



Quantifying the impact of viscosity variations induced by a chemical reaction on mixing efficiency in porous media



Center for Frontiers of
Subsurface Energy Security

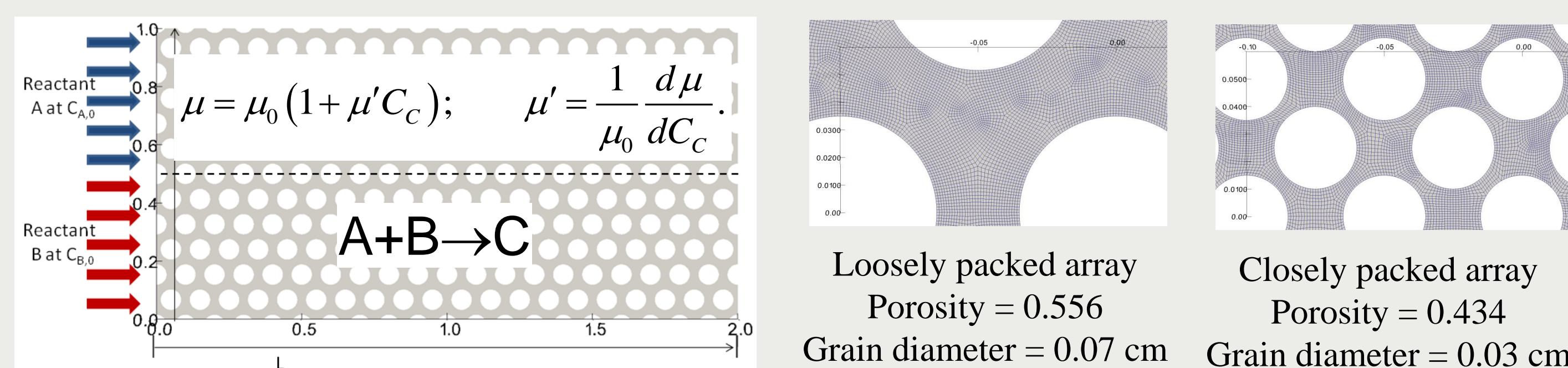
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Overview

- Mixing-induced reacting flows in porous media can be used to develop subsurface flow for enhanced subsurface natural resource recovery and carbon sequestration
- In this work, we examine the case of reaction products that change the viscosity of the fluid to evaluate :
 - the impact of viscosity variations on mixing efficiency in porous media
- Computationally powerful & highly parallelized pore-scale model implemented in the SIERRA/ARIA finite element CFD code is used to examine:
 - flow in porous media with chemical reaction dependent viscosity

Pore Scale Modeling

- Mixing-induced chemical reactions can alter fluid properties (viscosity and density), mixing efficiency, and shear rate for engineered solutions



Incompressible Navier-Stokes equation: Velocity (u) at pore scale

Multicomponent Reactive Transport at pore scale

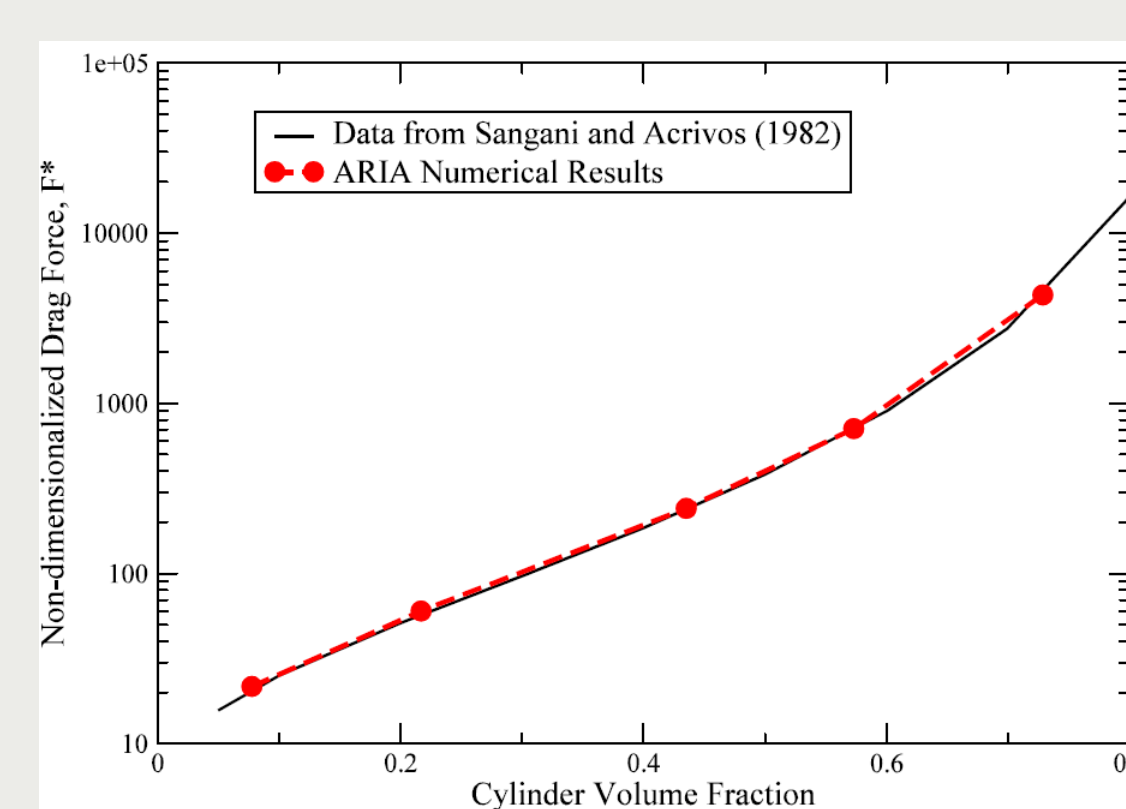
$$\begin{aligned} \left(\frac{\partial}{\partial t} + \mathbf{u} \cdot \nabla \right) C_A &= D_A \nabla^2 C_A - k C_A C_B \\ \left(\frac{\partial}{\partial t} + \mathbf{u} \cdot \nabla \right) C_B &= D_B \nabla^2 C_B - k C_A C_B \\ \left(\frac{\partial}{\partial t} + \mathbf{u} \cdot \nabla \right) C_C &= D_C \nabla^2 C_C + k C_A C_B \end{aligned} \Rightarrow \begin{aligned} \left(\frac{\partial}{\partial t} + Pe \mathbf{u} \cdot \nabla \right) C_A &= \delta_A \nabla^2 C_A - Da C_A C_B \\ \left(\frac{\partial}{\partial t} + Pe \mathbf{u} \cdot \nabla \right) C_B &= \delta_B \nabla^2 C_B - Da C_A C_B \\ \left(\frac{\partial}{\partial t} + Pe \mathbf{u} \cdot \nabla \right) C_C &= \nabla^2 C_C + Da C_A C_B \end{aligned}$$

$$Pe = \frac{U l}{D_C} \quad Da = \frac{k C_{A0} l^2}{D_C} \quad \delta_A = D_A/D_C \quad \delta_B = D_B/D_C$$

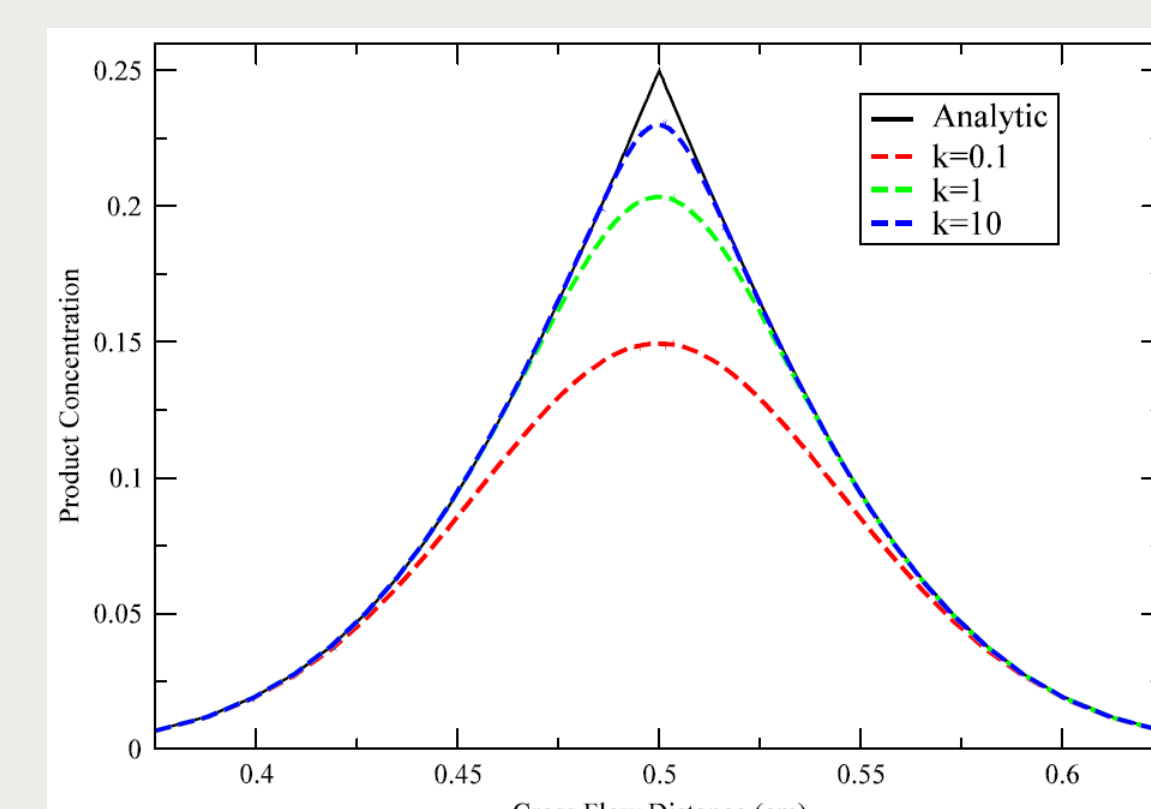
Fluid Viscosity Update

$$\bar{\mu} = \mu/\mu_0 = 1 + \bar{\mu}' C_C \quad \bar{\mu}' = \frac{C_{A0}}{\mu_0} \frac{d\mu}{dC_C}$$

Drag force on an array of cylinders



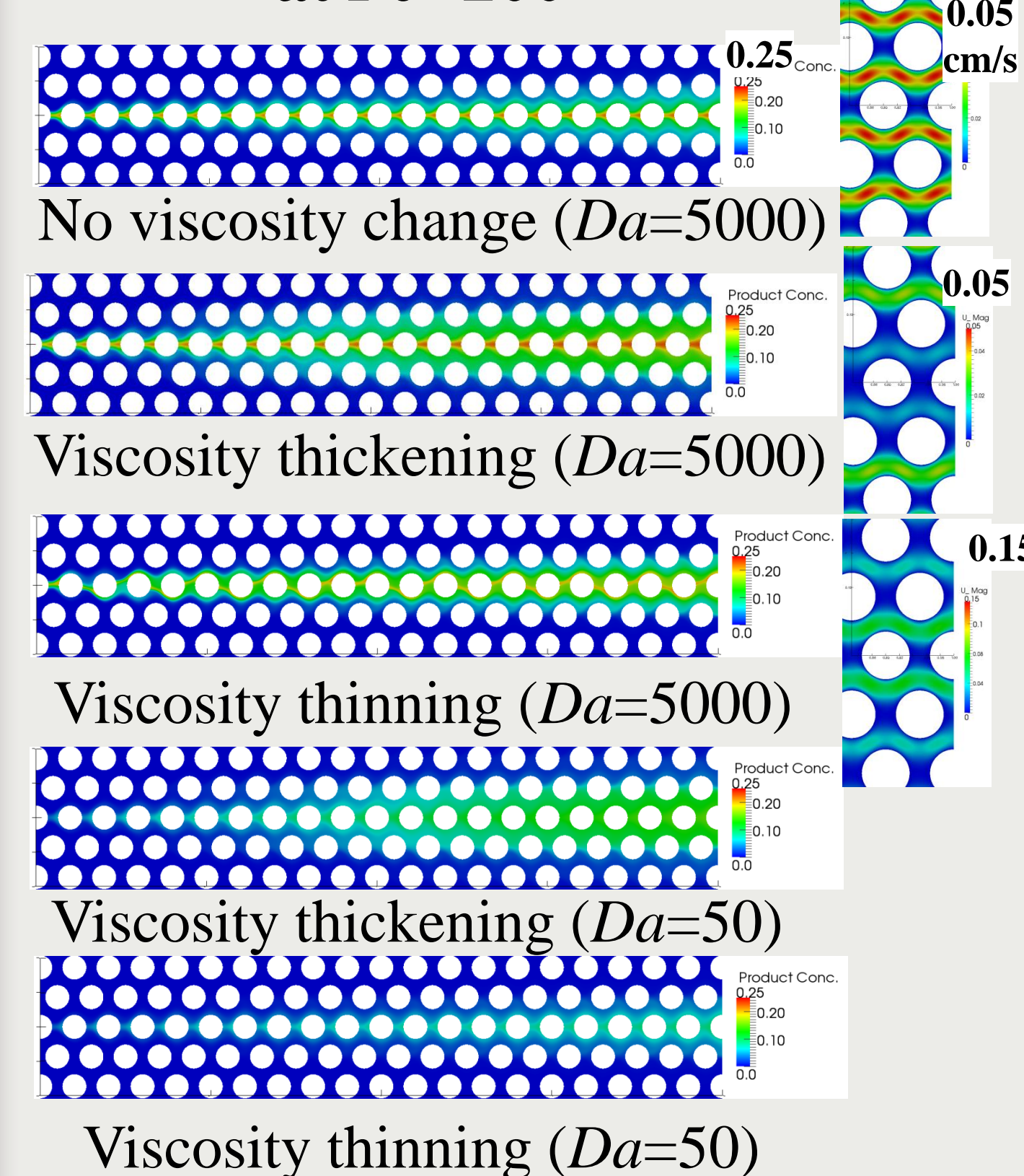
Reaction along a transverse mixing zone with constant viscosity



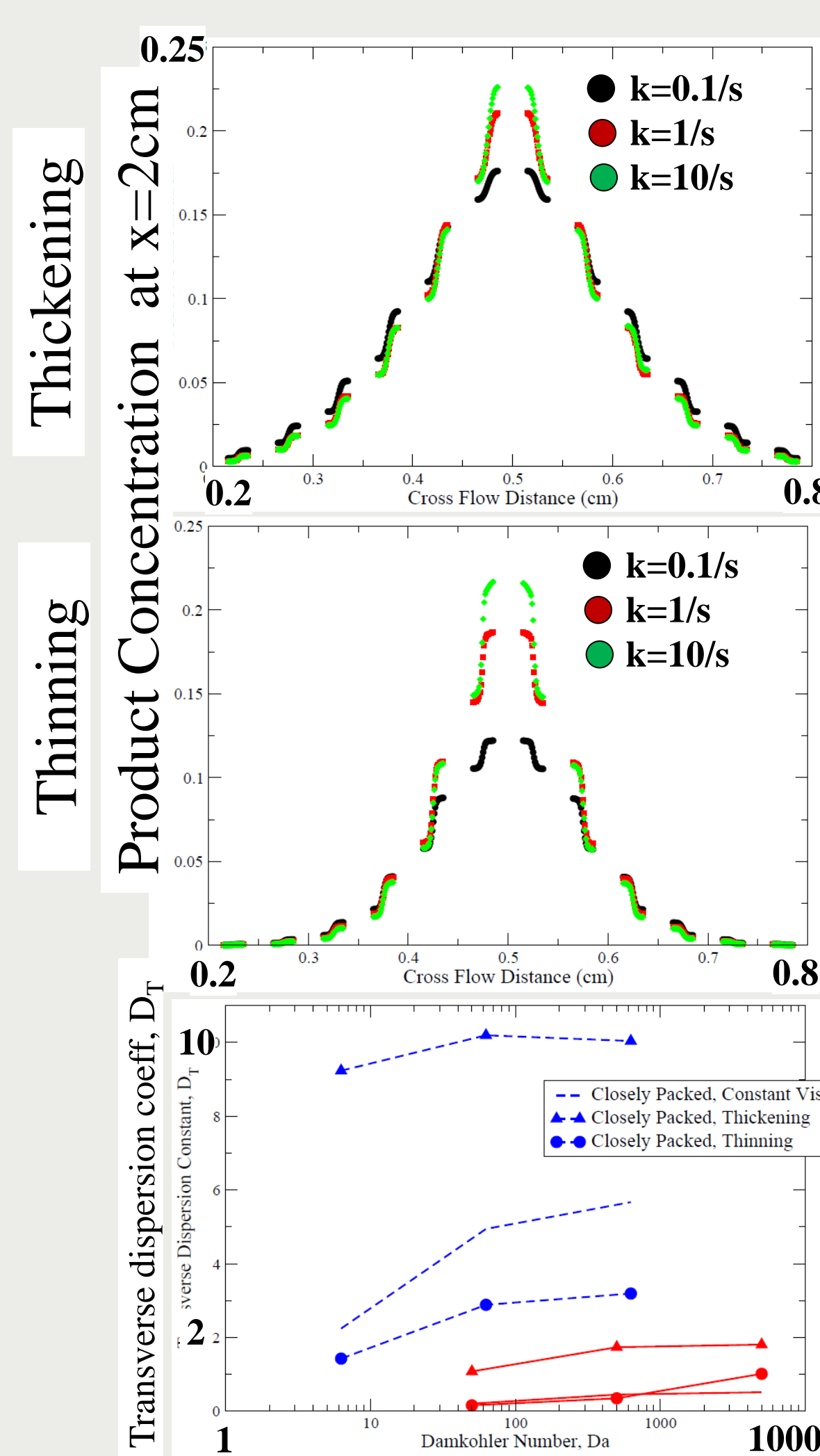
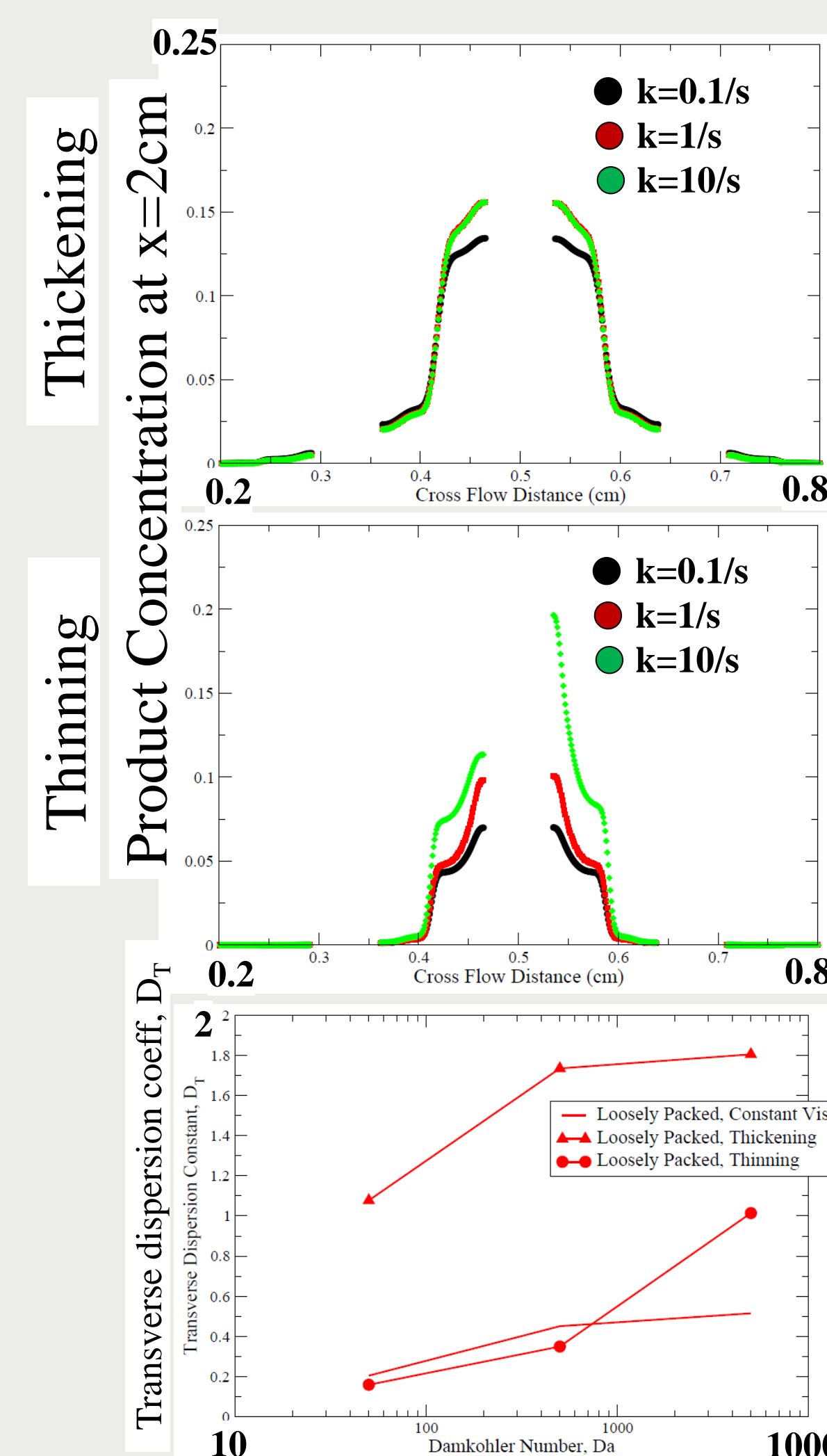
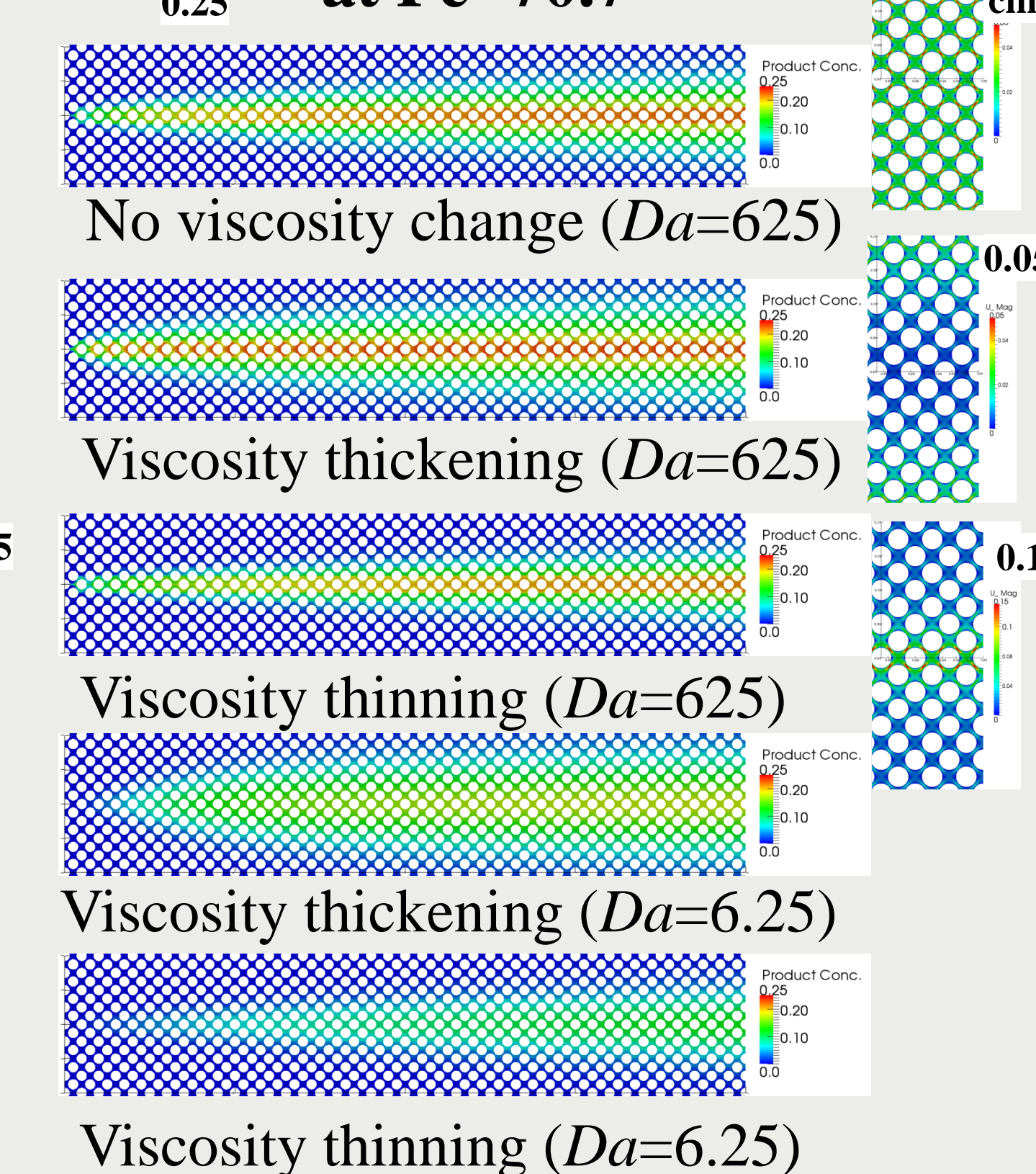
Pore Scale Modeling Results

Product concentration and flow velocity change

Loosely packed array at $Pe=200$



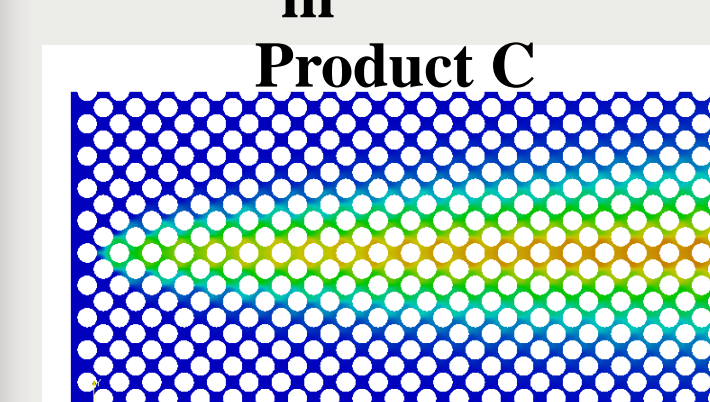
Closely packed array at $Pe=70.7$



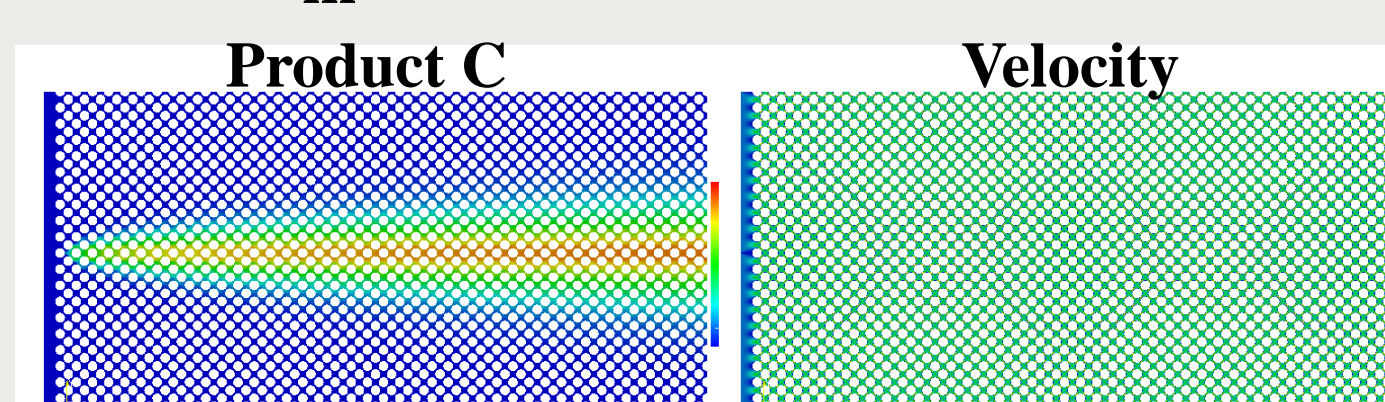
- More reaction product was formed when fluid viscosity increases with increasing product concentration (viscous thickening) than the opposite case (viscous thinning)
- Enhanced mixing at pore scale leads to enhanced reaction rates at high Da and lower porosity due to the higher interfacial area and smaller diffusion time scale
- Thinning viscosity creates flow focusing along the mixing line, resulting in streamline compression and lower transverse dispersion
- Flows with viscous thinning reactions can become unstable at high Da , leading to enhanced mixing and reaction rates under high Pe and higher porosity

$Pe=7$ & $Da=62.5$

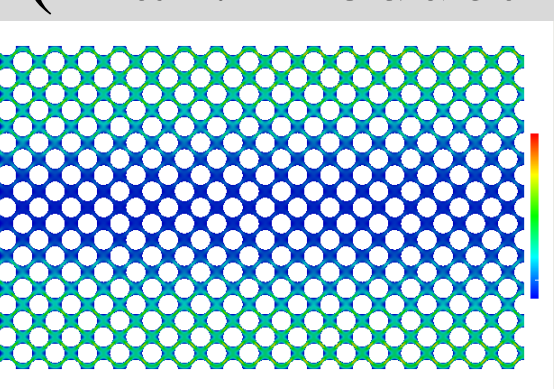
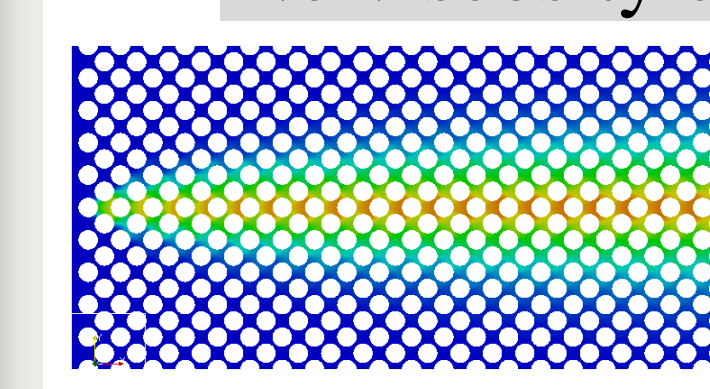
$U_{in}=0.01\text{cm/s}$ & $k=2.5/\text{s}$



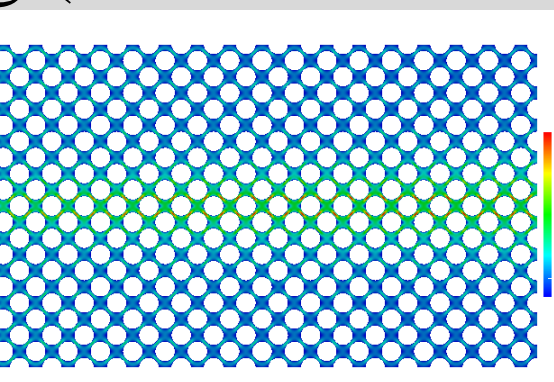
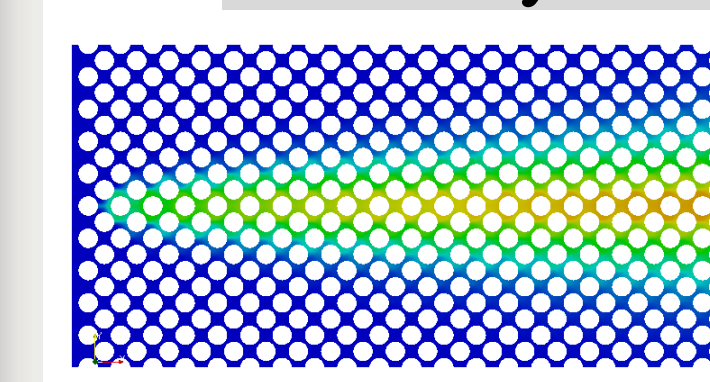
$U_{in}=0.02\text{cm/s}$ & $k=10/\text{s}$



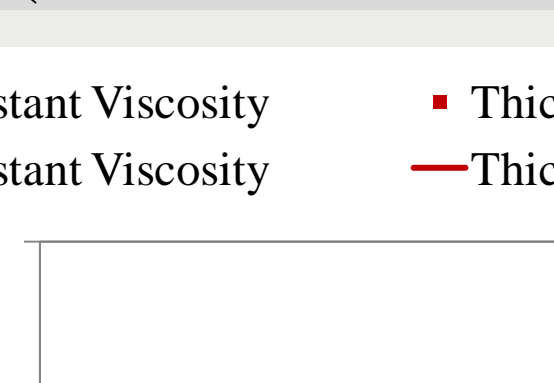
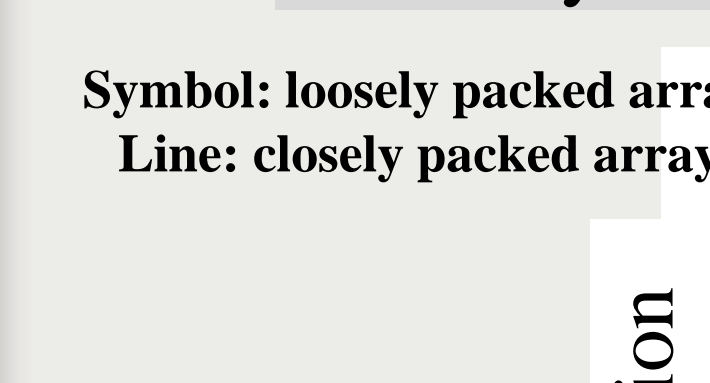
No viscosity change (Max. Product C=0.25; Max velocity=0.15cm/s)



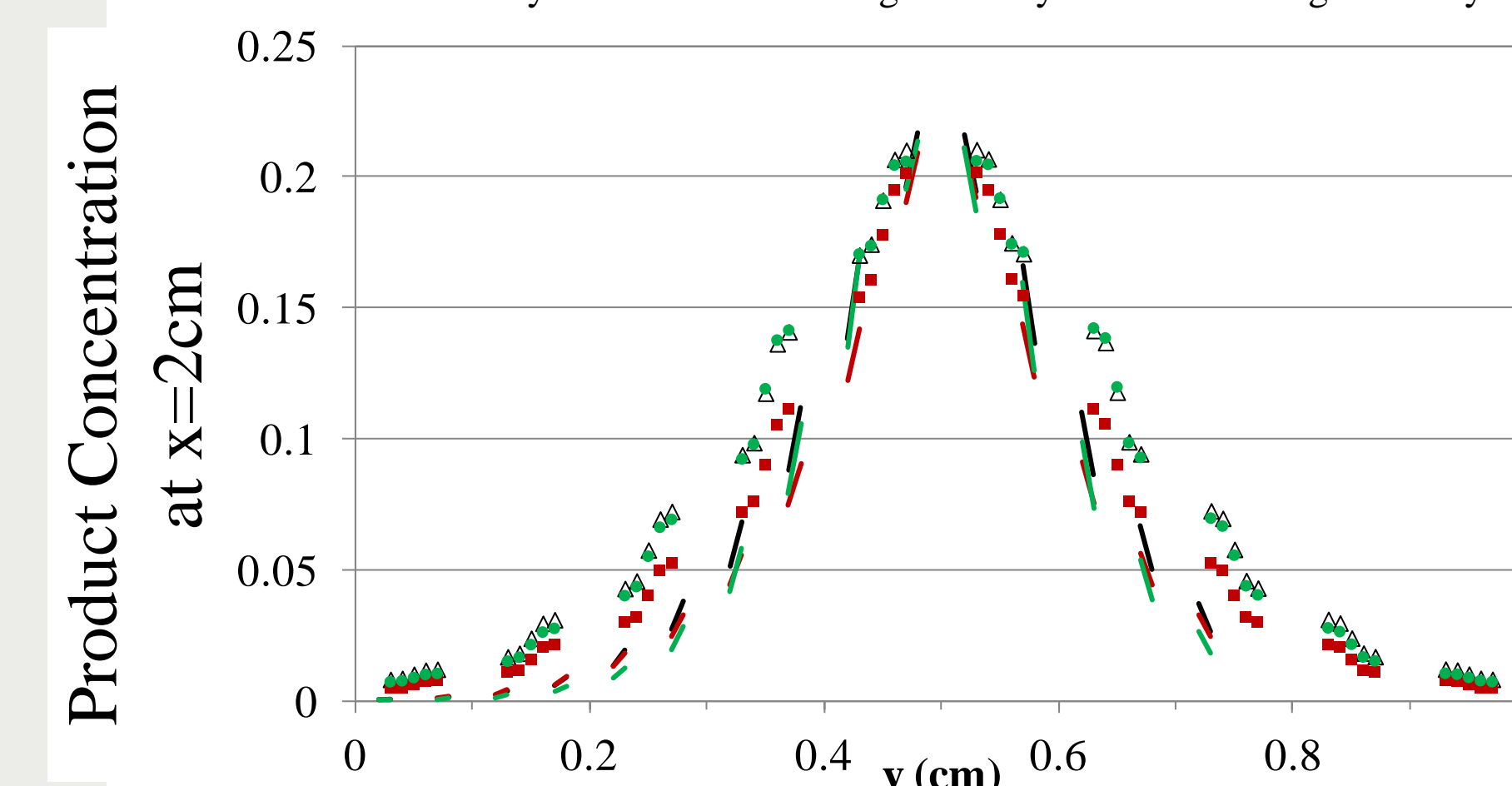
Viscosity thickening (Max. Product C=0.25; Max velocity=0.15cm/s)



Viscosity thinning (Max. Product C=0.25; Max velocity=0.15cm/s)

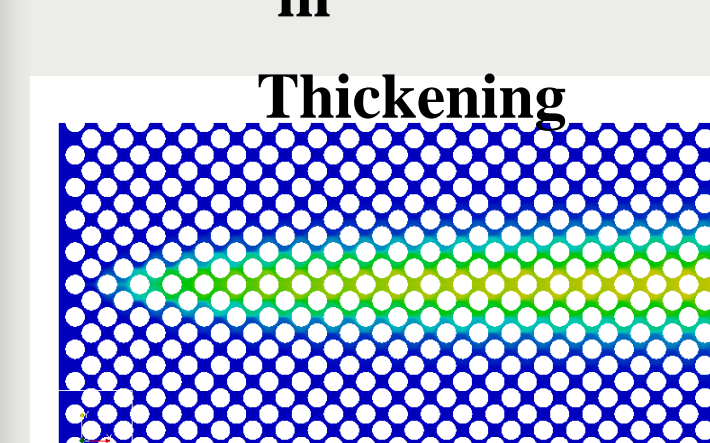


Symbol: loosely packed array Δ Constant Viscosity \square Thickening Viscosity \circ Thinning Viscosity
Line: closely packed array \square Constant Viscosity \square Thickening Viscosity \square Thinning Viscosity

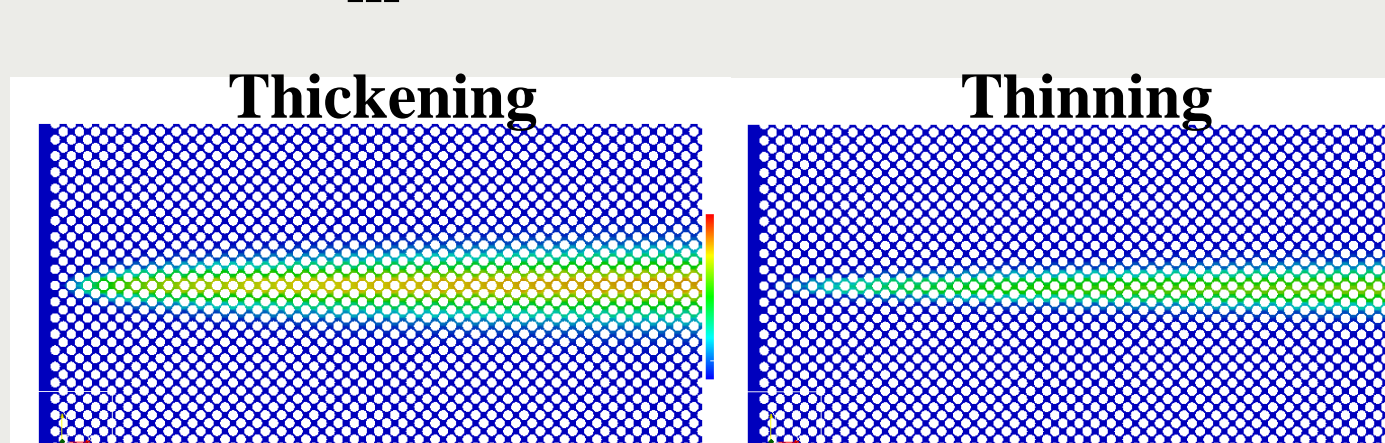


$Pe=70$ & $Da=62.5$

$U_{in}=0.01\text{cm/s}$ & $k=0.25/\text{s}$



$U_{in}=0.02\text{cm/s}$ & $k=1/\text{s}$



- At $Pe=7$ and $Da=62.5$, the effect of viscosity variations on product concentration at the end of domain was minimal in both packed arrays
- At $Pe=70$ and $Da=62.5$, the effect of viscosity variations on product concentration is significant in both packed arrays
- This comparison shows that at a moderate Da (62.5) a case with the lower Pe has more significant dependence of the overall reaction rate on Pe . A range of Da and Pe values need to be tested.

- Pore scale model with high performance computing capability will be used to test experimental results with emulsion-stabilizing nanoparticles in order to find optimal delivery of engineered solutions under a variety of pore-geometry conditions

References: • Davison, S. M., H. Yoon, and M. J. Martinez, 2012, Pore scale analysis of the impact of mixing-induced reaction on viscosity variations, Advances in Water Resources, 38, 70-80.