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2010

Designing an Enhanced Groundwater Sample Collection System

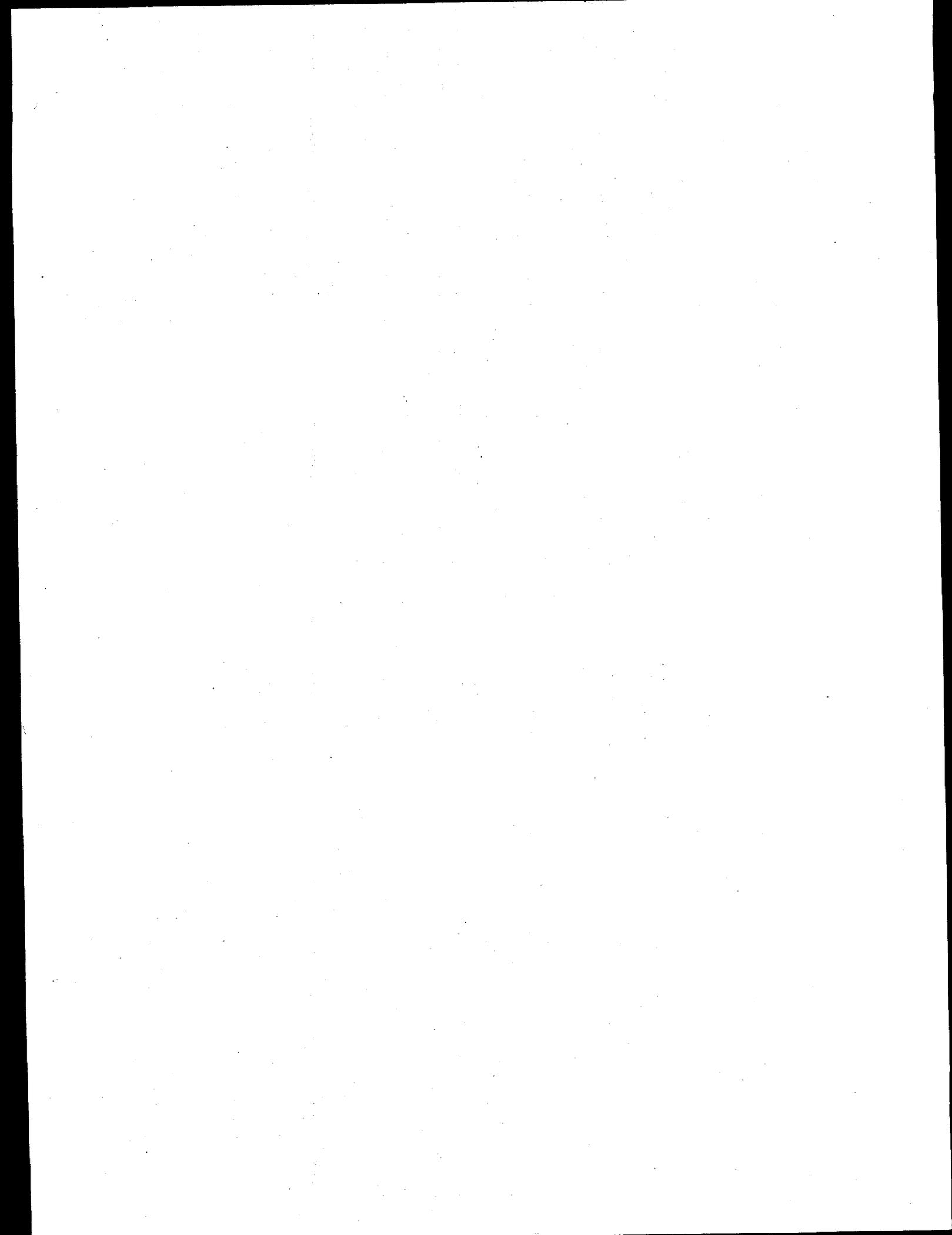
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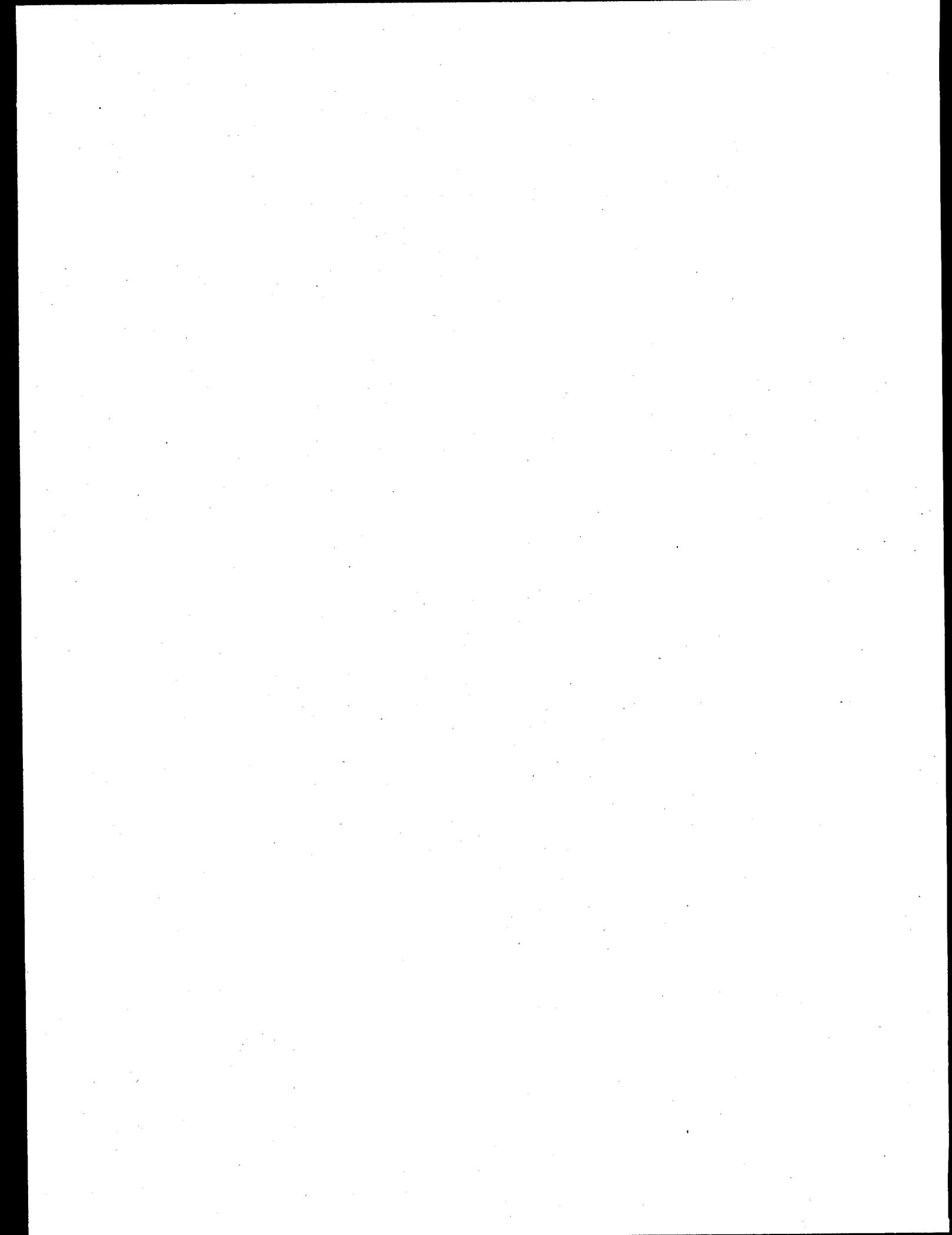
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Executive Summary

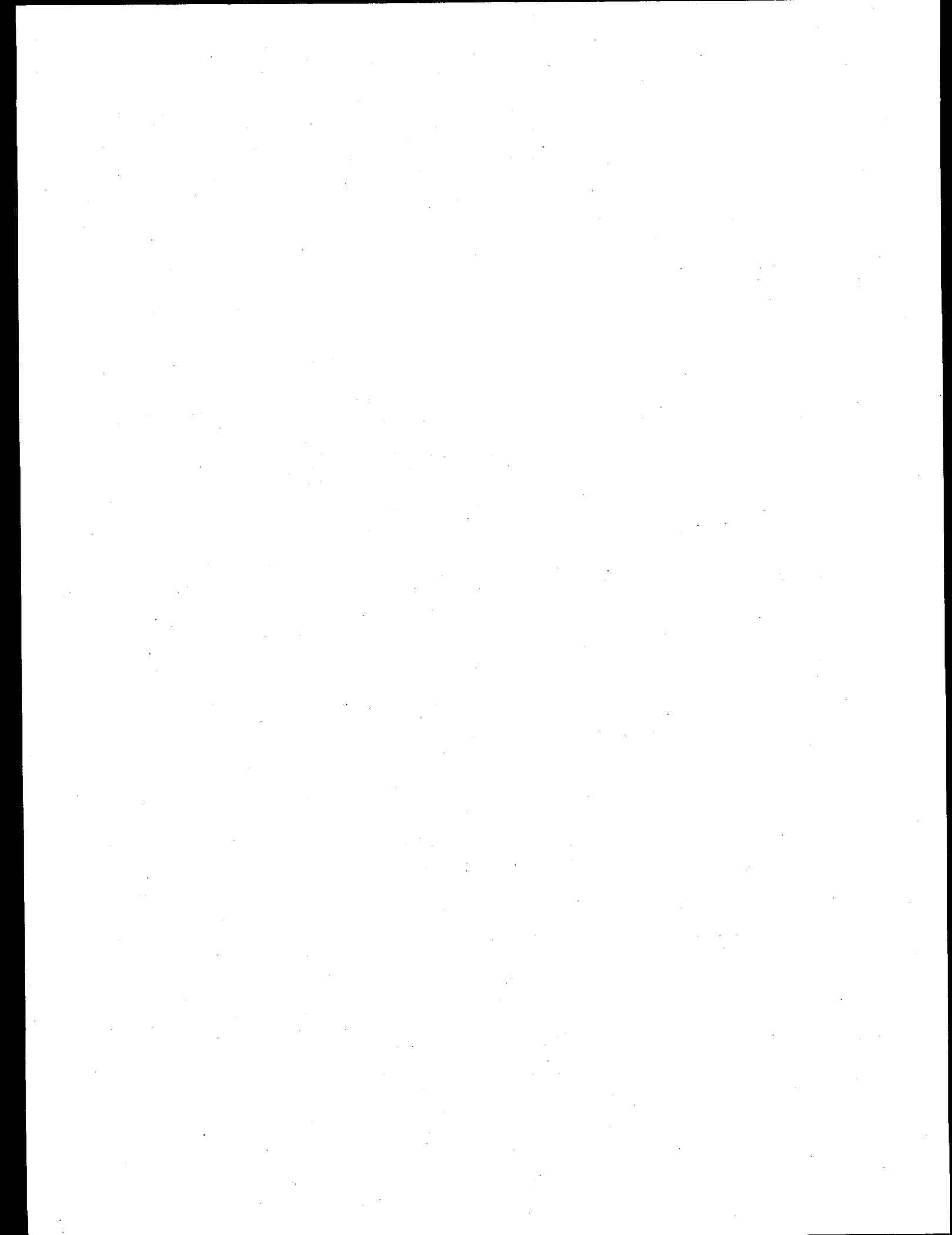
As part of an ongoing technical support mission to achieve excellence and efficiency in environmental restoration activities at the Laboratory for Energy and Health-Related Research (LEHR), the LEHR project manager requested Pacific Northwest Laboratory (PNL) guidance on the design and construction of monitoring wells. The LEHR project, located at the University of California, Davis, also asked PNL to identify the most suitable type of groundwater sampling pump and accessories for their newly constructed monitoring wells. Primarily, the goal was to utilize a monitoring well design that would allow for hydrologic testing and reduce turbidity to minimize the impact of sampling. In the previously installed monitoring wells, the turbidity exceeded regulatory levels for drinking water during the purging cycle and sometimes during the sampling cycle. During the study, purging and sampling procedures were evaluated. Available expertise and American Society for Testing and Materials (ASTM) standards were used as the bases to design, construct, and develop the monitoring wells. Published literature was reviewed to identify the people working in groundwater monitoring who could aid in identifying the most effective sampling pumps to collect representative groundwater samples at LEHR.

The sampling results of the newly designed monitoring wells were clearly superior to those of the previously installed monitoring wells. The new wells exhibited reduced turbidity, in addition to improved access for instrumentation and hydrologic testing. Following the results of the literature review, the variable frequency submersible pump was selected as the best choice between several alternative devices for obtaining groundwater samples. The literature references are listed at the end of this report. Despite some initial difficulties, the actual performance of the variable frequency, submersible pump and its accessories was effective in reducing sampling time and labor costs, and its ease of use was preferred over the previously used bladder pumps. The surface seals system, called the Dedicator, proved to be a useful accessory to prevent surface contamination while providing easy access for water-level measurements and for connecting the pump. Cost savings resulted from the use of the pre-production pumps (beta units) donated by the manufacturer for the demonstration. However, larger savings resulted from shortened field time due to the ease in using the submersible pumps and the surface seal access system. Proper deployment of the monitoring wells also resulted in cost savings and ensured representative samples.



Glossary

<u>Abbreviation or Acronym</u>	<u>Definition</u>
ASTM	American Society for Testing and Materials
bgs	below ground surface
BV	screened interval, sand pack, and casing volume
ft/ft	foot per foot (slope)
gpm	gallons per minute
HSU	hydrostratigraphic unit
HWL	high water level
IC	internal combustion
LEHR	Laboratory for Energy and Health-Related Research
LWL	low water level
MFG	manufacturer
MSLD	depth below mean sea level
NTU	nephelometric turbidity unit
Pa	a pascal; unit of measure equal to one newton per square meter
psi	pound (force) per square inch (lbf/in ²)
PTFE	polytetrafluoroethylene
PVC	polyvinyl chloride
SC	screened interval
SPSC	screened interval and filter pack
SWAT	site wide assessment team
TEGD	technical enforcement guidance document
TOC	total organic carbon
TOH	total organic halogen
UCD	well designation (UC Davis)
UC Davis	University of California, Davis
VOA	volatile organic analyte
VOC	volatile organic constituent



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1.0 Introduction

As part of an ongoing technical support mission to achieve excellence and efficiency in environmental restoration activities at the Laboratory for Energy and Health-Related Research (LEHR), the LEHR project manager requested Pacific Northwest Laboratory (PNL)^(a) guidance on the design and construction of monitoring wells. The project manager also requested identification of the most suitable type of groundwater sampling pump and accessories for the newly constructed monitoring wells at LEHR.

This report includes a brief description of the hydrogeologic setting and wells used for this particular demonstration of enhanced groundwater sample collection systems. Some discussion is also provided regarding regulatory requirements and guidance, and contaminants of concern at LEHR. The report focuses primarily on the groundwater sample collection system which includes: the monitoring well, the sampling pump, and its accessory components. Included are descriptions of the construction and development of the monitoring wells and the resulting benefits, the performance criteria used to select the pump and accessories, and the actual performance of the enhancements of the groundwater collection system at 10 new wells. Conclusions are based on the literature review and the reference list in Section 7.0.

Radiological and chemical constituents are monitored in the groundwater at LEHR. The current missions of LEHR decommissioning, which include waste management and environmental restoration, as well as compliance with environmental regulations concerned with groundwater, require collection of reliable groundwater samples. To achieve this goal, an effective groundwater sample collection system was designed, constructed, and installed during the years 1990 through 1992.

This report contains seven sections. Section 2.0 describes the processes for constructing and developing monitoring wells. Section 3.0 explains the method for pump selection. Section 4.0 discusses the actual performance of the equipment. Section 5.0 includes details of various cost savings. Section 6.0 provides a concluding paragraph about the improvements of the groundwater collection system at the University of California, Davis (UC Davis). Section 7.0 lists the sources used as reference material for this report.

(a) Pacific Northwest Laboratory is operated for the U.S. Department of Energy by Battelle Memorial Institute under Contract DE-AC06-76RLO 1830.

1.1 Purpose

The purpose of this report is to present the results of the design, installation, and actual operation of the enhanced groundwater sample collection system at LEHR. The information presents the rationale used for the sample collection system improvements and delineates cost savings. Based on knowledge of the LEHR site, the groundwater was considered to contain contaminants of concern in solution in the aqueous phase.

1.2 Hydrogeologic Setting

The two most shallow hydrostratigraphic units (HSU-1 and HSU-2) and their hydraulic characteristics comprise the hydrogeologic setting of interest at the time the first 24 monitoring wells were installed. Descriptions of these units are provided in the following subsections.

1.2.1 Hydrostratigraphic Units

At the time of this effort, the focus was on the most likely contaminant transport pathways, the uppermost aquifers at the site. During this investigation, the focus was on two shallow hydrostratigraphic units. The shallowest, HSU-1, extends from 3 to 24 m (10 to 80 ft) bgs, and consists of very fine-grained sandy silt or silty sand to sandy clay. Located within 1.6 km (1 mi) of the site, the second unit, HSU-2, consists of coarse sand and gravel, and is relatively extensive. The HSU-2 unit is found between 24 and 41 m (80 and 135 ft) bgs. Because groundwater depths range from approximately 14 to 21 m (45 to 70 ft) bgs, HSU-1 is generally thought of as unconfined and the deeper HSU-2 layer is generally thought of as confined. Actually, the two units are hydraulically interconnected and the amount of isolation is minor. The character of these units not only affects the contaminant residence and travel times, but also can impact the sample collection system. Below HSU-2 is a lower clay zone that is several meters thick. Figure 1.1 is a generalized cross section of the LEHR site that indicates the high water level (HWL) and low water level (LWL) of two UCD wells.

1.2.2 Hydraulic Characteristics

Groundwater elevations beneath the site vary from approximately 1.5 m (5 ft) above to 6.1 m (20 ft) below mean sea level throughout the year. Generally, water levels are at their highest level in early spring and at their lowest in late summer. Lateral groundwater gradients in HSU-1 vary from 0.0001 to 0.0015 ft/ft, and are typically 0.0015 ft/ft in HSU-2. Generally, groundwater flow direction

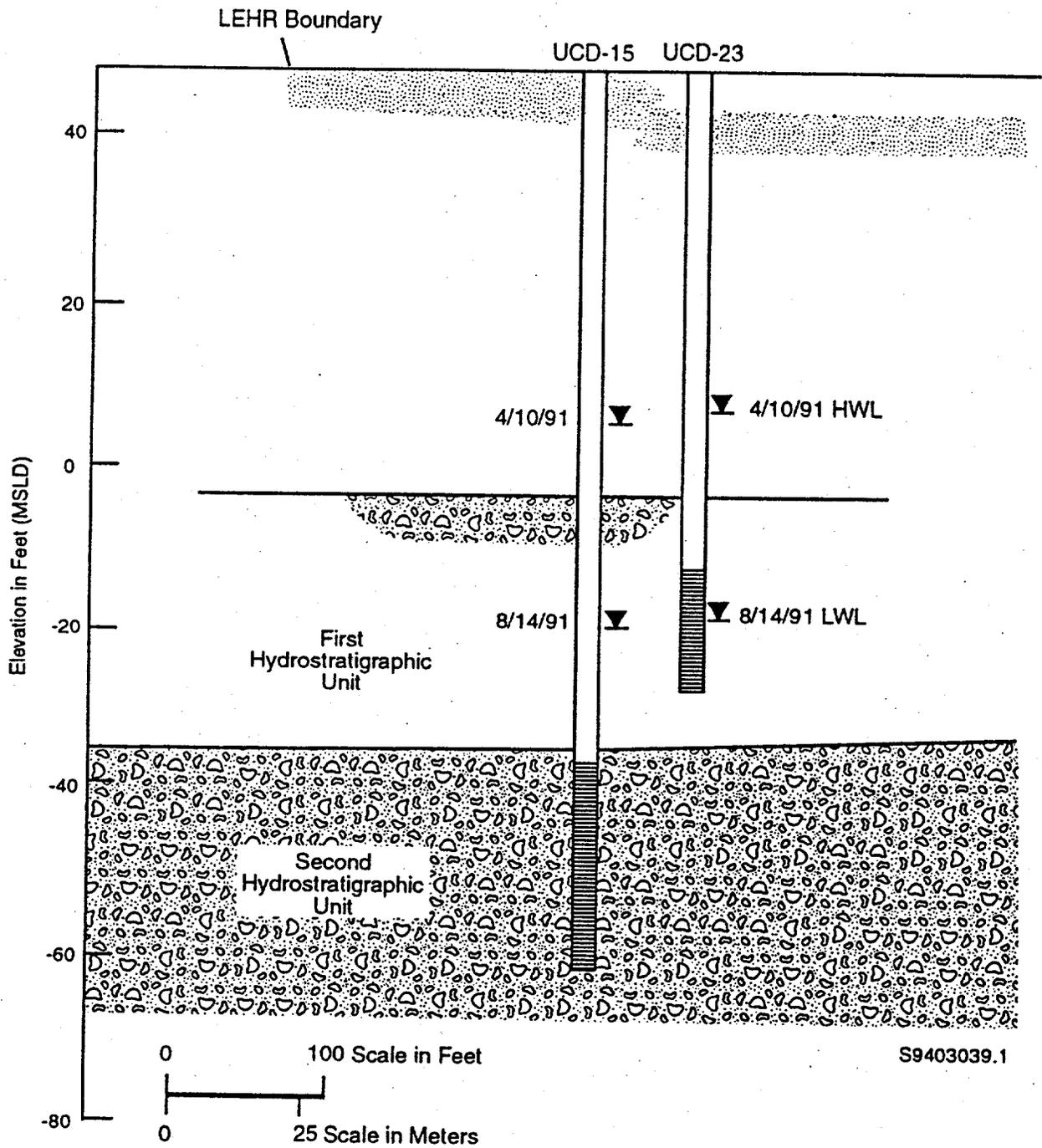


Figure 1.1. Generalized Cross Section of First and Second Hydrostratigraphic Units

is toward the northeast, but temporary local changes in flow direction occur, particularly in HSU-1. Putah Creek (see Figure 1.2) recharges locally and creates a groundwater flow barrier in HSU-1. Horizontal hydraulic conductivities average 1.5×10^{-3} cm/sec (4.9×10^{-5} ft/sec) for HSU-1 and 9.0×10^{-3} cm/sec (3.0×10^{-4} ft/sec) for HSU-2.

1.3 Well Locations

During the site investigation, 10 monitoring wells were constructed. Wells UCD-18 through UCD-24 were screened in the finer-grained silt-rich sand of the HSU-1 unit and three others, UCD-15 through UCD-17, were screened in the deeper, coarser-grained sequence of sand and gravel of HSU-2. Table 1.1 provides a summary of monitoring wells, including the 10 constructed most recently. The locations of the wells, in relation to the site, are shown in Figure 1.2.

1.4 History of Operations

During the 30-yr operation of the LEHR facility, a variety of wastes were generated and disposed of on-site. These wastes included radioactive, biological, chemical, municipal, and laboratory debris. A brief summary of waste generating processes and potential sources of environmental impacts on groundwater at the LEHR facility are presented in the following paragraphs.

UC Davis has conducted radiological studies on laboratory animals for the U.S. Department of Energy (DOE) since the 1950s. The initial studies, conducted for the U.S. Atomic Energy Commission (AEC, now DOE), involved the irradiation of beagles at the UC Davis main campus. Full-scale experimental use of radioactive materials, including strontium-90 and radium-226, began at LEHR in 1960. Disposal locations at the LEHR facility included the two disposal units of the UC Davis campus landfill. Disposal Unit No. 1 was used during the 1940s and 1950s. Disposal Unit No. 2 was used from 1956 to 1967. A third landfill disposal unit was used by LEHR from 1963 to 1967. The combined total acreage of the three landfills was approximately 2.4 ha (6 a).

Radiologic wastes generated from animal experiments using bone-seeking radionuclides were treated using two primary systems. From 1960 to 1987, effluent from strontium-90 experiments was processed through an Imhoff sewage treatment system. From 1982 to 1984, a total of 39.59 μ Ci of plutonium-241 and 0.136 μ Ci of americium-241 were processed through the Imhoff treatment

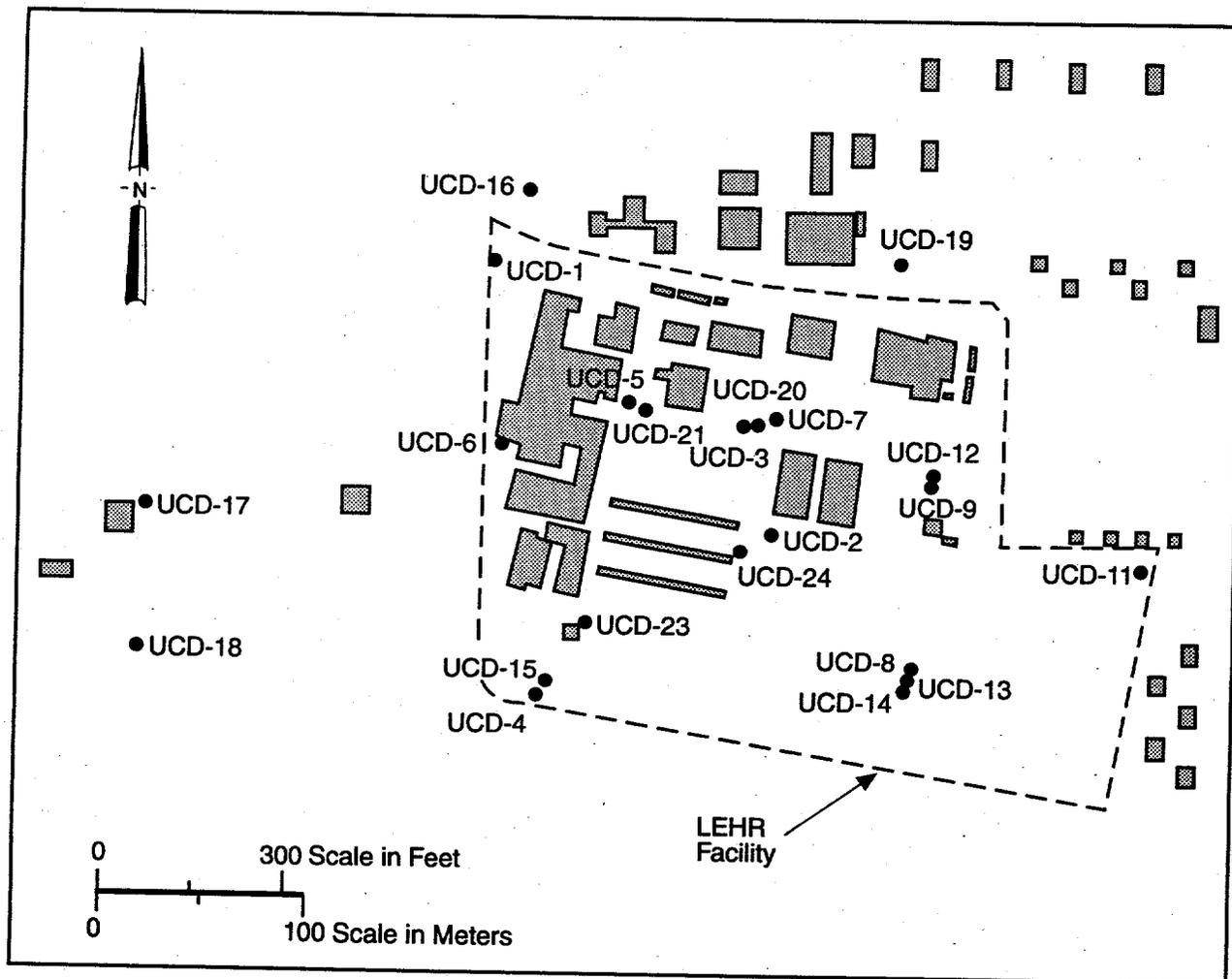


Figure 1.2. Monitoring Well Location Map at LEHR

system. This system uses a series of settling tanks and cation exchange columns to treat approximately 758 to 1895 L (200 to 500 gal) per day of waste, prior to discharge to leach fields. The total throughput of strontium-90 to the Imhoff system is estimated at 943.2 mCi. After treatment through the Imhoff system, an estimated 2.55 mCi of strontium-90 were released to the Imhoff leach field and subsurface soil. The half-life of strontium-90 is 29 yr.

Table 1.1. Monitoring Well Construction Summary

UCD-1 Through UCD-6

	UCD-1	UCD-2*	UCD-3	UCD-4	UCD-5	UCD-6
Casing Type/ Diameter	PVC/5.1 cm (2 in.)		PVC/5.1 cm (2 in.)	PVC/5.1 cm (2 in.)	PVC/5.1 cm (2 in.)	PVC/5.1 cm (2 in.)
Screen Type/ Slot Size	PVC/0.51 mm (0.020 in.)		PVC/0.51 mm (0.020 in.)	PVC/0.51 mm (0.020 in.)	PVC/0.51 mm (0.020 in.)	PVC/0.51 mm (0.020 in.)
Slot Type	Slotted		Slotted	Slotted	Slotted	Slotted
Screen Length	3.1 m (10 ft)		3.1 m (10 ft)			
Screen Interval bgs	14.7 - 17.2 m (46.5 - 56.5 ft)		11.9 - 14.9 m (39.0 - 49.0 ft)	13.7 - 16.8 m (45.0 - 55.0 ft)	11.6 - 14.6 m (38.0 - 48.0 ft)	12.2 - 15.2 m (40.0 - 50.0 ft)
Silt Trap	No		No	No	No	No
Filter Pack Type	Lone Star		Lone Star	Lone Star	Lone Star	Lone Star
Mesh Sieve Size	8 - 20		8 - 20	8 - 20	8 - 20	8 - 20
Filter Pack Interval	14.6 - 17.2 m (48.0 - 56.5 ft)		10.4 - 15.7 m (34.0 - 51.5 ft)	12.2 - 16.8 m (40.0 - 55.0 ft)	10.1 - 14.6 m (33.0 - 48.0 ft)	10.7 - 15.2 m (35.0 - 50.0 ft)
Primary Seal	Grout		Grout	Grout	Grout	Grout
Secondary Seal	Bentonite		Bentonite	Bentonite	Bentonite	Bentonite
Surface Completion	Aboveground		Aboveground	Aboveground	Aboveground	Belowground
Pump Type	Redi-Flo2		Bladder	Redi-Flo2	Bladder	Bladder
HSU Unit and Depth of Casing	1st/17.2 m (56.5 ft)		1st/14.9 m (49.0 ft)	1st/16.8 m (55.0 ft)	1st/14.6 m (48.0 ft)	1st/15.2m (50.0 ft)
Date Completed	10/09/87		10/23/87	10/14/87	10/22/87	10/21/87

*Abandoned well

UCD-7 Through UCD-12

	UCD-7	UCD-8	UCD-9	UCD-10	UCD-11	UCD-12
Casing Type/ Diameter	PVC/5.1 cm (2 in.)	PVC/5.1 cm (2 in.)	PVC/5.1 cm (2 in.)	PVC/10.2 cm (4 in.)	PVC/10.2 cm (4 in.)	PVC/10.2 cm (4 in.)
Screen Type/ Slot Size	PVC/0.51 mm (0.020 in.)	PVC/0.51 mm (0.020 in.)	PVC/0.51 mm (0.020 in.)	PVC/0.25 mm (0.010 in.)	PVC/0.25 mm (0.010 in.)	PVC/0.25 mm (0.010 in.)
Slot Type	Slotted	Slotted	Slotted	Slotted	Slotted	Slotted
Screen Length	3.1 m (10 ft)	3.1 m (10 ft)	3.1 m (10 ft)	4.6 m (15 ft)	4.6 m (15 ft)	4.6 m (15 ft)
Screen Interval bgs	24.4 - 27.4 m (80.0 - 90.0 ft)	13.3 - 16.3 m (43.5 - 53.5 ft)	12.2 - 15.2 m (40.0 - 50.0 ft)	16.5 - 21.0 m (54.0 - 69.0 ft)	15.2 - 19.8 m (50.0 - 65.0 ft)	15.1 - 19.7 m (49.5 - 64.5 ft)
Silt Trap	No	No	No	Yes	Yes	Yes
Filter Pack Type	Lone Star					
Mesh Sieve Size	8 - 20	8 - 20	8 - 20	16 - 40	16 - 40	16 - 40
Filter Pack Interval	22.9 - 27.4 m (75.0 - 90.0 ft)	11.9 - 16.3 m (39.0 - 53.5 ft)	10.8 - 15.2 m (35.0 - 50.0 ft)	15.9 - 21.3 m (52.0 - 70.0 ft)	17.4 - 20.3 m (57.0 - 66.5 ft)	14.3 - 20.3 m (47.0 - 66.5 ft)
Primary Seal	Grout	Grout	Grout	Grout	Grout	Grout
Secondary Seal	Bentonite	Bentonite	Bentonite	Bentonite	Bentonite	Bentonite
Surface Completion	Aboveground	Aboveground	Aboveground	Aboveground	Aboveground	Aboveground
Pump Type	Redi-Flo2	Bladder	Bladder	Redi-Flo2	Redi-Flo2	Redi-Flo2
HSU Unit and Depth of Casing	2nd/27.4 m (90.0 ft)	1st/16.3 m (53.5 ft)	1st/15.2 m (50.0 ft)	1st/21.3m (70.0 ft)	1st/20.3 m (66.5 ft)	1st/20.3 m (66.5 ft)
Date Completed	11/05/87	11/03/87	11/04/87	10/11/89	10/17/89	10/19/89

Table 1.1. (contd)

UCD-13 Through UCD-18

	UCD-13	UCD-14	UCD-15	UCD-16	UCD-17	UCD-18
Casing Type/ Diameter	PVC/10.2 cm (4 in.)	PVC/10.2 cm (4 in.)	PVC/10.2 cm (4 in.)	PVC/10.2 cm (4 in.)	PVC/10.2 cm (4 in.)	PVC/10.2 cm (4 in.)
Screen Type/ Slot Size	PVC/0.25 mm (0.010 in.)	PVC/0.51 mm (0.020 in.)	SS/0.51 mm (0.020 in.)	SS/0.76 mm (0.030 in.)	SS/0.51 mm (0.020 in.)	SS/0.25 mm (0.010 in.)
Slot Type	Slotted	Slotted	Wirewrap	Wirewrap	Wirewrap	Wirewrap
Screen Length	4.6 m (15 ft)	3.1 m (10 ft)	7.6 m (25 ft)	7.6 m (25 ft)	7.6 m (25 ft)	4.6 m (15 ft)
Screen Interval bgs	15.2 - 19.8 m (50.0 - 65.0 ft)	22.9 - 25.9 m (75.0 - 85.0 ft)	27.7 - 35.4 m (91.0 - 116.0 ft)	27.9 - 35.5 m (91.5 - 116.5 ft)	26.8 - 34.4 m (88.0 - 113.0 ft)	17.0 - 21.6 m (55.9 - 70.9 ft)
Silt Trap	Yes	No	No	No	No	No
Filter Pack Type	Lone Star	Lone Star	Lone Star	Lone Star	Lone Star	Lone Star
Mesh Sieve Size	16 - 40	16 - 40	12 - 20	12 - 20	12 - 20	16 - 40
Filter Pack Interval	14.3 - 20.6 m (47.0 - 67.5 ft)	21.0 - 26.2 m (69.0 - 86.0 ft)	26.2 - 36.7 m (86.0 - 120.5 ft)	27.1 - 37.2 m (89.0 - 122.0 ft)	25.6 - 34.4 m (84.0 - 113.0 ft)	15.5 - 21.2 m (51.0 - 69.5 ft)
Primary Seal	Grout	Grout	Grout	Grout	Grout	Grout
Secondary Seal Thickness	Bentonite	Bentonite	Bentonite 6.4 m (21 ft)	Bentonite 5.5 m (18 ft)	30-50 Mesh Sand 0.9 m (3.0 ft) Volclay 0.9 m (3.0 ft)	Bentonite
Surface Completion	Aboveground	Aboveground	Aboveground	Aboveground	Aboveground	Aboveground
Pump Type	Redi-Flo2	Redi-Flo2	Redi-Flo2	Redi-Flo2	Redi-Flo2	Redi-Flo2
HSU Unit and Depth of Casing	1st/20.3 m (66.5 ft)	2nd/25.9 m (85.0 ft)	2nd/35.4 m (116.0 ft)	2nd/35.5 m (116.5 ft)	2nd/34.4 m (113.0 ft)	1st/21.6 m (70.9 ft)
Date Completed	10/26/89	11/15/89	03/28/90	04/04/90	04/10/90	10/04/90

UCD-19 Through UCD-24

	UCD-19	UCD-20	UCD-21	UCD-22	UCD-23	UCD-24
Casing Type/ Diameter	PVC/10.2 cm (4 in.)					
Screen Type/ Slot Size	SS/0.25 mm (0.010 in.)	SS/0.25 mm (0.010 in.)	SS/0.51 mm (0.020 in.)	SS/0.25 mm (0.010 in.)	SS/0.25 mm (0.010 in.)	SS/0.25 mm (0.010 in.)
Slot Type	Wirewrap	Wirewrap	Wirewrap	Wirewrap	Wirewrap	Wirewrap
Screen Length	4.6 m (15 ft)					
Screen Interval bgs	17.5 - 22.1 m (57.5 - 72.5 ft)	17.5 - 22.1 m (57.5 - 72.5 ft)	18.1 - 22.7 m (59.5 - 74.5 ft)	17.4 - 22.0 m (57.0 - 72.0 ft)	17.2 - 21.6 m (56.5 - 71.5 ft)	17.4 - 22.0 m (57.0 - 72.0 ft)
Silt Trap	No	No	No	No	No	No
Filter Pack Type	Lone Star					
Mesh Sieve Size	16 - 40	16 - 40	16 - 40	16 - 40	16 - 40	16 - 40
Filter Pack Interval	16.3 - 22.1 m (53.5 - 72.5 ft)	16.5 - 22.4 m (54.0 - 73.5 ft)	16.5 - 22.4 m (54.0 - 73.5 ft)	16.5 - 22.1 m (54.0 - 72.5 ft)	16.3 - 22.0 m (53.5 - 72.0 ft)	16.5 - 22.0 m (54.0 - 72.0 ft)
Primary Seal	Grout	Grout	Grout	Grout	Grout	Grout
Secondary Seal	Bentonite	Bentonite	Bentonite	Bentonite	Bentonite	Bentonite
Surface Completion	Aboveground	Aboveground	Belowground	Belowground	Belowground	Belowground
Pump Type	Redi-Flo2	Redi-Flo2	Redi-Flo2	Redi-Flo2	Redi-Flo2	Redi-Flo2
HSU Unit and Depth of Casing	1st/22.1 m (72.5 ft)	1st/22.1 m (72.5 ft)	1st/22.7 m (74.5 ft)	1st/22.0 m (72.0 ft)	1st/21.8 m (71.5 ft)	1st/22.0 m (72.0 ft)
Date Completed	10/01/90	10/09/90	10/11/90	10/25/90	10/17/90	10/22/90

1.5 Contaminants of Concern in Groundwater

In March 1990, DOE assumed responsibility for the Phase II site characterization at LEHR. The purpose was to continue to support ongoing characterization and assessment of possible environmental impacts, remediation of soil and groundwater, and decontamination and decommissioning of buildings, as required at the LEHR site. The goal was to further characterize potential contaminant sources and evaluate the geologic and hydrologic relationships at the site. The design of monitoring wells and suitability of sample collection equipment were evaluated with respect to contaminants of concern at LEHR. Monitoring well designs and sample collection equipment were also evaluated with respect to suitability of the materials and design that would facilitate cost-effective collection of representative samples of groundwater contaminants.

Hazardous constituents, or indicators of potentially hazardous constituents related to past LEHR site operations, are divided into the following general categories: heavy metals, such as chromium, hexavalent chromium, barium, thallium, and selenium; anions, such as chloride, nitrate, phosphate, and sulfate; radionuclides, such as tritium, carbon-14, and strontium-90; and organics. The organic constituents of concern can be divided into volatile organic constituents (VOCs), such as 1,1-dichloroethane, 1,1-dichloroethene, 1,2-dichloroethane, methylene chloride, chloroform, benzene, and toluene; and semivolatile organic constituents, such as di-n-butylthalate, bis-phthalate, and diethylphthalate.

Table 1.2 summarizes the contaminants of concern and constituents of interest at LEHR. Most of these constituents were identified as possible contaminants of concern and were considered in the design of the groundwater sample collection system. Later sampling confirmed that new UCD wells were installed in areas where these contaminants were present at elevated levels above upgradient monitoring wells, or were confirmed by groundwater samples from Hydropunch™ samples.

Table 1.2. Contaminants of Concern and Constituents of Interest

Contamination Indicator Parameters:

Specific Conductance (field and lab)
pH (field and lab)
Temperature

Total Organic Halogen (TOH)
Total Organic Carbon (TOC)
Gross Beta

Groundwater Quality Parameters:

Chloride
Total Dissolved Solids
Potassium

Sulfate
Sodium
Nitrate

Inorganic Drinking Water Parameters:

Barium
Thallium
Chromium
Hexavalent Chromium

Selenium
Turbidity

Organic Drinking Water Parameters:

1,1-Dichloroethane
1,1-Dichloroethene
1,2-Dichloroethane
Chloroform
Di-n-butylthalate
Diethylphthalate

Methylene Chloride
Benzene
Toluene

Bis-phthalate

Radionuclides:

Tritium
Carbon-14
Strontium-90

2.0 Monitoring Well Construction and Development

2.1 Basis for Improved Well Design

High turbidity problems in Phase I, with sitewide assessment team (SWAT) monitoring wells that were screened in the first HSU and with large water level fluctuations during the year, necessitated design changes in the screened intervals of Phase II wells. The goal for the monitoring well design was one that would allow for hydrologic testing and reduce the turbidity to minimize the impact of sampling on the quality of the samples collected. In the previously installed monitoring wells, the turbidity exceeded regulatory levels for drinking water during the purging cycle and sometimes the sampling cycle. Available expertise and ASTM standards were used as the bases to design, construct, and develop the monitoring wells (ASTM 1990a and b; Nielsen 1991; Williams 1981). Literature was reviewed to identify people working in groundwater monitoring. Such people aided in identifying sampling pumps and their proper placement, and the deployment methods used to collect representative groundwater samples at LEHR.

2.2 Construction

The earlier wells installed in Phase I and for the SWAT were installed at shallower depths, particularly in the HSU-1 unit. To accommodate seasonal water level fluctuations, wells screened in the HSU-1 unit were installed slightly deeper than earlier wells. The HSU-2 wells in Phase I were completed to 27.3 m (90 ft) bgs with 4.6-m (15-ft) screens, whereas the Phase II wells installed in 1990 were redesigned to 36.4 m (120 ft) bgs with 7.6-m (25-ft) screens spanning more than 75 percent of the HSU-2 water-production zone. Screened interval depth was selected to allow sample collection during summer and fall when water levels were at their lowest. Long screened intervals allowed measurement of the hydraulic conduction and transmission characteristics of each unit.

2.2.1 Well Screen and Filter Pack Design

Before 1990, wells were typically constructed with slotted 5.1-cm (2-in.) diameter (for the Phase I wells) or 10-cm (4-in.) diameter PVC casing used as well screen and PVC casing (for the SWAT wells). The 10-cm (4-in.) diameter casing was selected for newer wells to allow for a greater number of hydraulic testing methods. In addition, the larger diameter casing permitted the use of a larger variety of pumps for development and sampling to facilitate well development with conventional

methods. It also made the access easier for tools to measure water level and for the placement of in situ instrumentation. To reduce turbidity and expedite development in both zones, Phase II monitoring wells were constructed of 10-cm (4-in.) diameter, 304 stainless steel, continuous wire-wrap screen (Bikis 1979; Clark and Turner 1983; Jackson 1983; Rinaldo-Lee 1983; Paul et al. 1988; Schalla and Walters 1989; Nielsen 1991). This 304 screen type has a larger open area than other types, even in the smaller slot sizes selected (Nielsen 1991). Slot size chosen for wells screened in HSU-1 was 0.0254 cm (0.010 in.) (called 10-slot); an appropriate filter pack Lonestar 1C sand (a 16-40 mesh gradation) was selected on the basis of recommendations set forth in consensus society standards and recognized publications (ASTM 1990a and b; Nielsen 1991; Schalla and Walters 1989). Wells screened in HSU-2 used 0.05-cm (0.020-in.) slot openings of 10-cm (4-in.) diameter, stainless steel, continuous wire-wrap screen with a number 2/12 filter pack sand (a 12-20 mesh gradation). Schedule 40 PVC casing, 10 cm (4 in.) in diameter, was used from the top of the screened interval to above the ground surface for all wells to reduce the well cost while retaining the desirable characteristics of stainless steel wire-wrap screen. Flush-threaded casing, conforming to ASTM F480-90, was used for all screen and casing. To avoid a stagnant zone, no sediment trap or silt trap was added to the bottom of the well (Nielsen 1991; Yu 1989).

2.2.2 Material/Contaminant Compatibility

During the 1980s, the environmental community expressed concerns that certain monitoring well materials might leach or adsorb contaminants to (or even absorb contaminants from) groundwater. Many studies were conducted under laboratory and field conditions. Several of these studies are referenced in Nielsen 1991. Although Phase II groundwater monitoring wells at the LEHR site were based on the recommended practice in ASTM D5092-90, they also comply generally with the primary federal guidance document (EPA 1986). The 1986 Technical Enforcement Guidance Document (TEGD) recommends that all well construction materials be composed of inert material, such as fluorocarbon resin or stainless steel. More research, published after issuance of that TEGD, showed that PVC was a superior or equal choice, depending on the constituents contained in the groundwater (Barcelona and Helfrich 1986; Barcelona et al. 1988; Dunbar et al. 1985; Gillham and Ohannesin 1990; Miller 1982; Nielsen 1991; Parker 1992).

Field studies at hazardous waste sites have shown that types 304 and 304L stainless steel wells may, for many months, leach chromium in quantities of 10 to 30 parts per billion (Smith 1988; Smith et al. 1989; Schalla et al. 1988a; Chamness et al. 1990). In these studies, groundwater types ranged from calcium or sodium-calcium/carbonate types to calcium sulfate types with pH values ranging from 6.9 to 8.2. In general, conditions at LEHR fall within these ranges. A study under laboratory conditions shows that type 304 stainless steel wire wrap leached chromium, while type

316 stainless steel wire wrap had a slight tendency to absorb chromium (Parker 1992). Based on this data, type 304 was selected for the well screen. It was decided it would be preferable to have a false positive for chromium reported with 304 stainless steel leaching than a false negative caused by adsorption on 316L stainless steel well screen. Certain radioisotopes are absorbed by 316L stainless steel, including strontium-85, cesium-137, and selenium-75 (Raber et al. 1983). However, no specific evidence showed that sorption would occur for the isotopes at LEHR. Other research shows that residence time in the short pathway through the well screen should not have any effect on the sample (Robin and Gillham 1987). The casing above the stainless steel screen was Schedule 40, flush-threaded PVC. Based on many studies of sorption and leaching tests, the sample bias effects due to adsorption or leaching with well casing materials, including PVC, are negligible (Barcelona et al. 1983; Reynolds and Gillham 1985). Therefore, PVC was chosen as the lowest cost casing material compared to other available materials (such as stainless steel, fluoropolymers, and epoxy-reinforced fiberglass). Neither PVC nor stainless steel was a concern with respect to the organic volatiles found at the site (Barcelona et al. 1983; Barcelona et al. 1988; Gillham and Ohannesin 1990; Parker 1992; Reynolds and Gillham 1985).

2.2.3 Completion Issues

To further prevent migration of fines from fine-grained layers of sediment above the first HSU-2 unit, and thereby reduce turbidity, well screen tops were kept approximately 70 cm (2 ft) below the top of the sand and gravel zone. However, to obtain flow from that 70-cm (2-ft) interval, while holding back fine-grained sediments in the formation above, the coarse filter pack extended 70 cm (2 ft) above the top of the well screen and a 91-cm (3-ft) layer of the Lonestar 1C sand was used as a secondary filter in accordance with ASTM D5092-90. The bentonite slurry and fine sand was used as a secondary seal between the cement/bentonite grout and the filter pack. In HSU-2 Wells UCD-15 and 16, a 152-cm (5-ft) thick layer of bentonite pellets was used in lieu of the secondary filter pack as a barrier to the Volclay bentonite grout. This process prevented invasion of the sand pack by the 2 to 5 percent bentonite/cement grout mixture that filled the space above the pellets to just below ground surface. For the same reason, in HSU-1 wells, 0.64-cm (0.25-in.) diameter bentonite pellets were added to a depth of 91 cm (3 ft) above the filter packs.

Installation was accomplished by drilling all HSU-1 wells with hollow stem auger drills and all of the HSU-2 wells with air rotary drills. These techniques were selected to minimize the alteration of hydraulic characteristics of the formation (Nielsen 1991; Schalla 1986). Screen and casing were lowered into the well and kept in tension during placement of filter pack and sealants in the annulus. Filter pack sand was continuously fed by a special funnel feed device mounted on the drill rig derrick

as the tremie was pulled back. Pellets and grouts were placed using tremies to prevent bridging of materials in the well annulus. These fillers also prevented the voids and casing damage associated with bridging.

Phase II monitoring wells (UCD-15 through UCD-20) were completed with an above-ground, locking steel, protective casing or were flush-ground, watertight, locking well boxes (UCD-21 through UCD-24). Installations flush with the ground were placed in high-traffic areas to prevent damage to the wells. The ground surface was sloped away from the wellhead to prevent downward migration of water from precipitation or runoff.

2.3 Development

During October and November of 1990, development occurred in two stages for each well. Development first began after placement of the filter pack, but before the placement of the annular sealants. Wells were swabbed or surged to help settle the filter pack and, as settling occurred, additional filter pack was added, as needed. This type of surging is very effective for settling the filter pack because of the high velocities created in the well (Schalla and Landick 1986; Paul et al. 1988; Sevee and Maher 1989). After construction, a combination of surging and cleaning using a bailer and subsequent pumping with a submersible pump at 3.8 to 26.5 L per min (1 to 7 gpm) continued for a few hours to reduce well turbidity by removing fine-grained materials from the formation (Schalla 1986; Winegardner 1990). Initial turbidities in the HSU-2 wells were above 200 nephelometric turbidity units (NTU) during the first 10 min of pumping and gradually declined to less than 15 NTU at the end of development. Similar successes in reducing turbidity occurred in the HSU-1 wells, although some were nearly 50 NTU after development; two were less than 5 NTU.

3.0 Pump Selection Process

3.1 Sampling Process Considerations

Groundwater sample collection from monitoring wells requires two basic activities, purging and sampling (sometimes referred to as cycles). Purging is the activity of removing stagnant water that is in the well casing and screen (and sometimes in the filter pack surrounding the well screen) that must be removed before sampling in order to obtain a representative sample from the water-bearing layers. Excluding wells with very high groundwater velocities, (such as 30.3 m or 100 ft per day), purging most monitoring wells throughout the entire screened interval is a necessity for the purpose of removing stagnant water. This process is necessary to obtain representative samples, as is well-established in the literature by hundreds of papers representing tens of thousands of samples for both organic and inorganic compounds. Sample collection (or sampling) is the removal of specified quantities of groundwater from the well (after purging) to obtain samples for analysis. The goal of purging and sampling is to obtain analyses of constituents that are representative of the formation groundwater composition at the well site. To minimize costs and equipment in the wells, a single device to perform both activities, rather than two separate devices, was the desired choice.

3.2 Categories of Sample Collection Devices

Three broad categories of sample collection devices are described in the literature (Pohlmann and Hess 1988; Nielsen and Yeates 1985; Anderson 1977; and Herzog et al. 1991). The three sample collection categories used for this report are 1) grab mechanisms, 2) suction lift mechanisms, and 3) variable discharge rate pumps.

Grab mechanisms, such as bailers and syringe pumps, simply deploy a sampling device to the sample interval, where it is passively or actively filled with water. Suction lift mechanisms include centrifugal and peristaltic pumps that pull the sample up to the surface by decreasing the head, or pressure, over the sample. The variable discharge rate pump category includes both variable displacement and positive displacement mechanisms (typically, all are called pumps) and consists of eight commonly used variable discharge rate pumps. These pumps include gas-lift devices, gas-drive (also called gas-displacement) devices, gas-operated bladder pumps (also called squeeze pumps or

diaphragm pumps), inertial lift pumps, electric (centrifugal) submersible pumps, gear-drive pumps, progressive cavity pumps (also called helical rotor pumps), and internal combustion-driven piston pumps.

3.3 Pump Performance Criteria

Purging and sampling activities have practical considerations, regardless of the sampling device or pump type used. Where appropriate, a discussion of these considerations, which form the criteria for sample pump evaluation and selection in this report, is presented with reference to a specific pump type in this section. This section includes a generic discussion of these issues related to any type of pump.

The practical considerations for purging and sampling, using one pump to perform both functions, were used as criteria in the selection process and belong in four categories that include:

1. proper deployment in well
 - ability to properly deploy pump intake in relation to geohydrologic conditions (such as depth to water or permeable layers)
 - adequate accessibility and deployment in relation to well construction and development (that is, inside casing diameter, screen length, slot size, screen type, or turbidity during purging)
2. physical performance capabilities
 - adequate lift and discharge capabilities
 - appropriate pump flow rate control and range
3. ability to obtain a representative sample
 - minimal alteration by pump construction materials
 - minimal alteration of sample chemistry caused by purging
 - minimal alteration of samples by pump operation during sampling cycle
4. efficiency
 - ease of field sampling operation
 - ease of cleaning during maintenance and before installation (not a criterion in this report)
 - the maintenance record (not a criterion in this report) reflecting reliability and durability of the sample collection pump.

The reasons for excluding types of sampling devices or pumps are presented in the following discussion of deployment.

3.3.1 Proper Deployment in Wells

Proper deployment of sampling devices in the monitoring wells requires an understanding of the hydrogeology, the layers that transport the contaminants of interest, and the vertical distribution of the contaminants. The placement of pumps in screened intervals may have greatly affected (order of magnitude) the concentration of contaminants and general water quality parameters during purging (Barcelona and Helfrich 1992; Schalla 1992). Even small-scale vertical variations in well-screen inflow rates and placement of pump intakes may have large effects on the capability to collect representative groundwater samples (Gibs et al. 1993). The lack of discrete sampling intervals and the determination of equivalence intervals can lead to erroneous results and conclusions (Barcelona and Helfrich 1992; Barcelona et al. 1994).

Although the wells at LEHR could be divided into two depth-to-water ranges of 18.2 to 21.2 m (60 to 70 ft) and 27.3 to 30.3 m (90 to 100 ft), an average depth of 27.3 m (90 ft) was used for discussion of the best-suited sample collection pumps. The depth-to-water measurement is important because it represents the hydraulic head and, therefore, the lift capability the collection pump must be able to exert to obtain samples from the greatest depth.

3.3.1.1 Candidate Selection Process

To simplify the evaluation process, the greatest anticipated depth the pump would be set was 27.3 m (90 ft). At this depth, many types of pumps would not be able to purge stagnant water from wells at reasonable rates or to obtain representative samples. Agitation or high flow rates in some wells screened in HSU-1 with geologic units rich in silt and clay may produce unacceptably high turbidity and suspended particles (that is, greater than 5 NTU) and result in unrealistically high levels of metals (Puls et al. 1992; Powell and Puls 1993). The inability of grab mechanisms (such as bailers) to obtain samples without causing high turbidity and unrepresentative samples, the possible damage to a sand pack stabilized during development, and the potential spread of contamination because of spillage during purging and sampling prohibited further consideration of these sample collection devices as suitable to accomplish both purging and sampling (Puls and Powell 1992; Barcelona and Helfrich 1992). Suction-lift mechanisms (centrifugal and peristaltic pumps) were precluded from further consideration because they can draw samples only from very shallow depths [such as, 7.6 m (25 ft)] and produce erroneous results when pulling the sample up to the surface by decreasing the pressure over the sample (Barcelona et al. 1984; Imbrigiotta et al. 1988; Puls and

Barcelona 1989a and b). Of the eight variable discharge pumps, two [the internal combustion (IC) pump and the gas-lift pump] are not suitable for most sampling applications because an interface exists between the drive gas and the water to be sampled. This situation causes a potential for loss of dissolved gases and volatile constituents across the interface, and for contamination to enter the sample water from the drive gas (Barcelona et al. 1985).

Therefore, based on reports in the literature and the proper deployment requirement, the first two categories of sampling devices, grab and suction-lift mechanisms, were eliminated from further consideration. Two of the variable discharge pump types were eliminated as sampling devices, but were considered with respect to the other criteria. The remaining six variable discharge rate pumps under discussion (centrifugal submersible pump, bladder pump, piston pump, progressive cavity pump, gear-driven pump, and inertial lift pump) and their operational characteristics, relevant to LEHR, are shown in Table 3.1.

Table 3.1. Operational Characteristics of Purging and Sampling Devices

	<u>Centrifugal Submersible Pump</u>	<u>Bladder Pump</u>	<u>Single-Acting Piston Pump</u>	<u>Helical Rotor Submersible Pump</u>	<u>Gear-Drive Submersible Pump</u>	<u>Inertial Lift Pump</u>
Approximate Diameter (inches)	1.81	1.5	1.7	1.75	1.75	0.75
Maximum Lift (feet)	270	1000	400	180	125	260
Maximum Design Flow rate (gpm)	9.0	3.5	5.0	1.2	1.4	4.0
Typical Flow Rate @ 90 ft L/min [Lift (gpm)]	29 (7.7 gpm)	5 (1.3 gpm)	18 (4.7 gpm)	3 (0.8 gpm)	1 (0.3 gpm)	10 (2.6 gpm)
Minimum Achievable Flow [Discharge rate (gpm)]	<0.026	<0.026	0.25	<0.026	<0.026	<0.026
Power Source	Electric	Pneumatic	Pneumatic/ Mechanical	Electric	Electric	Manual, Electric, or IC Engine

3.3.1.2 Site Specific Characteristics for Candidate Pumps

The accessibility and ease of pump deployment in monitoring wells at LEHR are practical limitations related to the inside diameter of well screen, screen length, slot size, and turbidity during purging. At a minimum, the pump must be small enough in diameter to fit inside the well screen and casing. Where needed, the pump should also allow enough clearance for water-level measurements and installation of subsurface monitoring devices. Hydraulic conductivities in both HSU units can sustain discharge rates of 5 gpm for properly constructed monitoring wells with sufficient screen length. Well construction would include Schedule 40 PVC casing and stainless steel well screen with diameters of 10 cm (4 in.). The volume contained in a given length of a 10-cm (4-in.) well is four times greater than that for a 5-cm (2-in.) well (Rinaldo-Lee 1983). Also, the entrance velocities at the well screen are inverse to the square of the well diameter, and higher purge rates are allowable in the larger 10-cm (4-in.) diameter wells. Therefore, the purge volumes are much larger in the wells with the larger diameter. The well screen diameter and length are important for determining well equivalent volumes of purge water to be removed from the screened interval (SC); the screened interval and the filter pack (SPSC); or the screened interval, the filter pack, and the volume of water in the casing above the screen (BV) (Barcelona et al. 1994; Schalla 1993).

The well screen diameter, length, and slot size or percentage of open area are important in determining the flow velocity in the slots and in the well during pumping which, in turn determines appropriate purging and sampling rates (Puls et al. 1992; Powell and Puls 1993; Barcelona et al. 1994). If approximately 1 L/min (0.26 gpm) is an appropriate purge rate for a 5-cm (2-in.) diameter, 152.4-cm (5-ft) long, 6.25-mm (0.010 in.) continuous wire wrap slot size, stainless steel casing in formations having hydraulic conductivities ranging from 10^{-2} to 10^{-3} cm/sec (Barcelona et al. 1994), then it also should be true that a 10.2-cm (4-in.) diameter screen should be purged at 4 L/min (1.04 gpm) for every 152.4 cm (5 ft) of screen. The wells in HSU-1 have 4.6-m (15-ft) screens and could be purged at up to 12 L/min (3.12 gpm). For larger screen slot sizes, such as 0.050 cm (0.020 in.) and correspondingly coarser filter packs in wells screened in HSU-2, it should be possible to double the purge rates [that is, to 8 L/min (2.08 gpm)] for each 1.5 m (5 ft) of screened interval, if the water-bearing units have hydraulic conductivities equal to or greater than 10^{-2} cm/sec (4×10^{-3} in./sec). The wells in HSU-2 have 7.5-m (25-ft) screens and can be purged at a rate up to 40 L/min (10.4 gpm).

3.3.1.3 Specific Deployment Issues

To reduce the time necessary to remove the required amount of purge water from a well, it is preferable to purge at as high a rate as possible without causing undesirable turbidity during purging

and sampling. This reduction in time also reduces effort, cost, and safety hazards. For the deeper HSU-2 wells that year round have at least a few feet of water in the casing above the screened interval, the wells should be purged (as a minimum requirement) with the pump intake located 3 to 5 well diameters above the screen to eliminate the need to dispose of large volumes of purge water and to reduce the amount of time required for purging. The placement of the pump at this location eliminates the need to purge the column of stagnant water located above the well screen. This statement is true, if at least 0.5 m (1.5 ft) of drawdown occurred or the pump was initially lifted 0.5 m (1.5 ft), then slowly lowered just prior to sampling (Barcelona et al. 1985; Robin and Gillham 1987; Barcelona and Helfrich 1992; Kearl et al. 1992; Schalla 1992; Unwin and Maltby 1988; Maltby and Unwin 1992). A primary consideration for all wells at the LEHR site is to ensure the isolation of the stagnant water above the well screen. During isolation, the purge rate should lower the stagnant water column to less than one foot. During subsequent phases, this purge volume was planned to be further reduced by displacement or isolation devices (Schalla 1992; Barcelona and Helfrich 1992; Maltby and Unwin 1992; Schalla 1993). The rate and the volume of stagnant water to be removed during purging influenced the decision regarding which pump was considered best suited for sampling under various design scenarios.

To obtain consistent and representative results, the ideal location of the pump intake for the shallower HSU-1 wells would be opposite the most permeable layer containing the highest concentration of contaminants of concern. In fact, the vertical distribution of permeability opposite the screened interval can be accurately and easily determined (Hall et al. 1991; Hall and Raymond 1992; Hall 1993). Setting the pump intake opposite the permeable zone or zones is not practical because vertical variations have not been studied adequately in each well. Also, seasonal water levels decline to such an extent that a few wells go dry and the primary permeable zones are no longer saturated (Robbins and Martin-Hayden 1991; Martin-Hayden et al. 1991).

3.3.1.4 Purging and Sampling Rate Issues

Although it may be true that certain zones exist within the subsurface where hydrogeology-based sampling would be advantageous (Gibs et al. 1993; Barcelona and Helfrich 1992; Gibs and Imbriotta 1990), such sampling has not been done. However, site experience and empirical data guided purging and sampling protocols. In general, wells should be pumped at rates that do not cause substantial drawdown from the mid-screen portion of a well and that efficiently remove a consistent number of purge volumes from each well prior to sampling (Barcelona et al. 1994). At the time of this evaluation, it was decided that a minimum number for all monitoring wells should be three to five equivalent volumes (that is, five SC for HSU-1 wells and three SC for HSU-2 wells), if indicator parameters [such as, turbidity, redox potential, pH, electrical conductivity, or dissolved

oxygen in-line (flow through), or actual contaminants of interest] have stabilized within approximately 10 percent over at least two measurements (Garske and Schock 1986; Gibs and Imbriogiotta 1990; Barcelona et al. 1994). Although 1.2 equivalent volumes is possible, it was not considered an identifiable lower limit for the LEHR site because of insufficient data. With isolation and displacement devices that minimize the volume of water above and below the pump, the volume of purge water can be reduced to less than 10 percent of the required amount without such devices (Schalla 1992). Considering the obvious problems associated with collecting, transporting, storing, and disposing of the contaminated purge water, the use of isolation and displacement devices may have seemed like a good idea (Puls et al. 1992; Powell and Puls 1993). However, isolation was not considered in the selection of pumps; therefore, the minimum volume to be removed from HSU-1 wells with 4.6 m (15 ft) of well screen is approximately 284 L (75 gal) each time the well is purged. In the case of HSU-2 wells with 7.6 m (25 ft) saturated, the minimum volume removed is about 758 L (200 gal). Therefore, it was desirable to have a pump that could purge about 190 L (50 gal) in as little as 10 min, requiring a discharge rate of 19 L/min or 5 gpm.

In addition, the collection procedures recommended at the time included operating pumps so the sampling flowrate did not pulsate, or exceed 300 ml/min (9 fl oz/min), during volatile constituent sampling. Flow rates used while sampling for other constants could be greater before sampling for volatile constituents has been completed. This limitation was set as a practical upper limit for filling a 40-ml (1.2-fl oz) volatile organic analyte (VOA) sample vial. The literature review indicated a recommended sampling of 100 ml/min (3 fl oz/min); therefore, this rate was used as the lower limit for the selection process (Barcelona et al. 1985; Barcelona et al. 1983).

Because of the selection of the pump and corresponding sampling and purge rates, it has been inferred the ideal purge rate should be less than 0.2 to 0.3 L/min (0.05 to 0.08 gpm), regardless of well design and configuration (Puls and Powell 1992; Puls and Barcelona 1989a and b). More recent literature indicates that if wells are properly constructed and developed, purge rates can be determined specific to hydrologic conditions and well construction, including well diameter and screen length (Barcelona and Helfrich 1992; Gibs et al. 1993; Barcelona et al. 1994). Most wells, if properly constructed to standards (ASTM D5092), even in silt-rich formations, can be purged at rates much higher than 0.3 L/min (0.08 gpm) without exceeding 5 NTU. Admittedly, some wells in certain formations will typically have higher turbidities, regardless of development, if the purging and sampling rate is high (Robin and Gillham 1987). The entrance velocity at the slots in the well screen will be a determining factor for the amount of turbidity; therefore, the length of screen, slot size (percentage of open area), sediment sump, and well diameter will be significant factors (Bikis 1979;

Clark and Turner 1983; Dunbar et al. 1985; Gillespie 1992; Jackson 1983; Kill 1989; Paul et al. 1988; Rinaldo-Lee 1983; Schalla 1986; Schalla and Walters 1989; Schalla and Landick 1986; Sevee and Maher 1989; EPA 1975; Winegardner 1990; Williams 1981; Yu 1989).

3.3.2 Physical Performance Capabilities

To achieve variation in purging and sampling rates that are necessary for the 10.2-cm (4-in.) diameter wells, the pump must be able to discharge water at the surface over an extensive range of flow rates while purging. In 10.2-cm (4-in.) diameter wells, the range of discharge flow rates at the surface needs to be from as little as 0.1 to 0.3 L/min (0.03 to 0.08 gpm) for sampling volatiles to 19 L/min (4.9 gpm) for purging. To achieve this end, pumps must have adequate lift and corresponding discharge capabilities to pump from a depth of approximately 27.3 m (90 ft). Discharge flow rates that span the range described are possible only with small diameter pumps at depths of 15.2 m (50 ft) or less (Nielsen and Yeates 1985; Pohlmann and Hess 1988). In small diameter pumps, the higher end of the discharge range typically is much less as the depth-to-water measurement increases.

3.3.3 Capability of Obtaining a Representative Sample

To obtain a representative sample, the pump construction material must be totally inert or inert to the extent that it will not significantly alter analyte concentrations as a result of loss from sorption, degradation, or chemical interaction with pump materials. The preferred materials were 300 series stainless steels (most commonly used types are 304 and 316L) and Teflon®, actually polytetrafluoroethylene (PTFE) (Barcelona et al. 1985; Barcelona et al. 1983; Barcelona et al. 1988). Sampling equipment may include discharge tubing that is Teflon-lined. Rigid PVC is acceptable, but flexible PVC is not (Barcelona et al. 1985). The suitable materials include rigid PVC, 300-series stainless steel, and Teflon for most organic and inorganic compounds (Barcelona et al. 1985; Barcelona et al. 1988; Miller 1982; Parker 1992; Pearsall and Eckhardt 1987; Pohlmann and Hess 1988). Studies have shown that if adequate purging is done and sampling follows immediately, the nature of the materials will have no significant impact on water chemistry (Robin and Gillham 1987).

If purge rates are too high, the possibility of altering sample chemistry caused by purging with positive displacement sample pumps has been suggested (Puls and Powell 1992; Puls et al. 1992; Puls and Barcelona 1989a and b). The possibility exists of some volatile loss from groundwater by some sampling devices, including a few positive displacement devices. However, most variable discharge pumps (such as variable displacement and positive displacement pumps) perform purging and sampling functions without evidence of volatile loss. This statement is supported by numerous reports of relevant research in the scientific literature (Barcelona 1985; Barcelona et al. 1988; Garske

and Schock 1986; Gass et al. 1991; Gibs and Imbrigiotta 1990; Gibs et al. 1993; Imbrigiotta et al. 1988; Knobel and Mann 1993; Liikala et al. 1988; Miller 1982; Muska et al. 1986; Panko and Barth 1988; Parker et al. 1993; Pearsall and Eckhardt 1987; Pohlmann and Hess 1988; Schalla et al. 1988b; Stolzenburg and Nichols 1985; Unwin 1984; Unwin and Maltby 1988).

Studies conducted by Gass et al. (1991) and Knobel and Mann (1993) concluded that low flow rate submersible centrifugal pumps can deliver representative groundwater samples. A study conducted by Paul and Puls (1992), comparing a low flow rate submersible centrifugal pump, a bladder pump, and a peristaltic pump, concluded the submersible centrifugal pump produced the fewest negative impacts when trying to obtain representative and reproducible groundwater samples at the particular site and wells investigated. Research performed by Yeskis et al. (1988) indicates that submersible impeller pumps perform similarly to bladder pumps when collecting samples for volatile organics analysis. Higher discharge rate submersible pumps also are capable of obtaining representative samples (Liikala et al. 1988; Muska et al. 1986).

3.3.4 Pump Efficiency

The efficiency of a device (that is, one that works better, faster, safer, and incurs fewer operational problems) is less easily quantified than the physical performance features. Therefore, descriptions of routine use, not first-time implementation, are discussed. Also, at the LEHR site, each sample collection pump is dedicated to a single well, which means the difficulties of installation or removal for maintenance and subsequent cleaning requires minimal discussion. Neither of these issues are considered as part of the criteria for this evaluation. The primary concern, relative to efficiency, is the ease of system operation in the field by the user, including two primary activities, purging and sampling.

3.4 Choice of Sampling Pump

Previously discussed limitations of other sampling devices (grab mechanisms and suction lift mechanisms) in this report (Section 3.3.1) caused their removal from further discussion because they are either not suitable for the purging and sampling performance range of interest or for the conditions that exist in the monitoring wells at the LEHR site. By eliminating these two categories of sampling devices and by specifying the approximate performance ranges used by the six pumps remaining to be evaluated, criteria were simplified. Furthermore, based on the evaluation considerations in Section 3.3, it is apparent that only four criteria are necessary to evaluate the relative merits of

the remaining six variable discharge rate pumps: bladder pumps, inertial lift pumps, centrifugal submersible pumps, gear-driven pumps, progressive cavity pumps, and internal combustion pumps. (Refer to Table 3.1.)

Proper deployment of the pump intake in relation to hydrogeologic conditions (that is, depth to water) and the well screen apparently could be accommodated by any one of the six pumps, if it has the ability to discharge water at the surface at rates specified for physical performance. For the purging cycle, issues related to inside diameter, screen length, slot size, and percentage of open area are collectively discussed, using the suggested upper physical performance capability to eliminate significant turbidity and ensure the representativeness of samples taken from the well. Based on the literature, all six pumps have the capability to obtain a representative sample and have pump construction materials that do not alter the samples during purging or sampling cycles. Therefore, chemical considerations were removed from final consideration. All of the pumps could be installed in 10-cm (4-in.) diameter wells with adequate clearance to allow for in situ monitoring devices or manual measurements. Thus, the questions that remained for the evaluation were:

1. Could the pump discharge water at the surface at rates from as low as 0.1 L/min (0.026 gpm) or sampling up to 19 L/min (4.94 gpm) for purging?
2. Is the pump easy to use for purging and sampling (that is, how is it better at controlling flow rates, faster [up to the limits required], or safer to use)? For example, how easily can discharge flow rates be controlled?

Based on the literature review, only one sample collection pump fully met the requirements to satisfy the desired purge performance range, even though several pumps could obtain representative groundwater samples consistently and reliably. This sample collection pump, a variable frequency submersible pump, had recently become available by Grundfos. The commercial unit available today is called the Grundfos MP1 Redi-Flo2™. The units used at the site were precursors (actually beta units) and simply called Grundfos MP1 pumps.

Although most of the six pumps are easy to use, this submersible pump was the easiest. For an electrically powered system, the low-discharge centrifugal submersible pump was very easy to control because hookups to power and the control box are simple and take only seconds to complete. Because this system provides a continuous stream of water, filling sampling bottles is quite easy. Adjusting the flow rate is almost as easy as operating a water faucet. In addition, at the DOE Hanford Site in Washington, a power monitor is connected for the Ground-Water Surveillance Program during

sample collection. This system is recent and more complex, but it increases the safety factor for operating electrical devices near water. For the procedures used at LEHR and the ease of access to all wells, the power monitor unit was not thought necessary.

4.0 Performance of Monitoring Wells, Pumps, and Accessories

The technical performance of monitoring wells, pumps, and accessories is discussed separately in the following sections; however, the performance is actually a composite of all components. If the monitoring wells are not properly designed, constructed and developed, it does not make any difference what type of sampling pump was chosen. With improper well design, the groundwater samples would be turbid and not representative of groundwater chemistry; sampling would be difficult, or impossible, for most constituents. Also, frequent maintenance of the well would be required to remove the buildup of fines and possibly biological growth in the well screens. If a less efficient pump or sampling device is chosen, cost of contaminant spillage on the ground or personnel increases sampling costs and reduces efficiency. Installation and operational costs could be higher for systems less easy to install, maintain, and use. The enhanced groundwater sample collection system includes all of the improved components.

4.1 Monitoring Well Performance

As expected, monitoring wells performed very well. Unlike earlier wells that frequently had turbidities in excess of 200 NTU, these new monitoring wells consistently had turbidities below 5 NTU during sampling and usually during purging. The exceptions during purging were short periods in two HSU-1 wells when the turbidity would occasionally reach approximately 50 to 90 NTU for about 20 to 30 sec near the start of the purging cycle. Perhaps the best evidence for success of the new well designs is the turbidity that is currently observed during the sampling cycles. For example, in the May 1993 quarterly sampling at LEHR, the older UCD wells (such as, UCD-07 to UCD-14), which are sampled with bladder or submersible pumps, had turbidities ranging from 1.55 to 3.77 NTU and averaging 2.46 NTU. In contrast, turbidities in the newly designed wells (such as, UCD-15 to UCD-23), which are sampled with variable frequency submersible pumps, ranged from 0.14 to 2.39 NTU and averaged 0.58 NTU. With the exception of one well, all turbidity values in the new wells were less than 1.0 NTU. In other quarterly samplings, the values may average somewhat higher, but the proportions are roughly the same. The older wells have turbidities averaging 5 to 10 times as high as the newer wells, probably because the older wells were not constructed with wire-wrap well screen, have too coarse a filter pack and slot size for the HSU-1, and may not have been adequately developed during and following construction.

For a period of time, water would accumulate in the above- and below-ground protective housings in the annulus between the PVC and the outer steel casing. After the fittings on the pump discharge lines were adjusted to prevent leakage, only one leakage issue remained. This issue was the possibility of accumulation of water in Christy boxes in below-ground wells or in an annulus between the PVC and steel casings caused by the leaking hose fitting. On January 22, 1991, the above-ground housings did not have a weep hole in the protective steel casing, as recommended in ASTM D5092-90 and other recognized documents for proper monitoring well design (Nielsen 1991). These weep holes were to have been drilled into the steel casing to allow fluids to drain from the annulus of the above-ground wells. Water had accumulated in the annulus of Well UCD-19, which may have occurred during the initial sampling of the well, when it was bailed, or during development. An alternative to weep holes is the improvement of the surface fittings on the discharge lines. This alternative was chosen to prevent accumulation of water in the annulus between the PVC and the outer steel casing,

The below-ground completions had special needs. Either the PVC casing threads had to be left in place to allow for a flush-threaded seal or another type of seal to prevent introduction of surface contamination into the well bore. The difficulty and expense of obtaining casings of different short lengths to construct the well on top with a threaded connection resulted in an agreement that Christy boxes could serve as the sole hydraulic barrier. The issue was finally resolved by agreeing that flush-mounted, water-tight, locking well boxes will be installed in positive grout mounts in high traffic areas. Initially, none of the Christy boxes had gaskets or O-rings on the lid or lockdown bolts to prevent water from entering the Christy boxes through these gaps. To prevent surface water contamination, manhole covers and bolts at the site were provided with sufficiently leak resistant gaskets. In addition, special surface seal systems, called Dedicators, were later put on the PVC casing when the pumps and access ports were installed. These seals on the PVC casing are discussed in detail in the next section.

4.2 Performance of Submersible Pump and Accessories

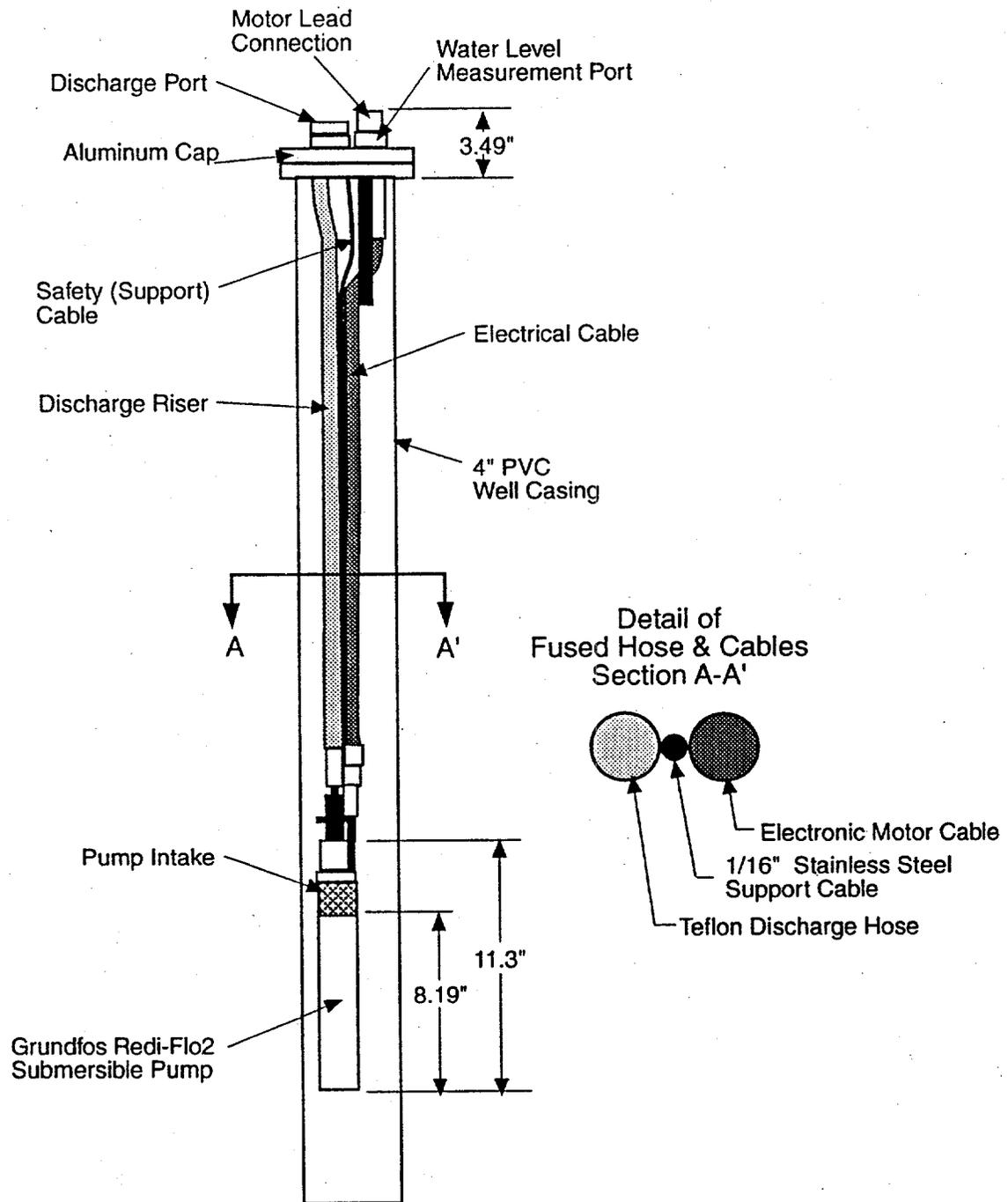
On November 8, 1990, the Redi-Flo2 Pump Model No. MP1 was installed in 3 deep wells of the 10 new wells at the site. On January 22, 1991, the same model of pump was installed on the seven remaining shallow wells. The purging/sampling pumps are 4.6 cm (1.82 in.) outside diameter, 13-in. long, stainless steel mini-submersible pumps with a 4-wire motor lead and 0.625-in. outside diameter all Teflon® discharge riser tubes. The pump uses a single-phase converter 230V input that varies the voltage from 46 to 400 hertz. This variable speed motor allows discharge rate from approximately 50 ml/min (1.5 fl oz/min) to 25,000 ml/min (750 fl oz/min). The surface seal and

pump support system consisted of a homemade cap made of PVC that did not form an airtight seal with the well. The cap also protruded nearly a foot above the top of the well. Later in August 1992, the wells were retrofitted with two accessory systems called Dedicator and Happy Hose to correct the problems described in the following paragraphs.

Initially, the system worked as planned with the exception of the following problems. These difficulties included leakage of the discharge fittings on the Grundfos pumps and the concomitant problem of water accumulation in the annulus between the PVC well casing and the protective steel housing.

The discharge hose fittings on the top cap surface seal or PVC header cap leaked. When the discharge extension hoses that extend from the top of the PVC header cap were originally installed with larger diameter, less flexible Teflon hoses, they did not leak during field discharge tests. However, these hoses could not be coiled up inside the protective steel casing or Christy boxes because of their diameter and lack of flexibility. These discharge hoses were replaced with smaller and more flexible polyethylene tubing. In February, a representative from Grundfos replaced these surface discharge hoses with reducer swage fittings and a 1.3-cm (0.5-in.) outside diameter, Teflon-lined, polypropylene tubing. These new 1.82-m (6-ft) long discharge hoses could be coiled up and stored in the protective housings, thus eliminating the inconvenience and safety concerns associated with disconnecting, transporting, and storing the larger diameter hoses. Apparently, the fittings in the new hoses were not tightened sufficiently or properly. The Grundfos installer indicated that a clearance of 10.2 cm (4.0 in.) between the steel cap of the protective housing and the top of the PVC in Well UCD-17 was insufficient to effectively coil up 1.82 m (6 ft) of discharge hose inside the protective housing. The installer cut off about 12.7 to 15.2 cm (5 to 6 in.) of PVC, using the internal pipe cutter, at a visit to the site in March 1991 to repair the leakage of the discharge fittings on the Grundfos pumps. Following repair of each of the discharge fittings, it was necessary to test the fitting to determine if the leakage had stopped. To do this required pumping at the maximum discharge rate of each pump for approximately 1 min while discharging a total of approximately 19 L (5 gal) of water. This effort proved to be a short-term solution because it was still difficult to store the long hoses in the spaces available.

The solution to this problem was equipment, known as the Dedicator, which consists of a surface well seal with quick connect multiport connections, an access port with a fused riser, a support cable, and a motor lead connected to the pump shown in Figure 4.1. In June 1992, when these new systems were added, it was discovered that one Redi-Flo2 pump needed replacement because of declining performance. Also, nine properly functioning Redi-Flo2 pumps were to be retrofitted with the new



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Figure 4.1. Purging and Sampling System

seal/discharge/access system, called Dedicator, shown in Figure 4.1 and in detail in Figure 4.2. The enhancements in June 1992 were to address issues expressed by staff of Dames and Moore, the site assessment subcontractor. Staff mentioned the Grundfos pumps should be removed and examined to determine if biofouling or other deterioration of the pumps was present. They also suggested replacing one of the pumps in the UCD-22 monitoring well that had shown a steady deterioration in performance. The representative also noticed the surface discharge risers needed replacement because they were breaking and leaking as a result of coiling them inside the steel housing. The scope of work included:

1. Remove and examine the existing pumps, hoses, and seals on August 19 and 20, 1992, at the LEHR facility, University of California, Davis, California.
2. Install a replacement pump for the pump that had shown declining performance in well UCD-22.
3. Replace the existing seals, hoses, and cables on 10 wells (UCD-15 through UCD-24) on August 19 and 20, 1992. Retrofit existing pumps with new assemblies of surface seal, motor lead, support cable, discharge hose (Teflon-lined polyethylene), and surface discharge riser. The discharge hose attached to the bottom of the seal had a single-fused cable and hose line that contained the 1.27-cm (0.5-in.) diameter discharge hose, a stainless steel support cable [180-kg (400-lb) test], and the motor lead (an electrical cable supplying power to the pump). (Actual replacement took place on August 31 and September 1 and 2, 1992.)

The Dedicator surface seal has a multiple access port system with the following features: a leak-proof up to 13,790 pascals (Pa) (2 psi) seal on the PVC well casing, which serves as a surface seal; a capped leakproof access port for water-level measurements or other sensors; the 1.8-m (6-ft) long discharge riser hose extensions used during purging and sampling and the storage port for them; and attachment of the fused motor lead, discharge riser, and stainless steel support cable to the pumps and surface seal.

The Dedicator has several advantages that include: 1) no leakage from the ground surface into below-ground completions past the waterproof seal, 2) the surface discharge hoses are quick connects and can be stored in the well casing when not in use, 3) all access ports are secured by cables or chains so they cannot accidentally fall into crevices or recesses of the outer housing and get lost or contaminated, 4) all wells are labeled with their proper well number so that surface seals can be easily identified during service or removal activities, and 5) the continuously sealed surface of the hose results in less contamination.

The first system of tubing and electrical cable was replaced with a product called Happy Hose. Happy Hose is a Teflon-lined polyethylene discharge riser hose that is fused with a supporting stainless steel cable, in addition to a shielded and sealed electrical cable. The advantages of the Happy Hose over the previous system that make it faster, cheaper, and safer include: 1) quick and easy

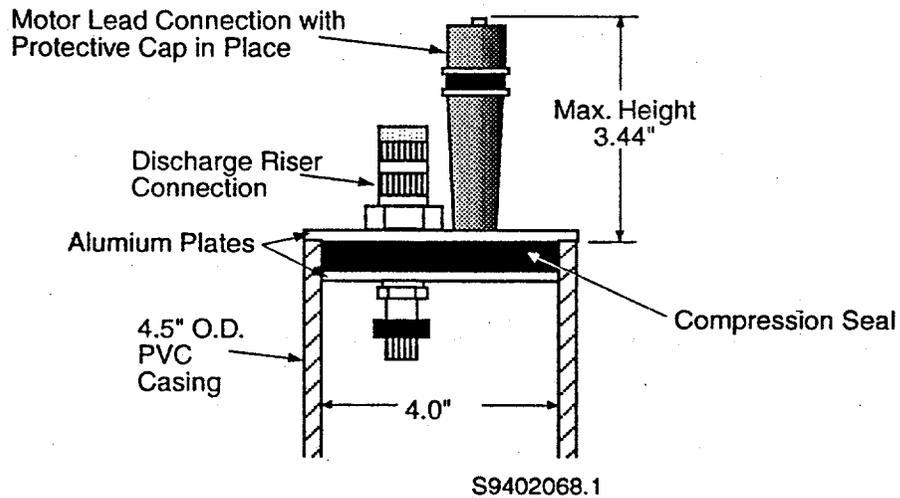
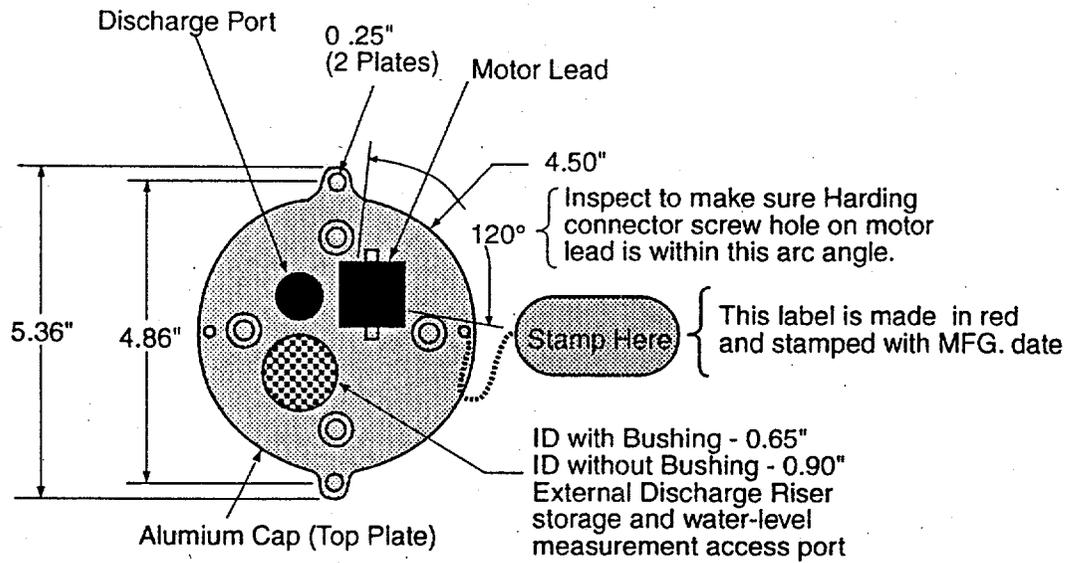


Figure 4.2. Details of Dedicator System

installation, decontamination, and removal because no kinking or tangling of the three lines occurs during installation and no place is found to trap contamination, 2) safer because it is nearly impossible for entanglement with the cables or tapes of water-level measurement devices or chemical sensors during their insertion and withdrawal, 3) safer and cheaper because the security cable built into the electrical cable reduces the chance of the pump pulling loose and falling to the bottom of the well or

of the hose or electrical connections being pulled apart during installation and removal of the pump or other systems in the well. Previously, no steel support cables were used for supporting installed equipment, such as sampling pumps, in any of the wells at LEHR.

To ensure representative sampling by selecting optimal placement of the pump depth, the following factors were considered: the seasonal changes in water levels, the hydrostratigraphy based on well logs, and the stagnant water intervals present in all wells. By considering these factors, the amount of purge water could be reduced to obtain a representative sample. The following lengths from the top of the PVC casing to the bottom of the Redi-Flo2 pumps were used:

UCD-15: 27.9 m (92 ft)	UCD-20: 21.2 m (70 ft)
UCD-16: 28.2 m (93 ft)	UCD-21: 21.2 m (70 ft)
UCD-17: 27.3 m (90 ft)	UCD-22: 21.2 m (70 ft)
UCD-18: 20.3 m (67 ft)	UCD-23: 21.2 m (70 ft)
UCD-19: 21.8 m (72 ft)	UCD-24: 21.2 m (70 ft)

The resulting depths of installation and location of pump intake in relation to screened interval and lowest water levels are shown in Table 4.1. Recommendations were made to the manufacturer

Table 4.1. Well Construction Information and Pump Depths at LEHR (August 1992)

Well Name	Screened Interval BGS (ft)	PVC Casing Above (+) or BGS (-) (ft)	Height of Top of PVC Pipe Elevation (ft)	Lowest Water Level Depth BGS (ft)	Pump Intake Depth Below Top of PVC (ft)(a)	Pump Intake Depth Below BGS (ft)(a)
UCD-15	116.0 - 91.0	+1.6	50.94	70.94	91.3	89.7
UCD-16	116.5 - 91.5	+1.0	49.18	69.18	92.3	91.3
UCD-17	113.0 - 88.0	+1.7	51.48	70.48	89.3	87.6
UCD-18	70.9 - 55.9	+0.9	47.75	64.75	66.3	65.4
UCD-19	72.5 - 57.5	+1.2	50.49	70.49	71.3	70.1
UCD-20	72.5 - 57.5	+1.0	48.94	68.94	69.3	68.3
UCD-21	74.5 - 59.5	-0.7	48.00	67.00	69.3	70.0
UCD-22	72.0 - 57.0	-0.6	48.36	68.36	69.3	69.9
UCD-23	71.5 - 56.5	-0.6	48.57	67.57	69.3	69.9
UCD-24	72.0 - 57.0	-0.6	48.16	68.16	69.3	69.9

Note: All deep wells have 7.6 m (25 ft) of 304 stainless steel screen. All shallow wells have 13.7 m (15 ft) of 304 stainless steel screen.

BGS = Below Ground Surface.

(a) Bottom of pump is approximately 0.21 m (0.7 ft) below the pump intake.

(Instrumentation Northwest, Inc.) to improve the Deducator. These recommendations were incorporated into the next version of Deducator systems installed at LEHR. Manufacturers of the system were informed of the following PNL recommendations:

- The tops of PVC casing must be cut level.
- The inside diameter of water level measurement access port should be enlarged.
- The bushing should allow for storage of the discharge hose in a separate port.
- All fittings and connectors should have coarser threads with fewer threads per inch for easier, quicker connections and to eliminate cross threading.
- Deducator should not slip over but slip inside and rest on the top edge of the PVC for minimal clearance and to eliminate problems of sealing.
- If male-threaded end was on the PVC casing, a compression system was used to provide a 34,475-Pa (5-psi) seal, or a sliced thread to release built up pressure in the well during removal of the access port caps.
- The system should be factory built or retrofitted. Retrofitting of the new hose in the field and dedicator system took nearly 40 min for each of the 9 wells. (In contrast, the installation of the factory-assembled unit in well UCD-22 took about 1 min to install.)

5.0 Cost Evaluations

Monitoring well costs are exclusively capital costs, but cost savings occur during development and the operational phase of the pump portion of the system. Even though capital costs were not an issue at the time of initial installation of the pumps and accessories (discharge hoses, electrical and support cables), because they were provided free-of-charge for demonstration purposes, some capital costs of the sampling pumps and the retrofitted sampling pumps are discussed, in addition to the operational costs of the system.

5.1 Monitoring Well Costs

The 10 new monitoring wells were constructed with stainless steel wire-wrap well screen to expedite development, minimize turbidity, and maximize the percentage of open area in the screened interval. The cost of stainless steel for three deep and seven shallow wells is shown in Table 5.1. The total additional cost of the stainless steel casing, above PVC slotted casing was \$6462. Most of this cost was justified by reduced development time, and by long-term reduction of turbidity to meet more stringent regulatory requirements for groundwater samples. Additional advantages of stainless steel over both types of PVC screens include superior strength, and negligible risk of damage during

Table 5.1. Cost Comparison of Screen Alternatives in 10-Cm (4-In.) Diameter Wells

<u>Unit Description and Dimension</u>	<u>304 Stainless Steel Wire-Wrap Screen (\$)</u>	<u>PVC Wire-Wrap Well Screen (\$)</u>	<u>PVC Slotted Casing (\$)</u>
Cost per Foot	41.70	18.30	5.80
Cost per Deep Well for 25 ft	1042.50	457.50	145.00
Cost per Shallow Well for 15 ft	625.50	274.50	87.00
Cost of 3 Deep Wells	3127.50	1372.50	435.00
Cost of 7 Shallow Wells	4378.50	1921.50	609.00
Total Cost of 10 Screens	7506.00	3294.00	1044.00
Additional Cost Above PVC Slotted Casing	6462.00	2250.00	None

installation and development because of high collapse and column strength of the stainless steel screen. Relative to the cost of construction and development of the 10 wells, the additional cost of the stainless steel wire-wrap well screen represents less than 3 percent of additional cost to well construction. Reduction of well development time at \$150 per hour for 40 hours per 10 wells may account for most of the \$6462, but operational cost savings resulting from lower turbidity samples are difficult to assess.

5.2 Costs of Pump and Accessories

A total of 10 new Redi-Flo2 purge and sample pumps, manufactured by Grundfos, with 30.3-m (100-ft) motor leads and 1.27-cm (0.5-in.) risers, were installed in the new monitoring wells at LEHR. This pump model represents new technology for purging and sampling monitoring wells. The pump [about 33 cm (13 in.) long] and its associated components are constructed of materials recommended for sampling hazardous waste compounds from monitoring wells. The pump has a single-phase, converter 230 V input and varies the voltage frequency from 46 to 400 hertz. Thus, a variable speed and variable performance range of 26.5 L per min (7 gpm) during well purging to 100 ml (3 fl oz) per minute during sampling are possible. Discharge rates may be easily varied by adjusting a single control dial. The 4.62-cm (1.82-in.) outside diameter of the pump allows generous clearances for water-level measurement devices and instrumentation. This improvement has not been possible with other commercial submersible pumps in 10.2-cm (4-in.) diameter monitoring wells. Only one other sampling pump on the market, the Hydrostar™, has the performance range needed at LEHR for both sampling and purging. As shown in Table 5.2, the Hydrostar is more costly to install than the Grundfos Redi-Flo2.

Table 5.2. Comparison of Three Variable Discharge Pumps

<u>Parameter</u>	<u>Original Bladder Pump</u>	<u>Hydrostar Piston Pump</u>	<u>Redi-Flo2 Submersible Pump</u>
Installation Cost per Well	\$ 650	\$ 1320	\$ 900
Total Installation Cost	\$6500	\$13,200	\$9000
Purge Rate (L/min)	3.79	17.8	26.5
Sampling Rate (ml/min)	100	100	100
Field Sampling Efficiency	Fair	Fair	Good
Ease of Operation	Fair	Fair	Good
Reliability	Good	Good	Good
Suitability for Sampling VOC	Good	Good	Good
Ease of Installation	Good	Poor	Good

Note: Total cost is based on 10 wells, not including costs of controllers and surface seals (Dedicators).

Bladder pumps are the most commonly used purge and sampling pumps in the industry and for most installations typically cost 20 to 25 percent less (approximately \$250 each at LEHR) than the Redi-Flo2, but lack the advantages for labor saving during purging because bladder pumps of comparable size only purge at a maximum of about 3.79 L/min (1.0 gpm) for conditions at the UC Davis project. Approximately 284 to 758 L (75 to 200 gal) of water are purged from each 10.2-cm (4-in.) diameter monitoring well prior to slowing the discharge rate for sampling. At a 3.79 L/min (1.0 gpm) purge rate with a bladder pump, purging 284 L (75 gal) would take approximately 75 min, but Redi-Flo2 purging at 26.5 L/min (7 gpm) requires only 10 min. The time saved per well is 65 min for each of the seven shallow wells. For the three deep wells, the savings is even greater because the volume of 758 L (200 gal) can be purged in 29 min or a savings of 171 min, almost 3 hr. For the 10 wells at LEHR using these pumps, 16 hr of labor are saved each quarterly sampling. The ease of use of this pump probably saves an additional 1 hr or so of sampling time per quarter. However, that savings is not included in the calculations presented here because documentation consists of anecdotal information rather than observed results. At a fully burdened charge-out rate of \$75 per hr, this is a labor savings of \$1200 every quarter, or \$4800 annually. The additional cost of 10 Redi-Flo2 pumps is approximately \$2500, which is approximately equal to the savings achieved during the first two quarters of sampling. This 6-month time frame to amortize the costs is similar to, but shorter than, the 1- to 2-yr time frame at other sites (Parker et al. 1993). Cost of controllers and the surface seal (Dedicator) system was common to all pumping systems and was not added to their cost. The Dedicator surface well seal completion system is discussed in the following paragraphs.

The equipment known as the Dedicator consists of 10 surface well seals with quick connect multi-port connections and access port, and an average 24.2-m (80-ft) length of Happy Hose (a fused riser, support cable, and motor lead) for each of the 10 wells. These new systems cost \$640 for each well or a total of \$6400. The labor cost to install them is approximately \$1600. If all the wells had been factory-assembled, installation time would have been an average of 10 min for each of the 10 wells, not including driving time from well to well. Therefore, had they been assembled at the factory, the installation costs would have been reduced to about \$200. The total cost of adding these features was about \$8000. The quick connects on the Dedicator reduce setup and disconnect time while ensuring isolation from surface contaminants. The savings in operation costs per quarterly sampling is about 2 hr for 10 wells. At a fully burdened charge-out rate of \$75 per hr, the savings equals the modest sum of \$150 per quarter or \$600 per yr. It would require 10 yr of these cost savings to equal the additional cost of the Dedicator. However, other less easily quantifiable, but important, operational benefits are provided by ensuring sample integrity. The Dedicator ensures sample integrity because it eliminates entry of external contaminants and prevents surface spillage of contaminated water. It appears, based on repeated examination over 3 yr, the Happy Hose component will remain unfouled over years of use at LEHR.

6.0 Summary and Conclusions

The monitoring well portion of the enhanced groundwater collection system provided substantial improvement in the reduction of turbidity over previous designs of wells at the site. Dedicated groundwater sampling pumps were installed at LEHR at UC Davis to achieve cost savings and improved quality of the samples. The accessory items, Dedicator and Happy Hose, were added to improve ease of use, to improve safety, to ensure sample integrity from external influences, and to avoid future difficulties associated with degradation of the systems or obstructions to water level measurement and other instrumentation. The cost savings from the new well design that ensure vertical hydraulic isolation and reduce water sample turbidity is difficult to assess; however, at a minimum, the additional material costs were offset by the reduced development time. The long-term net cost savings of the pump portion of the groundwater sample collection system began in the summer of 1992, resulting in a net cost savings of at least \$4800 per year on these first 10 wells. Additional cost savings will be achieved as these pumps are added to other groundwater sampling wells on-site. Already the site uses 23 of these pumps. The monitoring well network is estimated to increase to 35 wells by 1995 for a total additional capital cost of \$8250. The annual cost savings will amount to \$16,800 or a net operational cost savings over 5 yr of \$75,750. Although quantifiable operational cost savings of the Dedicator and Happy Hose accessories contribute to the minor ease-of-use cost savings, their value added also lies in safety, the potential reduction of biofouling, and the assurance that well integrity is not compromised by introduction of foreign substances. The net additional cost of about \$3000 can be considered money well-spent, if it prevents even one well from being contaminated with external fluids and particulates over the next 5 yr.

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