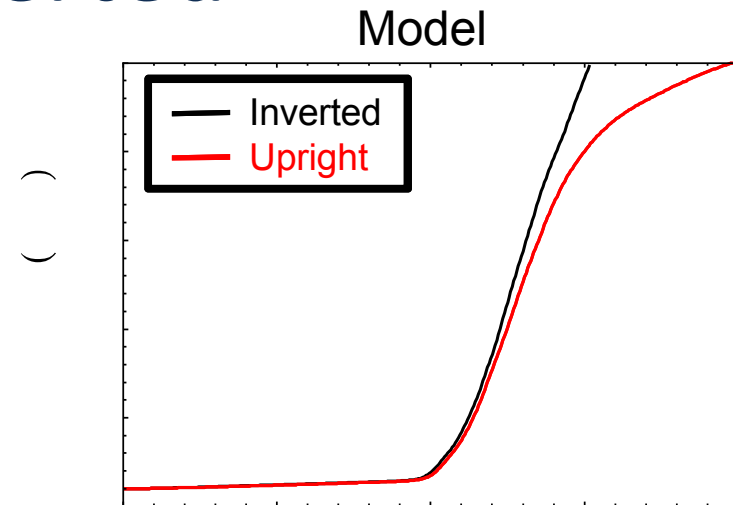
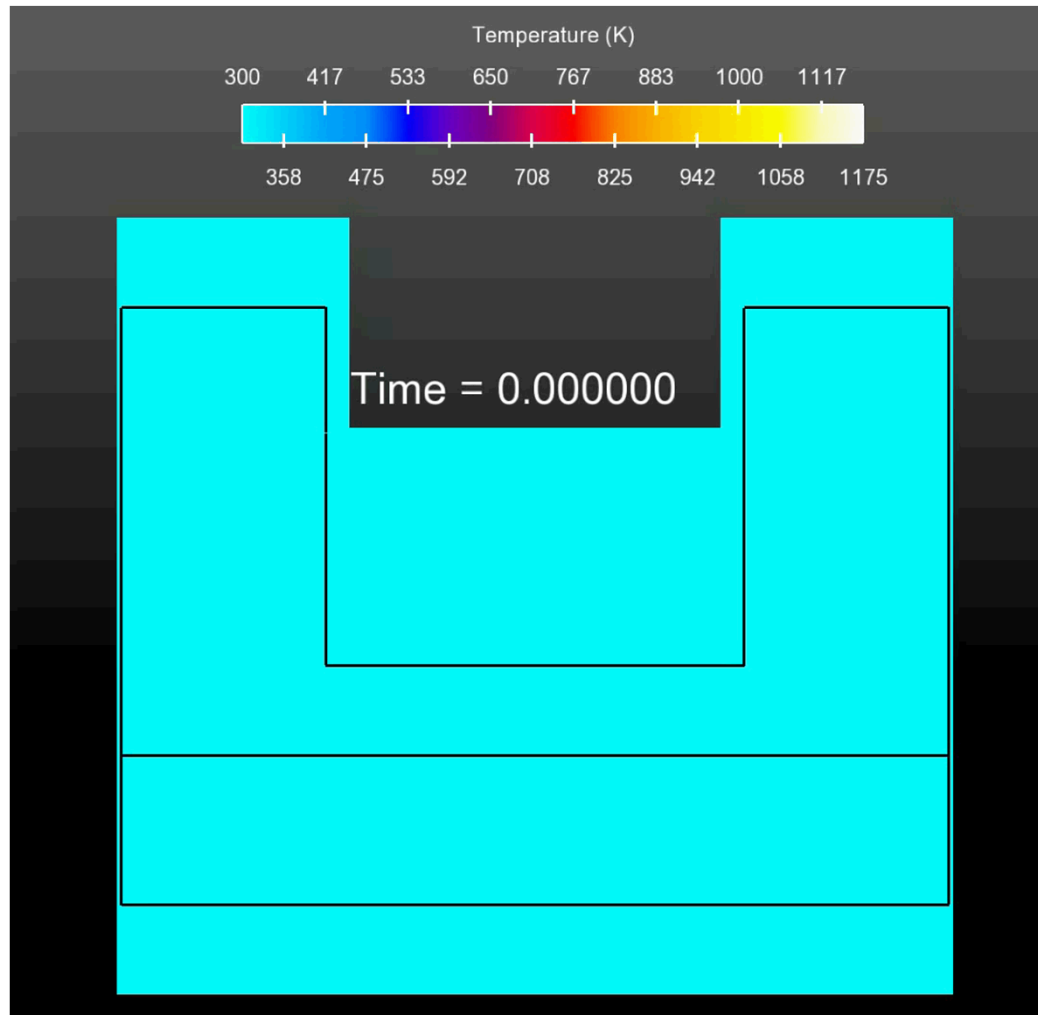
- Interface moves at the start of each time step

5 equation systems:

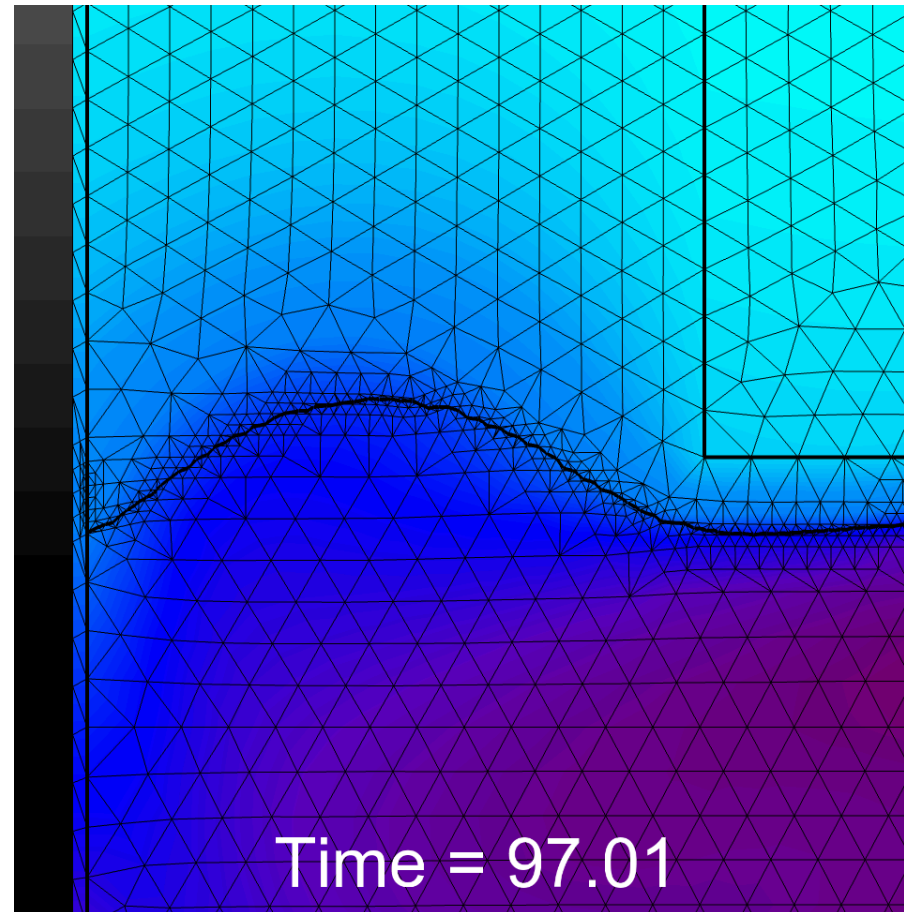
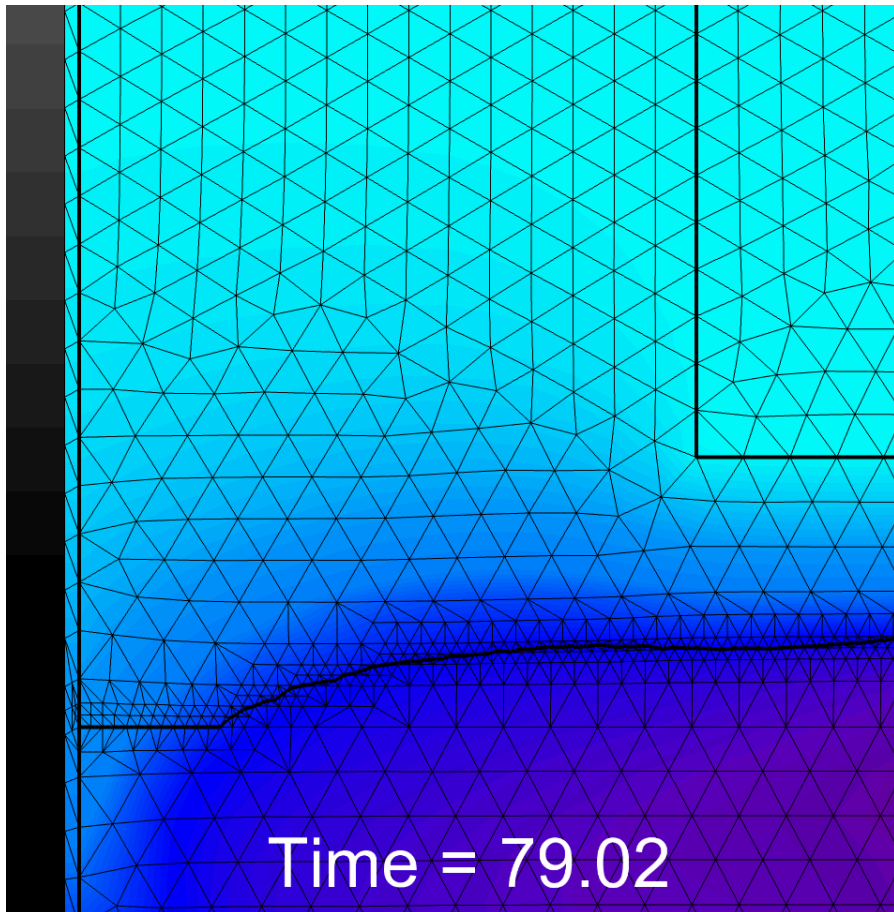
1. Solid Phase Mass Balance and Species
 2. Continuity, Momentum, Darcy Mass Balance
 3. Energy, Gas Phase Energy, Solid Phase Energy, Enclosure Radiation
 4. Energy
 5. Species, Gas Phase Species
- Loop until all equation system residuals $<$ tolerance
 - Run 1-3 Newton iterations per equation system in each outer iteration.
 - Essential to use same gas density from solution of 2 in solution of 3, 5.



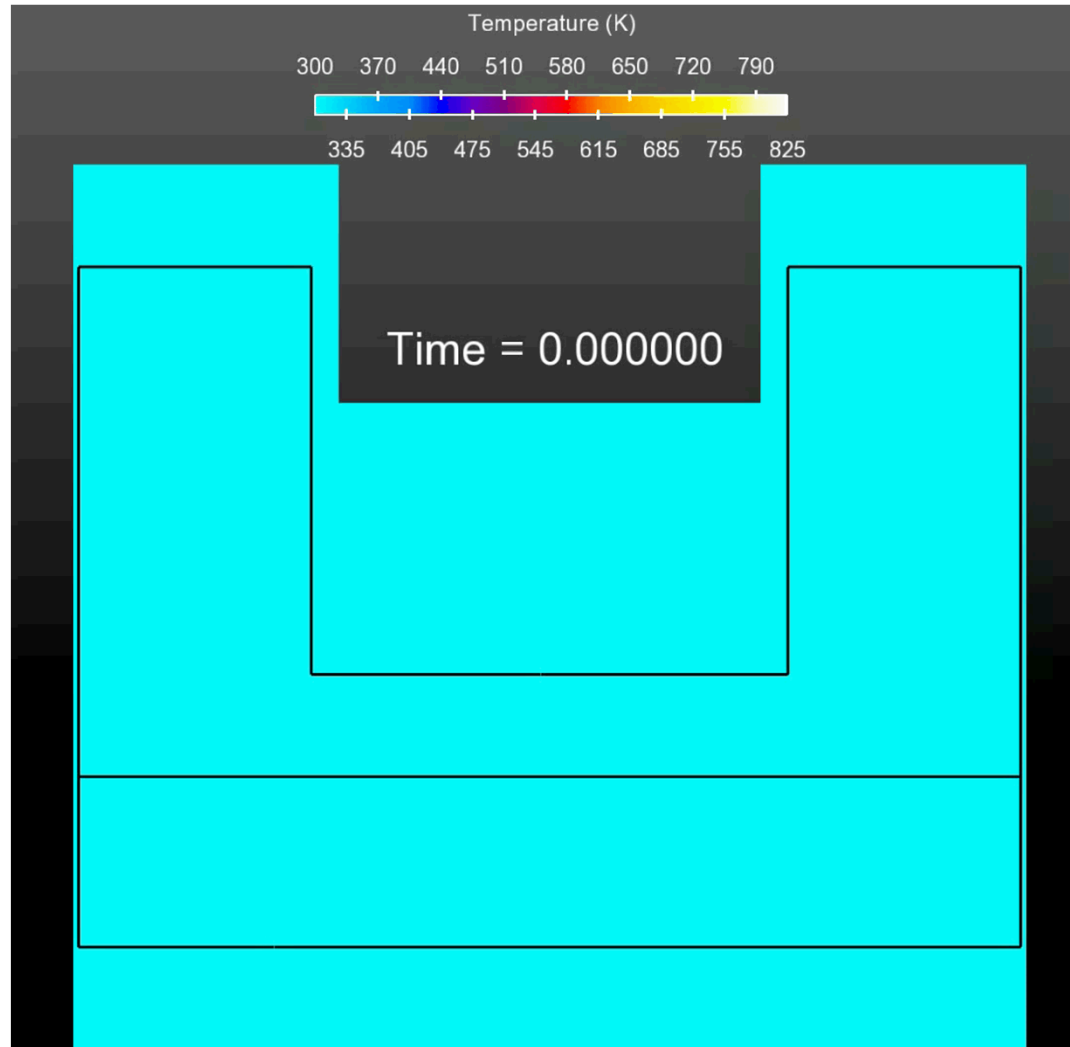
Model Captures Pressure Difference Between Upright and Inverted



Adaptivity Improves Interface Decomposition



Adaptivity Improves Interface Decomposition

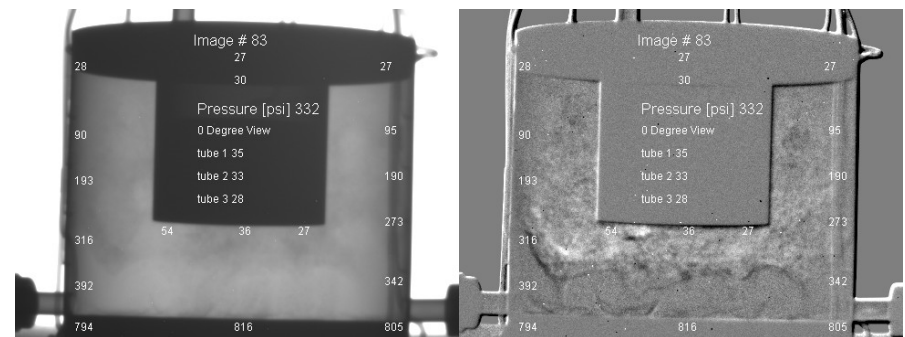
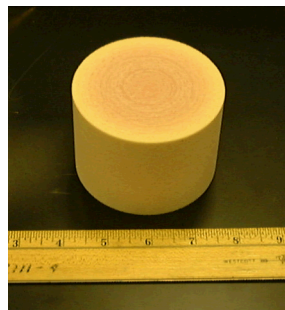
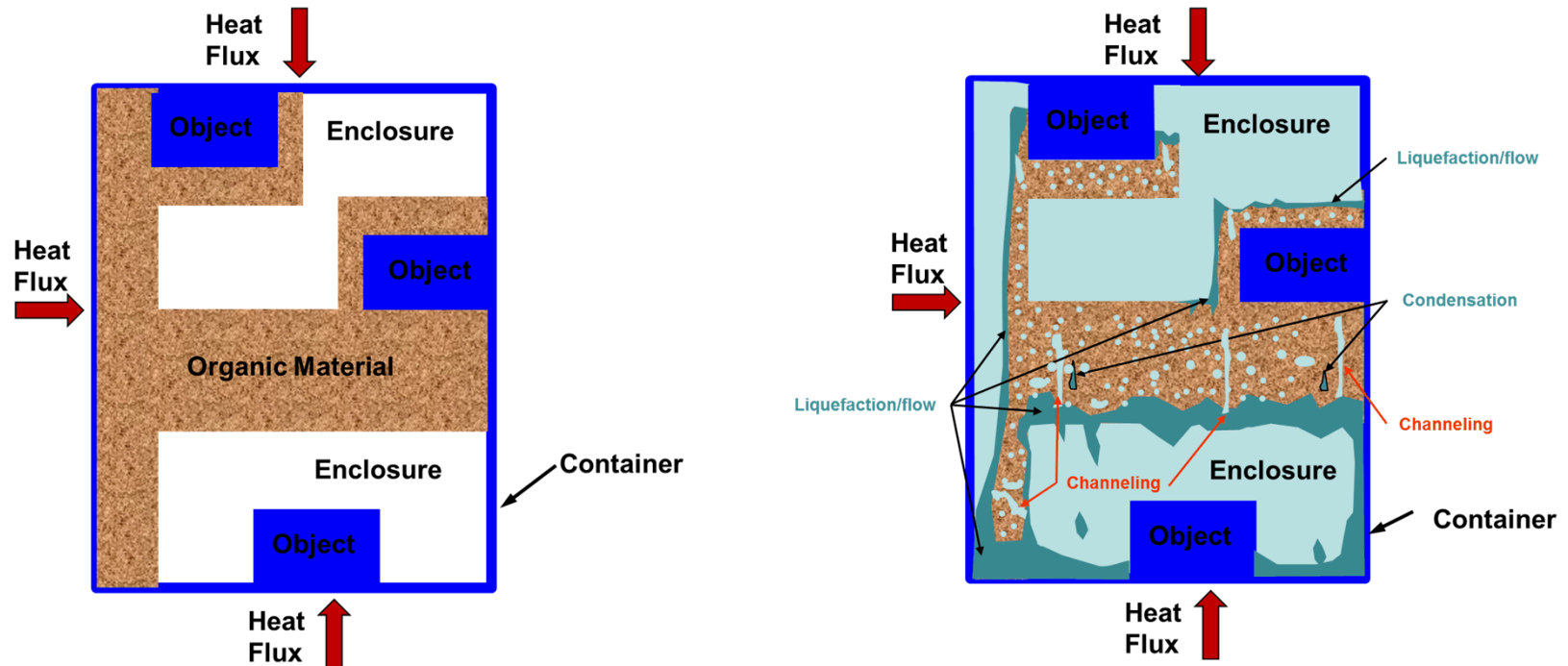


Conclusions and Future Work

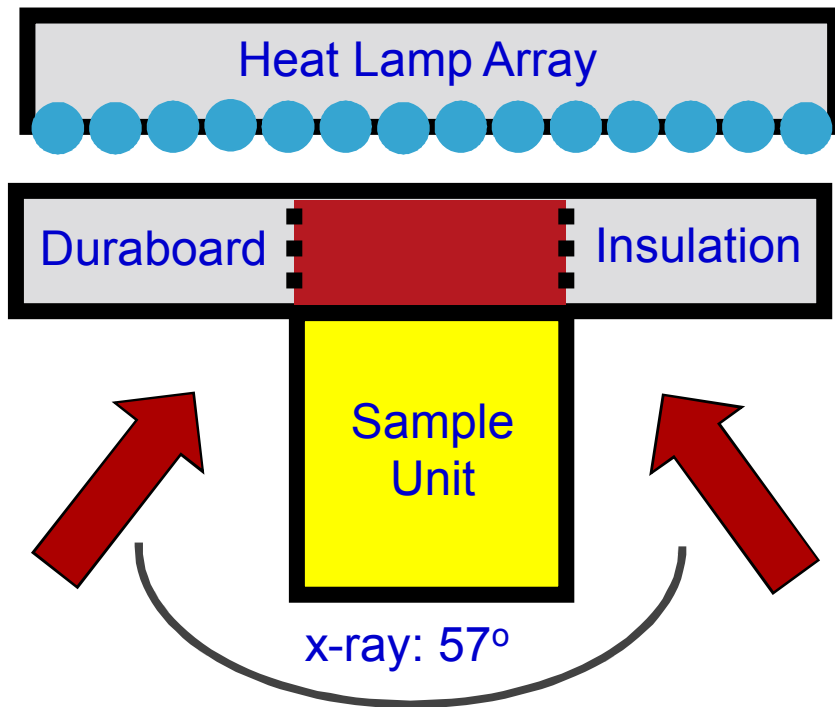
- CDFEM is attractive for interface capturing in multiphysics simulations
 - Different equations/fields on either side of interface
 - Standard element and boundary condition assembly everywhere
- 3D
- Adaptivity robustness
- Incorporating liquefaction and flow of foam.

Backup Slides

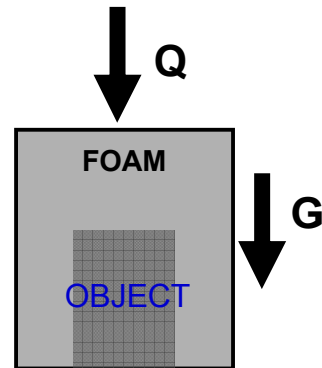
Modeling Heat Transfer to Components and Pressurization in Dynamic Geometries



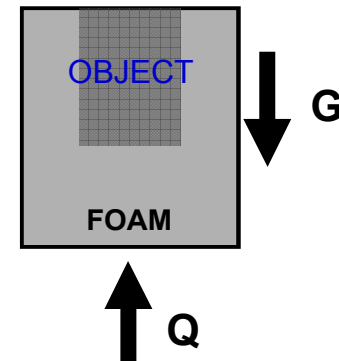
FIC Experimental Setup



Experiments Repeated in Different Orientations



Upright – 0°

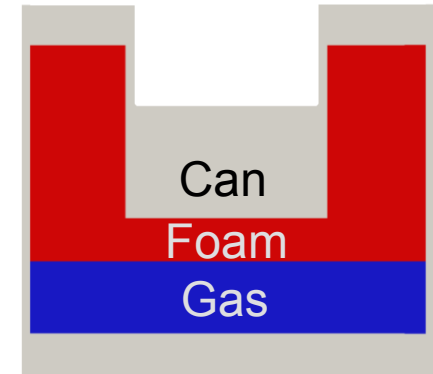


Inverted – 180°



Coupled Heat Transfer Between Foam and Can

- **Foam**-Can Interface
 - Heat transfer between can and both solid and gas phases



Foam

$$T_{\text{solid}} = T_{\text{can}}$$

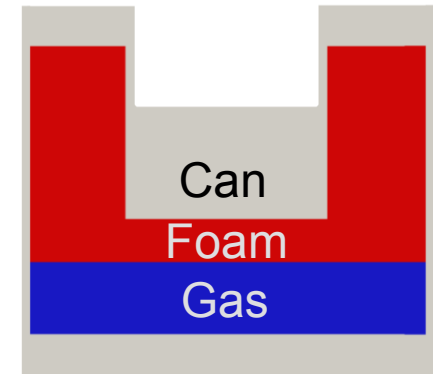
$$T_{\text{gas}} = T_{\text{can}}$$

Can

$$\vec{q} \cdot \hat{n} = (\vec{q}_{\text{solid}} + \vec{q}_{\text{gas}}) \cdot \hat{n} + \alpha(T_{\text{can}} - T_{\text{solid}})$$

Coupled Heat Transfer Between Gas and Can

- Gas-Can Interface
 - Heat transfer between gas and can



Gas

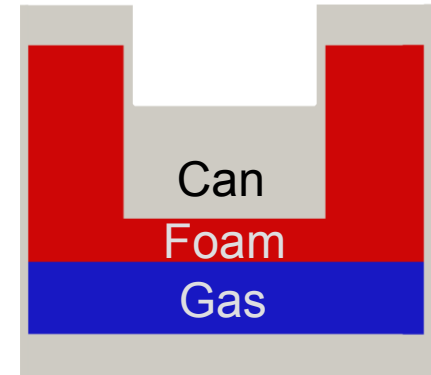
$$T_{\text{gas}} = T_{\text{can}}$$

Can

$$\vec{q}_{\text{can}} \cdot \hat{n} = \vec{q}_{\text{gas}} \cdot \hat{n} + \alpha(T_{\text{can}} - T_{\text{gas}})$$

Coupled Flow Between Foam and Gas

- **Foam-Gas** Interface
 - Coupled gas flow, species transport, and energy transport



Gas

$$\vec{J}_{\text{gas}} \cdot \hat{n} = \vec{J}_{\text{gas}}^{\text{foam}} \cdot \hat{n}$$

$$+ \alpha(X_{\text{gas}} - X_{\text{foam}})$$

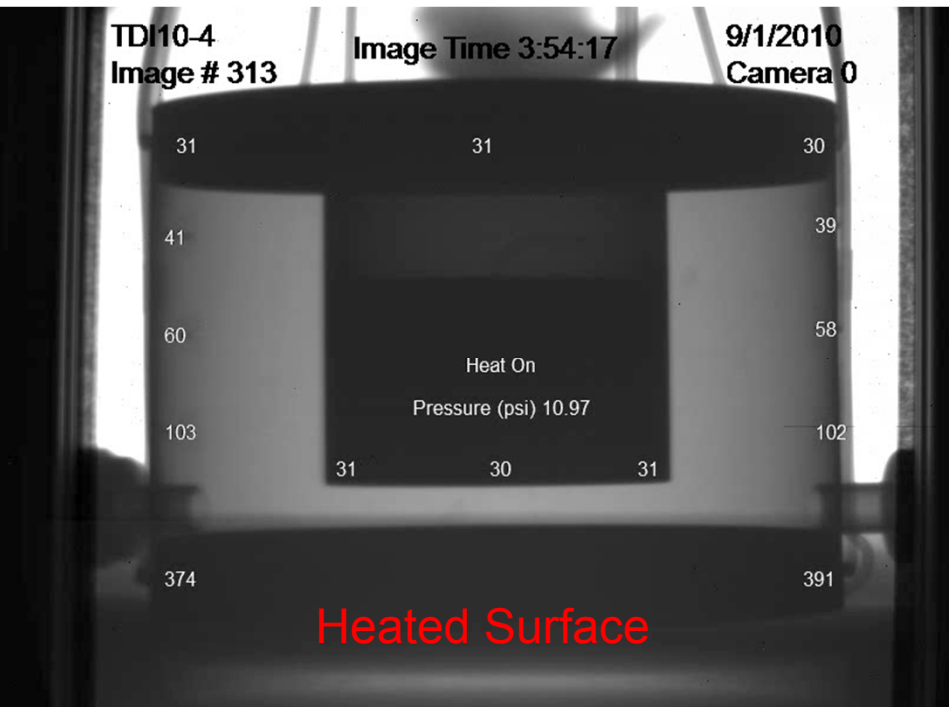
Foam

$$\vec{J}_{\text{gas}}^{\text{foam}} \cdot \hat{n} = \vec{J}_{\text{gas}} \cdot \hat{n}$$

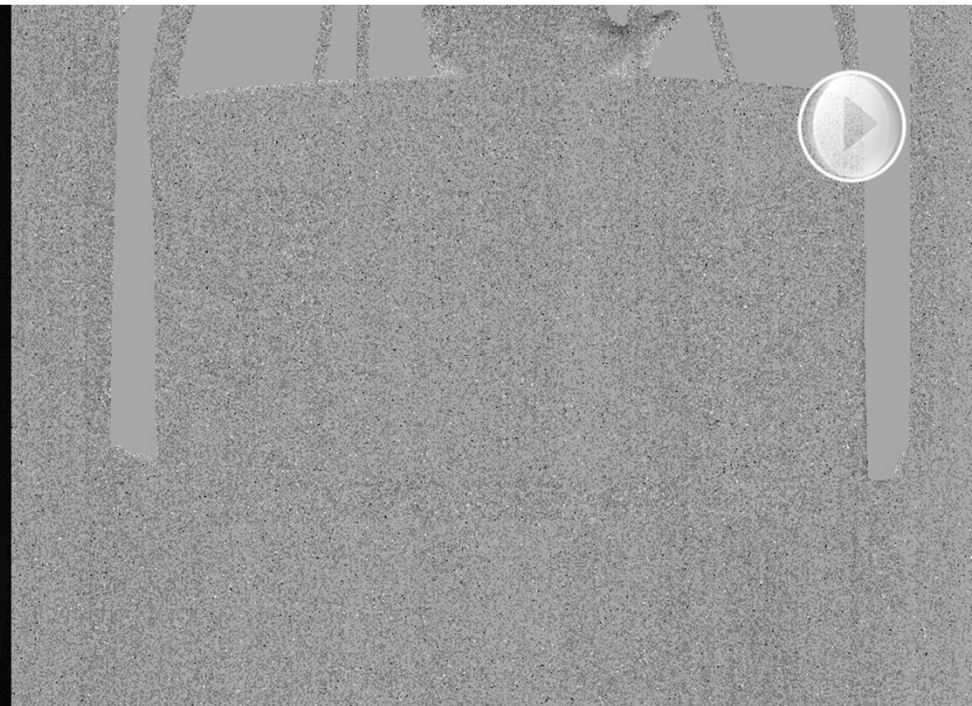
$$+ \alpha(X_{\text{foam}} - X_{\text{gas}})$$

X-ray Video Captures Foam Decomposition Front

X-ray



X-ray Frame Difference



Inverted 160 kg/m³ TDI polyurethane foam
Heated at 150C/minute

Decomposition Front Motion Controls Radiative Heat Transport

