

Supercritical CO₂ Direct Cycle Gas Fast Reactor (SC-GFR) Concept

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Outline

- Goals
- Advantages and Disadvantages
- Fast Gas, CO₂, and S-CO₂ Reactor Concepts
- Super Critical Cycle
- Reference Core and Plant Layout
- Heat Transfer and Thermal Hydraulics
- Keff, Burnup, and Void coefficient
- Natural Circulation Flow and Decay Heat Removal
- Economics



Goals Advantages and Disadvantages



Goal of CO₂ Reactor Design Study

Goal – Determine if a direct cycle, supercritical CO₂ cooled, fast reactor could be designed to be cost effective, maintain natural circulation decay heat removal, and last 20 years at 200 MWth (100 MWe)

- **Direct Cycle**

No primary heat exchanger. CO₂ coolant in the reactor is the same as in the power conversion system.

- **Cost Effective**

plant + power conversion system + pressure vessel + fuel < \$5000/kWe

\$500M at 100MWe

\$1,000M at 200MWe

- **Natural Circulation Decay Heat Removal**

Remove 1% of the steady-state operating power level through the power conversion system or auxiliary system with an acceptable ΔT through the reactor with no mechanical pump operating.

- **20 Years at 200 MWth**

Burnup in fuel/clad limited to an acceptable level (72,000 MWD/MT ?).

Reactivity change over core lifetime minimized.




Advantages and Disadvantages

Major Advantages -

- Natural circulation flow can allow for decay heat removal for loss of flow condition.
- Fast spectrum allows for effective breeding (conversion) and with the right geometry, a small reactivity swing over the core lifetime.
- Small void coefficient of reactivity ($< \$1.00$).
- Proven coolant (CO_2), fuel (oxide), and cladding (Cr-Ni-Fe-Nb) steels.
- Can use simple fuel rod design and core design.
- Coolant is inexpensive, relatively chemically inert, and is not flammable.
- Long blow down times for postulated leaks and large breaks.
- Pressure vessel can be made small ($\sim 2 - 2.5$ m diameter) to allow for replacement of core and PV as a single unit, if desired.
- Minimal infrastructure development.
- Supercritical cycle allows for high efficiency at 650°C core outlet temperature.
- Lower balance of plant costs due to direct cycle and small size of balance of plant.
- Brayton cycle allows for high-efficiency load following.
- High heat rejection temperature allows for efficient use of cooling water.

Major Disadvantages -

- High pressure required, ~ 20 MPa (3000 psi) – (could potentially be lowered)
- Engineered safety feature required for decay heat removal for loss of coolant accident due to large or small pipe break.
- Fission product isolation and buildup on cold components.
- Stainless-steel components required for corrosion minimization for CO_2 at high temperature.



Fast Gas, CO₂ and S-CO₂ Reactor Concepts



Commercial CO₂ Reactors

CO₂ Cooled Reactors (not supercritical, not direct cycle, thermal)

52 operated – 41 UK, 8 France, 1 Italy, 1 Japan, 1 Spain

14 AGRs, 4 Magnox still in operation

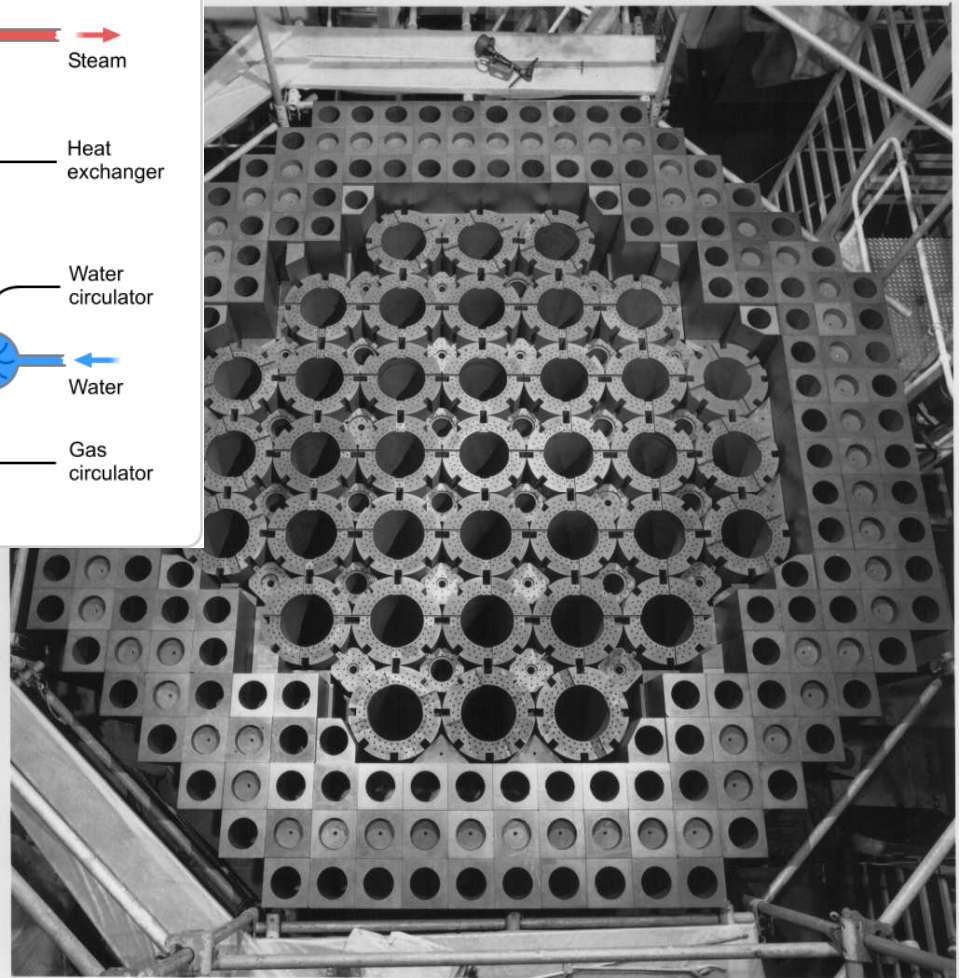
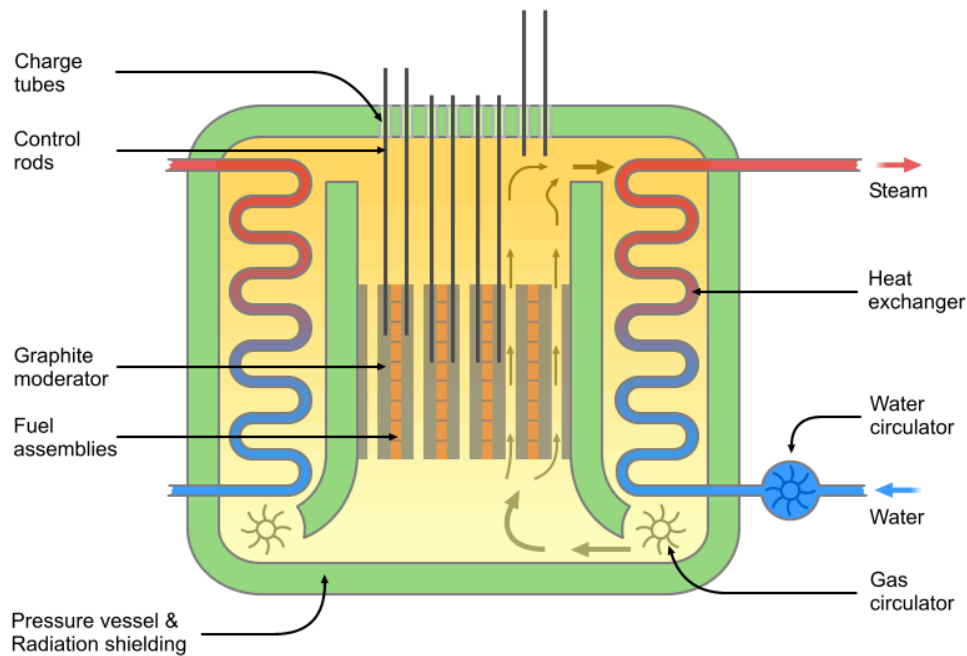
Magnox – UK and France (UNGG-independent and parallel), 1956

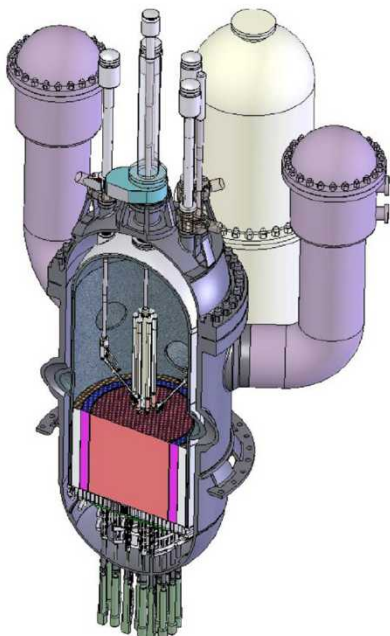
- Graphite moderated, U metal natural enriched
- Clad pin bundles in graphite matrix – online refueling
- Magnox from magnesium alloy cladding
- Secondary steam Rankine cycle
- Tout = 414°C, 1 W/cc, 5,500 MWD/MT, 200-500 MWe, 30% eff
- Pre-stressed concrete pressure Vessel with steel liner
- Pressure = 0.59 MPa (100 psia)

AGR – UK 1963

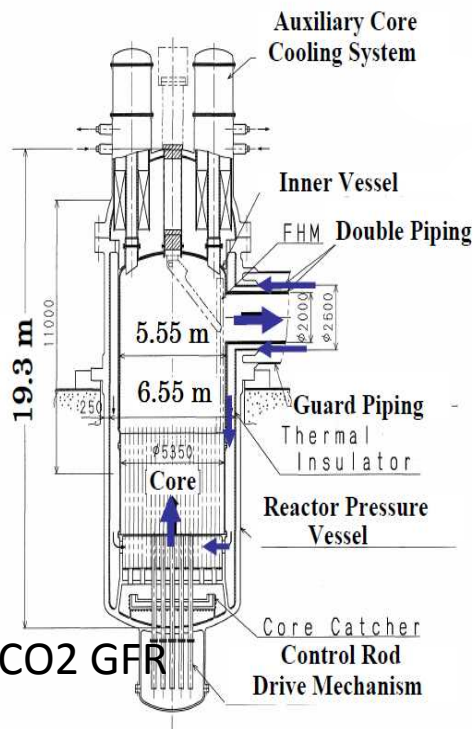
- Graphite moderated, UO₂ slightly enriched
- Clad pin bundles in graphite matrix – online refueling
- Stainless-steel cladding
- Secondary steam Rankine cycle
- Tout = 650°C, 2 W/cc, 24,000 MWD/MT, 555-625 MWe, 40% eff
- Pre-stressed concrete pressure Vessel with steel liner
- Pressure = 4.33 MPa (640 psia)

AGR Design



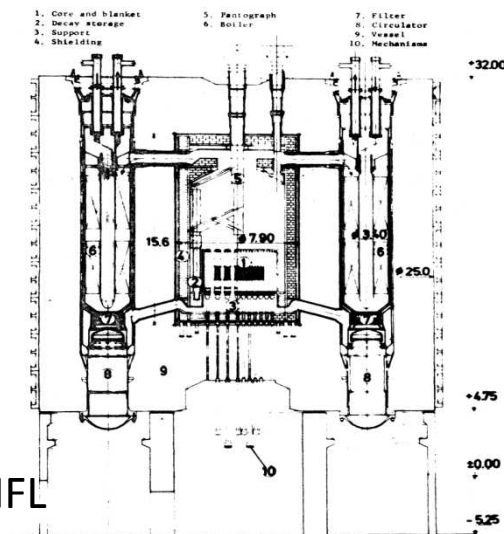


CEA



Japan CO2 GFR

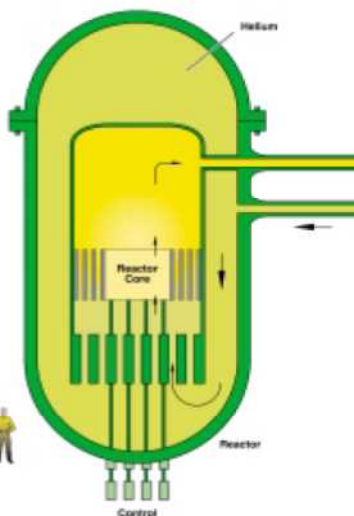
CO2/He GFR Pre-stressed Concrete PV



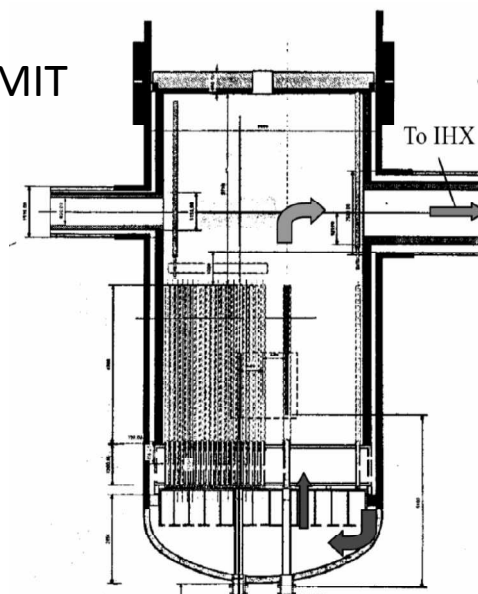
BNFL

GFR
Gas-Cooled Fast Reactor

INL



MIT



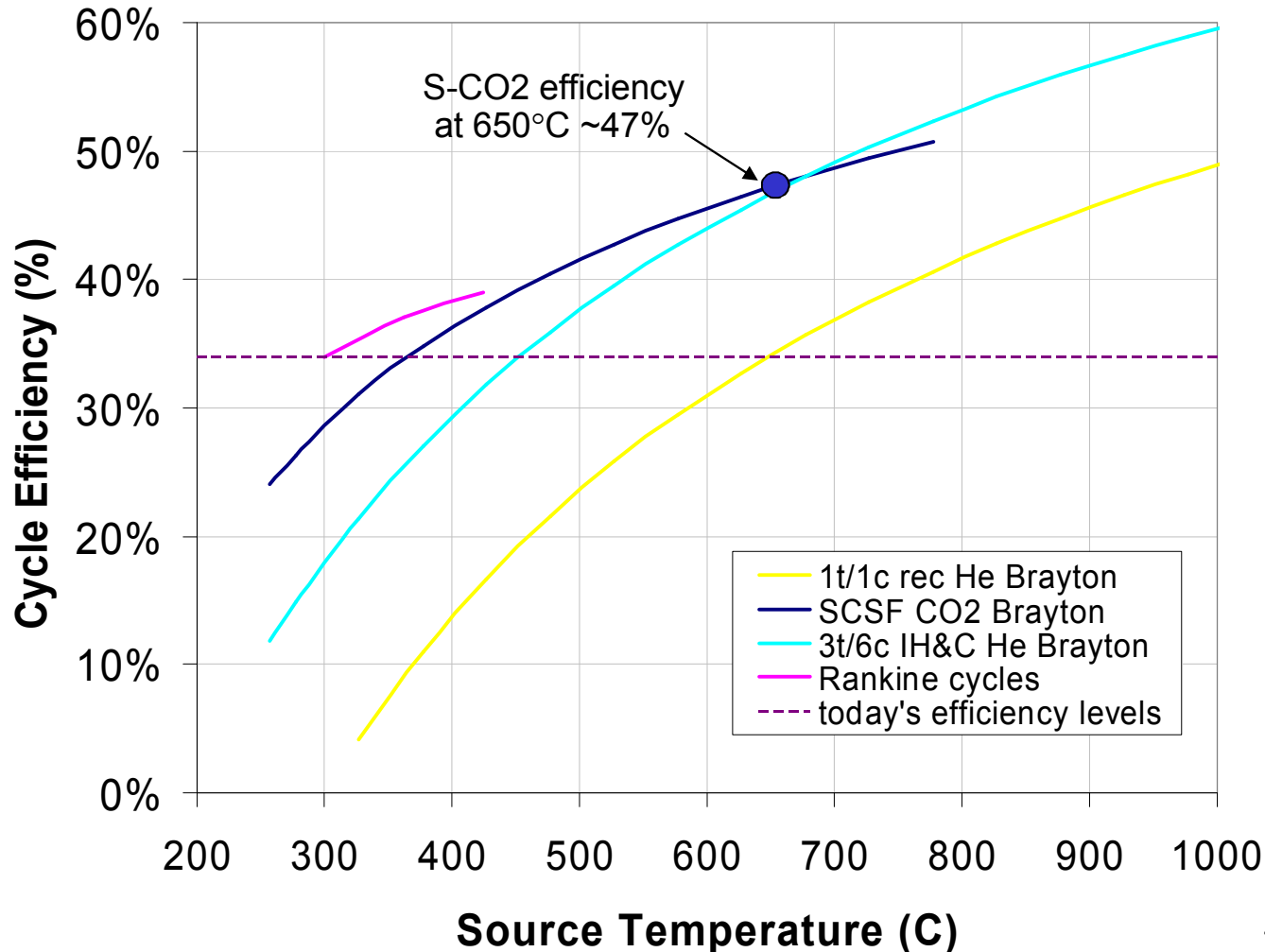


Super Critical Cycle

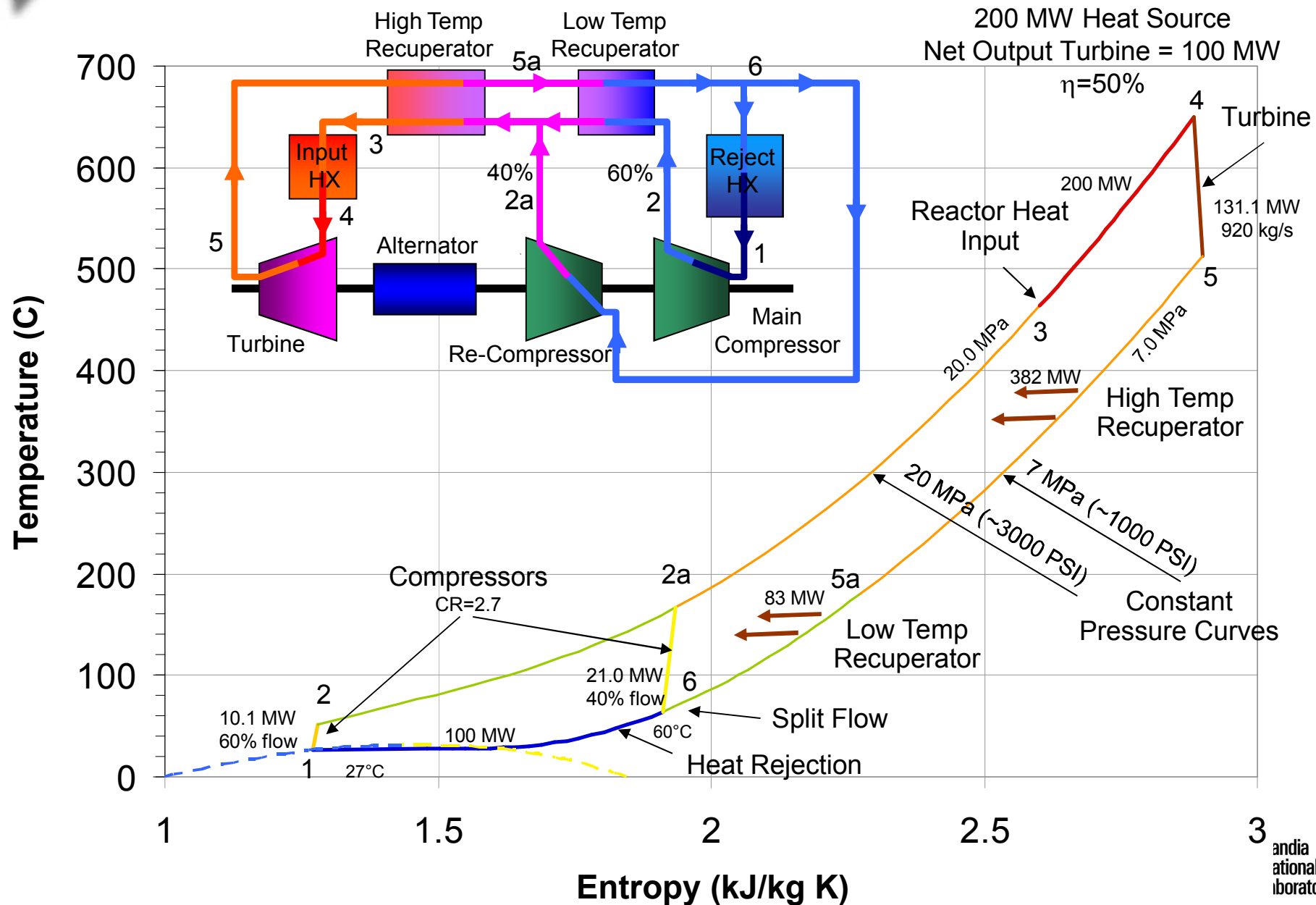
Cycle Efficiencies


Today's technology provides significant potential for improvement in cycle efficiency

Cycle Efficiencies vs Source Temperature
for fixed component efficiency



S-CO₂ Brayton Cycle With Split Flow





Reference Core and Conceptual Plant Layout



Baseline Reactor Concept

Baseline reactor and assumptions

200 MWth and 400 MWth with 20 year core lifetime.

0.75 cm OD fuel pin, $cf = 0.2$ (PWR ~ 1 cm OD, $cf = 0.5$)
and

1.20 cm OD fuel pin, $cf = 0.3$

UO₂ fuel, clad thickness = 0.0056 cm SS, gap = 0.008 cm
Initial fuel loading is 12% U-235

Reactor inlet temperature = 450°C

Reactor outlet temperature = 650°C

Reactor pressure (CO₂) = 20 MPa = 3000 psi

Core 1.7 m Dia. x 1.6 m H with 15 cm Ni reflector

Power density = 55 W/cc core at 200 MW

Desired Objectives

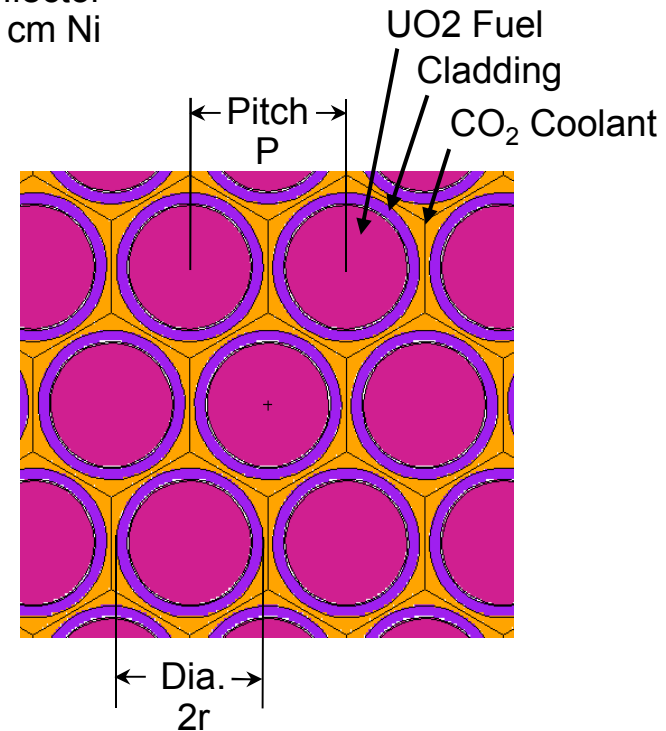
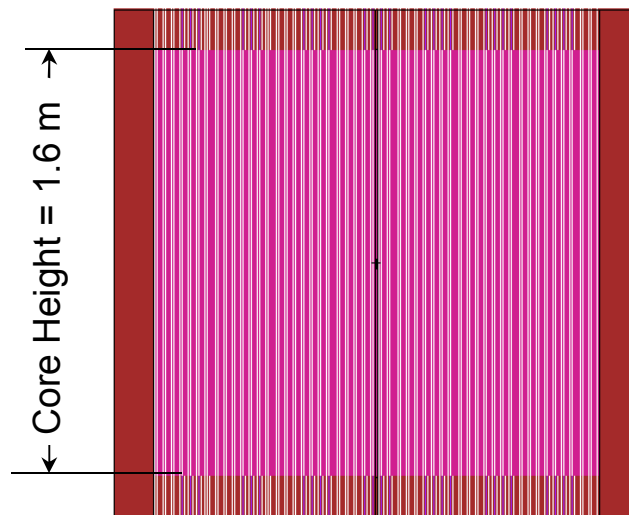
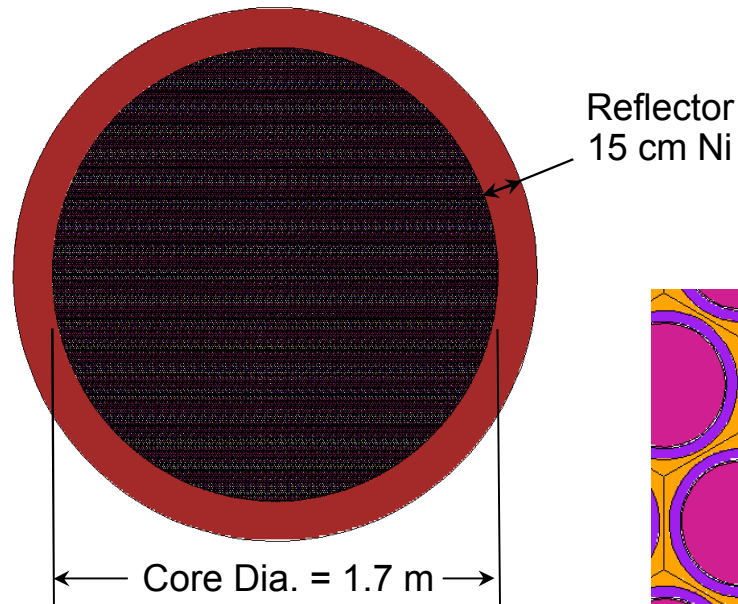
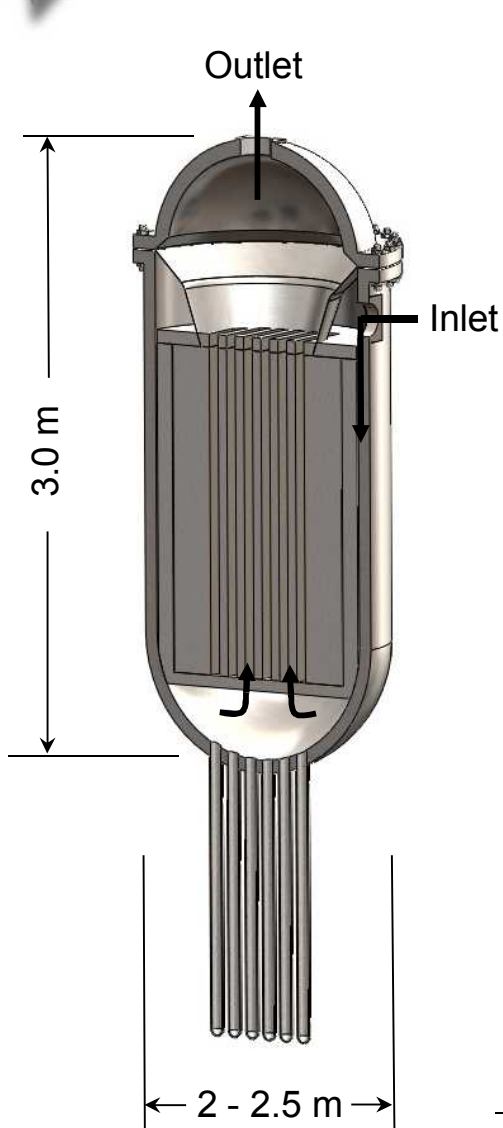
Minimal reactivity swing over core lifetime

Core pressure drop less than 1% total power

Small reactivity void coefficient

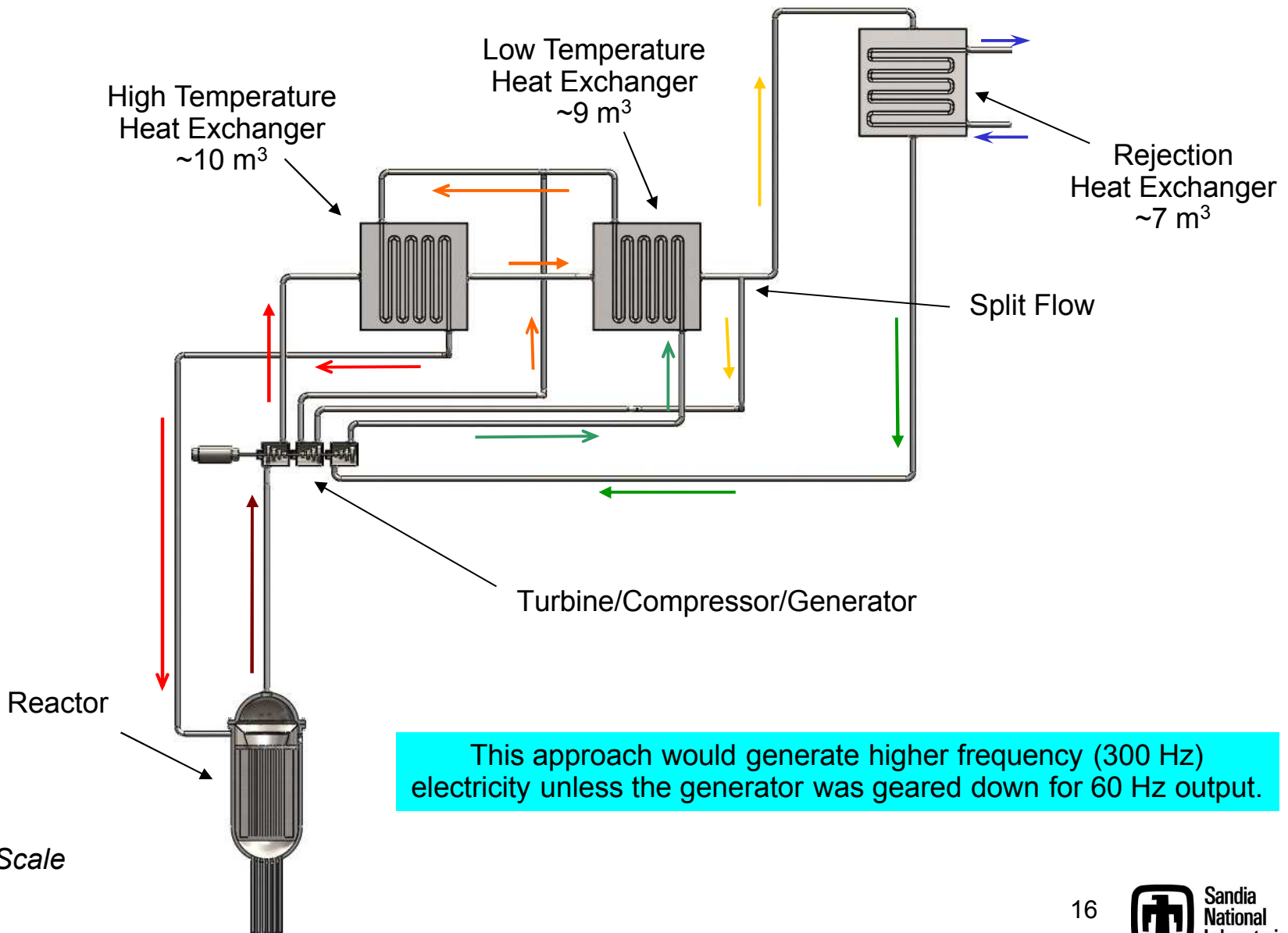
Acceptable clad and fuel peak temperature

MCNP Model of Core




$$\text{coolant fraction} = 1 - \frac{2\pi r^2}{\sqrt{3} P^2}$$

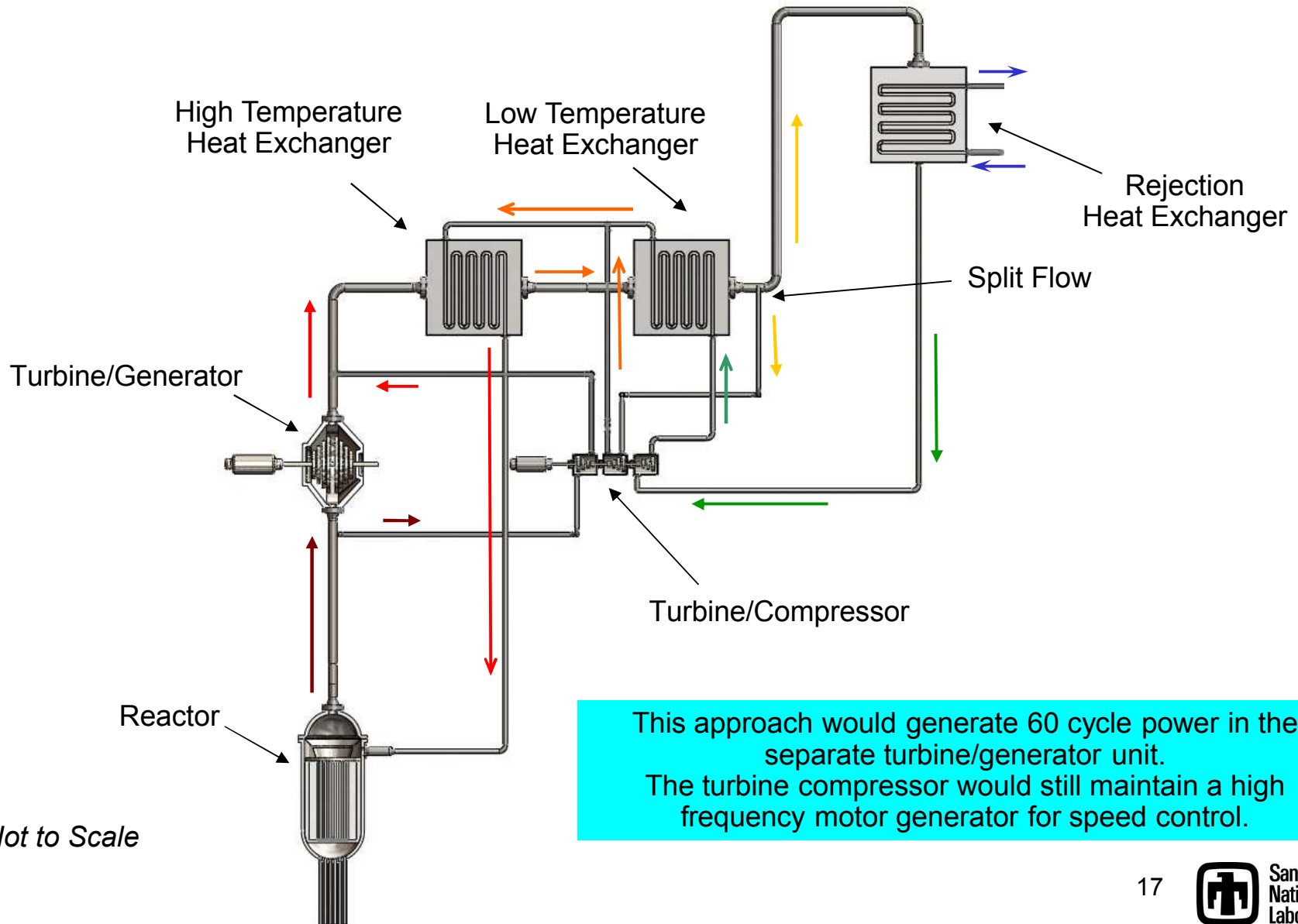
Split Flow With Combined Turbine/Generator/Compressor



Not to Scale

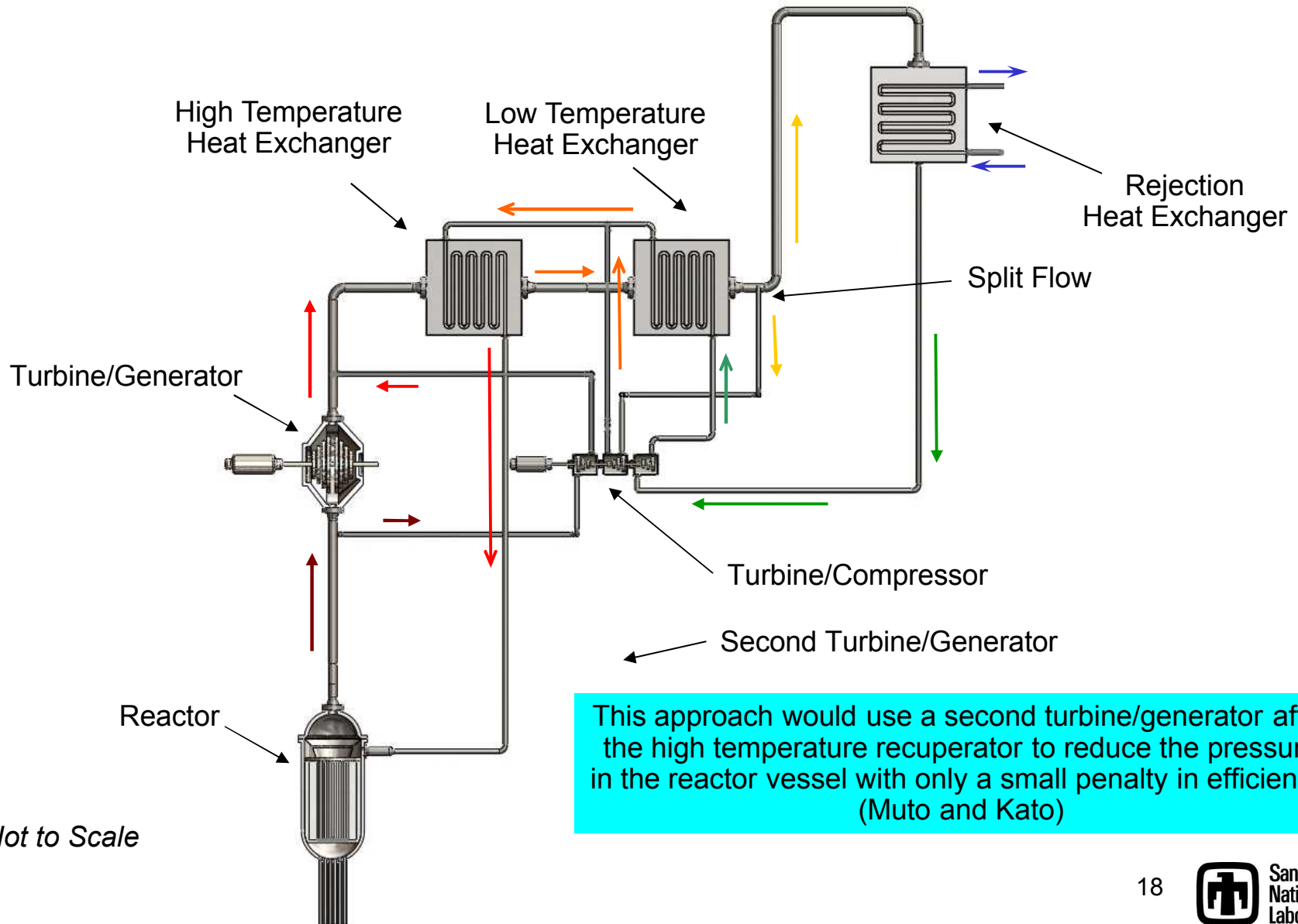


Split Flow With Separate Turbine/Generator and Turbine/Compressor

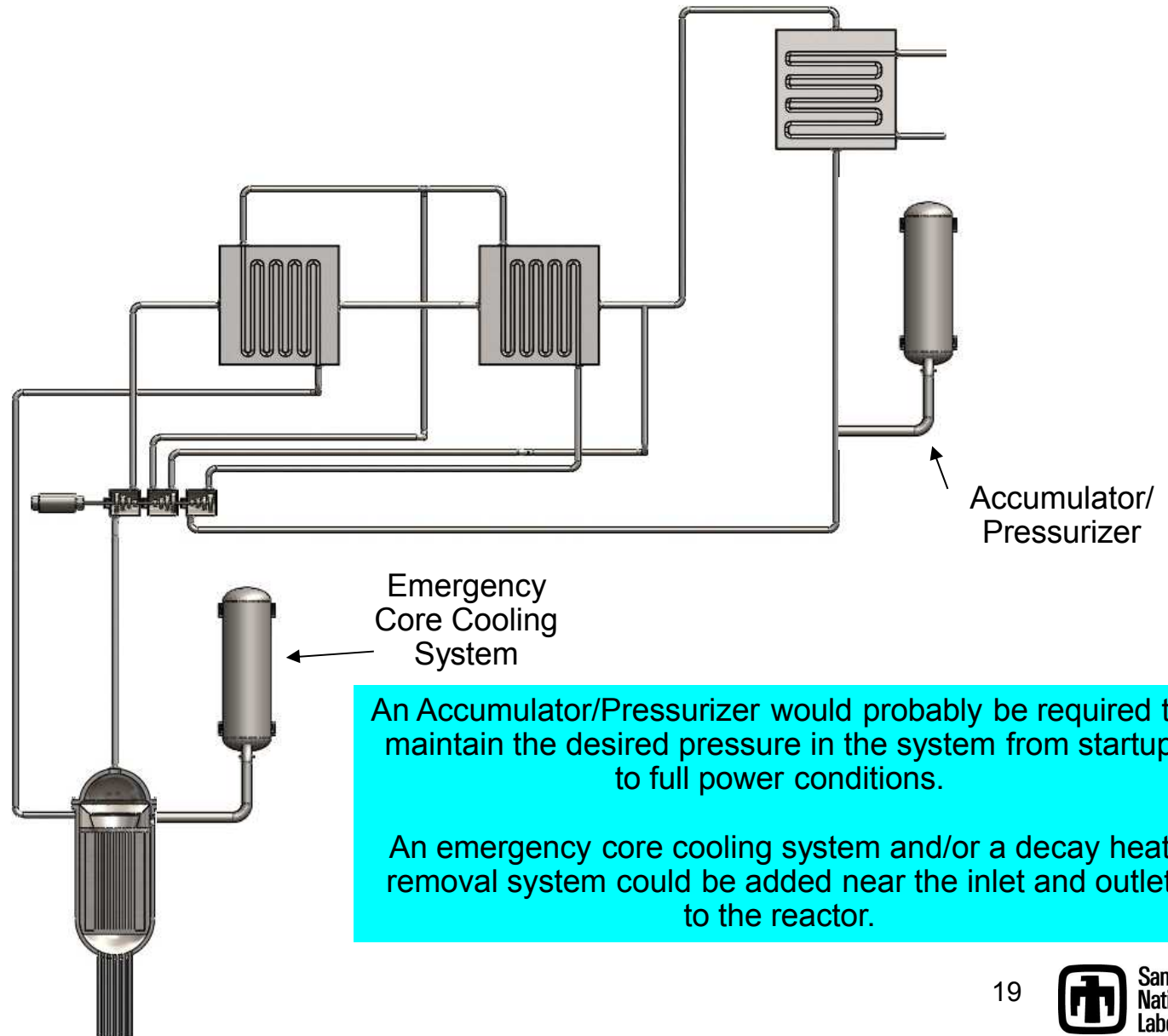


This approach would generate 60 cycle power in the separate turbine/generator unit.
The turbine compressor would still maintain a high frequency motor generator for speed control.

Split Flow With Two Turbine/Generators and Turbine/Compressor



Layout Showing Possible Locations for Pressurizer/Accumulator



An Accumulator/Pressurizer would probably be required to maintain the desired pressure in the system from startup to full power conditions.

An emergency core cooling system and/or a decay heat removal system could be added near the inlet and outlet to the reactor.



Heat Transfer and Thermal Hydraulics

Thermal Hydraulics Parametric Analysis

Parametric Analysis Assumptions

200 MW and 400 MW

Reactor inlet temperature = 450°C

Reactor outlet temperature = 650°C

Reactor average coolant temperature = 550°C

Reactor pressure = 20 MPa = 3000 psi

clad thickness = 0.0056 cm HT9, gap = 0.008 cm He

Core 1.7 m Dia. x 1.6 m H – additional height for plenum

MATHCAD SS-T-P Results

Parametric analysis for maximum fuel temperature and pressure drop performed as a function of coolant fraction and pin diameter.

0.75 cm dia 0.2 cf and 1.2 cm dia 0.3 cf

Both have about same fuel/core ratio of 0.55

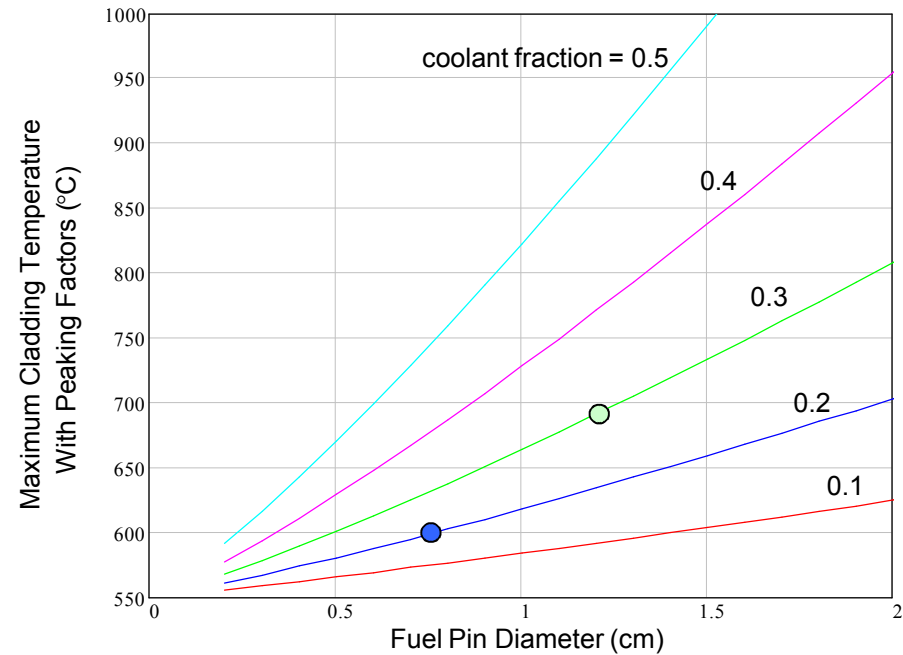
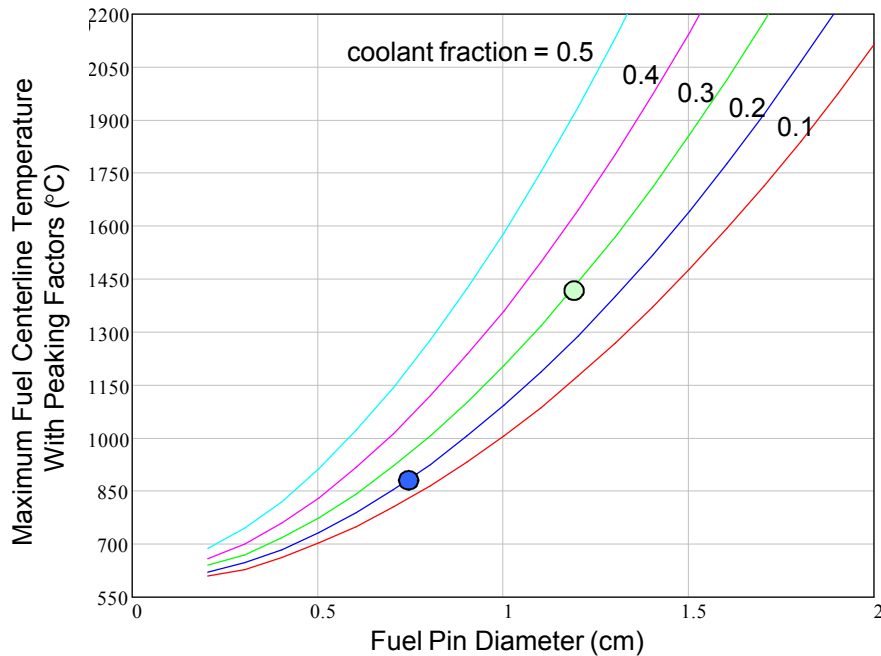
At 200 MW both work

At 400 MW pp is much higher for 0.2, temps much higher for 0.3

Flow rate (200 MW) = 900 kg/s = 5,600 Liters/s

Density in reactor = 0.146 g/cc

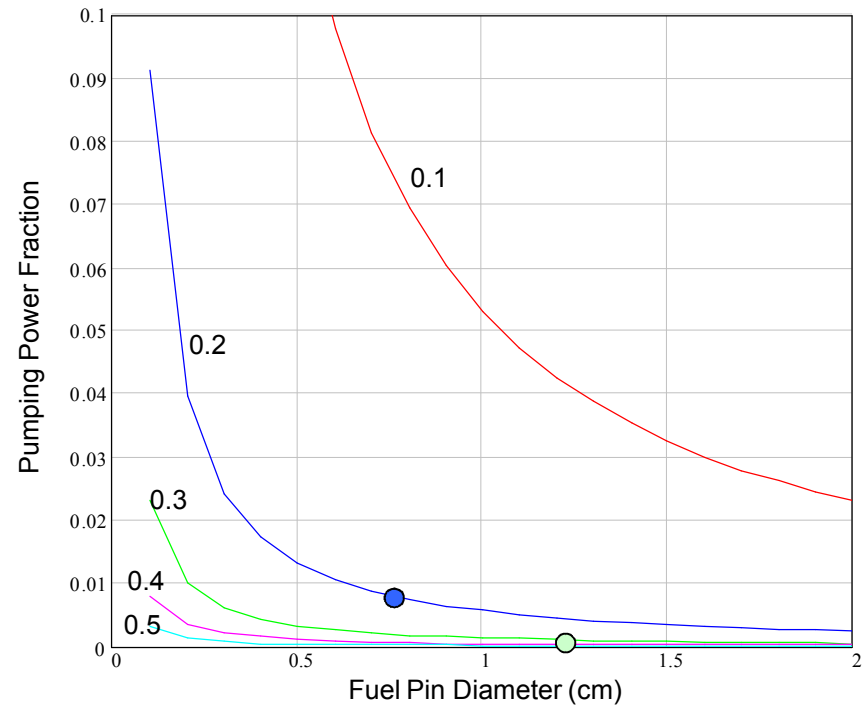
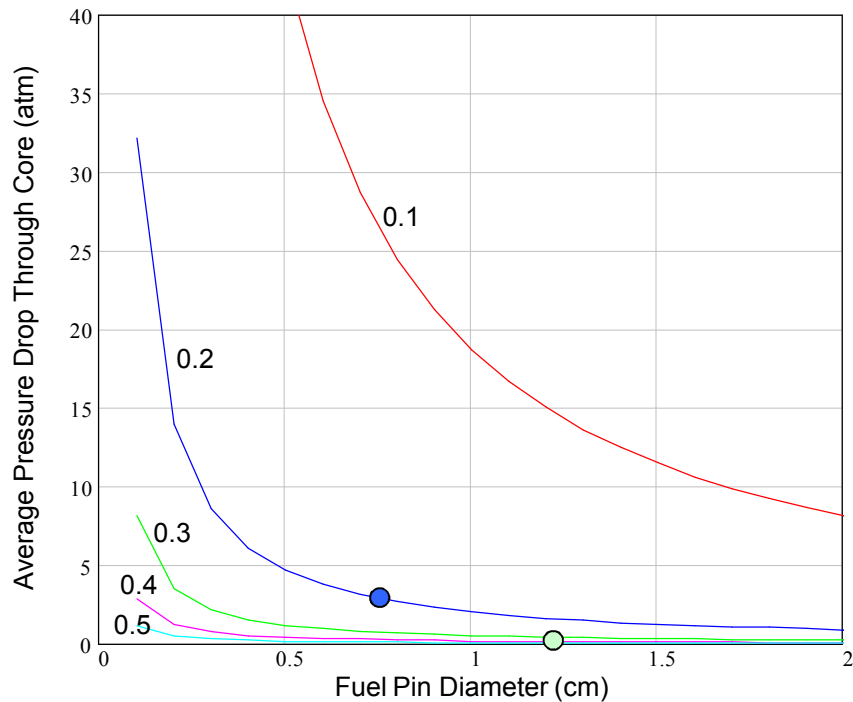
200 MWth Temperature Analysis



● 0.75 cm dia 0.2 cf - $T_{max} = 880^{\circ}\text{C}$, $T_{clad} = 600^{\circ}\text{C}$

● 1.20 cm dia 0.3 cf - $T_{max} = 1440^{\circ}\text{C}$, $T_{clad} = 690^{\circ}\text{C}$

200 MWth Flow Analysis



● 0.75 cm dia 0.2 cf - $\Delta P_{\text{core}} = 2.9 \text{ atm}$, PPfraction = 0.008 = 1.6 MW

● 1.20 cm dia 0.3 cf - $\Delta P_{\text{core}} = 0.4 \text{ atm}$, PPfraction = 0.001 = 0.23 MW



Keff, Burnup, and Void Coefficient



Reactor Burnup Calculations

Keff, Burnup, and Void Coefficients calculated using MCNP
Burnup using BURNAL (MCNP and Tallies)

Simple calculations performed to-date using one zone

Trade off reactor size, coolant fraction, and enrichment to maintain a constant Keff over the operating history.

UO₂ fuel, 12% en, clad thickness = 0.0056 cm HT9, gap = 0.008 cm
1.7 m dia x 1.6 m H, 15 cm Ni Reflector

Core Size

Case 1 - 0.75 cm OD, cf = 0.2

Core Vol = 3.63e6 cm³

f/c=0.550

Fuel vol = 2e6 cm³ ~20 MT

55W/cc core = 200 MW

Case 2 - 1.20 cm OD, cf = 0.3

Core Vol = 3.63e6 cm³

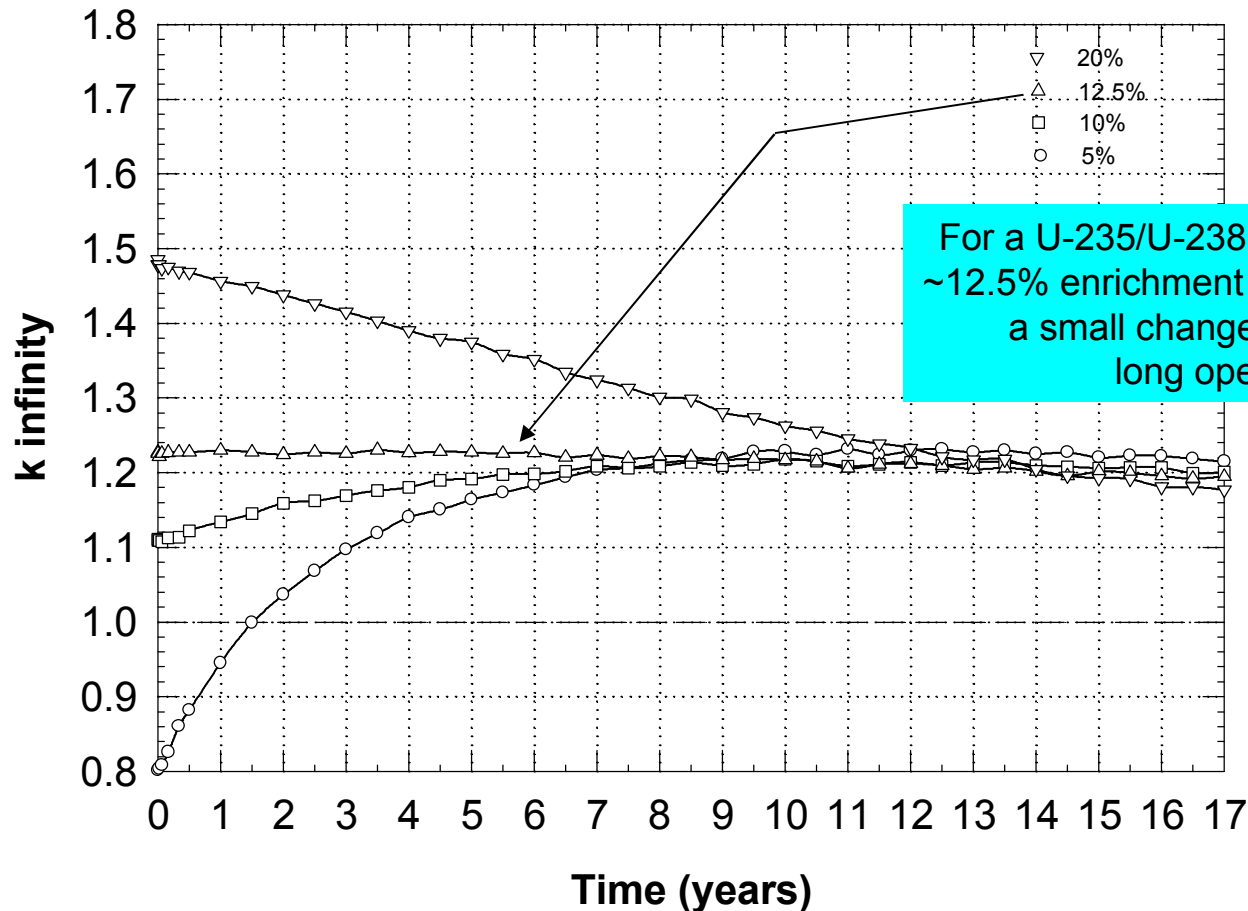
f/c=0.5586

Fuel vol = 2e6 cm³ ~20 MT

55W/cc core = 200 MW

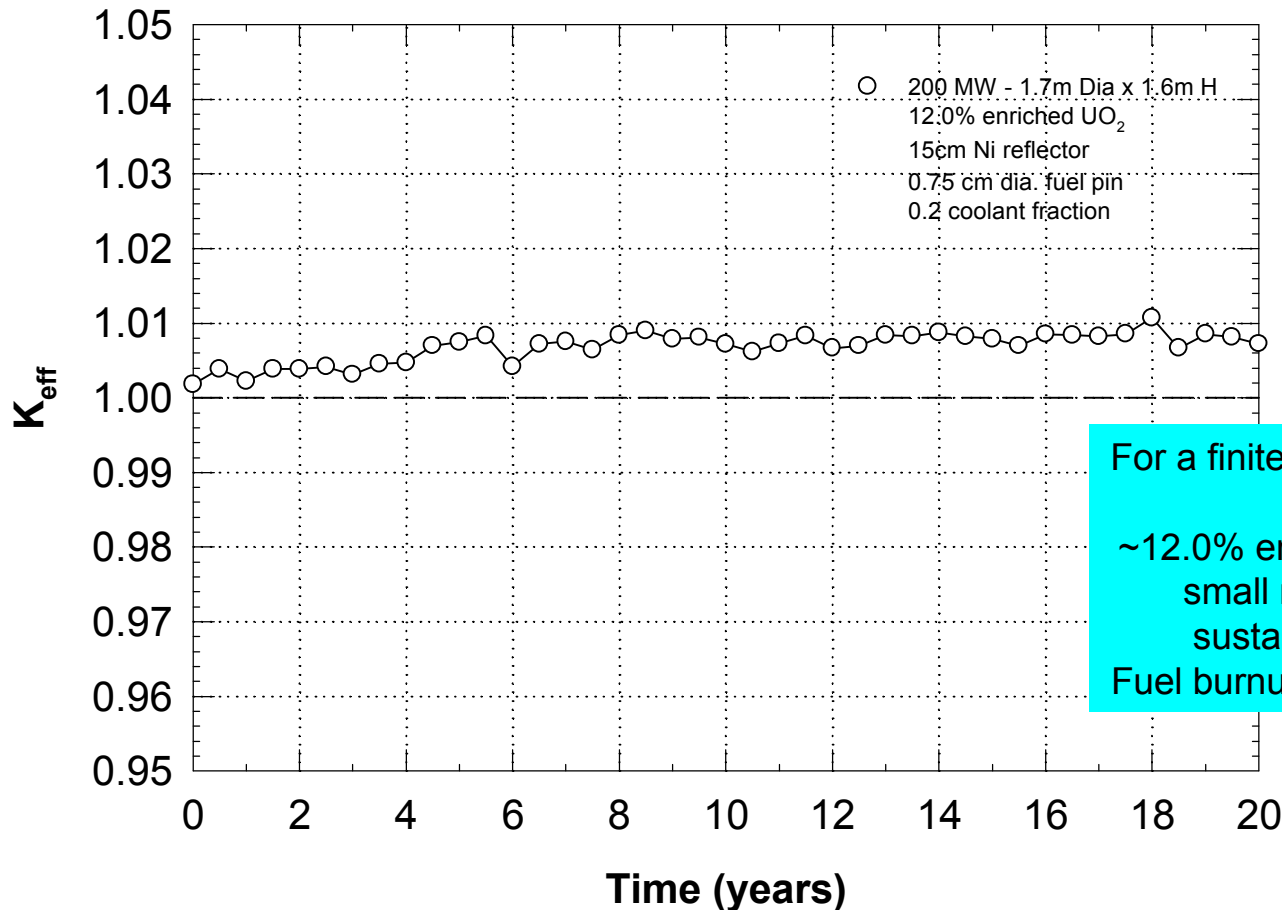
K infinity Burnup Calculation

MCNP k Infinity vs. Operating Time
U-235 UO₂ 20%v CO₂ 50 MW/MT



200 MW Burnup for 12.0% Core – Case 1

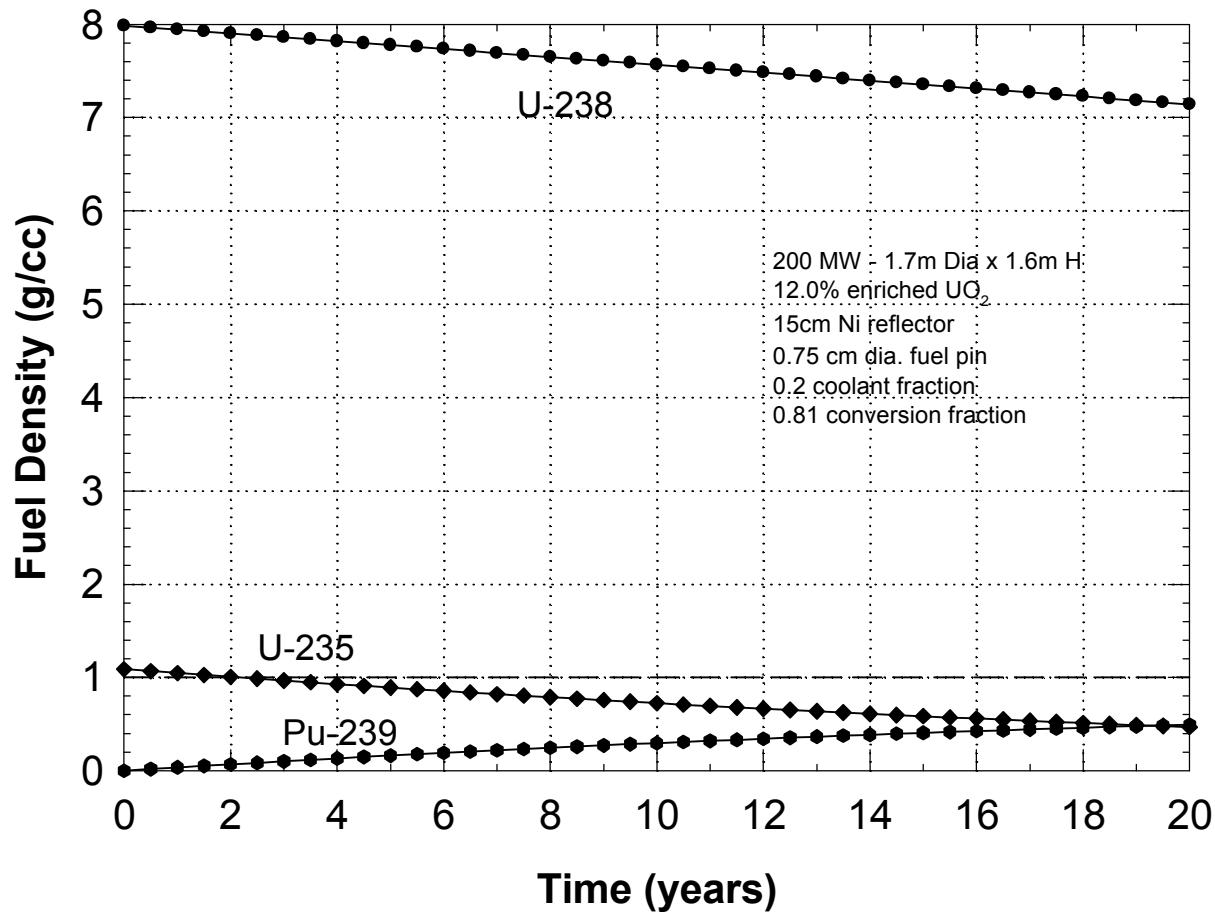
MCNP k effective vs. Operating Time
12.0%U-235 UO₂ 20%v CO₂ 200 MW



For a finite core with 0.2 cf and 0.75 cm diameter fuel pin, ~12.0% enrichment works. A relatively small reactivity change over time is sustainable ($\Delta k=0.01$) at 200 MW. Fuel burnup would be 72,000 MWD/MT

Fuel Constituent Density

MCNP Fuel Density vs. Operating Time
12.0%U-235 UO₂ 20%v CO₂ 200 MW



Reactivity Void Coefficient

Void Coefficients calculated using MCNP at 20 MPa (3000 psi) and 0.1 MPa (14.7 psi) pressure and 550°C temperature gas.

From Lewins – Fast Fission - $\beta(\text{U-235}) = 0.0066$
 $\beta(\text{U-238}) = 0.0161$
 $\beta(\text{Pu-239}) = 0.00212$

Estimates for the delayed neutron fraction β

$\beta \text{ BOL} = 0.0080$

$\beta \text{ EOL (200 MW @ 20 yrs)} = 0.0062$

$\beta \text{ EOL (400 MW @ 20 yrs)} = 0.0052$

Case 1 - 0.75 cm OD, cf = 0.2

$\Delta k/k \text{ (BOL)} = 0.00185 \pm 0.0016$

$\rho = +\$0.23 \pm \0.20

$\Delta k/k \text{ (200MW@20yrs)} = 0.0020 \pm 0.0015$

$\rho = +\$0.32 \pm \0.24

$\Delta k/k \text{ (400MW@20yrs)} = 0.0015 \pm 0.0013$

$\rho = +\$0.29 \pm \0.25

Case 2 - 1.20 cm OD, cf = 0.3

$\Delta k/k \text{ (BOL)} = 0.00056 \pm 0.0015$


$\rho = +\$0.07 \pm \0.19

$\Delta k/k \text{ (200MW@20yrs)} = 0.0057 \pm 0.0015$

$\rho = +\$0.92 \pm \0.24

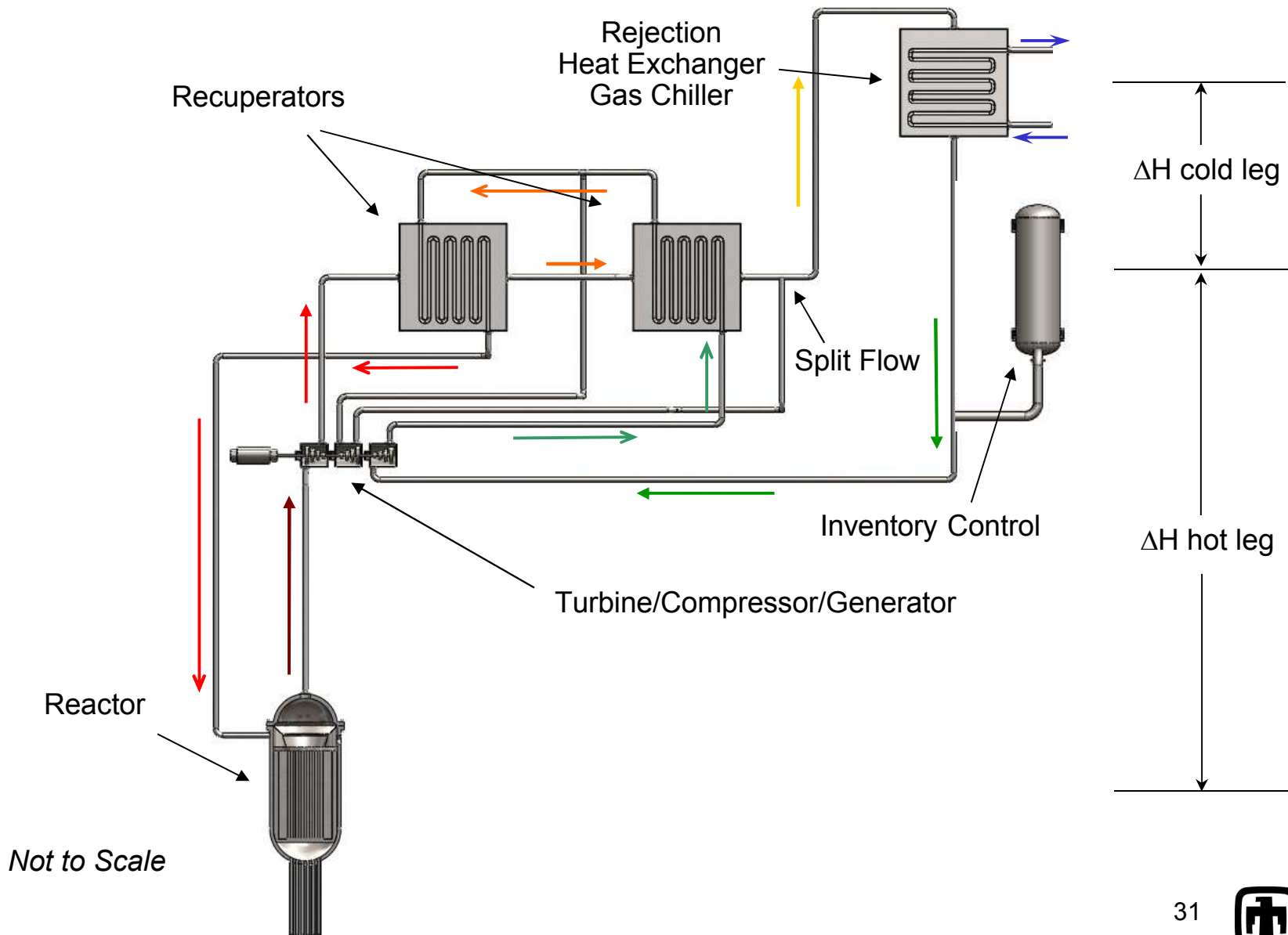
$\Delta k/k \text{ (400MW@20yrs)} = 0.0040 \pm 0.0014$

$\rho = +\$0.76 \pm \0.27



Natural Circulation Flow And Decay Heat Removal

Natural Convection Flow





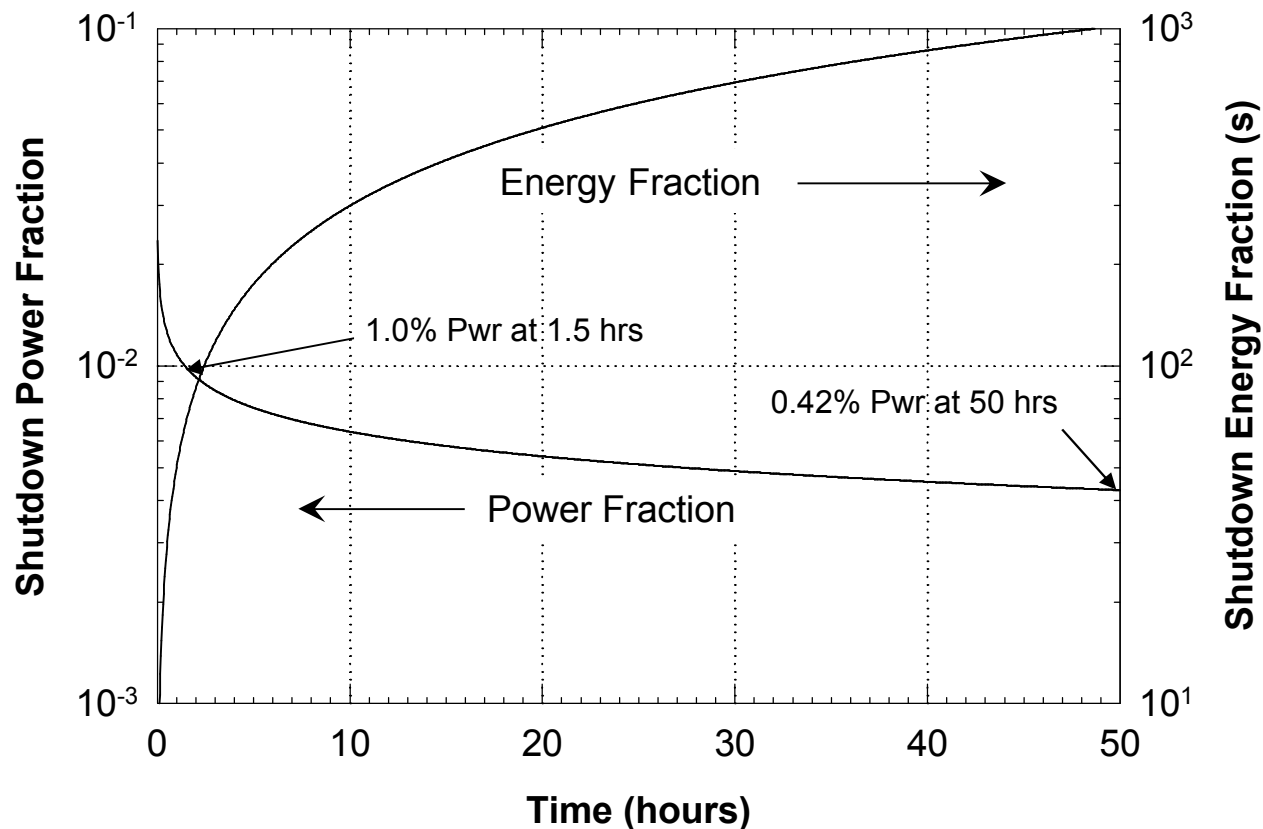
Natural Circulation Summary

- **Developed Simple Scoping Calculation Models in Excel**
 - Based on theory described by D. Milone
 - Validated against experiments in a 1/2" OD Loop 72" Tall
- **Modified Scoping Model to Apply it to**
 - Reactors, Heat Exchangers, Gas-Chiller
 - Evaluated Proposed SNL Experiment
- **Developed a 3 D CFD model by modifying a fire code C3D**
 - Implement Nist Calls
 - Modified Energy Equation to use Enthalpy
 - Verified against D. Milone Report
 - Explored Natural Circ in Rx, with HXs and with Gas Chiller

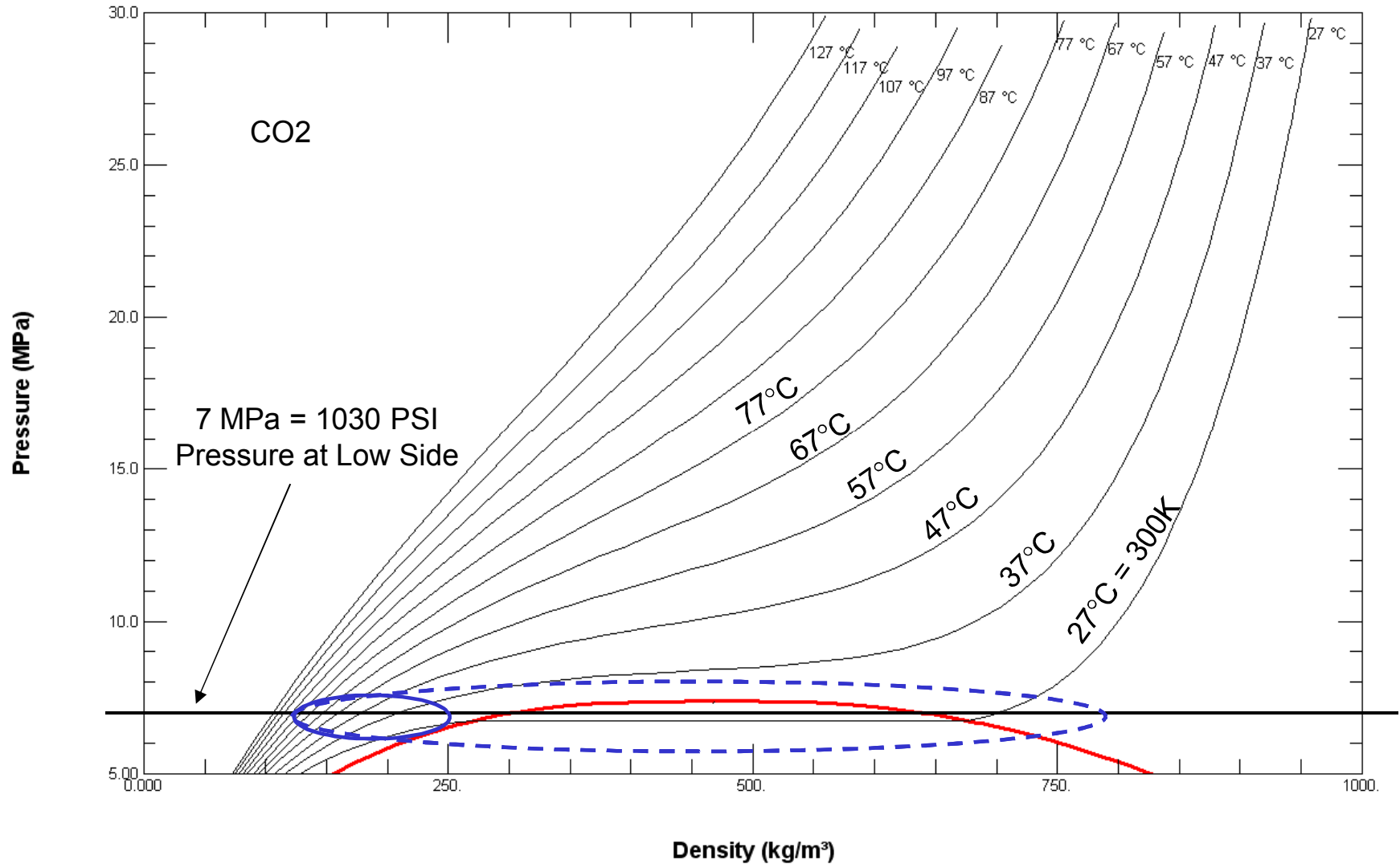
Background

Wigner-Way Formulation for Decay Power

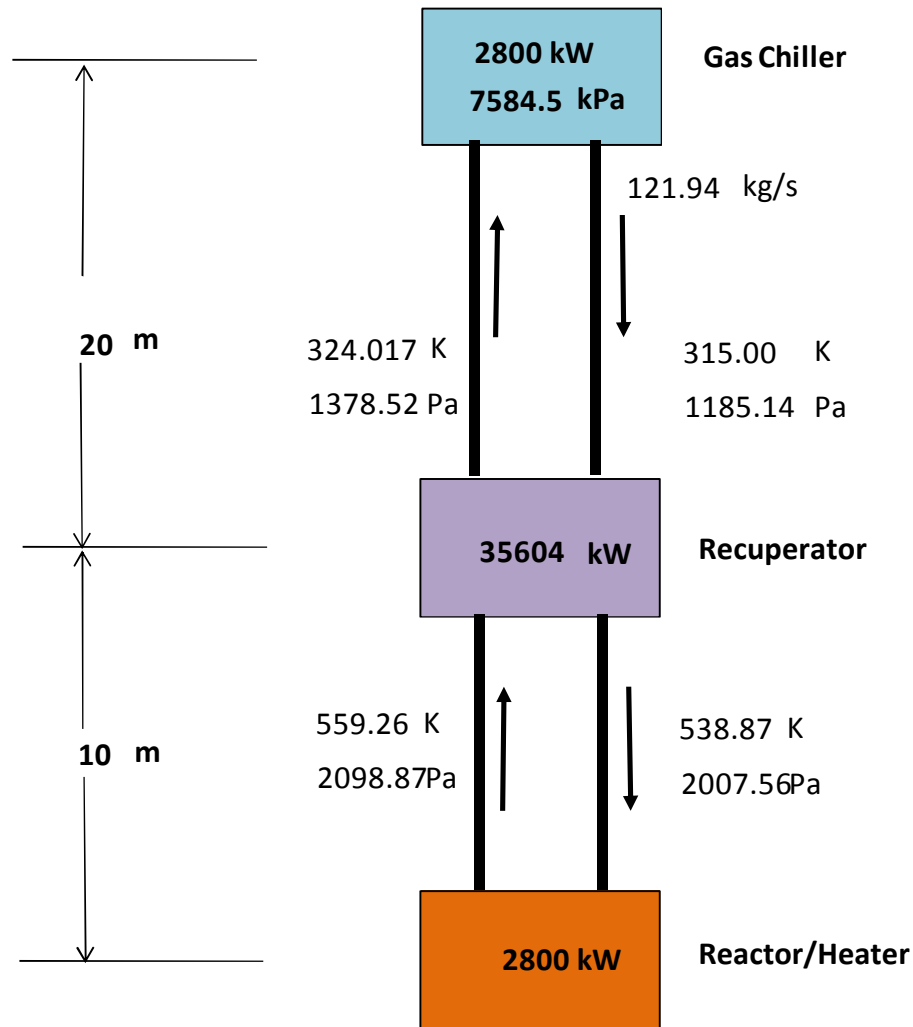
$$P_d(t) / P_0 = 0.0622 \left[t^{-0.2} - (t_0 + t)^{-0.2} \right]$$



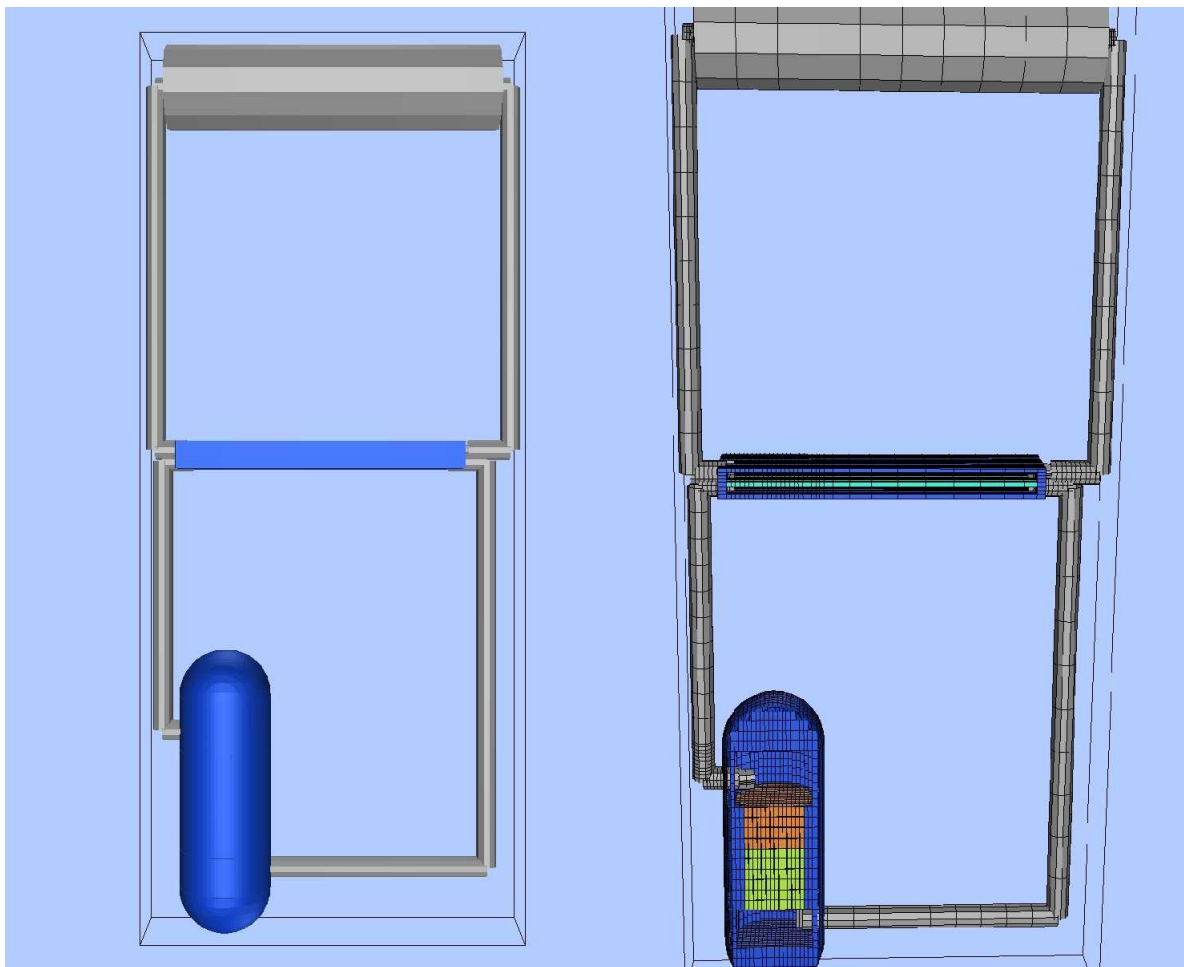
Conditions for Natural Circulation



Lumped Parameter Analysis (2.8 MW decay heat source)



CD3-SC Natural Convection Flow





Natural Circulation Concussions

- Large amounts of natural circulation occur in S-CO₂
 - Need a sufficiently large elevation difference between the gas chiller and the heat sources (10 m)
 - Pressures need to be kept near the critical pressure
 - (5-12 MPa)
 - HXs/Recuperators do not destroy the ability for natural circulation
 - Pressure drop is important large dPs must be avoided
 - e. g. turbine and compressor
 - If large dP's exist they can be bypassed
 - There is sufficient flow to remove decay heat given proper design
 - SNL now has tools to evaluate S-CO₂ Natural Circulation
 - Both scoping and CFD codes
 - So effect on reactor can be modeled



Economics



Cost Estimates

Initial Core Loading Fuel Cost (20 MT, 12% enriched = 7,500\$/kg) = **\$150M**

- future cores with Pu recycle would be expected to be much less

HX cost (2 recuperators and 1 heat rejection = **20 to \$50M**

Pressure Vessel and Piping = **\$50M**

Total = **\$250M**

At \$5,000/kW a 100 MWe system would cost **\$500M**



Summary

- From the analyses that we have preformed so far, we believe that the direct cycle, S-CO₂ cooled, fast reactor concept is worth further study.
- The concept is simple and relatively straight forward. We have shown that a reactor power of 200 to 400 MWth is achievable with a reactivity burnup lifetime of potentially up to 20 years.
- The concept has many advantages over other advanced reactor concepts. The reactor can be cooled by natural circulation flow in the event of a loss of flow condition.
- The major disadvantages are the high pressure of the reactor coolant and the corrosion at high temperatures. The pressure can be lowered significantly without a large penalty in efficiency using a slightly different cycle configuration, and will be studied in future work. Corrosion issues requires further experimental work.