

# Used Fuel Disposition Campaign

## Corrosion Related Experimental Work

**David Enos, Charles Bryan**  
**Sandia National Laboratories**

**Neil Brown**  
**Los Alamos National Laboratory**

**UFD Workshop**  
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## **Summary of Work in Progress**

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- **Two experimental programs are currently underway, with two very different goals**
  - Legacy experiments
  - Localized corrosion experiments under deliquescent conditions
- **Both experiments are applicable to a wide variety of potential interim and long-term repository solutions**

## Long Term Immersion Tests

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### ■ Initiated in 2010

- Opportunity cost associated with halting experiments was high – an alternative funding source was located to maintain the experiments at a maintenance level (i.e., no sample pulls or analyses)
- Experiments being performed on Hastelloy C22 (i.e., “Alloy 22”) in two environments from previous studies (simulated acidified water (SAW) and simulated concentrated water (SCW)) and one generic environment (0.5M NaCl) at three temperatures
- Goal: establish a general corrosion rate and temperature dependence which is free from the significant experimental uncertainties of previously generated data..

### ■ Details

- Samples polished to a mirror finish and pickled/passivated prior to exposure
- Exposure flasks are inert (glass) and care has been taken to avoid contamination with organics or other materials

### ■ Current Status

- Specimens pulled at 3, 9, 18, and 24 months.
- Weight change and surface condition being assessed
- Experimental program will be concluded with a final report to be issued at the end of 3Q12

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## Pourbaix Diagram for Cr in Chloride Containing Solutions

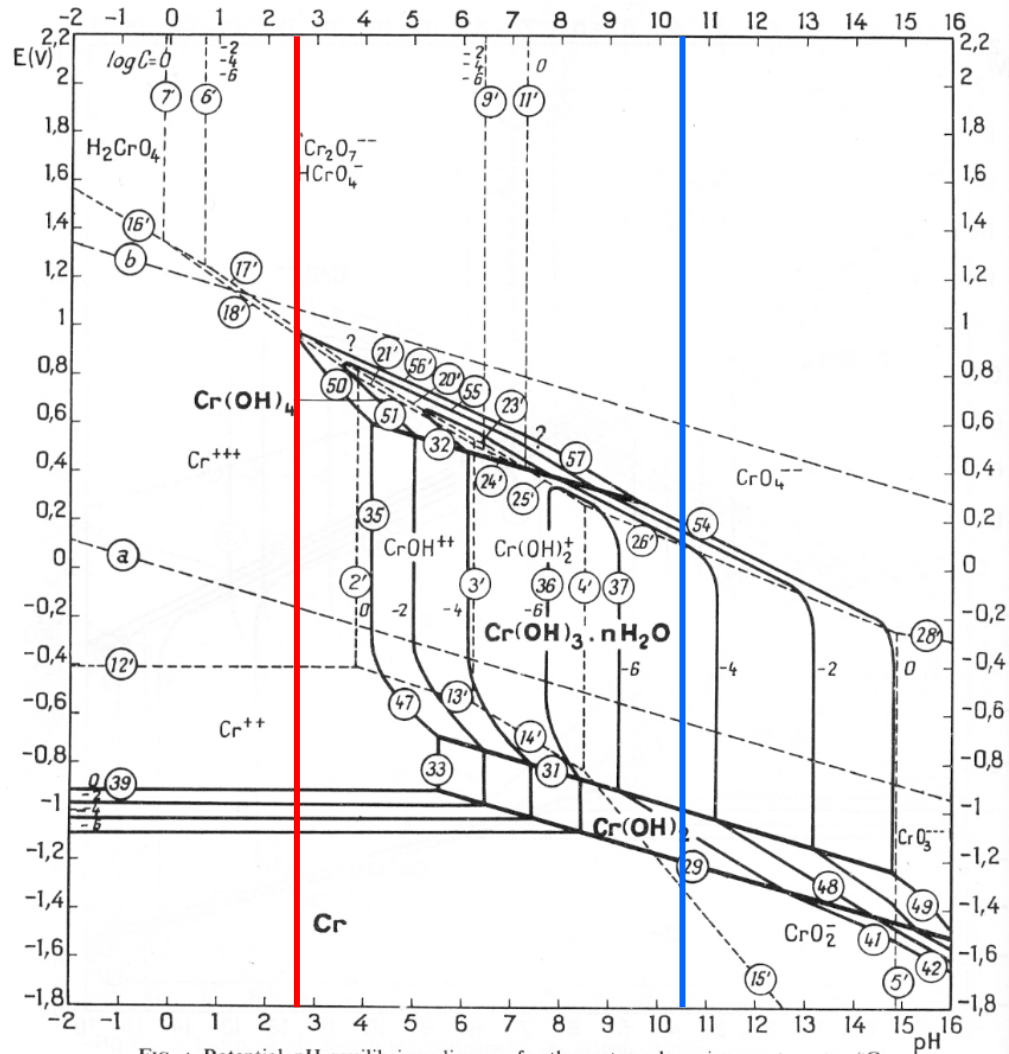
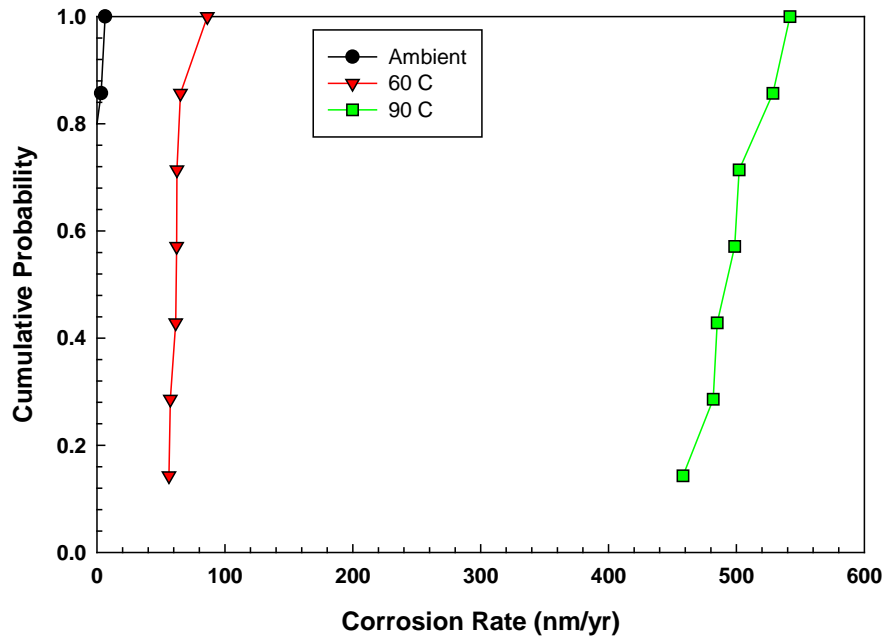


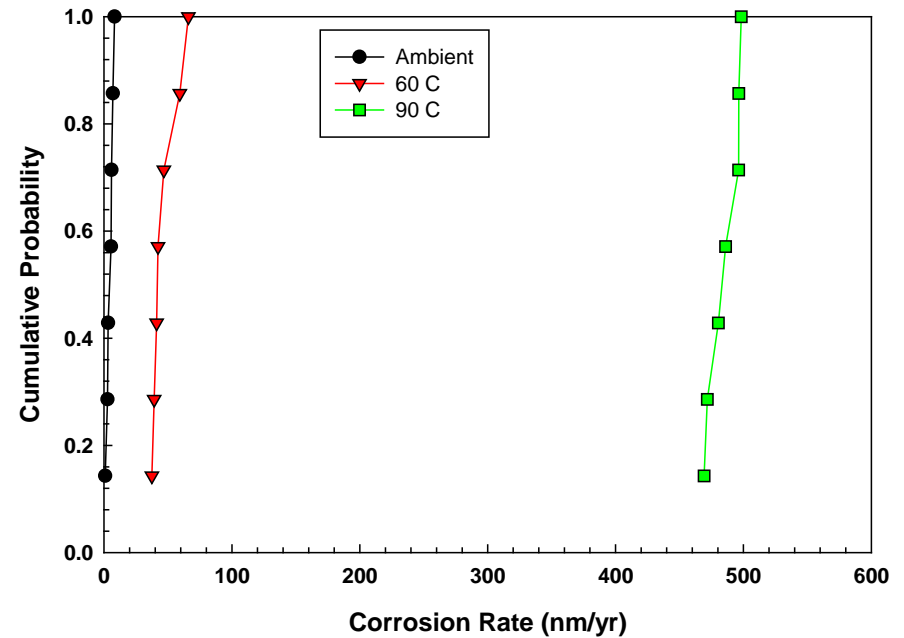
FIG. 4. Potential-pH equilibrium diagram for the system chromium-water, at 25°C.  
In solutions containing chloride.  
[Approximate representation made by considering  $\text{Cr(OH)}_3 \cdot n\text{H}_2\text{O}$ .]

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## SAW 3 and 9 month



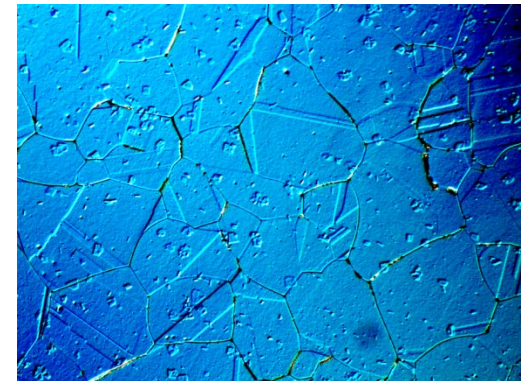
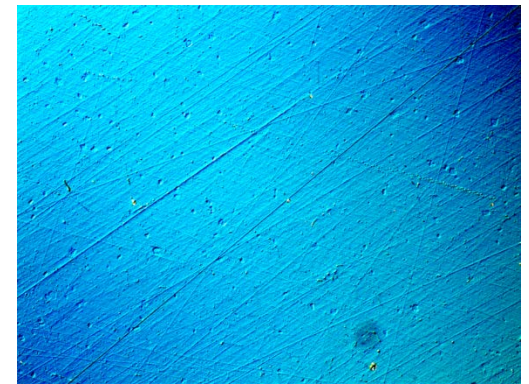
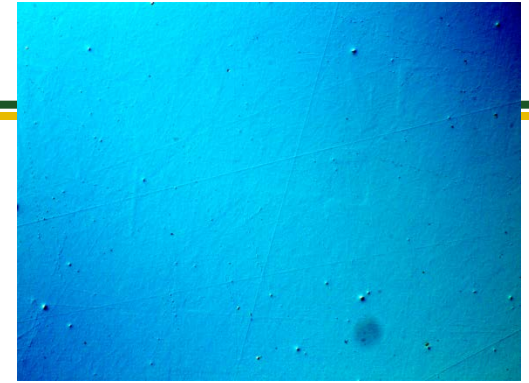
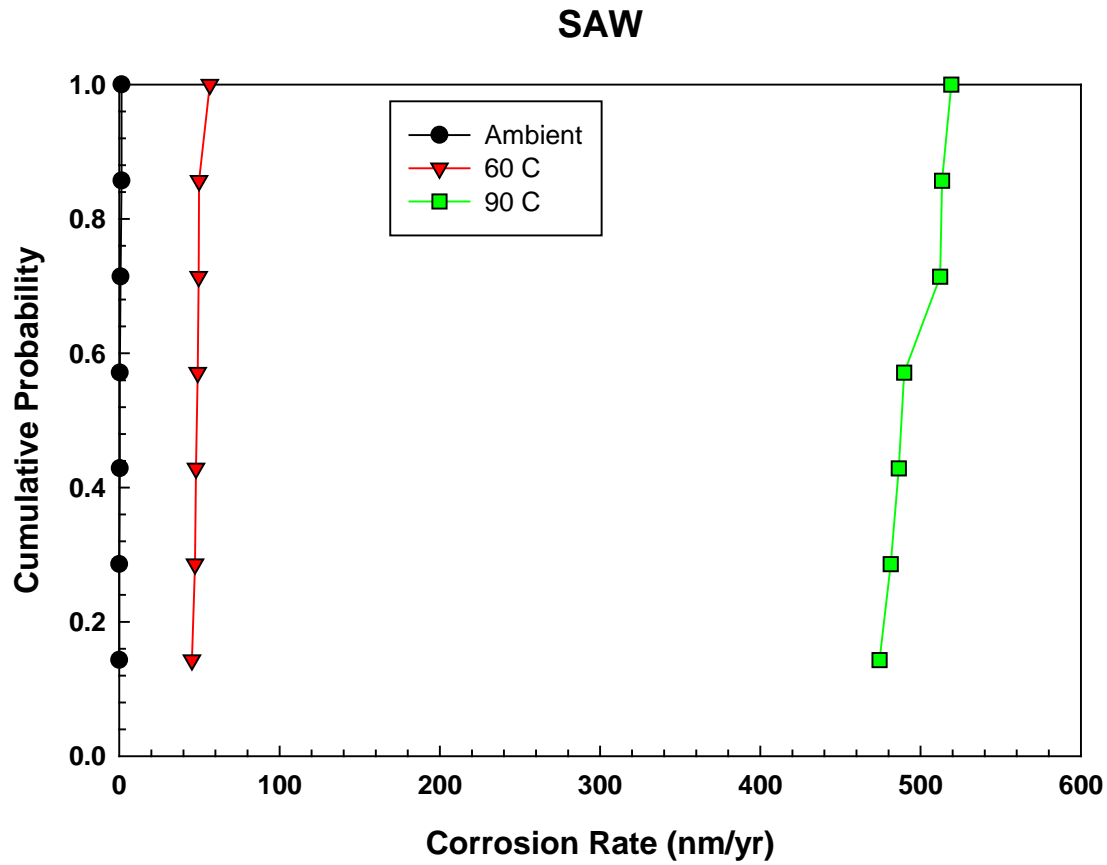
3 month



9 month

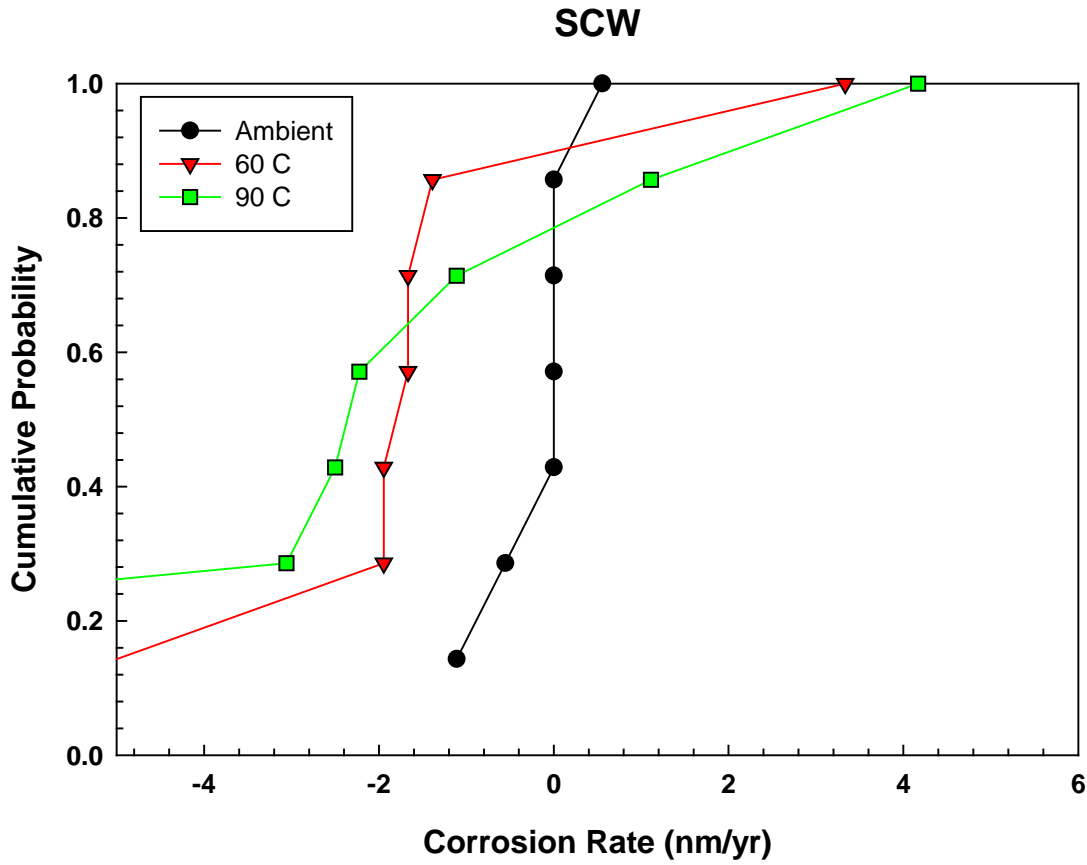
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## SAW 18 month



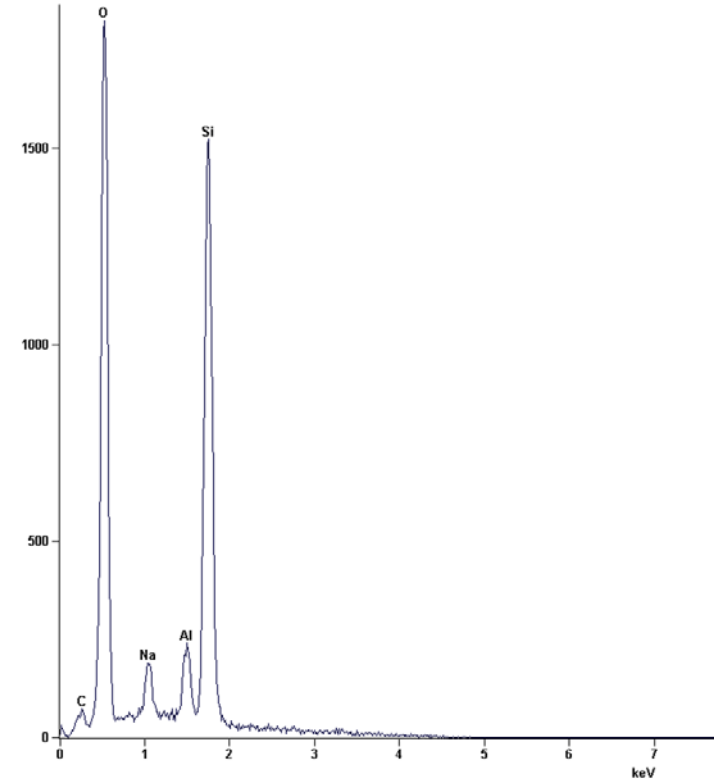
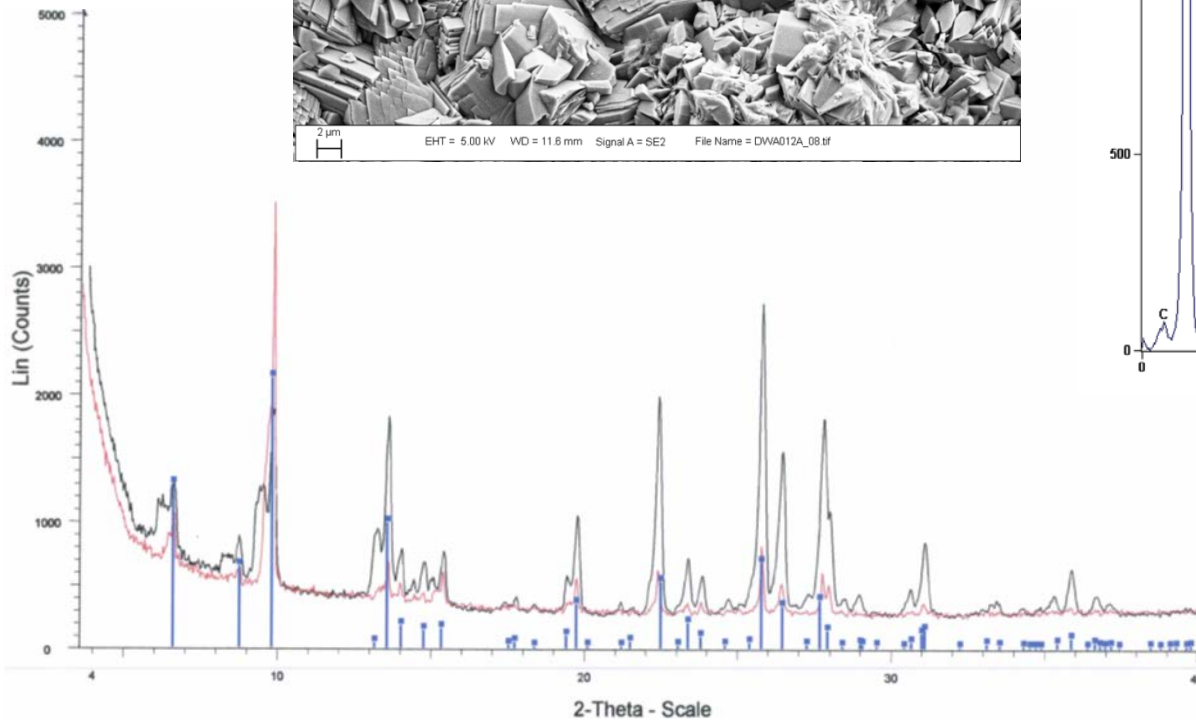
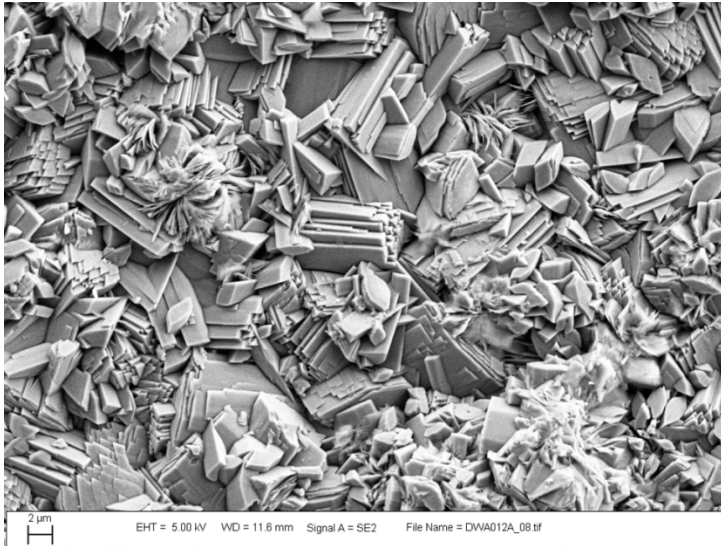
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SCW 18 month



# Used Fuel Disposition

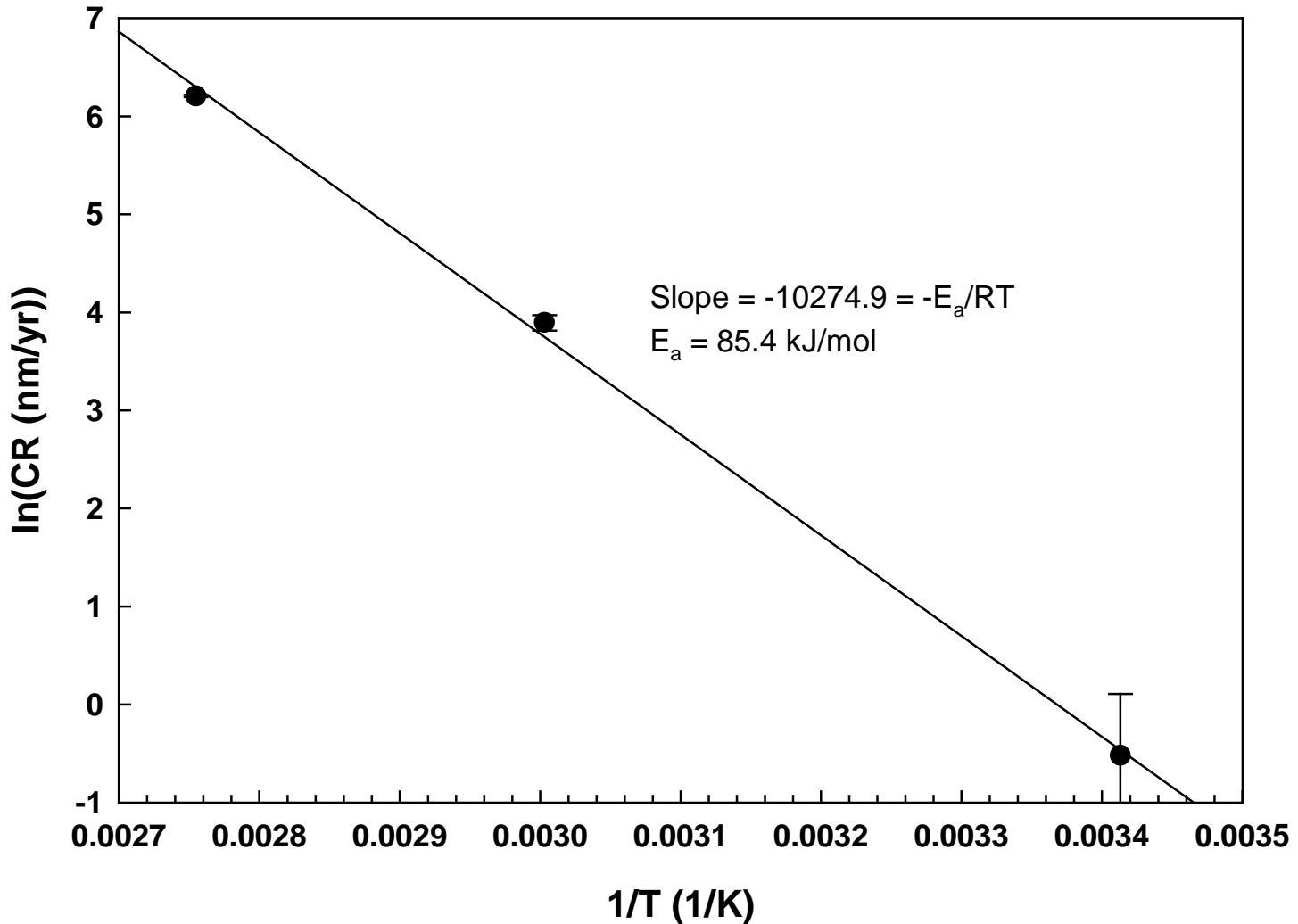
## Precipitate on 90°C SCW coupons



XRD patterns for the 3-month and 24-month SCW test coupons, along with matching phase patterns. The blue lines represent mordenite ( $\text{Na}_{0.31}\text{Al}_{3.55}\text{Si}_{42.72}\text{O}_{96} \cdot 2.76\text{H}_2\text{O}$ )

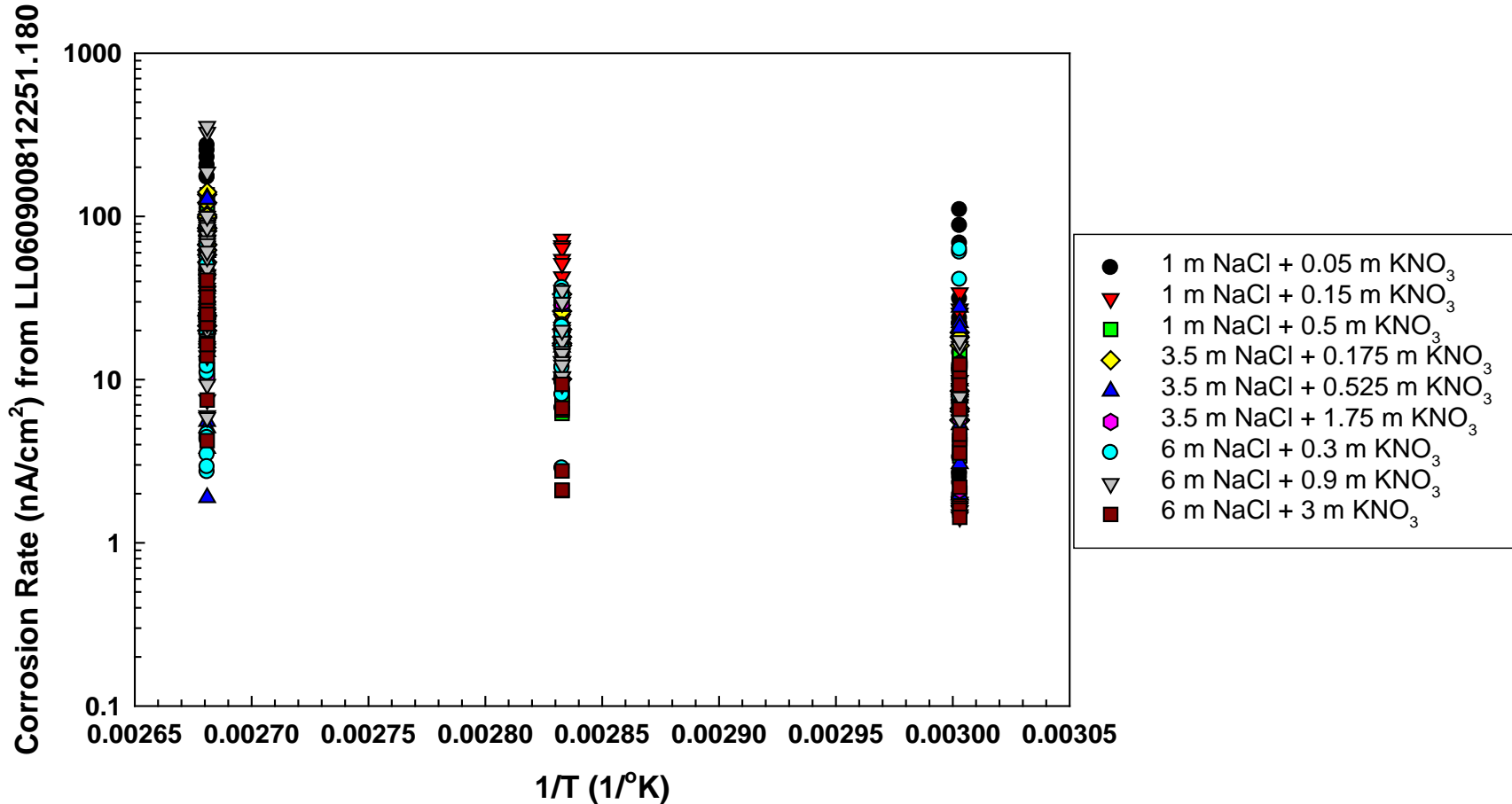
# Activation Energy – Alloy 22 in SAW

SAW, 18 Months



# Temperature Dependence of the General Corrosion Rate

Data used in AMR for T Dependence



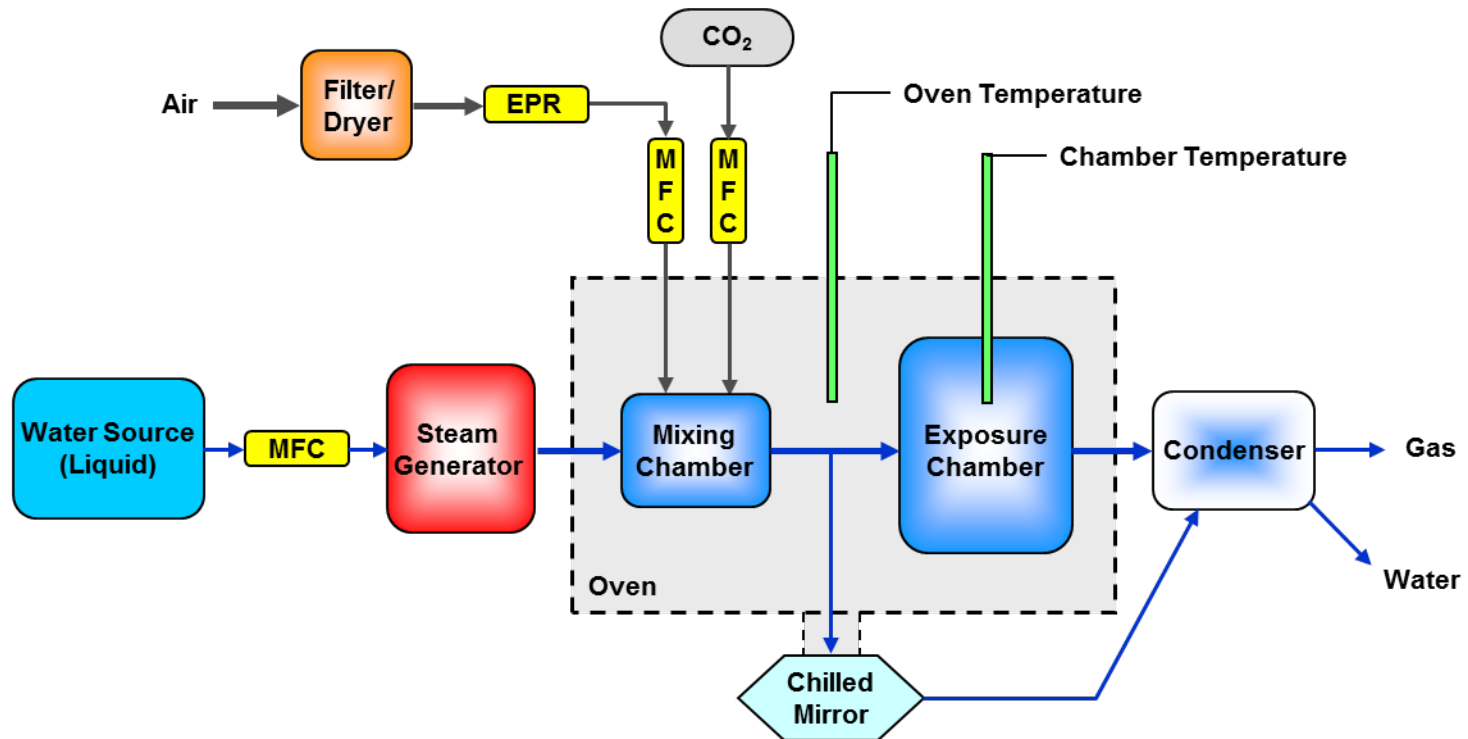
*With uncertainty incorporated, the calculated activation energy ranged from 3.37 kJ/mol to 60.05 kJ/mol*

**Goal: Establish if localized corrosion (crevice corrosion) can initiate under deliquescent conditions**

- **A series of relevant materials are being evaluated**
  - Alloy 22
  - Inconel 625
  - Hastelloy C276
  - 80:20 Ni:Cr
  
- **Thin film of salt (with known mass loading) deposited on surface, followed by the use of a traditional PTFE coated ceramic crevice former**

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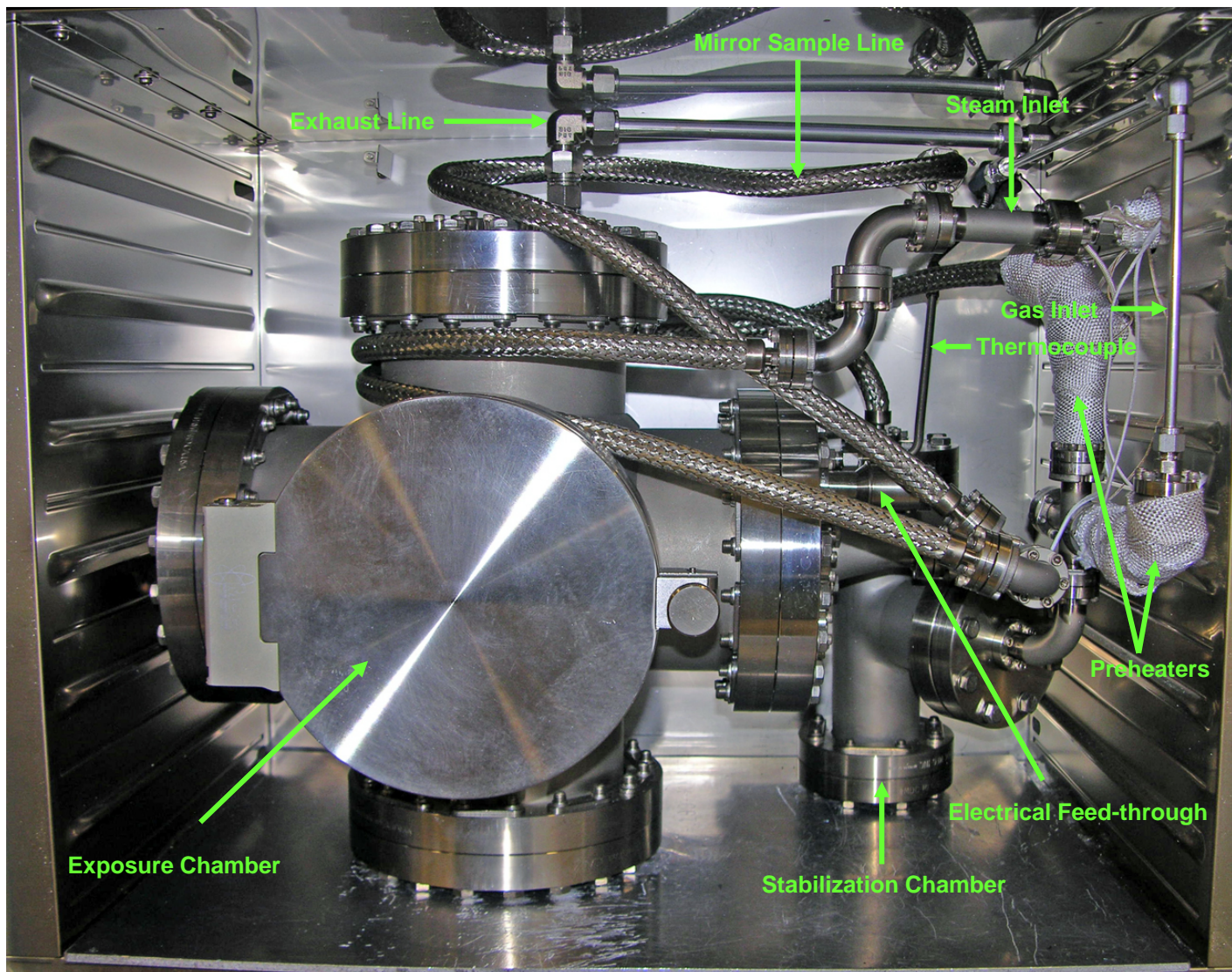
# Schematic of High Temperature System



EPR = Electronic Pressure Regulator and MFC = Mass flow controller

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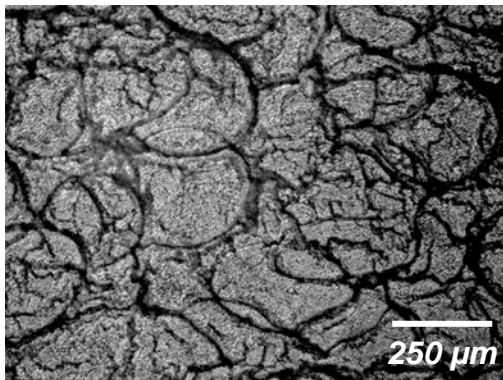
## High Temperature, Controlled Dewpoint System



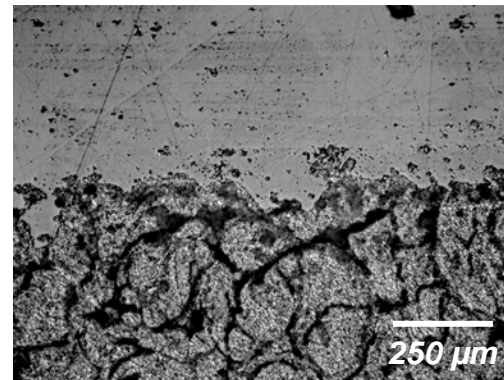
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## Experiments in Chloride-Rich Brines

- Alloy 22, Inconel 625, Hastelloy C276, 80:20 Ni:Cr, 304SS, and 303SS evaluated
- PTFE coated ceramic crevice former torqued to 70 in-lbs, Mirror finish on coupon surface
- Range of salt loadings from 50 to 250  $\mu\text{g}/\text{cm}^2$  of a NaCl-KCl mixture
- $T=105^\circ\text{C}$ ,  $T_d\sim 94.5^\circ\text{C}$  (pure steam) for test intervals of 100 days



**120  $\mu\text{g}/\text{cm}^2$**

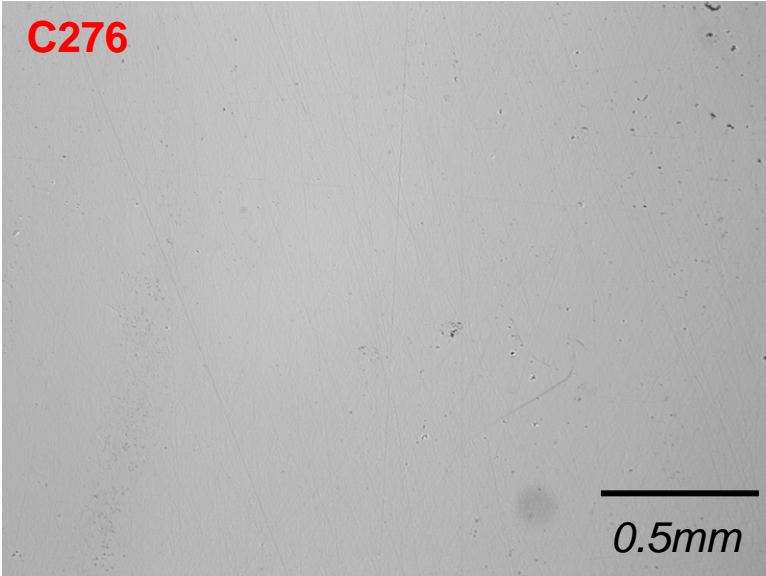


**Wiped region**

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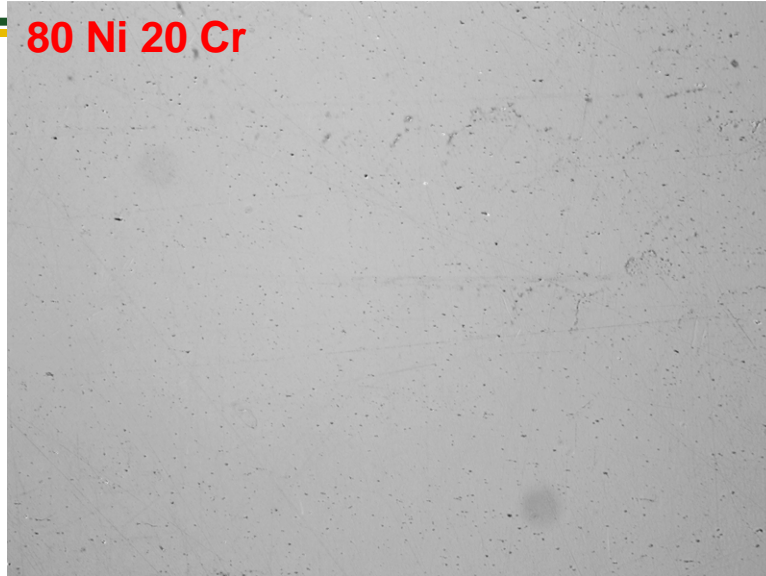
# Nickel Alloys in Chloride Brines

**C276**

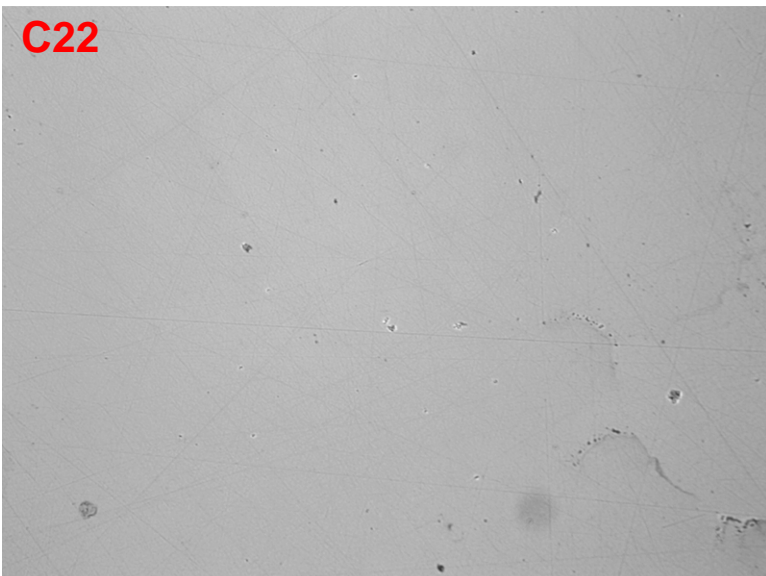


0.5mm

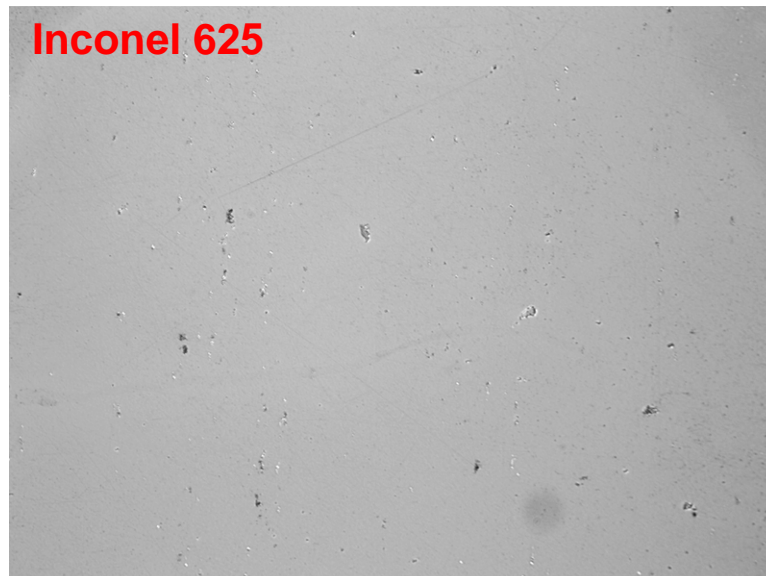
**80 Ni 20 Cr**



**C22**



**Inconel 625**



*No crevice  
corrosion  
initiation*

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## Significant Attack on 303SS

*To alleviate concern that technique was not capable of supporting crevice corrosion even on highly susceptible materials, 303SS was introduced into the test matrix*



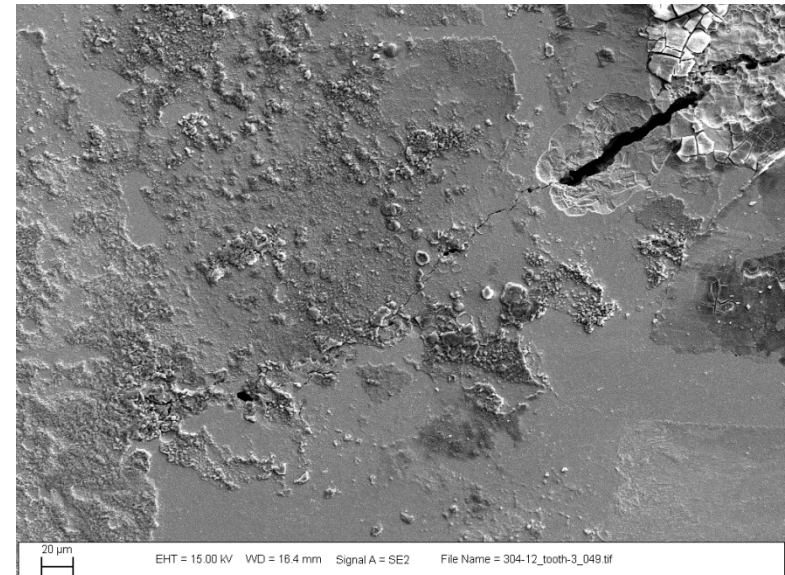
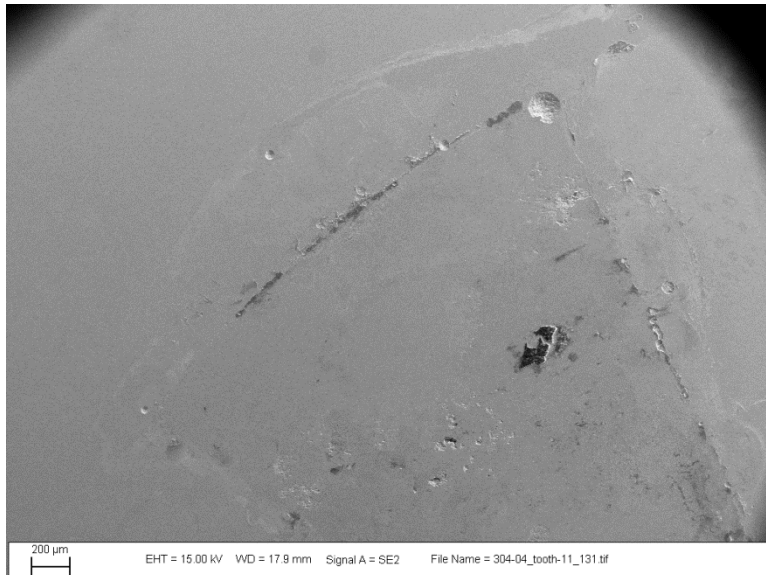
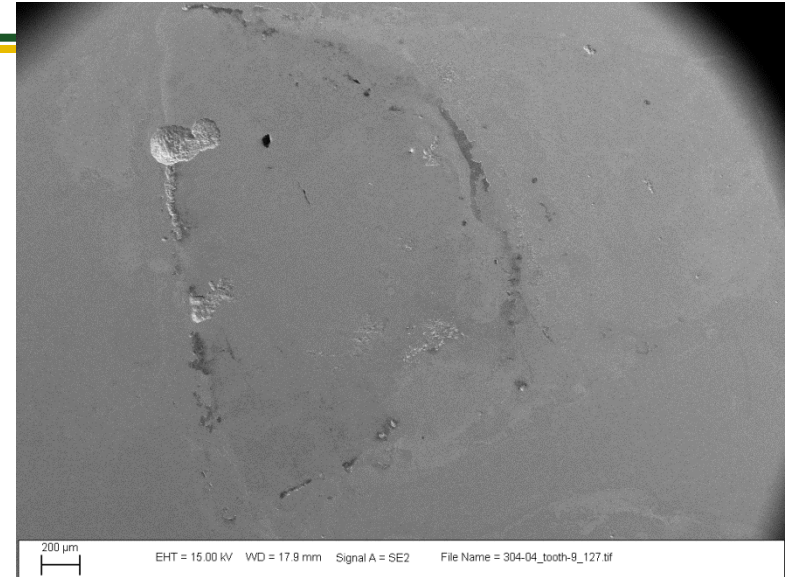
*Evaluation of the impact of salt loading was pursued for 304SS (difficult to interpret 303SS results as material was too active) to explore stifling argument*

- Three different mass loadings evaluated (50, 100, and 200  $\mu\text{g}/\text{cm}^2$ )
- Initiation observed at all mass loadings, but extent of attack correlated with mass loading
- Samples exhibited SCC in a number of cases, but did not correlate with mass loading
- 303SS too susceptible – significant attack wherever salt mixture was present

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## Impact of Salt Loading on 304SS 50 $\mu\text{g}/\text{cm}^2$

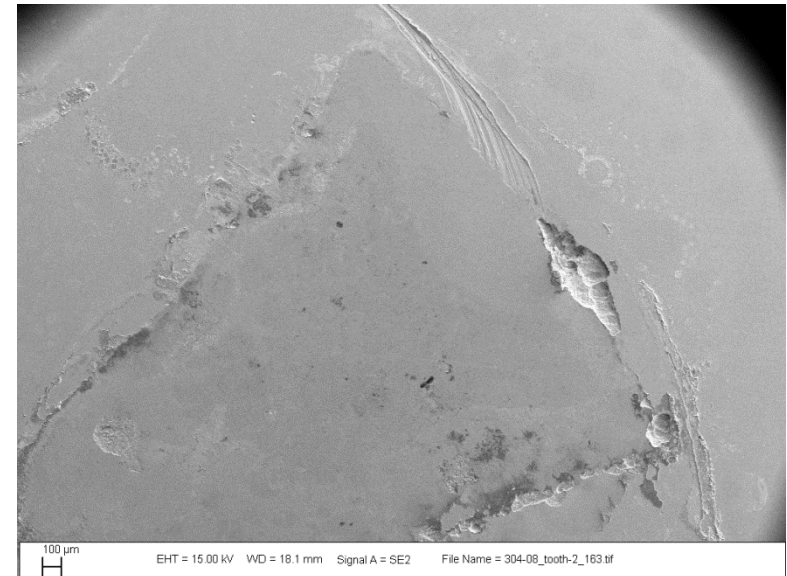
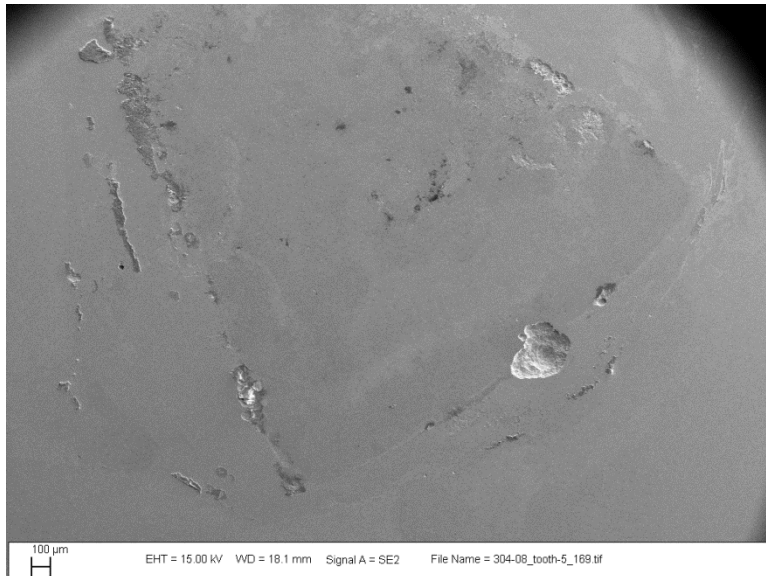
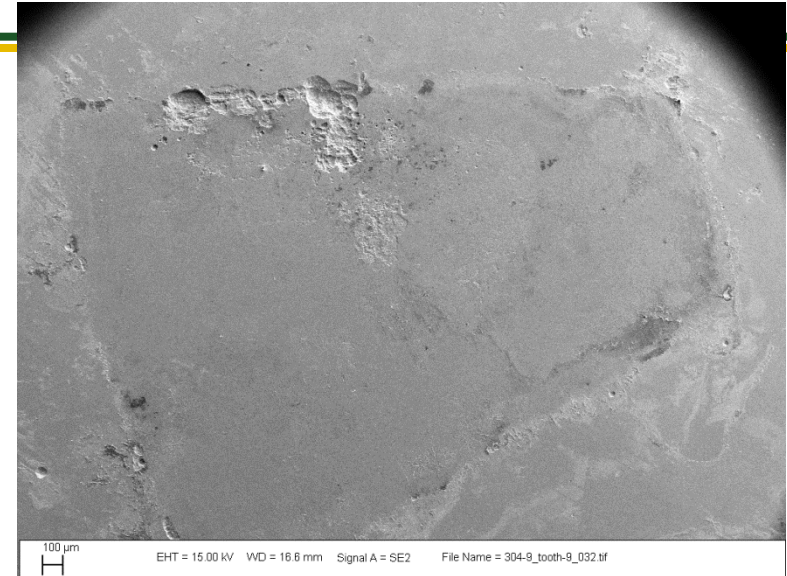
- *At least small sites on most teeth*
- *Cracking observed on some teeth*
- *Propagation limited in extent*



# Used Fuel Disposition

## Impact of Salt Loading on 304SS 100 $\mu\text{g}/\text{cm}^2$

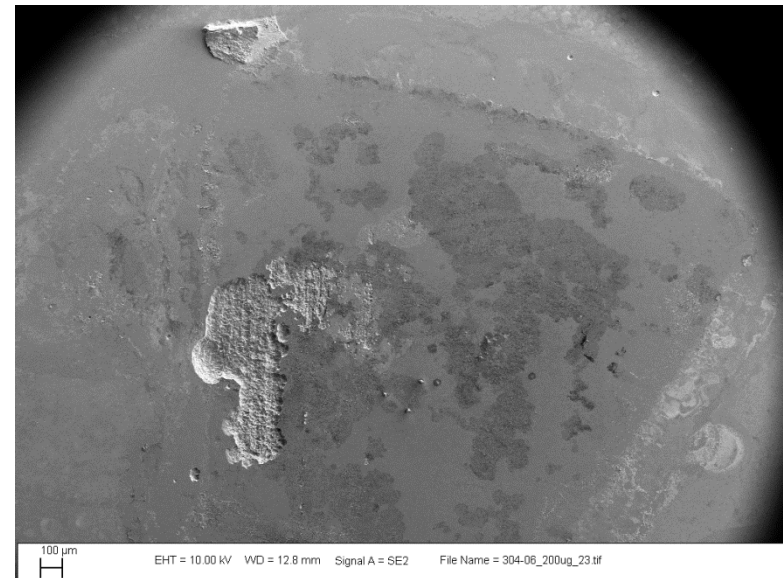
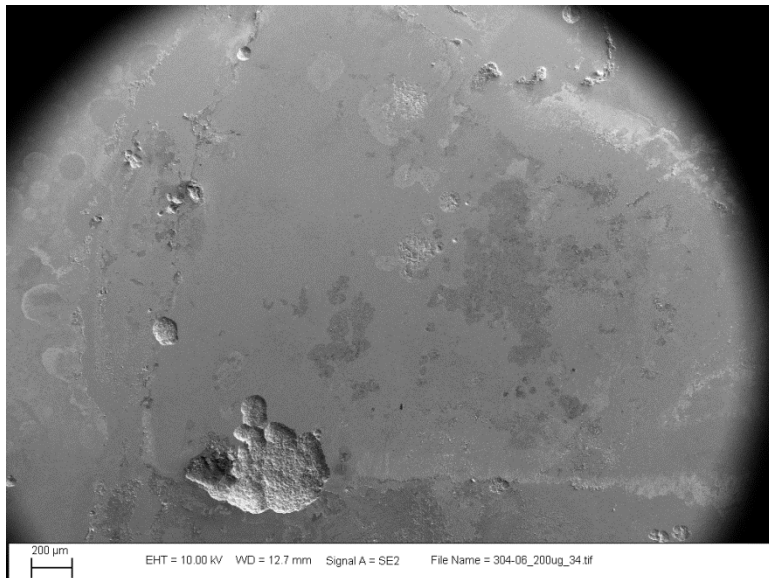
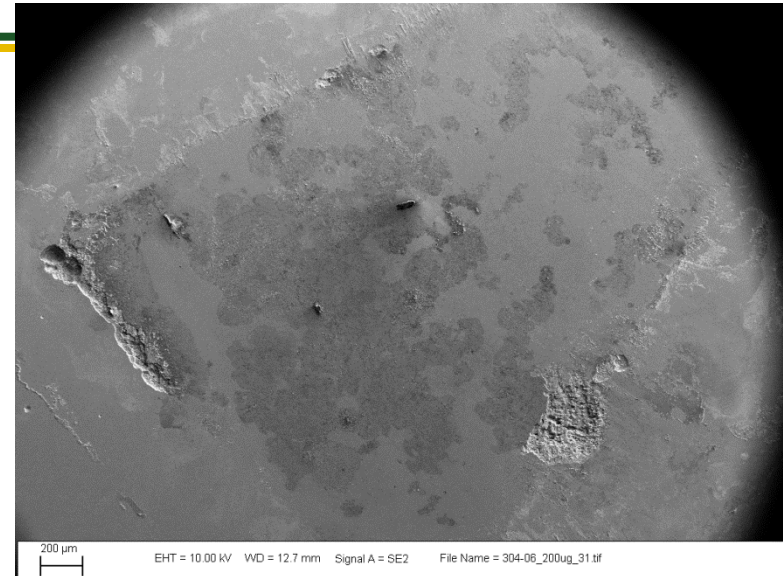
- *More teeth where crevice corrosion initiated*
- *Typically multiple sites on teeth where crevice corrosion initiated*
- *Propagation more extensive (further/deeper)*



# Used Fuel Disposition

## Impact of Salt Loading on 304SS 200 $\mu\text{g}/\text{cm}^2$

- *Crevice corrosion initiated on most teeth*
- *Typically multiple sites on teeth where crevice corrosion initiated*
- *Propagation more extensive (sites tended to be larger/deeper)*



- **Experimental work defined in technical work plan FCRD-UFD-2012-000052**
  
- **Aqueous Immersion**
  - Completion of Alloy 22 and issue final report
  - Initiate experiments on materials of interest to interim storage
  
- **Dust Deliquescence**
  - Time dependence of damage on 304SS
  
- **Copper Corrosion in Anoxic Water**
  - Hydrogen permeation measurements on Pd under humid, anoxic conditions

- **Goal is to establish accurate general corrosion rates for interim storage casks under relevant conditions**
  - Stainless steels in welded and unwelded condition
  - Metallic seal (o-ring) materials
  
- **Need information**
  - Are general corrosion rates really needed?
  - Technical basis for relevant environments?

- **Experiments to date have been fixed, long term (100 day) tests**
  - No information on damage propagation
  
- **New experiments focus on gaining knowledge of the time dependence of corrosion propagation**
  - Similar sample geometry and salt loading
  - Test periods will vary
  - Extent of damage, time of initiation, etc. will be quantified

- **Copper corrosion in electrochemically reducing environments**
  - Traditional understanding is that copper (metal) is thermodynamically stable under such conditions, and as such corrosion will not take place.
  - Recent studies claim to demonstrate that corrosion of copper can take place at an appreciable rate under these conditions, But...
    - *Corrosion product has been theorized, but not observed/documentated*
    - *Corrosion detection is based upon the observation of a hydrogen partial pressure which is claimed to be the result of water reduction (presumably supporting oxidation of the copper)*
  - Experimental work will explore several potential artifacts which may explain the literature results as well as explore the corrosion behavior of copper in relevant aqueous environments.

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## Copper in Anoxic Water

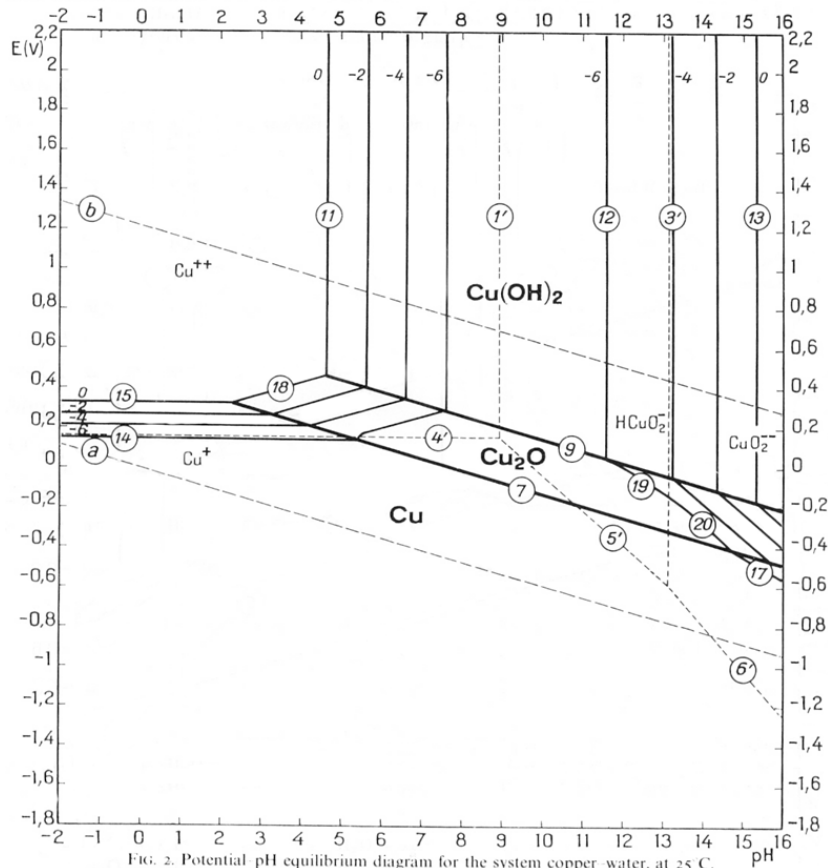
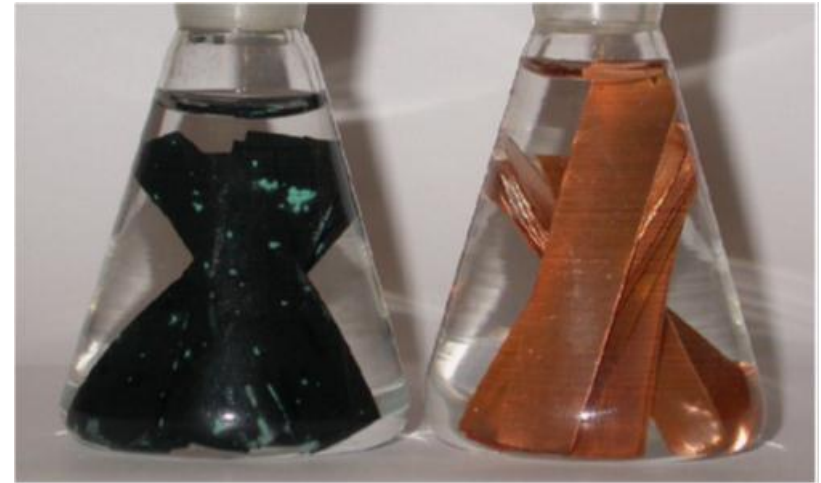


FIG. 2. Potential pH equilibrium diagram for the system copper-water, at 25 C.  
[Considering the solid substances Cu, Cu<sub>2</sub>O and Cu(OH)<sub>2</sub>, CuO is not considered.]



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# Copper in Anoxic Water: Approach

