

Towards a Coupled Multiphysics Model of Molten Salt Battery Mechanics

Scott A. Roberts, Kevin N. Long, Jonathan R. Clausen,
Mario J. Martinez, Edward S. Piekos, and Anne M. Grillet

Engineering Sciences Center
Sandia National Laboratories, Albuquerque, NM

sarober@sandia.gov

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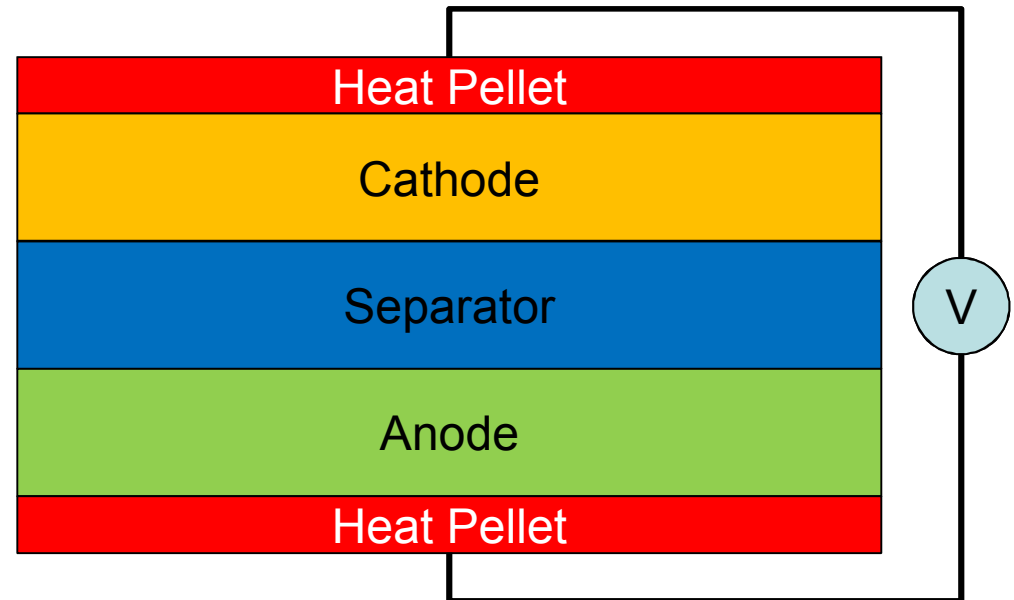
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- Battery activation is a complicated, multi-step process

- Heat pellet burning
- Thermal diffusion
- Melting of the electrolyte
- Deformation of the separator
- Flow of the electrolyte
- Activation

- A true multi-physics problem

- Thermal
- Mechanical
- Fluid
- Electrochemical



- Why performance models of thermal batteries?

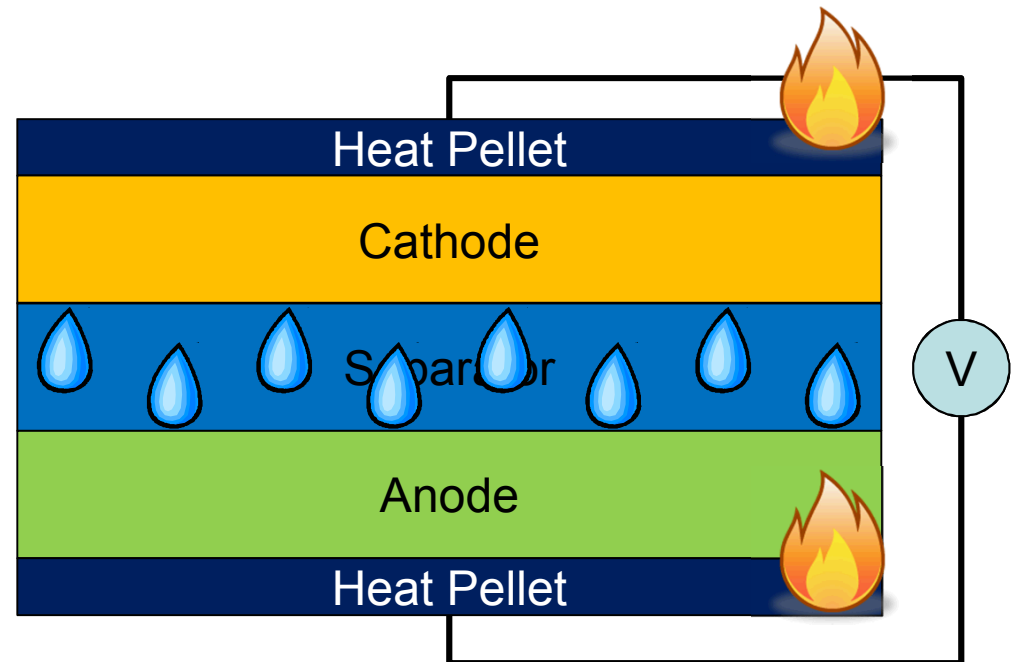
- Predict activation times
- Optimize volume, insulation, manufacturing

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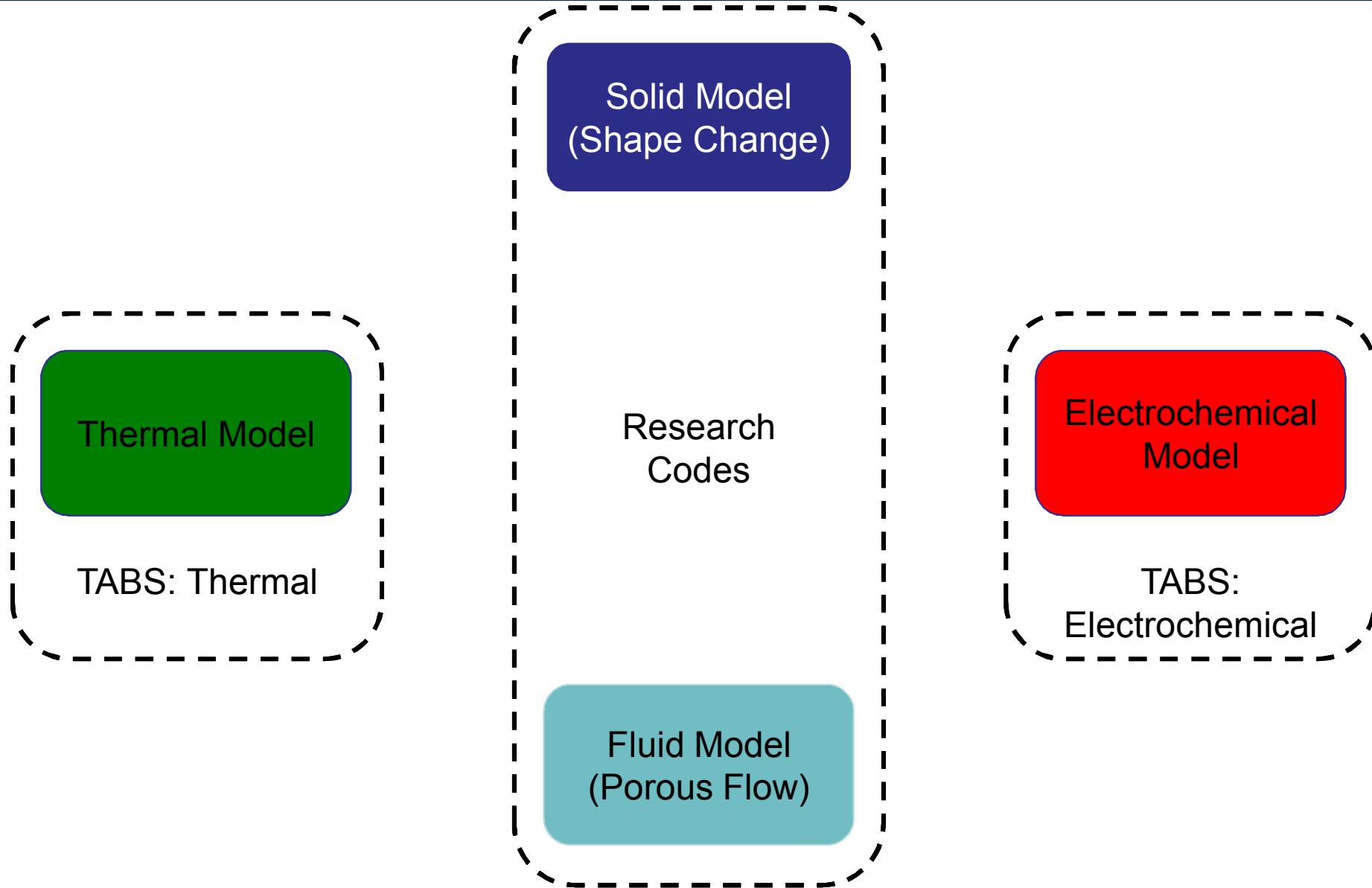
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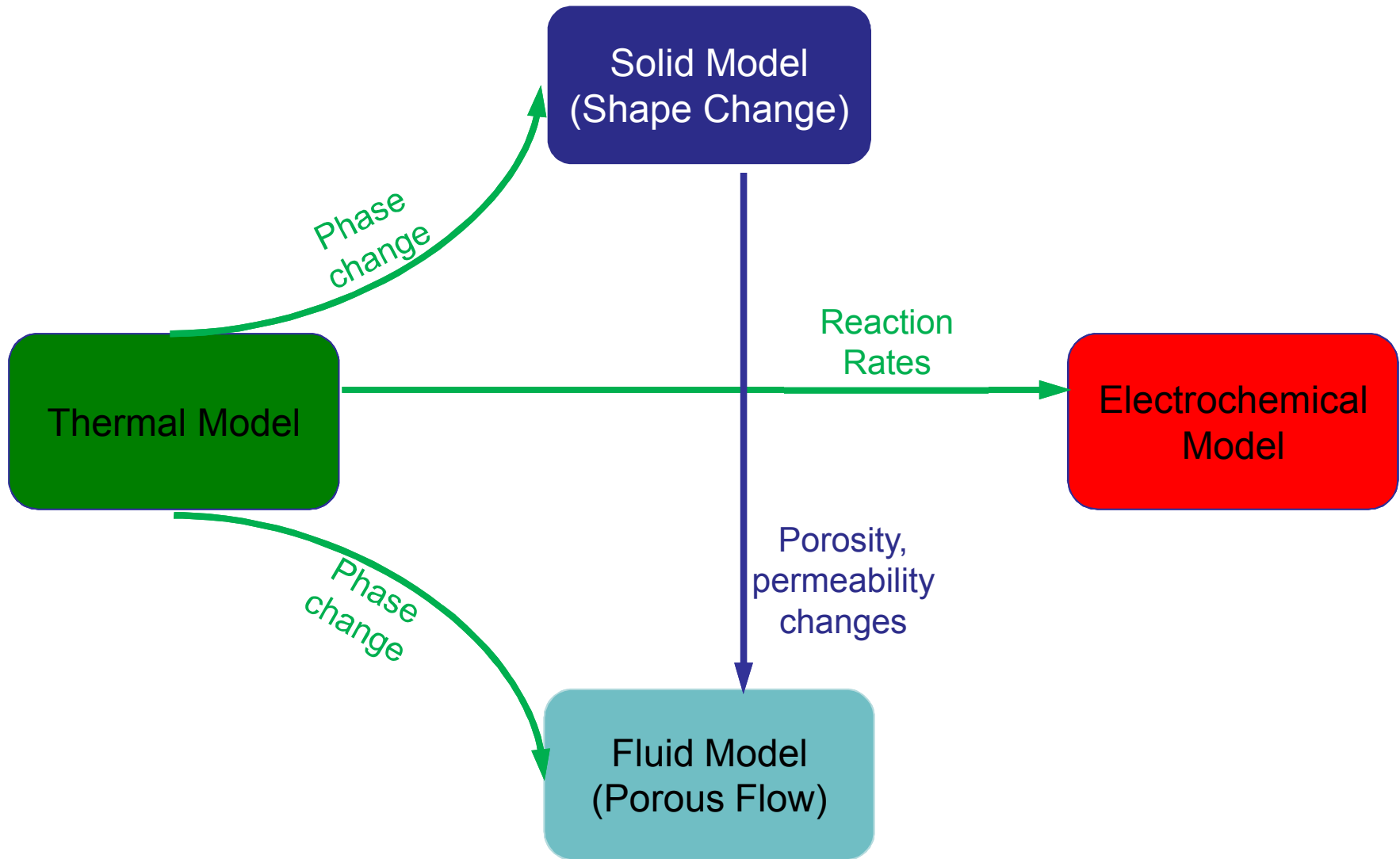
Solid Model
(Shape Change)

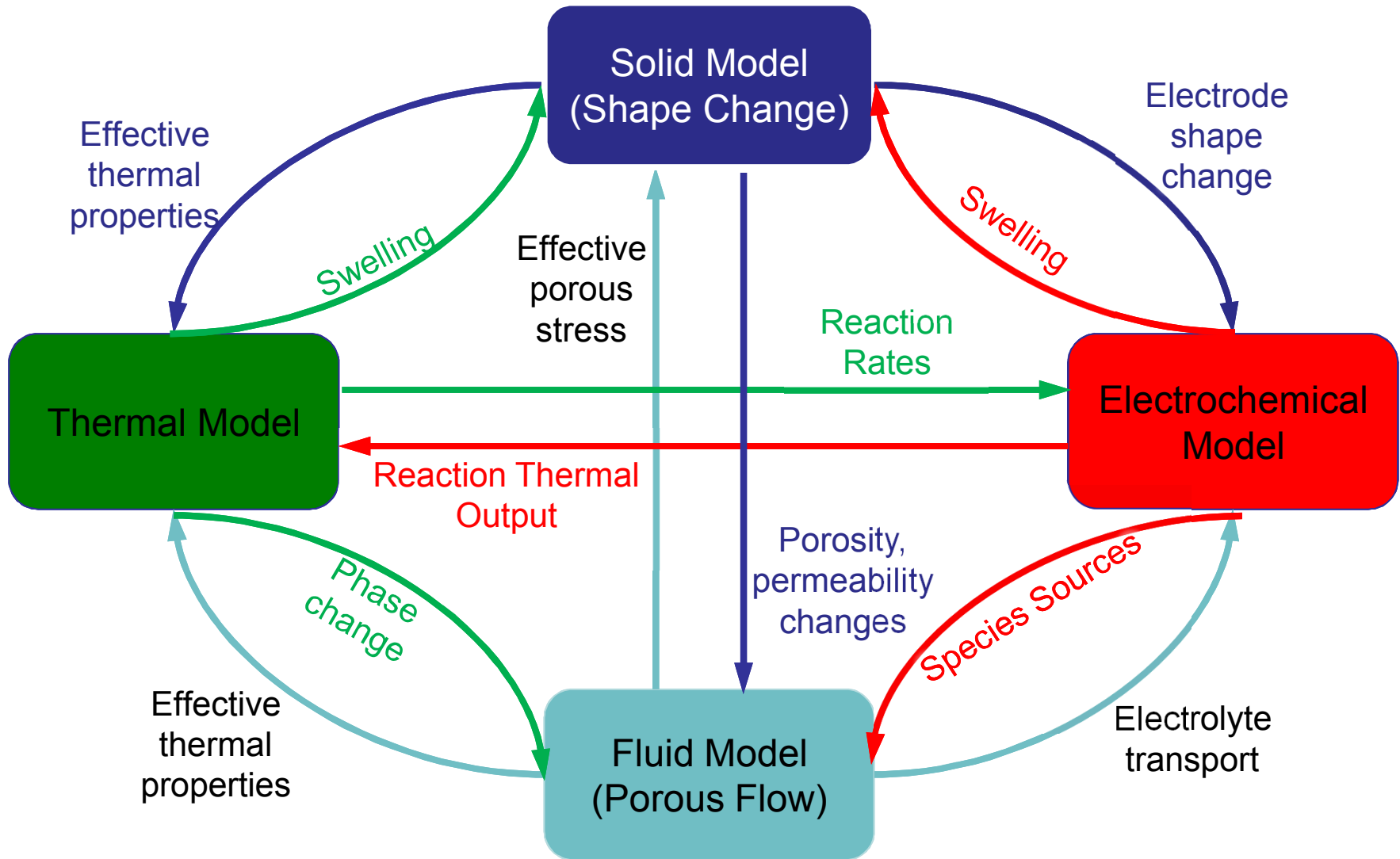
Thermal Model

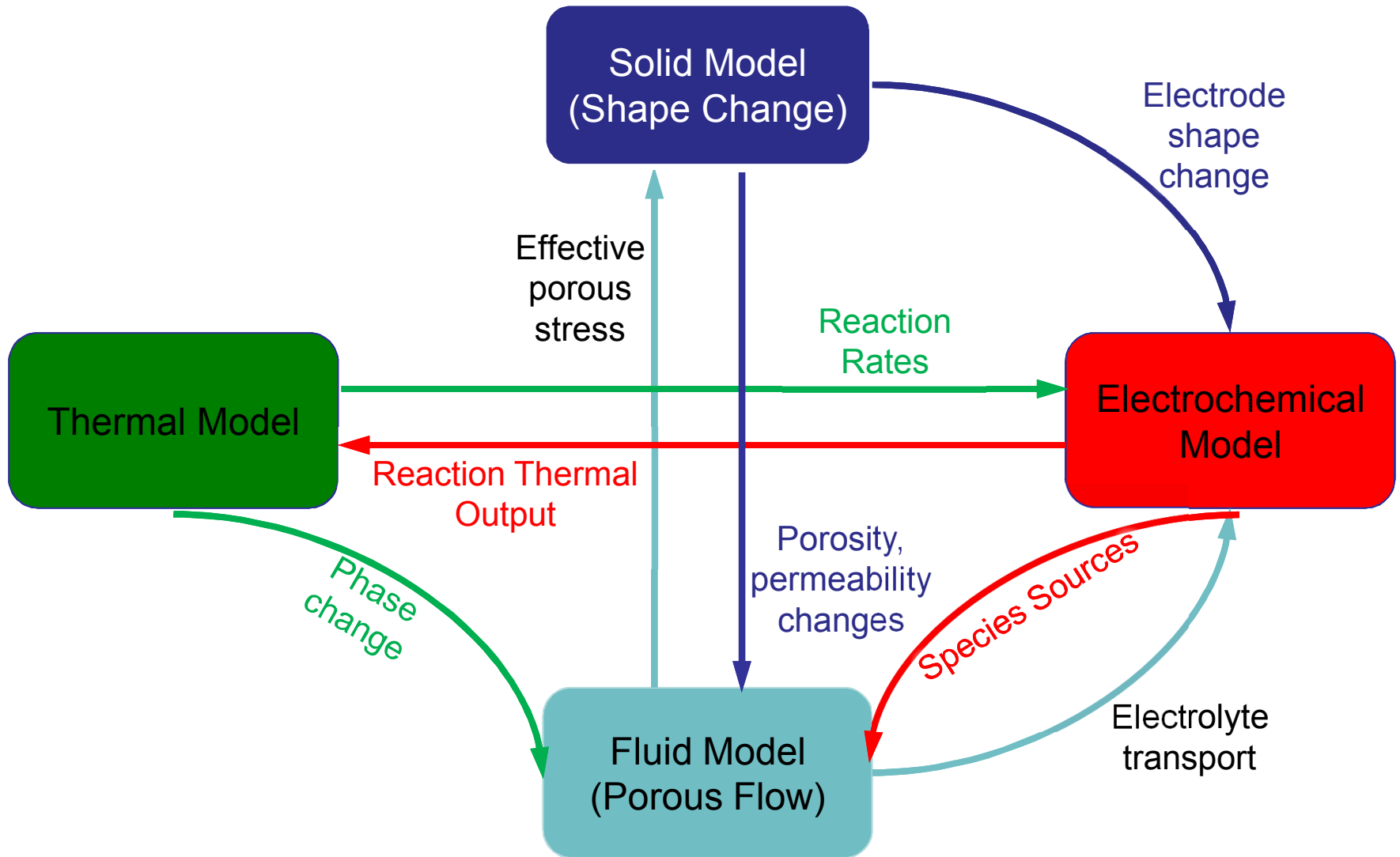
Electrochemical
Model

Fluid Model
(Porous Flow)









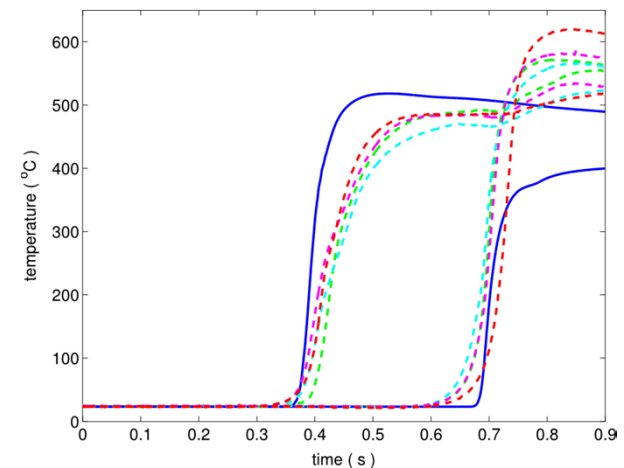
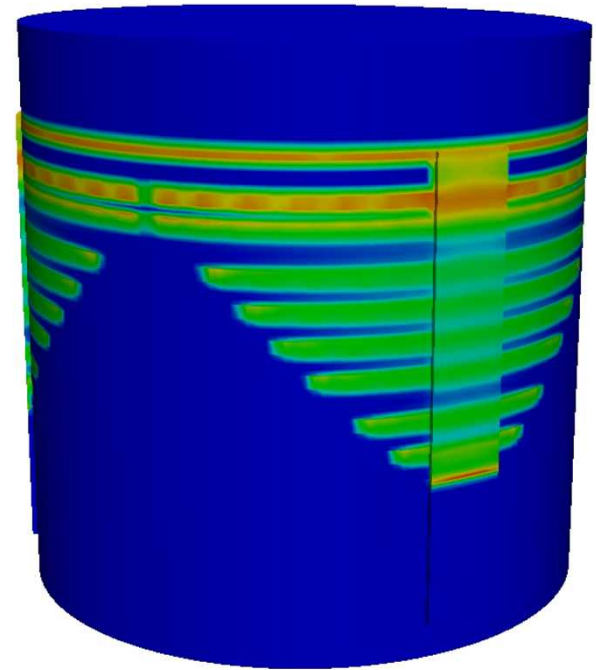
- Thermo-poro-mechanical coupling
 - Thermal model
 - Mechanical deformation model
 - Thermo-mechanical demonstration
 - Porous flow model
 - Thermo-porous flow demonstration
 - Coupled thermo-poro-mechanical demonstration problem

- Thermo-electrochemical coupling
 - Electrochemical model
 - Demonstration problem

- Standard heat equation:

$$\frac{\partial T}{\partial t} = \alpha \nabla^2 T + Q$$

- Source term Q applies to heat pellet, paper
- Level set tracking of burn fronts
 - Constant propagation speed
 - Heat released over a narrow region near burn-front position
- Presented at Power Sources 2012
 - Paper 30-2



■ Custom constitutive model

- Capture the inelastic volumetric and isochoric deformation of the *MgO skeleton* before, during, and after activation
- Isotropic, thermal-elastic-plasticity
- **Plasticity governs activation deformation**
- Kinematic split of deformations

$$\underline{\underline{F}} = \underline{\underline{F}}^e \underline{\underline{F}}^p \underline{\underline{F}}^T$$

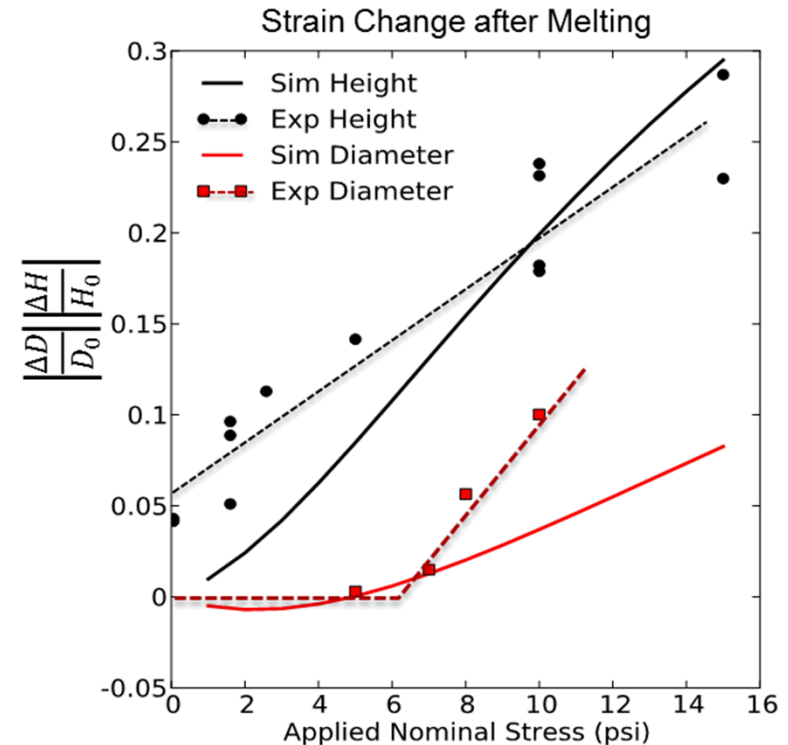
- Rule of mixtures for phase decomposition

$$\chi = \frac{T - (T - T_w/2)}{T_w}$$

- Kirchhoff stress: $\underline{\underline{\tau}} = \mu_x(T) \text{dev}(\underline{\underline{b}}^3) + \frac{\kappa_x(T)}{2} (J_e^2 - 1) \underline{\underline{\delta}}$

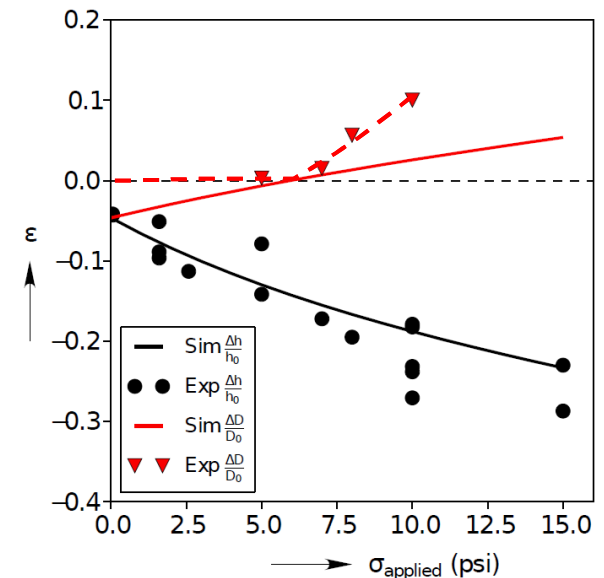
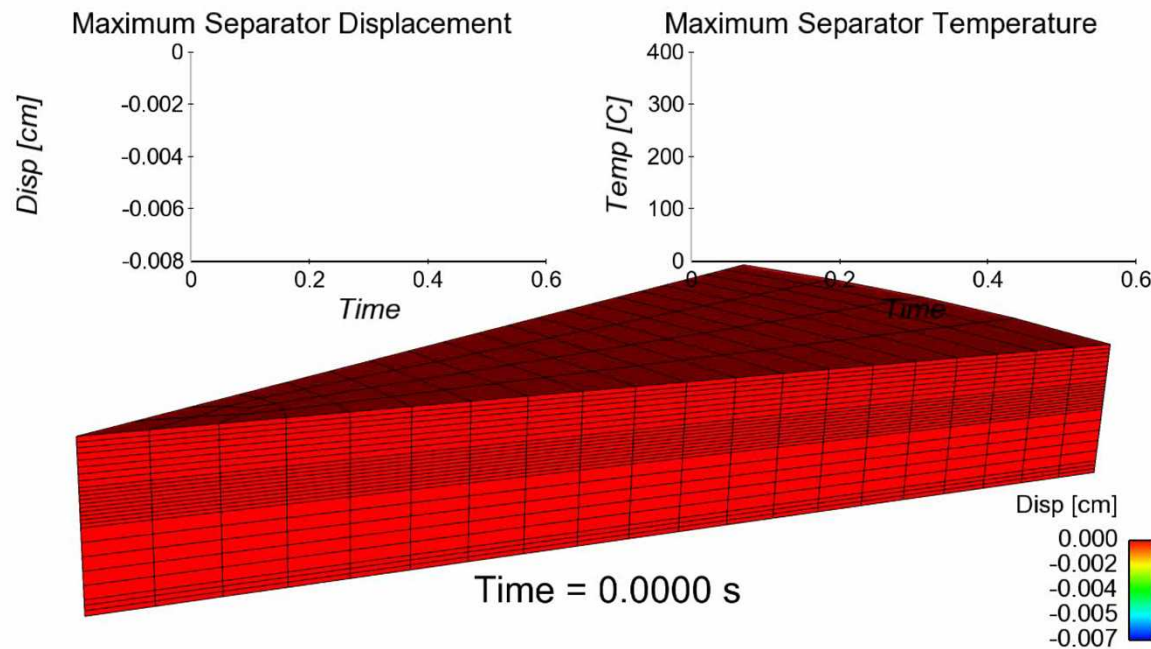
- Conservation of momentum: $\underline{\underline{\nabla}} \cdot \underline{\underline{\sigma}} = \underline{\underline{0}}$

- Coupled to porous-flow through effective stress: $\underline{\underline{\sigma}} = \underline{\underline{\hat{\sigma}}} + p \underline{\underline{\delta}}$



Demonstration: Themo-mechanical deformation

- As the separator heats to above the electrolyte melting temperature, the separator mechanically deforms in a process calibrated to experimental data.
- Current models capture the height change well, but not the diameter change
 - Related to the lack of effective stress in current implementation
 - Will be improved with thermo-poro-mechanical coupling



- Electrolyte and gas form two immiscible phases upon melting

$$\frac{\partial(\rho_w \phi S_w)}{\partial t} = \nabla \cdot \left(\rho_w \frac{k_{rw}}{\mu_w} \underline{\underline{K}} \cdot (\nabla p_w - \rho_w \underline{g}) \right) + Q_w$$

$$\frac{\partial(\rho_n \phi S_n)}{\partial t} = \nabla \cdot \left(\rho_n \frac{k_{rn}}{\mu_n} \underline{\underline{K}} \cdot (\nabla p_n - \rho_n \underline{g}) \right) + Q_n$$

- Saturation and capillary pressure related to DOFs (wetting and non-wetting pressures) through model relations

$$S = S(p_c); \quad p_c = p_n - p_w$$

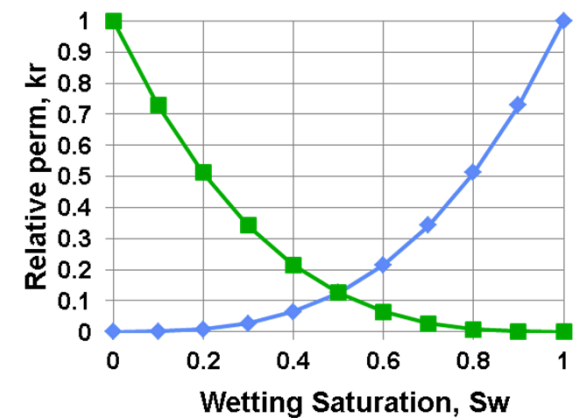
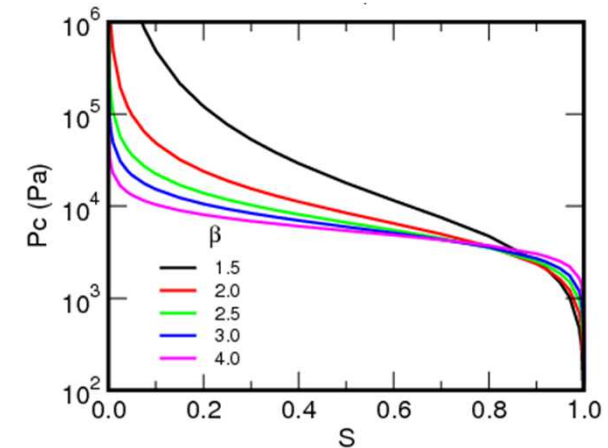
- Coupling to other physics important!

- Required:

$$\phi = \phi(\underline{d}); \quad \mu_i = \mu_i(T)$$

- Optional?:

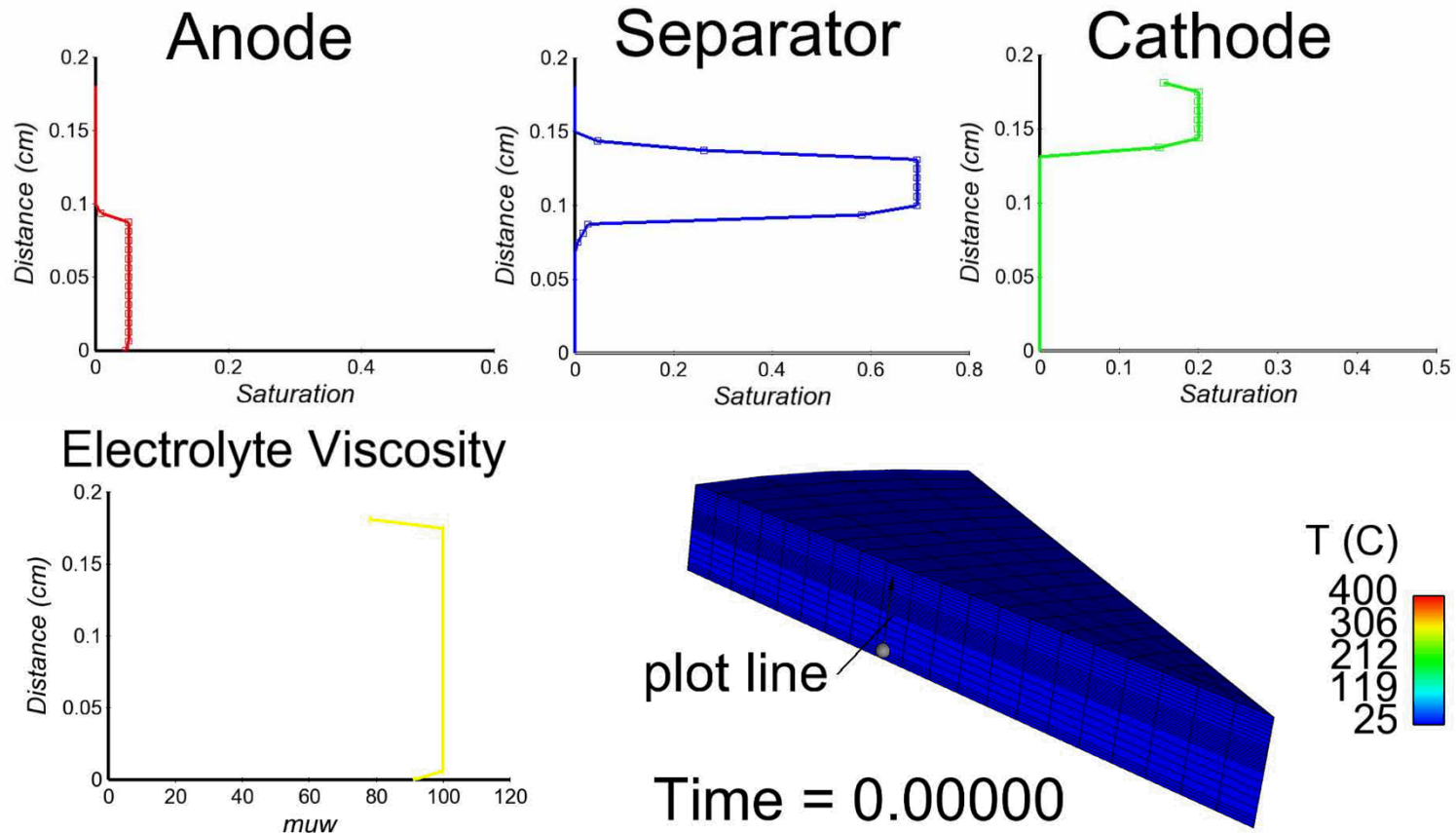
$$S_i = S_i(p_c, \underline{d}); \quad \underline{\underline{K}} = \underline{\underline{K}}(\underline{d})$$



Capillary pressure (top) and relative permeability (bottom) depend on wetting phase saturation and electrode pore structure

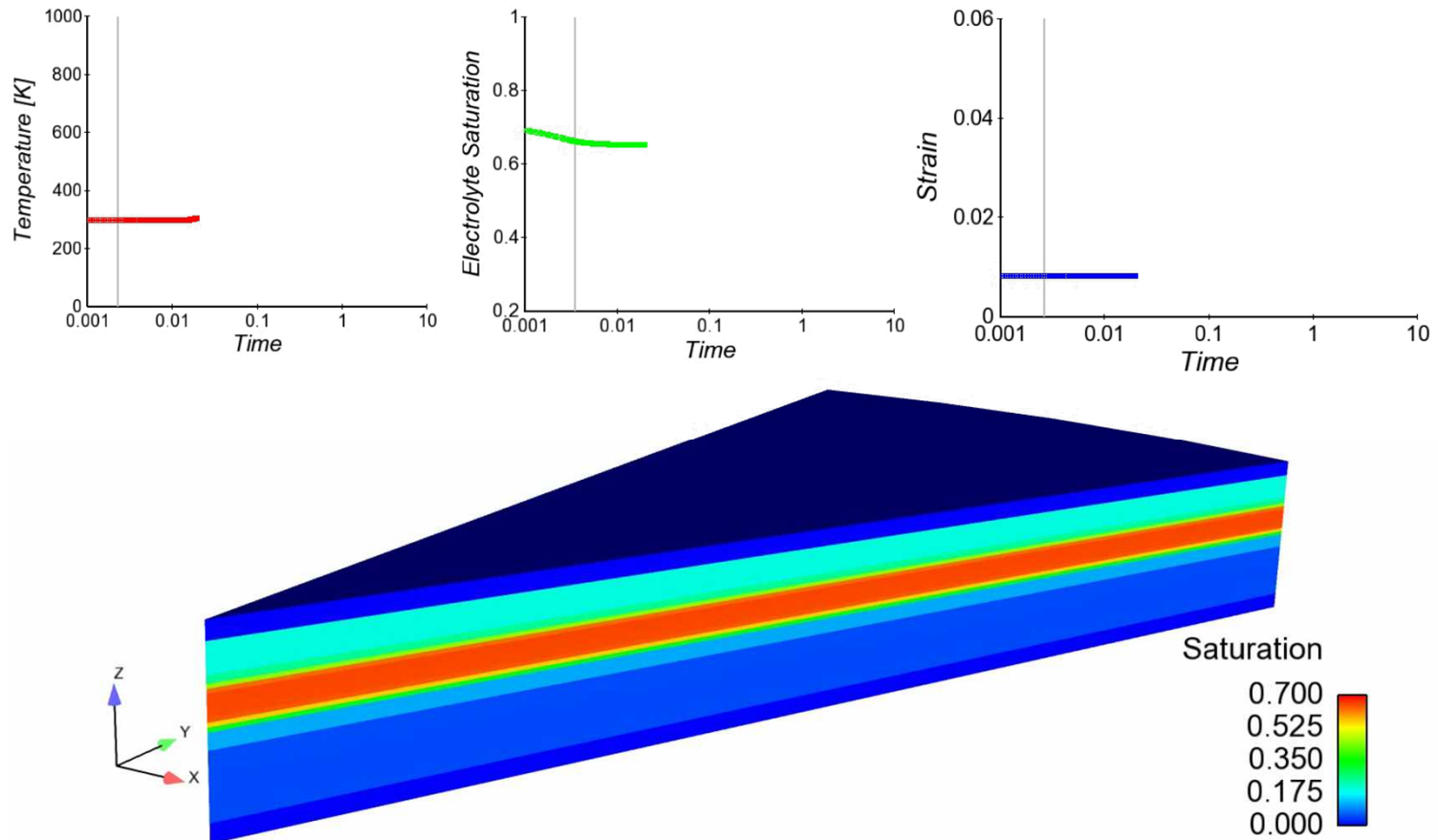
Demonstration: Thermo-porous flow

- Two-pressure porous-flow formulation enables stable solution of flow from the separator to the cathode and anode.
- Flow is “frozen” before activation by an artificially high viscosity. As the electrolyte melts, the viscosity drops.

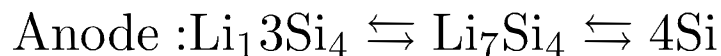
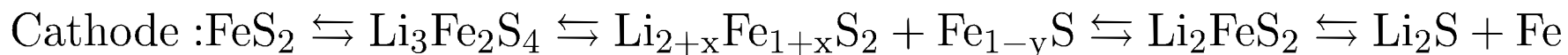


Demonstration: Thermo-poro-mechanical coupling

- Thermo-poro-mechanical single-cell simulation with full coupling:
 - Heat pellet burn
 - Two-phase porous flow upon activation
 - Separator deformation upon activation

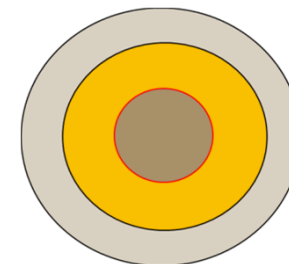


- Reactions, especially for the cathode, are stoichiometrically complicated



- Cantera's "Electrode Object" deploys multiple sub-grid models

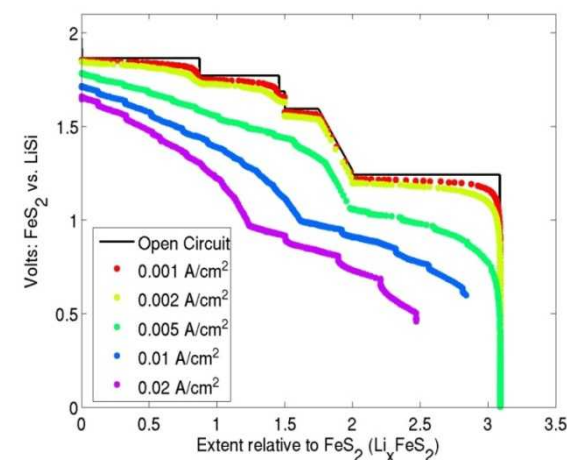
- Infinite capacity
- Multi-plateau
- Newman reaction extend
- Finite capacity



Shrinking Core Model

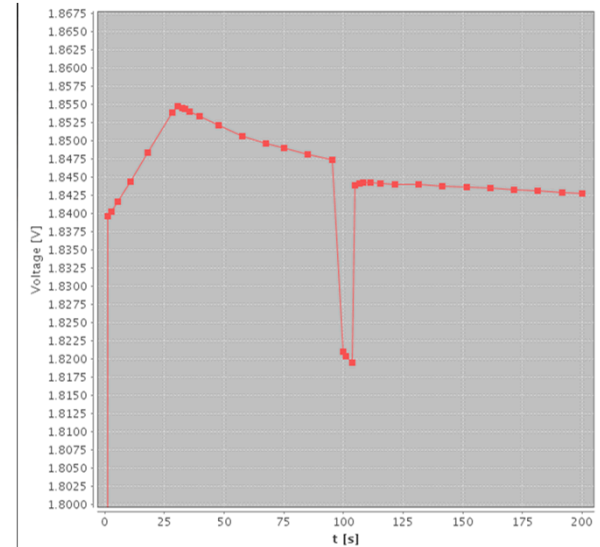
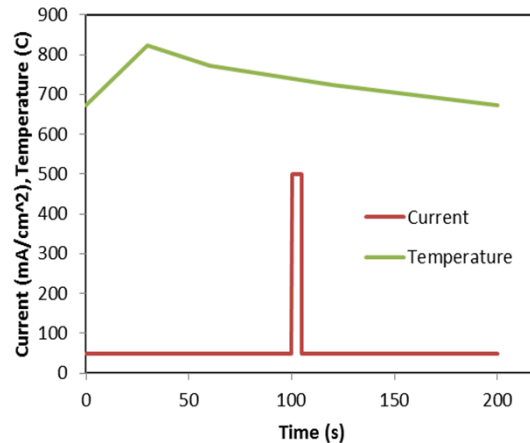
- Multiple plateaus can react simultaneously
- Diffusional losses with transport

- Primary electrochemical coupling is the temperature
 - Cantera's thermodynamics all temperature-dependent
- Future: Use deformed geometry to affect porosity in electrochemical calculations

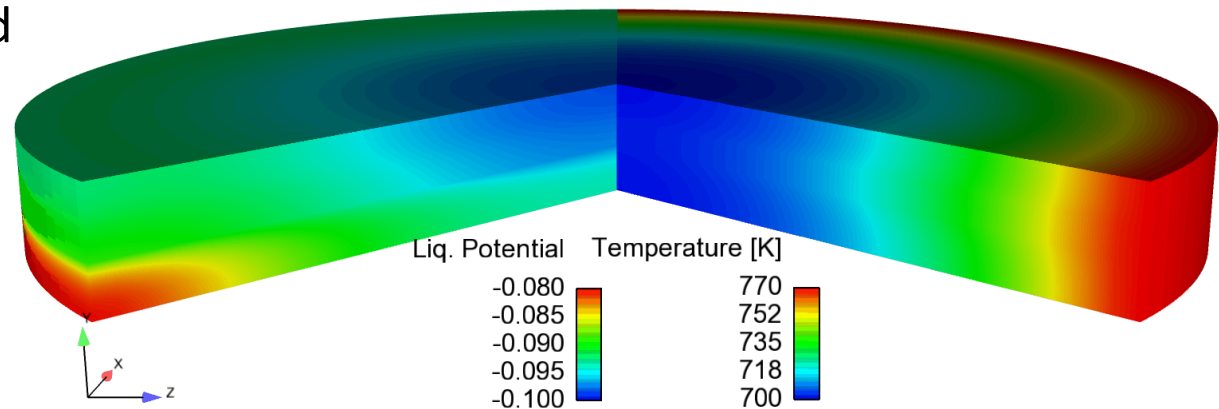


Demonstration: Thermo-electrochemical coupling

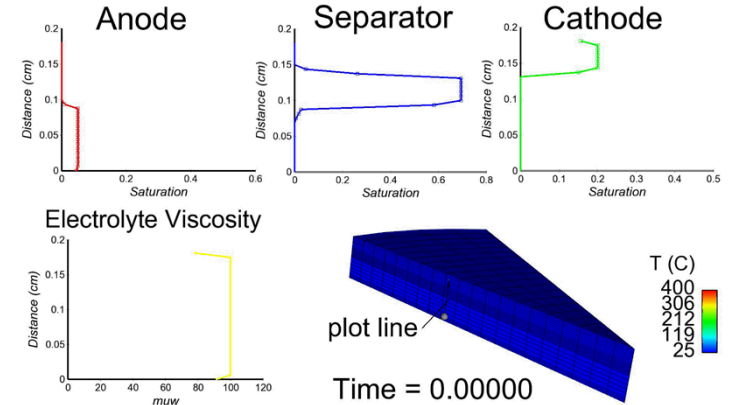
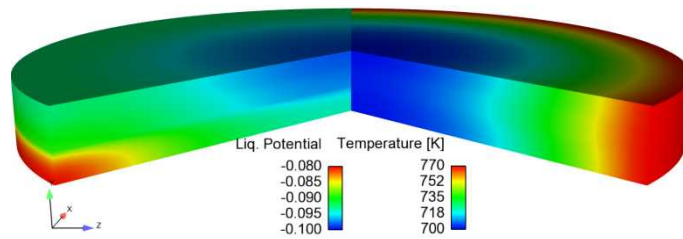
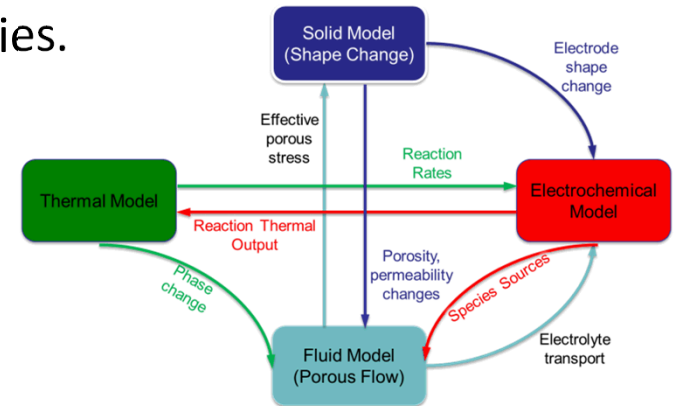
- Voltage responds to temperature and current



- Spatial temperature variations affect local potentials and current densities



- “Intelligent” coupling of physics can provide significantly higher-fidelity models, with potentially only modest performance penalties.
- Future investigation of additional couplings:
 - Material properties for all physics affected by:
 - Mechanical deformation (change in solid fraction)
 - Saturation (change in liquid fraction)
 - Eventually couple electrochemistry to the thermo-poro-mechanics



- Acknowledgements:
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 - Victor Brunini, Lindsay Erickson, Adrian Kopacz

BACKUP

Free Energy

Density

$$\rho_0 \psi = \mu_x[T] (\bar{I}_{1e} - 3) + \frac{\kappa_x[T]}{4} (J_e^2 - 1 - 2 \log J_e)$$

Kirchoff Stress

$$\boldsymbol{\tau} = 2\rho_0 \mathbf{b} \frac{\partial \psi}{\partial \mathbf{b}} = \mu_x[T] \text{dev}[\mathbf{b}^e] + \frac{\kappa_x[T]}{2} (J_e^2 - 1) \mathbf{1}$$

Isochoric (Radial) Yield

$$\phi_\mu = \sqrt{J_2} - A_x \frac{I_1}{3} - B_x \left(\frac{I_1}{3} \right)^2 - Y_{psx} - H_{\mu x} \epsilon_\mu^{m_x}$$

Plastic Flow Rules

$$\mathcal{L}[\mathbf{b}^e] = \mathbf{F} \dot{\mathbf{C}}^{p-1} \mathbf{F}^T = -2 \left(\dot{\lambda}_{iso} \mathbf{n}_{iso} + \dot{\lambda}_{vol} \mathbf{n}_{vol} \right) \mathbf{b}^e$$

$$\mathbf{n}_{iso} = \frac{\text{dev} \boldsymbol{\tau}}{\|\text{dev} \boldsymbol{\tau}\|}, \quad \mathbf{n}_{vol} = \frac{1}{3} \mathbf{1}$$

Kinematic Split of the Deformation Gradient: Thermal, Elastic, and Plastic

$$\mathbf{F} = \mathbf{F}^e \mathbf{F}^p \mathbf{F}^\theta$$

Cold/Hot State Phase

Decomposition

$$\begin{aligned} \text{if } T < T_m - T_w/2, \quad \chi &= 0, \\ \text{elseif } T > T_m + T_w/2, \quad \chi &= 1, \\ \text{else } \chi &= \frac{T - (T_m - T_w/2)}{T_w}, \end{aligned}$$

Volumetric Yield

$$\phi_\kappa = \frac{I_1}{3} - Y_{Px} - H_{\kappa x} \epsilon_\kappa^{n_x}$$

Net Yield Surface is the Phase Volume Fraction Weighted Sum

$$\phi = (1 - \chi) (\phi_\mu^C + \phi_\kappa^C) + \chi (\phi_\mu^H + \phi_\kappa^H)$$