

# **Flame-aerosol (soot) interactions and some work on fire suppression at Sandia**

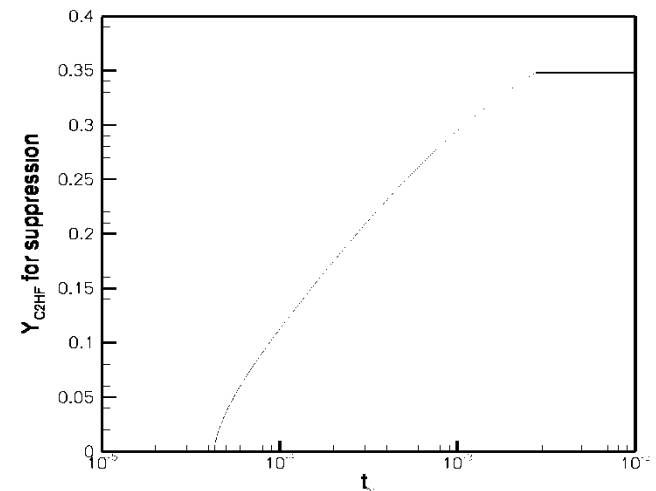
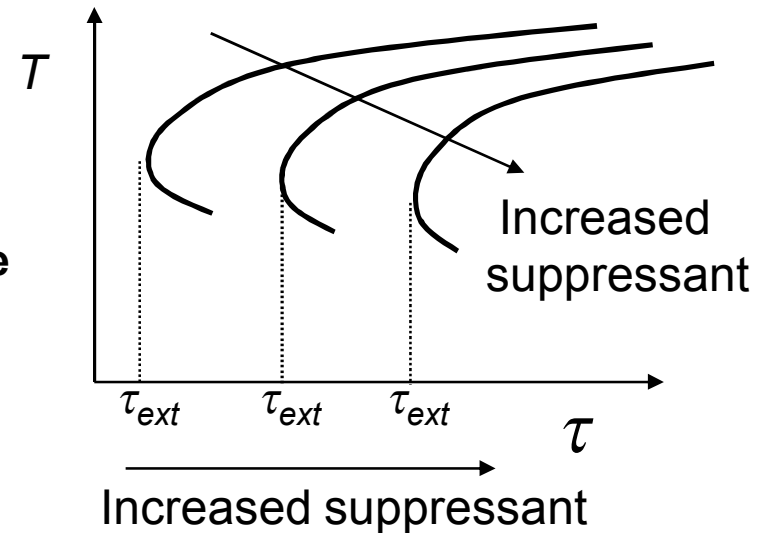
**John Hewson, Allen Ricks, Sheldon Tieszen**

**Fire and Aerosol Sciences  
Sandia National Laboratories  
Albuquerque, NM 87185 USA**

Sandia is a multiprogram laboratory operated by Sandia Corporation, a Lockheed-Martin company, for the United States Department of Energy's National Nuclear Security Administration under contract DE-AC04-94AL85000

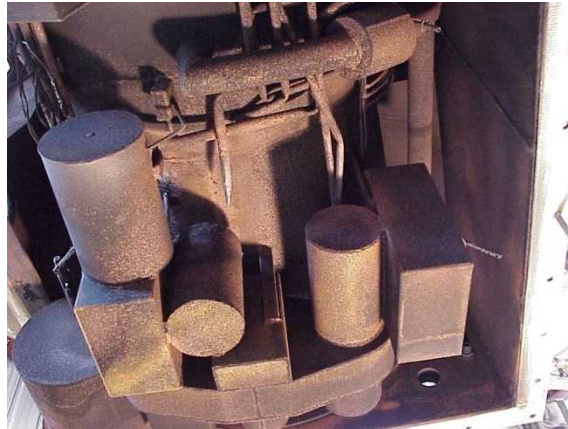
# What is required to suppress a flame?

- Flames suppressed when heat loss rate  $>$  chemical rate
- Rate of heat loss proportional to fluid mixing time rate,  $1/\tau$ , or scalar dissipation rate,  $\chi$ .
- Chemical rate is function of temperature and reactant composition including suppressant.
  - Suppressant typically reduces chemical rates.
- Damkohler extinction criteria:
  - Extinction if  $\tau/\tau_{chem} < Da_{crit}$



# Fire suppression in aircraft nacelles

- Aircraft fire suppression must fit within constraints.
  - Mission success limits mass of suppression system.
  - Clutter both *impedes* and *enhances* agent transport and acts to stabilize fires.
  - Air flow to remove combustible vapors also removes suppressants.



# Fluid Dynamics of Suppression behind Clutter

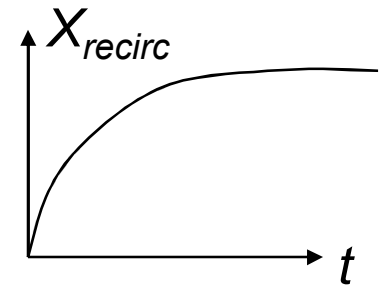
- How does clutter influence suppression requirements?
- Clutter reduces ability of suppressants to reach hidden areas, stabilizes flames.



- In designing suppression systems with CFD, it can be difficult to resolve mixing around all clutter.

- Stirred reactor subgrid model works for isolated clutter

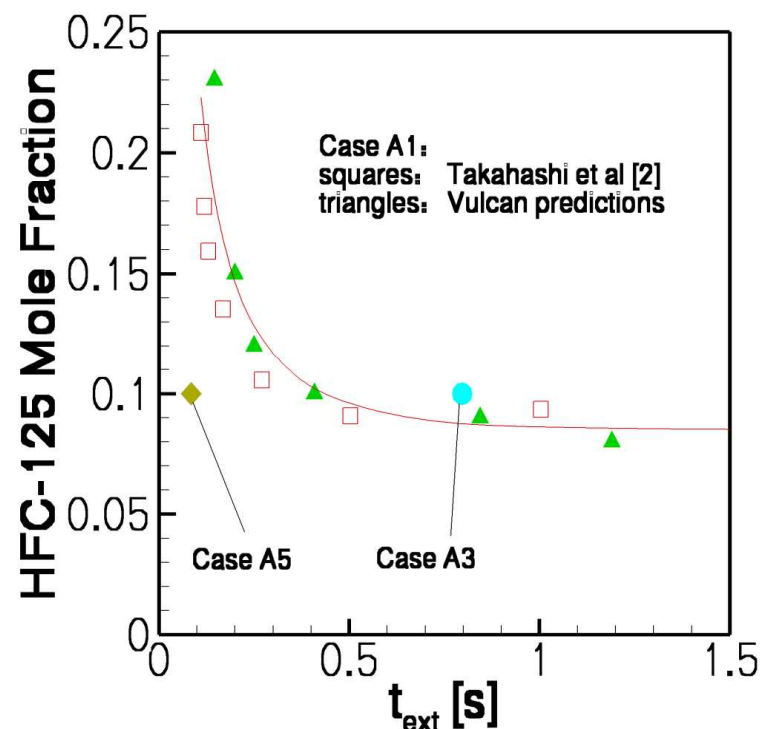
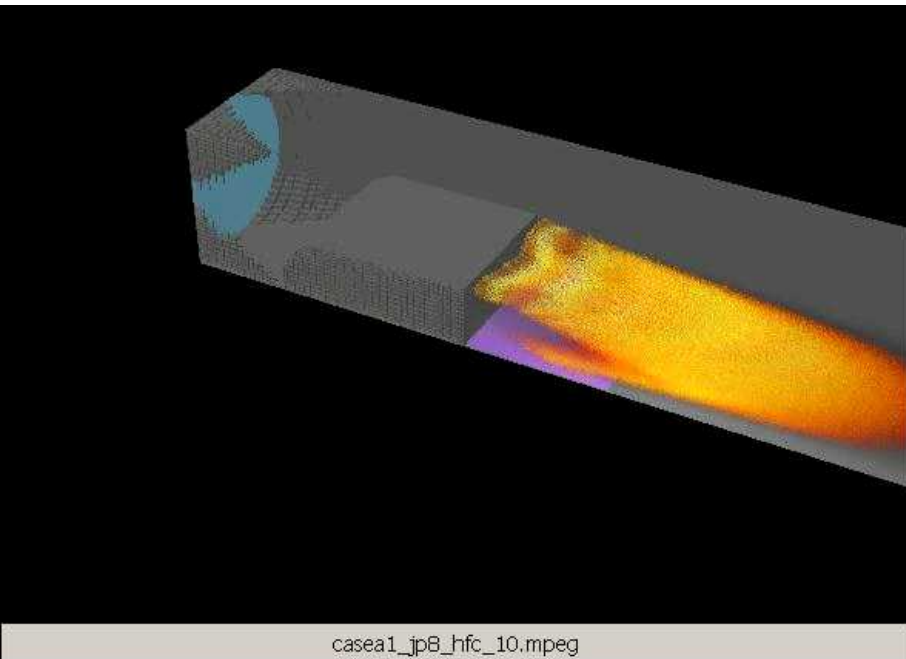
$$X_{recirc} = X_{\infty} [1 - \exp(-t / \tau_{mix})]$$



- BUT interacting clutter significantly affects mixing time scales...

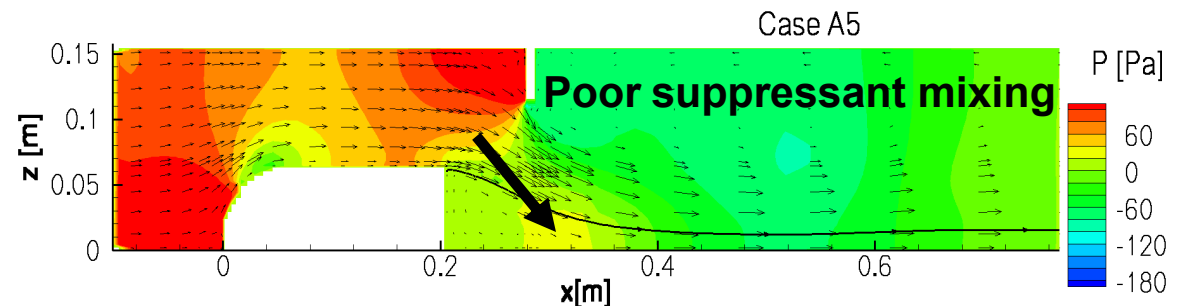
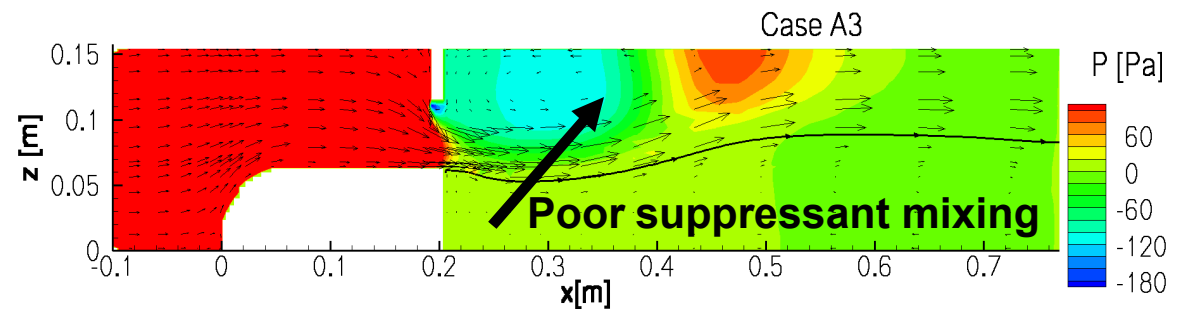
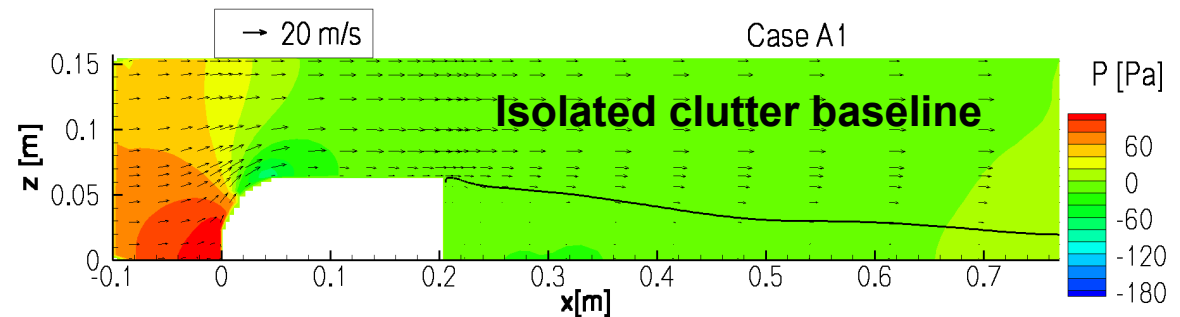
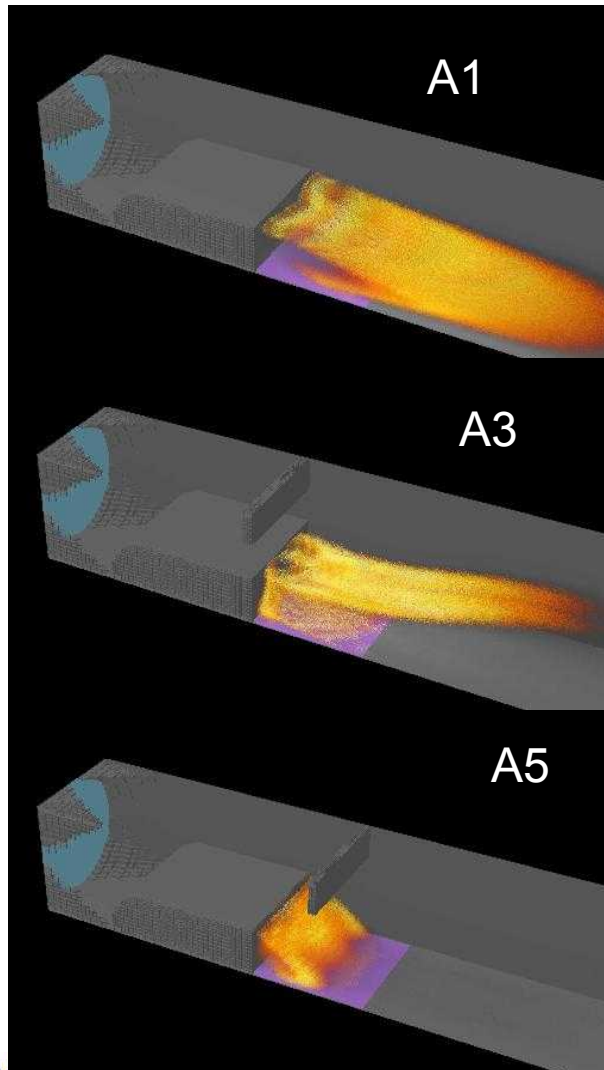
# Fluid Dynamics of Suppression behind Clutter

- Isolated clutter: Predicted suppression behind backward facing step follows stirred-reactor subgrid model.



Hewson et al., CFD Modeling of Fire Suppression and Its Role in Optimizing Suppressant Distribution, *Proc. Halon Options Tech. Working Conf. (HOTWC)*, 2003.

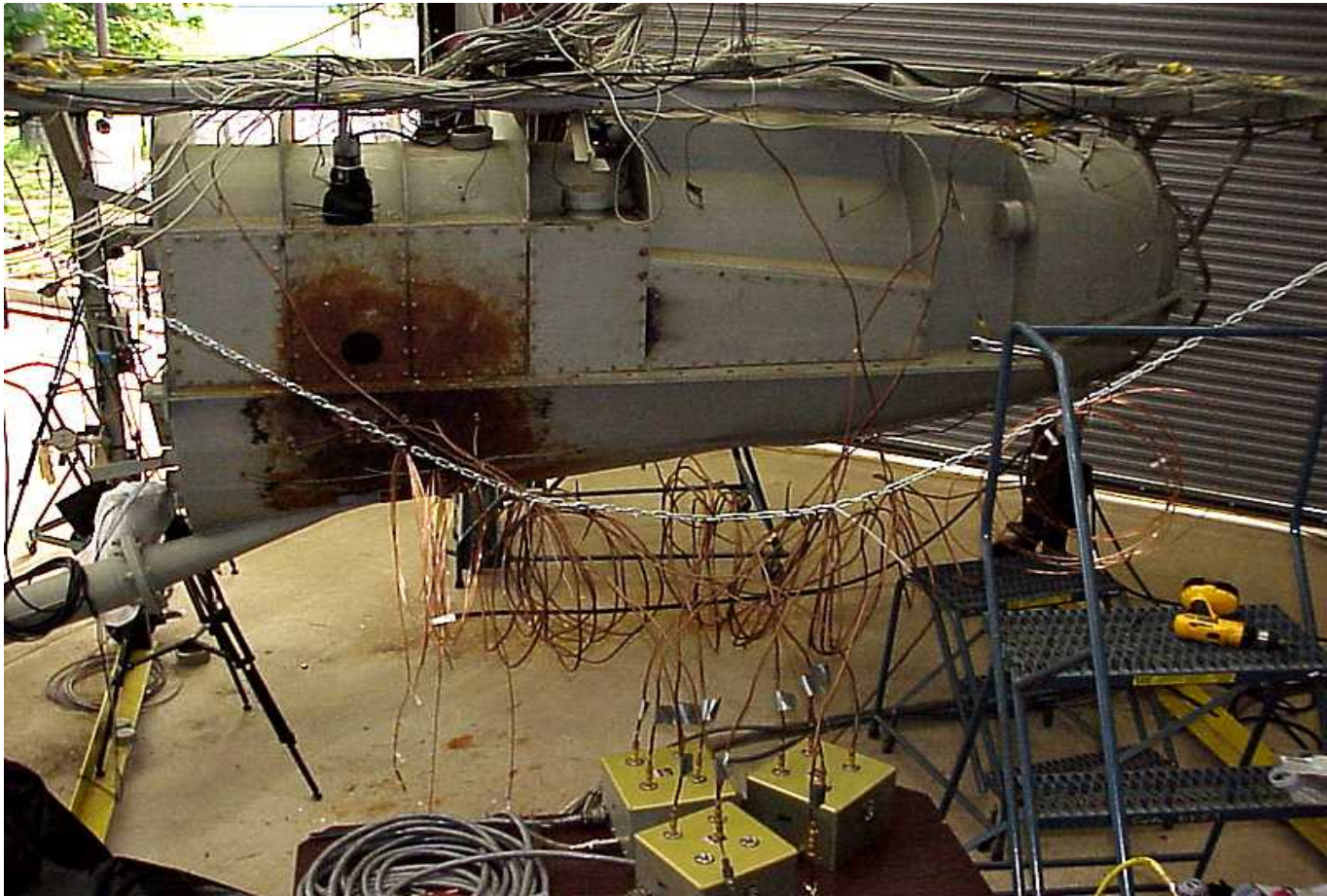
# Additional clutter changes pressure field and suppressant mixing into recirculation zone



Arrows indicate direction of pressure gradient forcing



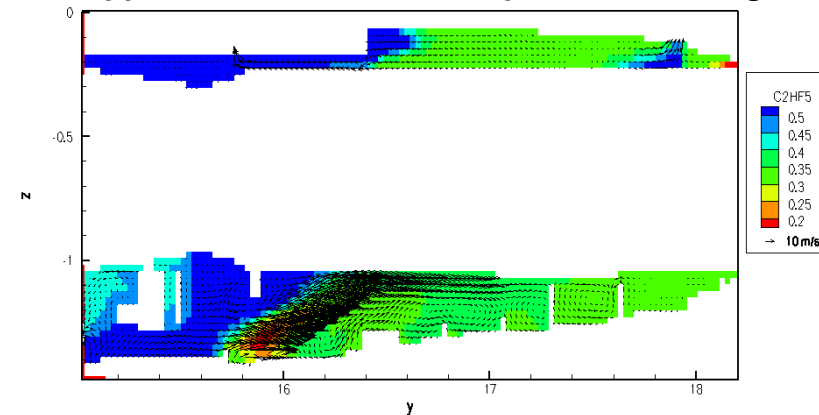
# NAVAIR Ground Nacelle Simulator



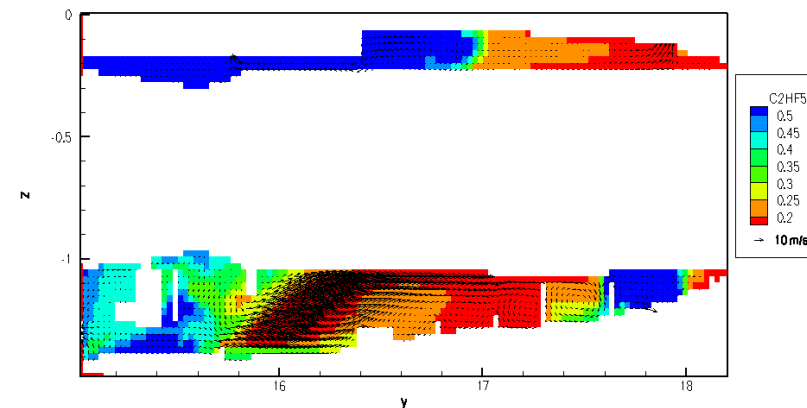
# Role of predictive suppression modeling

- For total-flooding agents, complete coverage is primary concern.
  - Determination of complete coverage in test-based program requires intelligent sensor (or fire) placement.
  - Simulations can identify regions of greatest concern: **Simulations are “fully exposed.”**
  - For nacelles, simulated suppressant distribution
    - Identified volumes not fully covered by suppressant as function of distribution nozzle arrangement.
    - Results showed which nozzles were potentially critical and which were redundant.
    - Validation tests indicated general agreement, though CFD “requirements for suppression” were conservative.

Suppressant distribution for production design



Suppressant distribution with key nozzle removed

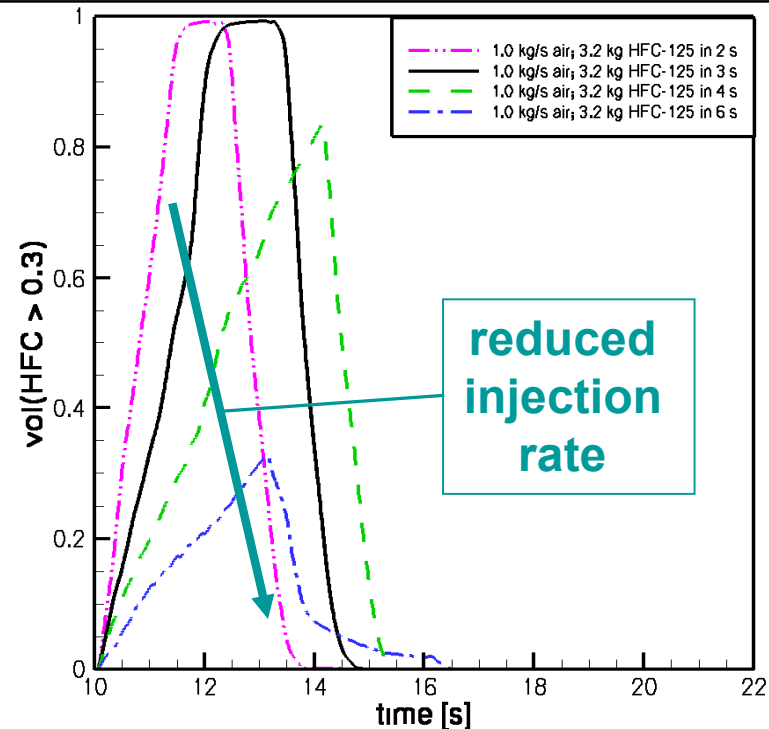




# Comparing suppressant injection rate to ventilation rate

- To get an average concentration, compare suppressant injection rate with ventilation rate.
- Inhomogeneities result in less than complete coverage.
- Here CFD results guide suppressant bottle pressurization: identify volume fraction not fully covered.
- Estimated average mass fractions at 0.59, 0.51, 0.44 and 0.35 with decreasing injection rate compared with 0.3 required for suppression.

Volume fraction where  $Y_{C_2HF_5} > 0.3$



• In ALL cases average concentration was “sufficient” but inhomogeneities resulted in insufficient coverage.

# Modeling Differential Diffusion in Nonpremixed Combustion: Soot transport in mixture fraction space

- **Overall Goal:** To develop predictive capability describing heat transfer due to fire.
  - Soot radiant heat transfer is dominant. Depends on the correlation of soot mass fraction and temperature.

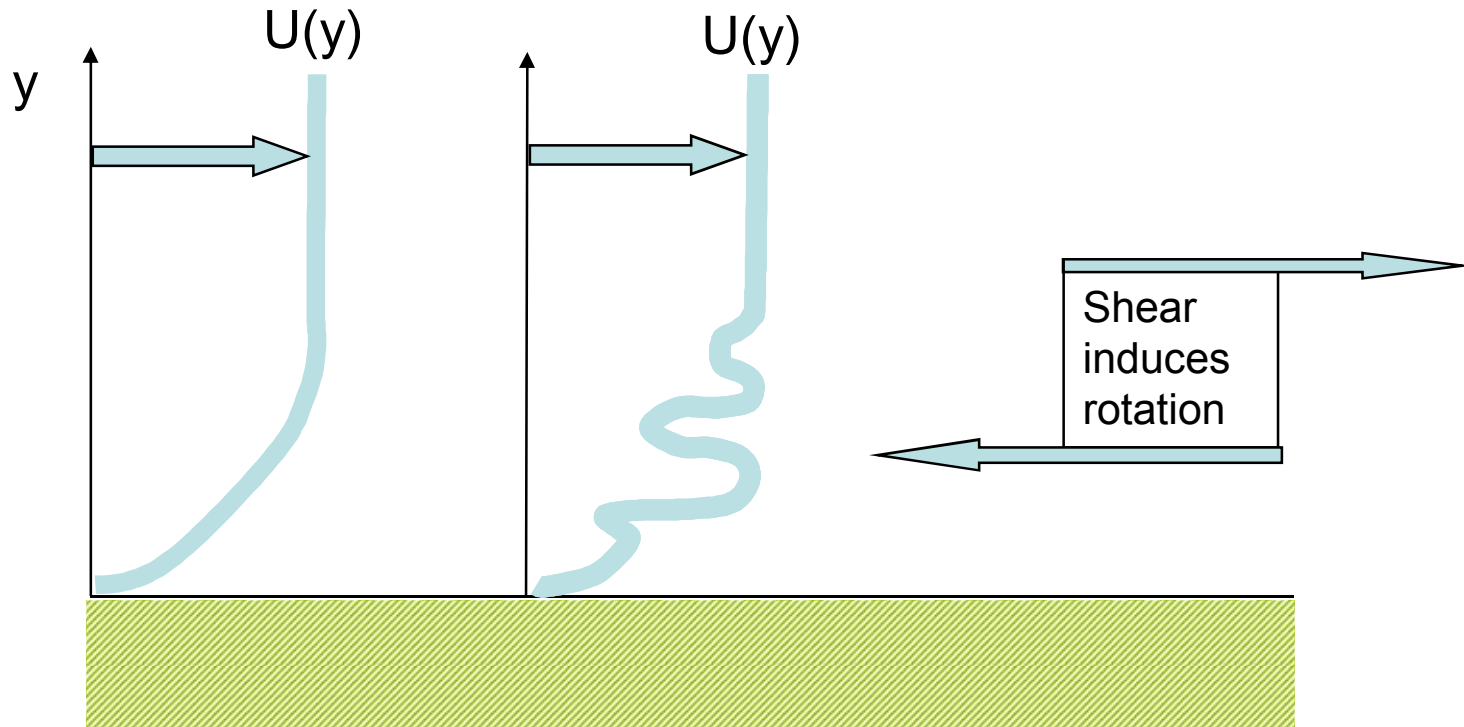
$$E_s \propto Y_s T^5$$

- **Understanding flame-soot interactions through one-dimensional turbulence (ODT) modeling of buoyant diffusion flame,**
  - Identified new CMC formulation describing soot-mixture fraction differential diffusion.
  - Model suggested turbulent diffusive process for soot and other aerosols.



# Flow description in 1-D

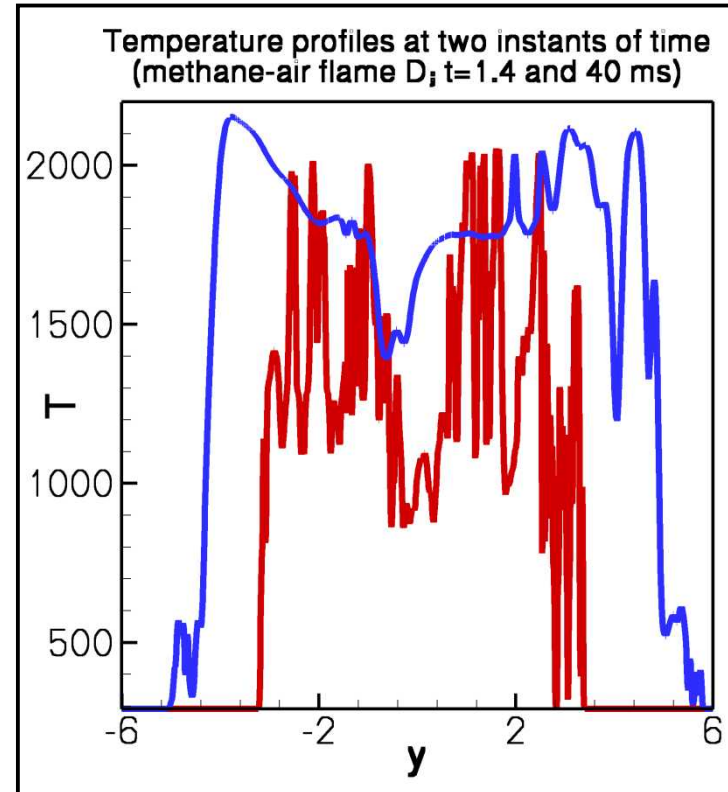
- 1-D picture can **describe** flow evolution.



- Can 1-D model **replicate** flow evolution?

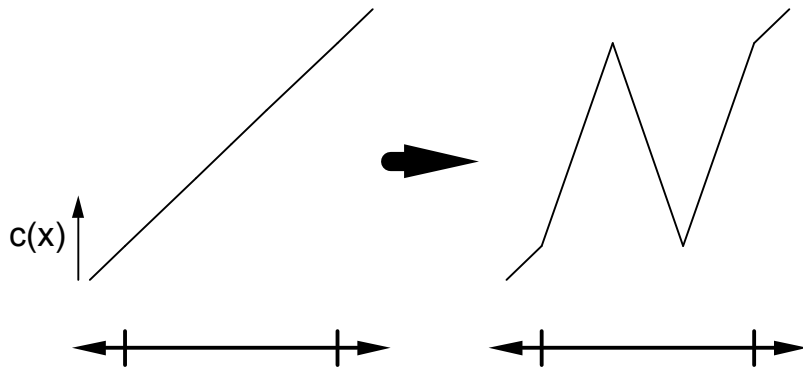
# Modeling Approach: One-Dimensional Turbulence (ODT)

- Carry all scalars and velocity on 1-D domain.
- Resolve full range of scales in 1-D.
- Two simultaneous processes:
  - Evolution of reaction-diffusion.
  - Advective mixing by “eddies.”
- Require:
  - Model for advective mixing in 1-D.
  - Rate for advective mixing in 1-D.



# Model for turbulent advection

## TRIPLET MAP



Salient features of turbulent advection:

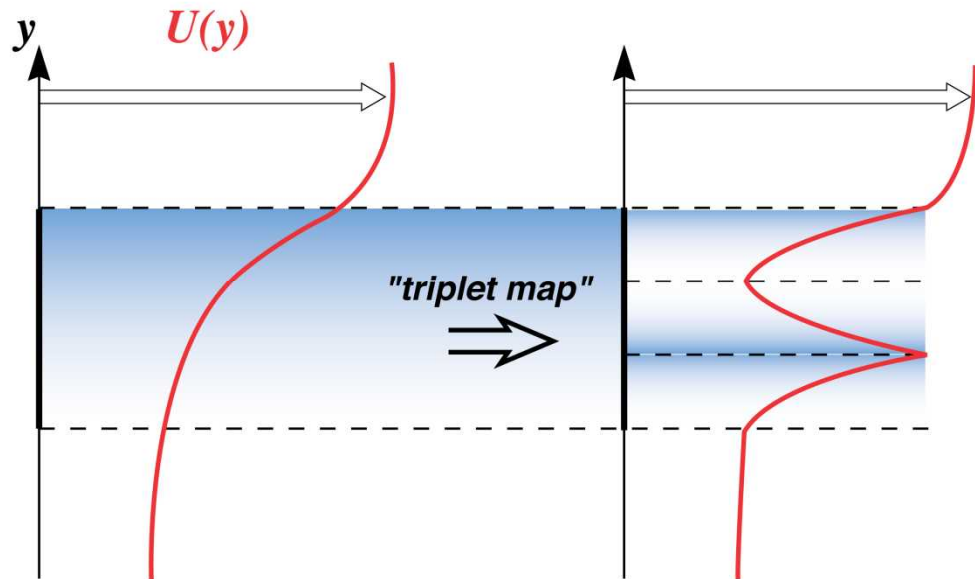
- Increase scalar and velocity gradients.
- Increase isoscalar surface area.
- Transfer of fluctuations to next smallest scale.



# Rate for Turbulent Advection

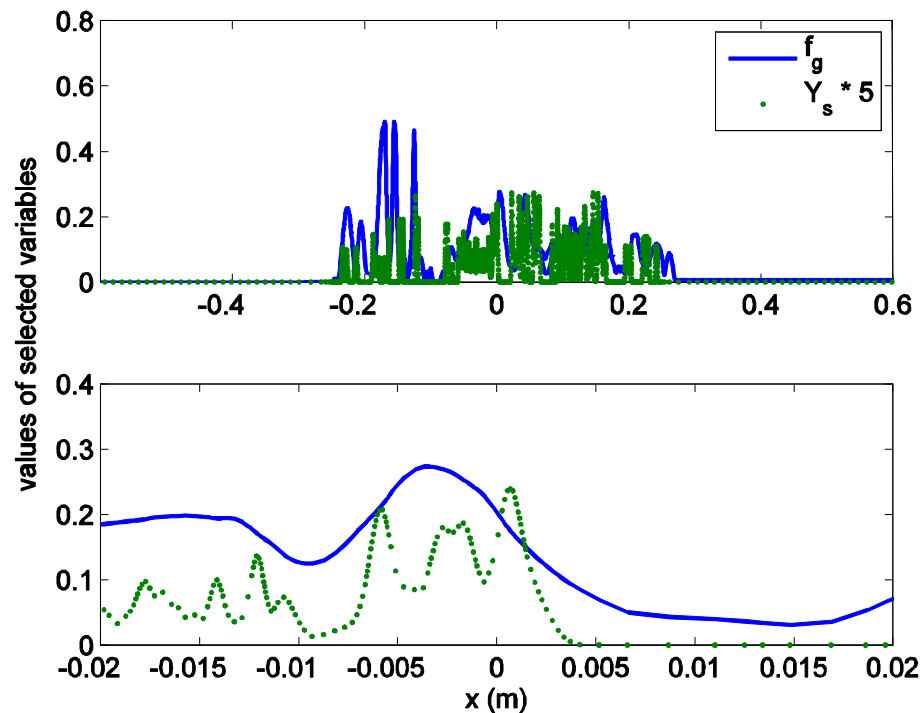
- Rate is based on measure of local shear energy.
- Triplet map “eddy” size, location randomly sampled from rate distribution.
- “Eddy” occurrence probability is function of local shear energy.
- Rate is time varying based on instantaneous flow structure.
- Transfers energy to smaller scales (cascade).

*One-dimensional turbulence*



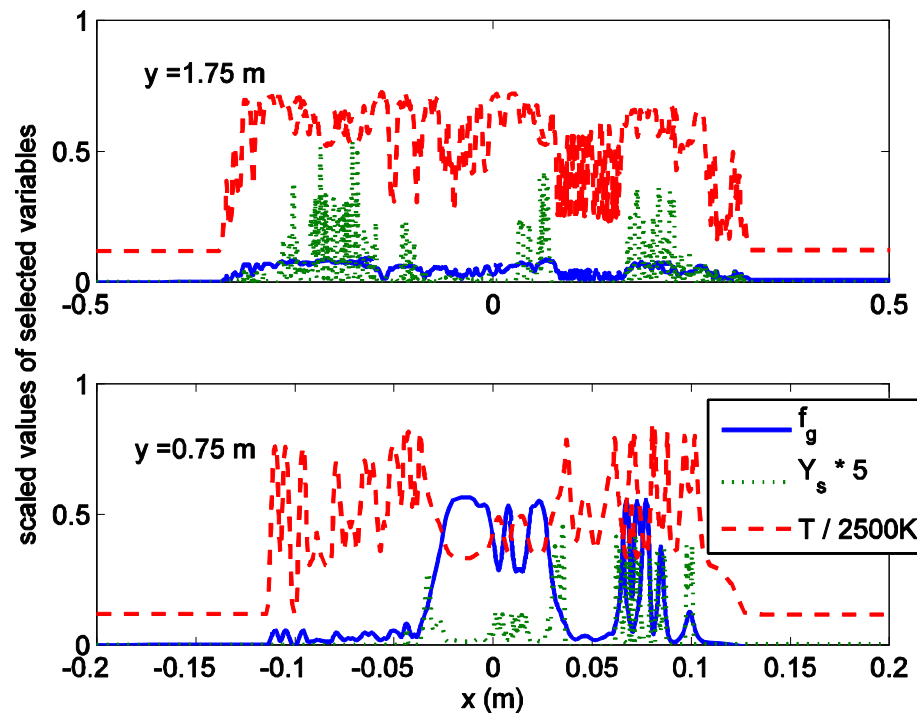
# ODT simulations provide high-fidelity data to evaluate closures

- **Mixture fraction and soot mass fraction from a single realization of the simulation at a height of 0.95 m.**
- Two levels of detail shown: Dots on the soot mass fraction plot indicate the location of control volume centroids.

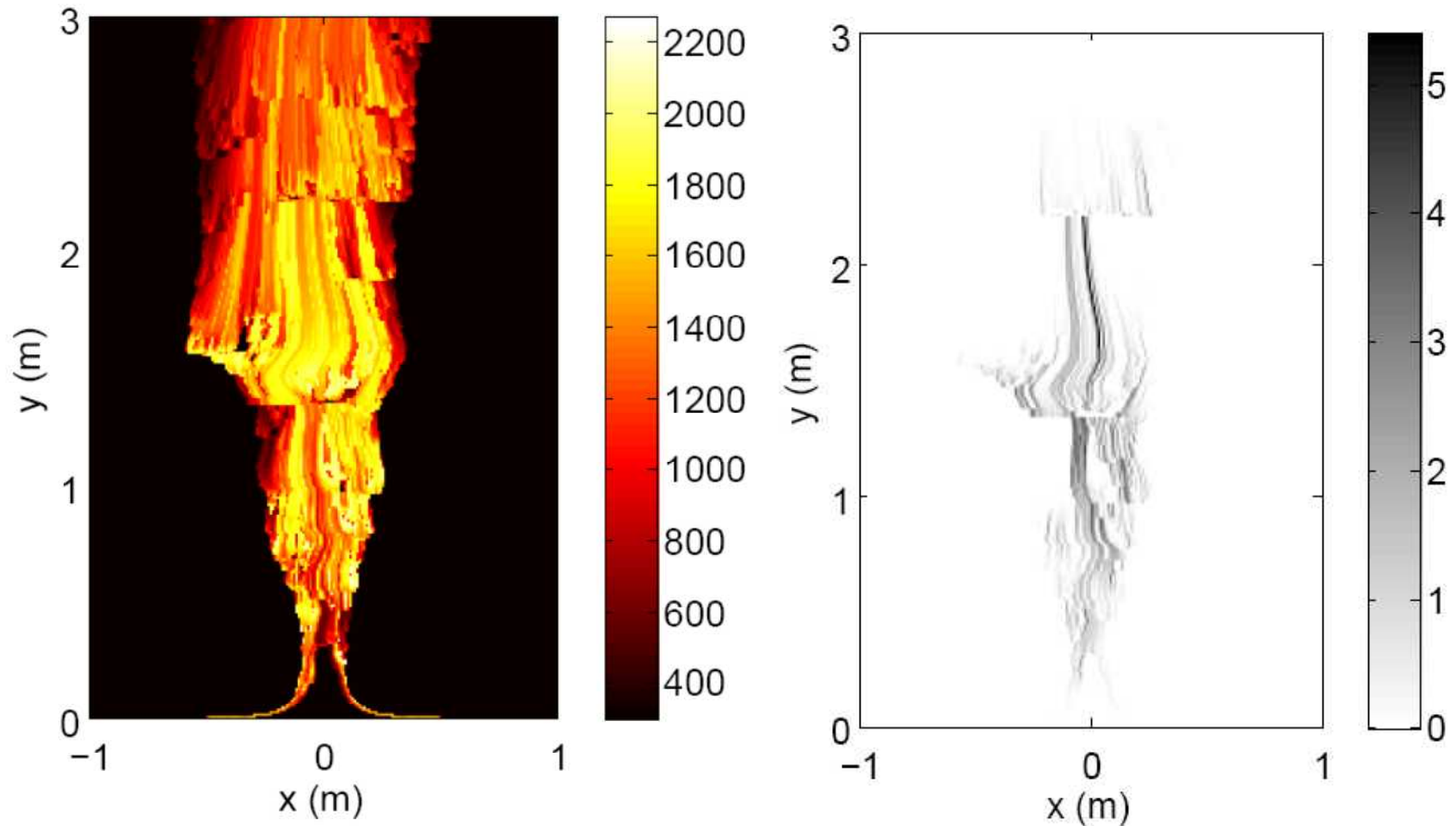


# ODT simulations provide high-fidelity data to evaluate closures

- Mixture fraction, soot mass fraction and temperature from a single realization of the simulation at two heights.

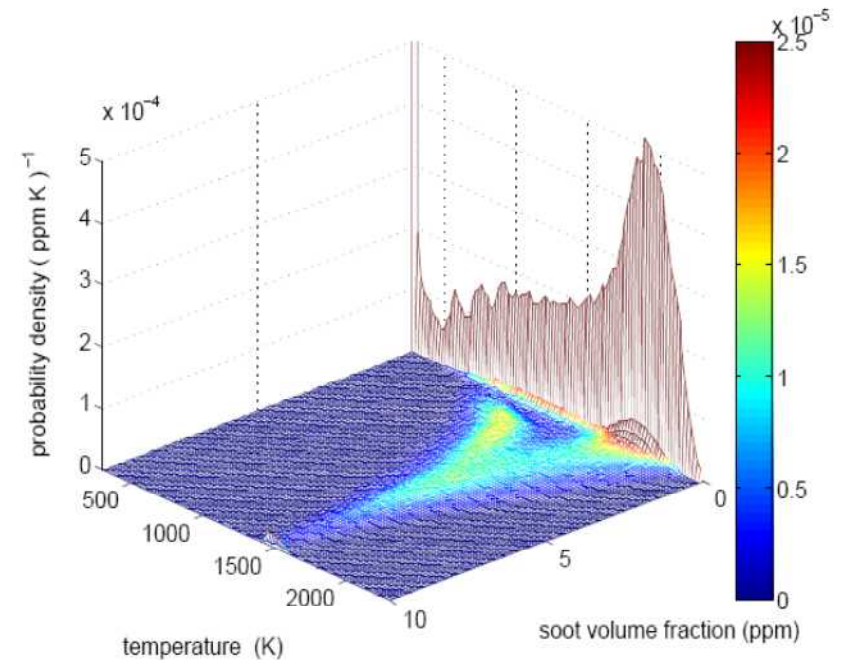


# ODT simulations provide high-fidelity data to evaluate closures



# ODT simulations provide high-fidelity data to evaluate closures

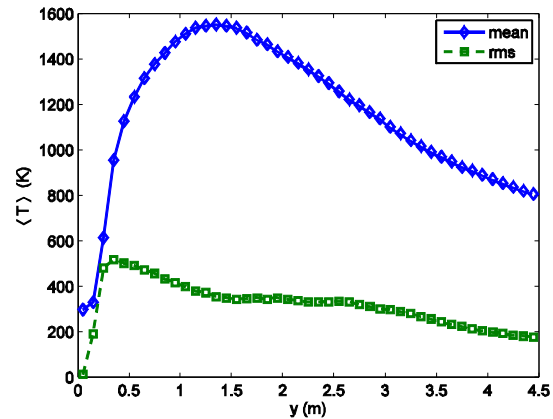
- Buoyant 1 m wide ethene plume (line fire) spatially evolving ODT simulation.
- Simple soot model (Fairweather *et al.* 1992) with steady laminar flamelet source terms tabulated by enthalpy and mixture fraction.
- Generate statistical quantities like soot-temperature joint PDF.



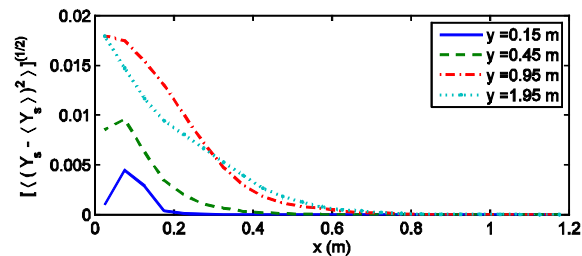
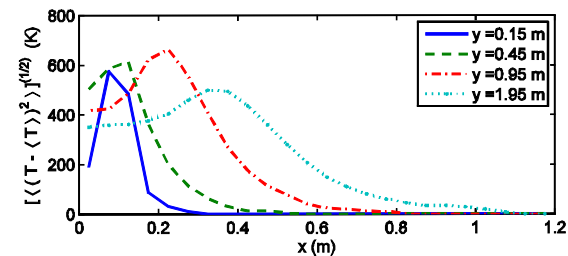
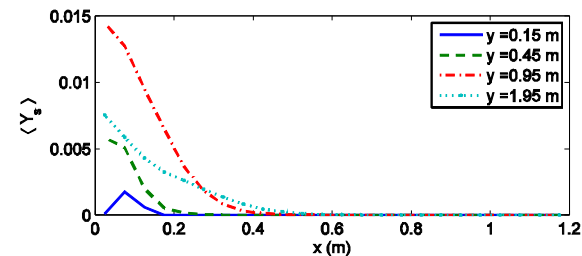
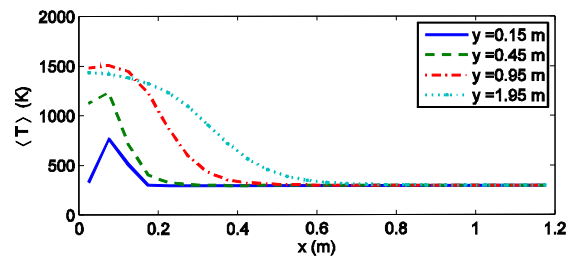
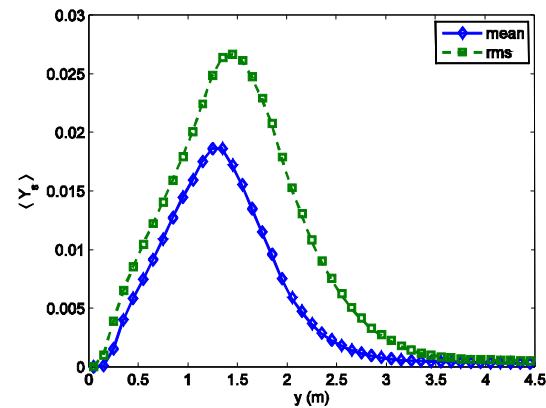


# ODT results – mean and rms evolution

## Temperature



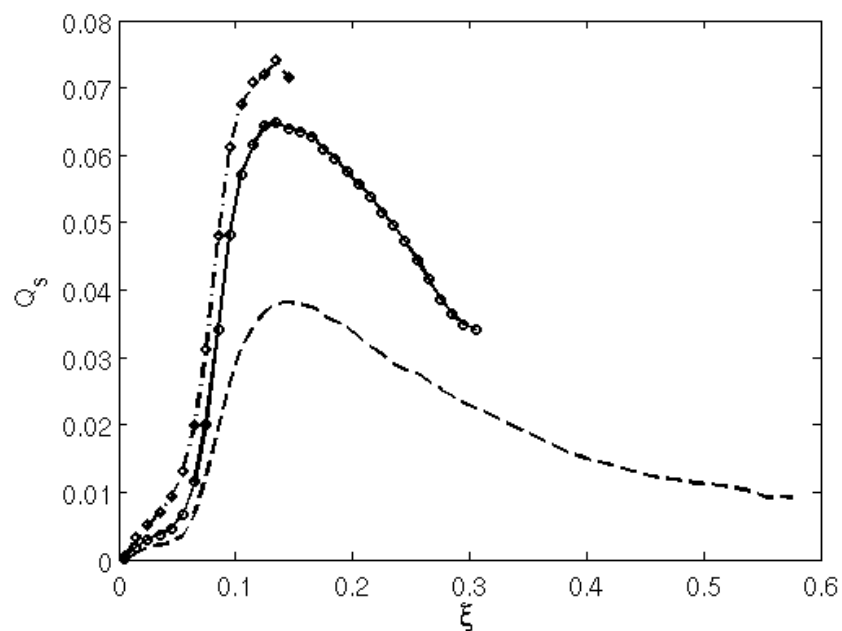
## Soot mass fractions



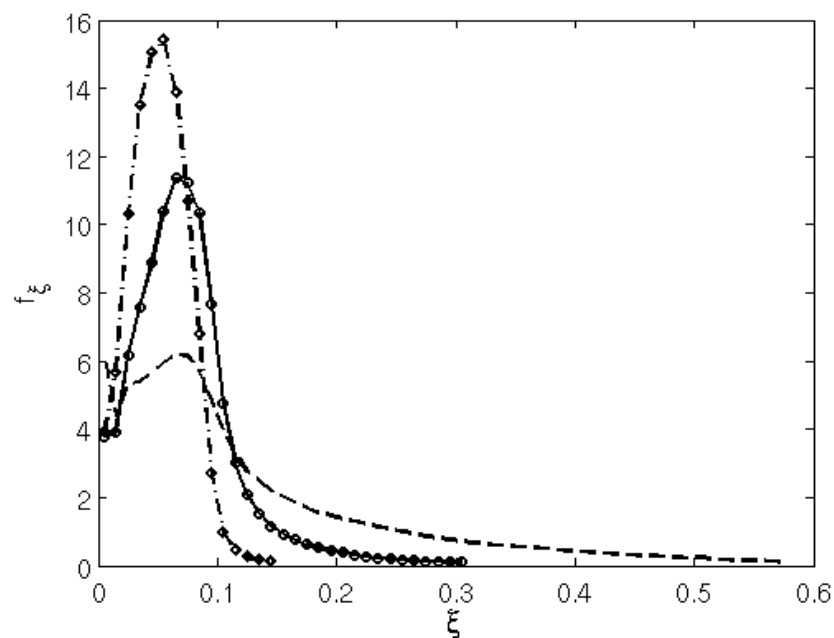
Ricks, A. J., J. C. Hewson, et al. (2010). "A spatially developing one-dimensional turbulence (ODT) study of soot and enthalpy evolution in meter-scale buoyant turbulent flames." *Combustion Science and Technology* **182**(1): 60-101.

# ODT results – conditional statistics

Soot mass fractions



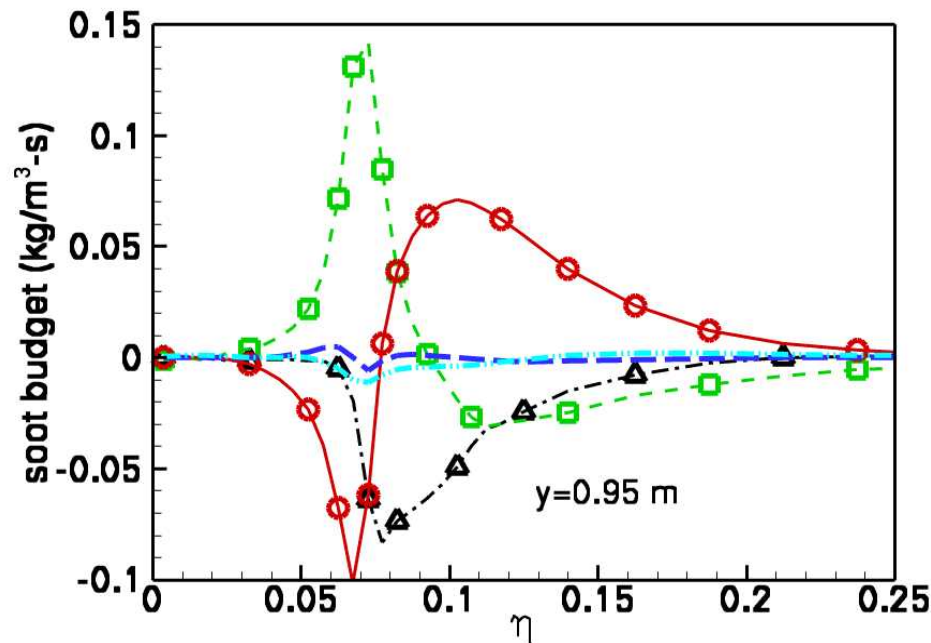
Mixture fraction PDF



heights are 0.9, 1.4 and 1.9 source widths

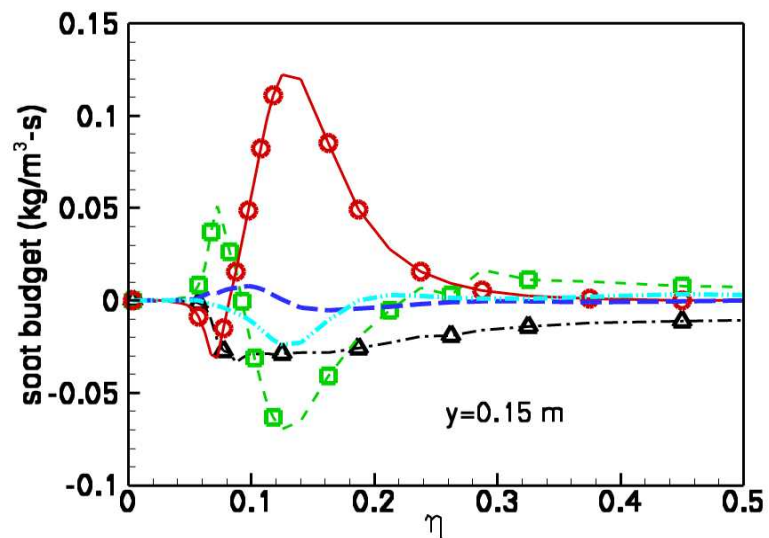
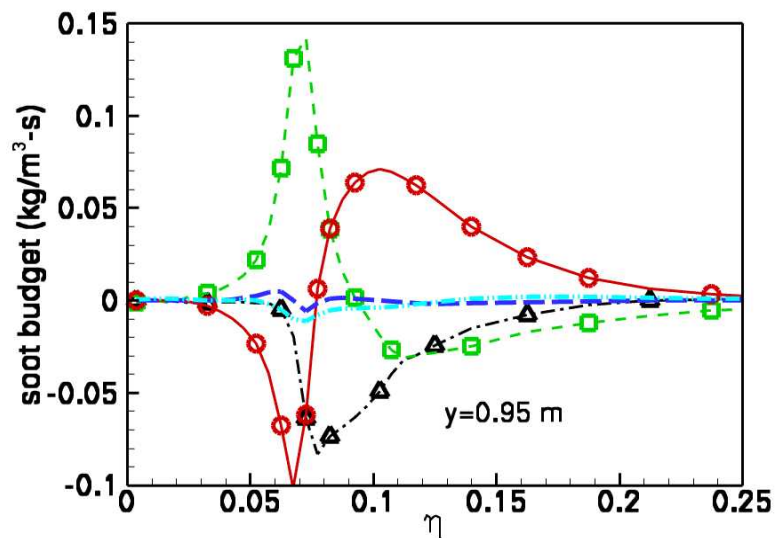
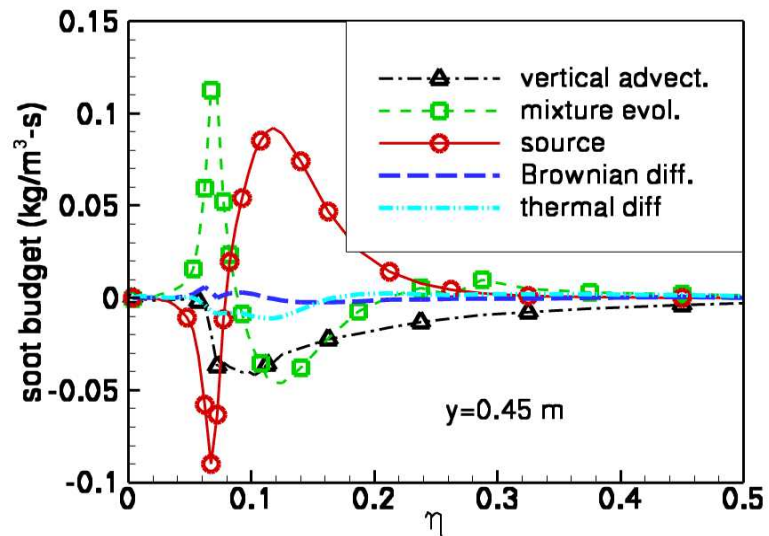
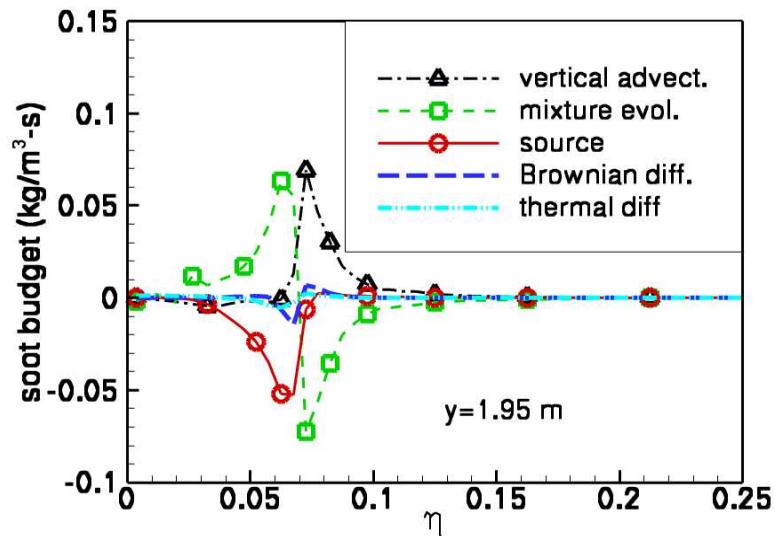
# ODT results – conditional budgets for soot

$$\begin{aligned}
 \partial_y \left( \langle \rho v Y_s | \eta \rangle P(\eta) \right) &= -\partial_x \left( \langle \rho u Y_s | \eta \rangle P(\eta) \right) && \text{advection} \\
 &+ \langle S_{Y_s} | \eta \rangle P(\eta) && \text{chemical source} \\
 &+ \langle \partial_x (\mu \partial_x Y_s) / Sc_s | \eta \rangle P(\eta) && \text{Brownian diffusion} \\
 &+ \langle \partial_x (0.55 \mu Y_s \partial_x \ln T) | \eta \rangle P(\eta) && \text{thermal diffusion} \\
 &- \partial_\eta \left[ \left\langle Y_s \left[ \partial_x \left( \frac{\mu \partial_x f_g}{Sc} \right) - S_{Y_s} - \partial_x (\rho u'_{corr,g} f_g) \right] \right| \eta \right\rangle P(\eta) \right] && \text{mixture evolution}
 \end{aligned}$$



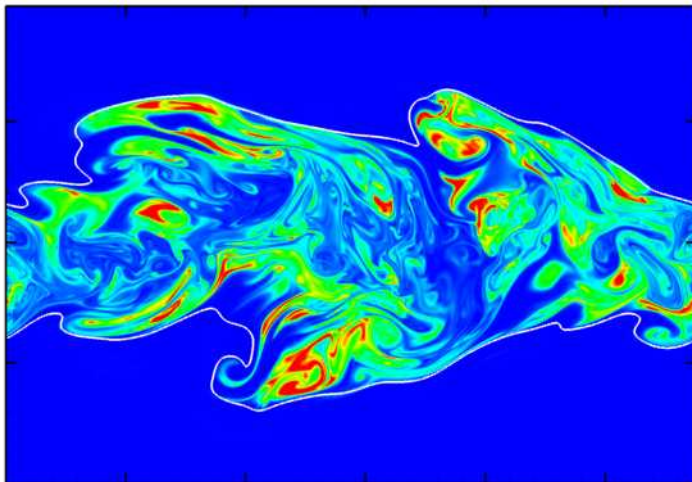
Ricks, A. J., J. C. Hewson, et al. (2010). Combust. Sci. Technol. **182**(1): 60-101.

# ODT results – conditional budgets for soot

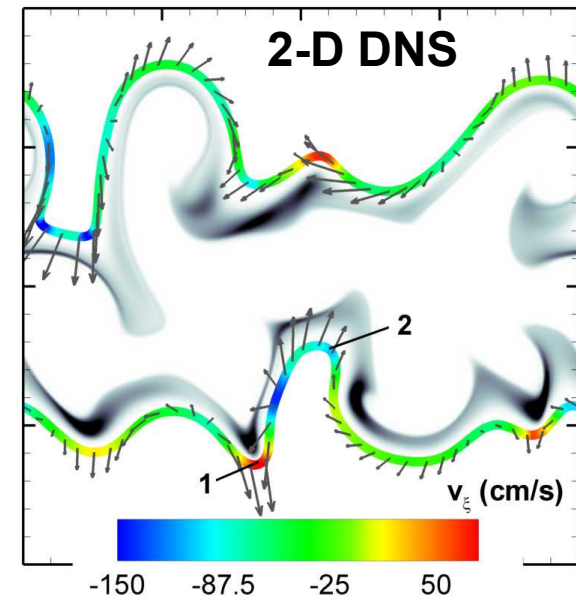


# Aerosol mixing differs from that of gases

- Soot is example of species for which differential diffusion is significant.
  - Zero soot diffusivity.
  - Mixture fraction diffuses.
- Diff-diff dominated by high wave-numbers:
  - Random directions
- More complex structure in 3-D



Vectors show flux of soot through flame



3-D DNS, Lignell



# A new CMC formulation to address differential diffusion in turbulence

- Using PDF approach to conditional-moment closure (CMC) derivation but use aerosol Lewis number (infinite) in derivation...
- Differential diffusion manifest in term

$$\frac{\partial}{\partial \eta} \left[ \left\langle \nabla \left[ \rho (D_\xi - D_k) \nabla \xi \right] Y_k \middle| \vec{\eta} \right\rangle P(\vec{\eta}) \right]$$

[Mix frac/time]
Scalar
Density

- Looks like total scalar-flux term, but in the mixture fraction coordinate.
- Closure: separate using  $\langle VY | \eta \rangle \approx \langle V | \eta \rangle \langle Y | \eta \rangle + \langle v'' y'' | \eta \rangle$

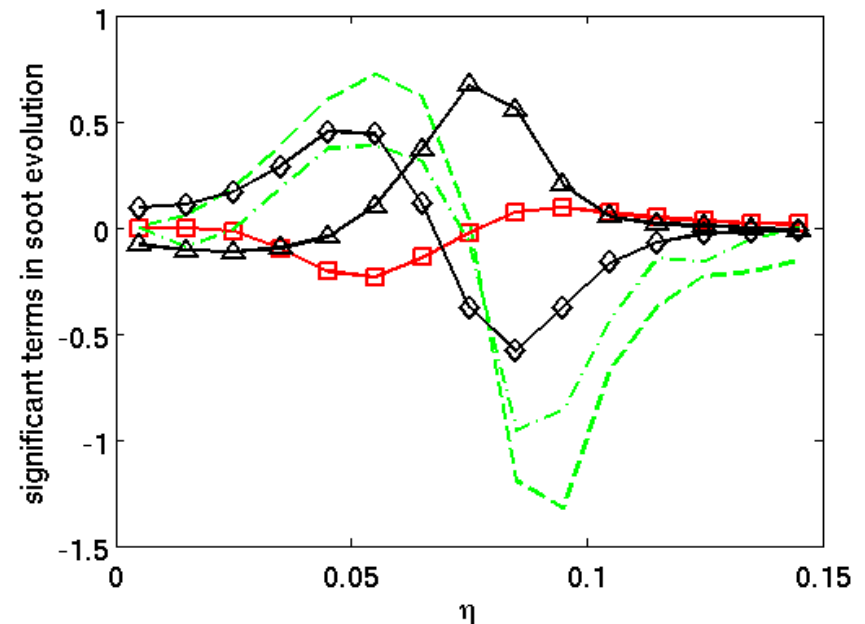
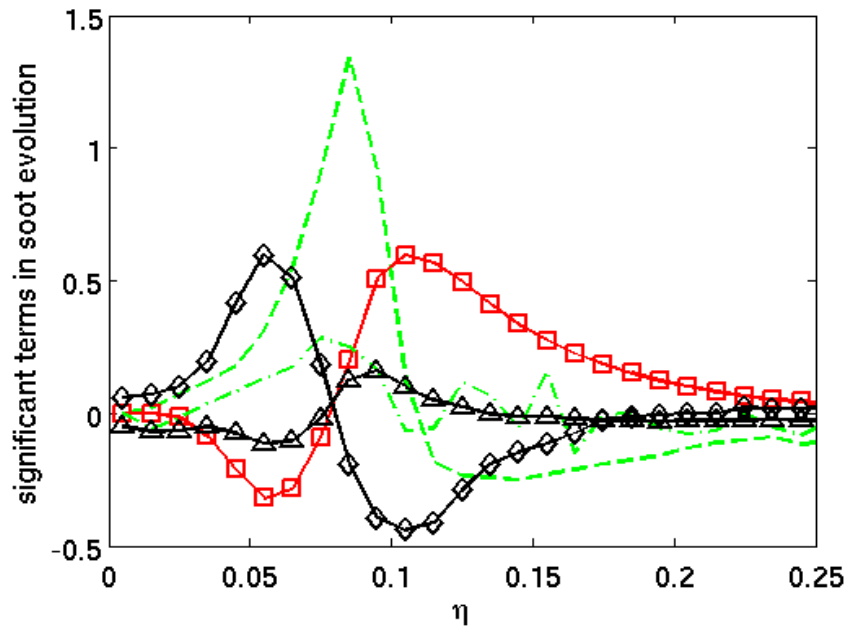
- Diff-diff flux by means related to mean PDF evolution

$$\frac{\partial}{\partial \eta} \left[ \langle V | \eta \rangle \langle Y | \eta \rangle P(\vec{\eta}) \right] = \frac{\partial}{\partial \eta} \left[ \left\langle \nabla \left[ \rho (D_\xi - D_k) \nabla \xi \right] \middle| \vec{\eta} \right\rangle P(\vec{\eta}) Q_k \right]$$

Looks like PDF evolution

# ODT results

- Terms plotted below for heights in ODT simulations where mixture fraction pdf is centered on production (left) and on oxidation (right).



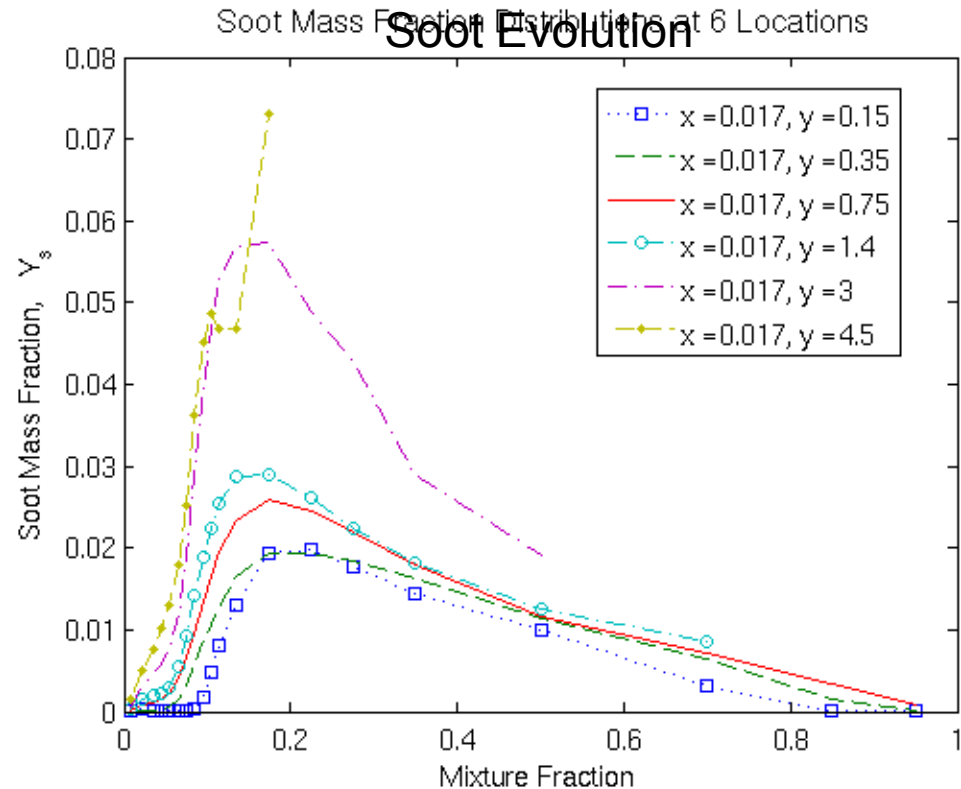
Advection (dash), pdf flux (dash-dot) -- long-term evolution of soot.

Soot source (squares).

Diff-diff by evolution of pdf (triangles) -- long-time advection in mixture fraction.

Diff-diff fluctuations  $R_{DD}$  (diamonds) -- short-time diffusion in mixture fraction.

# Soot Transport by Mean PDF



- Global fire scale PDF( $\xi$ ) evolution sweeps soot toward and then from the fuel-rich side as the PDF evolves from rich to lean.

# Closure for new CMC formulation to address differential diffusion in turbulence

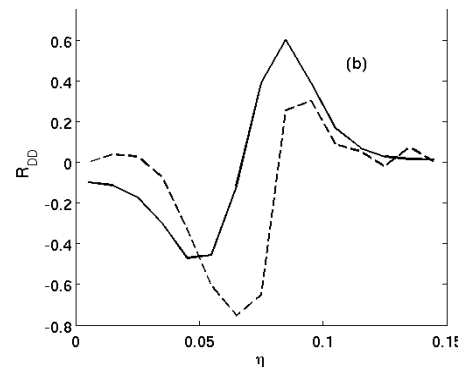
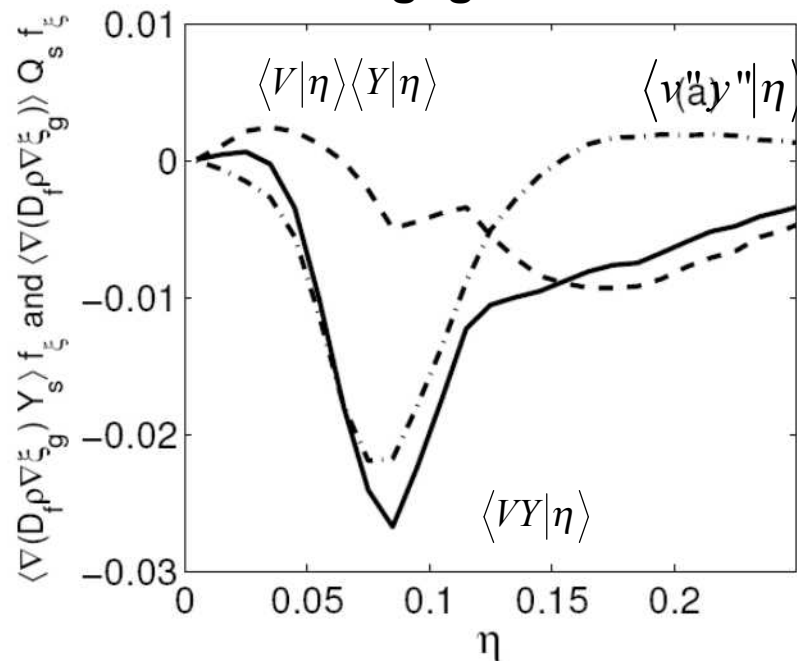
- Prior slides demonstrated primary closure of diff-diff term, but residual (fluctuations) are also important.

$$\langle v'' y'' | \eta \rangle \approx \langle V | \eta \rangle \langle Y | \eta \rangle - \langle VY | \eta \rangle$$

- Diff-diff dominated by high wave-number structures:
  - Random directions
  - Like turbulent scalar flux in mixture-fraction coordinate.
  - Model as diffusion process

$$R_{DD} = \frac{\partial}{\partial \eta} \langle v'' y'' | \eta \rangle \approx \frac{\rho_\eta \chi_\eta f_\xi}{2Le_{DD,t}} \frac{\partial^2 Q_s}{\partial \eta^2}$$

Non-negligible residual



# Summary: A new CMC evolution equation for soot and other species with strong diff-diff

$$\frac{\partial Q_s}{\partial t} + \langle \vec{u} | \eta \rangle \cdot \nabla Q_s = \langle \omega_s | \eta \rangle$$

Species Source Term

$$+ \frac{\langle \chi | \eta \rangle}{2\text{Le}_s} \frac{\partial^2 Q_s}{\partial \eta^2}$$

Species Diffusion

$$+ \frac{1}{2\rho_\eta f_\xi(\eta)} \frac{\partial}{\partial \eta} \left[ \rho_\eta \left( \frac{1}{\text{Le}_s} - 1 \right) \langle \chi | \eta \rangle f_\xi(\eta) \right] \frac{\partial Q_s}{\partial \eta}$$

Transport by PDF evolution

Current Focus

$$+ \left( 1 - \frac{1}{\text{Le}_s} \right) \frac{\langle \chi | \eta \rangle}{2\text{Le}_{\text{DD}}} \frac{\partial^2 Q_s}{\partial \eta^2}$$

Turbulent differential diffusion

+other terms

- Derived from combined PDF and soot conservation equations without the primary closure hypotheses.
- Turbulent diffusion term is new model from Hewson et al.
- Some definitions for above:

$$Q_s \equiv \langle Y_s | \eta \rangle \quad \langle \chi | \eta \rangle \equiv \langle 2D(\nabla \xi)^2 | \eta \rangle \quad f_\xi(\eta) \text{ is PDF}(\xi)$$



# Backup slides

# Soot transport in and out of flames

- Soot diffusion is
  - Slow relative to gas-phase species.
  - Affected by thermophoresis, etc.
- Soot is convected along with everything else.
- Flames diffuse!
  - Diffuse towards location of nearest mixture fraction extrema.

**z**

**y**

**Flame diffuses in**

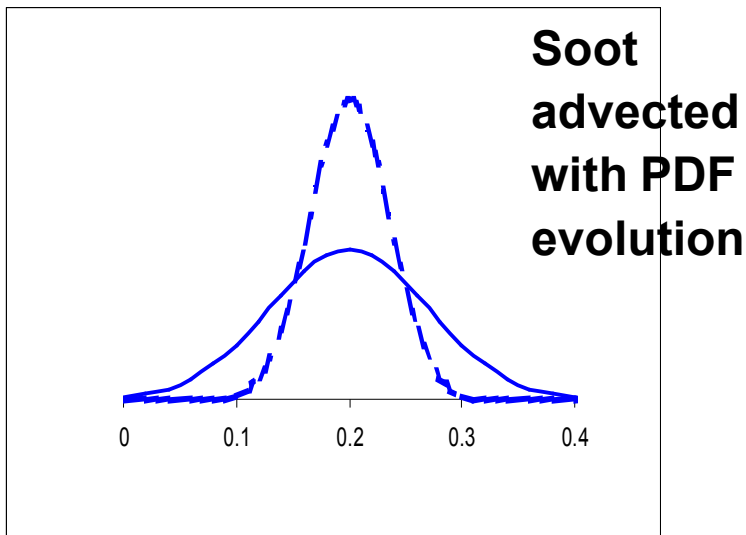
**z**

**y**

**Flame diffuses out**

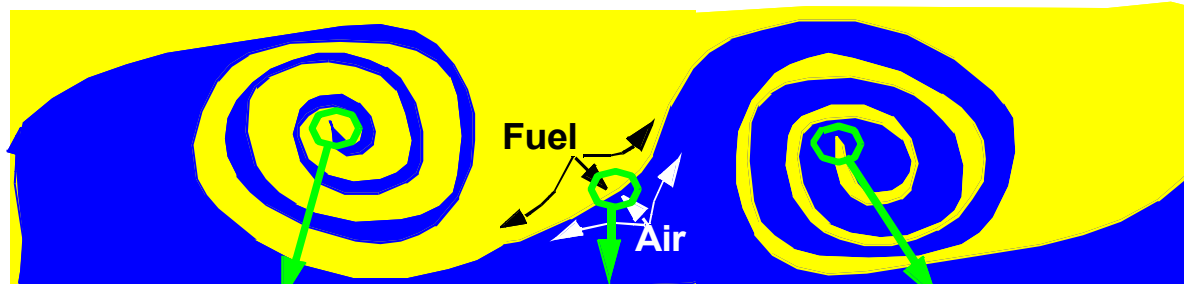
# Soot advection in mixture fraction space

- How does soot advection work in turbulent flows?
  - In CMC-based approach there is advection in the mixture fraction coordinate.
  - Candle analogy suggests mean behavior: Related to evolution of mixture fraction PDF.



$$\frac{\partial}{\partial \eta} \left\langle \nabla \cdot \left( \rho (D_\xi - D_k) \nabla \xi \right) Y_k \mid \vec{\eta} \right\rangle P(\vec{\eta})$$
$$\approx \frac{\partial}{\partial \eta} \left[ \left\langle \nabla \cdot \left( \rho (D_\xi - D_k) \nabla \xi \right) \mid \vec{\eta} \right\rangle P(\vec{\eta}) Q_k \right]$$

# Advection due to mixture fraction fluctuations



$z$

Burnout of lean regions forces flame to diffuse away from soot.



Burnout of rich regions forces flame to diffuse into soot.

$y$

What are the statistics for burn out of rich or lean mixtures?

