

Updated jet flame radiation modeling with buoyancy corrections

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In 2008, Air Products commissioned radiative heat flux measurements from 2 large-scale H₂ jet flames.

Flame	d_j [mm]	\dot{m} [kg/s]	L_f [m]	p_0 [barg]	T_0 [K]	RH [%]	T_{amb} [K]	p_{amb} [mbar]	U_{wind} [m/s]	Wind dir [°]
1	20.9	1.0	17.4	59.8	308.7	94.3	280	1022	2.84	68.5
2	52.5	7.4	48.5	62.1	287.8	94.5	280	1011	0.83	34.0

Flame 1



Horizontal jet flame tests were performed by GL Noble Denton (then Advantica) at the Spadeadam test site in North Cumbria, UK

Flame 2

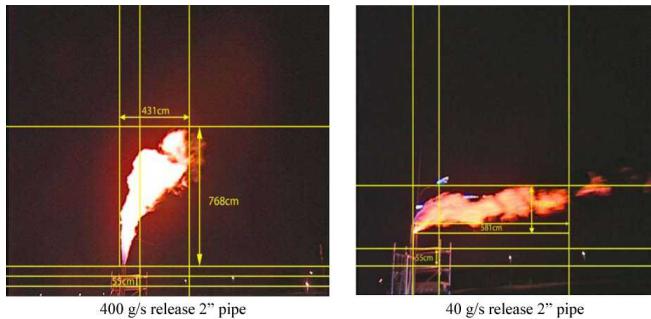


Analytic models did a poor job of predicting radiative heat fluxes from these flames... Why?

Simplified methods exist to model radiative heat flux boundaries from jet flames & flares

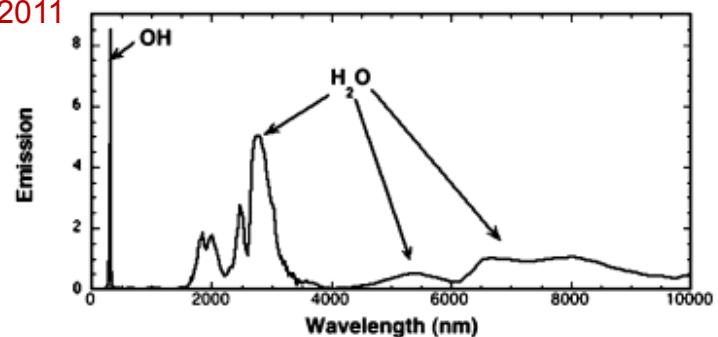
All methods require models of the following parameters:

1) Flame envelope ▶



Willoughby et al., ICHS4, 2011

2) Energy fraction converted to radiation ▶



Schefer et al., IJHE, 2009

◀ 3) Radiant energy transferred to observer

Models are often interdependent and only applicable for the given method

It is convenient to define jet flame/flare radiative heat flux models into 3 categories:

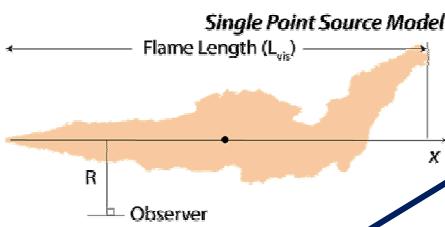
Single Point Source (SPS) models

Flame shape:

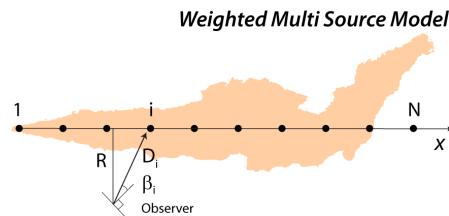
- Non-dimensional radiant power to estimate radiant load distribution

Radiant fraction models:

- Empirical function: **temperature, composition, release rate, soot, residence time, heat release**



Multi Source Models (MSM)



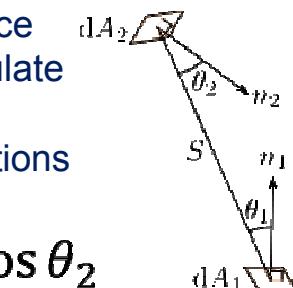
Flame shape:

- Weighted source emitters on flame centerline

Single Surface models

Flame shape:

- Assumed flame shape (e.g., cone) w/ empirically tuned radiating surface
- Geometric View Factors to calculate radiation transfer
- Empirical wind/buoyancy corrections



$$VF_{1 \rightarrow 2} = \frac{\cos \theta_1 \cos \theta_2}{\pi S^2}$$

Radiant fraction models:

- Empirical function of exit velocity

Radiant fraction models:

- Same as SPS models

Note that all models incorporate empirical flame length and atmospheric transmissivity corrections

It is convenient to define jet flame/flare radiative heat flux models into 3 categories:

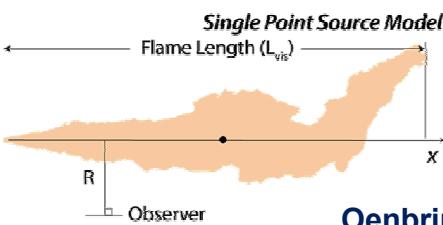
Single Point Source (SPS) models

Advantages:

- Simplicity
- Good far-field accuracy ($D > L_{vis}$)
- Large number of fuel types & flame sizes

Drawbacks:

- Poor near-field performance ($D < L_{vis}$)
- No wind/buoyancy corrections
- Neglects flame headed towards observer
- Not suitable for transient jets or “fireballs”



Oenbring & Sifferman,
API Proc., 1980

Corrections for emission angle

API Section 521, 1969

1970

1980

1990

2000

2010

Brzustowski & Sommer,
API Proc., 1973

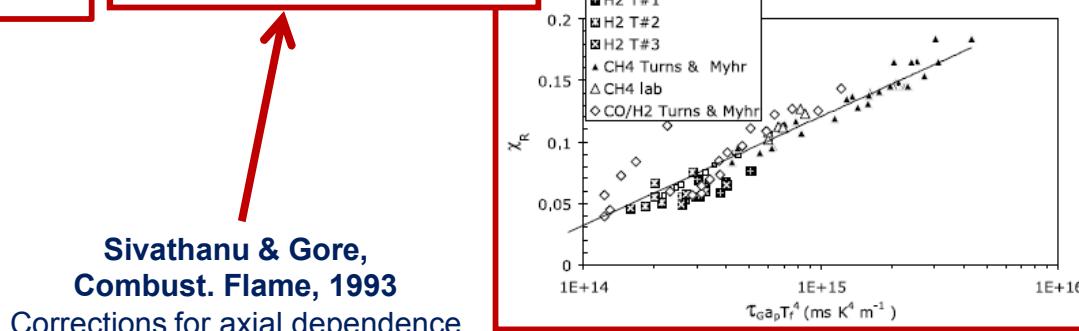
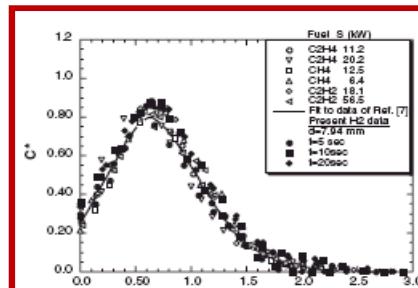
Corrections for observer angle

Turns & Myhr,
Combust. Flame, 1991

Corrections for flame residence time

Molina et al.,
Proc. Combust. Inst., 2007

Corrections for product species emissivity



$$q = \frac{\chi Q}{4\pi D^2}$$

χ : Radiant fraction

Q: Heat release

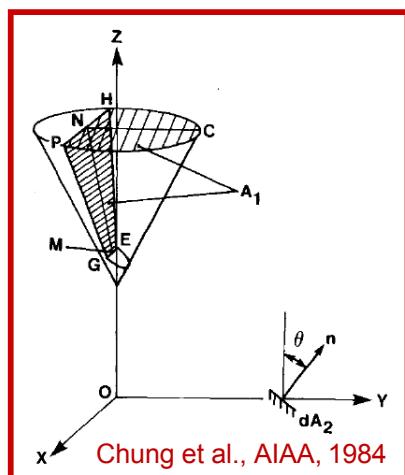
D: Distance to observer

q: Heat flux [W/m²]

It is convenient to define jet flame/flare radiative heat flux models into 3 categories:

$$E = \frac{\chi \dot{m} \Delta H}{A}$$

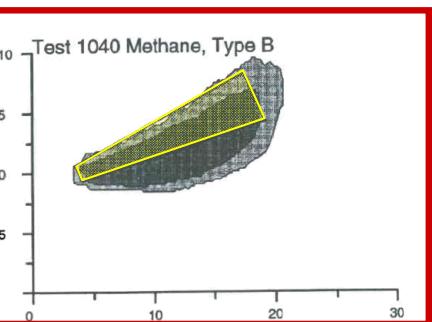
E: Emissive Power
 A: Surface Area
 ΔH : Heat of combustion
 m: mass



API Section 521, 1969

Leahy et al.,
 Alberta Environment, 1979
 Emissivity corrections
 (cone frustum)

1970



Cook et al.,
 Chem. Eng. Res. Des., 1987
 Radiant fraction correlation w/ velocity

1980

Johnson et al.,
 Process Safety Environ. Prot., 1994
 Empirical horizontal flame surface model
 w/ wind/buoyancy corrections

1990

2000

2010

Chamberlain,
 Chem. Eng. Res. Des., 1987
 Empirical vertical flame surface model
 w/ wind/buoyancy corrections

Single Surface models

Advantages:

- Good far-field accuracy & reasonable performance in near-field
- Simple to use w/ validated view factors
- Amenable to wind/buoyancy corrections

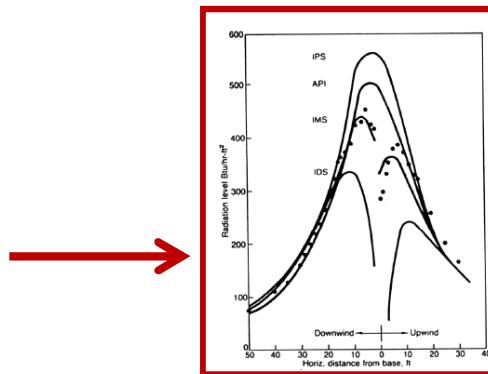
Drawbacks:

- Models depend on assumed shape (i.e., not always representative of flame envelope)
- Extensive calibrations required
- Gas type specific

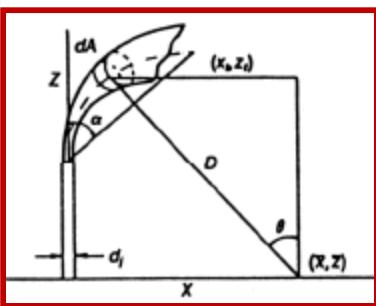
It is convenient to define jet flame/flare radiative heat flux models into 3 categories:

$$q = \int_0^L \frac{w \chi \dot{m} \Delta H}{4\pi D} \cos\beta$$

McMurray,
Hydrocarbon Processing, 1982
Integrated mixed source model
(combined surface & point sources)



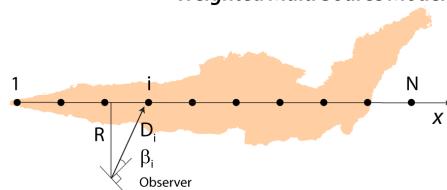
API Section 521, 1969



De-Faveri et al.,
Hydrocarbon Processing, 1985
Multi surface model w/ crosswind corrections

Multi Source Models (MSM)

Weighted Multi Source Model



Advantages:

- Good near/far-field accuracy
- Can account for flame trajectory
- Surface reflection corrections
- Can be used for transient flames
- Better flame emissivity corrections

Drawbacks:

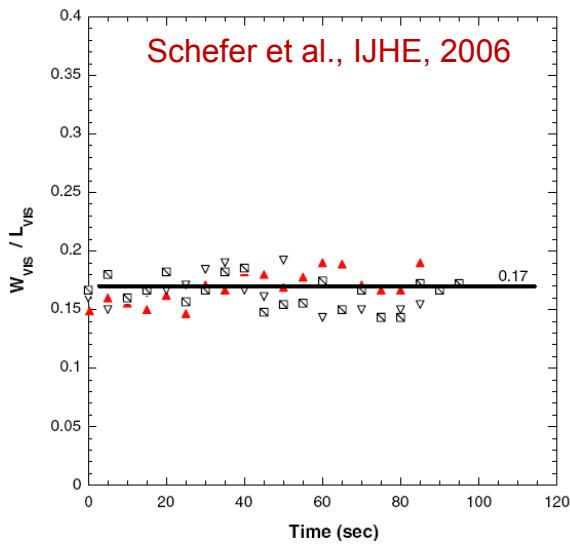
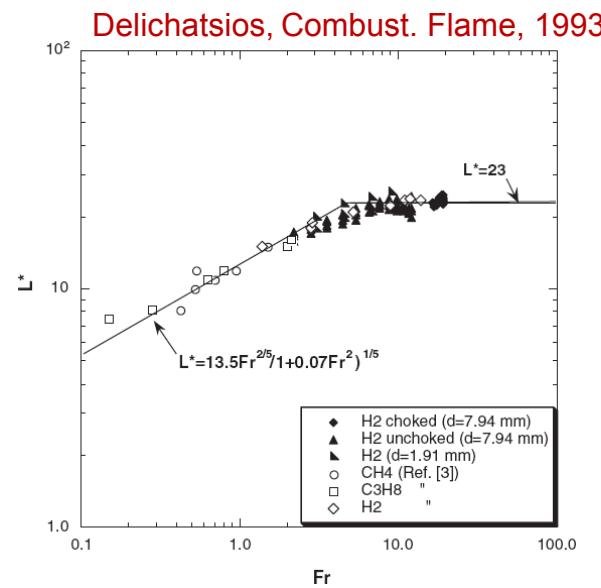
- Increased complexity

Validated empirical correlations are useful for establishing flame envelopes

$$L^* = \frac{13.5 Fr_f^{0.4}}{(1 + 0.07 Fr_f^2)^{0.2}} \quad \text{for } Fr_f < 5$$

$$L^* = 23 \quad \text{for } Fr_f \geq 5$$

where: $Fr_f = \frac{u_{eff} y_s^{1.5}}{\left(\frac{\rho_{eff}}{\rho_{amb}}\right)^{0.25} \left(\frac{T_{ad} - T_{amb}}{T_{amb}} \cdot g \cdot d_{eff}\right)^{0.5}}$



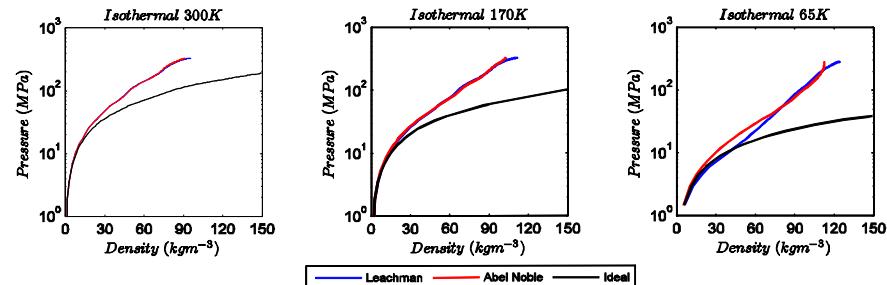
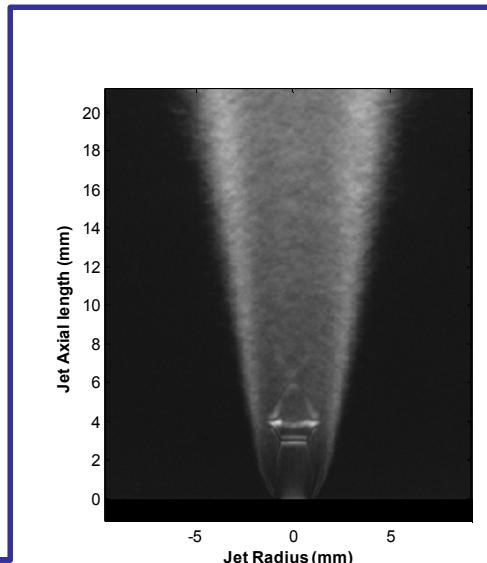
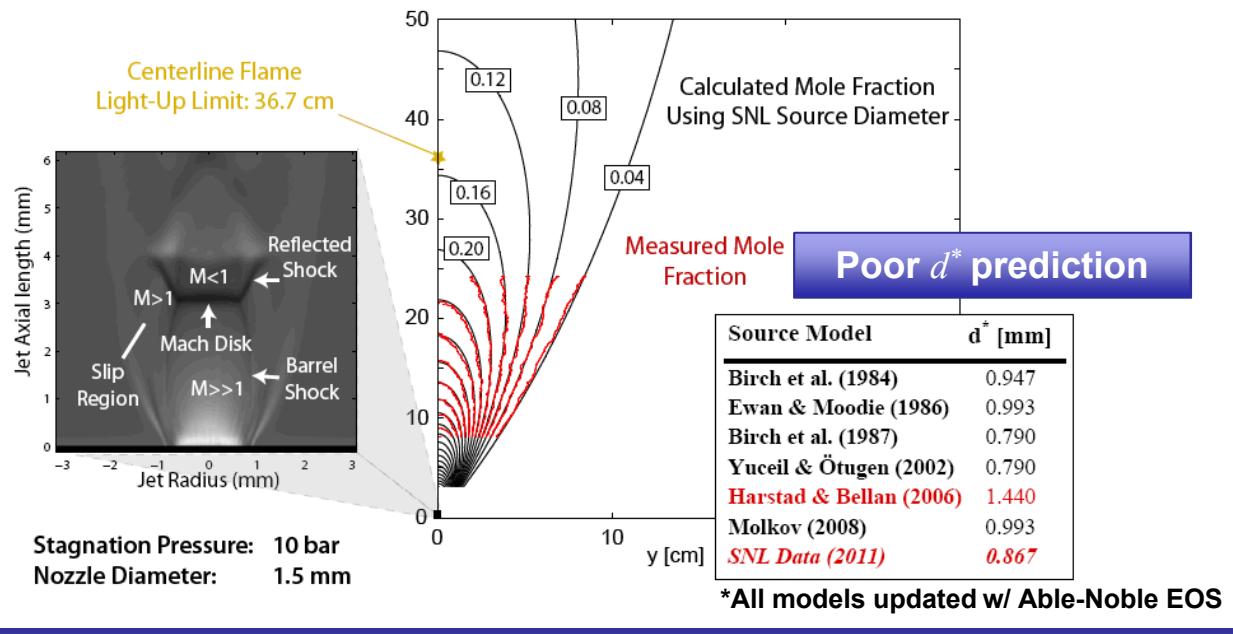
Flame width exhibits a strong dependence on length

$$L_f = \frac{L^*}{y_s} d^* \quad \& \quad W_f = 0.17 L_f$$

where: $d^* = d_{eff} \sqrt{\frac{\rho_{eff}}{\rho_{amb}}}$

Note that notional nozzle models needed to compute choked flow effective jet-exit conditions

Excellent agreement between computed & measured mole fraction statistics with measured d^*



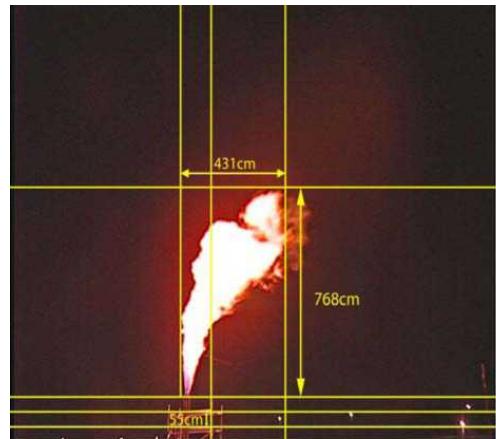
Most fluid appears to be in the slip region

Abel-Noble EOS

$$p = Z\rho RH_2T; Z = (1 - b\rho)^{-1}$$

- Works well at ambient T
- Cryogenic states poorly predicted (present in barrel shock; $T < 70$ K)

What about flame trajectory changes due to wind/buoyancy?



400 g/s release 2" pipe



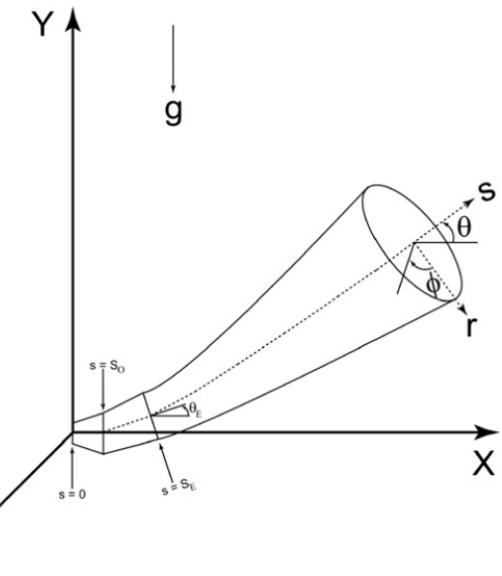
40 g/s release 2" pipe

Willoughby et al., ICHS4, 2011

1-D integral models based on jet self-similarity have been used to model Established Flow Zone



Reichardt, *VDI-Forschungsheft*, 1942



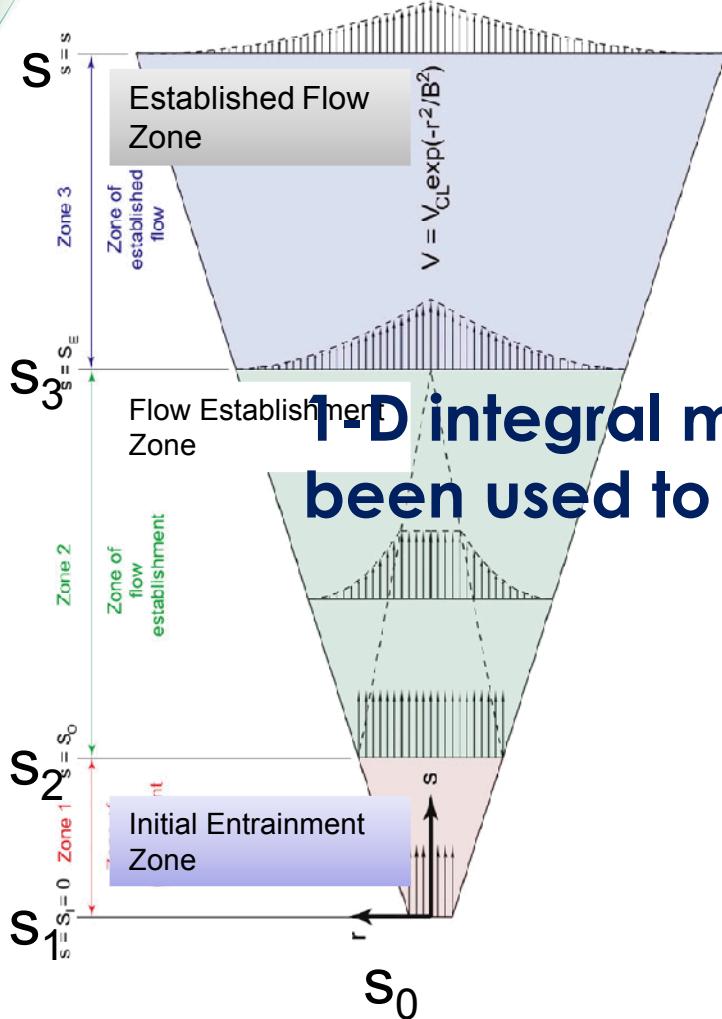
$$Mass \quad \frac{\partial}{\partial S} \int_0^{2\pi} \int_0^{\infty} \rho V r dr d\phi = \rho_{amb} E$$

$$x-Mom \quad \frac{\partial}{\partial S} \int_0^{2\pi} \int_0^{\infty} \rho V^2 \cos \theta r dr d\phi = 0$$

$$y-Mom \quad \frac{\partial}{\partial S} \int_0^{2\pi} \int_0^{\infty} \rho V^2 \sin \theta r dr d\phi = \int_0^{2\pi} \int_0^{\infty} (\rho_{amb} - \rho) g r dr d\phi$$

$$Species \quad \frac{\partial}{\partial S} \int_0^{2\pi} \int_0^{\infty} \rho V Y r dr d\phi = 0$$

$$Energy \quad \frac{\partial}{\partial S} \int_0^{2\pi} \int_0^{\infty} \rho V (h - h_{amb}) r dr d\phi = 0$$



1-D integral models based on jet self-similarity have been used to model Established Flow Zone

Velocity & Concentration profiles are Gaussian

B : Velocity jet width

λ : Concentration-to-Velocity jet width ratio

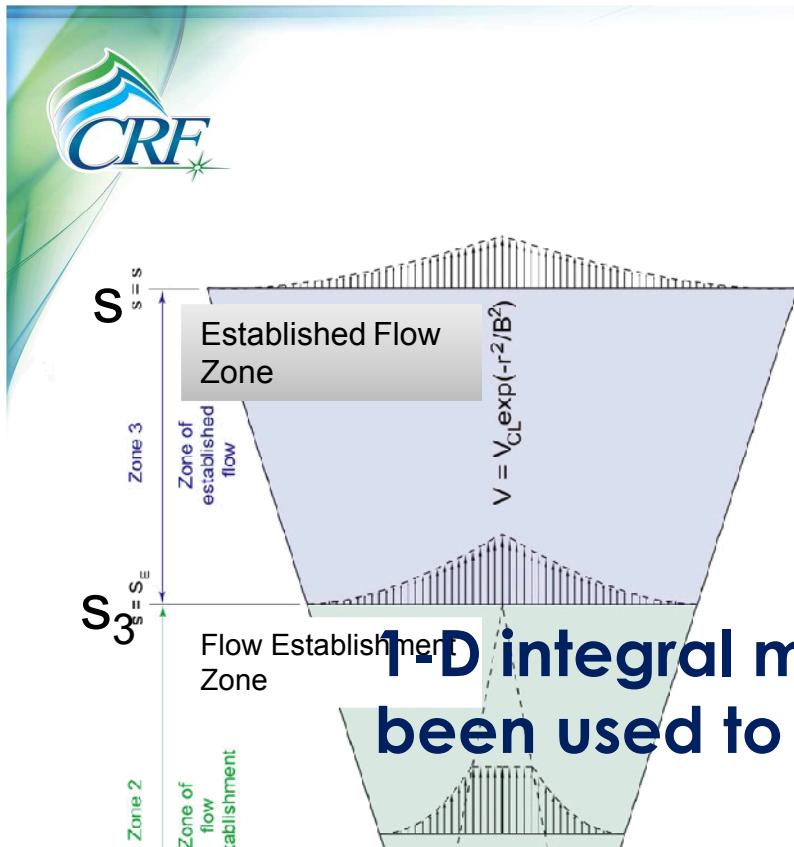
$$\frac{V}{V_{CL}} = \exp\left(-\frac{r^2}{B^2}\right)$$

$$\frac{\rho - \rho_{amb}}{\rho_{CL} - \rho_{amb}} = \exp\left(-\frac{r^2}{\lambda^2 B^2}\right)$$

$$\frac{\rho Y}{\rho_{CL} Y_{CL}} = \exp\left(-\frac{r^2}{\lambda^2 B^2}\right)$$

Unknowns

$$\text{Mass } \frac{d}{dS} \left\{ V_{CL} B^2 \left[\rho_{amb} - \frac{\lambda^2}{\lambda^2 + 1} (\rho_{amb} - \rho_{CL}) \right] \right\} = \frac{\rho_{air} E}{\pi}$$



**1-D integral models based on jet self-similarity
been used to model Established Flow Zone**





**Negligible change for side heat flux prediction
downstream predictions improved dramatically**



Summary

1. Three simplified methods exist to model jet flame radiat