

COMPUTATIONAL TEST DESIGN FOR HIGH-SPEED LIQUID IMPACT AND DISPERSAL

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Primary Goal:

In preparation for some testing to validate a unique impact to fireball computational capability, we are first simulating the environment to understand how best to instrument the test.

Methods:

- **Water dispersal from the braking of a rocket sled will be used to evaluate code capability.**
- ***Sierra/StructuralDynamics* Presto code for structural dynamics**
- ***Sierra/FluidMechanics* Fuego code for predicting reacting flows**
- **It is hoped that this capability will address aircraft impact simulation needs for scenarios like that of September 11, 2001**



Outline

- **Introduction and Demonstration of Past Work**
 - Novel Methods Introduction
 - Water Slug Impact Validation
 - Heptane Cube Impact
- **Methods**
 - Description of Rocket Test
 - Description of Simulation Matrix
- **Simulation Results (First Round)**
- **Subsequent Simulation Findings**
- **Summary**

Code Details

- **Presto SPH used for highly deforming structure and water**
 - Using constants to approximate liquid behavior
 - Typical runs on ~100 CPUs for a few days
- **Fuego CFD Lagrangian/Eulerian Drop Models used:**
 - Reactions modeled with Eddy Dissipation Concept (EDC) reactions and Temporal Filtering of the Navier-Stokes Equations (TFNS) turbulence model
 - Multiple levels of mesh refinement
 - Drop breakup with a modified Taylor Analogy Break-up (TAB) model
 - Typically run on ~200 CPUs for around 8 days

Simulation Codes

- Coupling methods are significant, and have required study and development to best model these scenarios
- Dimensionless drop separation distance used to define transfer time appropriate for individual drops:

$$B = \frac{\textit{CharacteristicSeparationDistance}}{\textit{CharacteristicDropLength}}$$

- Presto products initialized as spheres in Fuego
- Aluminum (casing) ignored in Fuego
- Impacting drops all stick in Fuego

Illustrating the Physics Challenge

| Presto | Phenomena | Fuego |
|--------|----------------------------------|-------|
| ✓ | Gravity Force | ✓ |
| ✓ | Structural Deformation | |
| ✓ | Mass Conservation | ✓ |
| ✓ | Momentum | ✓ |
| ~ | Energy Conservation | ~ |
| ✓ | Structural Material Interactions | |
| ~ | Sensible Energy | ✓ |
| ~ | Surface Tension Forces | ~ |
| ~ | Liquid Phase Viscous Forces | ~ |
| ~ | Gas Phase Transport | ✓ |
| ~ | Multiphase Interactions | ~ |
| ~ | Chemically Reacting Flows | ✓ |
| ~ | Wind | ✓ |
| ~ | Turbulence | ✓ |
| ~ | Thermal Response of Materials | ✓ |



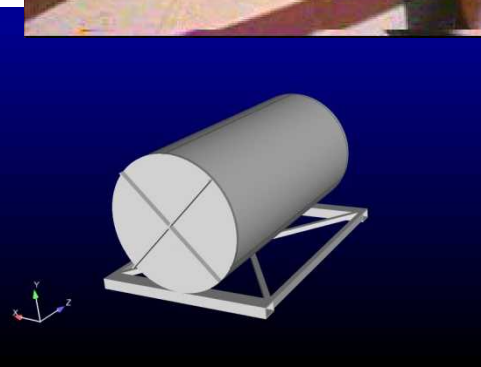
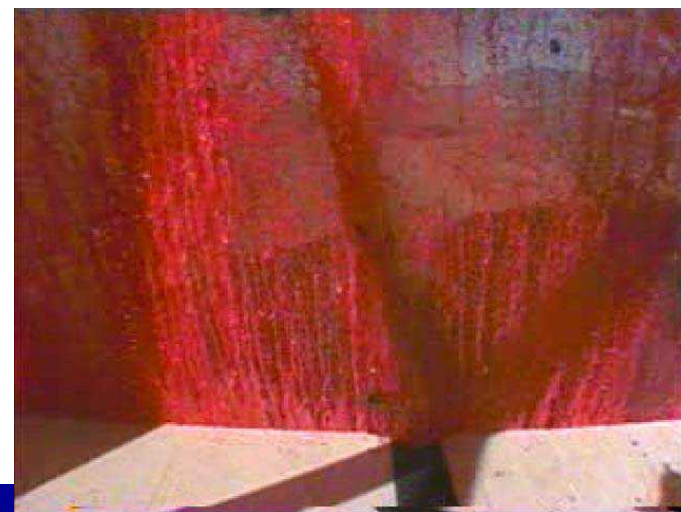
Scenarios

Two previous cases are presented here as introduction:

- **Validation to a large-scale water tank impacting a concrete barricade**
 - Brown A.L., Wagner, G.J., “Fluid Spread Model Validation for Emerging Liquid Tank Impact Predictive Methods,” Accepted to the ASME IHTC Conference, ASME IHTC-2010, August 8-13, 2010, Washington DC, USA, IHTC14-23067.
- **A notional impact of a 0.3 m square tank of heptane**
 - Brown A.L., “Impact and Fire Modeling Considerations Employing SPH Coupling to a Dilute Spray Fire Code,” Proceedings of the ASME 2009 Summer Heat Transfer Conference, ASME SHTC-2009, July 19-23, 2009, San Francisco, CA, USA, HT2009-88493.
 - Brown A.L., “Impact and Fire Modeling for Complex Environment Simulation,” The 2010 Western States Meeting of the Combustion Institute, Paper # 10S-12, March 21-23, 2010, Boulder, CO, USA.

Impact Validation

- Tests performed in 2002 provided data for validating liquid spread dynamics for an aluminum tank impacting a concrete slab
- Liquid deposition, particle sizing, and video data



Simulation Matrix

- Wind was not reported, so it was treated as a free parameter
- Geometry fidelity was examined, including undercarriage and cross-member for high fidelity
- Various temporal staging assumptions were analyzed

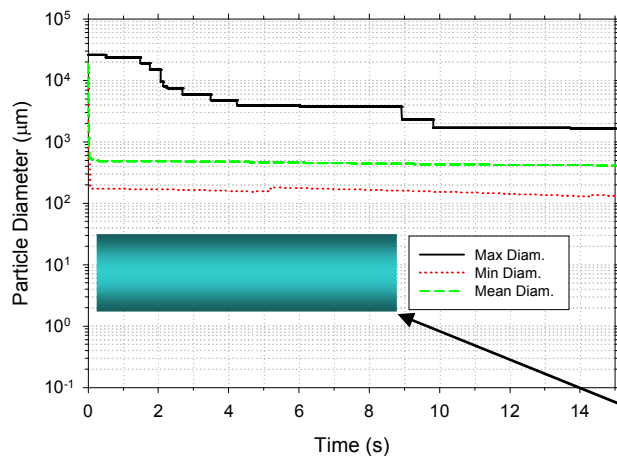
Fluid Test Matrix

| Case | Geometry Fidelity | Wind | Temporal Staging |
|--|-------------------|-------|------------------|
| 1 | Low | No | No |
| 2 | Low | No | 5 times* |
| 3 | High | No | 6 times** |
| 4 | Low | 2 m/s | No |
| 5 | Low | 1 m/s | No |
| 6 | High | No | 11 times** |
| 7 | High | 1 m/s | 11 times** |
| * Dimensionless Staging Distance: 1.7 | | | |
| ** Dimensionless Staging Distance: 1.5 | | | |

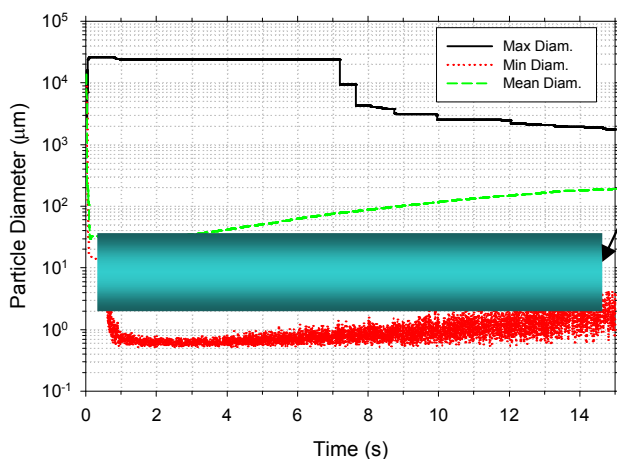
Drop size and Spread Distance Results

- Simulation matrix evaluated transfer coupling, geometry fidelity, and wind assumptions

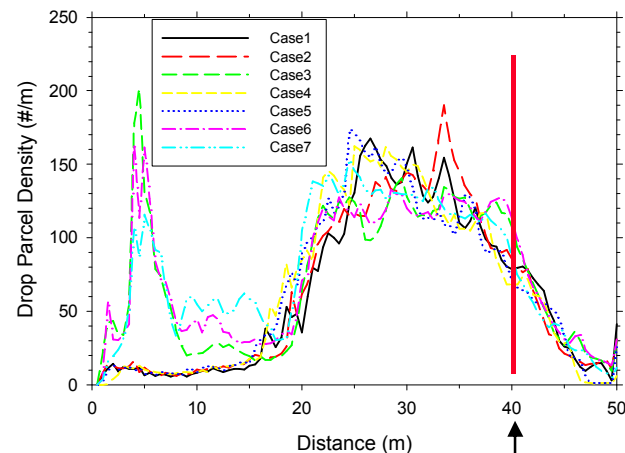
Low Geo. Fidelity



High Geo. Fidelity



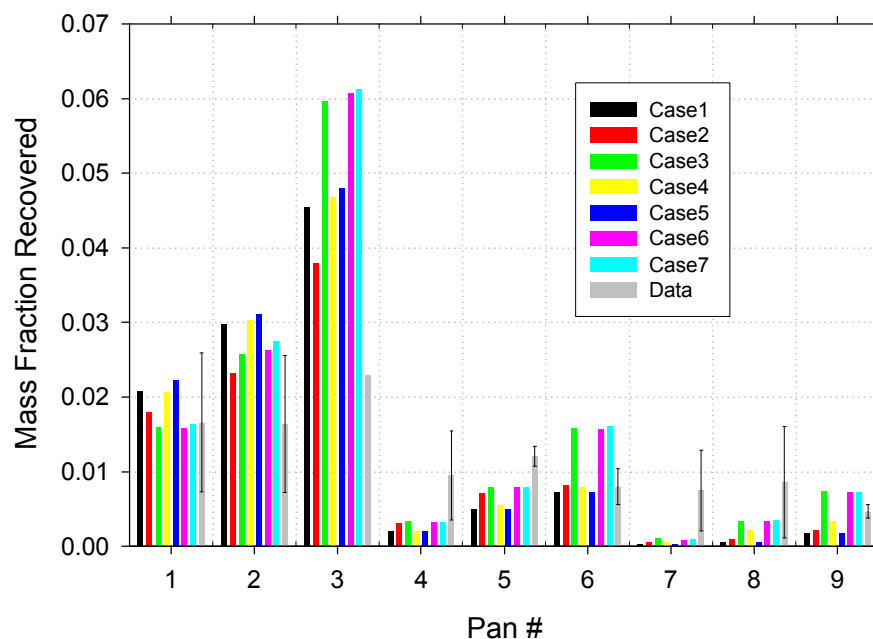
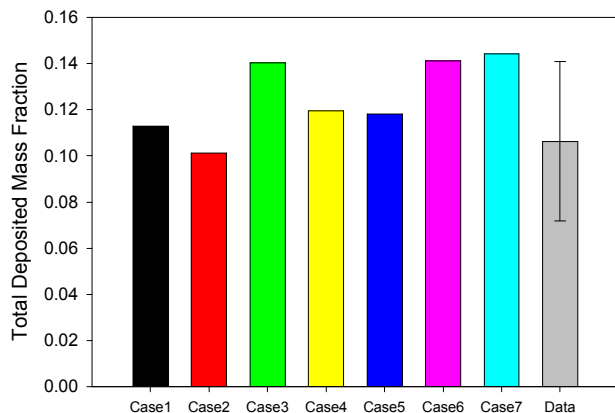
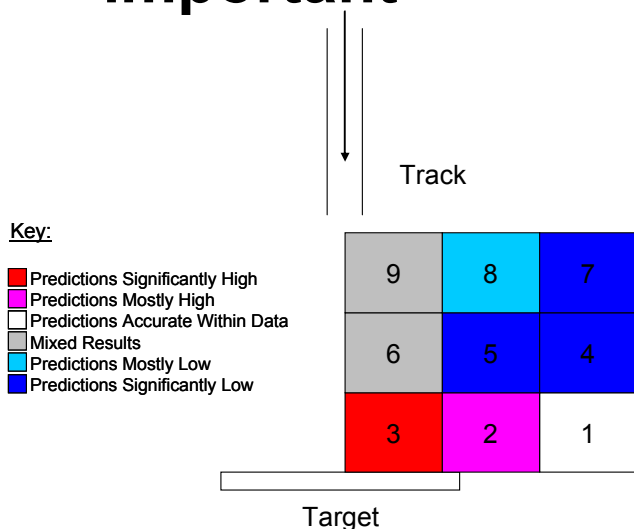
Data



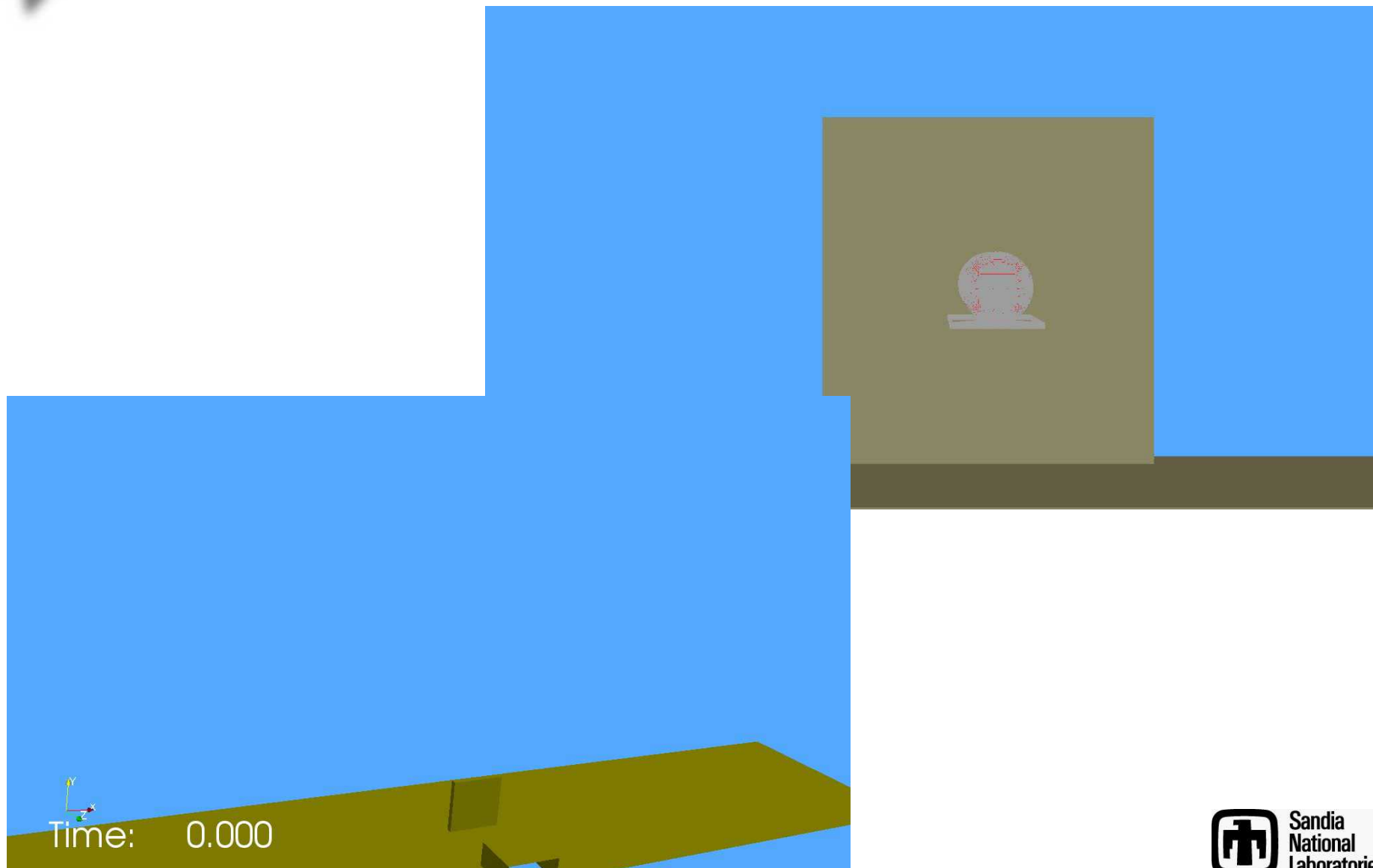
Data Peak

Liquid Deposition Results

- Geometry fidelity was found to be most significant, and coupling methodology was also important



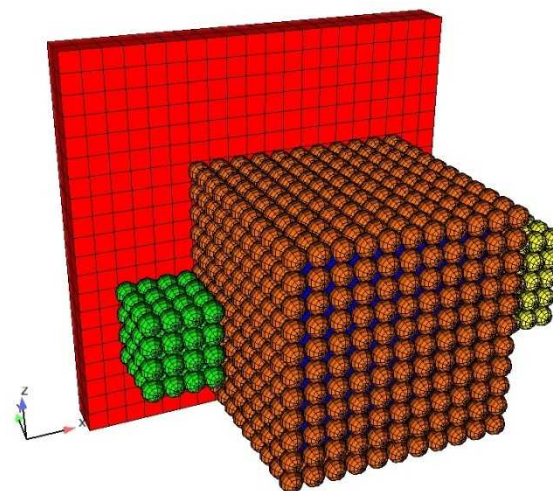
Simulation Videos



The Scenario

Designed to help understand discretization sensitivities

- **23 cm cube of liquid in a 2.54 cm thick aluminum tank with two adjacent cubes**
 - Impact an immobile target at 182 m/s
 - Presto modeled with SPH and 4 levels of refinement
- **Open air environment with ground located 6.35 m below impact point**
 - Two levels of fluid mesh refinement



Simulation Matrix

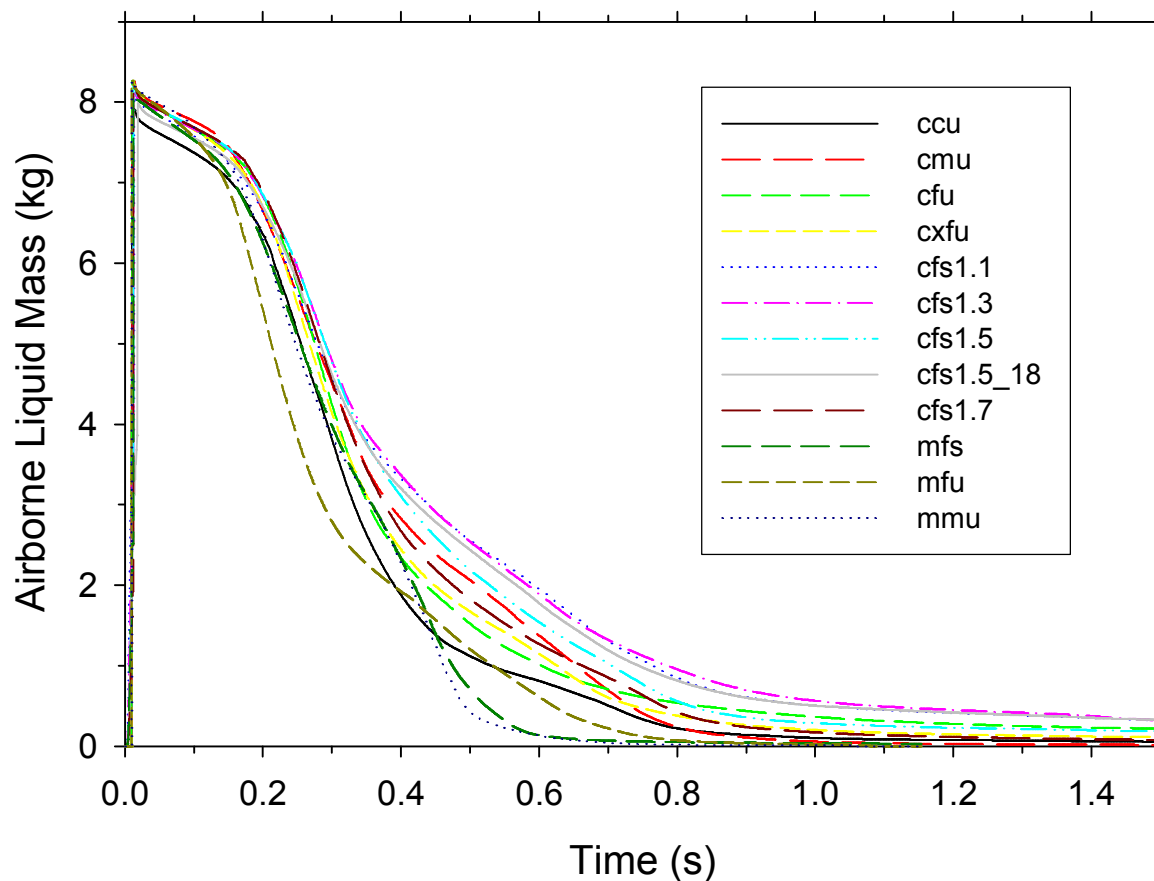
- Cases are named to indicate meshes used and staging assumptions
- Differences between cases reflect accuracies with discretization and staging

| Case | Fuego Mesh | Presto Mesh | Temporal Staging | Dimensionless Spacing |
|-----------|------------|-------------|------------------|-----------------------|
| ccu | coarse | coarse | No | |
| cmu | coarse | medium | No | |
| cfu | coarse | fine | No | |
| cxfu | coarse | xfine | No | |
| cfs1.1 | coarse | fine | Yes | 1.1 |
| cfs1.3 | coarse | fine | Yes | 1.3 |
| cfs1.5 | coarse | fine | Yes | 1.5 |
| cfs1.5_18 | coarse | fine | Yes* | 1.5 |
| cfs1.7 | coarse | fine | Yes | 1.7 |
| mfs | medium | fine | Yes | 1.5 |
| mfu | medium | fine | No | |
| mmu | medium | medium | No | |

*All staged cases use 1 ms steps out to 12 ms except this one, which uses 1 ms steps out to 18 ms.

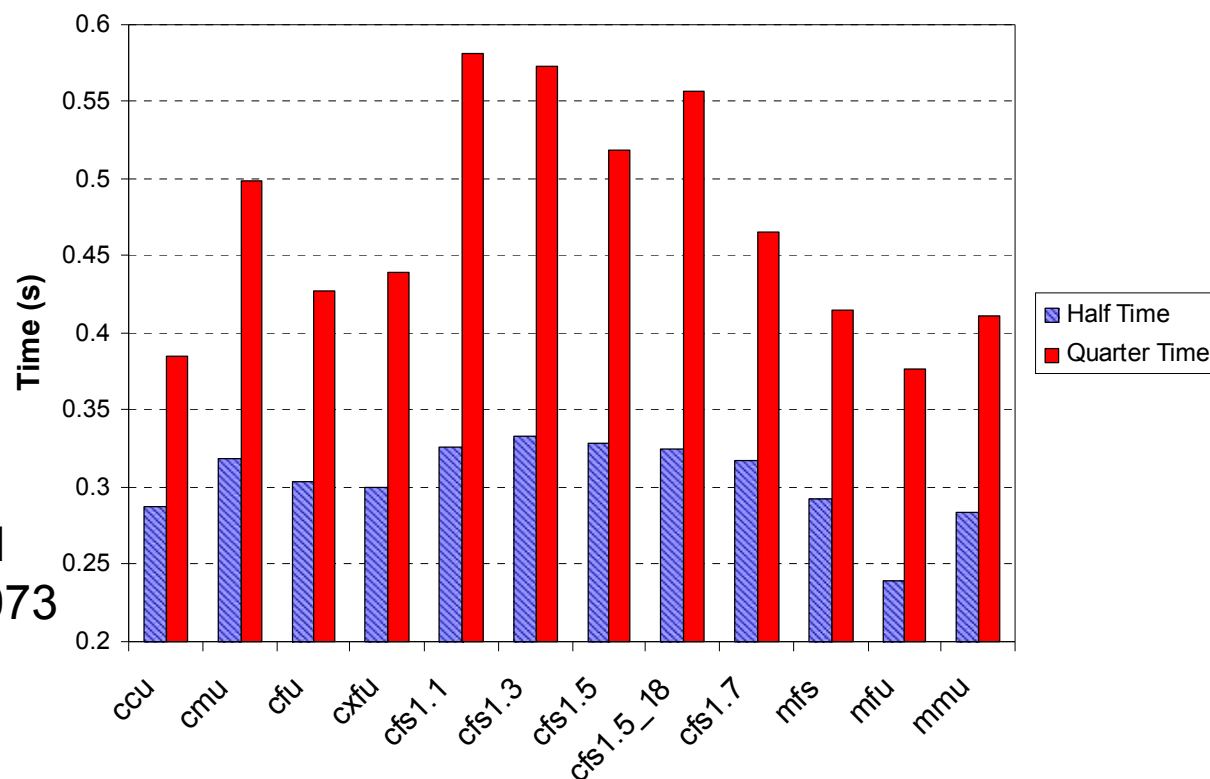
Mass Results (1/2)

- Results are relatively similar, with subtle differences not well illustrated by line plots.



Mass Results (2/2)

- Mass loss is slower for staged predictions
- Mass loss is faster for medium Fuego mesh
- Moderate trend depending on dimensionless spacing magnitude assumed

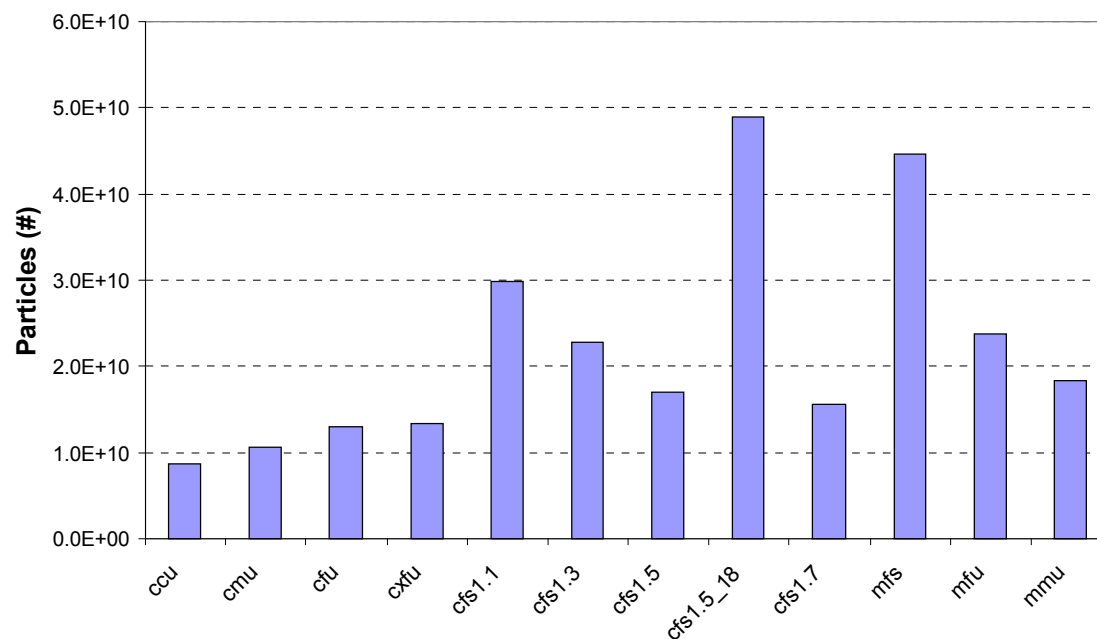


half avg. = 0.305
half st.dev. = 0.026

quarter avg. = 0.471
quarter st.dev. = 0.073

Maximum Predicted Particles Results

- Staging appears to increase break-up
- Finer Fuego mesh yields more particles
- Dimensionless spacing significant to result
- Small to moderate effect of Presto resolution
- 18 ms case results in substantially more particles

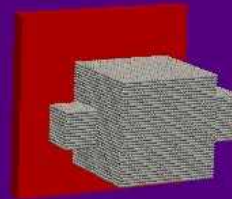


avg. = $2.2e10$
st.dev. = $1.29e10$

log avg. = 10.29
log st.dev. = 0.23

Coarse Video

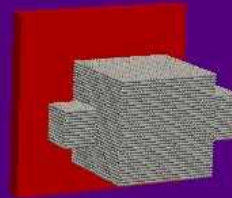
- Case cfs1.5



Time: 0.0000 s.

Medium Video

- Case mfs
- Substantial increase in resolution of the fireball

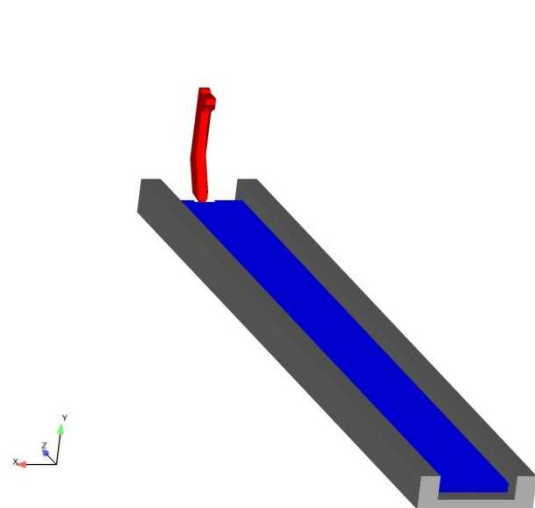


Time: 0.0000 s.

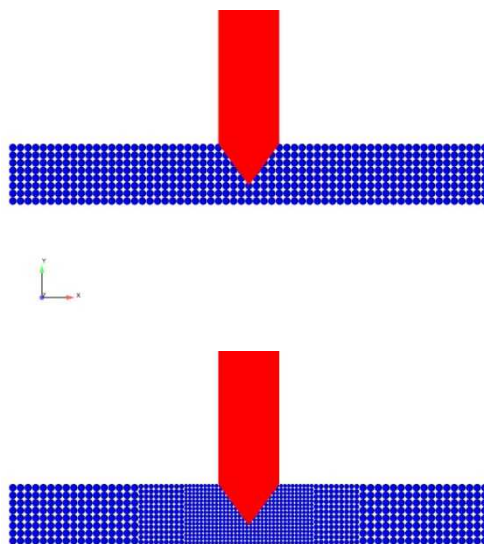
Sled Track Simulation Details

These simulations are pre-test design calculations to locate instruments for validation data:

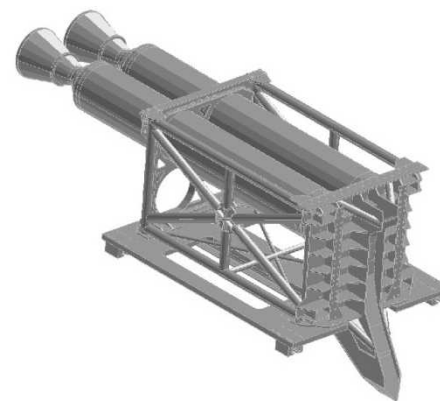
- liquid dispersal velocity (photometrics)
- local droplet size distributions and velocities (Malvern Spraytec and phase Doppler particle analyzer)
- ground level liquid deposition (catch pans)
- droplet evaporation and vapor transport (RH sensors)



Initial Presto Geometry



Two Mesh Densities Used



Designed Geometry

Simulation Matrix

The simulation matrix involved three Presto calculations and four Fuego calculations.

Structural Test Matrix

| Simulation | Water Element Size (cm) | Water Draw (cm) | Initial Scoop Velocity (m/s) |
|------------|-------------------------|-----------------|------------------------------|
| S1 | 1.9 | 10.2 | 146 |
| S2 | 1.9 | 15.9 | 91.4 |
| S3 | 0.95-1.9 | 10.2 | 146 |

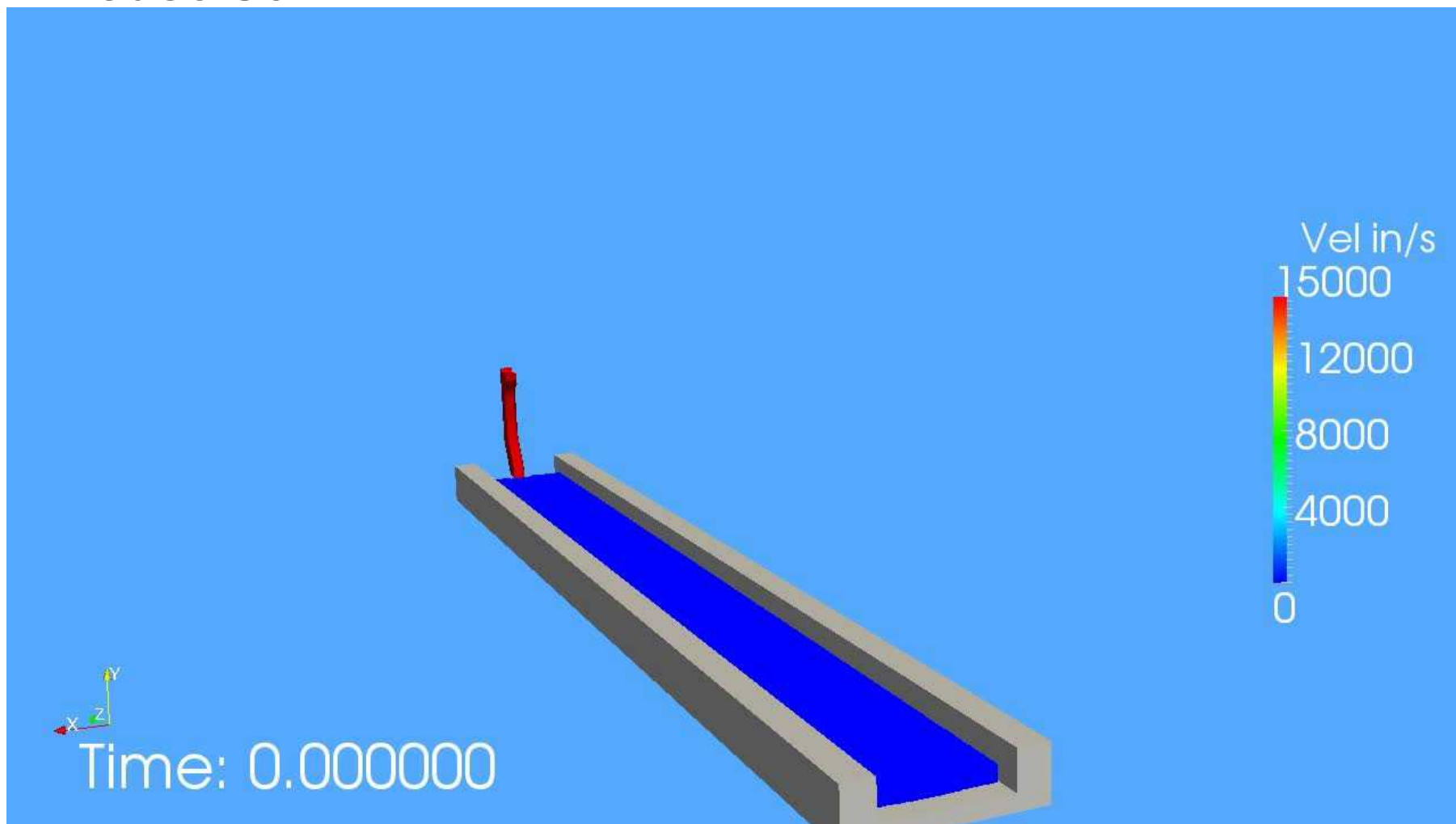
Fluid Test Matrix

| Fuego Simulation | Presto Sim. | Simulation Transfer Time (s) | Number of Transfers | Fuego Mesh Elements (Thousands) |
|------------------|-------------|------------------------------|---------------------|---------------------------------|
| F1 | S1 | 0.01-0.10 | 10 | 700 |
| F2 | S2 | 0.02-0.24 | 11 | 700 |
| F3 | S3 | 0.01-0.11 | 11 | 700 |
| F4 | S1 | 0.01-0.10 | 10 | 2,000 |

$$B=1.3$$

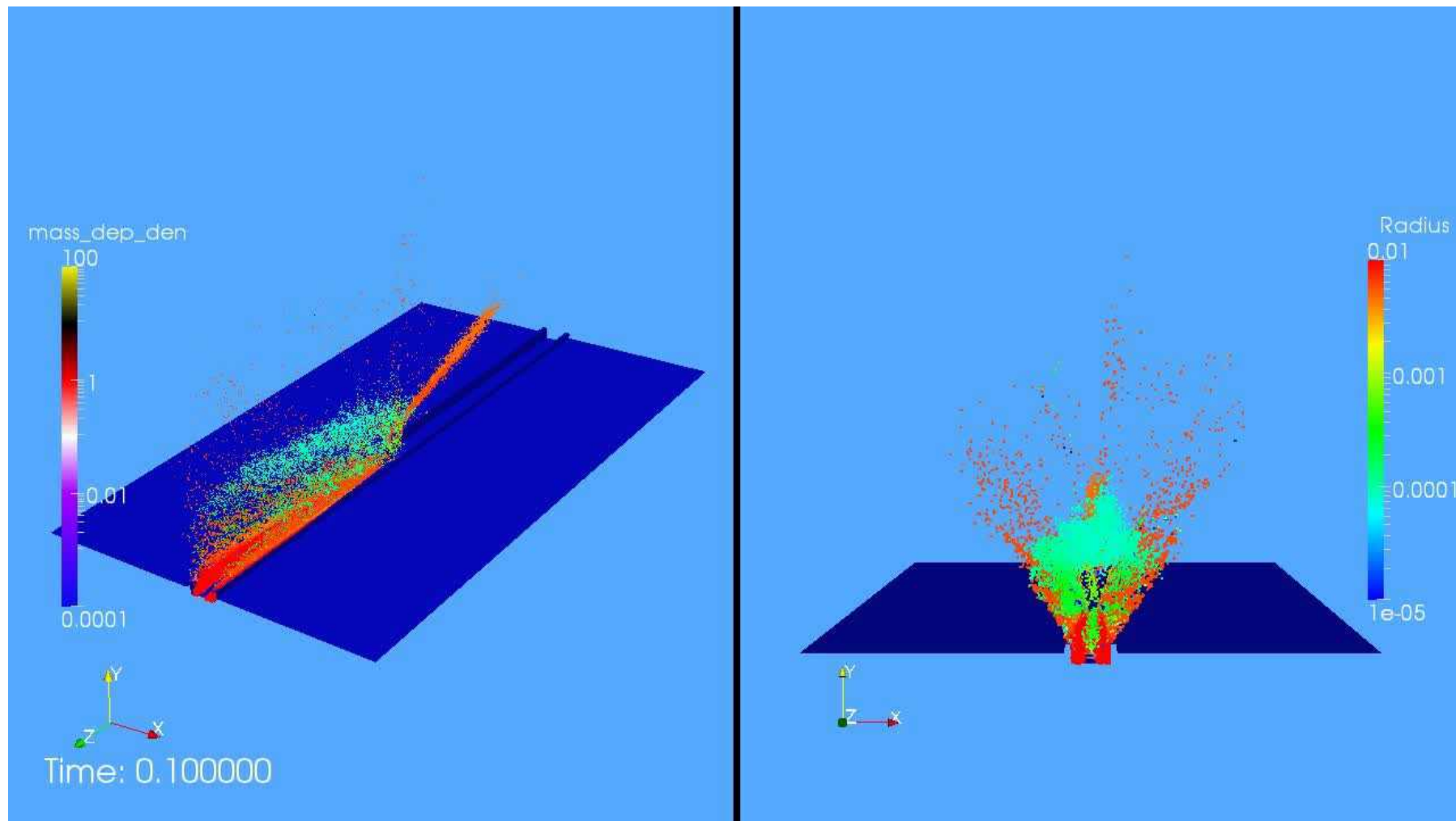
Sled Track Presto Video

Case S3



Sled Track Fuego Video

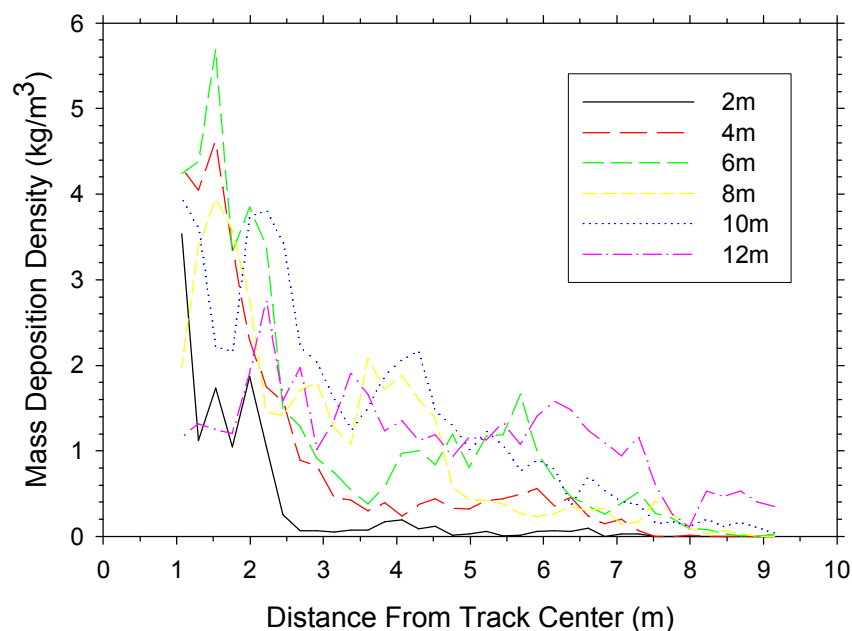
Case F1



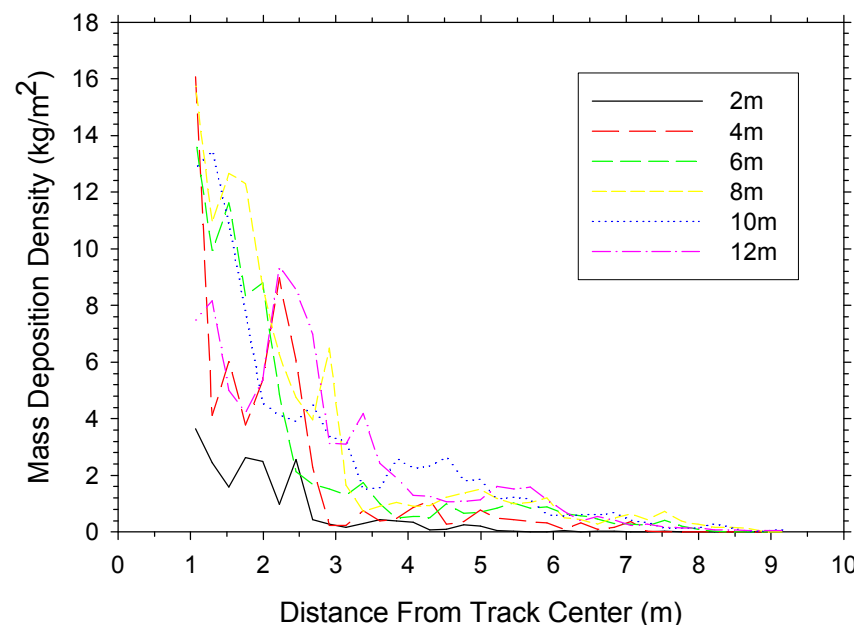
Predicted Environment

Ground deposition and air water vapor concentration predictions help locate instrumentation

Lesson: Catch pans need to be close to the track



Case F1 Deposition at Various Distances

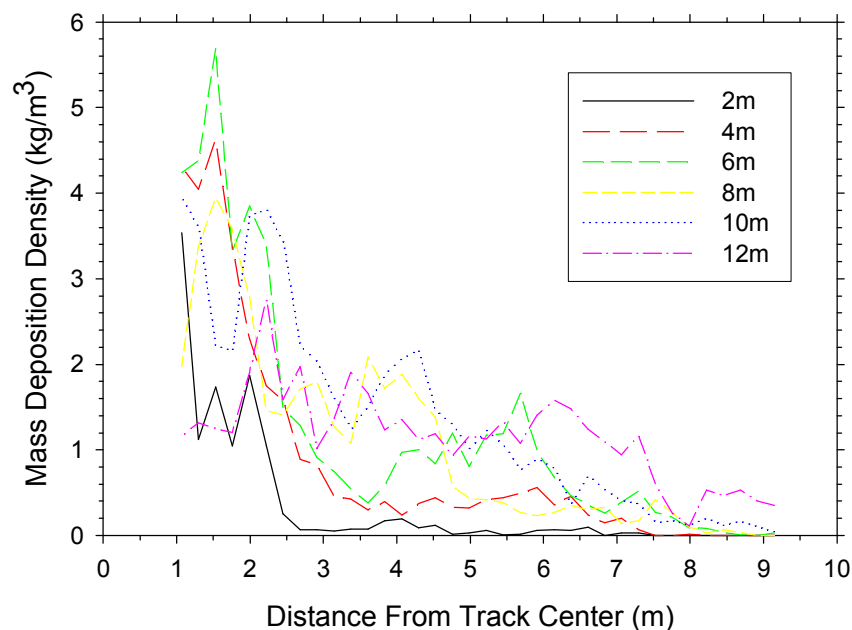


Case F2 Deposition at Various Distances

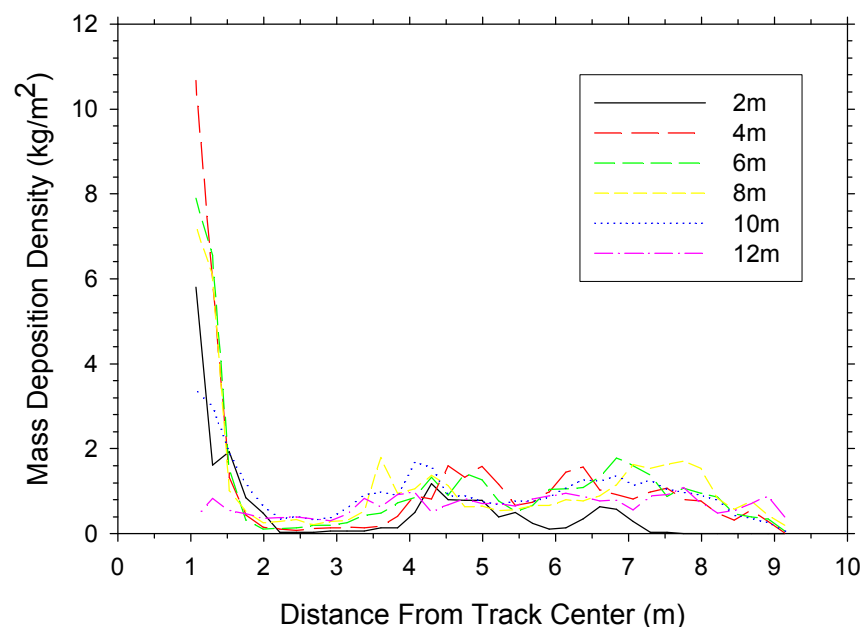
Structural Resolution Differences

Two otherwise identical cases with varying SPH resolution gave significantly different results (below)

The explanation did not make the conference paper



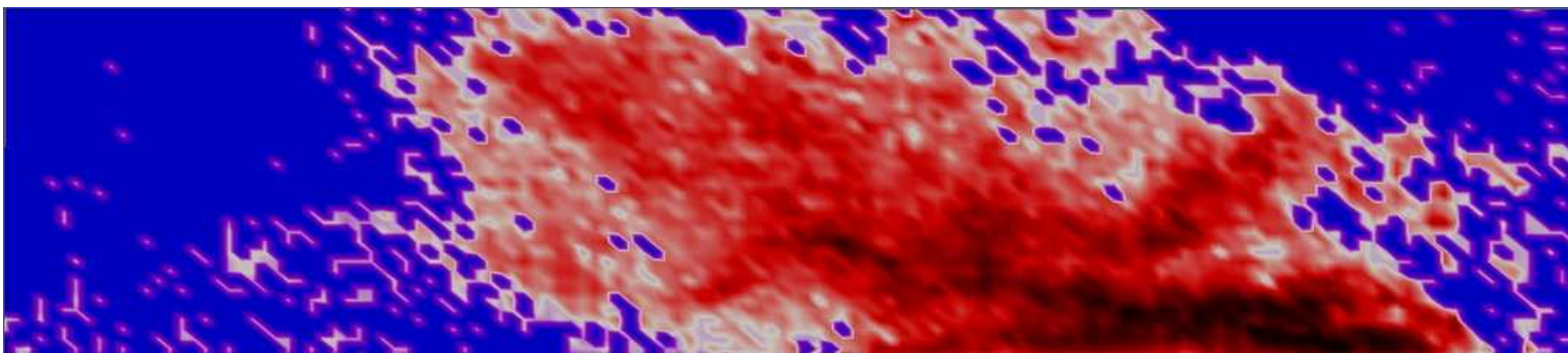
Case F1 Deposition at Various Distances



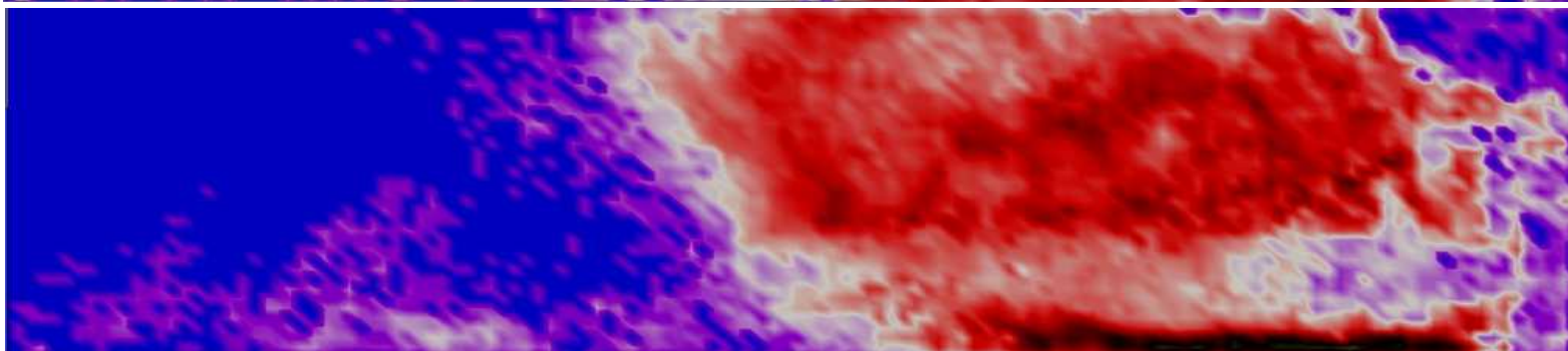
Case F3 Deposition at Various Distances

Deposition for SPH Resolution Increases

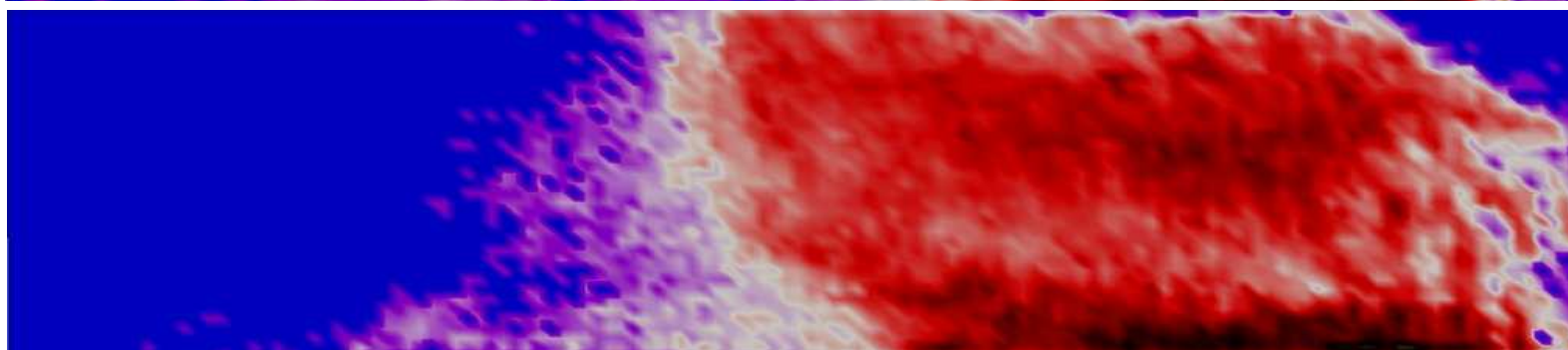
F1



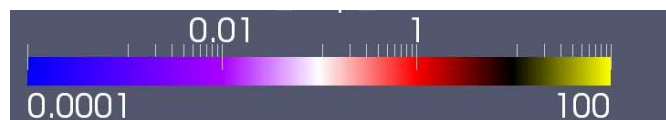
F3



Further
refinement



Mass Deposition Density
[kg/m²]



Issue Resolution

- A subsequent (additional) SPH refinement case was performed.
- Dip in deposition and recovery results were similar to the intermediate refinement case (S3/F3).
- Results were more similar in general.
- This demonstrates a length scale refinement sensitivity for this calculation methodology
 - Not clear yet if it is only expressed in the fluid code, or the structural code as well
 - More work needs to be done to fully understand mesh sensitivity

Summary

- A new capability exists to predict fires from impact scenarios involving code coupling.
- Model validation work is ongoing, with existing validation suggesting the accuracy of the capability.
- Modeling resolution assumptions including discretization and coupling transfer method have been analyzed, and are shown to be important to the predictive results.
- Predictions help locate instrumentation for the test.
- The validation work provides confidence in being able to employ these capabilities for other similar scenarios.
- Future work includes additional validation and scenarios more closely related to the application space.



Acknowledgements

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This work was made possible by support from the Sandia C6, LDRD, and ASC programs.

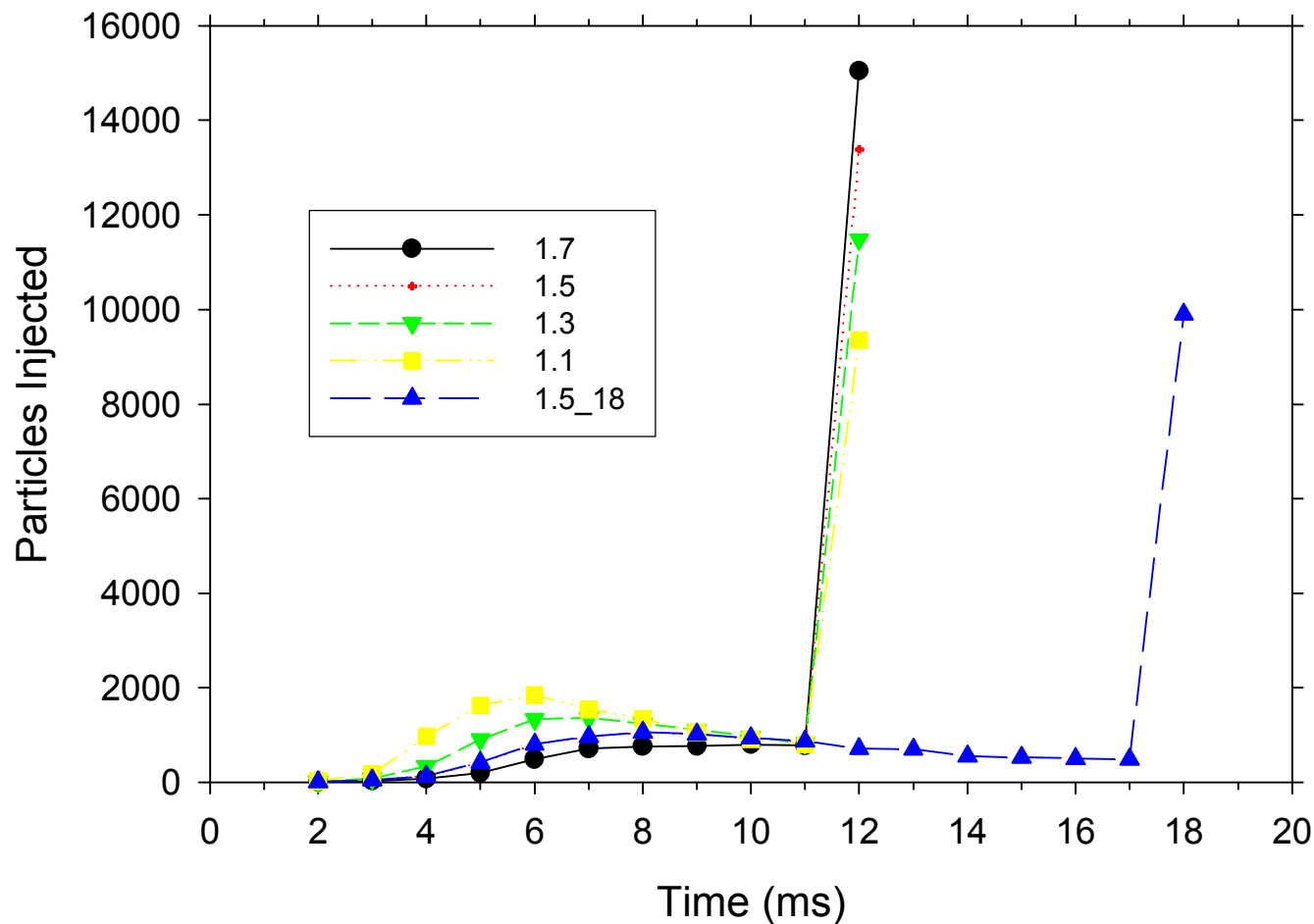
Significant contributions from Greg Wagner and Kurt Metzinger aided in the development of this capability.

Extra Viewgraphs

Properties

| Property | Units | Value |
|----------------------|-------------------|----------|
| Heat of Vaporization | kJ/kg | 310 |
| Boiling Temperature | K | 371.58 |
| Critical Temperature | K | 540.3 |
| Density | kg/m ³ | 692 |
| Thermal Conductivity | W/m/K | 0.15 |
| Specific Heat | J/kg/K | 2100 |
| Viscosity | kg/m/s | 0.000542 |
| Absorptivity | -- | 0.05 |
| Surface Tension | Nm | 0.0216 |

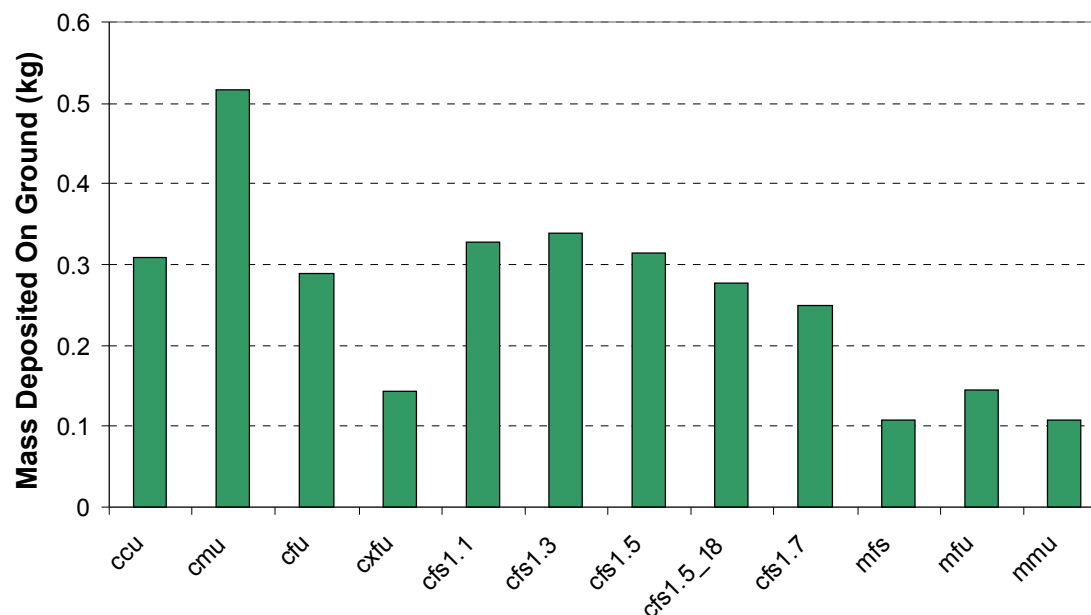
Coupling Details



Ground Deposit at 1.0 s

Deposit mass almost identical from 0.4 to 1.25 seconds: early versus late deposit

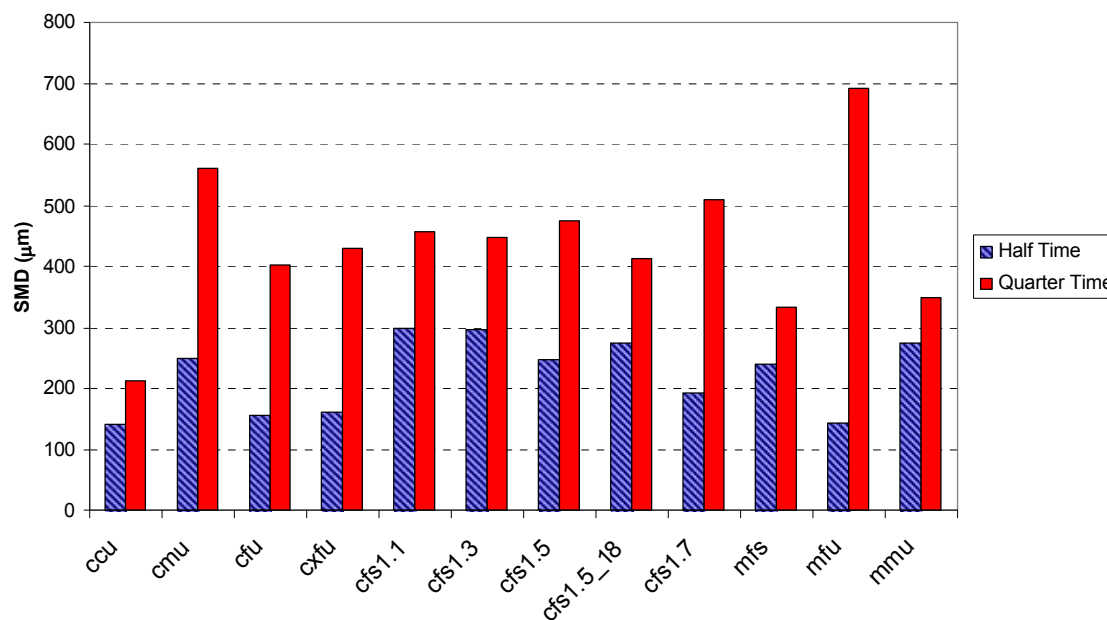
- Any refinement mostly lowers deposit
- Dimensionless spacing has minor effect



avg. = 0.261
st.dev. = 0.119

Sauter Mean Diameter

- No particular trends evident
- Uniformly, larger average drops predicted at later times



half avg. = 222.5
half st.dev. = 60.5

quarter avg. = 439.6
quarter st.dev. = 119.7