

# Updated jet flame radiation modeling with buoyancy corrections

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# In 2008, Air Products commissioned radiative heat flux measurements from 2 large-scale H<sub>2</sub> jet flames.

Flame	$d_j$ [mm]	$\dot{m}$ [kg/s]	$L_f$ [m]	$p_0$ [barg]	$T_0$ [K]	RH [%]	$T_{amb}$ [K]	$p_{amb}$ [mbar]	$U_{wind}$ [m/s]	Wind dir [°]
1	20.9	1.0	17.4	59.8	308.7	94.3	280	1022	2.84	68.5
2	52.5	7.4	48.5	62.1	287.8	94.5	280	1011	0.83	34.0

Flame 1



Horizontal jet flame tests were performed by  
GL Noble Denton (then Advantica) at the  
Spadeadam test site in North Cumbria, UK

Flame 2

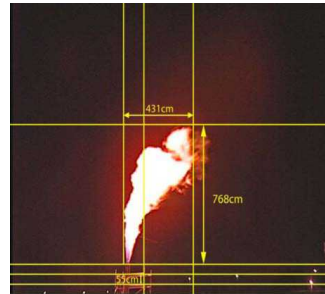


Analytic models did a poor job of predicting radiative heat fluxes from these flames... Why?

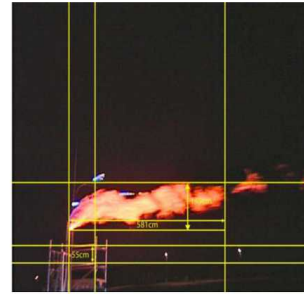
# Simplified methods exist to model radiative heat flux boundaries from jet flames & flares

All methods require models of the following parameters:

## 1) Flame envelope ►



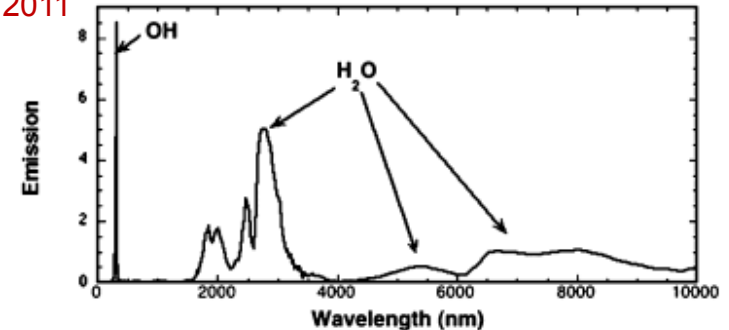
400 g/s release 2" pipe



40 g/s release 2" pipe

Willoughby et al., ICHS4, 2011

## 2) Energy fraction converted to radiation ►



Schefer et al., IJHE, 2009

## ◀ 3) Radiant energy transferred to observer

Models are often interdependent and only applicable for the given method

# It is convenient to define jet flame/flare radiative heat flux models into 3 categories:

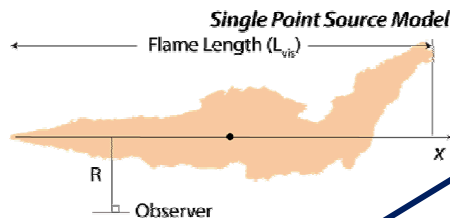
## Single Point Source (SPS) models

### Flame shape:

- Non-dimensional radiant power to estimate radiant load distribution

### Radiant fraction models:

- Empirical function: **temperature, composition, release rate, soot, residence time, heat release**



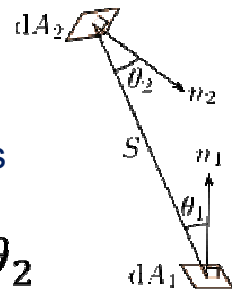
### Flame shape:

- Weighted source emitters on flame centerline

## Single Surface models

### Flame shape:

- Assumed flame shape (e.g., cone) w/ empirically tuned radiating surface
- Geometric View Factors to calculate radiation transfer
- Empirical wind/buoyancy corrections



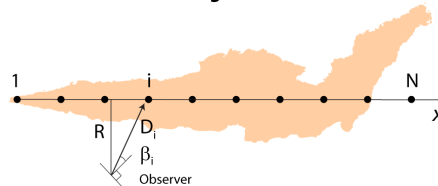
$$VF_{1 \rightarrow 2} = \frac{\cos \theta_1 \cos \theta_2}{\pi S^2}$$

### Radiant fraction models:

- Empirical function of exit velocity

## Multi Source Models (MSM)

### Weighted Multi Source Model



### Radiant fraction models:

- Same as SPS models

**Note that all models incorporate empirical flame length and atmospheric transmissivity corrections**

# It is convenient to define jet flame/flare radiative heat flux models into 3 categories:

## Single Point Source (SPS) models

### Advantages:

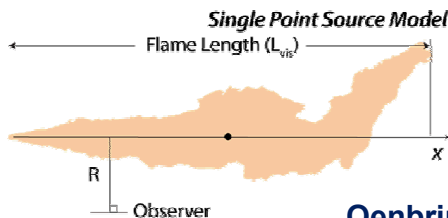
- Simplicity
- Good far-field accuracy ( $D > L_{vis}$ )
- Large number of fuel types & flame sizes

### Drawbacks:

- Poor near-field performance ( $D < L_{vis}$ )
- No wind/buoyancy corrections
- Neglects flame headed towards observer
- Not suitable for transient jets or "fireballs"

$$q = \frac{\chi Q}{4\pi D^2}$$

$\chi$ : Radiant fraction  
 $Q$ : Heat release  
 $D$ : Distance to observer  
 $q$ : Heat flux [ $W/m^2$ ]



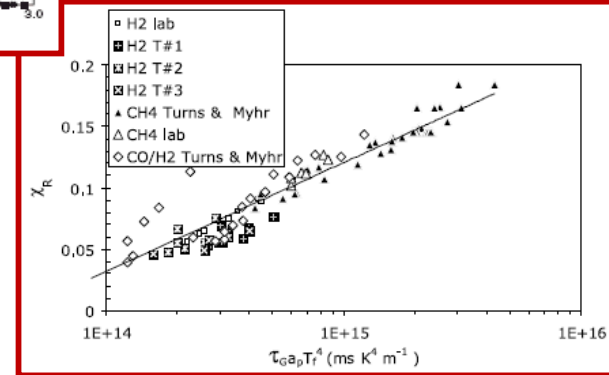
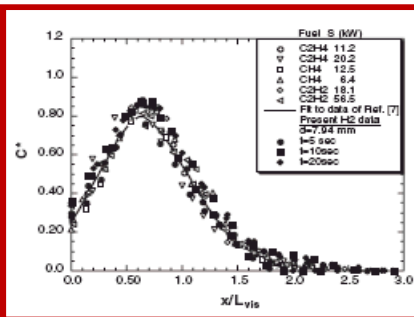
Oenbring & Sifferman,  
 API Proc., 1980

API Section 521, 1969

Corrections for emission angle

Sivathanu & Gore,  
 Combust. Flame, 1993

Corrections for axial dependence



# It is convenient to define jet flame/flare radiative heat flux models into 3 categories:

$$E = \frac{\chi \dot{m} \Delta H}{A}$$

E: Emissive Power  
A: Surface Area  
 $\Delta H$ : Heat of combustion  
m: mass

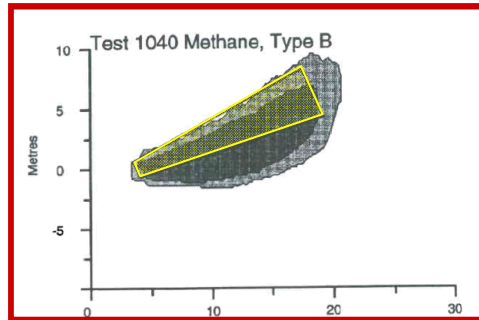
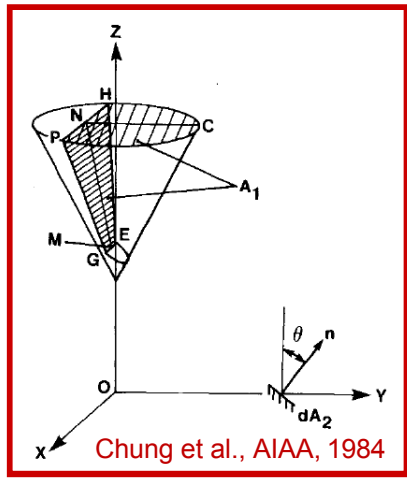
## Single Surface models

### Advantages:

- Good far-field accuracy & reasonable performance in near-field
- Simple to use w/ validated view factors
- Amenable to wind/buoyancy corrections

### Drawbacks:

- Models depend on assumed shape (i.e., not always representative of flame envelope)
- Extensive calibrations required
- Gas type specific



Cook et al.,  
Chem. Eng. Res. Des., 1987  
Radiant fraction correlation w/ velocity

Leahey et al.,  
Alberta Environment, 1979  
Emissivity corrections  
(cone frustum)

Johnson et al.,  
Process Safety Environ. Prot., 1994  
Empirical horizontal flame surface model  
w/ wind/buoyancy corrections

Chamberlain,  
Chem. Eng. Res. Des., 1987  
Empirical vertical flame surface model  
w/ wind/buoyancy corrections

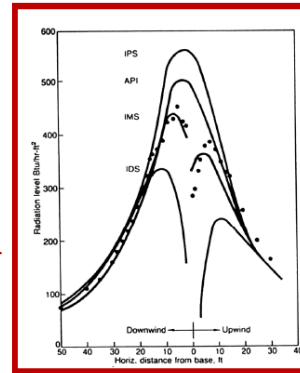
API Section 521, 1969



# It is convenient to define jet flame/flare radiative heat flux models into 3 categories:

$$q = \int_0^L \frac{w\chi\dot{m}\Delta H}{4\pi D} \cos\beta$$

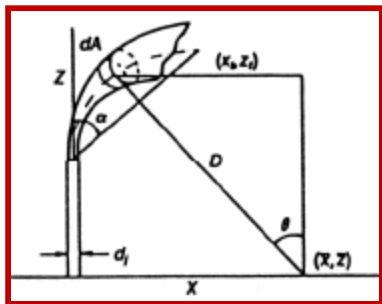
**McMurray,**  
**Hydrocarbon Processing, 1982**  
Integrated mixed source model  
(combined surface & point sources)



**Hankinson & Lowesmith**  
**Combust. Flame, 2012**  
Weighted multi-source

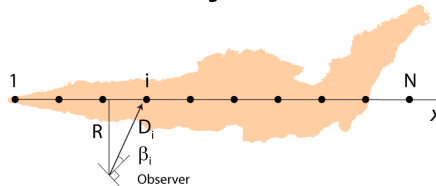
**De-Faveri et al.,**  
**Hydrocarbon Processing, 1985**  
Multi surface model w/ crosswind corrections

**Ekoto et al.,**  
**Proc. IPC, 2012**  
Ground reflection correction



## Multi Source Models (MSM)

*Weighted Multi Source Model*



### Advantages:

- Good near/far-field accuracy
- **Can account for flame trajectory**
- Surface reflection corrections
- Can be used for transient flames
- Better flame emissivity corrections

### Drawbacks:

- Increased complexity

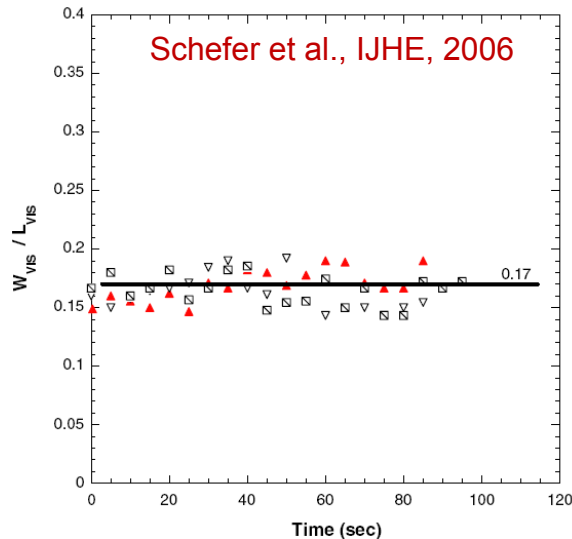
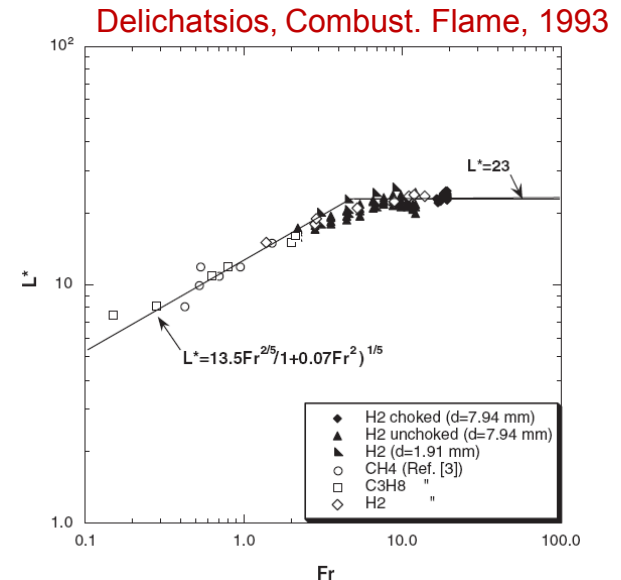
# Validated empirical correlations are useful for establishing flame envelopes

$$L^* = \frac{13.5 Fr_f^{0.4}}{(1 + 0.07 Fr_f^2)^{0.2}} \quad \text{for } Fr_f < 5$$

$$L^* = 23 \quad \text{for } Fr_f \geq 5$$

where:

$$Fr_f = \frac{u_{eff} y_s^{1.5}}{\left(\frac{\rho_{eff}}{\rho_{amb}}\right)^{0.25} \left(\frac{T_{ad} - T_{amb}}{T_{amb}} \cdot g \cdot d_{eff}\right)^{0.5}}$$



Flame width exhibits a strong dependence on length

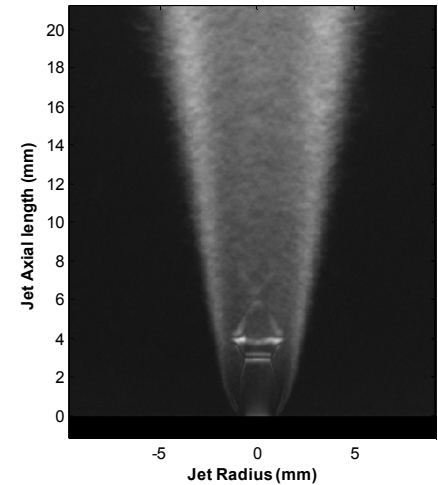
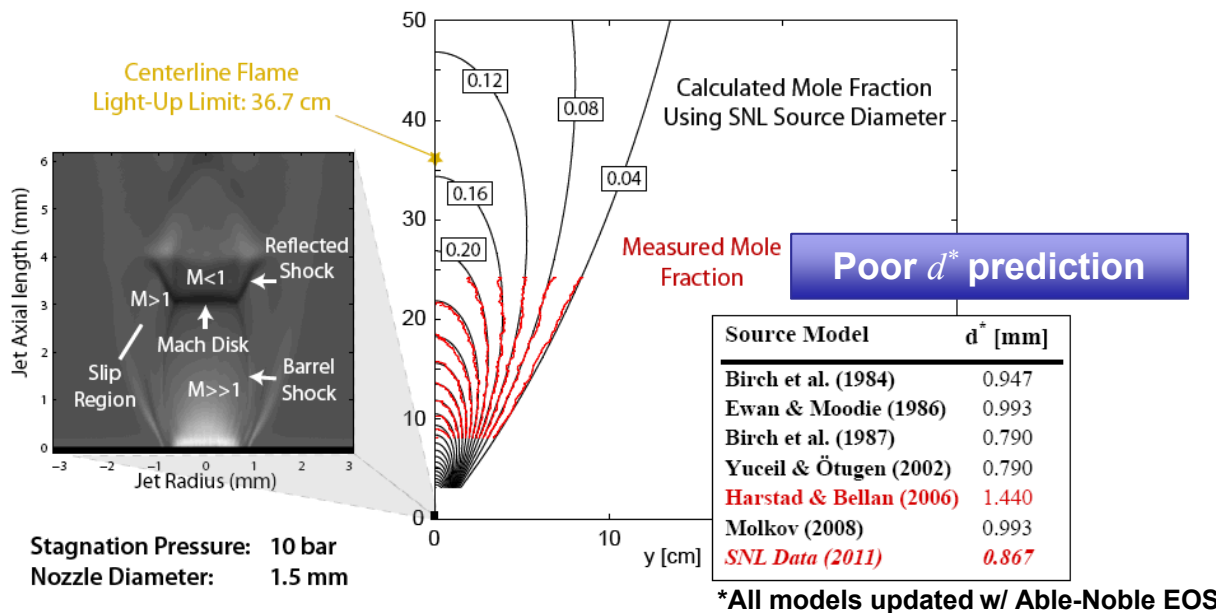
$$L_f = \frac{L^*}{y_s} d^* \quad \& \quad W_f = 0.17 L_f$$

where:

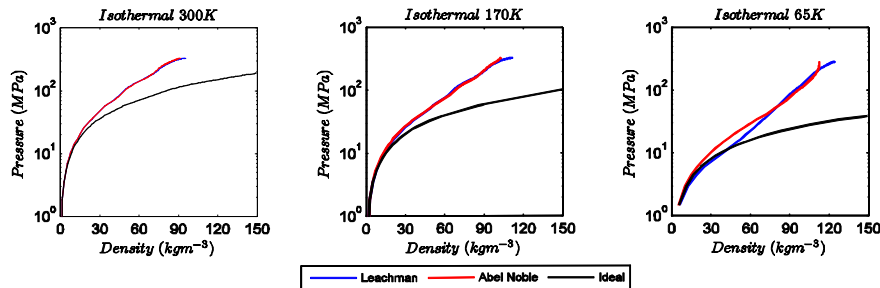
$$d^* = d_{eff} \sqrt{\frac{\rho_{eff}}{\rho_{amb}}}$$

**Note that notional nozzle models needed to compute choked flow effective jet-exit conditions**

# Excellent agreement between computed & measured mole fraction statistics with measured $d^*$



Most fluid appears to be in the slip region

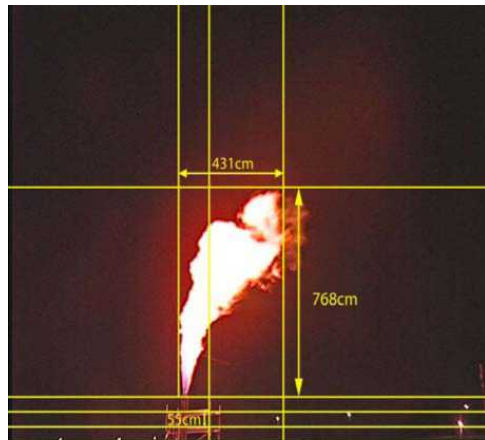


## Abel-Noble EOS

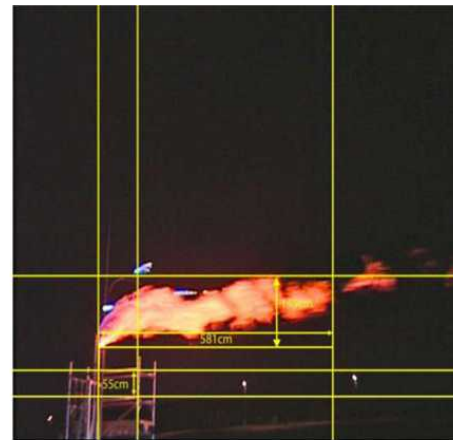
$$p = Z\rho R H_2 T; Z = (1 - b\rho)^{-1}$$

- Works well at ambient  $T$
- Cryogenic states poorly predicted (present in barrel shock;  $T < 70 \text{ K}$ )

# What about flame trajectory changes due to wind/buoyancy?



400 g/s release 2" pipe



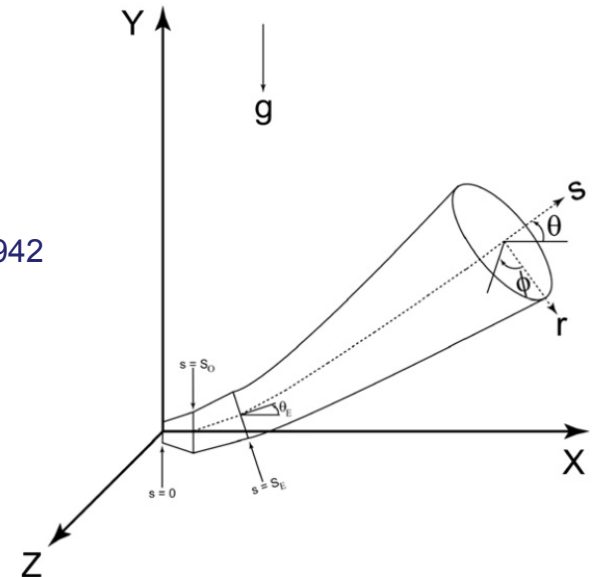
40 g/s release 2" pipe

Willoughby et al., ICHS4, 2011



# 1-D integral models based on jet self-similarity have been used to model Established Flow Zone

Reichardt, VDI-Forschungsheft, 1942



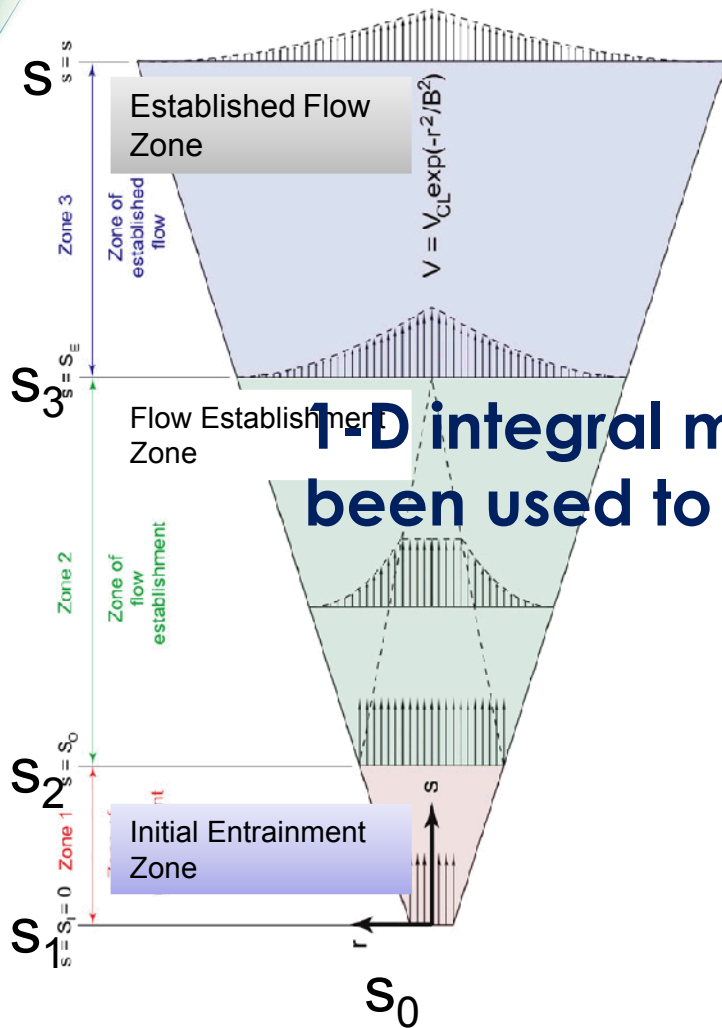
$$\text{Mass} \quad \frac{\partial}{\partial S} \int_0^{2\pi} \int_0^{\infty} \rho V r dr d\phi = \rho_{amb} E$$

$$x\text{-Mom} \quad \frac{\partial}{\partial S} \int_0^{2\pi} \int_0^{\infty} \rho V^2 \cos \theta r dr d\phi = 0$$

$$y\text{-Mom} \quad \frac{\partial}{\partial S} \int_0^{2\pi} \int_0^{\infty} \rho V^2 \sin \theta r dr d\phi = \int_0^{2\pi} \int_0^{\infty} (\rho_{amb} - \rho) g r dr d\phi$$

$$\text{Species} \quad \frac{\partial}{\partial S} \int_0^{2\pi} \int_0^{\infty} \rho V Y r dr d\phi = 0$$

$$\text{Energy} \quad \frac{\partial}{\partial S} \int_0^{2\pi} \int_0^{\infty} \rho V (h - h_{amb}) r dr d\phi = 0$$



**1-D integral models based on jet self-similarity have been used to model Established Flow Zone**

**Velocity & Concentration profiles are Gaussian**

$B$ : Velocity jet width  
 $\lambda$ : Concentration-to-Velocity jet width ratio

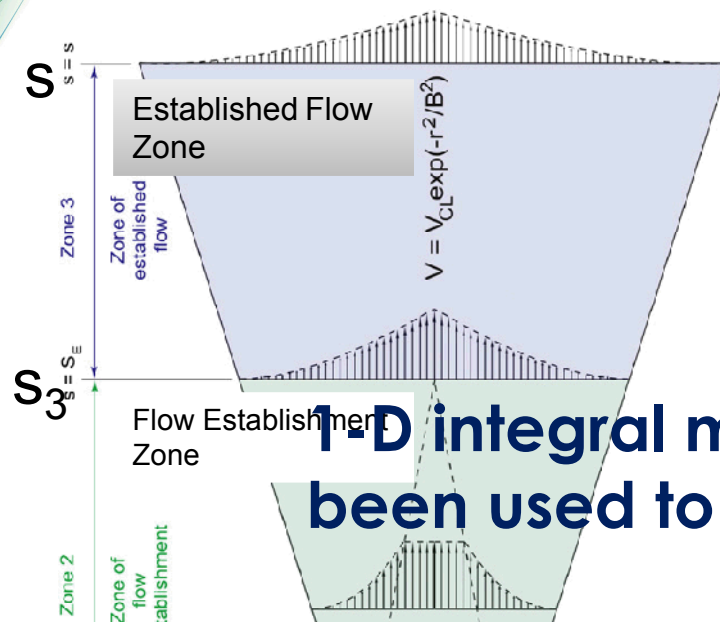
$$\frac{V}{V_{CL}} = \exp\left(-\frac{r^2}{B^2}\right)$$

$$\frac{\rho - \rho_{amb}}{\rho_{CL} - \rho_{amb}} = \exp\left(-\frac{r^2}{\lambda^2 B^2}\right)$$

$$\frac{\rho Y}{\rho_{CL} Y_{CL}} = \exp\left(-\frac{r^2}{\lambda^2 B^2}\right)$$

**Unknowns**

$$\text{Mass} \frac{d}{ds} \left\{ V_{CL} B^2 \left[ \rho_{amb} - \frac{\lambda^2}{\lambda^2 + 1} (\rho_{amb} - \rho_{CL}) \right] \right\} = \frac{\rho_{air} E}{\pi}$$



**1-D integral models based on jet self-similarity  
been used to model Established Flow Zone**



**Integral flame model w/ buoyancy corrections  
used to adjust source emitter placement.**

↓ g



**Negligible change for side heat flux prediction  
downstream predictions improved dramatically**



## Summary

1. Three simplified methods exist to model jet flame radiat