

# **Evaluation of Complete and Incomplete Mixing Models in Water Distribution Pipe Network Simulations**

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# Overview

- **Introduction**
- **Experimental Approach**
- **Modeling Approach**
- **Results**
- **Conclusions**



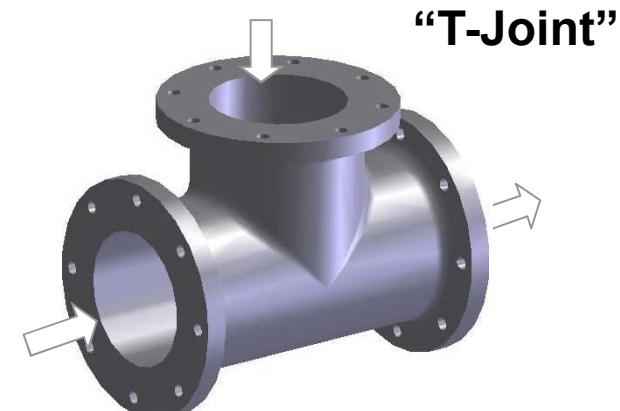
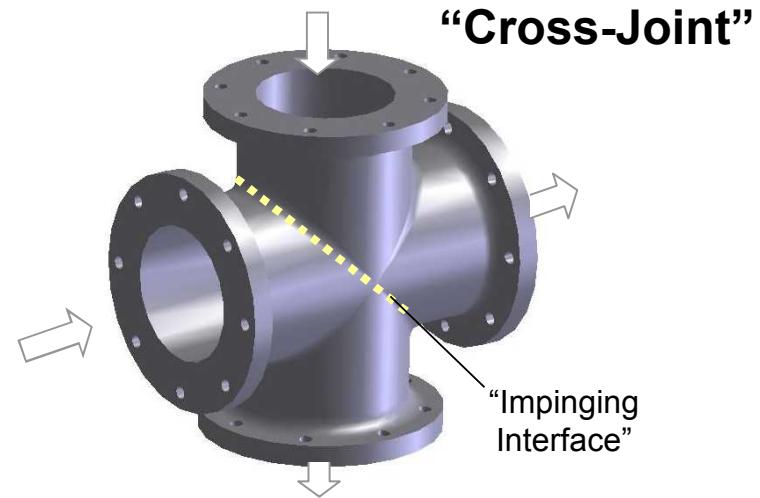
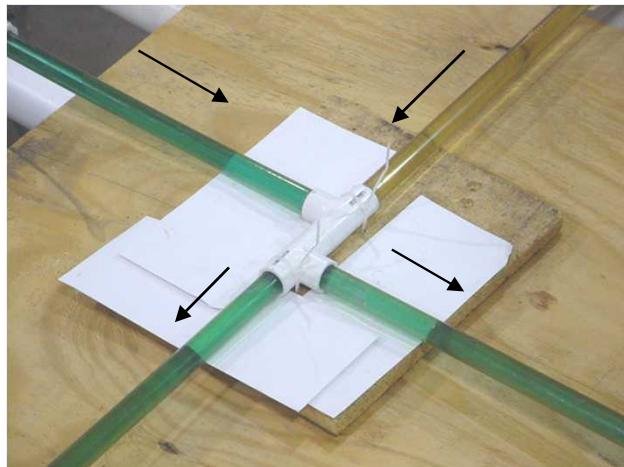
# Introduction

- **Contaminant transport in water-distribution pipe networks is a growing concern**
  - Need to understand and predict contaminant movement and mixing in junctions
  - Many network models assume complete mixing at junctions
- **Previous studies have shown incomplete mixing in pipe junctions (experimental and computational)**
  - van Bloemen Waanders et al. (2005)
  - O'rear et al. (2005)
  - Ho et al. (2006)
  - Romero-Gomez et al. (2006)
  - Webb and van Bloemen Waanders (2006)



# Objective

- Determine impact of incomplete mixing at individual junctions on network of junctions
- Determine conditions when complete mixing is valid





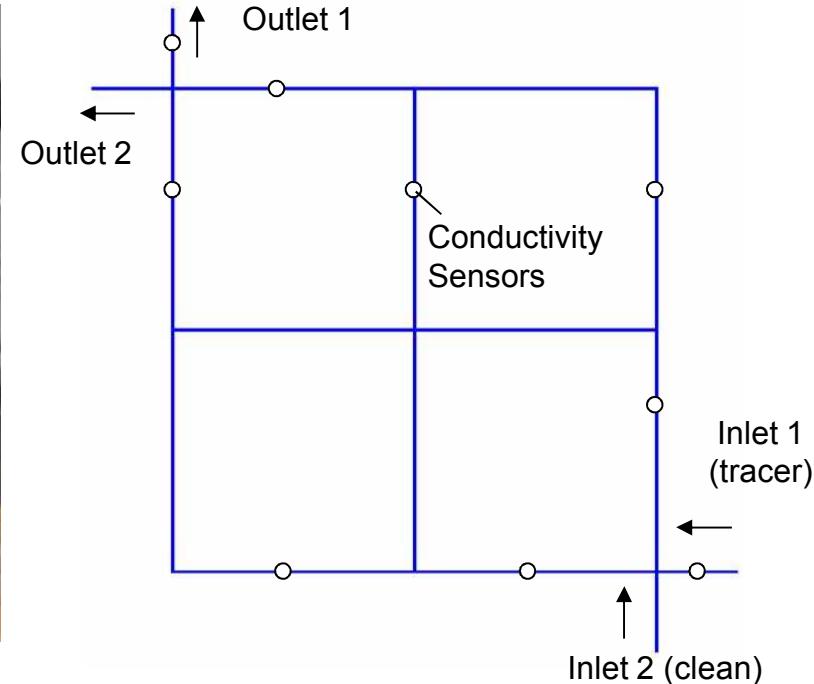
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# Small-Scale Network Tests

(O'rear et al., 2005)



- 3x3 array of cross joints with 3-foot pipe lengths
- Flow rates at inlets and outlets controlled
- Pipe diameter: 0.5"

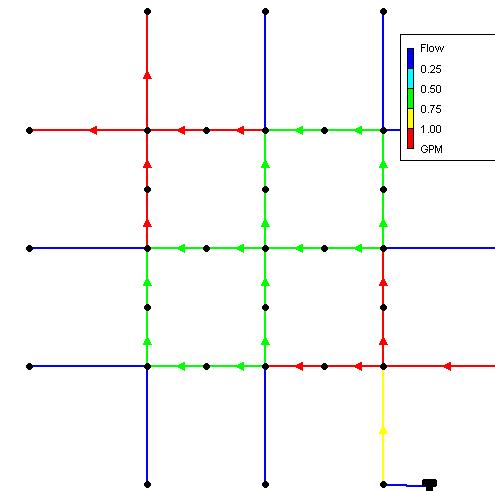
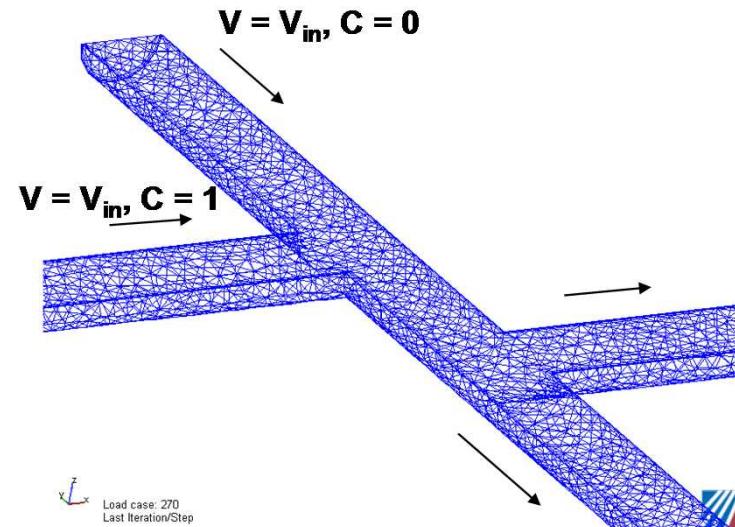


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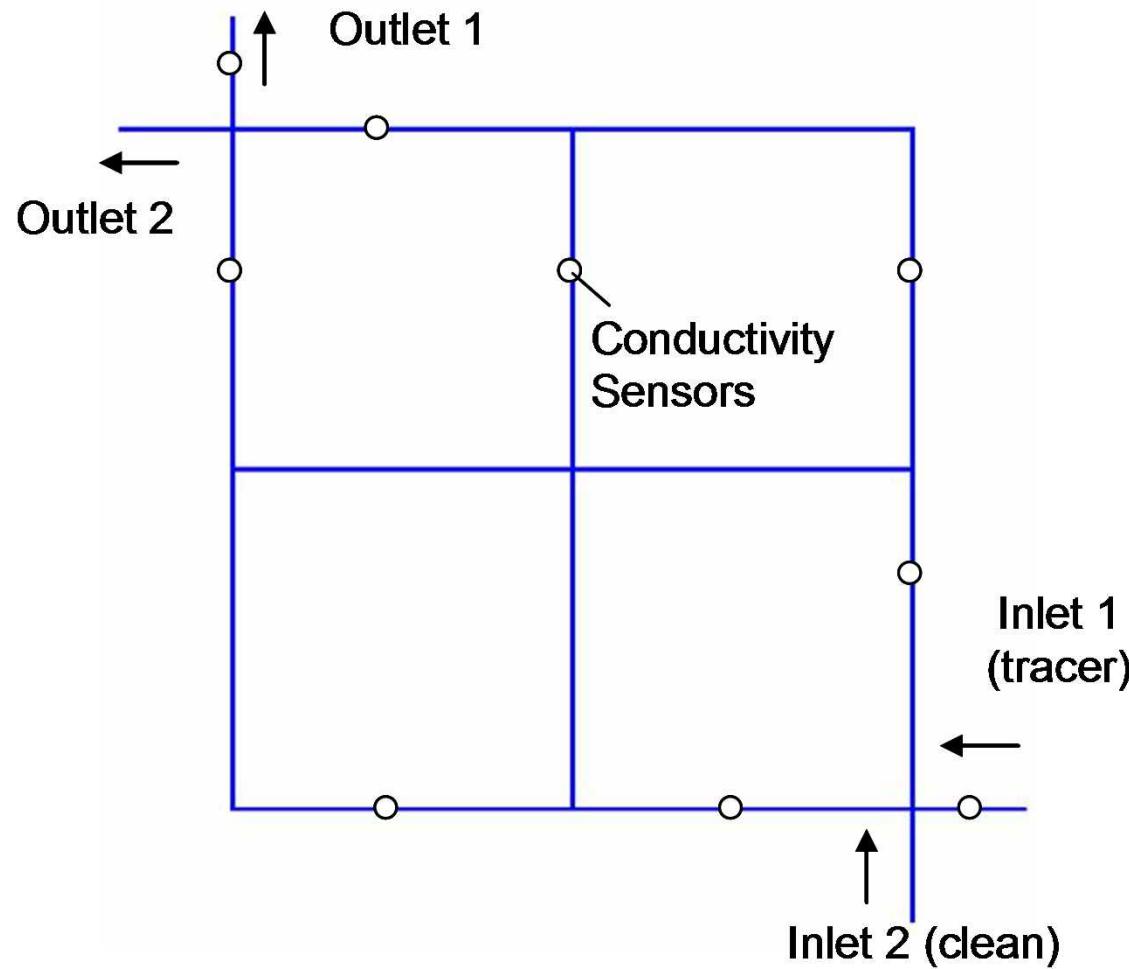
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# Modeling Approach

- Simulate network experiments using different models
  - Finite-element computational fluid dynamics simulations
    - K- $\epsilon$  turbulence model
    - Allows incomplete mixing in junctions
  - EPANET
    - Assumes complete mixing at junctions
    - Modified version developed to allow incomplete mixing based on empirical correlations



# Model Geometry





# Network Simulations

- Two simulations
  - Tracer inlet flow > clean-water inlet flow
  - Tracer inlet flow < clean-water inlet flow

Boundary Conditions (flow rates half actual values due to symmetry employed)				Reynolds Number	Turbulent Schmidt Number
Tracer Inlet Flow ( $Q_{tracer}$ )	Clean Water Inlet Flow ( $Q_{clean}$ )	Outlet 1 Flow ( $Q_{out,1}$ )	Outlet 2 Flow ( $Q_{out,2}$ )		
38 mL/s* (0.61 gpm)	31 mL/s (0.49 gpm) ( $P = 0$ gage used as B.C.)	33 mL/s (0.52 gpm)	37 mL/s (0.58 gpm)	4,000 – 9,000	0.01, 0.001
28 mL/s** (0.44 gpm) ( $P = 0$ gage used as B.C.)	50 mL/s (0.79 gpm)	32 mL/s (0.50 gpm)	46 mL/s (0.73 gpm)	7,000 – 11,000	0.01, 0.001

\*Test period from 19-20 minutes in Orear et al. (2005)

\*\*Test period from 8-9 minutes in Orear et al. (2005)

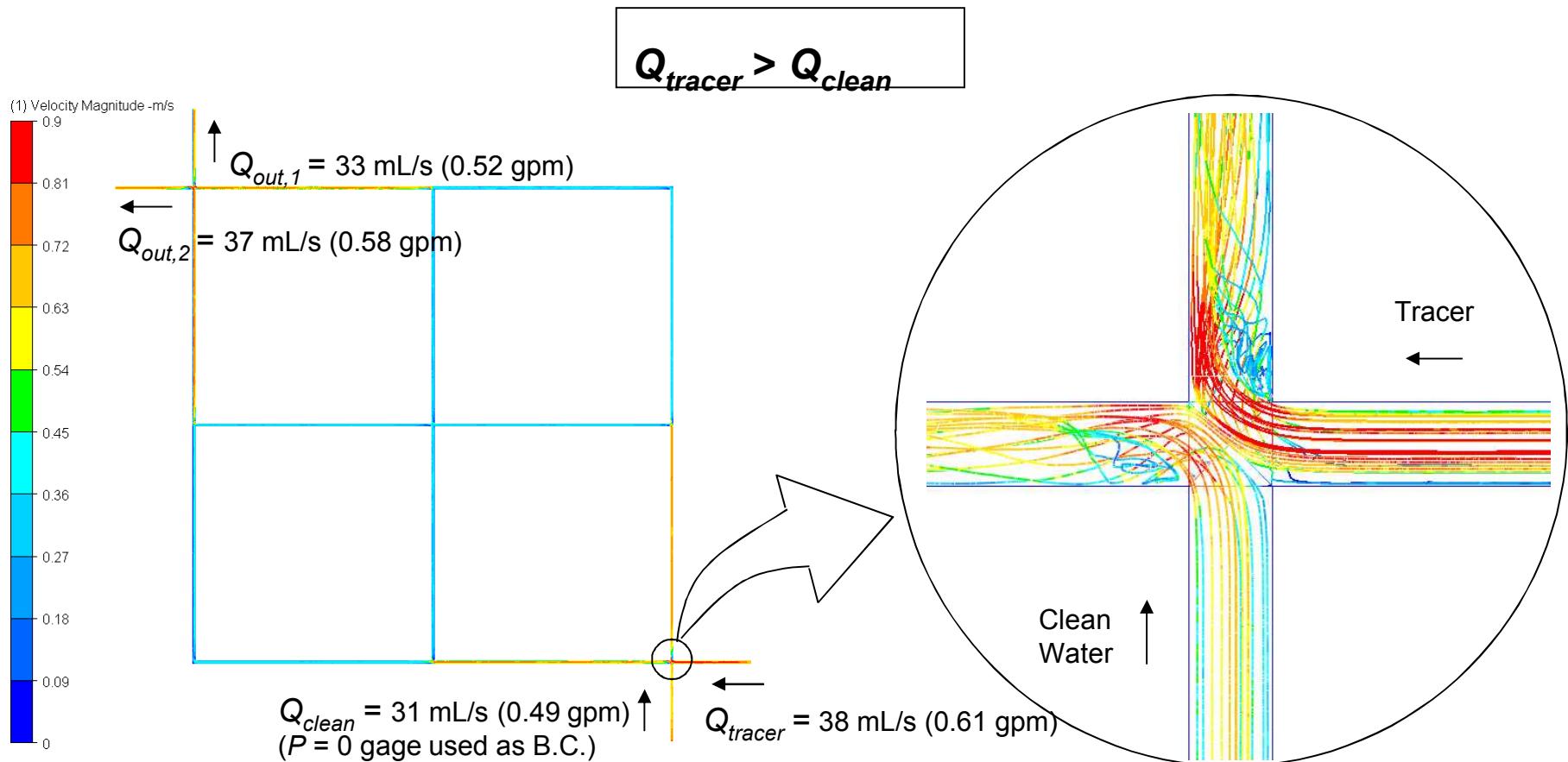


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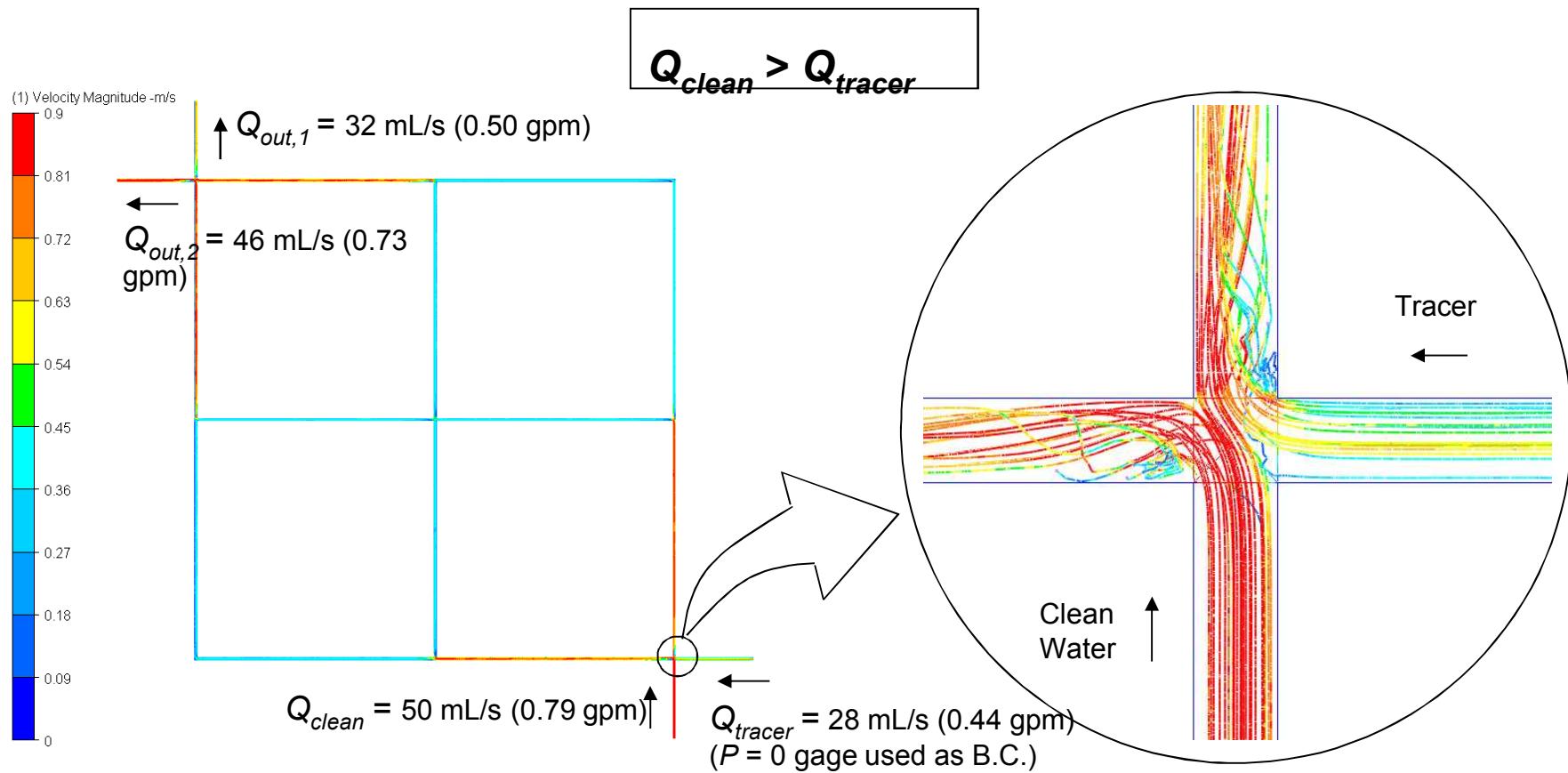
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# CFD Hydraulic Results



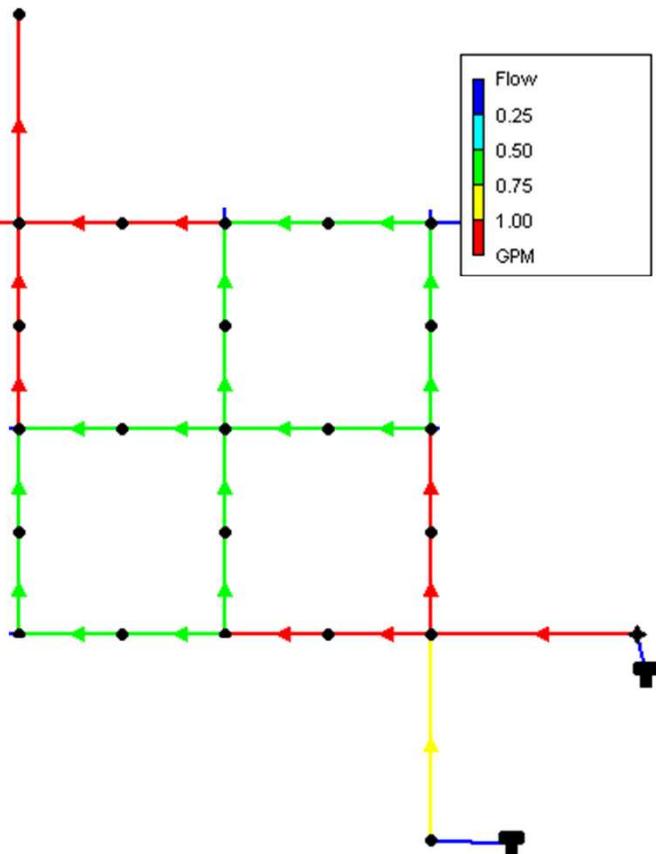
# CFD Hydraulic Results



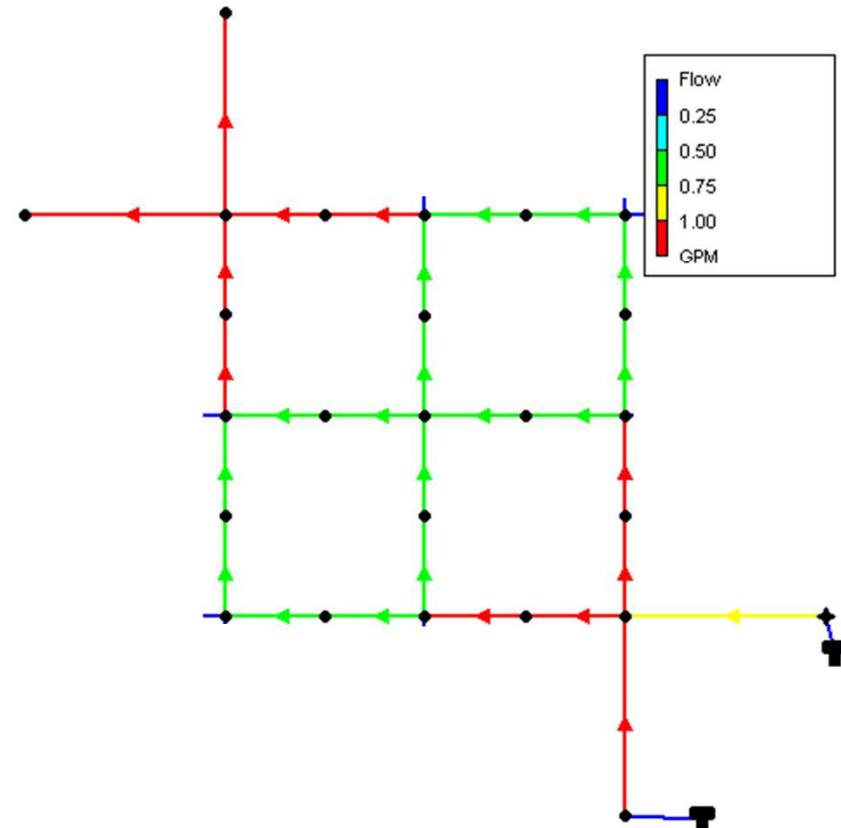


# EPANET Hydraulic Results

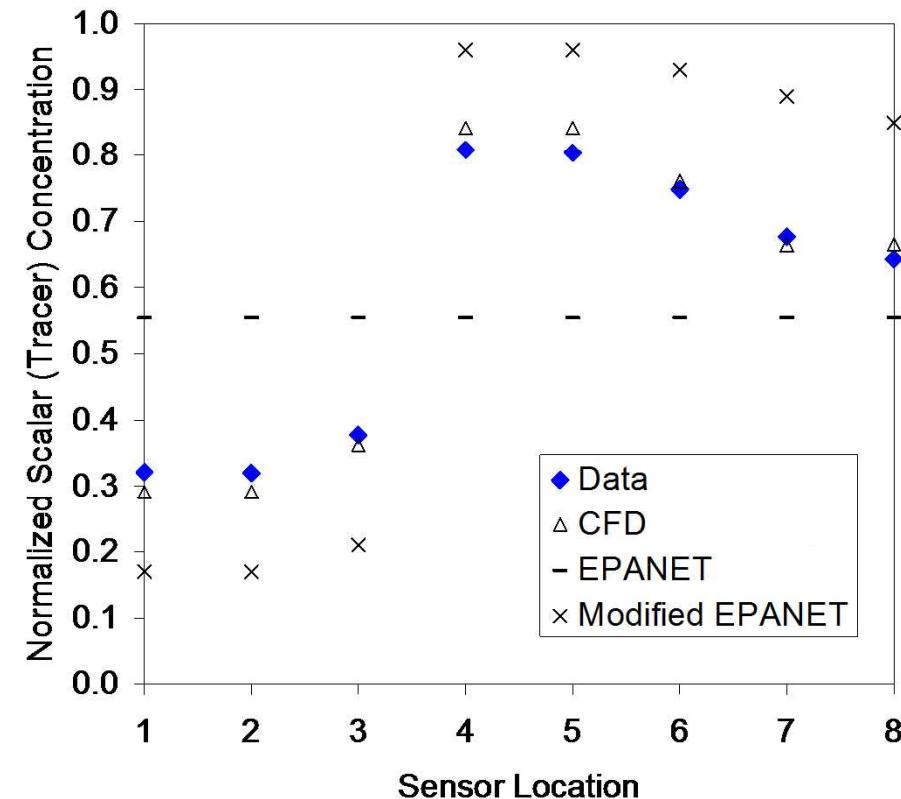
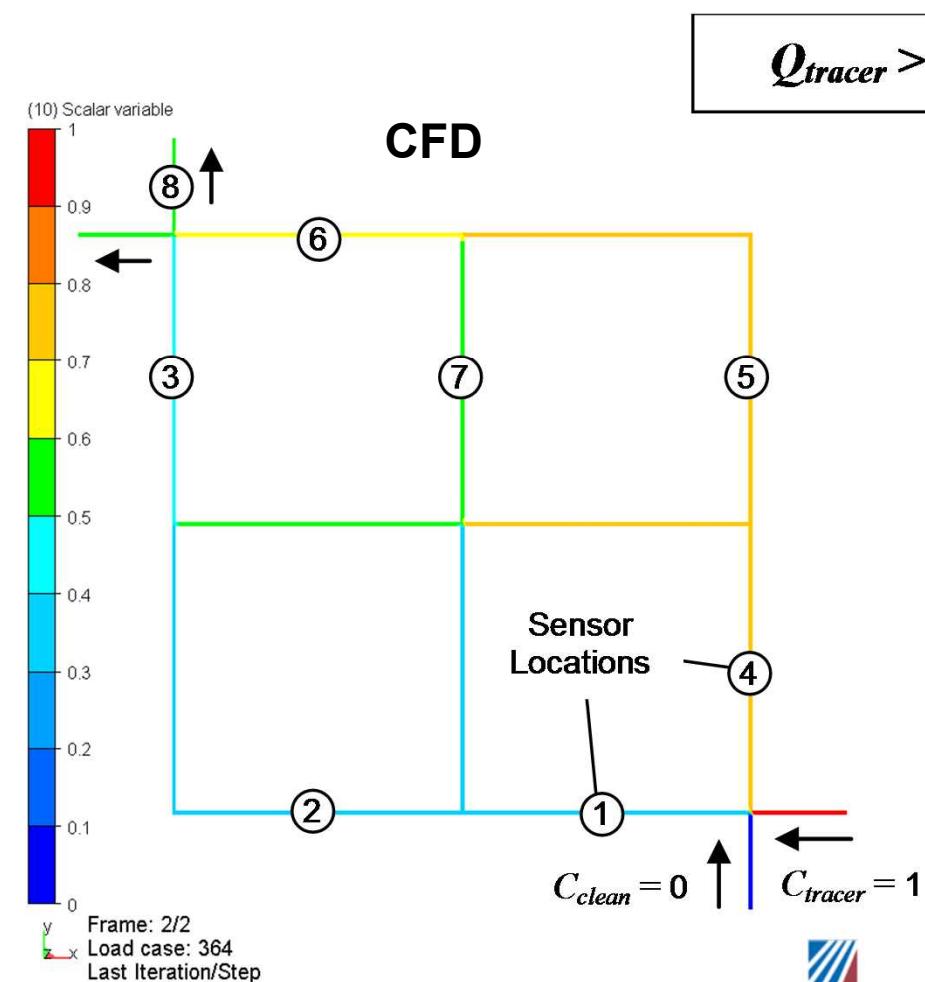
$Q_{tracer} > Q_{clean}$



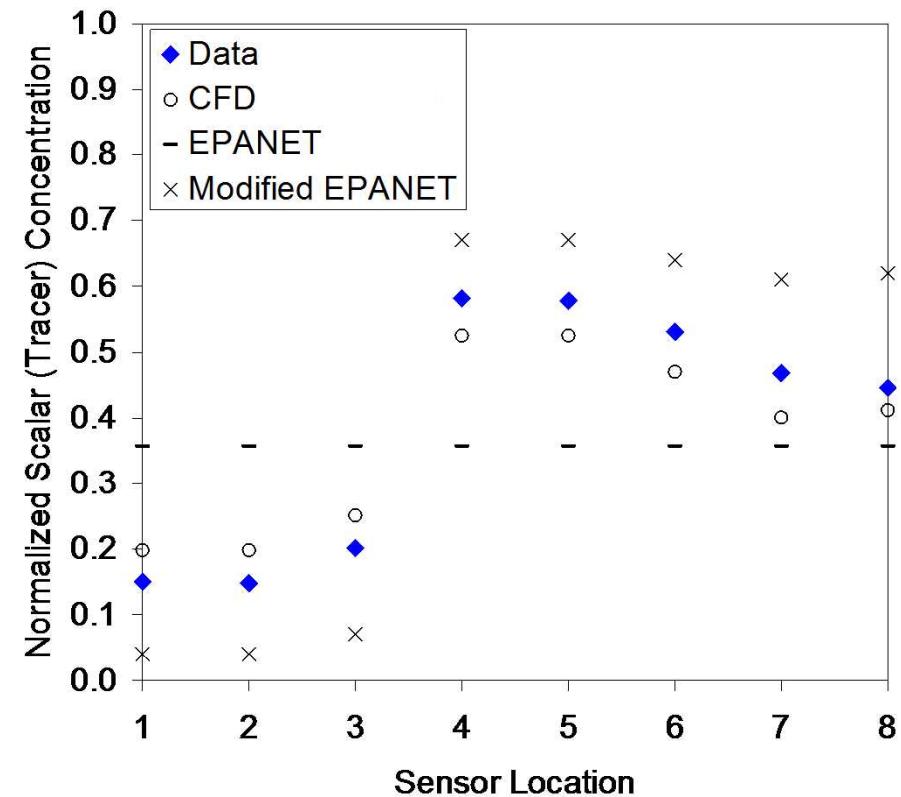
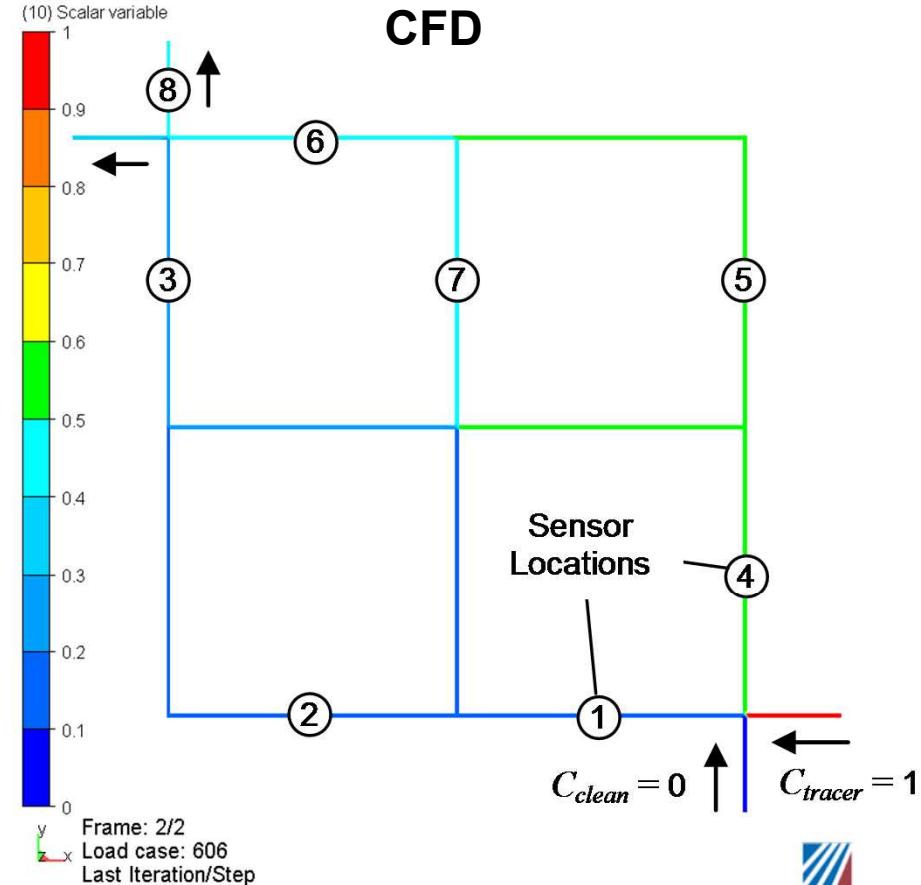
$Q_{clean} > Q_{tracer}$



# Solute Transport Results



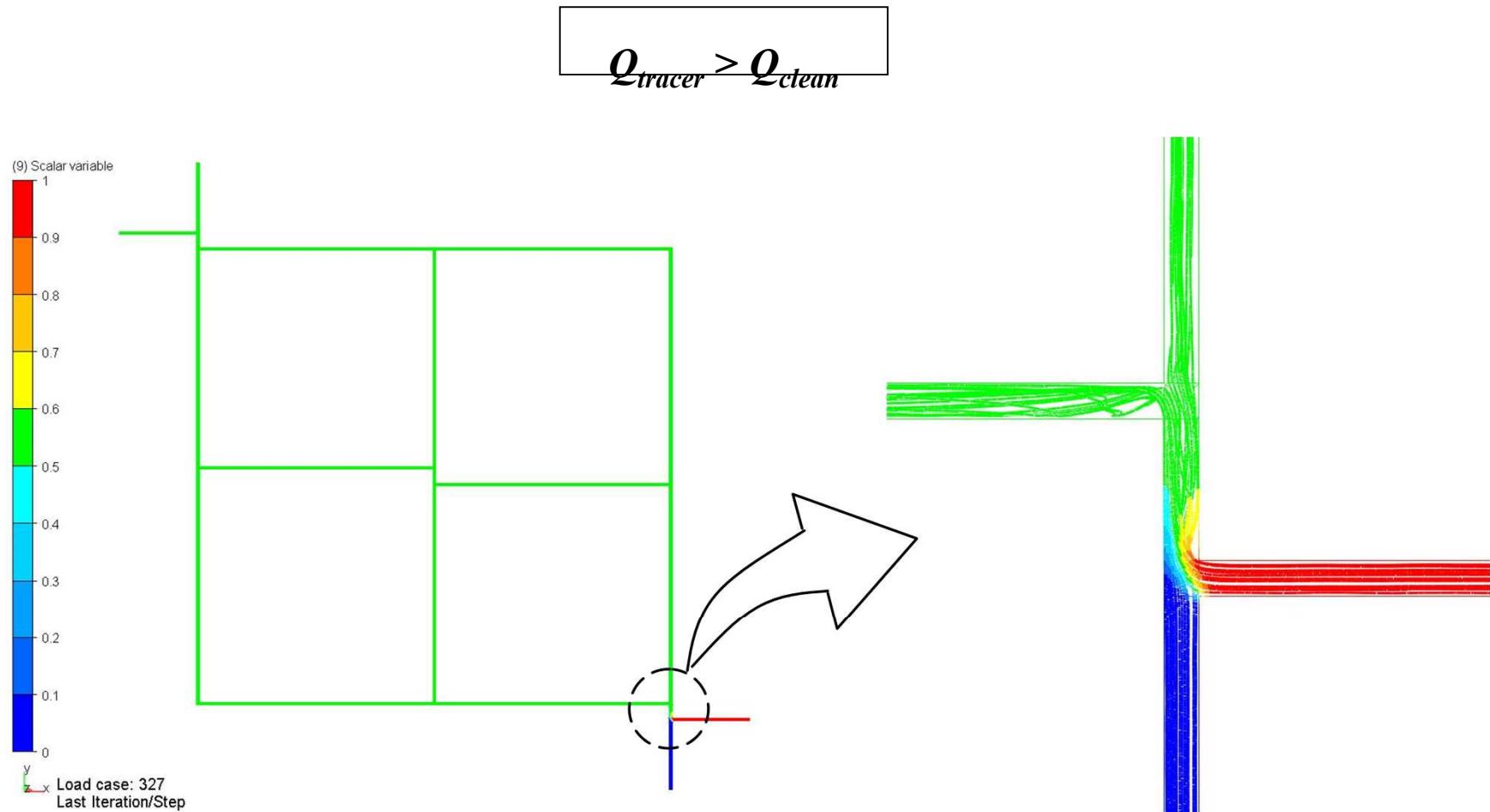
# Solute Transport Results



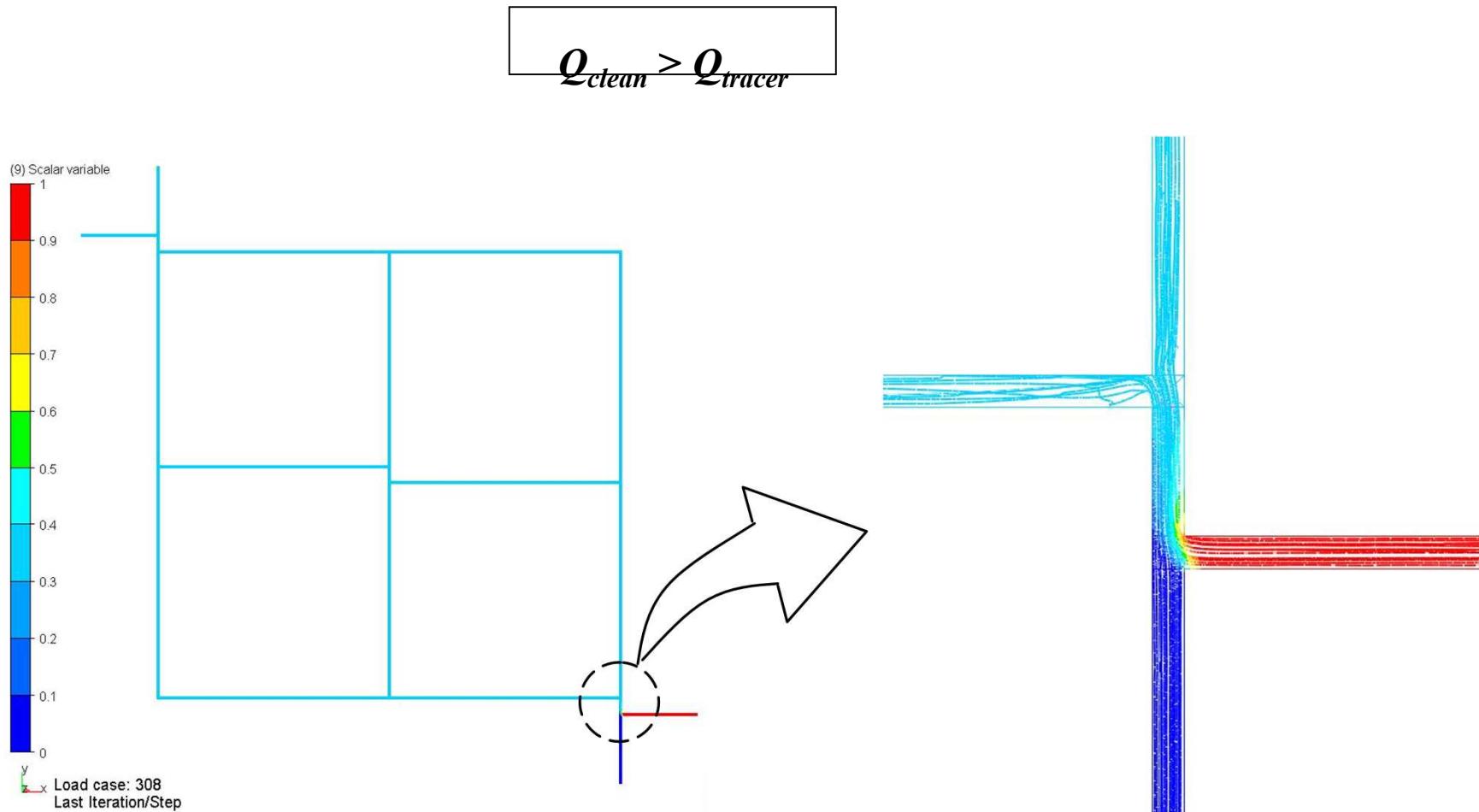


# Is Complete Mixing Ever Valid?

# Double-T Junctions



# Double-T Junctions





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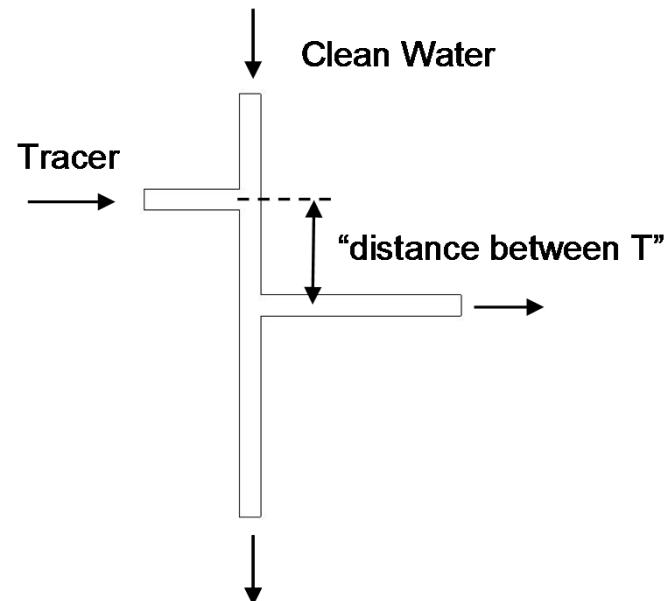
# Conclusions

- Water flow and solute transport in a small-scale network were evaluated experimentally and computationally
  - CFD (allows incomplete mixing at junctions)
  - EPANET (assumes complete mixing at junctions)
  - Modified EPANET (incomplete mixing based on correlations)
- Results with cross junctions resulted in incomplete mixing, even after several consecutive junctions
  - EPANET produced inaccurate results
  - Modified EPANET captured trends in mixing and solute concentration
  - CFD provided good matches with data



# Conclusions (cont.)

- **Simulations with double-T junctions resulted in completely mixed concentrations in the network**
  - Complete mixing is likely to occur in double-T junctions when separated by  $> 5\text{-}10$  pipe diameters





# Next Steps

- **Continue physical and numerical simulations**
  - Evaluate mixing in more complex configurations and networks
  - Evaluate the effects of transient oscillations and storage on mixing in pipe networks
- **Incorporate improved models of mixing into EPANET**

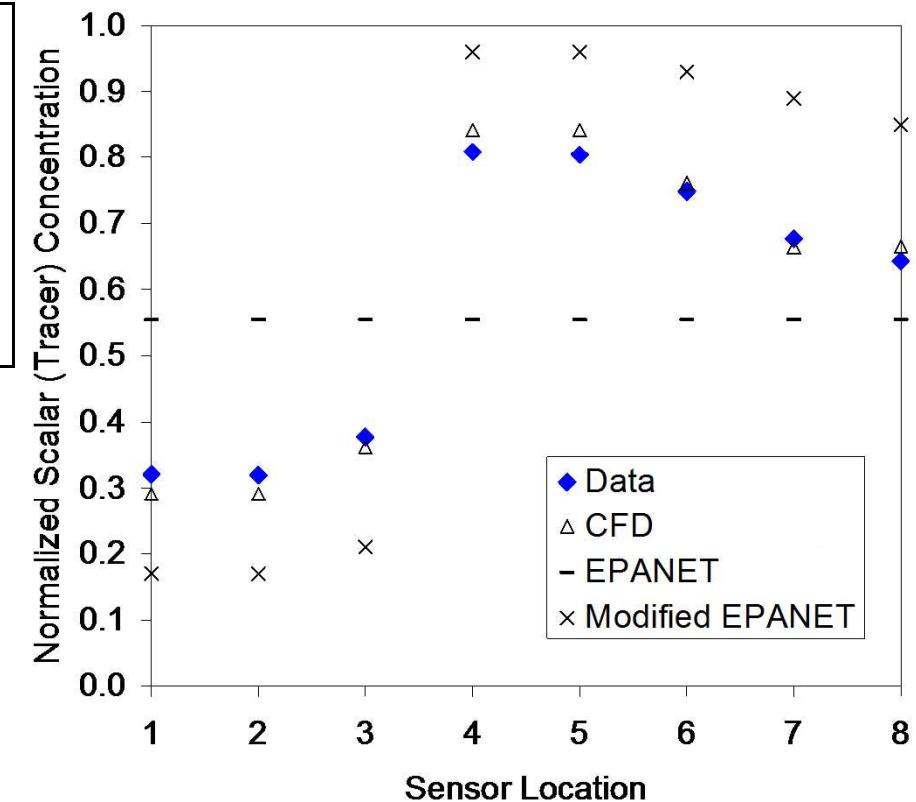
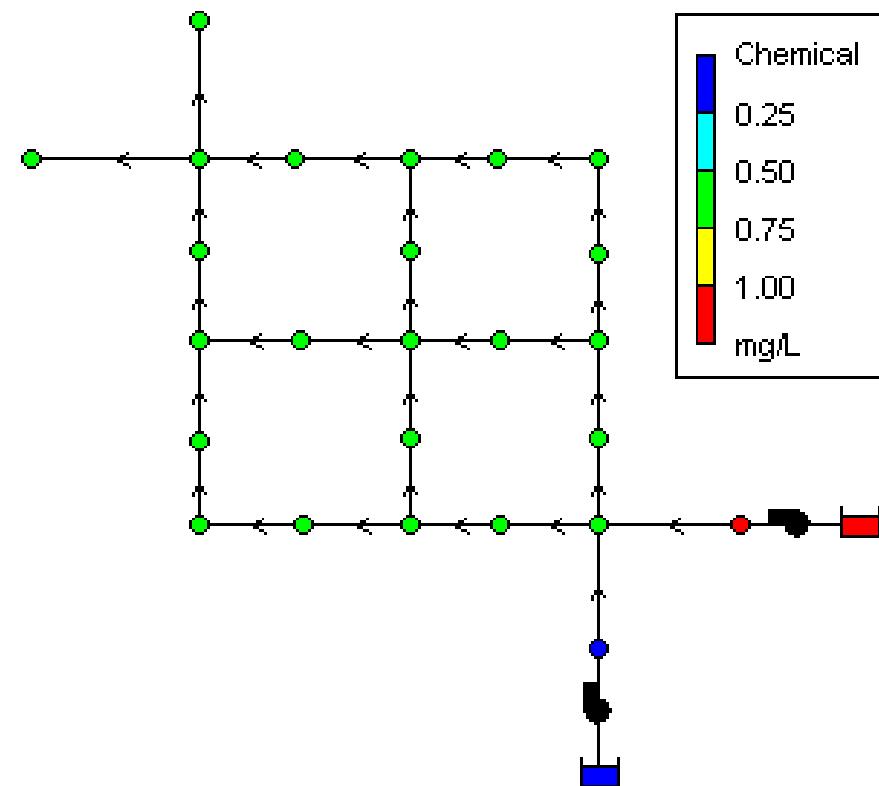


# Backup Slides

# Solute Transport Results

EPANET

$$Q_{tracer} > Q_{clean}$$



# Solute Transport Results

$$Q_{clean} > Q_{tracer}$$

EPANET

