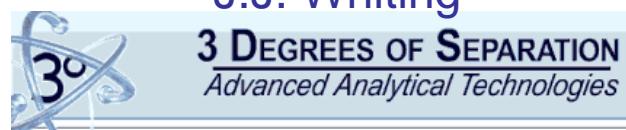


A Portable Microfabricated GCxGC System for Vapor Sampling and Analysis

37th International Symposium on Capillary Chromatography
and
10th GCxGC Symposium
Palm Springs, CA
May 16, 2013

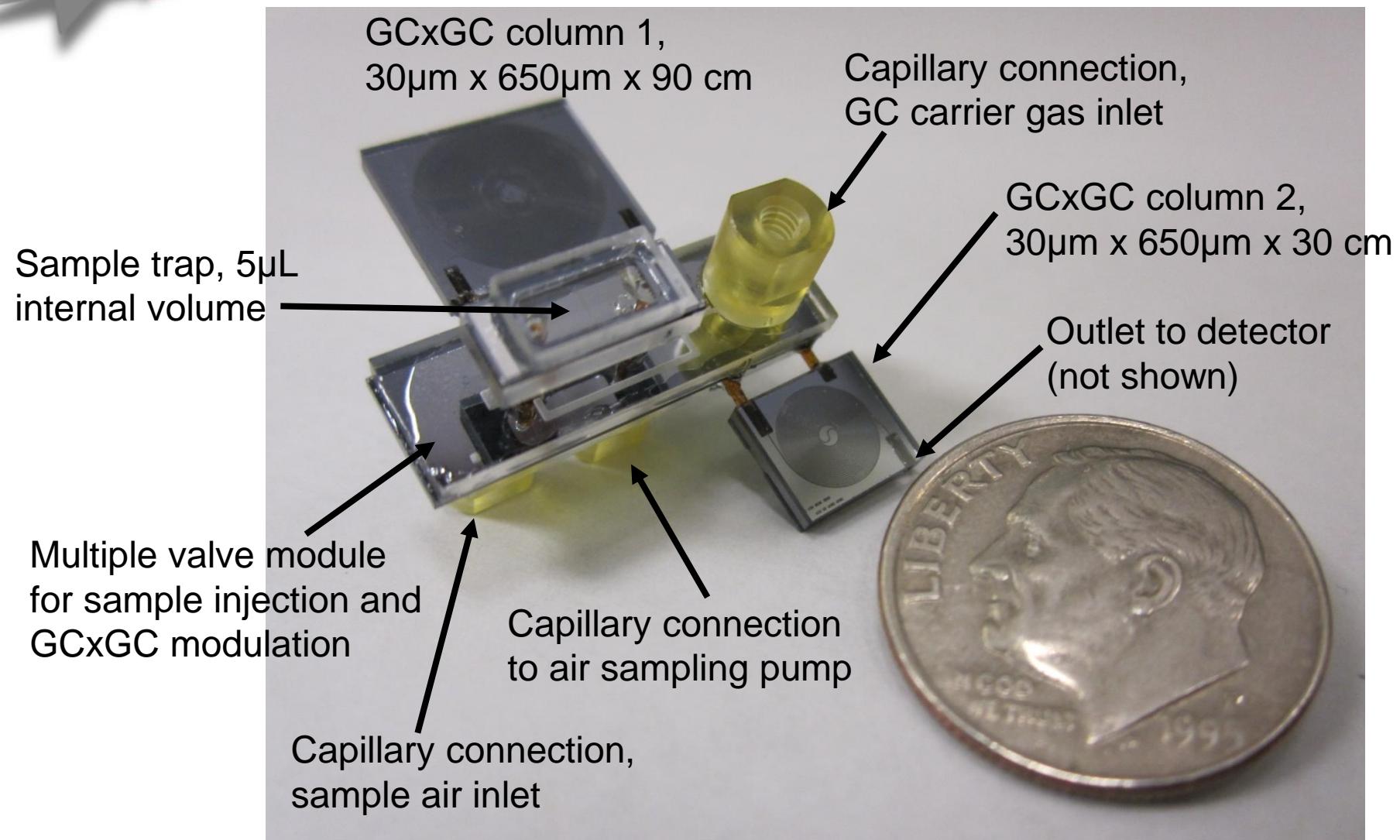
R.J. Simonson
Douglas H. Read, A.W. Staton
Sandia National Laboratories



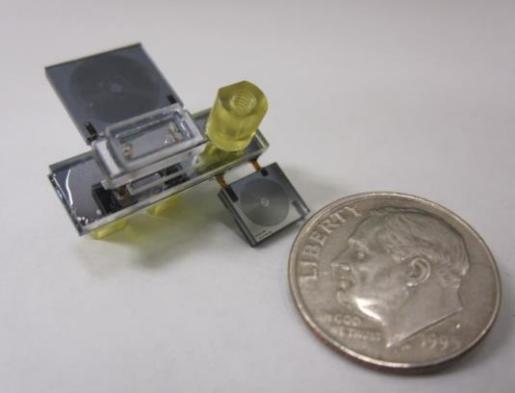
Sandia National Laboratories is a multi-program laboratory managed and operated by Sandia Corporation, a wholly owned subsidiary of Lockheed Martin Corporation, for the U.S Department of Energy's National Nuclear Security Administration under contract DE-AC04-94AL85000.



Previously Reported Design: We have built and tested 8 of these



Design Changes Now Ongoing



← Why did the first design look like this?

- **SPEED** – 4 second analysis cycle: Air sampling, GCxGC separation, detection, data analysis and alarm reporting
- Sensitivity – 1 ppt limit of detection requires fast sample injection (*splitless!*)
- Low power, small volume

Current design changes driven by:

1. Performance problems with the above design
 - GCxGC modulation flow restriction at junction between GC1 and GC2
 - Low device yield and robustness of sampling microvalve arrays
 - Sample injection speed limitations
2. Customer-requested changes
 - **Ambient air carrier gas**
 - **Vacuum outlet GC** (for compatibility with mass spectrometer detector)
 - **Limit GCxGC outlet flow rate to ≤ 3 sccm to minimize mass spec pumping**



GC Peak Capacity ~ 1/(False Alarm Rate)

- Alternative (non GC) detector technologies exist for various classes of toxic vapors
- Several of these succeed in terms of:
 - Detection sensitivity for individual target compounds
 - Form factor, detection speed, battery life
- *They often fail due to large false positive detection rates in complex environments*
- Consider the worst case chemical analysis scenario:
 - Complex mixtures of completely random compounds of different classes
 - No chemical selectivity in sample collection or eluent detection, so that the entire burden of target identification falls on the GC separation stage.
- Statistical analysis by Davis and Giddings (Analytical Chem. 55(1983)418.) To achieve:
 - 90% probability of single peak separationWould require:
 - 95% ***unused*** or ***“empty”*** GC peak capacity
- So for full separation, a mixture of ***only 30 compounds*** would require capacity
$$C_p = 1/(1-0.95) \times 30 = 600$$
- **Doing this separation in 1 min would require peak capacity production of at least 10 peaks/sec**

Micro Gas Analyzer Development

COTS GCxGC-MS



$V \sim 2 \text{ m}^3$
 $t \sim 10^3 \text{ sec}$
 $P \sim 2 \text{ kW, E} \sim 7 \text{ MJ}$
GCxGC
Peak capacity $\sim 10^3$

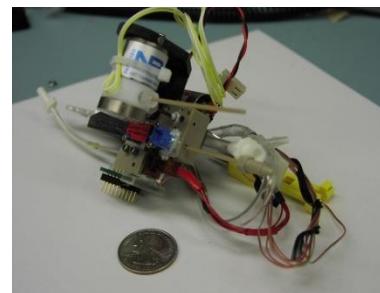
Peaks/sec ~ 1

Sandia handheld
GC-SAW



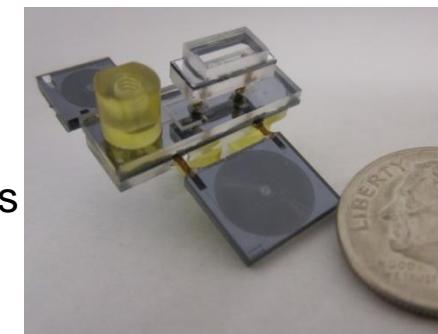
$V \sim 1000 \text{ cm}^3$
 $t \sim 10^2 \text{ sec}$
 $P \sim 2 \text{ W, E} \sim 100 \text{ J}$
Single GC
Peak capacity ~ 10
Peaks/sec ~ 0.1
(low FAR by limiting target chemistry)

Micro Gas Analyzer



Phase II
Single GC
 $V < 20 \text{ cm}^3$

Phase IV
 $V < 4 \text{ cm}^3$
(Analytical components only)

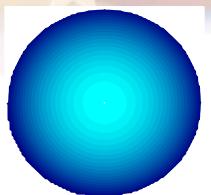


$t \sim 4 \text{ sec}$
E goal $< 1 \text{ J}$, actual 10-100J

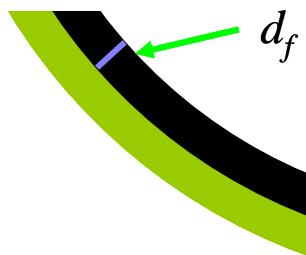
GCxGC
Peak capacity > 300

Peaks/sec ~ 50

Column Cross Section Effects



100 μm – round
7854 μm^2

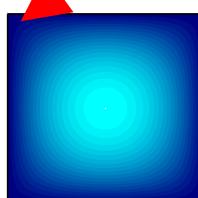


Round Cross Section

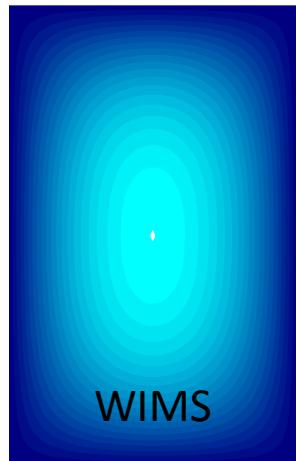
- Flow restriction and performance limited by radius
- Film deposition is uniform

Rectangular Cross Section

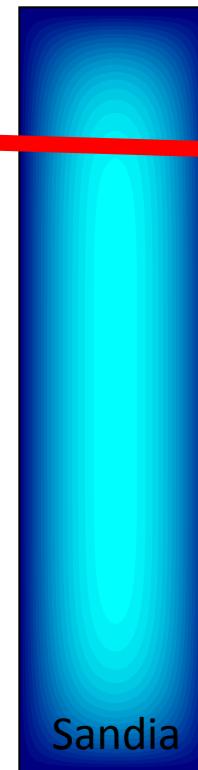
- Flow restriction controlled by height
- Performance limited by width
- End effects
 - Film deposition often results in thicker phases in the corner
 - Thicker stagnant flow regions in corners



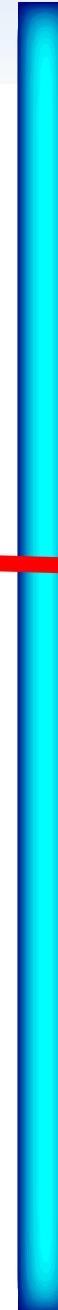
100 μm x 100 μm
10,000 μm^2



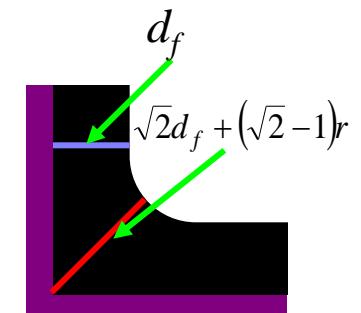
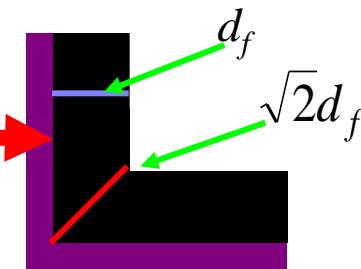
140 μm x 250 μm
35,000 μm^2



100 μm x 400 μm
40,000 μm^2



30 μm x 685 μm
20,550 μm^2
DARPA



Why Use Rectangular GC Columns?

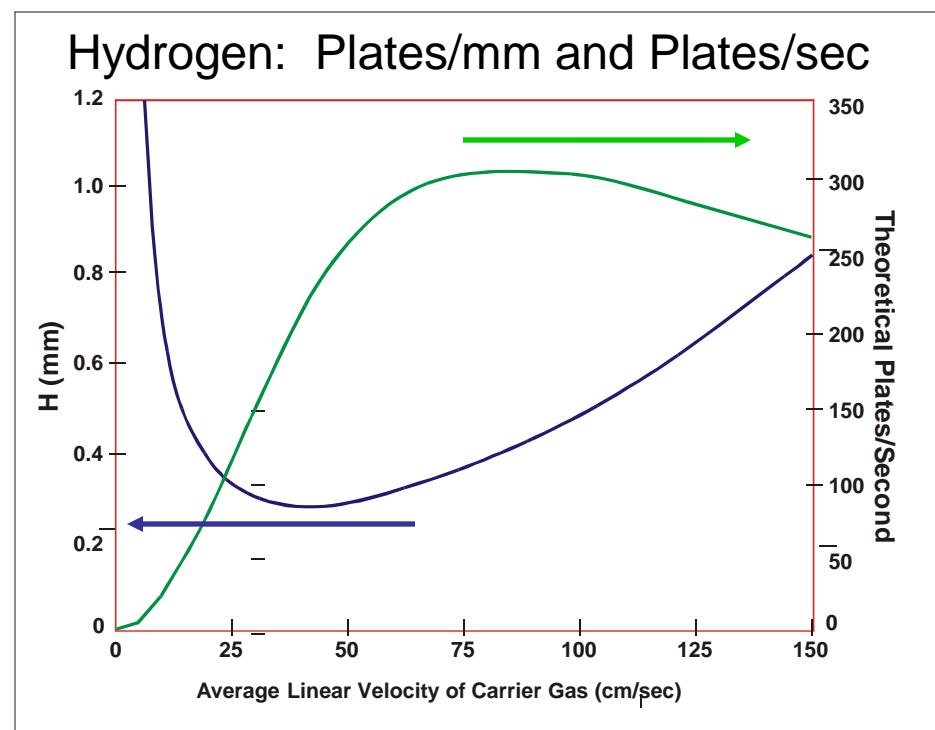
IF: Column efficiency is controlled by channel width, w (small);

And: flow resistance can be kept low by increasing channel height, h ;

THEN: Columns can operate at linear flow velocities higher than the usual \bar{U}_{opt} ("Golay minimum");

WHERE: Efficiency **per unit time** is optimized (see figure);

WITHOUT: Large increases in p_{inlet} , which require increased energy use and more stringent valve performance.



After fig. 5.16 in *Analytical Gas Chromatography*, 2nd edition, W. Jennings, E. Mittlefehldt, and P. Stremple, Academic Press (San Diego) 1997.

Other engineering advantages for portable GC applications:

- "Easy" variation of dimensions by Si etch processes
- Tight "wrapping" of columns, e.g. 1m/cm², reduces heat capacity for fast temperature programming

Golay Equation for Performance of Rectangular GC Columns

$$H = \frac{2D_g f_1 f_2}{\bar{u}} + \frac{(1 + 9k + 25.5k^2)w^2}{105(k+1)^2} \frac{f_1}{D_g} \frac{\bar{u}}{f_2} + \frac{2}{3} \frac{k}{(k+1)^2} \frac{(w+h)^2 d_f^2}{D_s h^2} \frac{\bar{u}}{u} + \frac{\Delta t^2 \bar{u}^2}{L(k+1)^2}$$

C \bar{u}

B/\bar{u}			Extra-column connections
Longitudinal diffusion	Mass Transport in the Mobile Phase	Mass Transport in the Stationary Phase	Extra-Column Band Broadening

\bar{u} – average linear carrier gas velocity

D_g – binary diffusion coefficient in gas phase

f_1 – Giddings-Golay gas compression correction factor

f_2 – Martin-James gas compression correction factor

k – retention factor

w – channel width

h – channel height

d_f – stationary phase film thickness

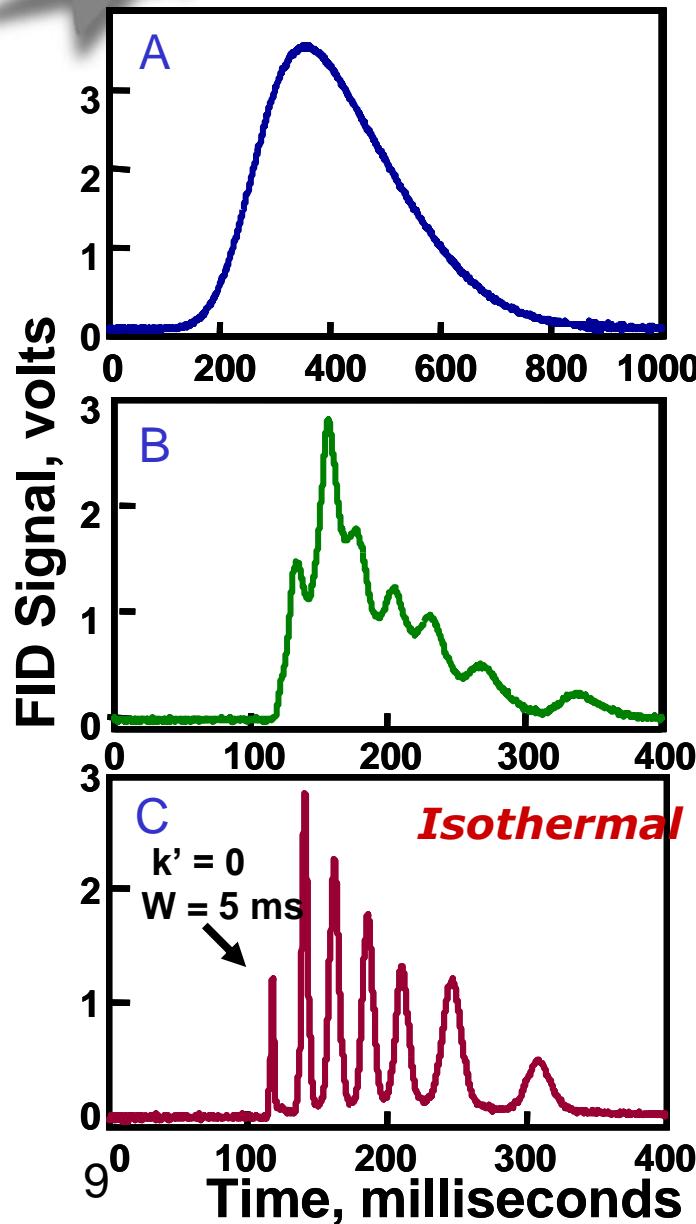
D_s – binary diffusion coefficient in stationary phase

Δt – time correlating to extra column band broadening

L – column length

1. M.J.E. Golay, in Gas Chromatography 1958 (Amsterdam Symposium), D.H. Destry, ed., Butterworths (London, 1958) pp. 139-143.
2. M.J.E. Golay, J. Chromatogr. 216 (1981) 1.

At High Speeds, Sample Injection Dominates Over Column Performance



Synovec et al. have demonstrated fast GC using COTS columns and high speed injection via fast valves and/or cryofocusing: cf. G.M. Gross, B.J. Prazen, J.W. Grate, R.E. Synovec, Anal. Chem. **76** (2004) 3517-3524.

- Example: Three types of injection under identical separation conditions (1 m x 100 μm column)
- Same 7-component mixture injected. Retention order: methanol, benzene, octane, chlorobenzene, anisole, decane, butylbenzene

- (A) standard primary autoinjector
- (B) single valve sample injector (20 ms)
- (C) synchronized dual valve injector (2.5 ms)

Flow-Modulated GCxGC Separations

Why do it?

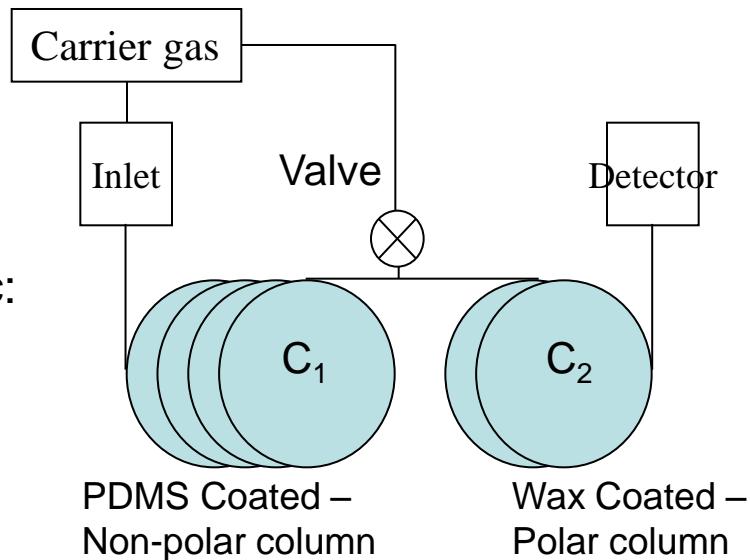
- By using two different stationary phases in series, different retention properties of the analytes are exploited
- We cannot afford cryogenic gases in a portable system, so we modulate gas flow instead of k
- Saves power, weight, and complexity at the cost of lost refocusing of analytes onto C2

How it works:

(We're modulating flow, instead of retention index)

$$u_{i,z} = u_z / (k_{i,z} + 1)$$

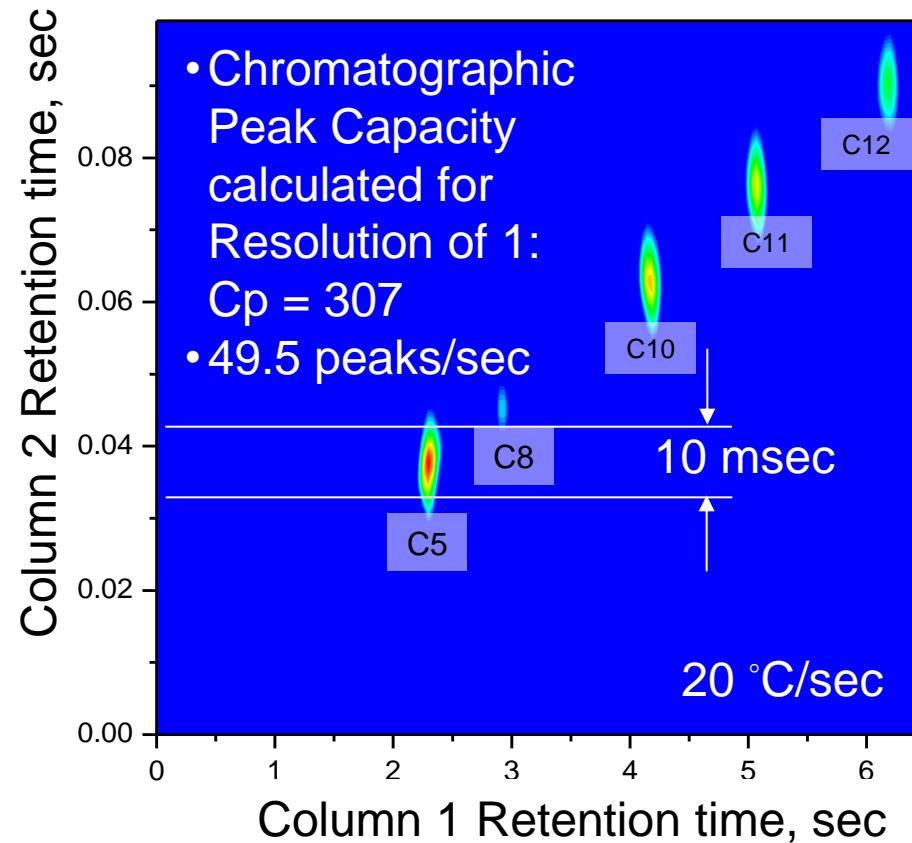
Stop-flow schematic:



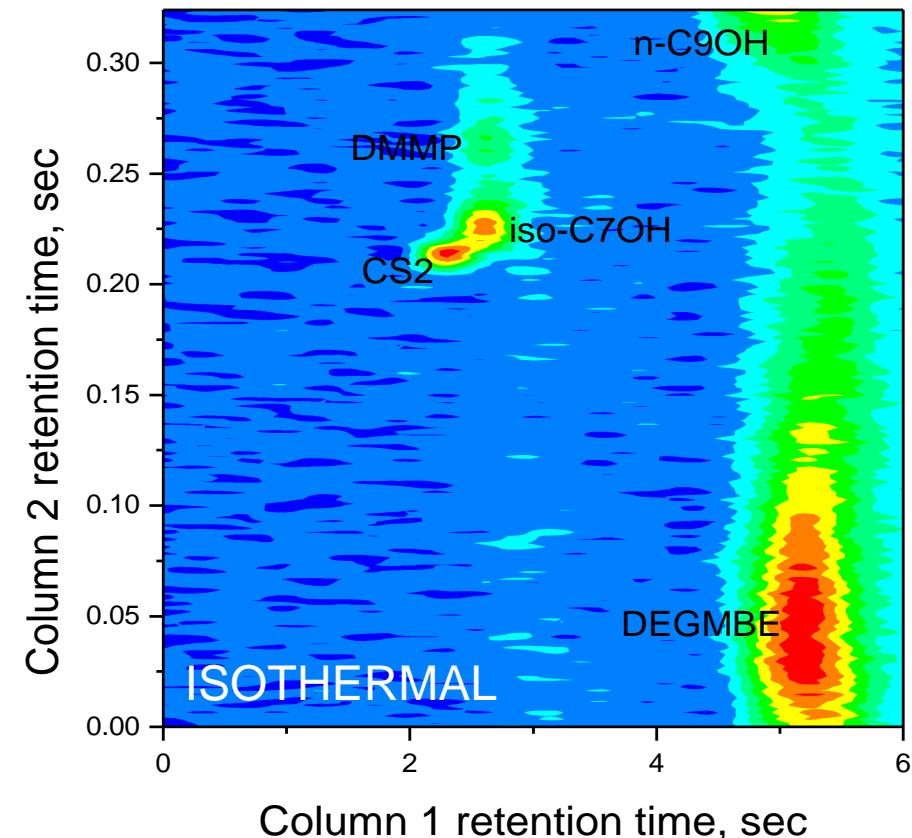
Rectangular Microcolumn GCxGC Results

Peak capacity estimated using alkane series and FID

Column 1 = Σ (Trennzahl numbers) = 30.63
Column 2 = mean isothermal Cp = 10.02



CW simulant separated from polar interferents. Detector is a coated NEMS resonator sensor (Caltech).



• Both used COTS sample injector **with high split ratio** and 2 sec “dead time”



GC Sample Injection Requirements -or- Why use MEMS?

- Fast GC separations require narrow sample injection pulse widths (in the absence of on-column sample refocusing, which typically requires temperature modulation capability that exceeds the energy budget for battery operated systems)
- Large injection split ratios are unacceptable for field instruments that have trace analytical requirements and limited sample acquisition times. Total collected sample mass can be in the pg range.
- Convective flow “sweep time” for a splitless injector depends on local gas flow rate and the volume of the injector:

$$\Delta t \sim \frac{\{\text{volume of sample collector (m}^3\}\}}{\{\text{local gas volumetric flow rate (m}^3/\text{sec})\}}$$

Golay Equation: The Extra-column Term

$$H = \underbrace{\frac{2D_g f_1 f_2}{\bar{u}}}_{\text{Longitudinal diffusion}} + \underbrace{\frac{(1+9k+25.5k^2)w^2}{105(k+1)^2} \frac{f_1}{D_g f_2} \bar{u}}_{\text{Mass Transport in the Mobile Phase}} + \underbrace{\frac{2}{3} \frac{k}{(k+1)^2} \frac{(w+h)^2 d_f^2}{D_s h^2} \bar{u}}_{\text{Mass Transport in the Stationary Phase}} + \underbrace{\frac{\Delta t^2 \bar{u}^2}{L(k+1)^2}}_{\text{Off-Column Band Broadening in interconnects}}$$

Only 1 term is quadratic in \bar{u} ... so extra-column broadening dominates at high speeds!

L = column length, which cannot be increased without increasing the analysis time

k = retention factor, determined by the analyte and stationary phase chemistries

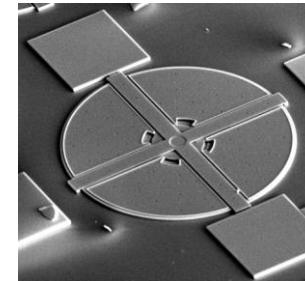
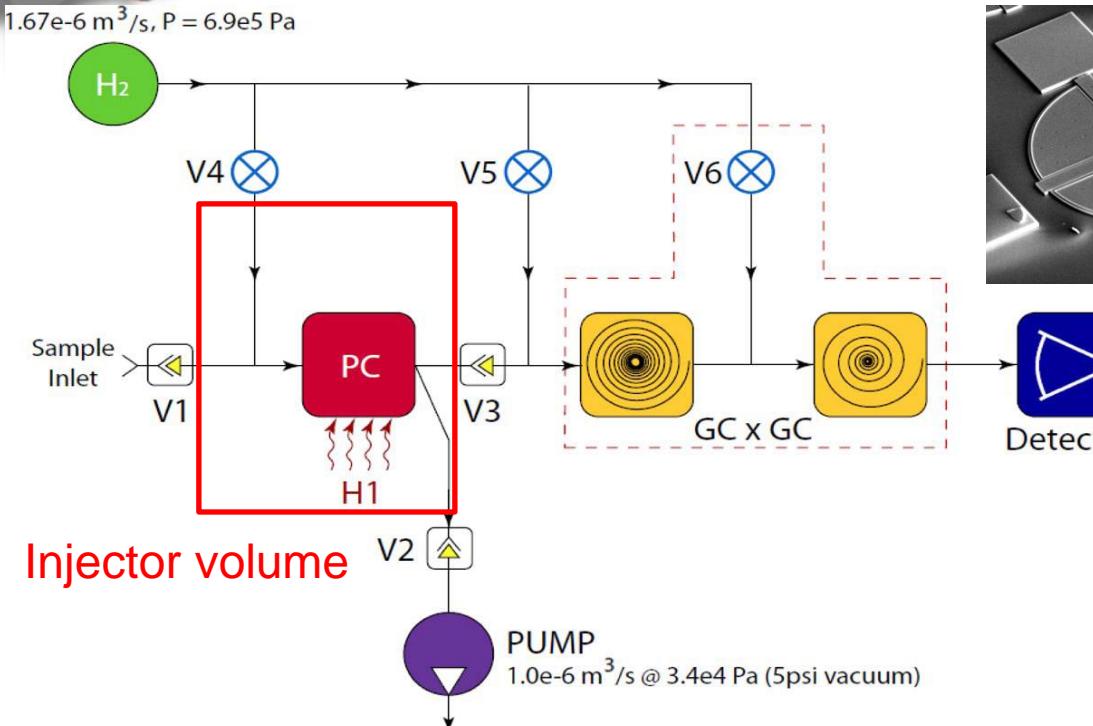
Δt = time correlating to extra column band broadening

$$\Delta t \sim \frac{\{\text{volume of extra-column interconnect (m}^3\}}{\{\text{local gas volumetric flow rate (m}^3/\text{sec)\}}$$

High-speed performance + low injection split ratio requirement \rightarrow small interconnect dimensions...

This drives the MEMS design for our MGA system!

“Micro” Portable GC Instrument.1.

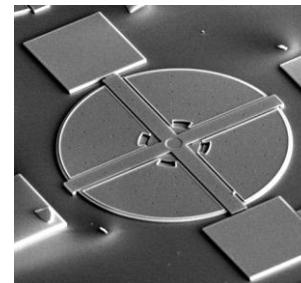
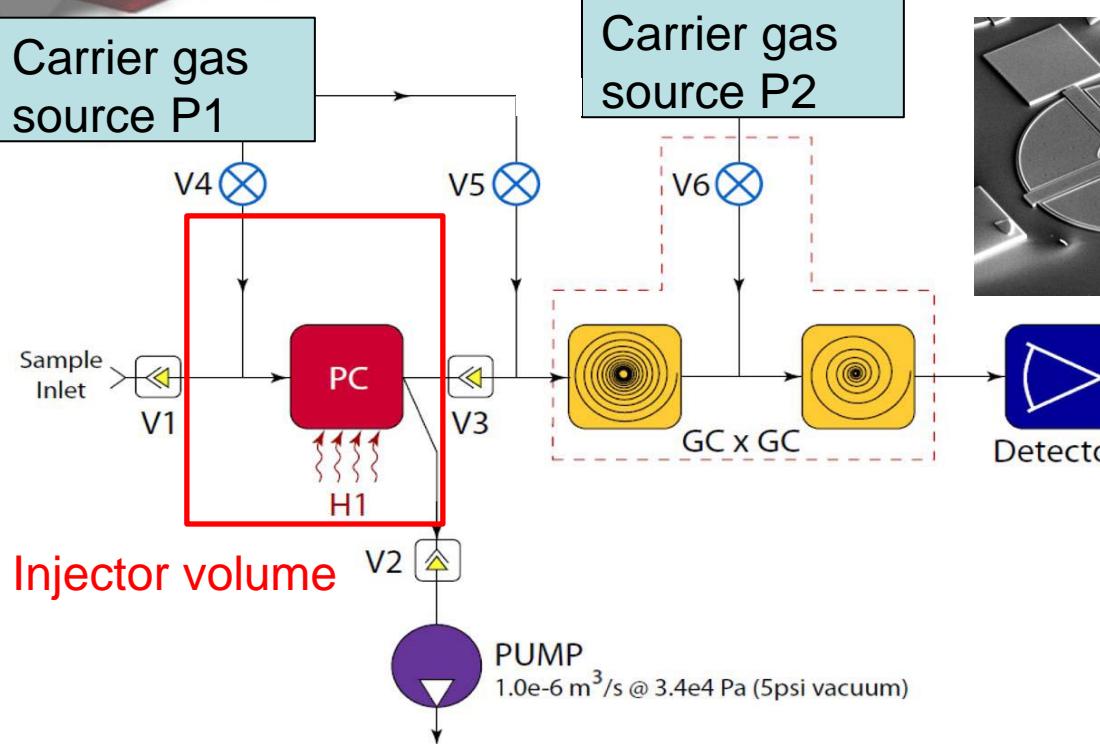


Microfabricated valves define the volume of a splitless injector (~5 μ L) for high speed flow-modulated GCxGC

P. Galambos, et al., Journal of Microelectromechanical Systems **20**(5) (2011) 1150 – 1161.

- Hardware changes needed as a result of testing these devices:
 1. Flow through V6 pathway is insufficient to completely stop GC1 flow using a single pressure source: Need separate V5 and V6 gas inlets.
 2. V1 and V2 valve arrays prone to low yield and particle contamination (16 valve arrays).
 3. Injector volume needs further reduction if flow rate at PC is to be reduced by customer's 3 sccm column flow requirement. (Column flow sets linear flow velocity at PC during injection.)

“Micro” Portable GC Instrument.2.

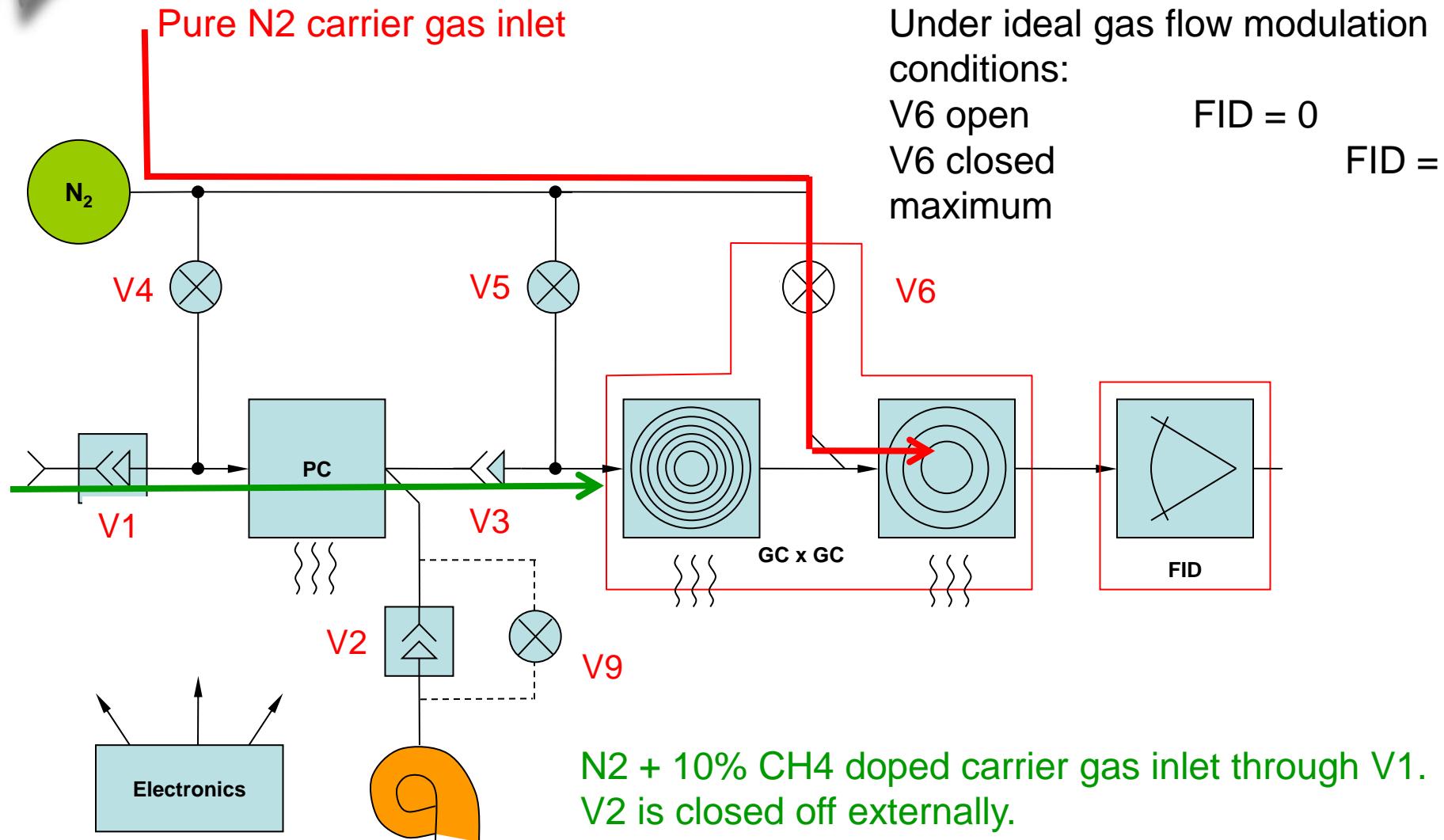


Microfabricated valves define the volume of a splitless injector (~5 μ L) for high speed flow-modulated GCxGC

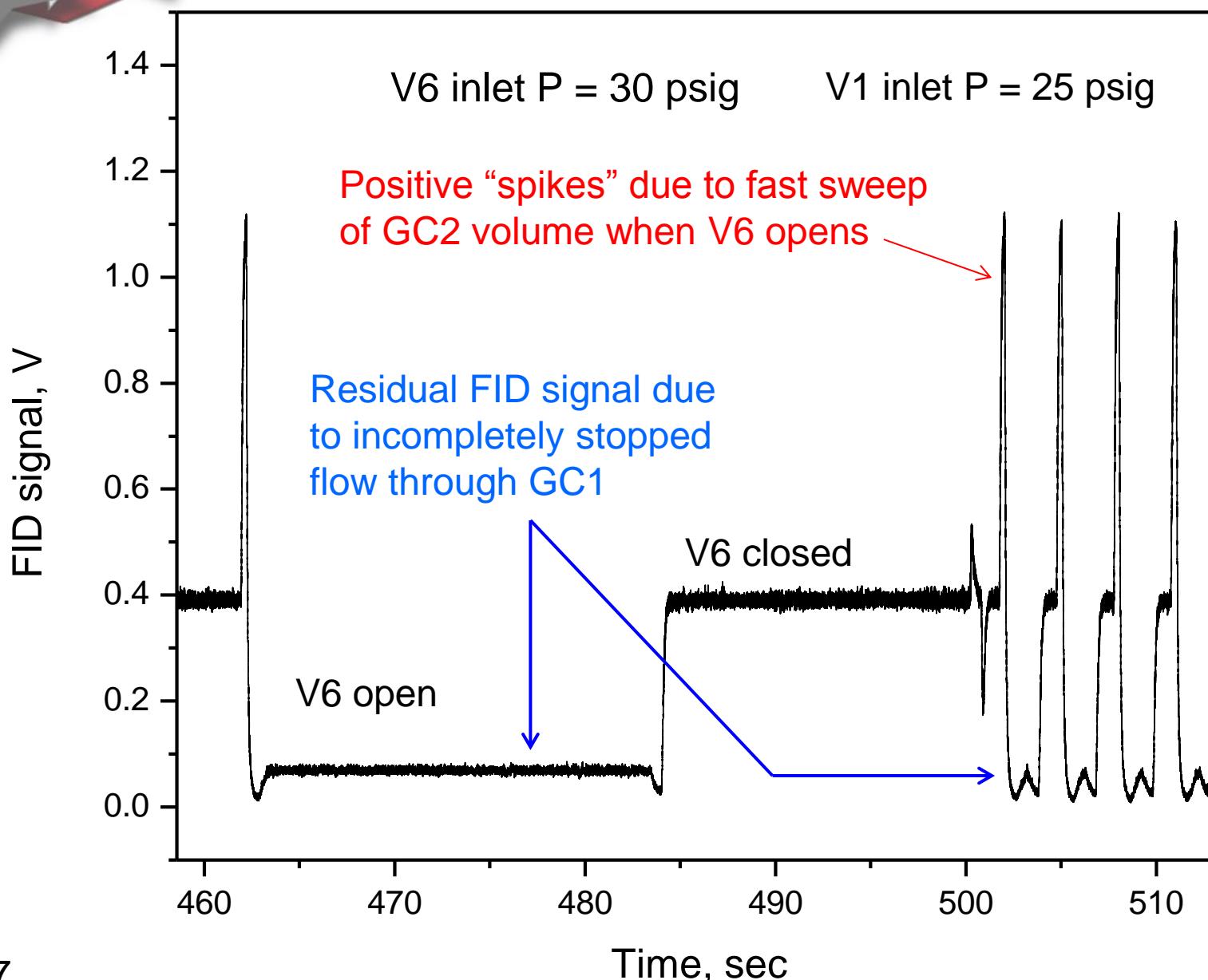
P. Galambos, et al., Journal of Microelectromechanical Systems **20**(5) (2011) 1150 – 1161.

- First design change: Provide separate carrier gas inlets at V5 and V6, so that modulation (V6 open) will fully stop the flow on GC1.

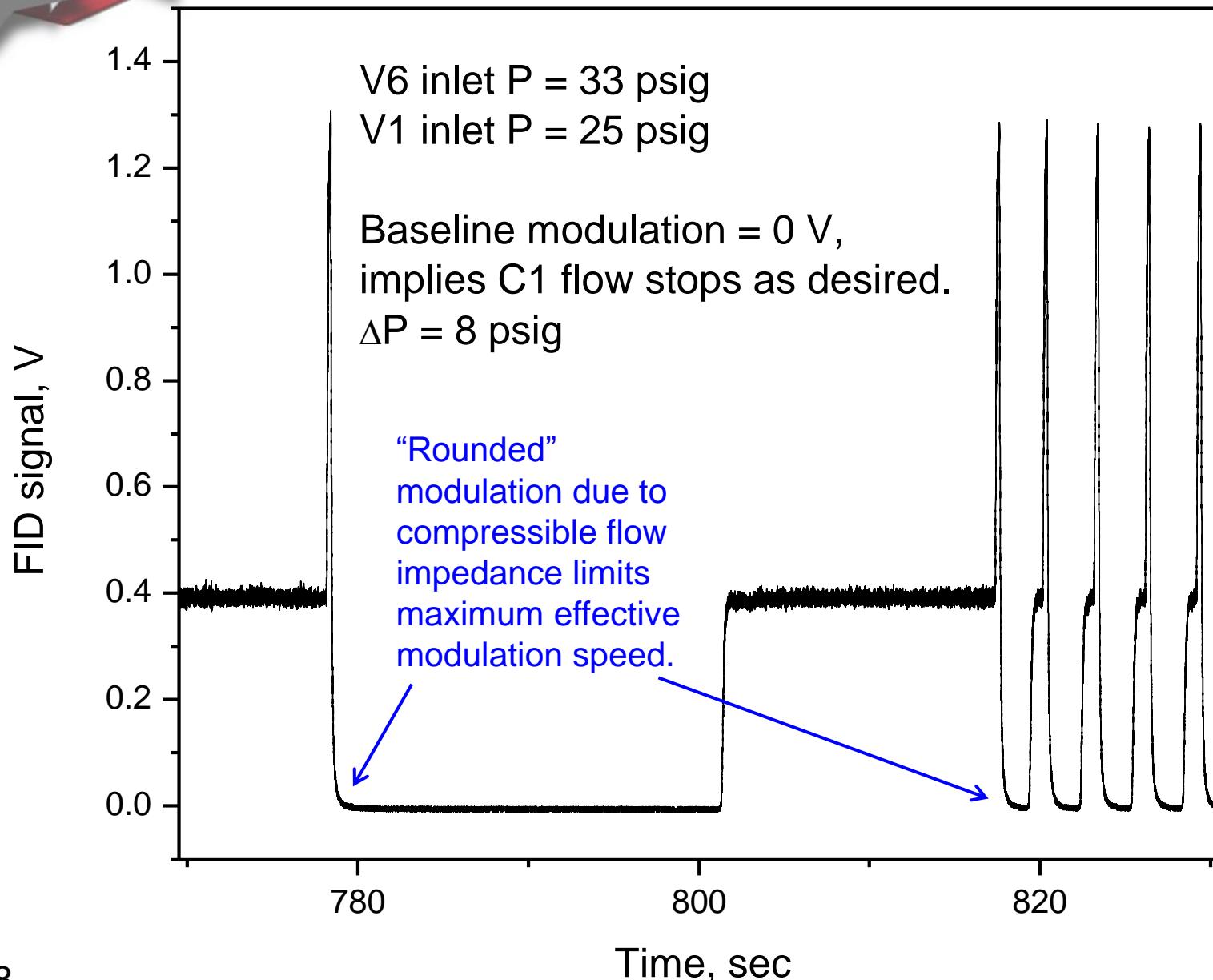
Modulation Flow Test: CH₄ Tracer Gas



Modulation Flow Test: $\Delta P = 5$ psi

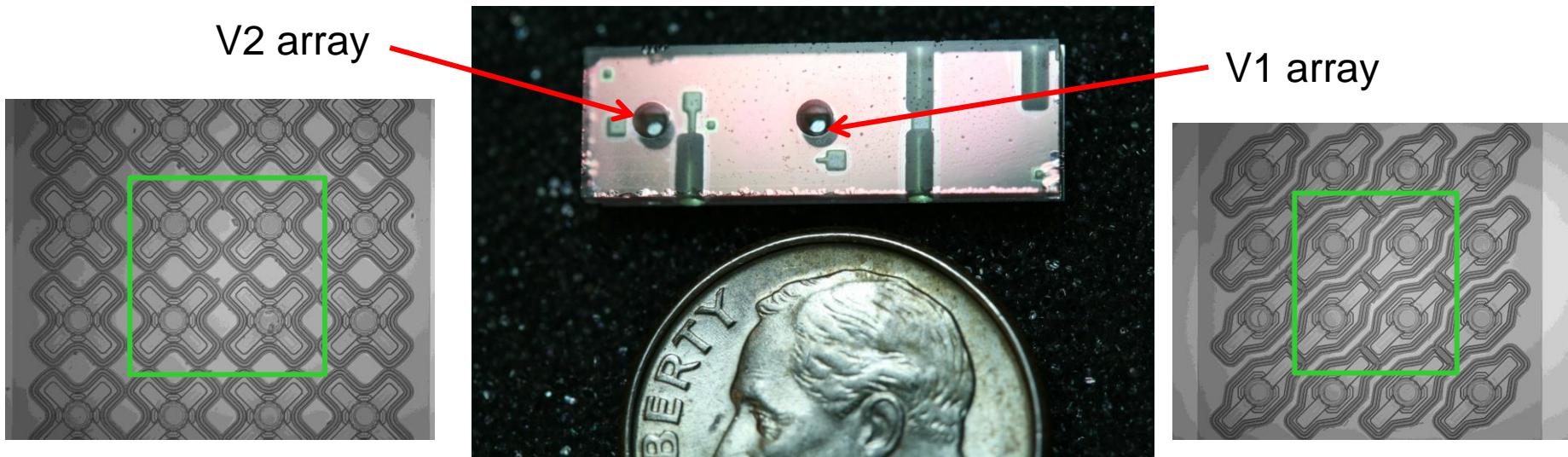


Separate Inlet P Enables Full Stop-Flow Modulation



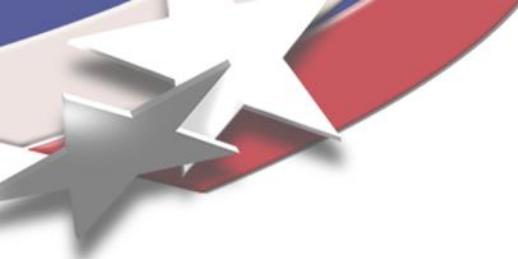
Design Changes for Higher Yield

- Old: 4 sec cycle time, 60 sccm sample air flow rate at $\Delta P = 2.5$ psi
 - Required 16 micro valves in parallel for air sampling (PC inlet and outlet)
- New: 60 sec cycle time (slower GC flow) → reduce sample air flow to 15 sccm
 - Reduce inlet and outlet valve arrays from 4x4 to 2x2



- Anticipated yield improvement between Valve Module versions 1 and 2:

1. VM1 used 36 microvalves. Module yield = 25%. Individual valve yield estimate = $(0.25)^{1/36} = 0.962$
2. Eliminating 24 of 32 valves in V1 and V2 array (as described above) and moving V5 and V6 off chip (not shown) gives VM2 a total of 10 microvalves.
3. Assuming individual valve yield is unchanged, VM2 yield should be $(0.962)^{10} = 68\%$



3rd System Design Change: Reduce GCxGC Outlet Flow

- Goal: Integrate PC-GCxGC system with a mass spectrometer detector
 - Micro GC capable of useful m/e resolution at 1 Torr operating pressure for ionizer and mass filter (Prof. J.M. Ramsey, et al., U. of N. Carolina)
- In order to reduce vacuum pumping requirements at the detector, the current system design goals include the following constraints and targets:
 - Air carrier gas outlet flow \leq 3 sccm
 - t_R of critical target compounds \leq 1 minute
 - GCxGC peak capacity \geq 300/min, or $Cp/t > 5/\text{sec}$, i.e., average peak width at baseline \leq 200 msec.
- Our approach: Model rectangular GC column performance, seeking column dimensions that will balance tradeoffs between:
 - Gas flow rate
 - Performance (Cp/t)
 - Practical manufacturing constraints, i.e., aspect ratio available for deep reactive ion etch process in Si micro columns

Golay, Giddings, and Guiochon equation for rectangular columns^{1,2,3}

$$H = \underbrace{\frac{2D_g f_1 f_2}{\bar{u}}}_{\text{Longitudinal diffusion}} + \underbrace{\frac{(1+9k+25.5k^2)}{105(k+1)^2} \frac{w^2}{D_g} \frac{f_1}{f_2} \bar{u}}_{\text{Mass Transport in the Mobile Phase}} + \underbrace{\frac{2}{3} \frac{k}{(k+1)^2} \frac{(w+h)^2 d_f^2}{D_s h^2} \bar{u}}_{\text{Mass Transport in the Stationary Phase}} + \underbrace{\frac{\Delta t^2 u_o^2}{L(k+1)^2}}_{\text{Extra-Column Band Broadening}}$$

\bar{u} – average linear carrier gas velocity

u_o – outlet linear carrier gas velocity

D_g – binary diffusion coefficient in gas phase

f_1 – Giddings-Golay gas compression correction factor

f_2 – Martin-James gas compression correction factor

k – retention factor

w – channel width

h – channel height

d_f – stationary phase film thickness

D_s – binary diffusion coefficient in stationary phase

Δt – time correlating to extra column band broadening

L – column length

1 - Golay MJE. Theory of Chromatography in Open and Coated Tubular Columns with Round and Rectangular Cross-Sections. *Gas Chromatography*. New York: Academic Press; 1958;36-55

2 - Giddings JC, Chang JP, Myers MN, Davis JM, Caldwell KD. Capillary liquid chromatography in field flow fractionation-type channels. *J Chromatography A*. 1983;255:359-379

3 - Gaspar, G.; Annino, R. Vidal-Madjar, G.; Guiochon, G. *Anal. Chem.* 1978, 50, 1512

Model Evolution

Effect of Aspect Ratio, Film Thickness Correction

Ahn and Brandani Model – AIChE Journal, Dec. 2005

$$H = \frac{2D_g f_1 f_2}{\bar{u}} + \frac{\left(A + Bk + Ck^2 \right) w^2}{96(k+1)^2} \frac{f_1}{D_g f_2} \bar{u} + \frac{2k}{3(k+1)^2} \frac{d_{f_c}^2}{D_s} \bar{u} + \frac{\Delta t^2 u_o^2}{L(k+1)^2}$$

$$A = \frac{32}{35} \left[\frac{6.192(\alpha-1)^2}{(\alpha-0.1)^2} + 1.759 \right]$$

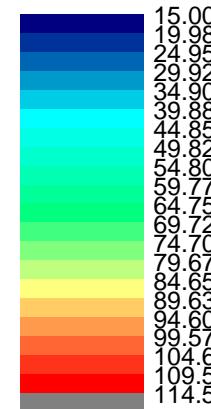
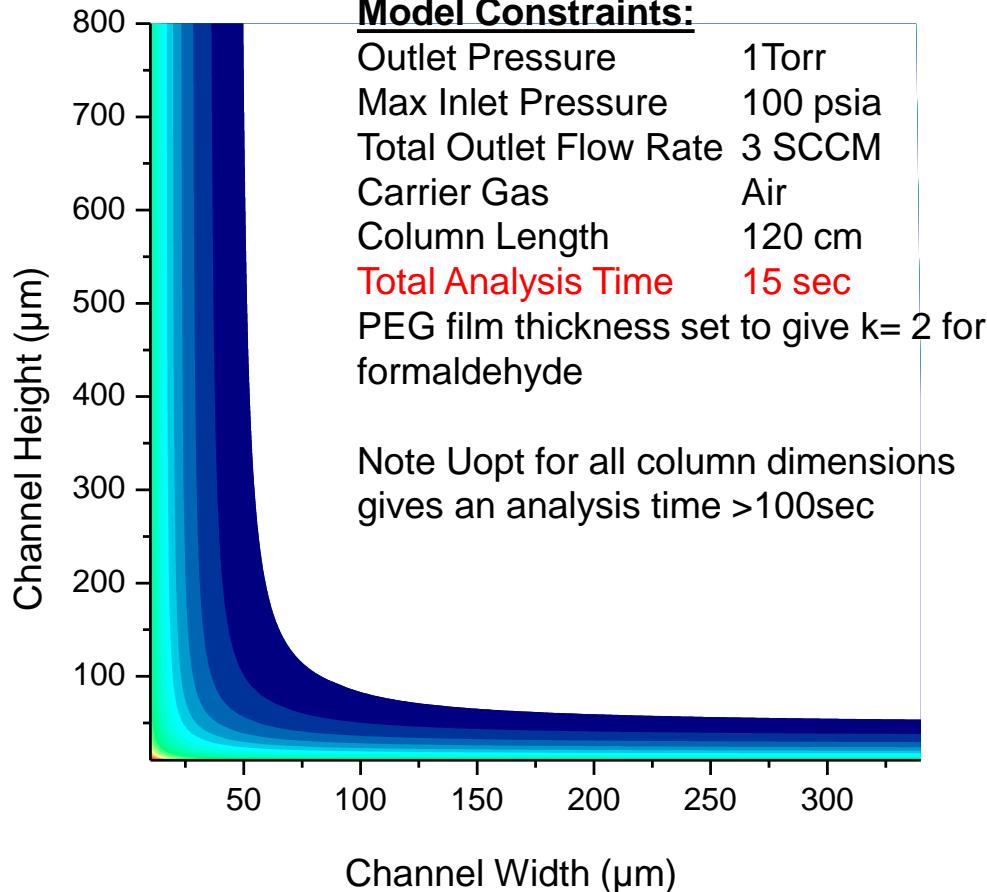
α = aspect ratio (always ≥ 1)

$$B = \frac{64}{35} \left[\frac{6.192(\alpha-1)^2}{(\alpha-0.1)^2} + 1.759 \right] + \frac{32}{5} \left[\frac{3.213(\alpha-1)^2}{(\alpha+0.2)^2} + 0.938 \right]$$

$$d_{f_c}^2 = \frac{\alpha+1 + \frac{2d_f}{w}}{\alpha+1} d_f$$

$$C = 16 \left[\frac{2\alpha^2}{(\alpha+1)^2} \right] + \frac{32}{35} \left[\frac{6.192(\alpha-1)^2}{(\alpha-0.1)^2} + 1.759 \right] + \frac{32}{5} \left[\frac{3.213(\alpha-1)^2}{(\alpha+0.2)^2} + 0.938 \right]$$

Model Result: 1D GC Isothermal Peak Capacity vs. Column Dimensions, With Constraints



Color bars represent total peak capacity achieved in 15 sec

Example: For $20\text{ }\mu\text{m} \times 500\text{ }\mu\text{m}$ channel dimensions, C_p achieved under these constraints would be ~ 40 .

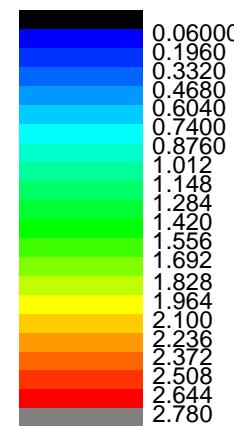
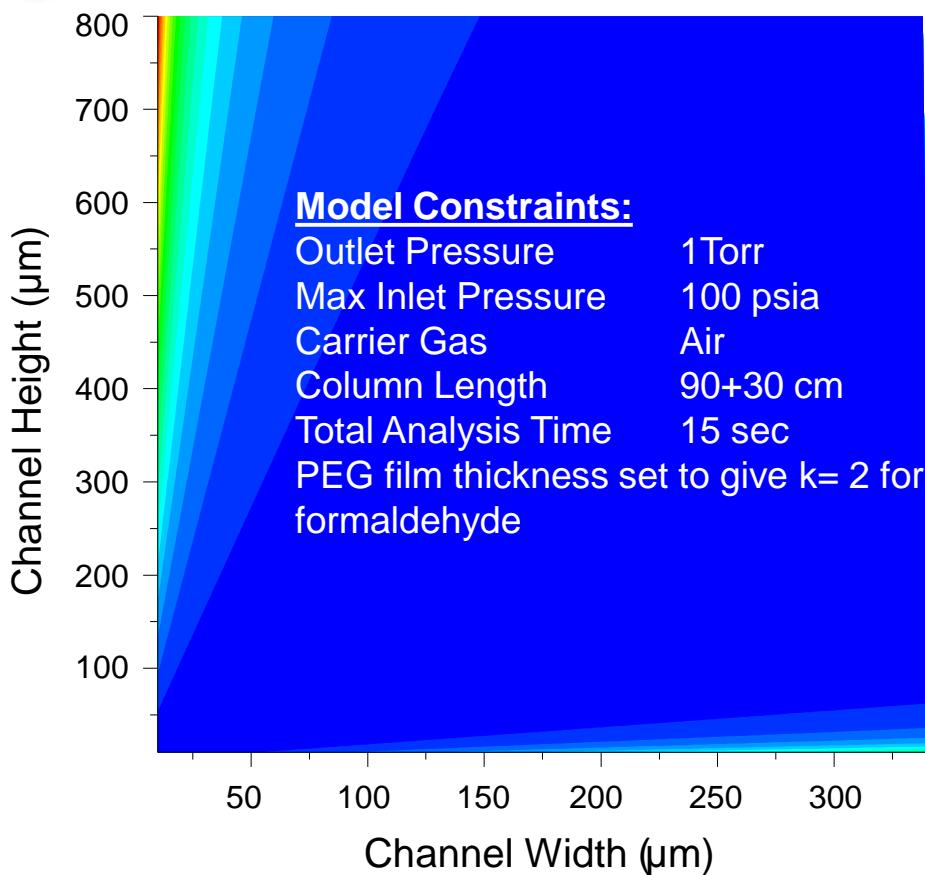
Extending to 1 min elution time gives modeled $C_p \sim 160$.

Increasing analysis time by 4X (to 1 min) would:

- Increase theoretical plates, N , by $\sim 4X$
- Increase C_p by $\sqrt{N} \sim 2X$
- For our example at $20\text{ }\mu\text{m} \times 500\text{ }\mu\text{m}$: Isothermal, 1D $C_p/\text{min} \sim 80$

- To achieve our target of $C_p/\text{min} = 300$ at the 3 sccm flow condition, we will need to “recover” a factor of 3X-4X in C_p/t over the model result, through use of GCxGC and T-programming.

Modeled Average Outlet Flow Rate (sccm) vs. Column Dimensions: Assumes GCxGC 50% duty cycle

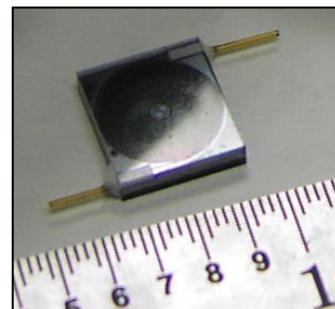
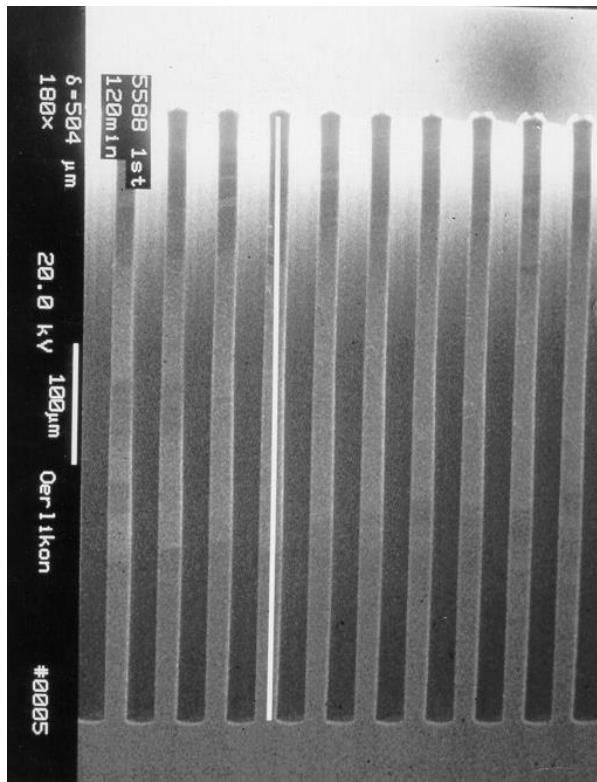


Color bars represent GCxGC outlet gas flow rate in SCCM

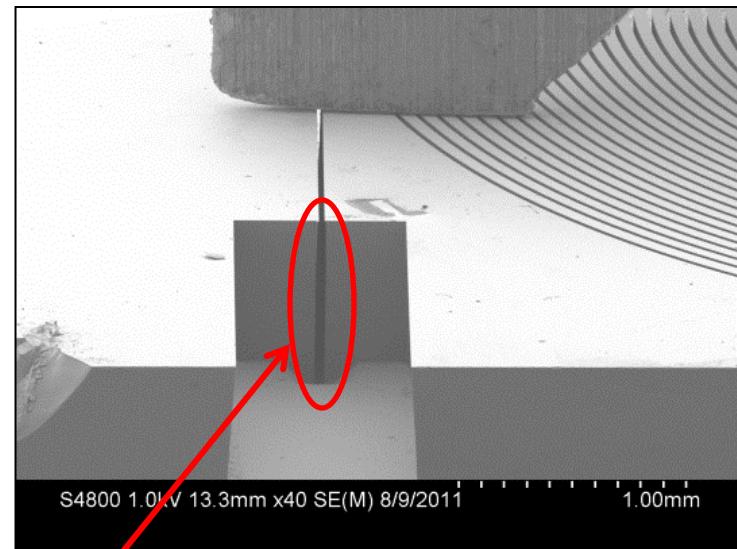
Example: For 20 μm x 500 μm channel dimensions, average gas flow under these constraints would be ~0.8 sccm.

- For our current column dimensions (30 μm x 685 μm) measured flow rates exceed model flows by up to ~3x
- Scaling to new dimensions (20 μm x 500 μm) allows a model safety factor to maintain flow < 3 sccm

New Micro GC Column Dimensions

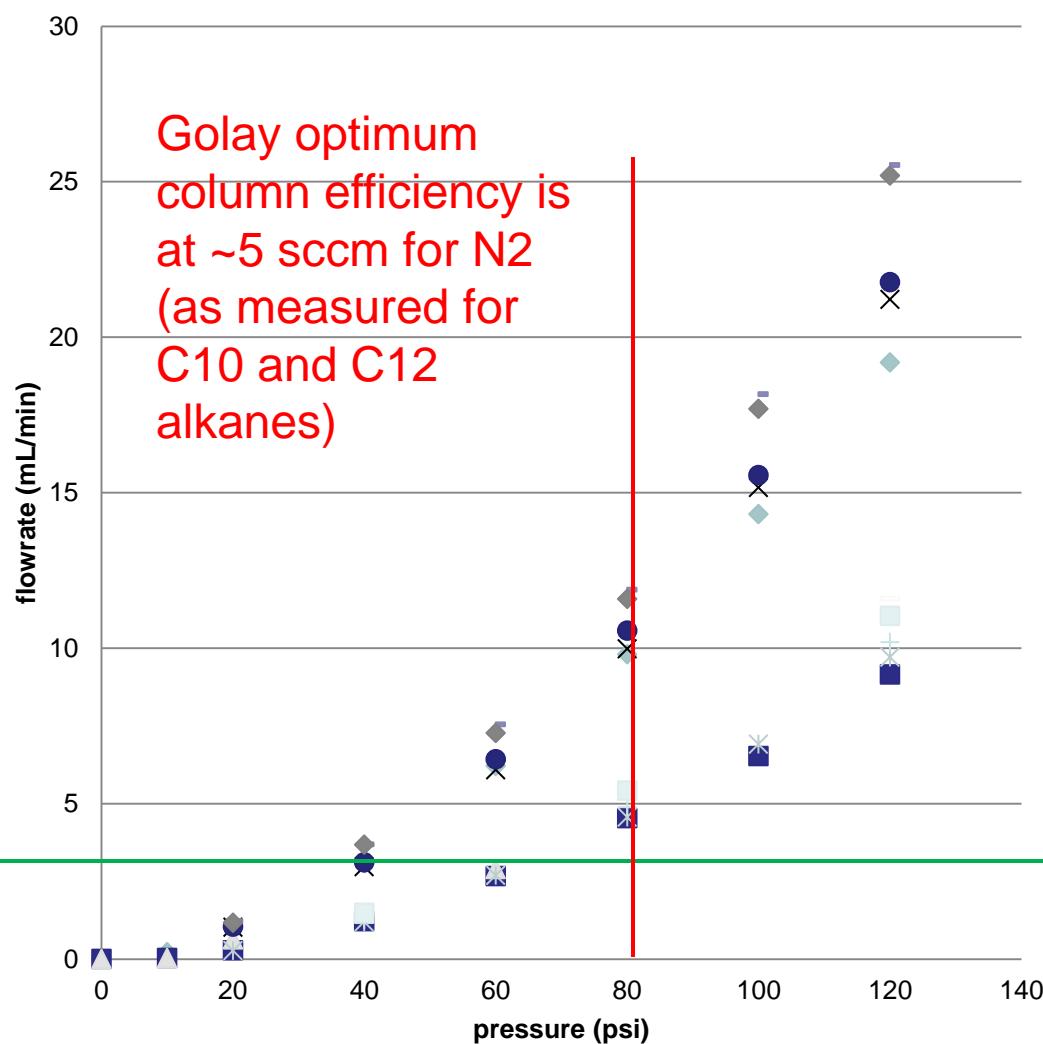


What's different?



- Column dimensions now 20 x 500 instead of 30 x 685 μm
- Column L = 1 m instead of 90 cm
- Aspect ratio of 25:1 at 20 μm critical dimension

Volumetric gas flow at outlet vs. inlet P for “20100” GC column using N2, He, and H2 carrier gases



B1-
Hydroge

B1-
Helium

B1-
Nitrogen

B2-
Hydroge

B2-
Helium

B-3 H2

B-3 He

A-1, H2

A1, He

A2,H2

Add note regarding column flow variation vs. critical dimension now 20 um not 30 um

This is a yield/manufacturing issue

System target flow rate, 3 sccm

“20100” GC column results to date: Significance

- Goal of model was to select dimensions that enable $C_p \sim 300$ in 1 minute for GCxGC, with outlet gas flow constrained to 3 sccm. Assumptions were made in the model regarding carrier gas, analyte diffusion coefficient, analyte retention index, and stationary phase volume ratio.
- Current results indicate that best column efficiency is found at 5-6 sccm rather than at 3 sccm
 - We may be able to affect this by changing phase volume ratio (modifying coating procedure).
- **The critical system issue: Restricting column flow increases sample injection peak width, which then restricts GC separation speed.**
 - Recall that extra-column effects dominate high speed GC performance.
 - Possible mitigation strategies:
 - Accept a sample split at the injector (increases system limit of detection)
 - Reduce system LOD by adding an ion multiplier at the Mass Spec?
Increases system pumping requirements, reducing portability.
 - Reduce sample injection volume even further (reduce PC dimensions)
 - Possible microfabricated cryofocusing? (cf. Zellers, et al.)

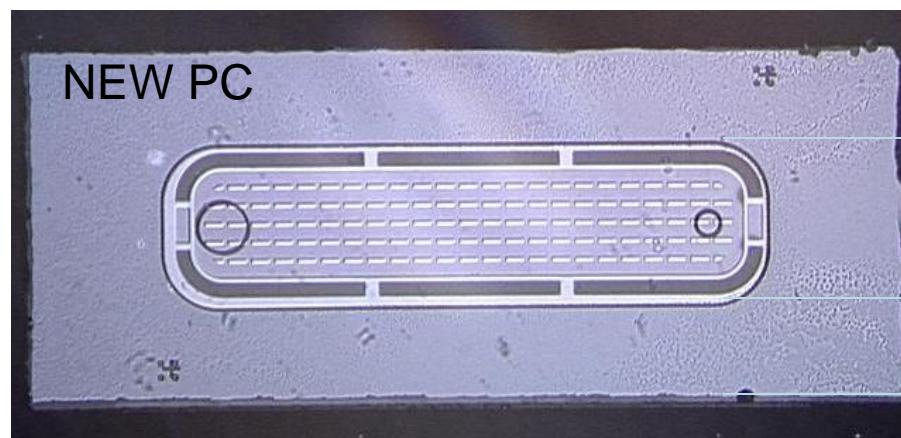
Modified Preconcentrator

Die dimensions unchanged, 9 mm x 3.4 mm



2070 μm

665 μm



1170 μm

1115 μm

PC volume
reduced by factor
of 1.76
(from 5 to 2.8 μL)

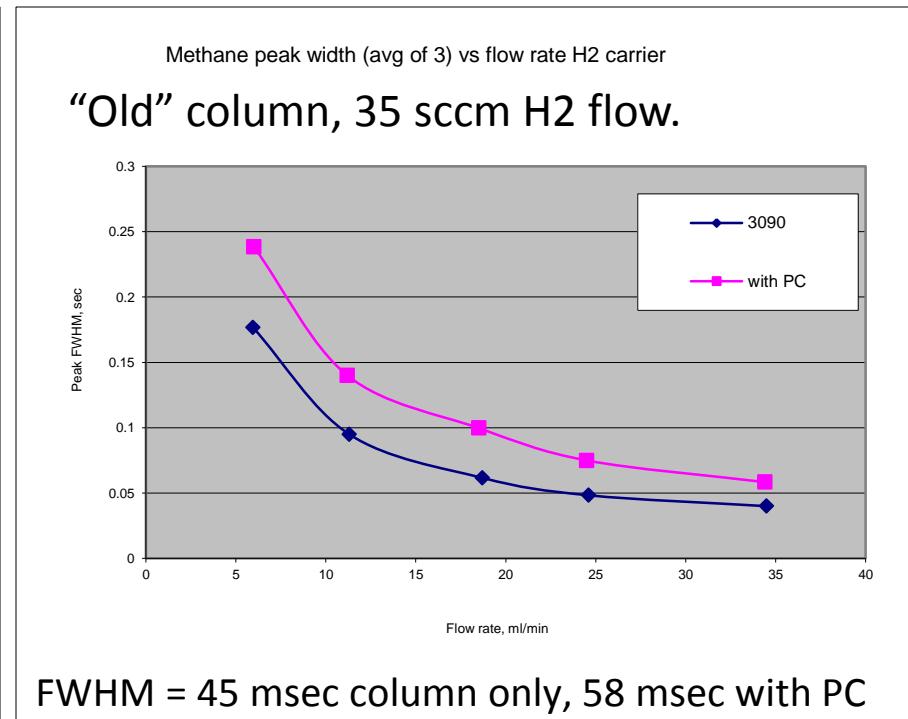
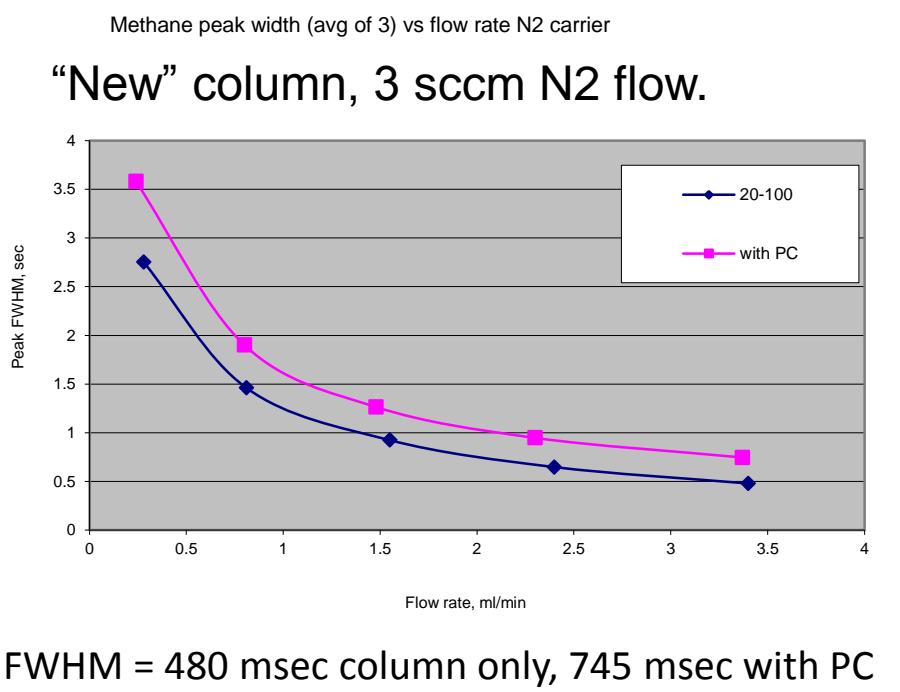
Surface area
available for
anodic bonding of
bottom glass
increased by 58%

Dominant PC
failure mode in
previous design
was failure of
bottom glass-Si
bond, causing gas
leakage

PC device yield increased from < 20% to approximately 75%

Preconcentrator Injection Peak Width vs. GC Outlet Flow

- Peak widths measured at FWHM for methane injection through columns at representative flow rates, with and without preconcentrators in the flow path.
- Note that methane results are “best case”: Dominated by convective flow and diffusion rates with no broadening due to chemical retention and PC desorption kinetics.



- Injection peak width required to achieve our separation performance goal of $C_p/t \sim 5$ is 200 msec at baseline, or ~ 118 msec FWHM.
- This target injection width was achieved with “old” columns at high flow, but not with new low flow columns.



Microfabricated GCxGC System: Summary

- Our design utilizes high aspect ratio GC columns to maximize peak capacity production per unit analysis time, **BUT...**
- **Sample injection, not on-column broadening, dominates fast GC performance.**
- We have designed a microvalve injector system to minimize injection peak width while maintaining splitless injection to maximize system sensitivity.
- System performance is closely coupled to operating constraints:
 - GC column dimensions have been optimized for C_p/t production at low carrier gas flow rates, in order to reduce mass spectrometer pumping requirements, **BUT...**
 - Reducing volume flow at outlet greatly reduces linear flow velocity at inlet (preconcentrator), which in turn slows GCxGC separation speed.
 - To mitigate this, we need to:
 - Reduce PC volume even further.
 - Accept a split and/or higher column flow.
 - Refocus injection on column or on a micro cryofocusing component.



Acknowledgements

- Collaborators:

Prof. Mike Ramsey, et al., University of North Carolina

Prof. Michael Roukes and Dr. Edward Myers, Caltech

Dr. Adam McBrady, Honeywell

Patrick Lewis and Dr. Doug Adkins, Defiant Technologies

Darin Graf, Gentech Concepts

- Support:

