

1 of 2

STATE WASTE DISCHARGE PERMIT APPLICATION
FOR THE 200 AREA EFFLUENT TREATMENT FACILITY
AND THE STATE-APPROVED LAND DISPOSAL SITE

Prepared for:

U.S. Department of Energy
P.O. Box 550
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Prepared by:

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and

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WHC Contract No. MLW-SVV-073750, Task Order S-93-26
SAIC Project No. 01-1011-03-4546

August 1993

MASTER *AS*

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STATE WASTE DISCHARGE PERMIT APPLICATION FOR INDUSTRIAL DISCHARGES TO LAND

For Office Use Only

Date Application Received _____	Date Fee Paid _____	Application/Permit No. _____
Date Application Accepted _____		Facility No. _____
Temporary Permit Effective Date _____		Temporary Permit Expiration Date _____

This application is for a waste discharge permit as required in accordance with provisions of Chapter 90.48 RCW and Chapter 173-216 WAC. Additional information may be required. Information previously submitted and applicable to this application should be referenced in the appropriate section.

SECTION A. GENERAL INFORMATION

1. Company Name:	U.S. Department of Energy		
2. Mailing Address:	Richland Operations Office		
	P.O. Box 1970		
	Street		
	Richland, Washington	99352	
	City/State		Zip
3. Facility Address:	200 East Area and 200 West Area		
	Street		
	Richland, Washington	99352	
	City/State		Zip
4. Person to contact who is familiar with the information contained in this application:			
	James E. Rasmussen	U.S. DOE, Staff Chief, Regulatory Permits	(509) 376-2247
	Name	Title	Telephone
5. Check One:	<input type="checkbox"/> Existing Discharge <input checked="" type="checkbox"/> Proposed Discharge Anticipated, date of _____ <u>October, 1994</u>		

I certify under penalty of law that this document and all attachments were prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gather and evaluate the information submitted. Based on my inquiry of the person or persons who manage the system, or those persons directly responsible for gathering the information, the information submitted is, to the best of my knowledge and belief, true, accurate, and complete. I am aware that there are significant penalties for submitting false information, including the possibility of a fine and/or imprisonment for knowing violations.

 Signature*	<u>8/25/93</u> Date	<u>Manager, Richland Operations Office</u> Title <u>John D. Wagoner</u> Printed Name
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Seal if applicable

*Applications must be signed by either the owner, the principal executive officer or a duly authorized representative.

SECTION B. PRODUCT OR SERVICE INFORMATION

- Briefly describe all manufacturing processes and products, and/or service activities. Provide the applicable Standard Industrial Classification (SIC) Code(s) for each activity.

SIC No(s): 9999

Description: See Attachment A. No existing manufacturing processes produce waste. The production of nuclear materials at the Hanford Site generated wastes over the past 50 years during the site's defense mission. The 200 Area Effluent Treatment Facility will initially provide treatment of the 242-A Evaporator Process Condensate which is key to the current Hanford Site mission of waste management and environmental restoration and remediation. Attachment A describes the pretreatment of the wastes in the 242-A Evaporator and contains a description of the waste water.

Attachment B provides a description of ETF treatment processes.

- Include a production schematic flow diagram of the process and service activities described above on a separate sheet.
See Attachment A, Figure A-2 and Figure A-3.
- List raw materials and products: The 242-Evaporator Process Condensate and the waste water stored in the Liquid Effluent Retention Facility will be the initial sources of the waste water treated at the ETF. Raw materials used at the ETF are listed in the table below. Quantities reflect the nominal storage capacity of the storage tanks.

RAW MATERIALS	
Type	Quantity
92% H ₂ SO ₄	7,500 gallons
50% NaOH	5,000 gallons
Hydrogen Peroxide	2,500 gallons
Cleaning Solution in Distillate Flush Tank Flush	To Be Determined
PRODUCTS	
The 200 Area ETF initially will receive process condensate from the 242-A Evaporator and the Liquid Effluent Retention Facility (LERF). The only raw materials used in the ETF process are hydrogen peroxide and concentrated and dilute solutions of sodium hydroxide and sulfuric acid. The finished "products" of the treatment plant are treated waste water and cooling tower blowdown to be disposed of at the State-Approved Land Disposal Site (SALDS), and a concentrated dry powder consisting primarily of ammonium sulfate and sodium sulfate.	

SECTION C. PLANT OPERATIONAL CHARACTERISTICS

1. Identify the waste stream for each of the production processes or activities described in Section B.1. Assign an identification number.

Process	Waste Stream Name	Batch or Continuous Process	Waste Stream ID #
Effluent Treatment Facility (ETF)	Process condensate stored in the Liquid Effluent Retention Facility (LERF)	Continuous	1
	Process condensate from the 242-A Evaporator	Continuous	2
	ETF cooling tower blowdown (combined with ETF treated waste water downstream of verification tanks and disposed at the SALDS)	Continuous	3
Other Hanford Areas	Other aqueous wastes to be treated if effluent meets discharge limits	Batch or Continuous	4

2. On a separate sheet, describe in detail the treatment and disposal of all waste waters as described above. Include a schematic flow diagram for all waste water treatment and disposal systems. See Attachment B, Section 2.0 for a description of the waste water treatment at ETF and Section 2.12 for a description of the ETF cooling tower unit and blowdown. Figure B-2 provides a schematic of the ETF processes. See Attachment C for a description of the SALDS.
3. Indicate treatment provided to each waste stream identified above.

Waste Stream(s) ID #	Treatment	Waste Stream(s) ID # ^a	Treatment
	Air flotation	1,2,4	pH correction
	Centrifuge		Ozonation
	Chemical precipitation	1,2,4	Reverse osmosis ^b
	Chlorination		Screen
	Cyclone		Sedimentation
1,2,4	Filtration		Septic tank
1,2,4	Flow equalization		Solvent separation
	Grease or oil separation		Bio. treatment, type:
	Grease trap		Rainwater diversion or storage
	Grit removal		Other phys. treatment type:
1,2,4	Ion exchange	1,2,4	Other chem. treatment type: UV oxidation

^a Secondary waste stream is discussed in Attachment B, Section 3.0.

^b Includes synthetic semipermeable membranes.

4. Describe any planned waste water treatment improvements or changes in waste water disposal methods:

The ETF is planned to start operations in October 1994. A load-in station will be added to the ETF. The load-in station will provide a waste acceptance area for wastes that may be transported from other locations on the Hanford Site in the future.

5. If production processes are subject to seasonal variations, provide the following information. Write "Yes" for each month waste stream is produced.

Note that waste stream #1 will be processed initially, and eventually this waste stream will be replaced by waste stream #2.

Waste Stream ID #	MONTHS											
	J	F	M	A	M	J	J	A	S	O	N	D
1,2	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes
3	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes
4	On an as-needed basis											

Shift information: The ETF will be operated on a schedule of 42 days of operation and 5-25 days of maintenance (16 days average of non-operation for maintenance). *As experience is gained in operation of the facility, the number of employees may increase or decrease as needed.

6. a. Number of shifts per work day: 3
 b. Number of work days per week: 7
 c. Average number of work days per year: 265
 d. Maximum number of work days per year: 365
 e. Number of employees per shift: Shift
- | | | | |
|-----|--------------------|-----|--------------|
| 1st | <u>-10 (4-15)*</u> | 1st | <u>7:30</u> |
| 2nd | <u>-10 (4-15)*</u> | 2nd | <u>15:30</u> |
| 3rd | <u>-10 (4-15)*</u> | 3rd | <u>23:30</u> |

7. List all incidental materials like oil, paint, grease, solvents, soaps, cleaners, that are used or stored on-site. (Use additional sheets, if necessary.)

Material/Quantity Stored: Small quantities of materials such as lubricating oils, solvents, and cleaners for maintaining the ETF equipment may be stored onsite. Quantities are unknown at this time. This information will be available at the ETF on completion of construction and purchasing of chemicals for operation startup.

8. Describe any water recycling or material reclaiming processes:
None.

9. Does this facility have:

-Spill Control and Containment Plan (per 40 CFR 112)? Yes No
 -Emergency Response Plan (per WAC 173-303-350)? Yes No

-Runoff, spillage, or leak control plan (per WAC 173-216-110(f))? Yes No
This information will be supplied in the RCRA Part B permit application.

SECTION D. WATER CONSUMPTION AND WATER LOSS

1. Water source(s) include the following: 1) Waste water received from LERF and 242-A Evaporator, 2) Raw water from the Columbia River transferred through the 200 East Area water supply system for the cooling tower, and 3) Demineralized water trucked to ETF or produced onsite for laboratory use.

Public System (Specify) _____

Private Well Surface Water

a. Water Right Permit Number: N/A. The U.S. Government has a reserved water right to utilize water for purposes of Hanford Site activities

b. Legal Description: S01 withdrawal point
 8 1/4S, B Section, 13 TWN, 24 RE

2. a. Indicate total water use: Gallons per day (average) 156,000 gpd waste water;
46,300 gpd raw water;
2,085 gpd demineralized water

Gallons per day (maximum) 216,000 gpd waste water;
64,000 gpd raw water;
2,880 gpd demineralized water

b. Is water metered? Yes No, not at the ETF

3. Attach a line drawing showing the water flow through the facility. Indicate source of intake water, operations contributing waste water to the effluent, and treatment units labeled to correspond to the more detailed descriptions in Item C. Construct a water balance on the line drawing by showing average flows between intakes, operations, treatment units, and outfalls. If a water balance cannot be determined (*e.g., for certain mining activities*), provide a pictorial description of the nature and amount of any sources of water and any collection or treatment measures.

See Attachment B, Figure B-1 for layout of ETF and Figure B-2 for waste water flows in ETF.

SECTION E. WASTEWATER INFORMATION

1. Provide measurements for the parameters listed below, unless waived by the permitting authority. All analytical methods used to meet these requirements shall, unless approved otherwise in writing by Ecology, conform to the Guidelines Establishing Test Procedures for the Analysis of Pollutants Contained in 40 CFR Part 136.

See Table B-1 for ETF anticipated effluent concentrations that are based on best engineering judgement. Because the values provided are estimated and no analyses have been performed, the analytical methods and detection limits are not applicable. See Table B-2 for anticipated cooling tower blowdown constituent concentrations.

Parameter/CAS No.	Concentrations Measured	Analytical Method	Detection Limit
pH			
Conductivity			
Total Dissolved Solid			
Total Suspended Solid			
BOD (5 day)			
COD			
Ammonia-N			
TKN-N			
Nitrate-N			
Ortho-phosphate-P			
Total-phosphate-P			
Total Oil & Grease			
Calcium/7740-70-2			
Magnesium/7439-95-4			
Sodium/7440-23-5			
Potassium/7440-09-7			
Chloride			
Sulfate			
Fluoride			
Cadmium/7440-43-9			
Chromium/7440-49-3			
Lead/7439-92-1			
Mercury/7439-97-6			
Selenium/7782-49-2			
Silver/7440-22-4			
Copper/7440-50-8			
Iron/7439-89-6			
Manganese			
Zinc/7440-66-6			
Barium/7440-39-3			
Total Coliform			

2. Waste water characteristics for toxic pollutants.

The intent of this question is to determine which chemicals are or might be present in the process water or waste water. For each chemical listed below:

- a. Use the letter **A** in the **ABST** column if the chemical is not likely to be present because it is not used in the production process or used on site.
- b. Use the letter **S** in the **ABST** column if the chemical may be present because it is used on site, but the chemical is not used in the production process.
- c. Use the letter **P** in the **PRST** column if the chemical is likely to be present because it is used in the production process, but the effluent has not been tested.
- d. Use the letter **K** in the **PRST** column if the effluent has been tested and found to be present.

Attach the analytical results.

Analytical Results
Waste Water Characterization for Toxic Pollutants

(The information in this table is based on ETF design criteria, see also Table B-1 for ETF anticipated effluent concentrations and Table B-2 for cooling tower blowdown constituent concentrations.)

Source: WHC (1992c)

ABST/PRST	CONSTITUENT/CAS No.	ABST / PRST	CONSTITUENT/CAS No.
<u>A</u> ___	Acrylamide/79-06-1	<u>A</u> ___	1,2 Dichloropropane/78-87-5
<u>A</u> ___	Acrylonitrile/107-13-1	<u>A</u> ___	1,3 Dichloropropene/542-75-6
<u>A</u> ___	Aldrin/309-00-2	<u>A</u> ___	Dichlorvos/62-73-7
<u>A</u> ___	Aniline/62-53-3	<u>A</u> ___	Dieldrin/60-57-1
<u>A</u> ___	Aramite/140-57-8	<u>A</u> ___	3,3' Dimethoxybenzidine/119-90-4
___ <u>P</u>	Arsenic/7440-38-2	<u>A</u> ___	3,3 Dimethylbenzidine/119-93-7
<u>A</u> ___	Azobenzene/103-33-3	<u>A</u> ___	1,2 Dimethylhydrazine/540-73-8
___ <u>P</u>	Benzene/71-43-2	<u>A</u> ___	2,4 Dinitrotoluene/121-14-2
<u>A</u> ___	Benzidine/92-87-5	<u>A</u> ___	2,6 Dinitrotoluene/606-20-2
<u>A</u> ___	Benzo(a)pyrene/50-32-8	<u>A</u> ___	1,4 Dioxane/123-91-1
<u>A</u> ___	Benzotrichloride/98-07-7	<u>A</u> ___	1,2 Diphenylhydrazine/122-66-7
<u>A</u> ___	Benzyl chloride/100-44-7	<u>A</u> ___	Endrin/72-20-8
<u>A</u> ___	Bis(chloroethyl)ether/111-44-4	<u>A</u> ___	Epichlorohydrin/106-89-8
<u>A</u> ___	Bis(chloromethyl)ether/542-88-1	<u>A</u> ___	Ethyl acrylate/140-88-5
<u>A</u> ___	Bis(2-ethylhexyl)phthalate/117-81-7	<u>A</u> ___	Ethylene dibromide/106-93-4

ABST/PRST	CONSTITUENT/CAS No.	ABST / PRST	CONSTITUENT/CAS No.
<u>A</u> ___	Bromodichloromethane/75-27-4	<u>A</u> ___	Ethylene thioureae/96-45-7
<u>A</u> ___	Bromoform/75-25-2	<u>A</u> ___	Folpet/133-07-3
<u>A</u> ___	Carbazole/86-74-8	<u>A</u> ___	Furmecyclohex/60568-05-0
___ <u>*P</u>	Carbon tetrachloride/56-23-5	<u>A</u> ___	Heptachlor/76-44-8
<u>A</u> ___	Chlordane/57-74-9	<u>A</u> ___	Heptachlor epoxide/1024-57-3
<u>A</u> ___	Chlorodibromomethane/124-48-1	<u>A</u> ___	Hexachlorobenzene/118-74-1
___ <u>*P</u>	Chloroform/67-66-3	<u>A</u> ___	Hexachlorocyclohexane (alpha)/319-84-6
<u>A</u> ___	Chlorthalonil/1897-45-6	<u>A</u> ___	Hexachlorocyclohexane (tech.)/608-73-1
<u>A</u> ___	2,4-D/94-75-7	<u>A</u> ___	Hexachlorodibenzo-p-dioxin, mix/ 19408-74-3
<u>A</u> ___	DDT/50-29-3	___ <u>**P</u>	Hydrazine/hydrazine sulfate/302-01-2
<u>A</u> ___	Diallate/2303-16-4	<u>A</u> ___	Lindane/58-89-9
<u>A</u> ___	1,2 Dibromoethane/106-93-4	<u>A</u> ___	2 Methyl aniline/100-61-8
<u>A</u> ___	1,4 Dichlorobenzene/106-46-7	<u>A</u> ___	2 Methyl aniline hydrochloride/ 636-21-5
<u>A</u> ___	3,3' Dichlorobenzidine/91-94-1	<u>A</u> ___	4,4' Methylene bis(N,N-dimethyl)aniline/ 101-61-1
<u>A</u> ___	1,1 Dichloroethane/75-34-3	___ <u>*P</u>	Methylene chloride (dichloromethane)/75-09-2
<u>A</u> ___	1,2 Dichloroethane/107-06-2	<u>A</u> ___	Mirex/2385-85-5
<u>A</u> ___	Nitrofurazone/59-87-0	<u>A</u> ___	O-phenylenediamine/106-50-3
<u>A</u> ___	N-nitrosodiethanolamine/ 1116-54-7	<u>A</u> ___	Propylene oxide/75-56-9
<u>A</u> ___	N-nitrosodiethylamine/55-18-5	<u>A</u> ___	2,3,7,8-Tetrachlorodibenzo-p-dioxin/ 1746-01-6
___ <u>*P</u>	N-nitrosodimethylamine/62-75-9	<u>A</u> ___	Tetrachloroethylene/127-18-4
<u>A</u> ___	N-nitrosodiphenylamine/86-30-6	<u>A</u> ___	2,4 Toluenediamine/95-80-7
<u>A</u> ___	N-nitroso-di-n-propylamine/ 621-64-7	<u>A</u> ___	o-Toluidine/95-53-4
<u>A</u> ___	N-nitrosopyrrolidine/930-55-2	<u>A</u> ___	Toxaphene/8001-35-2
<u>A</u> ___	N-nitroso-di-n-butylamine/ 924-16-3	<u>A</u> ___	Trichloroethylene/79-01-6
<u>A</u> ___	N-nitroso-n-methylethylamine/ 10595-95-6	<u>A</u> ___	2,4,6-Trichlorophenol/88-06-2
<u>A</u> ___	PAH/NA	<u>A</u> ___	Trimethyl phosphate/512-56-1
<u>A</u> ___	PBBs/NA	<u>A</u> ___	Vinyl chloride/75-01-4
<u>A</u> ___	PCBs/1336-36-3		

* These compounds are not process chemicals, but are predicted constituents of ETF influent.
 ** Hydrazine used historically at PUREX, but is not anticipated in 242-A Evaporator PC.

SECTION F. STORMWATER

1. Do you have a stormwater NPDES permit? Yes No
The ETF Building does not have a specific storm water permit.
2. Have you applied for a stormwater NPDES permit? Yes No
The ETF Building has not applied for a storm water permit.
3. Are you covered or have you applied for coverage under a general or group stormwater permit? Yes No
A General NPDES permit for stormwater has been applied for by the Department of Energy for the Hanford Site.

4. Describe the size of the stormwater collection area. ETF (This does not apply to SALDS which is not paved.)
 - a. Unpaved Area 634,000* sq. ft.
 - b. Paved Area 60,000 sq. ft.
 - c. Other Collection Areas (Roofs, Diked Areas, etc.) *inside security fence 78,000 sq. ft.

5. Describe the stormwater management systems.
Stormwater from the ETF building will be managed by a series of gutters and down spouts, which are shown on drawings H-2-89049 and H-2-89050 (Attachment D). Water will be collected from the roof by rain gutters and transferred to down spouts. The down spouts will drain to graveled areas which are shown on the maps near the ETF building. Water will either evaporate or soak into the soil at this point.

Paved areas will be sloped to direct stormwater away from the facility as shown on drawing H-2-89039 (Attachment D). The stormwater will be transferred to graveled ditches where the water will either evaporate or soak into the soil.

6. Attach a map showing stormwater drainage/collection areas, disposal areas and discharge points.
See maps in Attachment D.

SECTION G. OTHER INFORMATION

1. Describe liquid wastes or sludges being generated that are not disposed of in the waste stream(s).

No liquid wastes or sludges are generated that are not disposed of in the waste stream. See Attachment B, Section 3.0 for description of the processes that generate the powdered waste produced at the ETF. The powdered waste is regulated under RCRA and will be stored in the Hanford Facility Central Waste Complex until a disposal facility is identified.

2. Describe storage areas for raw materials, products, and wastes.

Raw materials such as sulfuric acid, sodium hydroxide, and hydrogen peroxide will be stored in tanks in the ETF building. Drummed powdered waste will be stored in the filled-drum storage area in the ETF building. Other wastes such as spent UV lamps, spent RO membranes, spent filters, spent HEPA filters, spent ion exchange resins, and peroxide decomposer cartridges will be drummed and temporarily stored in the filled drum storage area.

3. Have you designated your wastes according to the procedures of Dangerous Waste Regulations, Chapter 173-303 WAC? Yes No

4. Waste hauled off-site by: Waste hauler; Self; Other (identify)

Drummed wastes from the ETF are not hauled off the Hanford Site. The waste will be stored at the Central Waste Complex.

Name

Name

Address

Address

City/State

City/State

Telephone

Telephone

5. Have you filed a SARA Title 313 Disclosure? Yes No

After the ETF is in operation, SARA Title 313 information will be submitted as part of the Hanford Site annual report.

SECTION H. SITE ASSESSMENT

1. Give the legal description of the land treatment site(s). Give the acreage of each land treatment site(s). Attach a copy of the contract(s) authorizing use of land for treatment. See Attachment C, Section 1.0
2. List all environmental control permits or approvals needed for this project; for example, septic tank permits, sludge application permits, or air emissions permits.

Air Permitting

- Approval to Construct, National Emission Standards for Hazardous Air Pollutants
- Approval to Construct, Radiological Airborne Emission
- Approval to Construct, Controls for New Sources of Toxic Air Pollutants
- Notification of Startup, National Emissions Standards for Hazardous Air Pollutants

Waste Water Permitting

- Septic System Permit
- State Waste Discharge Permit

Hazardous Waste Permitting

- Dangerous Waste Permit
- Delisting Petition

3. Attach a topographic map with contour intervals used by USGS. Show the following on this map:
See Attachment C, Section 2.0 and Figures C-1 and C-2.
 - a. Location and name of internal and adjacent streets
 - b. Surface water drainage systems N/A
 - c. Water supply and other wells within 500 feet of the site
No water supply wells within 500 feet.
 - d. Surface water diversions within 500 feet of the site N/A
 - e. Chemical and product handling and storage facilities
None within 500 feet of SALDS
 - f. Infiltration sources, such as drainfields, lagoons, dry wells, and abandoned wells within 500 feet of the site N/A
 - g. Waste water and cooling water discharge points with ID numbers
(See Section C.1)
 - h. Other activities and land uses within 1/4 mile of the site

4. Identify all wells within 500 feet of the site. Attach well logs when available and any available water quality data.

Monitoring well 699-48-77A is the only well located within 500 feet of the site. Figure C-2 (Attachment C) depicts the well location. Figure C-3 (Attachment C) provides summarized well log information. Copies of the borehole log are provided in the appendix to Attachment C.

5. Describe soils on the site using information from local soil survey reports. (Submit on separate sheet.)

See Attachment C, Section 3.0 and Figure C-5.

6. Describe the regional geology and hydrogeology within one mile of the site. (Submit on separate sheet.)

See Attachment C, Section 3.0

7. Information for this permit was obtained from the references listed in Attachment E, and from interviews with the cognizant Westinghouse Hanford Company personnel for the Hanford 200 Area ETF/SALDS. The permit application was compiled by:

Science Applications International Corporation
1845 Terminal Drive
Richland, WA 99352

See Attachment E for additional reference materials.

END - END - END

ATTACHMENT A

**WASTE SOURCES TO THE 200 AREA EFFLUENT TREATMENT FACILITY
AND TREATMENT PROCESS OVERVIEW**

ATTACHMENT A

200 AREA EFFLUENT TREATMENT FACILITY WASTE SOURCES AND TREATMENT PROCESS OVERVIEW

1.0 INTRODUCTION

Application is being made for a permit pursuant to Chapter 173-216 of the Washington Administrative Code (WAC), to discharge treated waste water and cooling tower blowdown from the 200 Area Effluent Treatment Facility (ETF) to land at the State-Approved Land Disposal Site (SALDS). The ETF is located in the 200 East Area and the SALDS is located north of the 200 West Area. These locations are depicted in Figure A-1.

The production of nuclear materials at the Hanford Site generated wastes over the past 50 years. The Standard Industrial Classification (SIC) code for the production of nuclear fuels is 2819. The production wastes included the following: (1) fuel fabrication wastes, (2) laboratory wastes, (3) decontamination wastes, and (4) research and development wastes. Some of these wastes were discharged to cribs, ponds, and ditches. Other wastes were stored in underground double-shell and single-shell tanks.

The ETF is an industrial waste water treatment plant that will initially receive waste water from the following two sources, both located in the 200 Area on the Hanford Site: (1) the Liquid Effluent Retention Facility (LERF) and (2) the 242-A Evaporator. The waste water discharged from these two facilities is process condensate (PC), a by-product of the concentration of waste from DSTs that is performed in the 242-A Evaporator. Because the ETF is designed as a flexible treatment system, other aqueous waste streams generated at the Hanford Site may be considered for treatment at the ETF. The origin of the waste currently contained in the DSTs is explained in Section 2.0. An overview of the concentration of these waste in the 242-A Evaporator is provided in Section 3.0. Section 4.0 describes the LERF, a storage facility for process condensate.

Attachment A responds to Section B of the permit application and provides an overview of the processes that generated the wastes, storage of the wastes in double-shell tanks (DST), preliminary treatment in the 242-A Evaporator, and storage at the LERF. For purposes of the application, the 242-A Evaporator is considered similar to a manufacturing process because it generates the waste water that is proposed for treatment in the ETF and disposal at the SALDS.

Attachment B addresses waste water treatment at the ETF (under construction) and the addition of cooling tower blowdown to the treated waste water prior to disposal at SALDS. Attachment C describes treated waste water disposal at the proposed SALDS. A general schematic of the treatment processes is presented in Figure A-2.

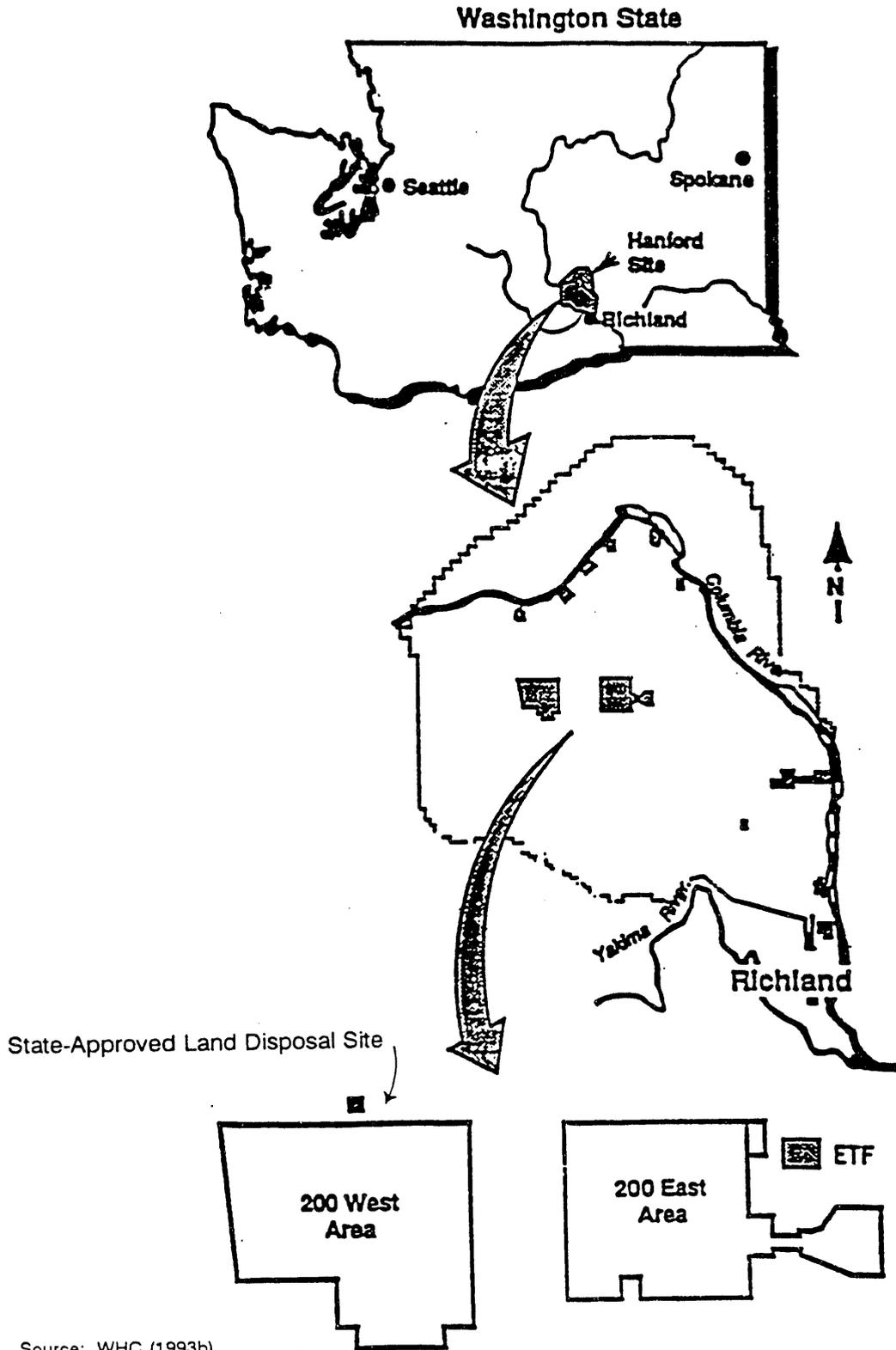
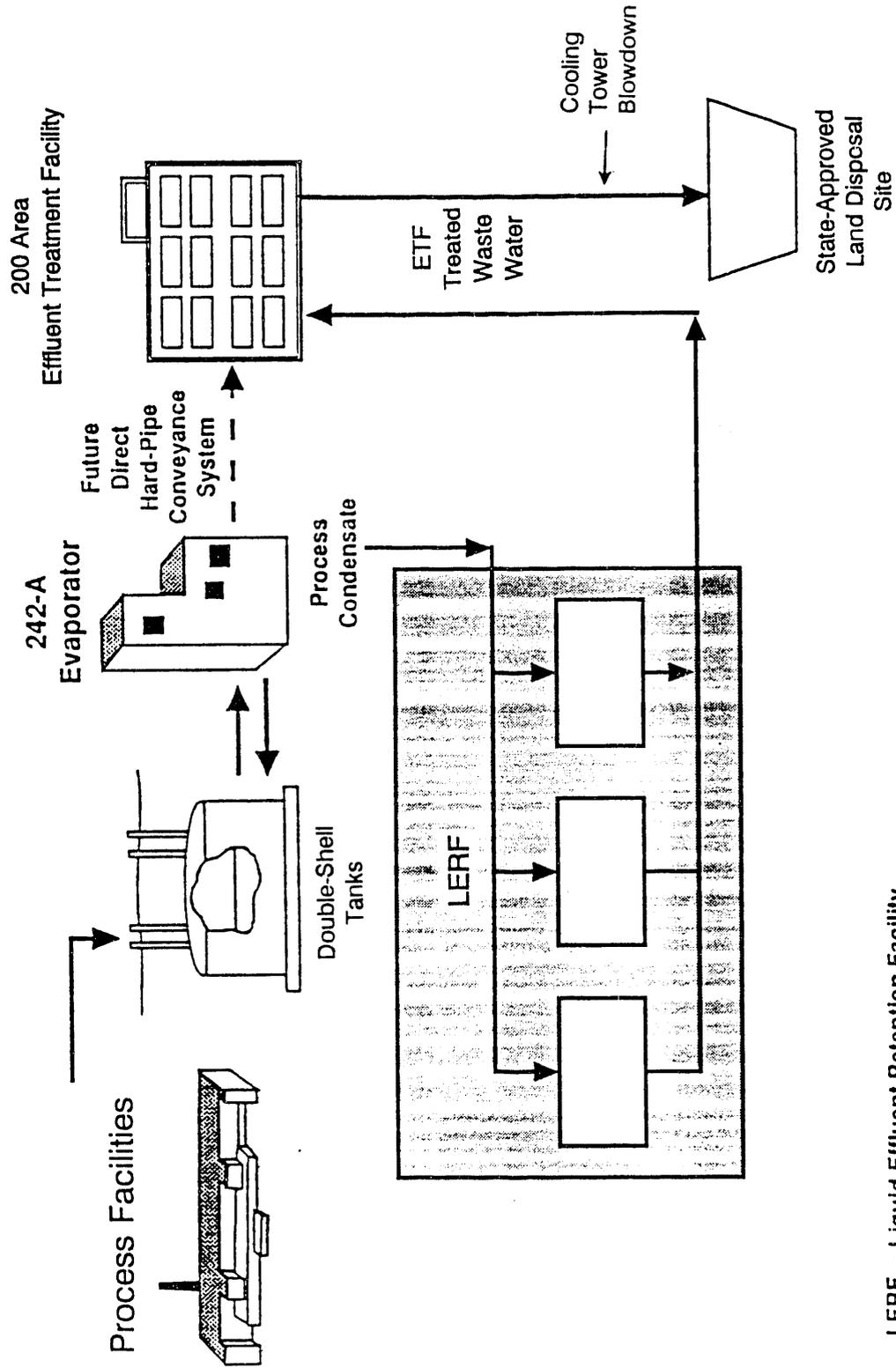


Figure A-1. Location of the State-Approved Land Disposal Site and the Effluent Treatment Facility.



LERF = Liquid Effluent Retention Facility

Source: DOE (1992a)

Figure A-2. Overview of Waste Water Source and Treatment Program.

2.0 SOURCES OF THE WASTE STREAMS TO THE 242-EVAPORATOR

The 242-A Evaporator will process wastes generated by past and present operations of numerous Hanford Site waste generators and processors. The wastes will be withdrawn from storage in the underground DSTs and processed in the 242-A Evaporator in different campaigns according to their classification by total organic carbon, transuranic content, and potential effects on the evaporation process (DOE 1992b). Some waste now stored in DSTs was generated before the DSTs were in service. This waste was originally stored in single-shell tanks but has been transferred to DSTs (DOE 1991). Other wastes currently stored in the DSTs were generated from, but not limited to, the following processing operations (DOE 1992b):

- S Plant laboratory and decontamination wastes
- T Plant spent decontamination solutions
- 300 Area laboratory wastes
- 300 Area fuels fabrication
- 400 Area laboratory waste
- 100-N dilute phosphate decontamination waste, and 100 Area spent fuel storage basin sulfate waste from ion exchange regeneration and sand filter backwashing
- Single-shell tank salt well pumping waste
- Plant process and miscellaneous waste, including cell drainage and vessel cleanout waste
- PUREX Plant.

The DSTs are located in the 200 East and 200 West Areas. Each tank has a nominal capacity of 1 million gallons (3.8 million liters). The liquid wastes in the tank contain low concentrations of fission products that generate low quantities of heat (less than 0.1 BTU per hour per gallon). The wastes are considered mixed waste, because the waste contains both radioactive components regulated under the Atomic Energy Act, and listed hazardous wastes regulated pursuant to the Resource Conservation and Recovery Act and Washington Dangerous Waste Regulations, WAC 173-303. Additional information on the contents of the DST waste can be found in the *Double-Shell Tank System Dangerous Waste Permit Application* (DOE 1991).

3.0 WASTE PROCESSING AT THE 242-A EVAPORATOR

The 242-A Evaporator is used as a waste concentrator for the wastes that are stored in the DSTs. The purpose of the 242-A Evaporator is to concentrate liquid wastes into a slurry of reduced volume to allow for greater storage capacity in the existing DSTs. The 242-A Evaporator uses a conventional forced recirculation, vacuum evaporation system to concentrate the waste solutions. In this treatment process, water and volatile substances are evaporated from the waste feed, and the vapor is subsequently recondensed as process condensate (PC) and stored at the LERF. The residual concentrated slurry contains the majority of the radionuclides and inorganic constituents. The slurry is designated as an extremely hazardous mixed waste and is returned to the DSTs for storage pending further treatment.

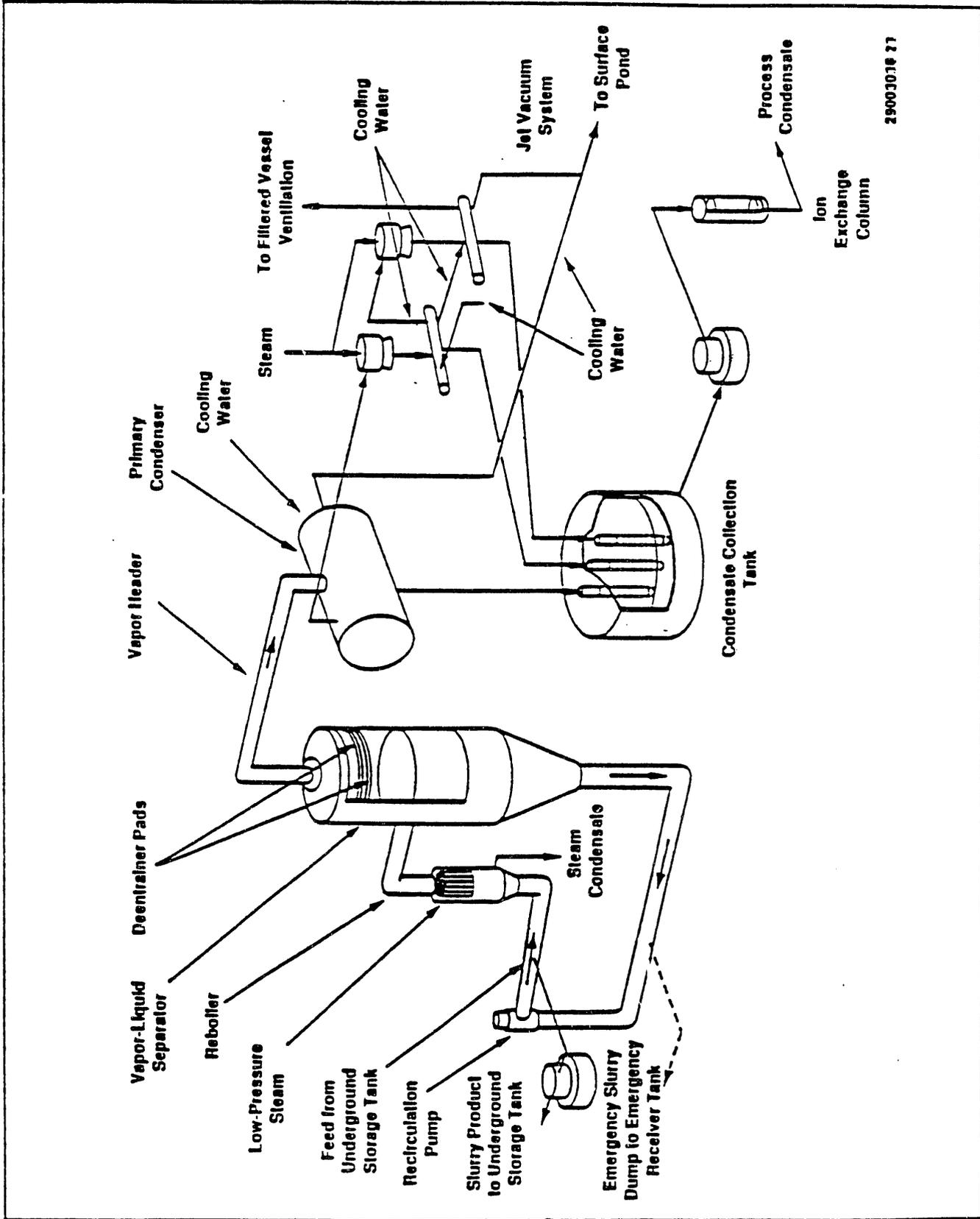
The 242-A Evaporator process is depicted schematically in Figure A-3. In general terms, the 242-A Evaporator receives waste feed in the recirculation line, where the waste feed blends with the main process slurry stream. The waste feed and the recirculated slurry flow together into the reboiler where the waste stream is heated and the pressure is reduced to cause the liquid to flash to steam. The slurry remaining in the separator continues to be concentrated by removal of the boiled-off liquid. The slurry is removed; when it has reached a target-specific gravity (an indicator of increasing solute concentration), some of the slurry stream is transferred to a DST. The remaining slurry is recirculated and blends with the waste feed.

The vapor from the separator chamber is transported to a condenser where it is cooled and condensed forming the PC. The PC is contained in the condensate collection tank (C-100) which has a nominal capacity of 17,800 gallons (67,400 L). An agitator operates intermittently to keep the tank contents mixed and to prevent settling of solids, as the liquid is pumped through a filter to remove particulates greater than 5 microns.

The PC then passes through an ion exchange column to remove radionuclides (primarily cesium-137 and strontium-90) (DOE 1992b). Following filtration, the PC is pumped to the LERF where it awaits further treatment. The PC will be stored at the LERF while the ETF is under construction. After completion of the ETF, the PC will be pumped directly to the ETF treatment system, bypassing the LERF. Because the ETF design incorporates an ion exchange unit, the 242-A Evaporator ion exchange column will be bypassed when PC is pumped directly to the ETF. This will allow for a greater rate of processing of the DST feed streams.

The PC contains a variety of constituents including organic and inorganic constituents and radionuclides. Thirty-four samples of PC were analyzed prior to shutdown of the 242-A Evaporator. Additionally, process control samples were collected during the operation of the 242-A Evaporator. The analytical data from both sets of samples are summarized in Table A-1, which represents an initial estimate of PC composition. These data were

presented in the *200 Area Effluent Treatment Facility Delisting Petition* (DOE 1992). The exact composition of the PC, however, will vary depending on the source of the DST waste that is treated in the 242-A Evaporator. Table A-2 presents the analytical methods used.



29003018 27

Figure A-3. 242-A Evaporator Process Schematic.

Source: WHC (1991)

4.0 LIQUID EFFLUENT RETENTION FACILITY

The LERF consists of three covered surface impoundments with a capacity of 6.5 million gallons each. These basins will be used to store PC until the ETF can process it. Only two basins will be used at any one time; the third basin will be held in reserve. A RCRA Part B permit application for this storage facility was submitted to The Washington State Department of Ecology (Ecology) in June 1991 and is currently being reviewed by Ecology.

Table A-1. 242-A Evaporator Effluent Characterization Data.^a

Parameter	Units ^b	Average	90% Confidence Interval ^c	Maximum
Conductivity	μS	304	--	590
pH		10.0	--	11.3
Inorganic Constituents				
Total Dissolved Solids	ppb	NA	NA	2,700
Aluminum	ppb	1,295	1,330	4,992
Ammonium	ppb	482,511	511,344	9,350,000
Barium	ppb	6.8	7.2	8
Boron	ppb	65	97	151
Cadmium	ppb	5	SD	SD
Calcium	ppb	2,600	2,800	8,300
Carbonate	ppb	98,000	104,347	750,00
Chloride	ppb	1,000	1,200	2,300
Chromium	ppb	52	66	156
Copper	ppb	60	67	127
Fluoride	ppb	874	971	12,273
Iron	ppb	112	131	503
Magnesium	ppb	122	153	3,670
Manganese	ppb	5	SD	SD
Mercury	ppb	0.3	0.31	0.69
Phosphorus	ppb	1,177	1,336	6,195
Nickel	ppb	14	15	17
Nitrate	ppb	2,800	2,292	5,000
Potassium	ppb	5,944	6,495	19,238
Silicon	ppb	15,616	24,252	985,819
Sodium	ppb	3,586	4,469	51,497
Sulfate	ppb	2,600	2,800	13,000
Sulfide	ppb	36,000	66,000	66,000
Vanadium	ppb	6.3	6.7	7

Table A-1. 242-A Evaporator Effluent Characterization Data.^a (cont.)

Parameter	Units ^b	Average	90% Confidence Interval ^c	Maximum
Organic Constituents				
Total organic carbon	ppb	42,024	218,415	4,920,000
Acetone	ppb	980	1,000	5,100
Benzyl alcohol	ppb	13	14	18
Benzaldehyde	ppb	23	SD	SD
2-Butoxyethanol	ppb	380	400	920
1-Butanol	ppb	9,800	11,000	88,000
2-Butanone	ppb	51	53	120
Butoxyglycol	ppb	280	290	810
Butoxydiglycol	ppb	19	44	27
Butoxytriethyleneglycol	ppb	35	SD	SD
Butraldehyde	ppb	56	62	230
Caproic acid	ppb	70	SD	SD
Chloroform	ppb	14	14	27
3,5-Dimethylpyridine	ppb	21	23	24
Dimethylnitrosamine	ppb	57	SD	SD
Dodecane	ppb	43	52	46
Ethoxytriethyleneglycol	ppb	99	120	150
Ethyl alcohol	ppb	2	SD	SD
Hexadecane	ppb	17	SD	SD
Heptadecane	ppb	18	SD	SD
Methoxydiglycol	ppb	40	52	52
Methoxytriglycol	ppb	220	370	370
Methylene chloride	ppb	120	140	180
Methyl n-propyl ketone	ppb	9.3	9.7	12
Methyl n-butyl ketone	ppb	13	14	79
MIBK (Hexone)	ppb	11	14	68
2-Methylnonane	ppb	16	17	17
Pentadecane	ppb	20	SD	SD
Phenol	ppb	33	SD	SD

Table A-1. 242-A Evaporator Effluent Characterization Data.^a (cont.)

Parameter	Units ^b	Average	90% Confidence Interval ^c	Maximum
2-Propanol	ppb	22	SD	SD
Pyridine	ppb	550	SD	SD
Tetradecane	ppb	76	83	440
Tetrahydrofuran	ppb	37	39	170
Tributyl phosphate	ppb	3,900	4,100	21,000
1,1,1-Trichloroethane	ppb	5	SD	SD
Tridecane	ppb	70	77	350
Triglyme	ppb	90	SD	SD
Radionuclides				
Alpha	pCi/L	160	350	750
Beta	pCi/L	4,600	6,000	74,000
¹³⁷ Cesium ^d	pCi/L	4,400	5,400	26,000
¹⁵⁵ Europium	pCi/L	1,400	SD	SD
²³⁹ Plutonium	pCi/L	0.00037	0.00068	0.0024
¹⁴⁷ Promethium	pCi/L	1,300	1,600	4,100
¹⁰⁶ Ruthenium	pCi/L	10,500	11,080	17,800
⁹⁰ Strontium ^d	pCi/L	5,200	7,600	81,000
¹¹³ Tin	pCi/L	540	770	2,500
Tritium	pCi/L	5,600,000	6,300,000	24,000,000
Uranium (gross)	pCi/L	20	33	140

^a Source: DOE (1992b)^b μ S = microsiemen; ppb = parts per billion; SD = single detection; pCi/L = picocuries per liter; NA = not available.^c 90% Confidence Interval based on 34 samples of 242-A Evaporator Process Condensate (DOE 1992b)^d ¹³⁷ Cesium and ⁹⁰ strontium values have been multiplied by 10 to account for the removal of the existing ion exchange system in the 242-A Evaporator

Table A-2. 242-A Evaporator Process Condensate Analytical Methods.^a

Parameter	Test Method	Source ^b
Organics		
Volatile organics	EPA 8240	SW-846
Semivolatile organics	EPA 8270	SW-846
Total organic carbon	EPA 9060	SW-846
Inorganic Anions		
Chloride	EPA 9250	SW-846
Fluoride	EPA 340.2	EPA-600
Nitrate/nitrite	EPA 9200	SW-846
Phosphate	EPA 365.2	EPA-600
Sulfate	EPA 300.0	EPA-600
Sulfide	EPA 9030	SW-846
Inorganic Cations		
Ammonium	ASTM D 1426-89	ASTM
Aluminum	EPA 6010	SW-846
Arsenic	EPA 6010	SW-846
Barium	EPA 6010	SW-846
Cadmium	EPA 6010	SW-846
Calcium	EPA 6010	SW-846
Chromium	EPA 6010	SW-846
Lead	EPA 6010	SW-846
Magnesium	EPA 6010	SW-846
Manganese	EPA 6010	SW-846
Mercury	EPA 6010	SW-846
Selenium	EPA 6010	SW-846
Silver	EPA 6010	SW-846
Sodium	EPA 6010	SW-846

Table A-2. 242-A Evaporator Process Condensate Analytical Methods.^a (cont.)

Parameter	Test Method	Source ^b
Zinc	EPA 6010	SW-846
Miscellaneous		
Alpha activity	EPA 9310	SW-846
Beta Activity	EPA 9310	SW-846
Biochemical oxygen demand (BOD)	EPA 405.1	EPA-600
pH	EPA 9040	SW-846
Specific gravity	SM-2710.F	SM
Temperature	SM-2550 (field)	SM
Total dissolved solids	EPA 160.1	EPA-600

^a Source: DOE 1992b

^b SW-846 (EPA 1990); SM (APHA 1989); EPA-600 (EPA 1983); ASTM (ASTM 1990)

ATTACHMENT B

200 AREA EFFLUENT TREATMENT FACILITY

ATTACHMENT B

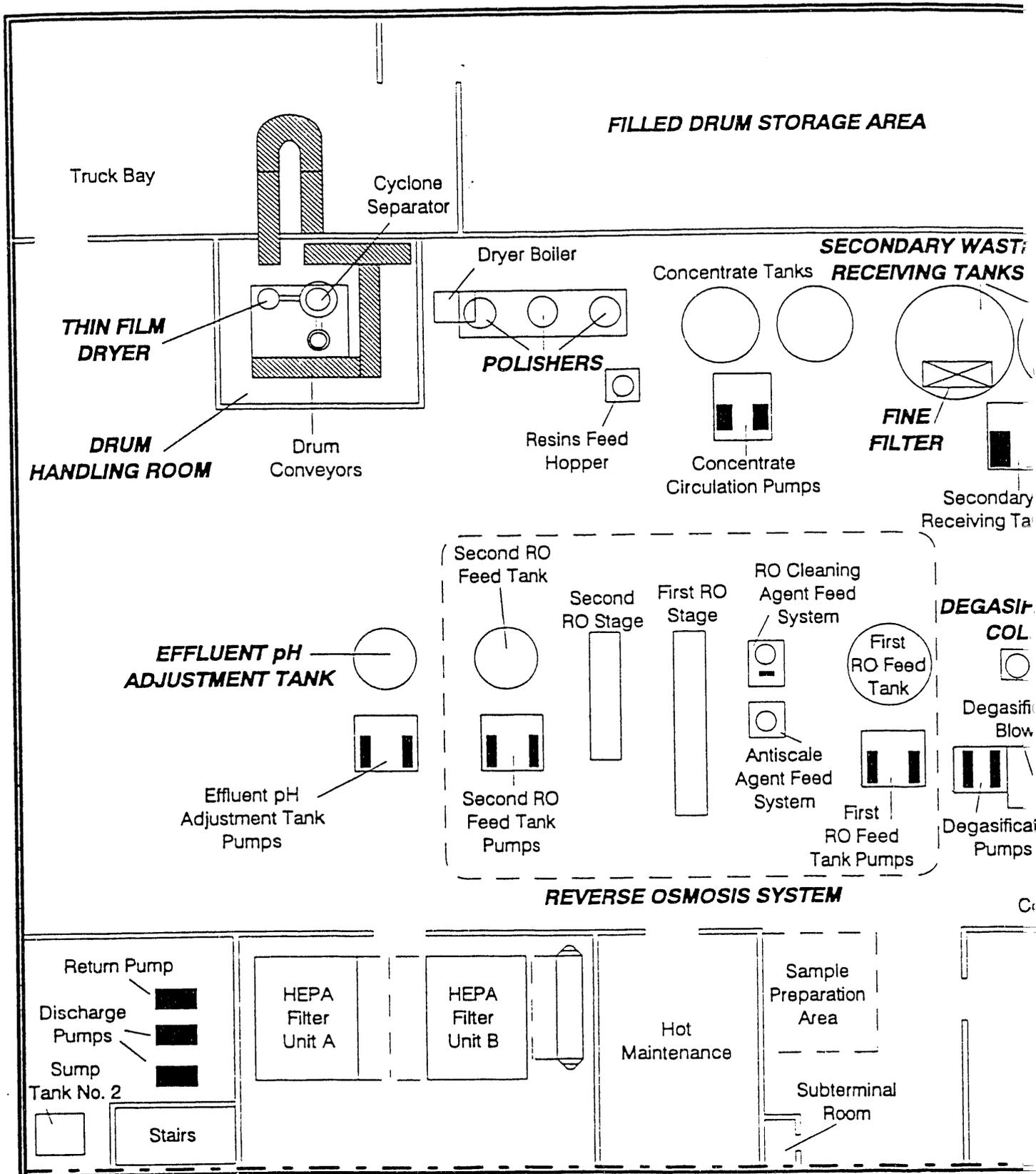
200 AREA EFFLUENT TREATMENT FACILITY

1.0 INTRODUCTION

The 200 Area Effluent Treatment Facility (ETF) receives waste water from the 242-A Evaporator and the LERF. In the future, it is intended to route other waste streams from the Hanford Site to the ETF for treatment. Other waste streams that can be treated to meet the established effluent discharge limits will be treated at the ETF. The waste waters are treated in a series of process units or systems, applying best available technology to reduce radioactive constituents, except tritium, and to reduce the concentrations of the organic and inorganic constituents. Before discharge, the quality of the treated waste water is analyzed to verify that the discharge limits have been met. The treated waste water is piped to the State-Approved Land Disposal Site (SALDS) north of the 200 West Area, where the treated waste water is discharged to the ground under the authority of a Washington State Waste Discharge Permit and an approved Hazardous Waste Delisting Petition.

The ETF contains several tanks and process unit systems for the treatment of dilute waste waters generated on the Hanford Facility. Figure B-1 provides an overview of the ETF Building layout and Figure B-2 is the flow diagram of the treatment process. The ETF effluent concentrations to be disposed at the SALDS are provided in Table B-1. Information about the ETF effluent concentrations in Table B-1 was derived from health-based limits, ground water protection limits, and best engineering judgement of treatment capability. Information about the concentrations anticipated in the cooling tower blowdown is provided in Table B-2 and was derived from the *Columbia River Characterization Data Report in Support of Project L-045* (WHC 1992d). The concentrations in both tables are estimates and will be revised based on the results of the pilot plant testing and any additions or deletions of influent streams. The pilot plant results will be submitted to Ecology as part of the Delisting Petition (DOE 1992b).

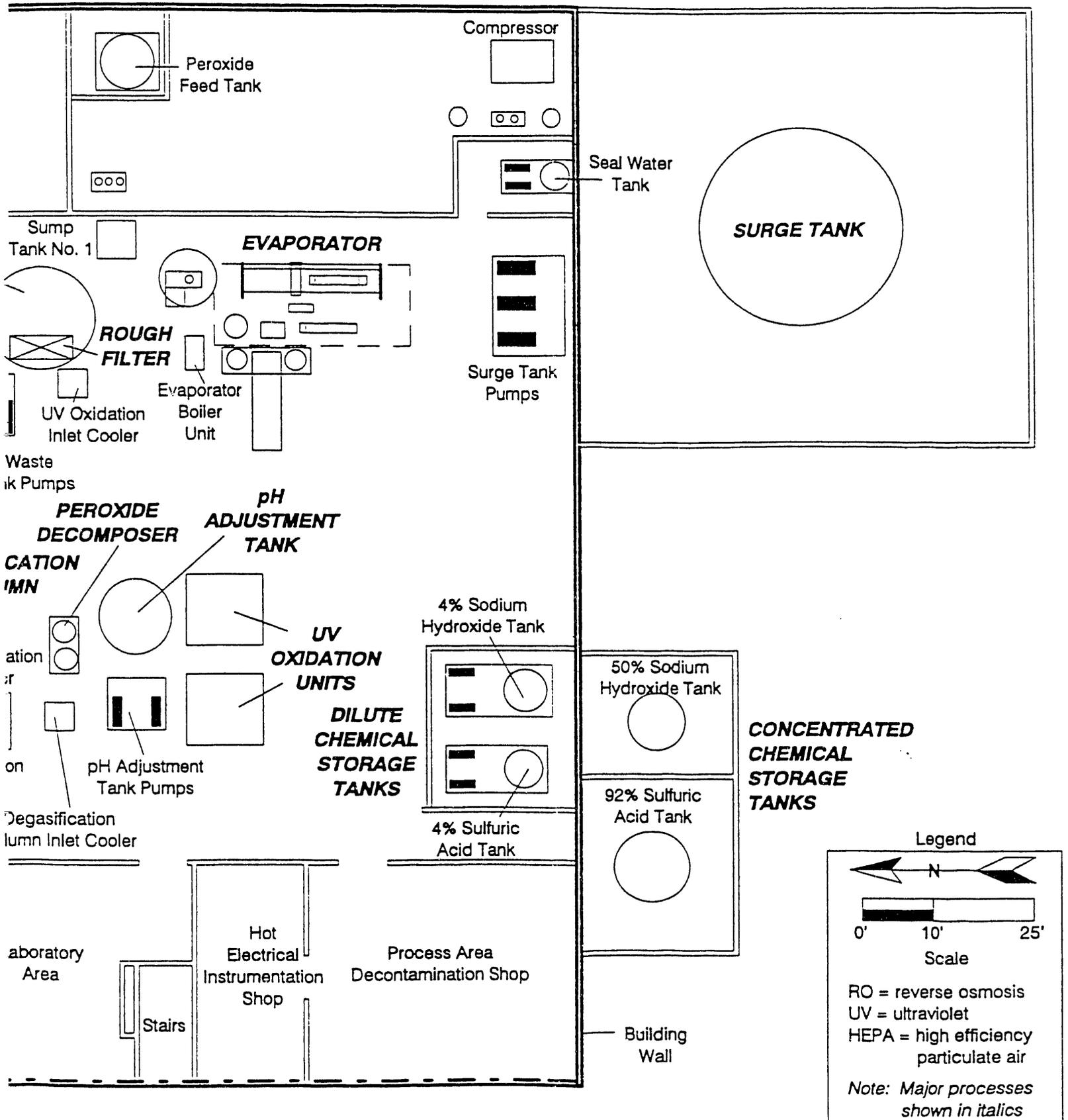
Waste water is piped to the ETF through two lines. One pipeline extends directly from the LERF to the surge tank at the ETF. The second pipeline extends to the ETF from the major elbow in the transfer piping between the 242-A Evaporator and the LERF. The ETF receives waste water for treatment in the surge tank. The waste water passes from the surge tank into the primary treatment train where the organic, inorganic, and radioactive constituents are removed from the waste water. Waste generated during the primary process passes into the secondary treatment train where the waste is processed and prepared for final transfer to an onsite TSD unit. The primary and secondary treatment trains are described in the following sections.



Source: Dwgs. H2-89029, H2-89033, H2-89162

Building continues

Figure B-1. Location of Treatment Units



200 Area Effluent Treatment Facility Process Area.

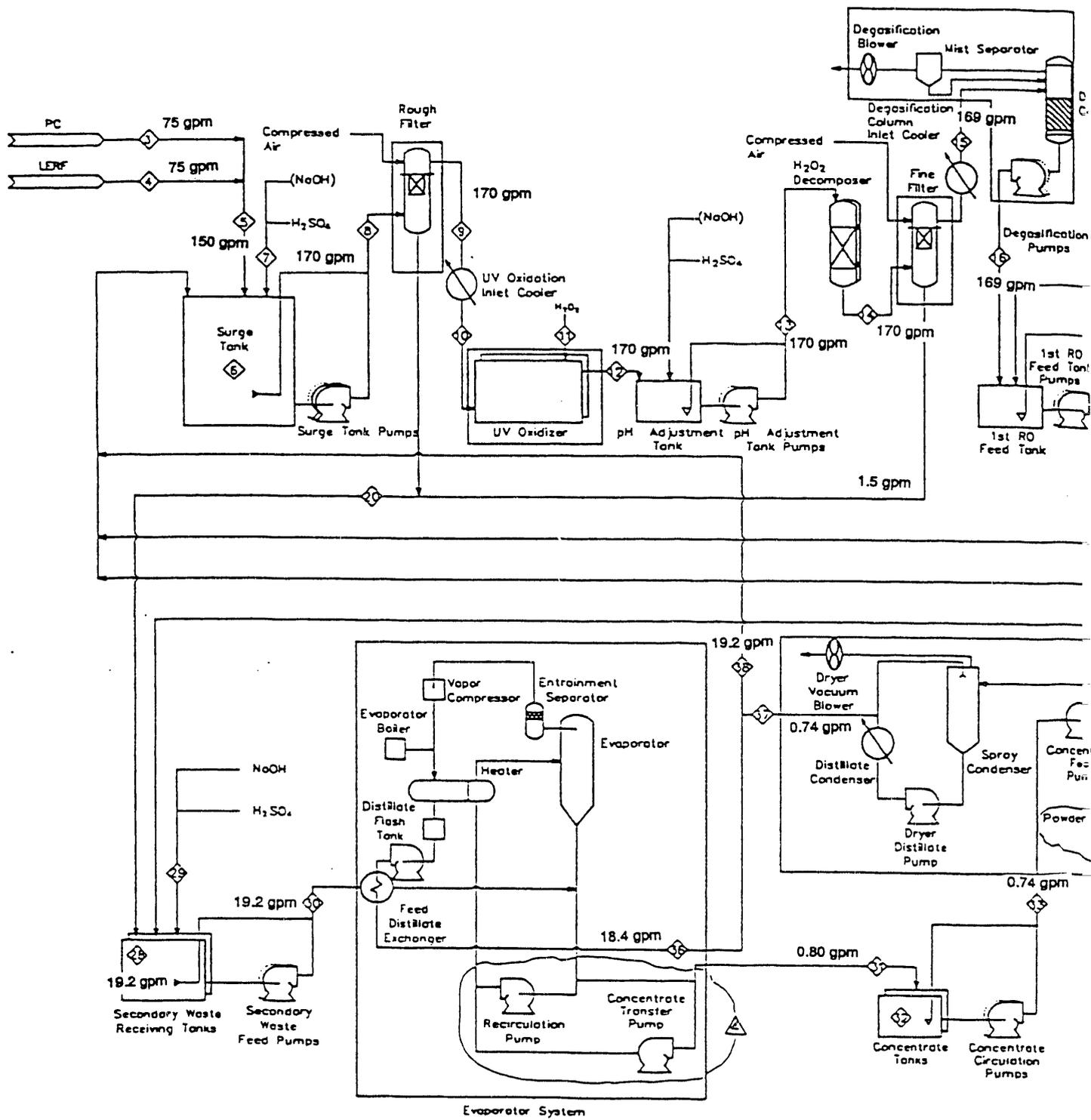
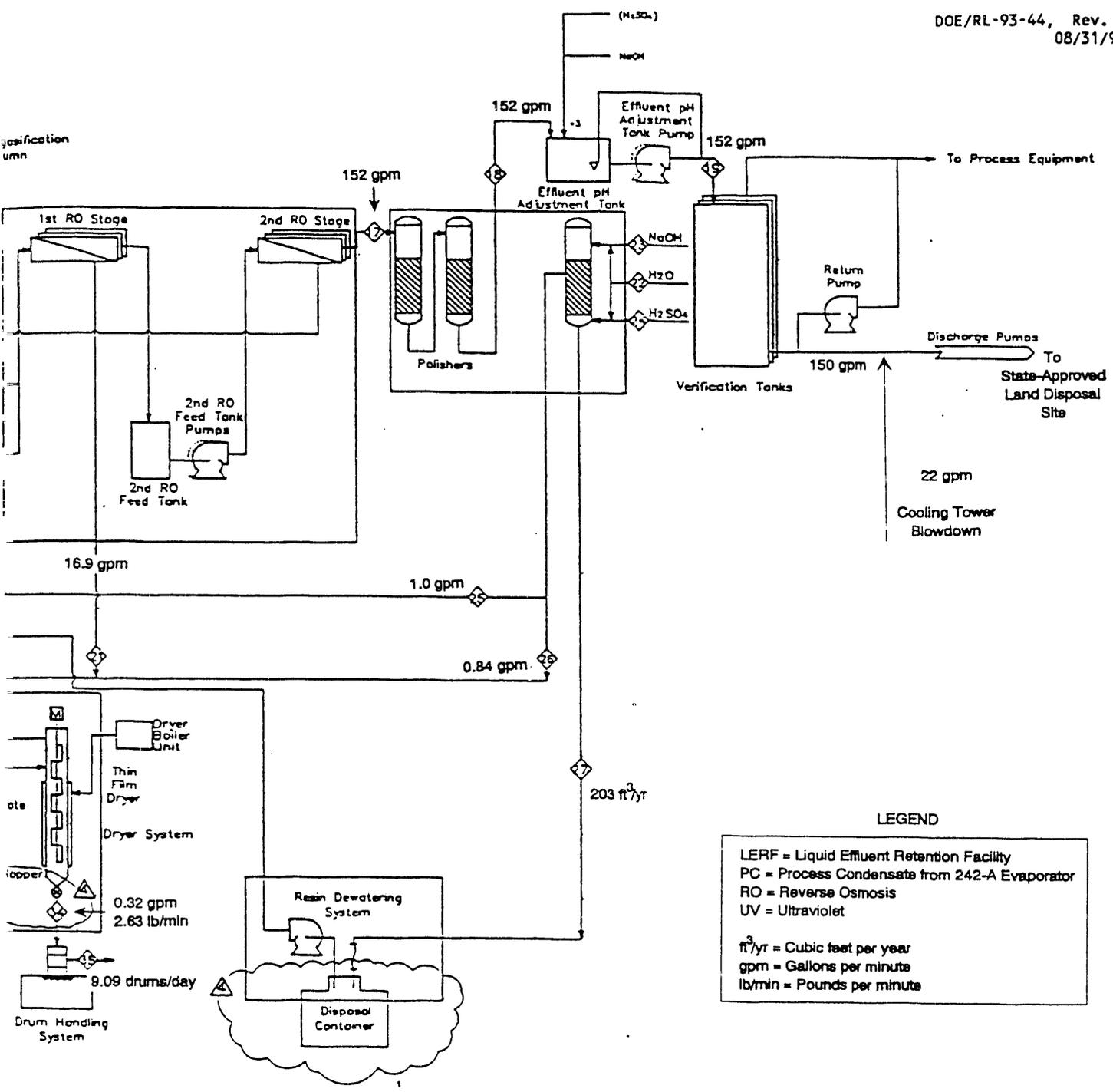


Figure B-2. 200 Area Effluent Treatment



LEGEND

LERF = Liquid Effluent Retention Facility
 PC = Process Condensate from 242-A Evaporator
 RO = Reverse Osmosis
 UV = Ultraviolet

ft³/yr = Cubic feet per year
 gpm = Gallons per minute
 lb/min = Pounds per minute



U.S. DEPARTMENT OF ENERGY	
BOX FIELD OFFICE, RICHLAND	
JOC CORPORATION	
PROCESS FLOW DIAGRAM	
DATE	NOV 18 1993
BY	F. SHERRE
NO.	H-2-88970
SCALE	AS SHOWN

reatment Facility Flow Diagram.

Table B-1. ETF Effluent Concentrations.

Parameter	ETF Effluent
pH	6.5-8.5
Inorganic Constituents (ppb) ^a	
Aluminum	7,000
Antimony	6
Arsenic	50
Barium	1,000
Beryllium	4
Cadmium	10
Chloride	200
Chromium	50
Copper	1,000
Cyanide	200
Fluoride	4,000
Iron	300
Lead	50
Manganese	50
Mercury	2
Nickel	100
Nitrate	44,268
Selenium	50
Silver	200
Sulfate	250,000
Vanadium	200
Zinc	5,000
Radionuclides (pCi/L) ^b	
Gross Alpha Radiation	2,500
Gross Beta Radiation	5,000
⁹⁰ Strontium	8
Tritium	24,000,000 ^c

Table B-1. ETF Effluent Concentrations. (cont.)

Parameter	ETF Effluent
Organic Constituents (ppb) ^a	
Acetone	4,000
Benzene	5
Benzyl alcohol	10,000
Carbon tetrachloride	150
Chloroform	70
Cresylic acid (cresols)	2,000
Di-n-octyl phthalate	700
Ethyl ether	7,000
Ethylbenzene	700
Isophorone	9
Methanol	20,000
Methylene chloride	50
Methyl ethyl ketone	2,000
Methyl isobutyl ketone (MIBK)	2,000
Naphthalene	1,000
2-Naphthylamine	10
N-Nitrosodimethylamine	10
Phenol	20,000
Pyridine	40
Styrene	100
Toluene	1,000
1,1,1-Trichloroethane	200
1,1,2-Trichloroethane	50
Xylenes (total)	10,000

a
b
c

ppb = parts per billion

pCi/L = picocuries per liter

Source: WHC 1989. Based on 83 samples with detectable levels of tritium.
Expected tritium values from 242-A Evaporator: Average = 5.6E+06 pCi/L;
90% Confidence Interval = 6.3E+06 pCi/L; Maximum = 2.4E+07 pCi/L.

Table B-2. Anticipated Cooling Tower Blowdown Concentrations.^a

Parameter	Blowdown Concentration ^b	Analytical Method	Detection Limit ^b
pH	6 - 9	---	---
Conductivity	900 μ S	NV	NV
Total Dissolved Solids	1.07x10 ⁶	EPA 160.1	3,000
Total Suspended Solids	42,000	EPA 160.2	3,000
BOD (5 day)	BDL	EPA 405.1	2,000
COD	400,000	EPA 410.4	7,000
Ammonia-N	420	EPA 350.2	10
TKN-N	NA	---	---
Nitrate-N	BDL	EPA 353.3/354.1	30
Ortho-Phosphate-P	BDL	EPA 365.2/365.3	10
Total Phosphate-P	300	EPA 365.2/365.4	10
Total oil and grease	NA	---	---
Calcium	108,000	EPA 200.7/SW6010, -TR	NV
Magnesium	BDL	EPA 200.7/SW6010, -TR	25
Sodium	500	EPA 200.7/SW6010, -TR	0.1
Potassium	BDL	EPA 200.7/SW6010, -TR	300
Chloride	16,000	EPA 325.3	1,800
Sulfate	124,000	EPA 375.4	1,000
Fluoride	600	EPA 340.2	100
Cadmium	BDL	EPA 213.2/SW7131, -TR	0.1
Chromium	BDL	EPA 200.7/SW6010, -TR	7
Lead	BDL	EPA 239.2/SW7421, -TR	0.8
Mercury	BDL	EPA 245.1/SW7470	0.2
Selenium	BDL	EPA 270.2/SW7740, -TR	0.8
Silver	BDL	EPA 270.2-TRM/272.2-T	0.2
Copper	BDL	EPA 200.7/SW6010, -TR	2

Table B-2. Anticipated Cooling Tower Blowdown Concentrations.^a (cont.)

Parameter	Blowdown Concentration ^b	Analytical Method	Detection Limit ^b
Iron	250	EPA 200.7/SW6010,-TR	10
Manganese	BDL	EPA 200.7/SW6010,-TR	25
Zinc	BDL	EPA 200.7/SW6010,-TR	2
Barium	160	EPA 200.7/SW6010,-TR	1.0
Total Coliform	3,000	SM 908A	2 MPN/dL

^a Source: maximum numbers were abstracted from WHC 1991b using the following assumptions:

- 1) Blowdown flow rate is 22 gal/min (83.8 L/min)
- 2) Blowdown concentration is six times the concentration of raw water constituents
- 3) Addition of the following chemicals to control corrosion, scaling, and biological growth: Na⁺ = 5.0 E+02 ppb; ClO⁻ = 5.0 E+02 ppb; SO₄⁻² = 5.8 E+04 ppb; and TRC²²³ = 1.2 E+04 ppb (Calgon proprietary chemical made of organophosphate polymer. TRC²²³ is a Calgon, Inc. trademark.)

^b Concentrations are in µg/L unless otherwise noted.

- NV = Data not available
 NA = Not analyzed
 BDL = Below detection limit
 ppb = parts per billion

2.0 PRIMARY TREATMENT TRAIN

The primary treatment train in the ETF receives waste water in the surge tank, processes the waste water, and discharges the treated waste water to the soil column. The primary treatment train consists of the following systems:

- Surge tank (pH adjustment)
- Coarse filtration
- Ultraviolet/Oxidation (UV/OX) system
- pH adjustment
- Hydrogen peroxide decomposer
- Fine filter
- Degasification
- Reverse Osmosis (RO) system
- Polisher Ion Exchange columns
- pH adjustment
- Verification tanks
- Cooling tower unit and blowdown.

2.1 SURGE TANK

The waste water enters the ETF at the surge tank, located outside the ETF Building on the south side. The surge tank also receives waste extracted by various systems within the primary treatment train, such as sumps, regeneration rinsing water from the polisher, and the distillate from the ETF evaporator and the thin film dryer.

The surge tank is insulated and the contents heated to prevent freezing. The pH of the contents is adjusted to about 6.0 by the metered addition of 92-weight percent sulfuric acid (H_2SO_4) or 50-weight percent sodium hydroxide (NaOH). The main purpose of pH control in the surge tank is to change free ammonia into ammonium ion to prevent ammonia from being discharged into the vessel ventilation system. This pH range also corresponds to the operation range for the UV/OX system. A titration analyzer is used to adjust and maintain the pH.

One of the three surge tank pumps circulates the contents, mixing the sulfuric acid or the sodium hydroxide and the waste water to a uniform pH. A second pump forces the pH adjusted waste water through the rough filter. The remaining pump serves as a spare.

2.2 COARSE FILTRATION

The 2-micron rough filter removes the larger particulates from the waste water. The solids accumulating on the filter element are backwashed to the secondary waste receiving tanks with pulses of compressed air, forcing water back through the filter. The backwash operation is started automatically by a rise in differential pressure across the filter. The backwash operation is accomplished in 5 minutes, at an expected frequency of less than once a week.

The filter medium is expected to operate for at least 1 year between replacements. The filtered waste water then passes through a plate cooler, to reduce the temperature to less than 100 °F (38 °C), before entering the UV/OX chambers.

2.3 ULTRAVIOLET OXIDATION SYSTEM

The purpose of the UV/OX system is to break down the organic compounds in the waste water, producing carbon dioxide, water, and inorganic ions. The UV/OX system uses the photochemical reaction of UV light on hydrogen peroxide to decompose the organic constituents.

Hydrogen peroxide is mixed with the waste water, and then exposed to UV light. The photochemical reaction of UV light and hydrogen peroxide causes the formation of hydroxyl radicals and other reactive species that cause the decomposition of organics.

Organic destruction is accomplished in two UV/OX units. During the UV/OX process, the waste water passes through mixing and dosing chambers in turn within the reaction chamber where the hydrogen peroxide is added.

In each reaction chamber, a high-intensity UV lamp is covered by a quartz tube with a tube-cleaning device. Cleaning of the quartz tube exteriors and reaction chamber interiors is performed automatically by rubber rings that slide across the surface of the quartz tubes. This cleaning process occurs in a stand-by mode as necessary without process shutdown.

The UV/OX system is equipped with automatic shutdown should the following circumstances occur: overpressurization, moisture in lamp end enclosure, high temperature, low water, failure of the hydrogen peroxide storage/feed module, high lamp drive enclosure temperature, and open access door. Also provided is a level sensor to protect the UV lamps against the risk of exposure to air. Should the liquid levels fall low enough to expose the lamps to air, the UV lamps are shut down automatically. After shutdown, the UV lamps cannot be restarted until the lamp temperature decreases to a specified level. After UV/OX, the waste water is received in the pH adjustment tank.

2.4 pH ADJUSTMENT

The pH adjustment chemically alters the ammonia and carbonate ions in the waste water. The waste water pH is adjusted with a solution of 4 weight percent sulfuric acid or 4-weight percent sodium hydroxide to a pH of approximately 4.0. In this acidic solution, ammonia is converted to an ammonium ion specie that is removed downstream by the RO system. Acidification also changes the chemistry of the carbonate ion, causing it to form carbon dioxide, a gas with low solubility that can be removed from the waste water.

The pH adjustment tank has two pumps, one of which operates as a spare. A constant liquid level is maintained in the tank to facilitate an even and constant pH of the waste water. The waste water is pumped next through the hydrogen peroxide decomposer.

2.5 HYDROGEN PEROXIDE DECOMPOSER

The purpose of the hydrogen peroxide decomposer is to reduce the amount of hydrogen peroxide left in the waste water from the UV/OX system. The hydrogen peroxide injected for the UV/OX system is not completely consumed in the process of organic destruction, leaving approximately 100 to 200 parts per million in the waste water. A strong oxidant, hydrogen peroxide could harm the membranes in the RO system. Therefore, the waste water is sent through a simple packed column that decomposes the hydrogen peroxide into water and oxygen.

The residual hydrogen peroxide is decomposed by flowing through one of two vessels containing packed beds of catalyst. A safety relief valve on each vessel opens to relieve excessive system pressure to sump tank No. 2. The break down of hydrogen peroxide forms water and oxygen as the waste water flows through the catalyst bed. The gas generated by the decomposition of the hydrogen peroxide accumulates at the top of the hydrogen peroxide decomposer column and is discharged to the sump tank, which is vented to the vessel offgas system. The waste water discharge flows from the decomposer to the fine filter.

2.6 FINE FILTRATION

The purpose of the fine filter is to remove suspended solids larger than approximately 0.5 micron. The filter is designed to operate at up to 150 pounds per square inch gauge.

Differential pressure between the inlet and outlet of the fine filter is monitored. When the differential pressure reaches a predetermined value, the filter goes into the backwash operation automatically. Solids accumulating on the filter element are backwashed to the secondary waste receiving tank with pulses of compressed air that force water back through the filter. The backwashing operation is expected to last 5 minutes and occur less than once a week. The filter is expected to operate for at least 1 year before replacement. The waste water discharged through the filter then undergoes degasification.

2.7 DEGASIFICATION

The function of the degasification column is to remove the carbon dioxide formed when the waste water was acidified in the pH adjustment tank. Carbonate ions are removed to prevent increasing the contaminant loading to the RO system and other downstream ETF processes (i.e., IX, evaporation, and drying).

A plate-type heat exchanger is provided for cooling the waste water fed to the degasification column. The carbon dioxide-laden waste water passes down through a packed bed at a slight vacuum [approximately 2 inches of water (0.051 kilograms per square centimeter)] with air blowing up through the packed bed. Because of the low solubility of the carbon dioxide, contact with the countercurrent air purges the waste water of the carbon dioxide molecules. Offgas from the degasification column is discharged by the degasification blower to the vessel offgas system.

Extremely low pressure developed by the column blower that could compromise column integrity is relieved by a pressure relief safety valve. The column liquid level is controlled automatically. The degasified waste water is fed to the first stage RO feed tank by the degasification pump.

2.8 REVERSE OSMOSIS SYSTEM

The function of the RO system is to reduce the concentration of dissolved solids, radionuclides, and any remaining large molecular weight organic materials in the waste water.

Reverse osmosis is a process that uses pressure to force clean water molecules through special membranes while keeping the larger-molecule contaminants within the membranes. The waste water passes through two or more of the pressure vessels containing the RO membranes before going to the next system.

The membranes are of a composite polyamide type that are nearly impermeable to ammonium ions. Contaminants, including the ammonium, are removed from the waste water as the fluid moves through the membranes. The cleaned waste water discharged from the system is referred to as the permeate, while the contaminated waste is called the reject stream, concentrate, retentate, or brine.

The RO system used at the ETF enhances contaminant removal by using two stages (instead of one) and by a crossflow pattern through the membrane modules. The solute concentrate from the first stage RO membranes are collected in the secondary waste receiving tanks, and the permeate (the waste water that has passed through the membranes) is routed to the second stage RO for additional treatment before being discharged to the polisher. Concentrate from the second stage RO is routed back to the first stage RO feed tank. Note that the complete RO system is designed with 50 percent excess capacity (i.e., one third of the system is always in a cleaning or standby mode, while the other two thirds are in operation).

2.9 POLISHER

The purpose of the polisher is for final removal of residual dissolved solids from the waste water.

The discharge permeate from the second RO stage is pumped to the polisher, which consists of three IX columns, each with mixed beds of cation and anion resin. Two of the columns operate while the third is regenerated, or cleaned. The IX columns operate in series, meaning waste water flows down through one IX column and then down through the second column.

When the capacity of the resin in the first of the two online columns is exceeded, as detected by an increase in the conductivity of the IX column effluent, the column is removed from service for regeneration. The third unit, which was offline, is placed in service (to become the second of two on-line columns).

The column removed from service is prepared for regeneration by separating the resins into a layer of anion resin and a layer of cation resin. The resins are separated by an upflow of clean water from the verification tank, which floats the lighter anion resin to the top of the resin bed. The contaminants in the cation resin is eluted with dilute (4 weight percent) sulfuric acid and the anion resin with dilute (4 weight percent) sodium hydroxide. The resulting concentrated (salt-loaded) regeneration waste streams are collected in the secondary waste receiving tanks. Thereafter, a dilute rinsing of both the anion and cation resins occurs, producing a solution (rinse waste) that is collected in the surge tank. Compressed air is used to remix the cation and anion bed after regeneration is complete.

Eventually, the IX resins become exhausted so that further regeneration is useless. When that happens, the spent resins are slurried, or washed, with water from the IX vessels into a disposal container. The container is sealed with a special lid that allows the following: spent resin to go in the containers, resin dewatering and water removal, and television monitoring of the resin and water levels within the container. Slurried resin enters the container through the lid to displace air that is removed by a blower. The air flows through an entrainment separator to remove water drops and then flows through a high-efficiency particulate air (HEPA) filter into the vessel ventilation system. Liquid is removed from the container by a pump, and sent to the surge tank as required to remove water from the resin.

The IX vessels are equipped with visual inspection ports that allow observation during resin separation, bed expansion, and operation. Each vessel outlet is monitored for conductivity and pH to prevent overloading of the resin beds between regeneration cycles. Automatically operated valves recycle poor quality effluent back to the surge tank, if needed, to prevent contamination of the verification tanks. Resin traps and a resin strainer prevent resin loss into the verification tanks. The waste water discharged from the polisher system is piped to the effluent pH adjustment tank.

2.10 pH ADJUSTMENT

This final pH adjustment tank neutralizes the waste water for discharge. A small flow of dilute sulfuric acid or dilute sodium hydroxide is used to

adjust the pH to between 6.5 and 8.5. An eductor in the tank ensures adequate mixing of the added chemicals. The pH of the waste water is monitored and controlled continuously.

The liquid level in the effluent pH adjustment tank is kept at a constant level to facilitate the pH adjustment process. A signal from the tank liquid level sensor transmitted to the flow control valve on the tank outlet adjusts the level in the tank by causing a corresponding increase or decrease in the flow to the verification tanks. Should an overflow occur, the waste water is collected in sump tank No. 2.

2.11 VERIFICATION TANKS

Three verification tanks hold the treated waste water while a laboratory analysis is performed to determine if treatment is complete. The verification sample is taken by a flow proportional sampler as the treated waste water is pumped from the effluent pH adjustment tank to the verification tanks. The treated waste water can be pumped back into the treatment train, if the waste water does not meet the Washington State waste discharge limits.

The three verification tanks alternate between three operating modes: receiving treated waste water, holding treated waste water during laboratory analysis and verification, or discharging verified waste water.

All of the verification tanks have a liquid level sensor, a liquid level indicator, and a high level alarm. The verification tank system includes three pumps: one delivers treated waste water to the SALDS, one pump circulates the treated waste water through tank eductors and serves as a water supply to various processes within the ETF, and one pump is a spare on standby.

2.12 COOLING TOWER UNIT AND BLOWDOWN

Two ETF processes (UV/OX and RO) have upper temperature limitations. Consequently, the ETF design incorporates heat exchangers and a cooling tower unit to control waste water temperatures.

Blowdown from the cooling tower is discharged to the SALDS through the same pipeline that carries the ETF treated waste water. The blowdown is combined with the waste water flow downstream of the verification tanks. Either one or both of the waste streams can flow down the pipeline to the SALDS at any one time. The blowdown results from an average of six cycles of concentration and averages up to 22 gal/min (5.8 L/min). Raw water is used in the cooling systems. Corrosion and scale inhibitors are added during routine operations.

3.0 SECONDARY TREATMENT TRAIN

The following waste, generated by the primary treatment train systems, is processed in the secondary treatment train:

- Concentrate from the first RO stage
- Backwash from the rough and fine filters
- Regeneration waste from the polisher.

The secondary treatment train collects, concentrates, dries, and packages the waste in 55-gallon (208-liter) steel containers. The secondary treatment train consists of the following systems:

- Secondary waste receiving tanks
- ETF evaporator
- Concentrate receiving tanks
- Thin film dryer
- Container handling system.

3.1 SECONDARY WASTE RECEIVING TANKS

Secondary waste is collected in two secondary waste receiving tanks. The tanks alternate between receiving the secondary waste generated, and serving as a feed tank for the ETF evaporator feed tank. The rising liquid in the tank activates a high-level switch that diverts the flow to the other tank. Each secondary waste receiving tank has a pump on the tank outlet that can be used to circulate the tank contents or to supply feed to the ETF evaporator. A high-level alarm indicates an abnormal situation.

Chemical pH adjustment of the tank contents is accomplished by the controlled addition of dilute sulfuric acid or dilute sodium hydroxide. The pH is adjusted to approximately 6.0 for corrosion control of the ETF evaporator and thin film dryer equipment and to minimize any ammonia generation.

3.2 200 AREA EFFLUENT TREATMENT FACILITY EVAPORATOR

The purpose of the ETF evaporator is to reduce the volume of waste before drying. Feed from the secondary waste receiving tank is pumped through a preheater (feed/distillate exchanger) to a forced circulation evaporator loop. In the evaporator loop, concentrate is produced as water is driven off overhead.

Water vapor in the overheads from the ETF evaporator passes through an entrainment separator, which removes entrained water droplets and solid particulates, returning them to the evaporator loop. The cleaned vapor is condensed and fed to the distillate flush tank. Some condensate from this tank is sprayed into the entrainment separator to scrub out particulates. Finally, the condensate is cycled back to the surge tank for further processing.

3.3 CONCENTRATE RECEIVING TANKS

The ETF evaporator concentrate is pumped to the two concentrate tanks. These concentrate tanks function alternately between concentrate receiver and feed tank for the thin film dryer. The rising liquid level in the tank receiving concentrate actuates a high-level switch that diverts the flow to the other concentrate tank. Should the tank fail to divert the flow to the alternate tank, the resulting overflow would go to sump tank No. 1.

Both concentrate tanks have a circulation pump on the tank outlet that can be used to circulate the tank contents or to supply feed to the thin film dryer via the concentrate feed pump. Dilute sulfuric acid and dilute sodium hydroxide can be added to the tanks for pH adjustment. Homogenization by an eductor and pH adjustment (if necessary) is completed before the tank is filled and enters the feed mode. The concentrate tank circulation pump feeds the concentrate feed pump, which in turn supplies the thin film dryer.

A sample from the recirculation line is taken to characterize the tank contents, which is used for container content characterization. This provides complete characterization of the container contents and minimizes exposure to workers.

The temperature of the concentrate is increased by a steam preheater to enhance the operation of the thin film dryer.

3.4 THIN FILM DRYER

The purpose of the thin film dryer is to dry the concentrated secondary waste into a powder. Concentrate is distributed on the inner cylinder of the thin film dryer by wiper blades that rotate on a shaft centered in the cylinder. The shaft is driven by an electric motor. The concentrate is dried by steam heat introduced into an annular space (steam jacket) between the outer shell and the inner cylinder. Steam heat transferred across the inner cylinder wall heats the concentrate as it flows down the inside surface. Heating is controlled by regulating the steam pressure to the steam jacket. Condensate from the steam is returned to a steam boiler dedicated to the dryer. A safety valve on the thin film dryer steam and vapor lines vent independently to sump tank No. 1.

Overhead vapor released by the drying of the concentrate is condensed in a spray condenser. The condensed vapor forms a distillate by direct contact within a spray condenser. The distillate flow is circulated by a dryer distillate pump. Excess heat is removed from the distillate by a water-cooled heat exchanger. Part of the distillate is circulated back to the condenser spray nozzles. The remaining distillate is pumped to the surge tank. Any noncondensable vapors and particulates from the spray condenser are exhausted by a vacuum blower to the vessel ventilation system.

The concentrate dries into a film as it flows down the length of the dryer. The dried film, or powder, is scraped off the dryer cylinder by blades attached to the rotating shaft. The powder is funnelled through a cone-shaped powder hopper at the bottom of the dryer and into a rotary valve that feeds the powder into a container. An air-driven vibrator mounted on the cone section assists powder movement out of the thin film dryer into a 55-gallon (208-liter) container.

3.5 CONTAINER HANDLING SYSTEM

Empty containers with liners and lids are removed from the empty-container storage and placed on a conveyor. The containers are moved into the container filling area after passing through an air lock. An empty container located under the powder port of the thin film dryer is raised into position by an elevator. The container is sealed to the thin film dryer and the rotary valve begins the transfer of powder out of the thin film dryer into the empty container. Air displaced from the container is vented to the extrainment separator attached to the ETF evaporator that exhausts to the vessel ventilation system.

The container is filled to a predetermined weight, then moved along the conveyor to the smear station airlock. At the smear station airlock, the container is moved onto the discharge conveyor by remote control. The airlock is opened and the smear sample (surface wipe) is taken and the radionuclide contamination level is counted. If the container has contaminated material on the outside, the container is moved to the washdown station where the container is washed with treated water from the verification tanks. The container wash water drains to sump tank No. 1. The washed container is air-dried and retested. Filled containers that pass the smear test are labeled, placed on pallets, and moved by forklift to the filled storage area at the ETF pending transfer to the Central Waste Complex.

ATTACHMENT C

STATE-APPROVED LAND DISPOSAL SITE

ATTACHMENT C

STATE-APPROVED LAND DISPOSAL SITE

1.0 INTRODUCTION AND LEGAL DESCRIPTION

The treated waste water from the 200 Area Effluent Treatment Facility (ETF) will be disposed to the soil column at the State-Approved Land Disposal Site (SALDS). An average flow of 150 gal/min (568 L/min) of ETF treated waste water and 22 gal/min (83 L/min) of ETF cooling tower blowdown will be piped to the SALDS, which is located north of 200 West Area. The combined flow of the two streams will be discharged to a crib (i.e., a covered structure with a bottom open to the ground) and infiltrate into the soil (WHC 1993b).

Disposal of the treated waste water from the ETF at the SALDS was selected from an evaluation of the following five candidate disposal alternatives:

Soil column disposal, including crib and pond disposal options

Discharge to the Columbia River

Evaporation, both solar and mechanical

Beneficial use options, including recycling and irrigation

No action.

The ranking process incorporated weighting factors to demonstrate the relative importance of the following criteria: (1) minimizing radiation exposure as low as reasonably achievable (ALARA), (2) environmental impacts, (3) permitting requirements, (3) capital and operating costs, and (4) implementation (WHC 1993b).

The highest total scores (most desirable option) were assigned to the soil column alternative. The crib and pond disposal scores for ALARA were higher (less risk) than for any of the other alternatives because the potential for radiation exposure is significantly lower for the soil column disposal system. Crib disposal ranked higher than pond disposal because the pond would provide a surface area with a potential for radiation exposure to animals (environmental impact criterion), and more effluent would evaporate from a pond (ALARA criterion). Because of extensive characterization requirements and the complexities associated with permitting, crib disposal was ranked lower (less desirable) than some other alternatives for permitting and implementation criteria.

The third highest ranked alternative was mechanical evaporation. This disposal alternative would cost considerably more than other disposal alternatives and would result in comparatively higher offsite exposure levels. Nonetheless, it was given comparatively high scores for environmental impact, permitting, and ease/feasibility of implementation criteria (WHC 1993b).

The selected disposal alternative was the crib. The disposal area will be designated as the SALDS when the State Waste Discharge Permit is issued (WHC 1993b).

The SALDS is located approximately 5.9 miles (3.7 kilometers) west of the ETF, north of the 200 West Area. The SALDS is located outside of the 200 West fenced boundary, approximately 1,200 feet (366 meters) north of 27th Street, and approximately 900 feet (274 meters) east of Dayton Avenue. The SALDS operations area is bounded by the following Hanford coordinates: N47900, W77000; and N48075, W76880 (Section 36 of T13N, R27E) (Figure C-1). The area of waste water infiltration is approximately 110 feet (34 meters) by 200 feet (61 meters). This property is currently owned by the U.S. Government, and the Department of Energy has tenancy. Thus, no contractual agreements are needed with other land owners.

This location was selected from a list of seven potential sites. Each site was evaluated on a set of determining (go/no go) criteria and a set of engineering criteria. The determining criteria included the following:

Sufficient land area and infiltration capacity to allow infiltration at the anticipated average flow rate

No unacceptable impacts on any identified RCRA or CERCLA site

No unacceptable impact on cultural, historical, or archeological resources

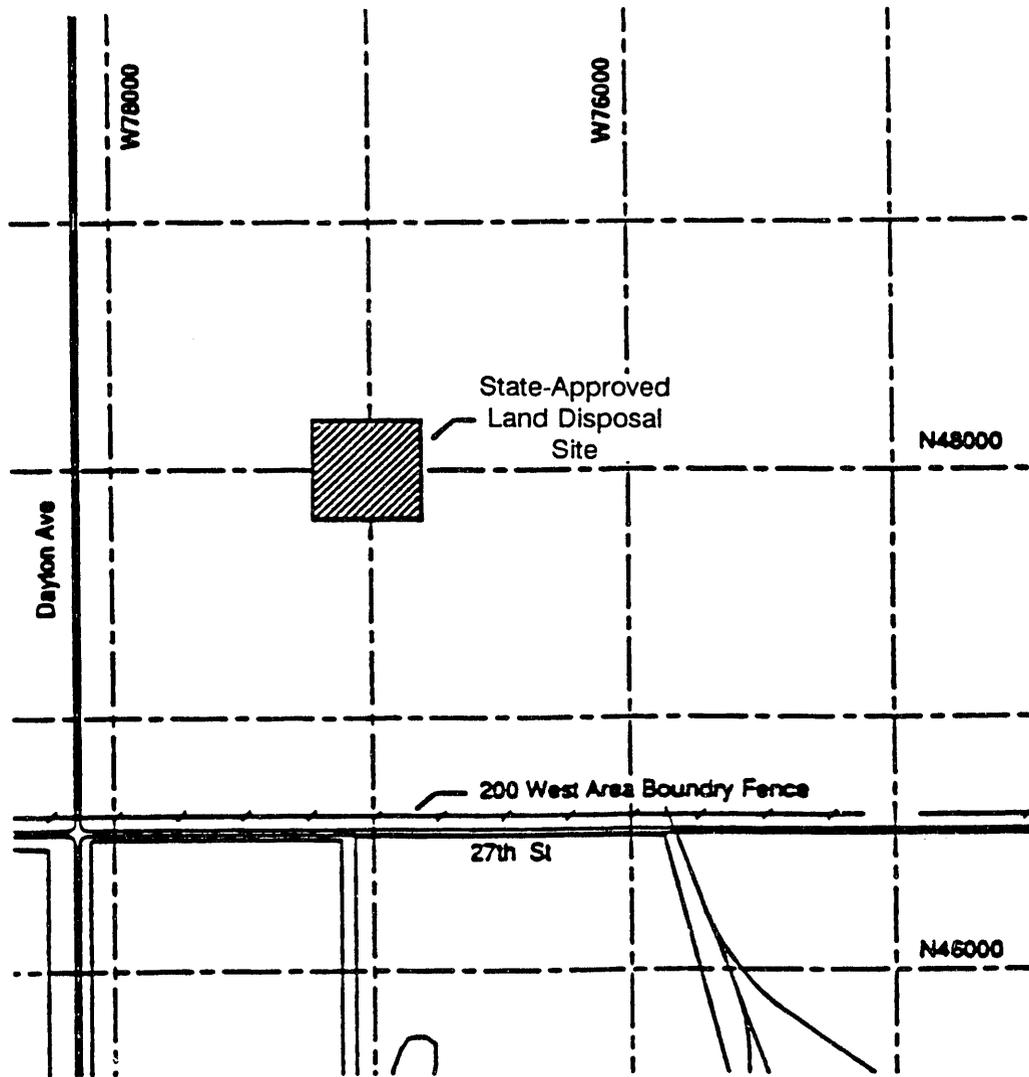
No unacceptable impact on endemic threatened or endangered plant or animal species

No land use conflicts (WHC 1993b).

The engineering criteria included the following: (1) health and safety, (2) environmental impact, (3) operational impact, and (4) land use. Each of these criteria was assigned a numerical weighting factor (WHC 1993b).

2.0 LOCATIONAL INFORMATION

Figure C-2 provides the locational information requested in Section H.3 of the permit application. No streets or roads are located within 500 feet of the site. No water supply wells, surface water drainage systems, or surface



Source: WHC (1993b)

Figure C-1. Location of State-Approved Land Disposal Site on Hanford Grid.

water diversions are located within 500 feet of the site. No drainfields, dry wells, or abandoned wells are located within 500 feet of the site. One monitoring well has been installed and an additional borehole drilled at the site; these are discussed in Section 3.0. Land uses within 1,500 feet (0.457 km) include the northernmost processing areas within the 200 West Area. A railroad line is located within 1,000 feet (305 m) of the site. A number of monitoring wells have been installed in the 200 West Area as depicted in Figure C-2.

3.0 HYDROGEOLOGY AND SOILS

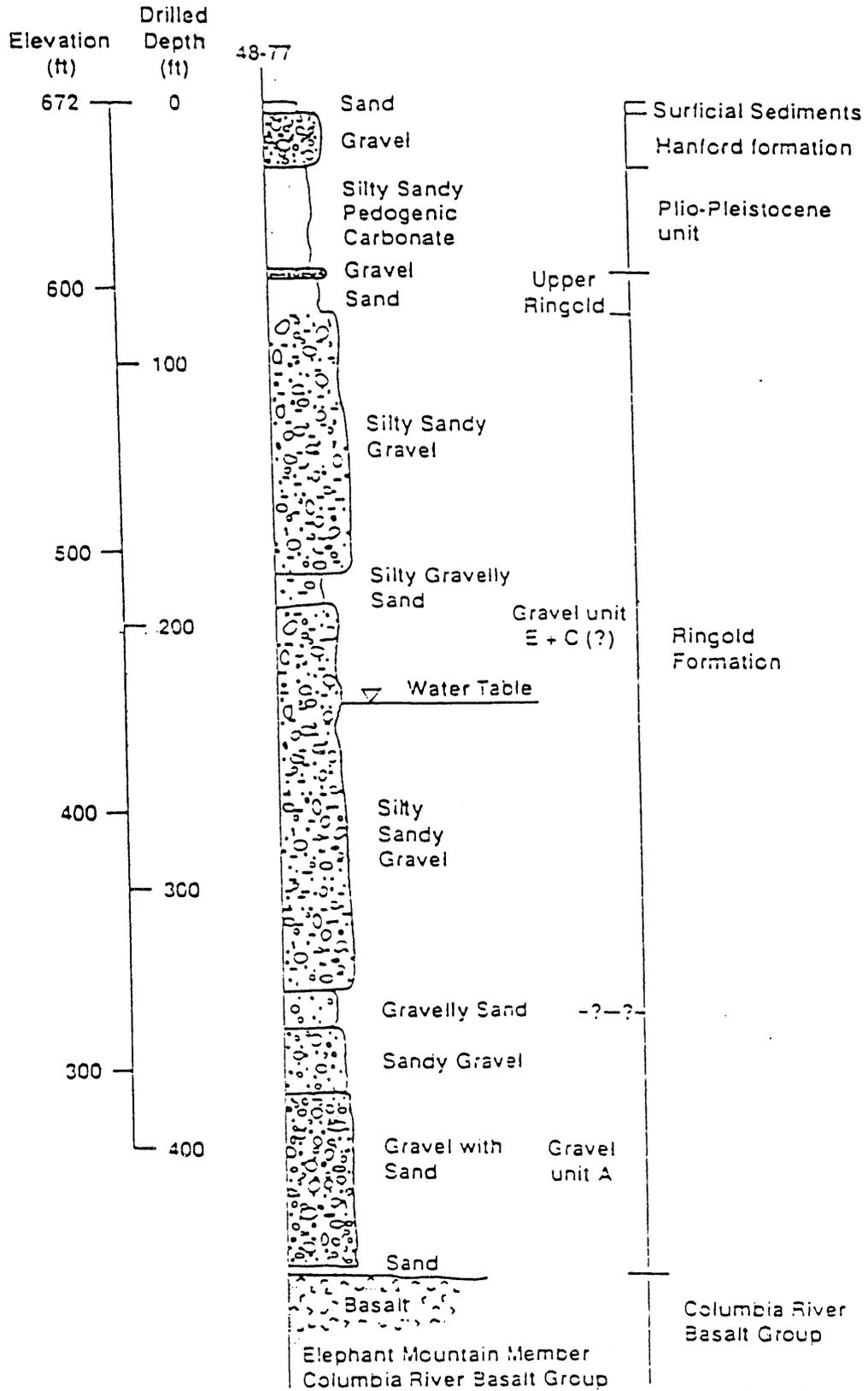
3.1 STRATIGRAPHY

Two boreholes were drilled and a well was installed in the second borehole at the SALDS location and reported in the *Characterization Report, C-018H Soil Column Disposal Siting Evaluation* (WHC 1993a). The first, borehole 699-48-77B, was drilled to a depth of 60 feet below ground surface (bgs), but was abandoned because it was drilled off-center. The second, well 699-48-77A, is located a few feet east of the first borehole. This borehole was drilled to a depth of 455 feet bgs using the cable-tool drilling method and core barrel sample recovery, where the Elephant Mountain Member of the Columbia River Basalt Group was penetrated. The well log information for well 699-48-77A and borehole 699-48-77B (0 to 60 feet bgs) are summarized in Figure C-3. A copy of the borehole log is provided at the end of Attachment C. Well 699-48-77A was completed as a RCRA groundwater monitoring well with a 10-slot, 20-foot (6.1-meter) long stainless steel screen installed between 212.4 and 232.4 feet bgs. Soil samples were collected during drilling for analyses to determine chemical and physical properties.

The stratigraphy between the ground surface and the water table is summarized as follows (WHC 1993a):

Hanford Formation. The Hanford formation is approximately 23 feet thick at the borehole site and consists predominantly of open-framework gravels with a sandy matrix typical of deposits of the gravel dominated facies. The formation shows little lithologic variation in the area of the proposed site. A thin silt lens occurs at the base of the gravel sequence above the Plio-Pleistocene and early Palouse interval. The Hanford formation thickens to the north and south of the site.

Plio-Pleistocene Unit and Early Palouse Soil. The combined thickness of the Plio-Pleistocene unit and early Palouse soil is approximately 42 feet, with the depth interval ranging from 23 feet to 65 feet bgs. The upper portion probably correlates to the early Palouse soil, but because of the method of drilling, no



Source: WHC (1993a)

H9208012.5

Figure C-3. Stratigraphic Units at Well 699-77A.

attempt was made to separate the early Palouse from the Plio-Pleistocene unit. The combined Plio-Pleistocene and early Palouse interval consists of the following: (1) interfingering carbonate-cemented silt, (2) sand, (3) gravel, and (4) carbonate-poor silt and sand. Thin pedogenic calcium lenses occur throughout the unit. Some cemented sands occur in the unit as well.

Ringold Formation. The Ringold Formation is approximately 390 feet thick in the borehole. The formation is dominated by gravel sequences which begin at 65 feet bgs and extend to the top of the Columbia River Basalt Group at 455 feet bgs. A major cataclysmic flood channelway is incised into the Ringold Formation which occurs approximately one-half mile north of the disposal site. The channelway, a result of erosion during a cataclysmic flood event, penetrates the Plio-Pleistocene and early Palouse interval, the upper Ringold, and a large portion of the Ringold E unit (Figure C-3). The channelway is filled with approximately 150 feet of Hanford formation gravel-dominated deposits. The exact position of the erosional channelway edge is not known because no boreholes penetrate deep enough to encounter the edge.

The sandy sequence that occurs between the base of the Plio-Pleistocene and early Palouse interval (65 feet bgs) and the top of the uppermost Ringold gravels (unit E) (83 feet bgs) at the site is interpreted to be erosional remnants of the upper Ringold unit. The Plio-Pleistocene and the early Palouse strata pinch out to the north, west, and east of the site. The upper unit extends to the south into the northern part of the 200 West Area.

The upper unit quickly grades downward into the gravels of unit E between 83 and 87 feet bgs. These gravels extend to a depth of 305 feet bgs with silt content increasing below 170 feet bgs. The next 40 feet (315 to 355 feet bgs) consists largely of sand with a significant gravel and silt component. These deposits are underlain by 40 feet (355 to 395 feet bgs) of sandy gravels that in turn overlie 57 feet (395 to 452 feet bgs) of gravels containing only minor amounts of sand. The base of the Ringold Formation is marked by a thin sandy unit (3 feet) overlying the basalt.

The lower mud sequence found south of the borehole is not present at the site and is interpreted to pinch out to the south. With the lower mud sequence absent, gravel unit E directly overlies gravel unit A, making differentiation between the two units impossible. However, if the top of unit A is projected towards the site from borehole 299-W6-1 (see geologic cross-section, Figure C-4), it would occur near the top of the sand-poor gravels at 395 feet bgs. Consequently much of the lower 60 feet of the Ringold section at the site may be part of gravel unit A.

Surface soils in the area of the SALDS are predominantly loamy sand and sandy loam (Figure C-5). The soils map indicates that Burbank Loamy Sand predominates in the immediate vicinity of the site. Under the Unified Classification System, this soil is classified as a medium sand. The soils to the southwest, north and northeast of the site are described as Ephrata Sandy Loam which is classified as medium sand to medium loam.

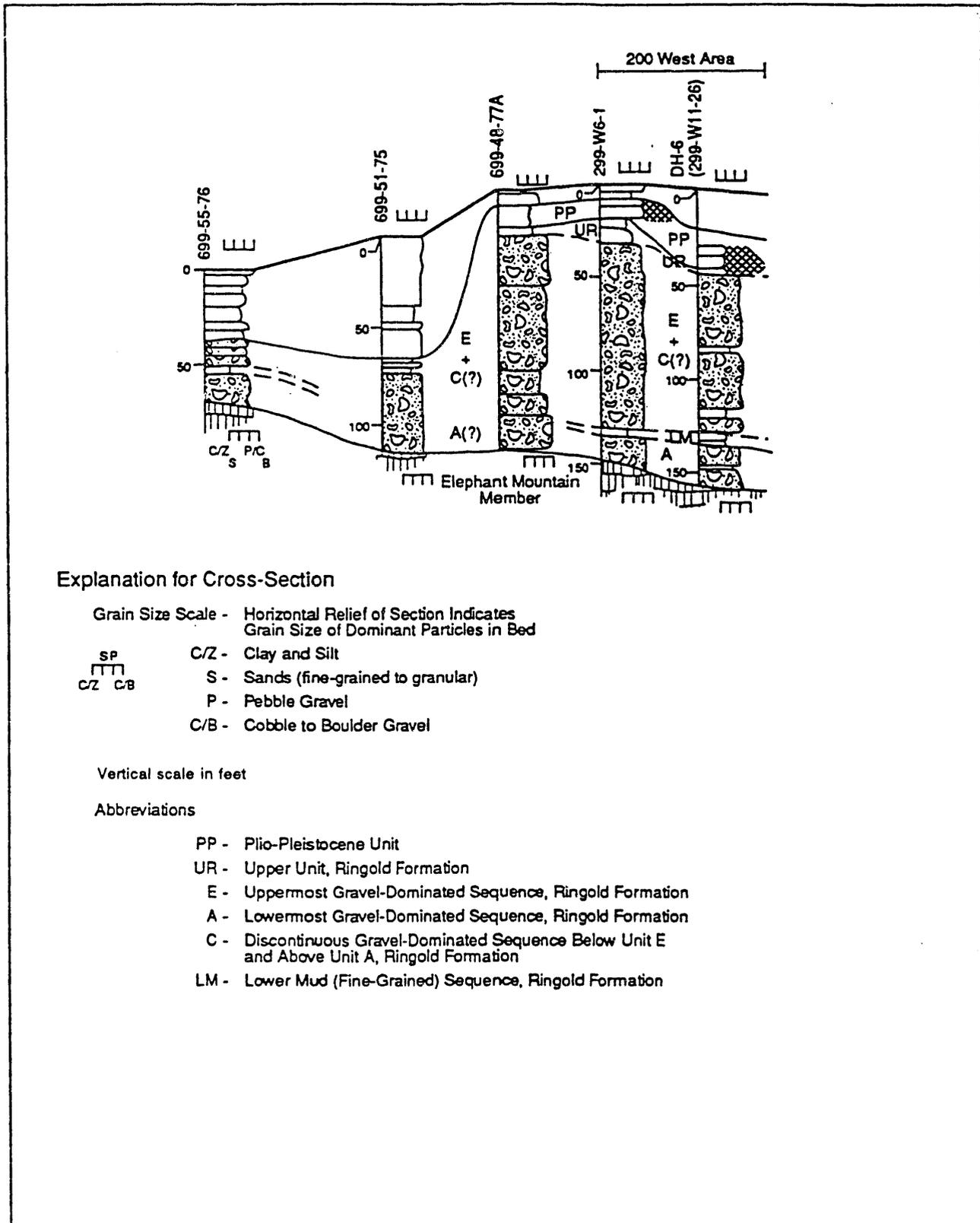
3.2 SOIL CHEMISTRY

Soil samples were taken at depth ranges and analyzed for the following: (1) metals, (2) anions and cations, (3) radionuclides, (4) volatile organics, (5) semivolatile organics, (6) pesticides, and (7) polychlorinated biphenyls (PCBs). The inorganic and radionuclide data are presented in Table C-1.

The concentrations of organic constituents were notably low. At a depth between 68.5 and 70 feet bgs, two volatile organic constituents were identified. These were 2-butanone (methyl ethyl ketone) and 4-methyl-2-pentanone (methyl isobutyl ketone) at concentrations of 27 and 130 micrograms/kilogram ($\mu\text{g}/\text{kg}$), respectively. These concentrations are well below Model Toxics Control Act Cleanup Regulation Method B cleanup standards (Washington Administrative Code [WAC] 173-340-720(3)). All pesticides and PCBs were below the limits of detection. The concentrations of semivolatile compounds were at or near the detection limits, except for trace concentrations of benzoic acid and phthalates that were reported for several samples. The compound 4-hydroxy-4-methyl-2-pentanone was reported as a tentatively identified compound, but was also identified in the field blank. Carboxylic acids were also tentatively identified compounds and are potential natural constituents of the soils (WHC 1993a).

3.3 HYDROGEOLOGY

The multiaquifer system within the Pasco Basin has been conceptualized as consisting of the following four primary units: (1) suprabasalt sediment of the Hanford and Ringold formations, (2) Saddle Mountain Basalt, (3) Wanapum Basalt, and (4) Grande Ronde Basalt. Groundwater reportedly flows both within a suprabasalt aquifer system, consisting of fluvial and lacustrine sediments, and within a system of deeper confined to semiconfined aquifers in the following strata: (1) basalt flow tops, (2) flow bottom zones, and (3) sedimentary interbeds (WHC 1993a). These deeper aquifers are intercalated with aquitards consisting of basalt flow interiors. Vertical flow and leakage between the aquitards are inferred from water level or potentiometric surface data, but the flow and leakage are not quantified and direct measurements are not available (DOE 1988). A discussion of the groundwater flow in the suprabasalt aquifer and the basalt confined aquifer systems is provided in the *Characterization Work Plan, C-018H Soil Column Disposal Site Evaluation* (WHC 1992c).



Source: WHC (1993a)

923 E026.020/44875/4-1-93

Figure C-4. North-South Cross Section Through the Sedimentary Units Above the Columbia River Basalt Group at the State-Approved Land Disposal Site.

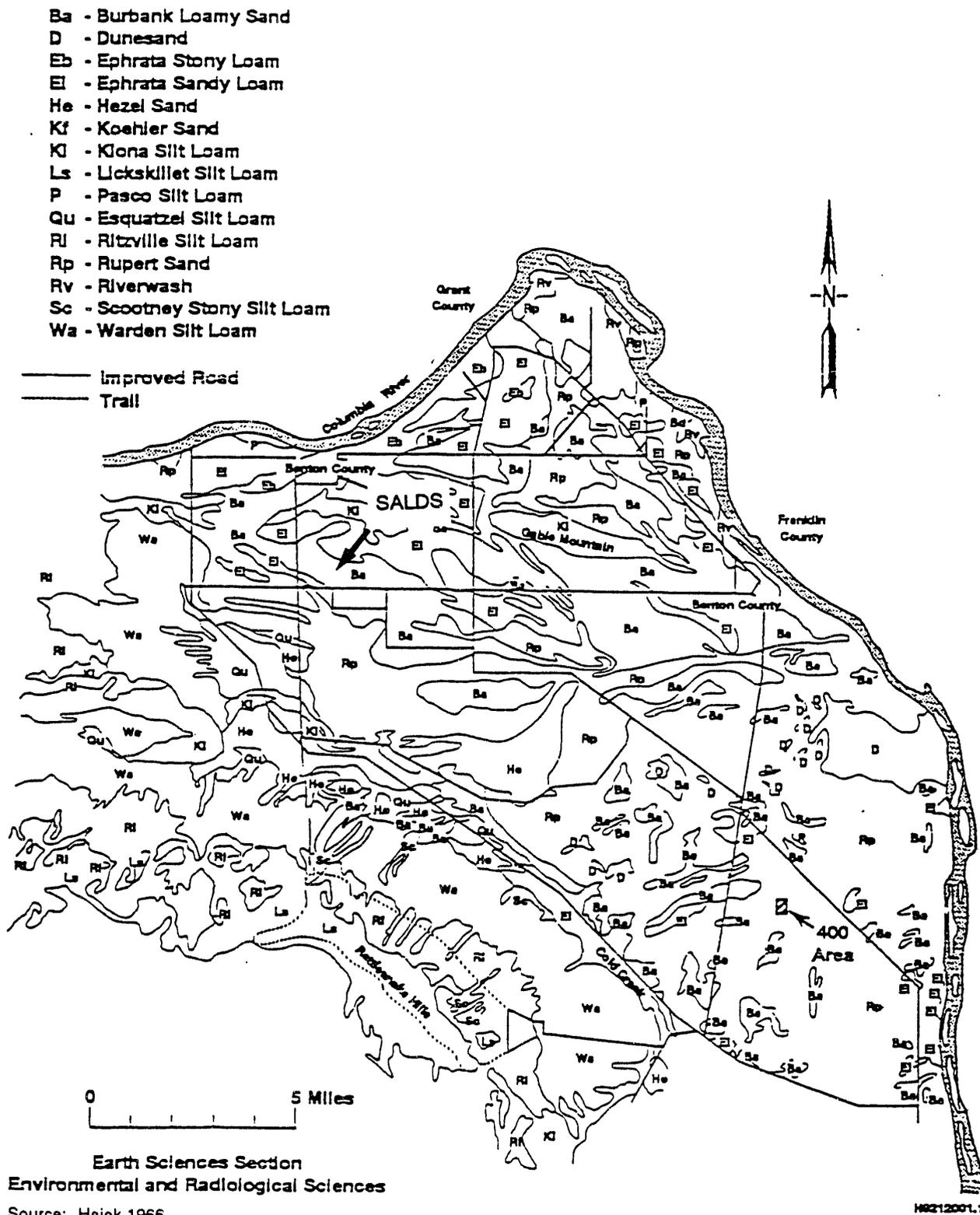


Figure C-5. Soil Survey Map of the State-Approved Land Disposal Site.

Table C-1. Concentrations of Inorganic Constituents and Radionuclides
in Soil Borings 699-48-77-A and B.^a

Analyte	Depth in Feet Below Ground Surface					
	1.5-2.5	26.5-27.5	29.7-30.7	68.5-70.0	Replicate 68.5-70.0	84.5-86.2
	229.5-231.5					
Metals ($\mu\text{g/g} = \text{mg/kg}$) ^b						
Aluminum	6,000	6,300	5,200	2,400	3,200	4,100
Antimony	6.4	5.6	4.7	<48	<45	6.6
Arsenic	<4.6	<4.3	<4.5	<48	<45	<4.6
Barium	70	56	42	40	36	60
Beryllium	0.29	0.32	0.24	<0.29	<0.27	0.20
Cadmium	<0.28	<0.26	<0.27	<2.9	<2.7	0.55
Chromium	7.2	7.8	10	<9.7	<9.0	6.4
Chromium-hexavalent	<0.04	<0.04	<0.04	<0.49	<0.49	<0.49
Cobalt	8.2	7.0	7.0	<4.8	<4.5	6.4
Copper	12	12	15	7.4	11	11
Iron	17,000	14,000	14,000	7,900	9,800	12,000
Lead	5.1	4.7	4.8.	<48	<45	4.9
Magnesium	3,300	2,800	3,600	1,900	2,500	2,900
Manganese	250	210	210	120	150	180
Mercury	<0.1	<0.0	<0.1	<0.1	<0.1	<0.1
Molybdenum	<0.92	0.92	<0.91	<9.7	<9.0	<0.91
Nickel	7.9	7.9	11	<9.7	11	10
Selenium	<4.6	<4.3	<4.5	<48	<45	<4.6
Silver	<0.55	<0.52	<0.54	<5.8	<5.4	<0.55
Strontium	22	24	49	18	15	21
Uranium	6.5	<2.6	<2.7	<29	<27	6.6
Vanadium	40	38	31	13	18	31

Table C-1. Concentrations of Inorganic Constituents and Radionuclides
in Soil Borings 699-48-77-A and B.^a (cont.)

Analyte	Depth in Feet Below Ground Surface						
	1.5-2.5	26.5-27.5	29.7-30.7	68.5-70.0	Replicate 68.5-70.0	84.5-86.2	229.5-231.5
Zinc	31	26	28	20	21	24	26
pH, Anions, and Cations ($\mu\text{g/g} = \text{mg/kg}$) ^b							
pH (dimensionless)	9.0	9.1	9.4	9.2	9.1	9.3	9.1
Bromide	<20	<20	<20	<20	<20	<20	<20
Calcium	5,700	5,200	20,000	3,800	4,200	4,500	2,300
Chloride	<20	<20	<20	<20	<20	<20	<20
Cyanide	<1.0	<10.	<1.0	<1.0	<1.0	<1.0	<1.0
Fluoride	<2	<2	<2	<2	<2	<2	5
Lithium	6.3	5.3	6.6	<3.9	<3.6	4.5	4.3
Nitrate	<20	<20	<20	<20	<0.2	<0.2	<20
Sodium	220	240	200	<19	38	220	170
Sulfate	<20	<20	37	<20	<20	<20	<20
Radionuclides (pCi/g) ^c							
Alpha	10.4	27.4	24.2	12.6	8.3	5.2	3.5
Beta	12.5	19.1	21.3	<10	<10	<10	<10
¹³⁷ Cesium	<2	<0.00001	<0.01	<2	<2	<2	<2

^a Source: WHC (1993a)

^b $\mu\text{g/g} = \text{micrograms per gram}$; $\text{mg/kg} = \text{milligrams per kilogram}$, unless otherwise noted

^c $\text{pCi/g} = \text{picocuries per gram}$

The groundwater flow at the proposed disposal site is to the northeast between Gable Mountain and Gable Butte towards the Columbia River (WHC 1992c) (Figure C-6). The gravels of unit E dominant in the Ringold Formation are the principal water table aquifer in the area. Groundwater was encountered at 218.72 feet bgs (approximately 465 feet above mean sea level) during the borehole drilling. A mini-pump test was performed on May 18, 1992. The test involved pumping for five hours at a rate of 1.65 gal/min (6.25 L/min), for a total discharge of 495 gallons (1,875 liters). The drawdown at the end of the test was 14.0 feet (4.3 meters). Water level recovery was relatively rapid (less than 100 minutes), although the water level recovered only to within 2 feet (0.6 meter) of the pretest static water level before it stabilized. An instantaneous slug test was performed for one hour on May 19, 1992. Test results are provided in the *Characterization Report, C-018H Disposal Siting Evaluation* (WHC 1993a).

The influence of the anticipated hydraulic loading of the treated waste water from the ETF on groundwater flow was modeled (WHC 1993c), and the resulting contour lines are provided in Figure C-7. The direction of groundwater flow results from the combined influences of the following: (1) recharge, (2) discharge at the SALDS location, and (3) aquifer transmissivity. The close spacing of the water table contours in the vicinity of the site indicates a groundwater mound and slow movement of the groundwater in the direction of the Columbia River.

3.4 GROUNDWATER QUALITY

The groundwater quality in the monitoring well that was installed in well 699-48-77A was initially monitored June 19, 1992, and will continue to be monitored on a quarterly basis. The groundwater temperature was approximately 65 degrees Fahrenheit, and the field pH and conductivity were 7.71 and 316 microMhos, respectively in June 1992. Table C-2 provides the available analytical data for the inorganic constituents that were above the laboratory quantitation limits (WHC 1993a). All constituents monitored were below detection limits except the following: (1) coliform, (2) nitrate, (3) carbon tetrachloride, (4) unfiltered iron, and (5) unfiltered manganese. Both of the filtered metals were below the detection limits, suggesting that the unfiltered values are an artifact of well construction or development. Nitrate concentrations were below the WAC 173-200 criterion. Coliform was detected at 65 counts/deciliter which is above the groundwater quality standard criterion of 1 count/deciliter. Carbon tetrachloride was detected at an estimated concentration of 1.3 ppb which is above the groundwater quality criterion of 0.3 ppb. The value for carbon tetrachloride is estimated because it is below the quantitation level contractually required (5 ppb). During the next sampling period, the contractual quantitation level will be lowered, providing more accurate data.

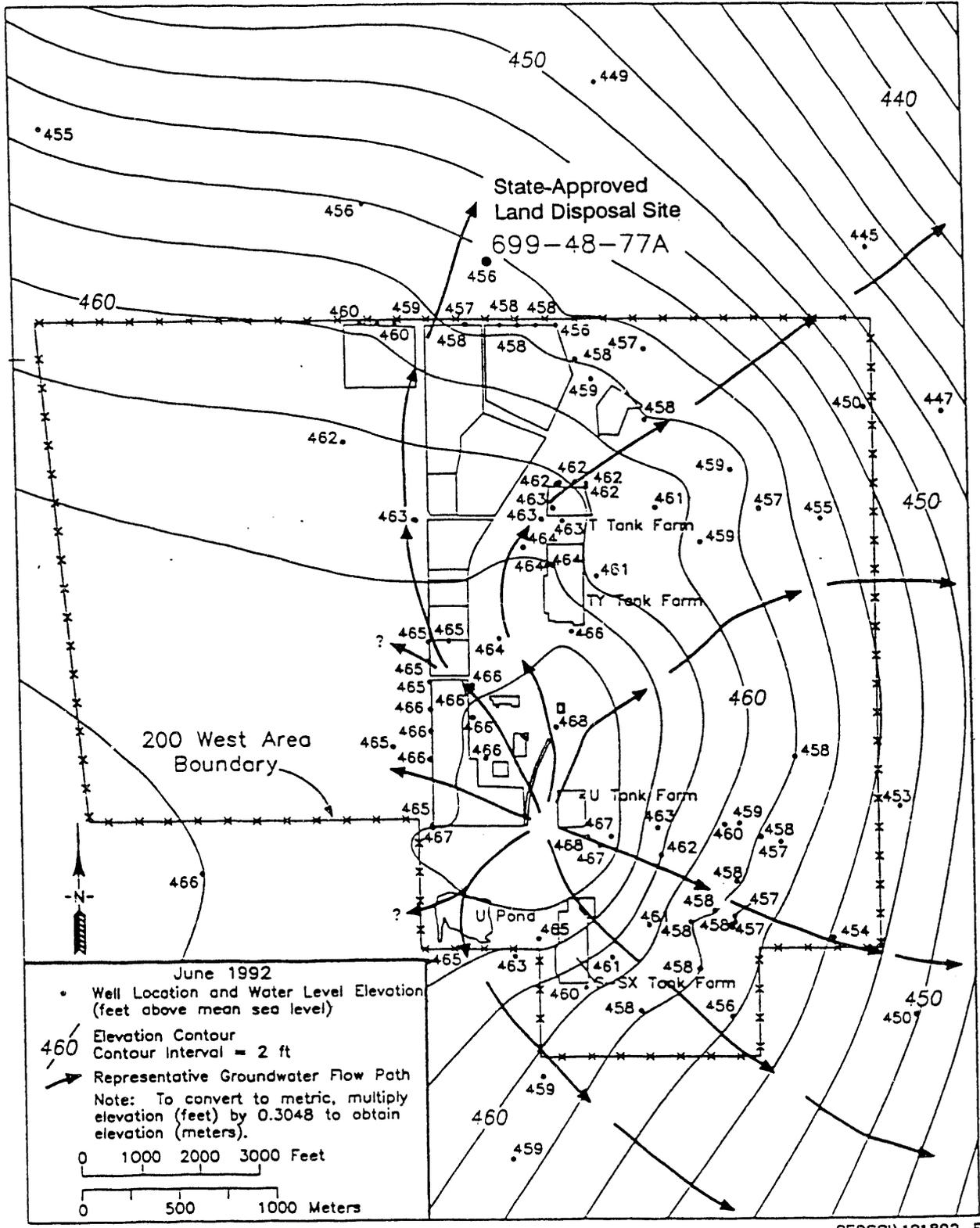
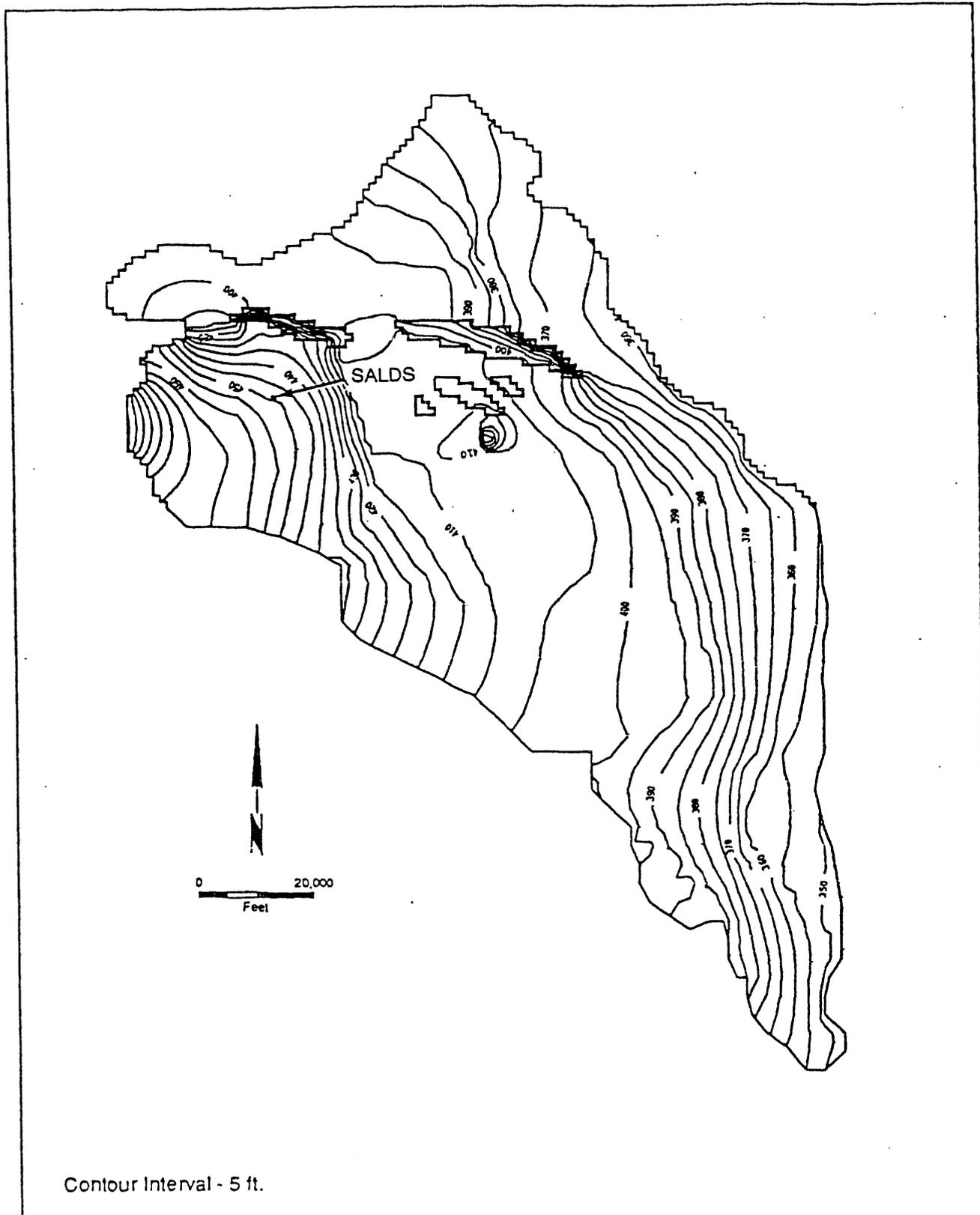


Figure C-6. Water Table Map for the State-Approved Land Disposal Site and Vicinity.



Source: WHC (1993b)

923 E026.020/45314/4-1-93

Figure C-7. Simulated Equipotentials with Disposal at the State-Approved Land Disposal Site.

Table C-2. Groundwater Quality Data From Well 699-48-77A
With At Least One Detected Value^a

Analyte	Concentration
	June, 1992
Metals (ppb) ^b	
Barium, total	74.0
Barium, dissolved	67
Iron, total	560
Iron, dissolved	20 U
Magnesium, total	12,000
Magnesium, dissolved	12,000
Manganese, total	27
Manganese, dissolved	10 U
Zinc, total	87.0
Zinc, dissolved	10.0 U
Cations and Anions (ppb) ^b	
Calcium, total	33,000
Calcium, dissolved	31,000
Chloride	6,600
Fluoride	400
Nitrate	28,000
Potassium, total	3,700
Potassium, dissolved	3,300
Sodium, total	17,000
Sodium, dissolved	15,000
Sulfate	25,000
Other Parameters (units as indicated)	
Coliform bacteria (counts/100 ml)	65 (2) ^c
Alpha particle activity (pCi/L)	1.73 U (1.76) ^c
Beta particle activity (pCi/L)	5.05 U (2.70) ^c

^a Source: WHC (1993a)^b ppb = parts per billion; pCi/L = picocuries per liter; ml = milliliter;
U = constituent present as concentrations below quantitation level^c September, 1992 data

Borehole Log: Well No. 699-48-77A

VALIDATED
 [Signature] 5/5/92
SIGNATURE/DATE

WELL CONSTRUCTION REPORT

Specification No. WHC-5-014 Rev No. 6
150143, 119902, 166752
 ECNS 127437, 169223, 150132, 150130, 150138, 150137
166757, 172294
 Project RCRA / WO17 CO18H

Well No. 699-48-77A Temp. Well No. 1A
 Coordinates N 137, 9169.02; E 566, 413.57
 Casing Elev. 674.72' Ground Elev. 672.25'

Location N of 200 W

Drilling Company Jensen Drilling

Driller Darrell Perkins

Other (Companies) MCE, Hart Crowder, Elmer D. NACE

Geologists (s) DENNIS ANDERSON - MCE; JCS Edrington

C. Wright - Hart Crowder - Ken Lane

RA. Wainman - Elmer D. Nancy Bellantyne - Elmer

Keith J. Swett - NACE

Drilling Method
 Verification Method VISUAL OBSERVATION
 Criteria WHC-5-014: 5.2, 5.3, 7.5, EIT 6.7 Sec 6.2

Item	Value	Initials	Date
Rotary	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>
Balance	<u>0-20'</u>	<u>100-105'</u>	<u>4/9/92</u>
Cable Tool	<u>20'-100'</u>	<u>100-157.7'</u>	<u>DJA</u>
Drilling Fluid	<u>CaH2O 1407.5 gals</u>	<u>DJA</u>	<u>4/9/92</u>
Other	<u>Well Guard</u>	<u>DJA</u>	<u>4/9/92</u>

Geophysical Logging		
Sonces	Interval	Date
<u>SPECTRA Gamma</u>	<u>0' - 56'</u>	<u>2/17/92</u>
<u>SPECTRA Gamma</u>	<u>54' - 115'</u>	<u>2/18/92</u>
<u>SPECTRA Gamma</u>	<u>113' - 162'</u>	<u>2-21-92</u>
<u>SPECTRA Gamma</u>	<u>162' - 30'</u>	<u>2-21-92</u>
<u>GROSS Gamma</u>	<u>334.5' - 130'</u>	<u>3-17-92</u>
<u>SPECTRA Gamma</u>	<u>334.5 - 130'</u>	<u>3-13-92</u>
<u>Spectra Gamma</u>	<u>384.5' - 327'</u>	<u>3/27/92</u>
<u>Gross Gamma</u>	<u>457' - 300'</u>	<u>4/9/92</u>

Completion Data	
Drilled Depth	<u>457.7'</u>
Completed Depth	<u>232.7' (SUMP)</u>
Date Started	<u>1/21/92</u>
Date Completed	<u>5/19/92</u>
Static Water Level/Date	<u>215.4' b/s 5-4-92</u>

Aquifer Testing	
Type	<u>INSTANTANEOUS SURGE</u>
Flow Meter I.D. No.	<u>N/A</u>
Cal Due Date	<u>N/A</u>
Length of Test	<u>1hr</u>
Volume Pumped	<u>N/A</u>
Drawdown	<u>N/A</u>
Date of Test	<u>5/19/92</u>

Completion Results

Cleaning		
Verification Method	<u>VISUAL INSPECTION</u>	
Criteria	<u>WHC-5-014 4.2.2, 7.6, 7.7 WHC-017-7.5</u>	
Drilling Tools/Rig	<u>DJA / CSW</u>	<u>4/4/92</u>
Temporary Materials	<u>DJA</u>	<u>4/9/92</u>
Permanent Materials	<u>K.L.</u>	<u>5-4-92</u>

Material Storage/Packing		
Verification Method	<u>VISUAL OBSERVATION</u>	
Criteria	<u>WHC-5-014: 4.2.2, 7.3</u>	
Mtl. Handling/Storage	<u>V.L.</u>	<u>5-4-92</u>
Material Packing	<u>V.L.</u>	<u>5-4-92</u>

Screen		
Type	Length	Slot Size
<u>T-304 STAINLESS, 1/2" DIA WIRE</u>	<u>(2) 10' SECTIONS</u>	<u>10 SLOT</u>
Depth(s)	<u>232.4' - 212.4'</u>	<u>b/s</u>
	<u>232.7' w/END CAP</u>	
Verification Method	<u>VERIFY w/ STEEL TAPE</u>	
Criteria	<u>WHC-5-014: 4.2.3, 4.2.5, 4.2.1, 12.2.1</u>	
Initials	<u>K.L.</u>	<u>Date 5-4-92</u>

Lubricants/Additives		
Verification Method	<u>VISUAL OBSERVATION</u>	
Criteria	<u>WHC-5-014: 7.2</u>	
Additives	<u>few H2O</u>	<u>DJA 4/9/92</u>
Lubricants	<u>Well Guard</u>	<u>DJA 4/9/92</u>

Straightness Test		
Verification Method	<u>VISUAL OBSERVATION</u>	
Criteria	<u>WHC-5-014: 8.2</u>	
Initials	<u>DJA</u>	<u>Date 4/9/92</u>

WELL CONSTRUCTION REPORT

639-48-77A

Type	Casing (permanent) Size	Placement
T-34 SS 10x10T SCREEN	4"	232.7 - 212.4'
T-34(2) SS LINK	4"	212.4' - 25' BGL
Verification Method	VERIFICATION w/ steel tape	
Criteria	WHC-5-014: 4.2.1, 4.2.4, 4.2.5, 12.2.1	
Initials	K.L.	Date 5-4-92

Well Protection		
Verification Method	Initials	Date
VISUAL OBSERVATION	E.C.L.	07/23/92
Criteria	WHC-5-014 4.2.10	
Protective Posts	E.C.L.	07/23/92
Protective Casing	E.C.L.	07/23/92
Site Restored	E.C.L.	07/23/92
Cap, Hasp and Lock	E.C.L.	07/23/92
Surface Pad	E.C.L.	07/23/92

Annular Seal/Filter Pack						
Verification Method	Type	Interval	Volume	Initials	Date	
VERIFICATION w/ steel tape	BOUNDARY CHECKS	237.1 - 457.1	1035 cu ft 150 sacks	K.L.	5-4-92	
	SILICA SAND 20-40	206.7' - 237.1	437 cu ft 37 sacks	K.L.	5-4-92	
	EMULSIFIC ANCHORS 3/4"	199.1 - 206.7'	37 cu ft 6 buckets	K.L.	5-4-92	
	BENTONITE CUMBLES	9.0' - 199.1	222.9 cu ft 314 sacks	K.L.	5-4-92	
	CEMENT GROUT	25' - 9.0'	15.4 cu ft 12 sacks	K.L.	5-4-92	

Well Survey/Labeling		
Verification Method	Initials	Date
REVIEW OF SURVEY REPORT	NB	7/28/92
Criteria	WHC-5-014: 3.9	
Measurement Point Surveyed	NB	7/28/92
Protective Casing/Brass Cap Surveyed	NB	7/28/92
Well Number Stenciled	NB	7/28/92
Brass Cap Labeled	NB	7/28/92

Pump Installation		
Verification Method	Initials	Date
VISUAL OBSERVATION	RJE	5/19/92
Criteria	WHC-5-014: 4.2.2, 4.2.11	
Pump Decon/Prep	RJE	5/19/92
Installed	RJE	5/19/92
Pump Tested	RJE	5/19/92

Other (initial if performed)

Well Abandonment: _____ Downhole TV Inspection: 16 Complete As-Built Diagram, Driller's/Geologist's Logs

Well Development: W. Stahler

Comments/Remarks

RAW H2O added - 2/3/92 = 259gal, 2/6/92 = 509gal + 259gal, 2/10/92 = 450gals, 2/11/92 = 159gal, 2/12/92 = 359gals, 2/13/92 = 259gals, 2/14/92 = 356gal, 2/17/92 = 256gals, 2/18/92 = 256gals, 2/19/92 = 102gal, 2/20/92 = 756gal, 2/25/92 = 185gal, 2/26/92 = 156gals, 2/27/92 = 125gals;

Well quad added 1/23/92, 1/30/92, 2/4/92, 2/5/92, 2/6/92, 2/14/92, 3/24/92, 3/31/92

Reed temp materials - casing: 1/30/92 casing, 1/22/92 casing, 2/12/92 casing, 3/13/92, 3/16/92, 2/26/92

Reed tools = 1/7/92, 3/31/92, 3/23/92, 3/24/92, 3/25/92, 3/26/92, 3/31/92

WELL SUMMARY SHEET

Boring or Well No. 699-48-77A

Sheet 1 of 3

Location N-200 WEST Project RCRA / W017 / CO18H
 Elevation 672.25' (ground surface) Drilling Contractor Jensen Drilling
 Driller Darrell Perkins Drilling Method and Equipment CABLETOOL - Sod Str
 Prepared By James Anderson Date 1/7/92 Reviewed By Edmund S. Ruffe Date 2/15/92
 (Sign/Print Name) (Sign/Print Name)

CONSTRUCTION DATA		Depth in Feet	GEOLOGIC/HYDROLOGIC DATA	
Description	Diagram		Graphic Log	Lithologic Description
CEMENT ABOUT 25'-20'		5		slightly silty sandy GRAVEL
1 1/2" temporary carbon steel casing to 19.71' b/s		10		" " " "
		15		silty sandy GRAVEL
		20		" " " "
		25		silty gravelly SAND
		30		slightly gravelly slightly silty SAND w/ calcite
		35		" " " " " "
PERCENITE CHUMBLER 9.0' - 100.1'		40		slightly gravelly slightly silty SAND
		45		" " " " " "
		50		slightly silty SAND
		55		slightly silty slightly gravelly SAND
		60		sandy SILT
		65		slightly silty sandy GRAVEL
		70		slightly silty slightly gravelly SAND
12" temporary carbon steel casing to 166.19' b/s		75		" ^{SP} SAND " " ^{SP} SAND
		80		" ^{SP} SAND " " ^{SP} SAND
		85		slightly silty sandy GRAVEL
		90		sandy GRAVEL
		95		" " " "
		100		slightly silty sandy GRAVEL
		105		" " " "
10" temporary carbon steel casing to 334.83' b/s		110		" " " "
		115		" " " "
		120		" " " "
		125		silty sandy GRAVEL
		130		sandy GRAVEL
8" temporary casing to 396.2' b/s		135		" " " "
		140		slightly sandy GRAVEL
		145		sandy GRAVEL
		150		" " " "
6" temporary carbon steel casing to 447.15'		155		" " " "
		160		" " " "

WELL SUMMARY SHEET

Boring or Well No. 699-48-77A

Sheet 2 of 3

Location 200 WEST AREA - CO18H
 Elevation 1672.25'
 Driller Darrell Perkins
 Prepared By Edward C. Ruffin (Sign/Print Name)
 Date 2/20/92

Project ACRA / WO17 / CO18H
 Drilling Contractor Jensen Drilling
 Drilling Method and Equipment Cabletool - Sid Str
 Reviewed By Edward C. Ruffin (Sign/Print Name)
 Date 2/15/92

CONSTRUCTION DATA		Depth in Feet	GEOLOGIC/HYDROLOGIC DATA	
Description	Diagram		Graphic Log	Lithologic Description
		170		sandy GRAVEL
		175		silty sandy GRAVEL
INTENSIVE COLUMNS 8.2' - 109.1' b/s		180		" " "
10" temporary carbon steel casing set to 334.83' b/s -		185		slightly silty slightly gravelly SAND
		190		slightly silty slightly gravelly SAND
INTENSIVE PULLED (1/4") 100.1' - 206.7' b/s		195		silty sandy GRAVEL
8" temporary carbon steel casing to 396.2' b/s		200		" " "
		205		" " "
Top of SAND ZONE (20-40) 206.3' b/s		210		" " "
20-25 SCREEN 212.4' b/s		215		silty sandy GRAVEL
6" temporary carbon steel casing to 247.65' b/s		220		" " "
212.4' - 232.4'		225		" " "
3/4" STEELWIRE STR. 10 SLOT SCREEN		230		" " "
BOTTOM of WELL (SUMM) 232.7'		235		" " "
static water level - 215.4'		240		" " "
		245		" " "
BOTTOM of SAND ZONE (20-40) 232.1'		250		" " "
BENTONITE CHIPS (course - 3/4") 232.1' - 452.1' b/s		255		silty sandy GRAVEL
		260		" " "
		265		" " "
		270		" " "
		275		" " "
		280		" " "
		285		" " "
		290		" " "
		295		slightly silty slightly gravelly SAND
		300		silty sandy GRAVEL
		305		slightly silty gravelly SAND
		310		silty sandy GRAVEL
		315		slightly silty gravelly SAND
		320		" " " "
		325		" " " "

WELL SUMMARY SHEET

Boring or Well No. 699-48-77A

Sheet 3 of 3

Location 200 West Area - C018H

Project RCRA / W017 / C018H

Elevation 672.25'

Drilling Contractor Jensen Drilling

Driller Darrell Perkins

Drilling Method and Equipment Rotator - Spd Str

Prepared By Shawn Chadman
(Sign/Print Name)

Date 3/13/02

Reviewed By Edmund C. Ruffe
(Sign/Print Name)

Date 05/15/02

CONSTRUCTION DATA		Depth in Feet	GEOLOGIC/HYDROLOGIC DATA	
Description	Diagram		Graphic Log	Lithologic Description
		335		slightly silty gravelly SAND
8" temporary carbon steel casing to 396.2' b/s		340		silty gravelly SAND
		345		" " "
		350		" " "
		355		slightly silty slightly sandy GRAVEL
BENTONITE CHIPS (course ~ 3/4")		360		" " " " "
237.1' - 457.1' b/s		365		" " " " "
		370		sandy GRAVEL
		375		" "
6" temporary carbon steel casing to 447.65' b/s		380		slightly silty sandy GRAVEL
		385		" " "
		390		slightly sandy GRAVEL
		395		slightly sandy GRAVEL
		400		GRAVEL
		405		GRAVEL
BENTONITE CHIPS (course ~ 3/4")		410		" w/ trace sand
237.1' - 457.1' b/s		415		"
		420		"
		425		"
		430		"
		435		"
		440		"
		445		"
		450		slightly gravelly SAND
BOTTOM of BENTONITE CHIPS 457.1' C.T.D.		455		slightly sandy GRAVEL @ 453.5'
BOTTOM of Hole 457.7' b/s		460		

KAISER ENGINEERS HANFORD		SURVEY DATA REPORT		Request ID: — 9 2 13 — 2 17 19
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Project/W.C. No.	Title	File No.
	600 AREA WELL SURVEY	6 9 19 — N 14 W 7

Client Job No. ER2411-32-77-26	Prepared By M.F. Harrington	Date 6/22/92	Reviewer <i>V. Coyne</i>
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DESCRIPTION OF WORK	ACCEPTABILITY (Within Plan Tolerance)		DISTRIBUTION	
	Yes	No	Survey File	OR
Horizontal and vertical location of well	<input type="checkbox"/>	<input type="checkbox"/>	Field Project File	—
699-48-77A and vadose borehole	<input type="checkbox"/>	<input type="checkbox"/>	P. Collier	1
	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	D. Weekes	1
	<input type="checkbox"/>	<input type="checkbox"/>	J. Rieger	1
	<input type="checkbox"/>	<input type="checkbox"/>		
	<input type="checkbox"/>	<input type="checkbox"/>		

SURVEY RESULTS AND COMMENTS

WELL NO.	COORDINATES		ELEVATIONS (NGVD'29 FEET)				
	200W (feet)	LAMBERT NAD'83 (meters)	TOP OF BRASS CAP	HYDROSTAR PLATE N. SIDE	TOP OF OUTER CASING N. SIDE	TOP OF INNER CASING N SIDE	
699-48-77A	N: 47602.7	N: 137,969.02	NGVD'29	672.25	674.74	674.72	N/A
	W: 77020.0	E: 566,413.57					
699-48-77B	N: 47590.0	N: 137,965.15	NGVD'29	671.73	N/A	N/A	N/A
	W: 77013.3	E: 566,415.60					

VALIDATED *W. J. [unclear]* p. 1 of 20

WHC-SU-CO18H-RPT-001 Spring or Well No. 699-48-77A

BOREHOLE LOG 8/5/92 Sheet *3 of 27

SIGNATURE/DATE

Location ZOO W CO18H Project RCRA / W017 CO18H
 Elevation 672' ground surface Drilling Contractor Tensen
N 137, 969 E 566, 414
 Driller Darrell Perkins Drilling Method and Equipment CABLE TOOL - 3" PISTON 60
 Prepared By Jenni's Anderson Date 1/16/92 Reviewed By Edward C. Kufner Date 2/4/92
Nancy Anderson (Sign/Print Name) (Sign/Print Name)

Depth (feet)	Sample		Graphic Log	Sample Description	Comments
	Type and No.	Blows or Recovery			
60*				slightly silty sandy GRAVEL (5% silt 25% sand 70% GRAVEL) 10% vcs 10% vcp 5% sc 15% cs 10% cp	caliche @ 60.3-60.5' bls
61.3	NO RECOVERY	6"-6 blows 6"-6 blows 6"-9 blows 6"-24 blows		15% ms 20% mo 30% fs 25% fp 30% vfs 25% vfp	minor CaCO3 cementation @ 63.0-63.9' bls
63.3		ST		3.75y 2/3.5 olbrn-olwet, 2.5y 1/3 lt yellow dry, mod sorting, rnd-wellnd / spherical-subdisc	carbonate coated clasts @ 65' bls
65'	1 rad / moist 2 1/4" DB	DB		mod Rtn to 10% HCl on carbonate coated clasts, weak in sands 60% basalt 30% Qtz 5% vol porph 5% Qtz	65' sample 1/16/92 @ 1100
67.5'	A/P # 17 col loc 6"-29 blows chem sample 6"-46 blows " 6"-42 blows " 6"-15 blows			slightly silty slightly gravelly SAND (5% silt 10% gravel 25% SAND) 10% mp 10% vcs 25% fs 20% fp 10% cs 35% vfs 40% vfp 20% ms	split tube samples taken from 67.5' - 70' bls, 11/30/92 @ 1405
70'	1 rad / moist 2 1/4" DB	ST / DB		3.75y 1/2 v yd dk gr brn - dk olary wet 3.75y 1/2 lt brn gry - lt olary dry; sample dry, well - mod sorting, No Rtn, 45% basalt 40% Qtz, 5% Qtz, 5% vol porph 5% felsic argstone	fair amt of magnetite to .25 mm
75'	1 rad / moist 2 1/4" DB	DB		musc, subrnd-rnd / subprismatic-subdisc slightly silty slightly gravelly SAND (5% silt 10% gravel 85% SAND) 10% vcs 10% cp 20% vcs 10% rfp 30% ms 35% fp 20% fs 45% vfa 20% vfs	70' sample 1/30/92 @ 1655
75'	1 rad / moist 2 1/4" DB	DB		3.75y 1/2 lt brn gry - lt olary dry, 3.75 yd dk gr brn - dk olary wet; mod-well sorting, No Rtn	75' sample 2/3/92 @ 0845
80'	1 rad / CaCO3 2 1/4" DB	DB		slightly silty, slightly gravelly SAND - 5% silt - 10% gravelly 85% SAND dist and color sample same as 75'	1 gallon DI H2O added @ 79' bls for recovery
				well sorted, subrnd-rnd / spherical-subdiscardal, No Rtn	
				* Note: see BOREHOLE LOG FOR WELL 699-48-77B for a description of the 0' - 60' interval. (Report # 1)	No moist sample
				Nancy Ballentyne / Nancy Ballentyne	80' sample 2/3/92 @ 1545

BOREHOLE LOG

Boring or Well No. 699 48-77A

Sheet 4 of 22

Location 200 West Area Project RCRA / WO17 CO18H
 Elevation 672' (ground surface)
1137, 969 E 566, 414 Drilling Contractor Jenson
 Driller Darrell Perkins Drilling Method and Equipment Case Tool - Spd Str
 Prepared By Norma Anderson Date 2/4/92 Reviewed By Edward C. Ruff Date 2/11/92
 (Sign/Print Name) (Sign/Print Name)

Depth (feet)	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
80				Slightly silty sandy GRAVEL (5% silt, 25% sand, 70% GRAVEL) 5% sc 10% vcs 10% ves 10% cs 20% ms 30% fs 30% vfs 3.75 dk gray - vudk drabrn wet	Upper Ringold? loose - non compacted sands
85	1 rod 1 moist 2 1/4	6" - 15 blow ST/DB-95'		2.75 1/2 Holbrn - olgr dry dry sample very poor sorting subrd - wellnd / spn - subdisc. No Rtn 70% basalt	85' sample 2/4/92 @ 0815
	Chem 7 samples	6" - 13 blow 6" - 31 blow ST 6" - 75 blow		Sandy GRAVEL w/ less than 5% silt 5% sc 5% ves 5% vco 10% cs 15% cp 25% ms 20% mo 25% fs 25% fp 20% vts 30% vtp	split spoon samples taken from 84.2' - 86.2' 2/4/92 @ 1430 open framework non-consolidated
90	1 rod 1 moist 2 1/4	DB		3.75 3/4 vudk gray - vudk dry wet, 3.75 5/2 ambn - olgr dry v. poor sorting, 80% basalt 15% Qtz 5% Qtz vcl porph No Rtn subrd - rnd / spherical - subdisc.	split tube sample taken from 90.0' - 92.0' 2/5/92 @ 1050 90' sample 2/5/92 @ 0710
	AP 4 13 col wash 13	6" - 28 blow 6" - 22 blow 6" - 83 blow 6" - 80 blow ST		Sandy GRAVEL SIZE DIST, COLOR, SORTING, ang. min and Rtn same as 90' sample	open framework
95	1 rod 1 moist 2 1/4	DB			95' sample 2/5/92 @ 1615
				Slightly silty sandy GRAVEL (5% silt 15% sand 80% GRAVEL) 5% sc 5% vco 5% ves 15% cp 10% cs 20% mo 25% ms 25% fp 25% fs 30% vts A-14	open framework
100	1 rod 1 moist 2 1/4	DB		3.75 3/2 vudk gray brn - dk gray wet, 2.54 1/2 dk gray brn wet (sands); 2.54 5/2.5 gray brn - Holbrn dry 10% basalt 30% Qtz 5% Qtz 5% vcl porph	100' sample 2/6/92 @ 1335

BOREHOLE LOG

Boring or Well No. 699-AB-77A

Sheet 5 of 22

Location 200 W C018H Project RCRA / W017
 Elevation N 137,919 E 566,414 Drilling Contractor Jensen
 Driller Darnell Perkins Drilling Method and Equipment CABLE TOOL - 500 STR
 Prepared By Edward C. Rafine Date 2/11/92 Reviewed By Edward C. Rafine Date 2/14/92
 (Sign/Print Name) (Sign/Print Name)

Depth (Feet)	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
100'				slightly silty sandy GRAVEL (5% silt 10% sand 85% GRAVEL) 10% sc 10% vcs 20% cp 30% cs 25% mp 40% ms 25% fp 20% fs 20% vfp	sample taken by C. Wright recycled on 2/12/92
105'	1 rad / CaCO3 2 lith	DB	3.75y 3/2 v ydk grn - dk ol grn WET, 2.5y 1/2 dk grn, sample damp, poor sorting sub rnd - sub ang / sub discordant No Rtn	70% basalt 20% Qtz, 5% QtzE, 5% vol, 20% ph	105' @ 2/11/92 11:20
110'	1 rad / CaCO3 2 lith	DB	slightly silty sandy GRAVEL (5% silt 10% sand 85% GRAVEL)	sample similar to 105'	110 sample recycled from C. Wright. 2/11/92
115'	1 rad / CaCO3 2 lith	DB	slightly silty sandy GRAVEL (5% silt 15% sand 80% GRAVEL) 10% vcs 15% vcp 5% sc 25% cs 15% cp 30% ms 20% mp 25% fs 25% fp 10% vts 20% vfp	open framework > sands @ 112' bis	H2O added for recovery
120'	1 rad / CaCO3 2 lith	DB	3.75y 3/2 v ydk grn - dk ol grn WET, 3.75y 5/2 grn - ol grn dry, damp, poor sorting sub rnd - rnd / sub cis - sub disc. No Rtn 50%	basalt 30% Qtz 10% QtzE, 5% gran 5% vol, 20% ph	115 sample 2/12/92 @ 0815
			slightly silty sandy GRAVEL (5% silt 15% sand 80% GRAVEL)	sample similar to 115'	Note: silt lens @ 115.5 - 115.7' bis
					120' sample 2/12/92 @ 1100

BOREHOLE LOG

Boring or Well No. 699-98-77A

Sheet 6 of 22

Location 200 W C018H Project ACRA / WO17 C018H
 Elevation 672' 7.5 Drilling Contractor Jensen
N137, 96.9 E. 566, 41-1
 Driller Darrell Perkins Drilling Method and Equipment CABLE TOOL - 5/8" STC
 Prepared By Arnold Anderson Date 2/12/92 Reviewed By Edward C. Rapp Date 2/12/92
 (Sign/Print Name) (Sign/Print Name)

Depth (feet)	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
120				silty sandy GRAVEL (5% silt, 15% sand 80% GRAVEL 25% ucp 10% vcs 10% sc 20% cp 20% cs 20% mp 25% ms 15% fp 20% fs 10% vfp ~10% vfs	run H2O added for recovery poor drilling rate
125	1 rad 1 CaCO3 2.17h	DB		3.75y 3/4 vdkaryen-dkolaru WET 3.75y 3/4 garyen-olgyr dama very poor soaking subsd-rnd-sphar-subdisc. No Rxn 60% basalt 25% Qtz 5% QtzE 10% gran vulpr.	35 gals H2O added for recovery 2/12/92 125' 2/12/92 @ 1550
130	1 rad 1 CaCO3 2.17h	DB		sandy GRAVEL (10% sand 90% GRAVEL) 15% sc 15% ucp 10% vcs 15% cp 15% cs 20% mp 25% ms 20% fp 30% fs 5% vfp 20% vfs	all desc same as 125' sample 130' 2/13/92 @ 1000
135	1 rad 1 CaCO3 2.17h	DB		sample @ 135 similar to 125 + 130 samples	poor drilling rate open framework
140	1 rad 1 CaCO3 2.17h	HT		slightly sandy GRAVEL (210% sand 90% GRAVEL) gravels under due to HT sands: ms 35% fs 35% vfs 30% slurry = 5y 3/4 gray sands / GRAVELS 3.75 3/4 - 1/4 vdkary - ityelln-vreid due to HT 25% vol porph 10% QtzE 20% basalt 25% Qtz 20% greenstone 10% granites No Rxn	25 gals H2O added - 2/13/92 135' sample 2/13/92 @ 1420 Begin hand tooling @ 136.5' bls added 75 gals H2O 2/13/92 140' sample 2/13/92 @ 1440

BOREHOLE LOG

Boring or Well No. 699-48-77A

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Location 200 W C018H Project RCRA / W017 C018H
 Elevation 672' 9.3- N 137, 969 E 5666, 414 Drilling Contractor Jensen
 Driller Darrell Perkins Drilling Method and Equipment CABLE TOOL - Speed Star
 Prepared By Michael Anderson Date 2/19/92 Reviewed By Edward G. Ruffalo Date 2/21/92
 (Sign/Print Name) (Sign/Print Name)

Depth (feet)	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
140				sandy GRAVEL (< 10% sand 90% GRAVEL)	
				sands 15% ms	
				25% fs	poor recovery,
				60% H ₂ O drilling silt	very slow drilling
				slurry - 5y ^s / 19 clay, sands - GRAVELS:	due to cementation of
				3.75 3/8 - 1/4 v. dk gray - Hycl brn,	gravels
				var in color, wet + dry, imp to sub zone	
				due to HT, 25% vol. calc ph, 25% basalt,	100 gals H ₂ O used 2/19/92
				10% Qtz 20% granite, 9% iron, 20% Qtz	
145	1 rod 1 CaCO ₃ 2 1/4 HT	HT			No Rem.
				sample similar to 145' desc.	
					OUT CEMENTATION and slow drill rate
150	1 rod 1 CaCO ₃ 2 1/4 HT	HT			150' sample 2/19/92 @ 1200
				sample similar to 145-150'	
				< in sands	
155	1 rod 1 CaCO ₃ 2 1/4 HT	HT			155' sample 2/20/92 @ 1010
				sample consistent with 140-155	
				LACK of sands in previous samples	
				due in part to amt of H ₂ O added to bore hole	
	1 rod 1 CaCO ₃ 2 1/4 HT	HT			160 sample 2/20/92 @ 1320

BOREHOLE LOG

Boring or Well No. 699-48-77A

Sheet 8 of 22

Location 2000' N of 200W Force Project C018H / RCRA
 Elevation N 137, 969 E 564, 414 Drilling Contractor Jenson
 Driller D. Paulsen Drilling Method and Equipment Cable Tool Speed Star
 Prepared By C. W. [Signature] Date 2/25/92 Reviewed By [Signature] Date 2/29/92
 (Sign/Print Name) (Sign/Print Name)

Depth (Feet)	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
160'	2417L 1 Ret 1 Calc	HT		Sandy Gravel (<10% Sand, 90% Gravel) Sand 15% ms 25% FS 60% UFS SW 5y 5/1 Grey Sands: Gravel 3.75 % - 9/4 v. d. Grey - Lt. Yel. Brown v. in Color Average to Sh. Avg. 1/2 Due to HT 25% Vol. p. 1/4 25% Basalt 10% Qtz, 20% Gravel 20% Qtz No Rxn to HCl	2/20/92 1320
165'	2418L 1 Ret 1 Calc	HT		165' Similar to 160'	2/20/92 1720 N.B. 160' - 165' Cased From D. Anderson loc. SW
170'	2419L 1 Calc 1 Ret	HT		SILTY SANDY GRAVEL 15% Silt 30% Sand 65% Gravel Sand 15% ms 15% FS 40% ms 20% FS 25% UFS SW 5y 5/1 Grey Pebbles 3.75 % v. d. Grey w/d 30% Basalt 30% Qtz 10% metamorphous 30% Volcanics No Rxn Average fragments of rounded	Sample at 1420 2/25/92
175'	2420L 1 Ret 1 Calc	HT		no special pebbles 175' SILTY SANDY Gravel Similar to 170' - more silt.	1635 2/25/92

BOREHOLE LOG

Boring or Well No. 64A-48-77A

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Location 2000 N. of 200 W Fence

Project WO17 / CO18H

Elevation 672' 9.3"
N 137, 969 E 576, 414

Drilling Contractor Jansta

Driller D. Perkins

Drilling Method and Equipment Cable Tool 72 Speed SPN

Prepared By C. W. Hart
(Sign/Print Name)

Date 2/29/92

Reviewed By Edward C. Hart
Edward C. Hart
(Sign/Print Name)

Date 2/29/92

Depth (Foot)	Sample		Graphic Log	Sample Description	Comments
	Type and No.	Blows or Recovery		Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
180'	2 with 1 red 1 clay	HT		Silty Sand & Gravel Slightly Silty Gravelly Sand (50% Gravel, 35% Sand, 15% Silt, Sand 10% GS, 70% LMS, 20% FS) Slurry 5x5/1 Grey Gravel 3.75 3/4 - 1/4 U.O. Grey. Angular Fragment. 20% Basalt, 50% Qtz + Qtzite 30% Volcanics No Run to HCL	Good Drilled 0825 2/26/91 184' Casing Drops 3'
185'	2 with 1 red 1 clay	HT		185' Slightly Silty Slightly Gravelly Sand. (15% Gravel 10% Silt 75% Sand.) 100% Fg. - Basalt 80% LMS 20% FS Color similar to 180 Sand 60 to Felsic 40% medic Gravel Minus clay similar to 180 No Run to 40% HCL. Plastic	1035 2/26/92 Sand Ends 187L Sand Heaves 5' into Casing.
190'	2 with 1 red 1 clay	HT		190' Slightly Silty Slightly Gravelly Sand (20-25% Gravel 10 to Silt 65% Sand.) Similar to 185' Except For Slightly Higher Gravel Content	1120 2/26/92 1120
195'	2 with 1 red 1 clay	HT		195' Silty Sand & Gravel (50% Gravel 40% Sand 10% Silt) 10% LP 80% LMS 30% MP 20% FS 60% Fg 5x5/1 Grey Wet Angular Fragment Hard Rock 60% Qtz + Qtzite 30% Basalt 10% Gravel Pebbles (Fragments) Randomly Spaced To Discardal Sand 50% medic N/O Run to HCL	2/26/92 1400

BOREHOLE LOG

Boring or Well No. 699-48-77A

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Location 2000 NOE 200W Fence Project CO18H/RCRA work
 Elevation N 137, 969 E 566, 414 Drilling Contractor Jansen
 Driller D. Perkins Drilling Method and Equipment 72 Speed Star
 Prepared By C. W. WAT Date 23/03/92 Reviewed By Edward C. Agnew Date 23/4/92
 (Sign/Print Name) (Sign/Print Name)

Depth <u>FEET</u>	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCL.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
220'	2476 12ad 16.5cm	HT		220' SILTY SANDY GRAVEL 40% Sand 40% Gravel 20% SILT	1600 2/27/92
225'	2478 12ad 16.5cm	HT		225' SILTY SANDY Gravel (40% Gravel 40% Sand 20% SILT.) 10% ms 60% ms 90% FG 40% VFS 5y 6/1 Grav Wet (swampy) 50% QTZ 30% Basalt 15% Gneiss, 5% metamorphics Sand is 50% matrix. Angular To Sub Angular Gravel Due To Hard Tool. Sub discordant. No Rem To HCL.	1055 3/2/92 Hard Drilling 224 onward.
230'	2479 12ad 16.5cm A/P19 A/P20 A/P21 12ad 3.1cm 18/5/45/35 6/6/45/180	ST		226' SILTY SAND Gravel (40% Gravel 40% Sand 20% SILT) Similar To 225' SPLITSPECIM 229.5-231.5 + 230.5-283 Matrix supported coarse pebbles conglomerate. *WATER HT Fine Sand/SILT matrix pebbles ±50% total volume	1335 7/2/92 Water HT WITH Casing ST 229.24 TO 230 BS SWL SHOT UP TO 216' BS
235'	2478 12ad 16.5cm	HT		235' SILTY SANDY Gravel (70% Gravel 20% Sand 10% SILT/Clay 100% FG 50% ms 50% FS Fractured Lw HT. 5y 6/1 Grav Wet (AS SWAMPY) Angular From HT. 50% QTZ, 30% Basalt 20% Gneiss No Rem To HCL. Probably Similar To Above	3/3/92 1500 Five Sand Clumps in Slur

BOREHOLE LOG

Boring or Well No. 699-48-77A

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Location 200W C018H Project L/D17/C018H
 Elevation N 137, 969 E 566, 714 Drilling Contractor Jensen
 Driller D. Perkins Drilling Method and Equipment 72 Speed Star / Cable Tool
 Prepared By C. Wright / [Signature] Date 03/05/92 Reviewed By Edward C. Rosen / [Signature] Date 03/10/92
 (Sign/Print Name) (Sign/Print Name)

Depth (Feet)	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
260'	26in 12in 10in	HT	0.0'-0.0'	260' Silty Sandy Gravel (30% Gravel 50% Sand 20% SILT/clay) 20% ml 30% S 80% FL 50% ms 20% FS	1530 3/4/92 Thick mud
			0.0'-0.0'	5Y6/1 Grey silty. Angular fragments of rounded sub. sorted pebbles A 50% Qtz + ATCITE, 30% BASALT B 20% Volcanic + various Nomen To 108 HCL	
265'	26in 12in 10in	HT	0.0'-0.0'	265' Silty Sandy Gravel (40% Gravel 40% Sand 20% SILT/clay) Similar to 260'.	1050 3/5/92
270'	26in 12in 10in	HT	0.0'-0.0'	270' Silty Sandy Gravel 40% Gravel 40% Sand 20% SILT Similar to 260'	570 3/5/92
275'	26in 12in 10in	HT	0.0'-0.0'	275' Silty Sandy Gravel 50% Gravel 25% Sand 15% SILT Similar to Above.	620 3/5/92

BOREHOLE LOG

Boring or Well No. 652-UR-77A

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Location 200W Project W017/C018H
 Elevation 672.53 N137,969 E566,414 Drilling Contractor Jensen
 Driller D. Perkins Drilling Method and Equipment 72 Speed STA/cable Tool
 Prepared By C. Vincent / [Signature] Date 03/02/92 Reviewed By Edward C. [Signature] Date 03/14/92
 (Sign/Print Name) (Sign/Print Name)

Depth (Feet)	Sample		Graphic Log	Sample Description	Comments
	Type and No.	Blows or Recovery		Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
280'	261TH 1 inch 16203	HT		280' Silty Sandy Gravel Similar to 275'	1620 3/5/91
285'	261TH 1 inch 16203	HT		285' Silty Sandy Gravel (40% Gravel 40% Sand 20% Silt/clay) 30% ml, 20% CS 70% FG, 50% ms 30% FS 5/6 1/2 lt Olive Green. Swamy. Angular. Fragments of rounded substandard pebbles No Run to HCl, 50% AT, 30% Pass 20% Inertoss.	5/4/92 0840
290'	261TH 1 inch 16203	HT		290' Silty Sand Gravel (50% Sand 30% Gravel 20% Silt) Similar to 285, slightly more Sand	5/6/91 1000
295'	261TH 1 inch 16203	HT		295' Slightly Silty Slightly Gravelly Sand. (70% Sand 15% Gravel 15% Silt/clay) 100% FG, 30-20% CS 20% ms 5/6 1/2 lt olive green Sand 50% Moisture ± No Run to HCl	1500 3/6/92

BOREHOLE LOG

Boring or Well No. 699-48-77A

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Location 699 2000' N of 700' Fence Project W017/C018H
 Elevation N 137, 969 E 566, 414 Drilling Contractor Jensen
 Driller P. Perkins Drilling Method and Equipment Caliber Tool 72 Speed Star
 Prepared By C. [Signature] Date 3/16/92 Reviewed By Edward C. [Signature] Date 03/14/92
 (Sign/Print Name) (Sign/Print Name)

Depth Feet	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
300'	2 1/4 in 1 in 1 Calog	HT		300' SILTY SANDY GRAVEL 50% GRAVEL 30% SAND 20% SILT 100% F6 (Hard Ind) 40% LS 20% MS 30% FS 5 1/4 to 6 1/4 Grey-Silver 50% QTZ + QRTZ 30% B&J 20% Granite & metamorphic Angular fragments of rounded pebbles Sand 50% matrix No. 40 to 10% etc	1630 3/6/92 300'-305' - Heaving material in casing.
305'	2 1/4 in 1 in 1 Calog	HT		Slightly silty gravelly sand (25% gravel 65% sand 10% silt) 20% L6 20% LS 10% F6 30% MS 50% FS 5 1/4 to 5 1/2 LT Olive grey silver Pebbles - Angular fragments of rounded discordal pebbles. 40% B&J 30% QTZ + QRTZ 30% Gravel No. 40 to 10% etc Sand 50% matrix.	1095 3/10/92 Heaving into casing
310'	2 1/4 in 1 in 1 Calog	HT		310' SILTY SANDY GRAVEL 50% GRAVEL 30% SAND 20% SILT Similar to 300'	1145 3/10/92 No longer heaving 312
315'	2 1/4 in 1 in 1 Calog	HT		Slightly silty gravelly sand (25% gravel 65% sand 10% silt) Similar to 205'	1455 3/10/92

BOREHOLE LOG

Boring or Well No. 199-48-77A

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Location 200W COLEH Project COLEM
 Elevation N 137, 969 E 566, 414 Drilling Contractor Urmasen
 Driller D. Pertans Drilling Method and Equipment Cable Tool 72 Speed SER
 Prepared By C. Weight / [Signature] Date 03/11/92 Reviewed By Edward C. Rogers Date 03/11/92
 (Sign/Print Name) (Sign/Print Name)

Depth (Feet)	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
320'	2LIT 1REC 1CALCS	HT	0'-10'	Slightly Silty Gravelly Sand (25%) 65% Sand 10% Silt Similar to 315	1640 3/10/92
325'	2LIT 1REC 1CALCS	HT	0'-10'	225' Slightly Silty Gravelly Sand 25% Gravel, 65% Sand 10% Silt. 20% mb 20% GS 80% FS 30% ms 50% FS 5/16" - 5/8" LT olive green SLIPRY Angular Fragment of rounded pebbles 40% BWSH 30% QTZ + WFZTR Sand 50% matrix, No VSH TO HCL	10435 3/11/92
330'	2LIT 1REC 1CALCS	HT	0'-10'	330 Slightly Silty Gravelly Sand (25% Gravel, 65% Sand 10% Silt) Similar to Above	3/11/92 1030
335'	2LIT 1REC 1CALCS	HT	0'-10'	335' Slightly Silty Gravelly Sand (25% Gravel, 65% Sand 10% Silt) Similar to Above	3/11/92 1325 10' Silt at 334.83

BOREHOLE LOG

Boring or Well No. 699-48-77A

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Location 200W AREA / C018H Project C018H
 Elevation N 137, 969 E 566, 414 Drilling Contractor Tenzen Drilling
 Driller Darrell Perkins Drilling Method and Equipment CABLE TOOL / Spd Str
 Prepared By (Signature) Date 3/17/92 Reviewed By EDUARDO C. LAPINA Date 03/19/92
 (Sign/Print Name) (Sign/Print Name)

Depth (feet)	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
240				silty gravelly SAND (15% silt 30% gravel 55% SAND) gravels 20% cs predomit. m-p-p-ang 25% fs 55% vfs	Begin handtooling w/ 8" casing 13/17/92@ 1430
345	1 rad 1 CaCO3 2 lith	HT		3.75y 5/3 Htblbrn - olive wet 3.75y 4/3 Htblbrn - plol dry, sorting undet. sands are subang - subrnd, 40% basalt 30% Qtz, 20% Qtz, 10% vol porph, gmsstr No Rtn w/ 10% HCl	No H2O added. 240 sample 3/17/92@ 1615
350	1 rad 1 CaCO3 2 lith	HT		sample similar to 340'	345 sample 3/18/92 @ 0815
355	1 rad 1 CaCO3 2 lith	HT		silty gravelly SAND (10% silt, 35% gravel 55% SAND) 25% cs gravels undet for part size 25% fs 50% vfs 3.75y 2/3 Htblbrn - olive wet 3.75y 4/3 Htblbrn - plol dry, sorting undet gravels ang, sands subang - subrnd 45% basalt, 35% Qtz, 15% Qtz, 5% vol porph, musc, gmsstr, Ni Rtn. to 10% HCl	350 sample 3/18/92 @ 0935
360	1 rad 1 CaCO3 2 lith	HT		slightly silty slightly sandy GRAVEL (5% silt + 10% sand 85% GRAVEL gravels undet 25% cs 25% fs 50% vfs 3.75y 2/3 Htblbrn - olive wet 3.75y 4/3 Htblbrn - plol dry, sorting undet. gravels ang - sands subrnd 50% basalt 35% Qtz, 10% Qtz, 5% gran, musc, misc No Rtn	355 sample 3/18/92 @ 1300

BOREHOLE LOG

Boring or Well No. 699-48-77A

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Location ZOO W AREA - CO18H

Project WO17 / CO18H

Elevation N 137,969 E 566,414

Drilling Contractor Jensen Drilling

Driller Darrell Perkins

Drilling Method and Equipment CABLE TOOL / Spd Str

Prepared By Alana Cadman
(Sign/Print Name)

Date 3/19/92

Reviewed By Edward C. Raftery
(Sign/Print Name)

Date 04/06/92

Depth <i>feet</i>	Sample		Graphic Log	Sample Description	Comments
	Type and No.	Blows or Recovery		Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
380				slightly silty sandy GRAVEL (5% silt 15% sand 80% GRAVEL	No H ₂ O added
				25% fs 60% vfs	slower drill rate than 375-380
				3.75y, 3/3 H ₂ O brn - ol-wet; 3.75y 4/3 H ₂ O brn - pl ₁ dry; section undet.	
				gravel undet. sands sub-rnd. 40% basalt 45% Qtz 10% Qtz 5% rd. perph grn, No Rtn to HCl	
385	1 rad CaCO ₃ 2 lith	HT		sample similar to 380'	380' sample 3/19/92 @ 1100
					No H ₂ O used
390	1 rad CaCO ₃ 2 lith	HT		slightly sandy GRAVEL (10% sand - 90% GRAVEL) desc same as ABOVE	385' sample 3/19/92 @ 1400
395	1 rad CaCO ₃ 2 lith	HT		GRAVEL w/ possible small amt of sand. consolidated sands are fine - vfs gravel undet.	NOTED color change @ 393' > dk
				shaly: 5y 4/1 dk gray, 4/1 H ₂ O dry m ₄ : 3.75y 3/10 vdk gray - 3/1 vdk gray	drill advised slow drill rate due to cementation
				3.75y 5/1 gray - 3/1 gray	
				grn, No Rtn to 10% HCl. 80% basalt cons. 5% Qtz, 5% granite, Qtz, No cont.	
				magnetic to iron ~ 1% -	
400	1 rad CaCO ₃ 2 lith	HT			395' sample 3/23/92 @ 0800

BOREHOLE LOG

Boring or Well No. 699-48-77A

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Location 200 W Area - CO18H Project W017 - CO18H
 Elevation N 137, 969 E 516, 414 Drilling Contractor Jensen Drilling
 Driller Darrell Perkins Drilling Method and Equipment CABLE TOOL - Spd Str
 Prepared By Annina Anderson Date 3/23/92 Reviewed By Edward C. Raper Date 04/07/92
 (Sign/Print Name) (Sign/Print Name)

Depth <i>(feet)</i>	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
400				GRAVEL w/ trace sand consolidated gravels, sands are fine - vfs slurry = 5y 1/4 dk gray, 6/1 lt gray dry rock = 3.75y 3/8 vdk gray - 3/1 vdk gray 3.75y 5/8 gray - 5/1 gray gravels avg. No Rxn to 10% HCl, 80% basalt, 5% Qtz, 15% granite gran. Note magnetite to 1mm, noticeable amt of metallic material in sample due to hardtool	trout drilling slow drill rate very consolidated 400' sample 3/23/92 @ 0740
405	1 rad 1 CaCO3 2 lith	HT		GRAVEL w/ trace sand slurry = 5y 1/4 dk gray - 6/1 lt gray dry rock = 3.75y 3/8 - 3/2 vdk gray - vdk brown wet 3.75y 1/2 - 1/2 vdk gray - vdk gray dry 70% basalt, 20% granite, 10% Qtz, magnetite to 5mm, est. ssc mp - 10 - vts - ms, No Rxn to 10% HCl, sample avg. hardness undet.	Very consolidated shoe has become elongated will down size to 6" 8' casing set @ 396.2' bls metallic material in sample. 405' sample 3/24/92 @ 1510
410	1 rad 1 CaCO3 2 lith	HT		GRAVEL w/ trace sand sand vts - fs slurry = 5y 1/4 dk gray 6/1 lt gray dry rock = 3.75y 3/8 - 3/2 vdk gray - clay - vdk gray brown wet; 3.75y 1/2 - 1/2 vdk gray vdk gray dry: 30% basalt, 35% Qtz, 25% granite. No Rxn to HCl use same as above	Basin 6" hardtool 4/1/92 slow drill rate No H2O added PID detected 30cm @ borehole AM 4/1/92 pass middle Ringold. 410' sample 4/1/92 @ 0830
415	1 rad 1 CaCO3 2 lith	HT		GRAVEL w/ trace sand (<10%) vts - fs slurry = 5y 2.5 clay - ol wet 5.5y 1/1 gray - dry rock = 5y 1/2 - 1/2 clay → clay yellow - wet 5y 3/2 - 7/8 clay → yellow - dry poor sorting, avg due to HT, No Rxn to 10% HCl, 40% basalt, 40% Qtz, 20% granite	slow drill rate pass middle Ringold 415' sample 4/1/92 @ 1515
420	1 rad 1 CaCO3 2 lith	HT			

BOREHOLE LOG

Boring or Well No. 699-48-77A

Sheet 21 of 22

Location 200 W Area - C018H Project W017 - C018H
 Elevation N 137, 969 E 546, 414 Drilling Contractor Tension Drilling
 Driller Darrell Perkins Drilling Method and Equipment CABLE TOOL - Split Str
 Prepared By Samuel Anderson Date 4/1/92 Reviewed By Edward G. Ruff Date 04/07/92
 (Sign/Print Name) (Sign/Print Name)

Depth (feet)	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
420				GRAVEL w/ trace sand (<10%) vls-fs slurry - 5y 4/1 dk gray - wet 5y 5/2 clay - dry rock: 5y 3/2-4/3 dk gray - el - wet 5y 4/1-5/3 dk gray - el - dry sample wet, poor sorting, sample w/ for mtd rtd/subdiscoidal, No Rxn to 10% HCl 40% basalt, 10% Qtz 50% granite.	
425	1 rad 1 CaCO3 2 lith	HT			420' sample 4/1/92 @ 1515
					sample same as above
					> consolidation
430	1 rad 1 CaCO3 2 lith	HT			425' sample 4/1/92 @ 1045
					sample same as above, except as noted
					rock: 5y 3/1.5 vldk gray - dk gray - wet 5y 4/1 dk gray - clay driller stated @ lower material
					50% basalt 40% granite 10% Qtz-QtzE mass basaltic colluvium.
435	1 rad 1 CaCO3 2 lith	HT			430' sample 4/2/92 @ 1120
					GRAVEL color same as 420' sample. remaining desc. same as 425'-430' sample mass basaltic colluvium
				60% basalt 35% granite 5% Qtz	
440	1 rad 1 CaCO3 2 lith	HT		435' sample 4/2/92 @ 1315	

BOREHOLE LOG

Boring or Well No. 699-48-77A

Sheet 22 of 22

Location 200 W AREA - CO18H

Project W017 - CO18H

Elevation N 137, 769 E 566, 414

Drilling Contractor Jensen Drilling

Driller Darrell Reekus

Drilling Method and Equipment CAULETROL - Spd Str

Prepared By Alvin Anderson
(Sign/Print Name)

Date 4/2/92

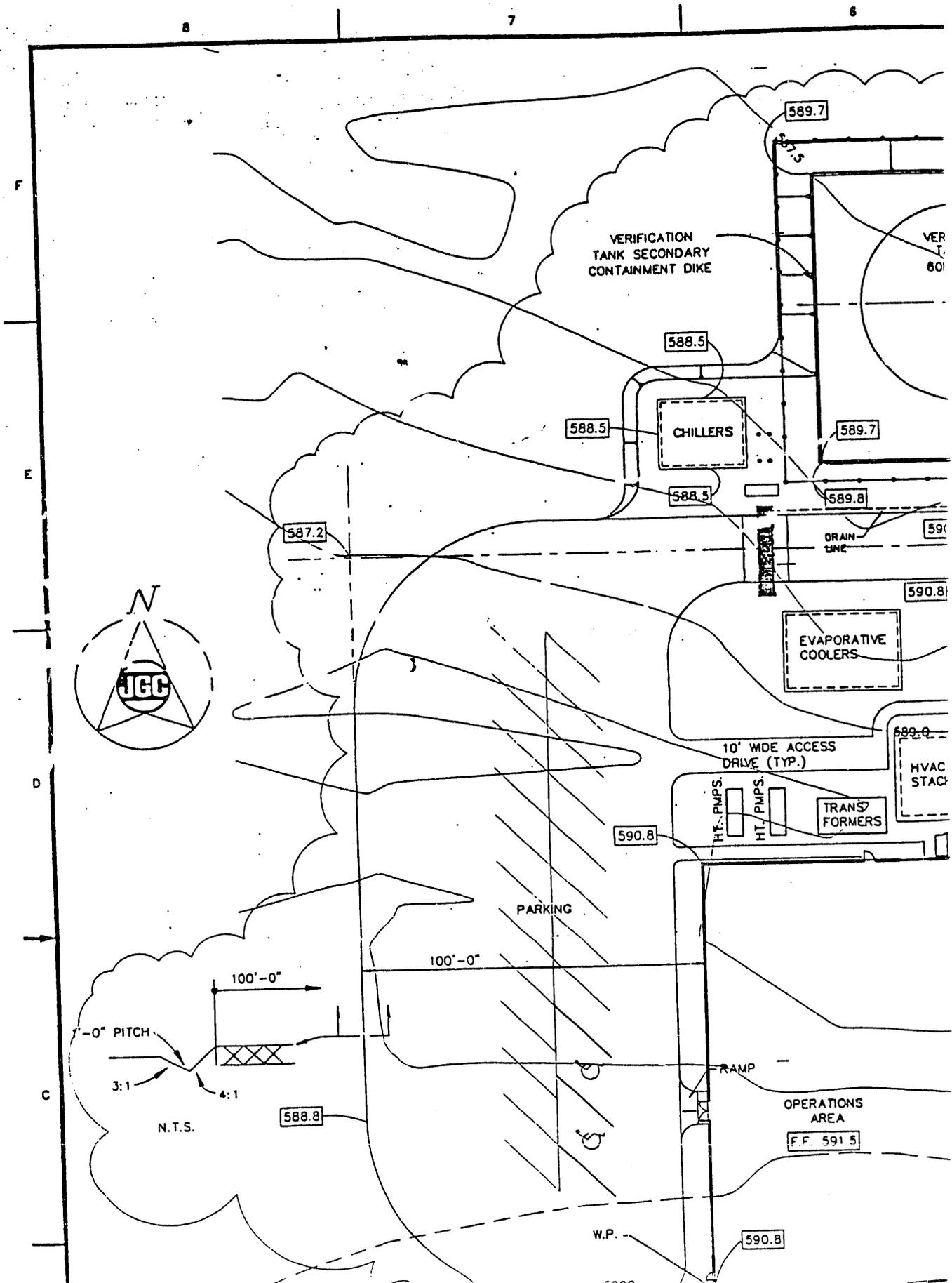
Reviewed By EDUARDO C. RIVERA
EDUARDO C. RIVERA
(Sign/Print Name)

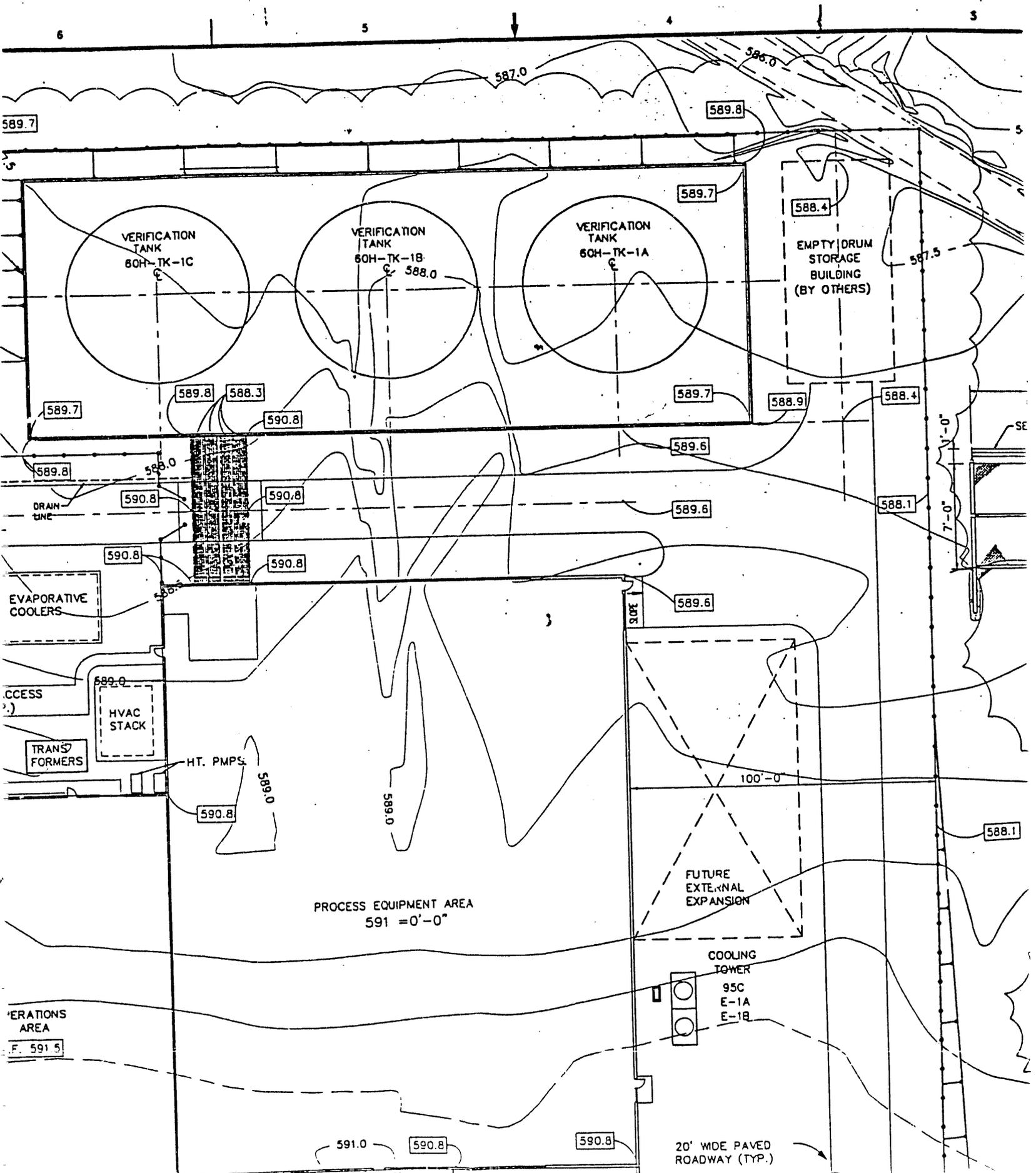
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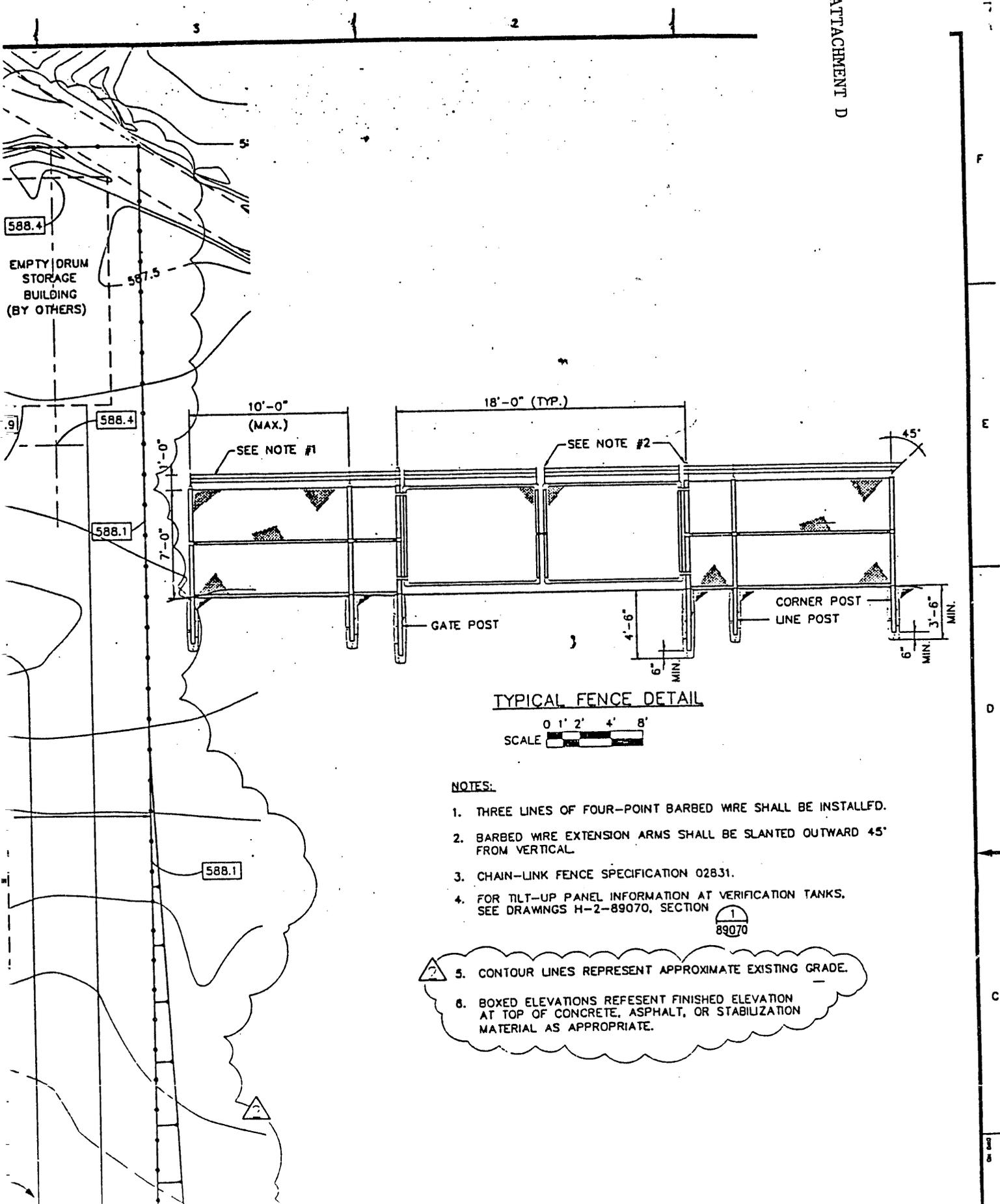
Depth (feet)	Sample		Graphic Log	Sample Description Soil Classification, Particle Size Distribution, Color, Moisture Content, Sorting, Angularity, Mineralogy, Reaction to HCl.	Comments Depth of Casing, Drilling Rate, Casing Size & Type, Bit Size, Water Level
	Type and No.	Blows or Recovery			
440				GRAVEL w/trace sand (95% GRAVEL 5% sand) GRAVELS undot sands vfs-fs	slow drill rate
				slurry sy 3/1 dk grey - v/dk grey wet	consolidated - closed framework
				rock sy 2.75/1.5 black dk ol gry wet	No H2O added
				sy 4/1.5 dk gry - ol gry dry	
				sample saturated, sorting undot, rdness undot	
				sands submed - subdisoidal No Rxn to 10% HCl	
				85% basalt, -chloritic basalt, 10% f/z w/	
				Fe stain 5% Qtz	
445	1 rad 1 CaCO3 2 lith	HT			440' sample 4/2/92 @ 1525
					445' sample same as above
				Very slow drill rate	
				consolidated material	
451	1 rad 1 CaCO3 2 lith	HT		445' sample 4/2/92 @ 1710	
				450' sample same as above	
				possible flow area due to fineness of material	
				sands encountered @ 452'	
				w/ minor gravels	
455	1 rad 1 CaCO3 2 lith	HT		450' sample 4/6/92 @ 1500	
				basalt (100%)	
				dese undot	
				Color: 2.75/1/0 black	
				No Rxn to 10% HCl	
				basalt @ 454.5'	
				< gravels	
				very slow drill rate	
460	1 rad 1 CaCO3 2 lith 1 x-ray			455' sample 4/8/92 @ 1150	

ATTACHMENT D

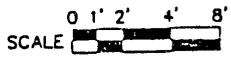
MAPS SHOWING STORMWATER DRAINAGE AREAS







TYPICAL FENCE DETAIL

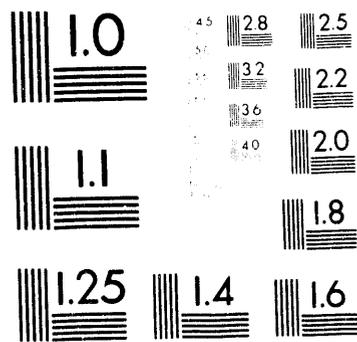


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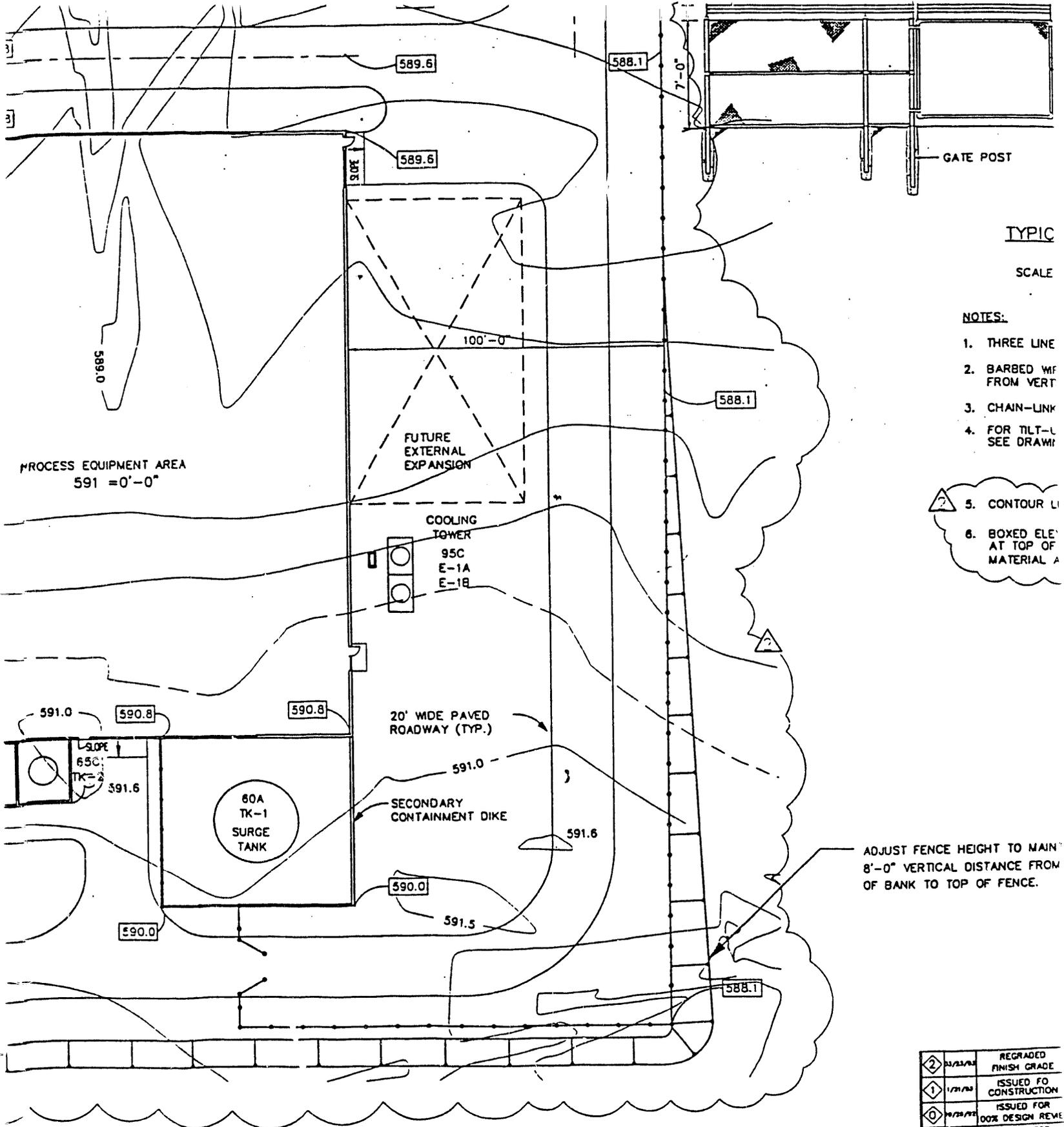
1. THREE LINES OF FOUR-POINT BARBED WIRE SHALL BE INSTALLED.
2. BARBED WIRE EXTENSION ARMS SHALL BE SLANTED OUTWARD 45° FROM VERTICAL.
3. CHAIN-LINK FENCE SPECIFICATION 02831.
4. FOR TILT-UP PANEL INFORMATION AT VERIFICATION TANKS, SEE DRAWINGS H-2-89070, SECTION 1

89070

5. CONTOUR LINES REPRESENT APPROXIMATE EXISTING GRADE.
6. BOXED ELEVATIONS REPRESENT FINISHED ELEVATION AT TOP OF CONCRETE, ASPHALT, OR STABILIZATION MATERIAL AS APPROPRIATE.



2 of 2



TYPIC
SCALE

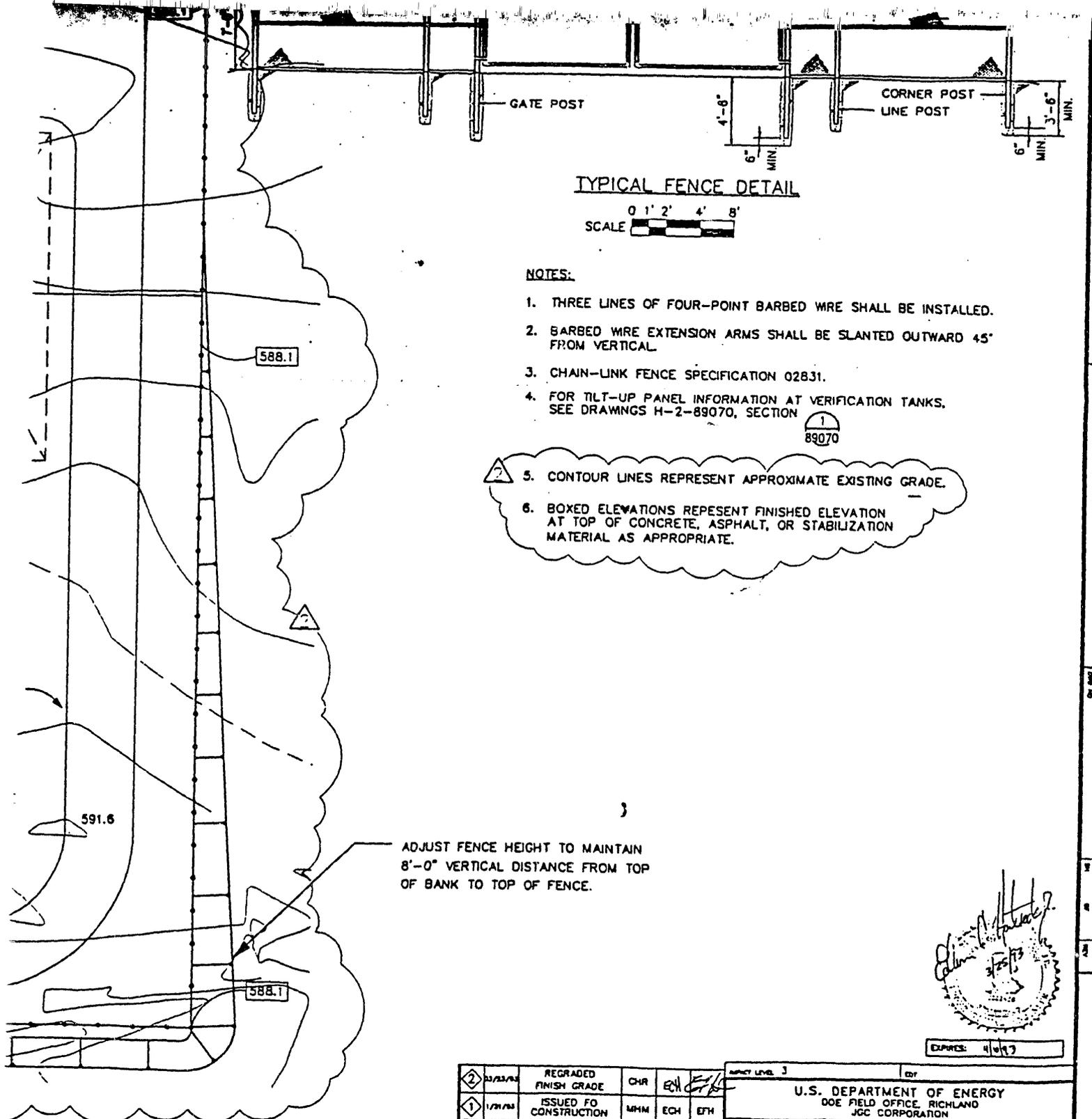
- NOTES:
1. THREE LINE
 2. BARBED W/F FROM VERT
 3. CHAIN-LINK
 4. FOR TILT-L SEE DRAWING

5. CONTOUR LINE
6. BOXED ELEMENT AT TOP OF MATERIAL

2	11/23/93	REGRADED FINISH GRADE
1	1/21/94	ISSUED FOR CONSTRUCTION
0	08/28/93	ISSUED FOR 100% DESIGN REVIEW
A	0/28/93	ISSUED FOR INTERNAL REVIEW
REV	DATE	DESCRIPTION

NUMBER	TITLE	NUMBER	TITLE
DRAWING TRACEABILITY LIST		REFERENCES	
NEXT USED ON		CAOFFILE 8889039A CA	

50'



TYPICAL FENCE DETAIL
 SCALE 0 1' 2' 4' 8'

- NOTES:
- THREE LINES OF FOUR-POINT BARBED WIRE SHALL BE INSTALLED.
 - BARBED WIRE EXTENSION ARMS SHALL BE SLANTED OUTWARD 45° FROM VERTICAL.
 - CHAIN-LINK FENCE SPECIFICATION 02831.
 - FOR TILT-UP PANEL INFORMATION AT VERIFICATION TANKS, SEE DRAWINGS H-2-89070, SECTION 1/89070

- CONTOUR LINES REPRESENT APPROXIMATE EXISTING GRADE.
- BOXED ELEVATIONS REPRESENT FINISHED ELEVATION AT TOP OF CONCRETE, ASPHALT, OR STABILIZATION MATERIAL AS APPROPRIATE.

ADJUST FENCE HEIGHT TO MAINTAIN 8'-0" VERTICAL DISTANCE FROM TOP OF BANK TO TOP OF FENCE.



<table border="1"> <tr> <th>REV</th> <th>DATE</th> <th>DESCRIPTION</th> <th>DESIGN</th> <th>CHK'D</th> <th>APP'D</th> </tr> <tr> <td>2</td> <td>03/23/73</td> <td>REGRADED FINISH GRADE</td> <td>CHR</td> <td>ECH</td> <td>EJH</td> </tr> <tr> <td>1</td> <td>1/21/73</td> <td>ISSUED FOR CONSTRUCTION</td> <td>MHM</td> <td>ECH</td> <td>EFH</td> </tr> <tr> <td>0</td> <td>10/20/72</td> <td>ISSUED FOR 100% DESIGN REVIEW</td> <td>MHM</td> <td>ECH</td> <td>EFH</td> </tr> <tr> <td>0</td> <td>1/20/73</td> <td>ISSUED FOR INTERNAL REVIEW</td> <td>MHM</td> <td>IWO</td> <td>ECH</td> </tr> </table>		REV	DATE	DESCRIPTION	DESIGN	CHK'D	APP'D	2	03/23/73	REGRADED FINISH GRADE	CHR	ECH	EJH	1	1/21/73	ISSUED FOR CONSTRUCTION	MHM	ECH	EFH	0	10/20/72	ISSUED FOR 100% DESIGN REVIEW	MHM	ECH	EFH	0	1/20/73	ISSUED FOR INTERNAL REVIEW	MHM	IWO	ECH	SHEET LEVEL 3 U.S. DEPARTMENT OF ENERGY DOE FIELD OFFICE, RICHLAND JGC CORPORATION SITE PLAN FINISH GRADE PROJECT 0-918A, 242-A EVAPORATOR/PURIFIED PLANT PROCESS COND. TREATMENT FACILITY	
REV	DATE	DESCRIPTION	DESIGN	CHK'D	APP'D																												
2	03/23/73	REGRADED FINISH GRADE	CHR	ECH	EJH																												
1	1/21/73	ISSUED FOR CONSTRUCTION	MHM	ECH	EFH																												
0	10/20/72	ISSUED FOR 100% DESIGN REVIEW	MHM	ECH	EFH																												
0	1/20/73	ISSUED FOR INTERNAL REVIEW	MHM	IWO	ECH																												
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TRACEABILITY LIST	NEXT USED ON	REFERENCES																															
SIZE	BLOB NO	NOISE NO	DWG NO	REV																													
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3

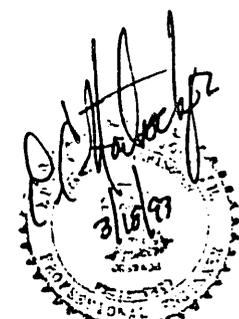
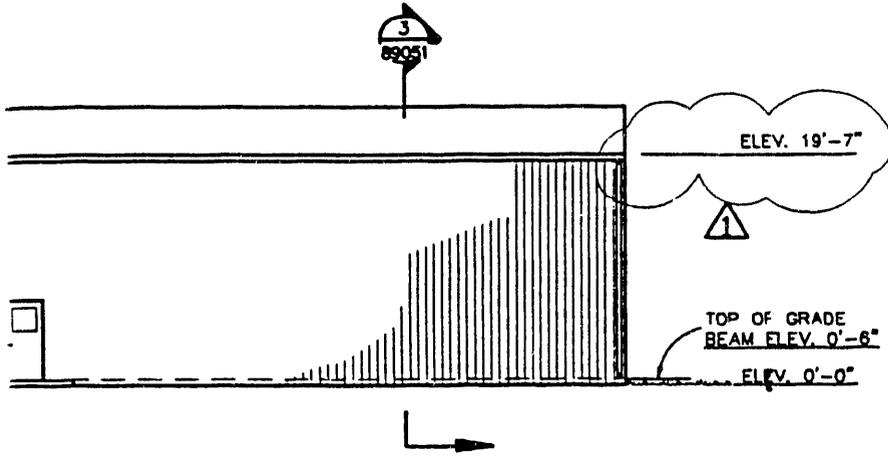
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NOTE:

1. SEE ARCHITECTURAL DRAWINGS
H-2-89047 AND 89048



EXPIRES 4/10/93

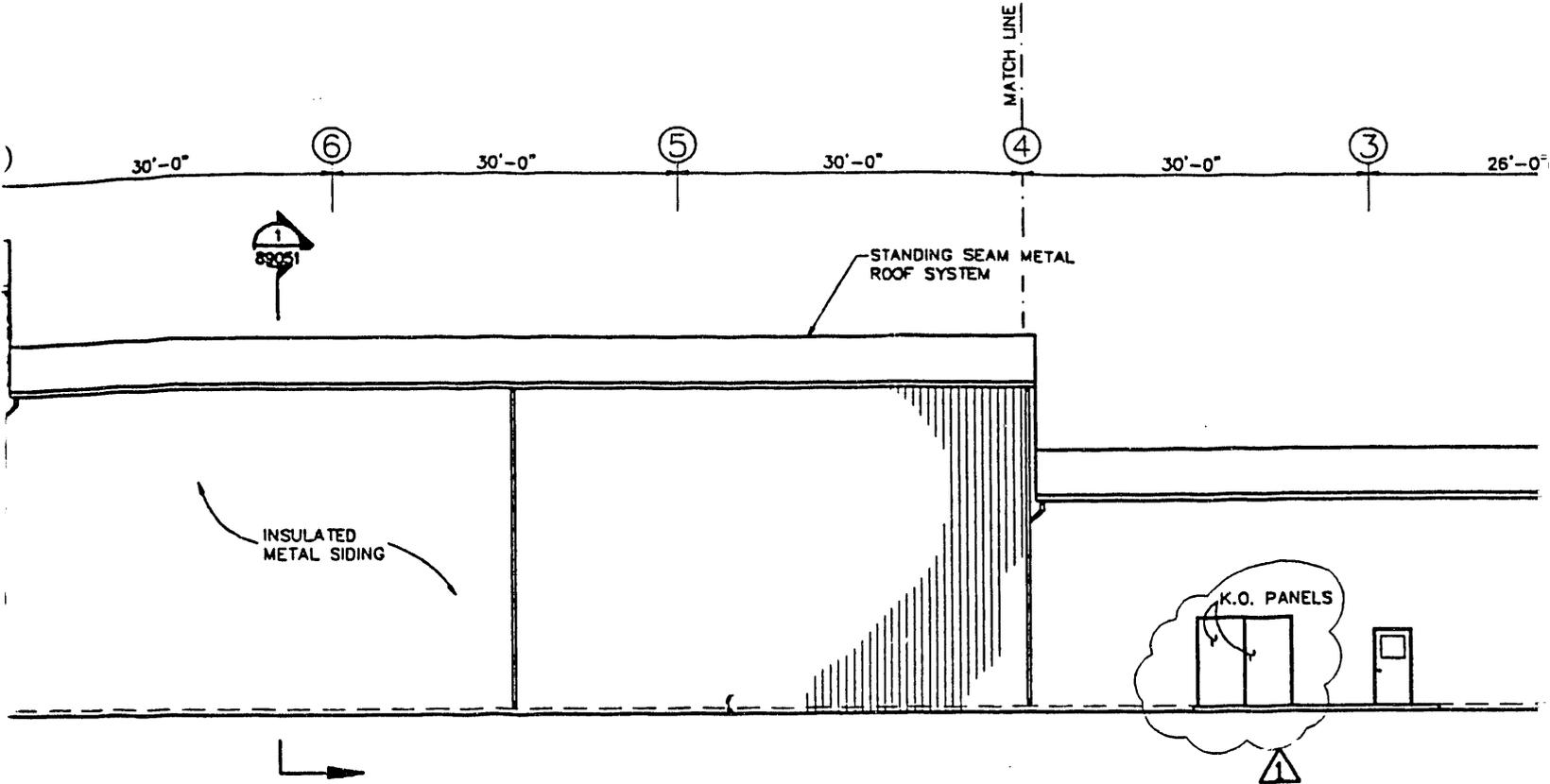
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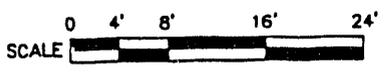
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ARCHITECTURAL NORTH AND SOUTH ELEVATIONS		
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SCALE 1/8"=1'-0"	D-1302-003	REV 1

19930221 • CHUCK R. • 89049

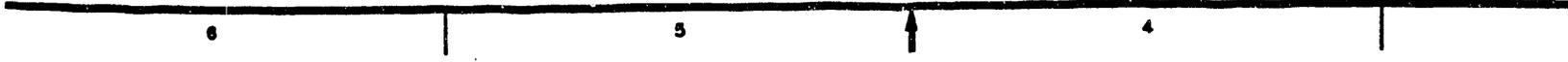
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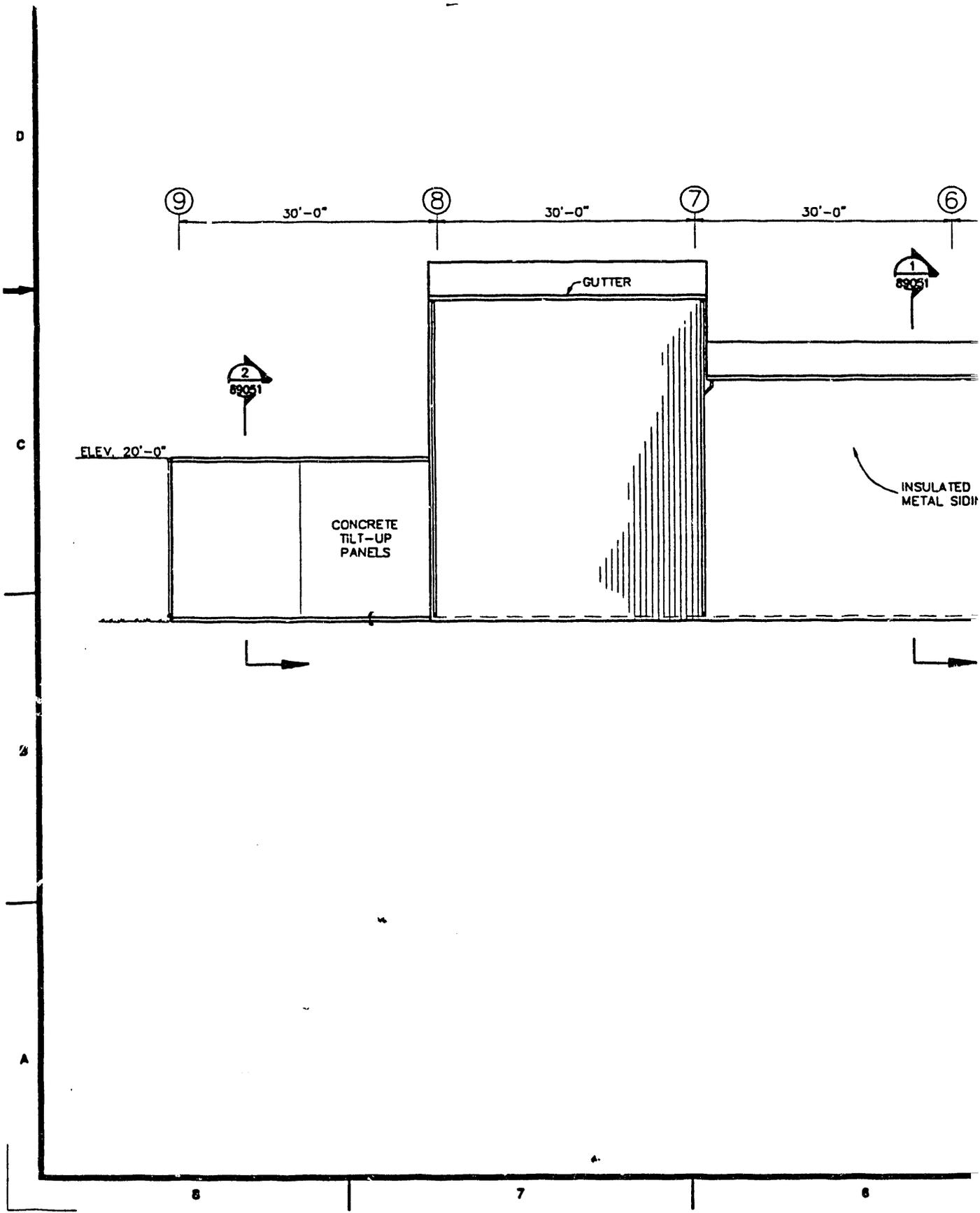


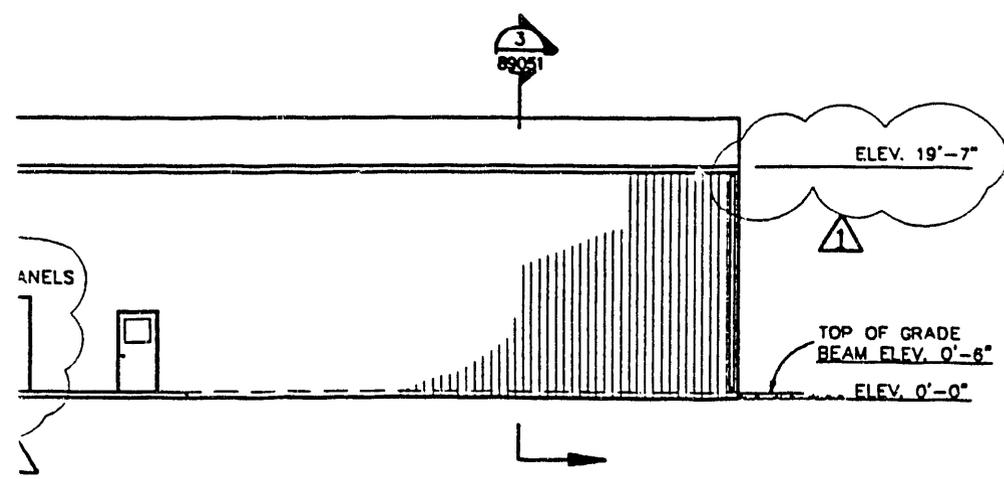
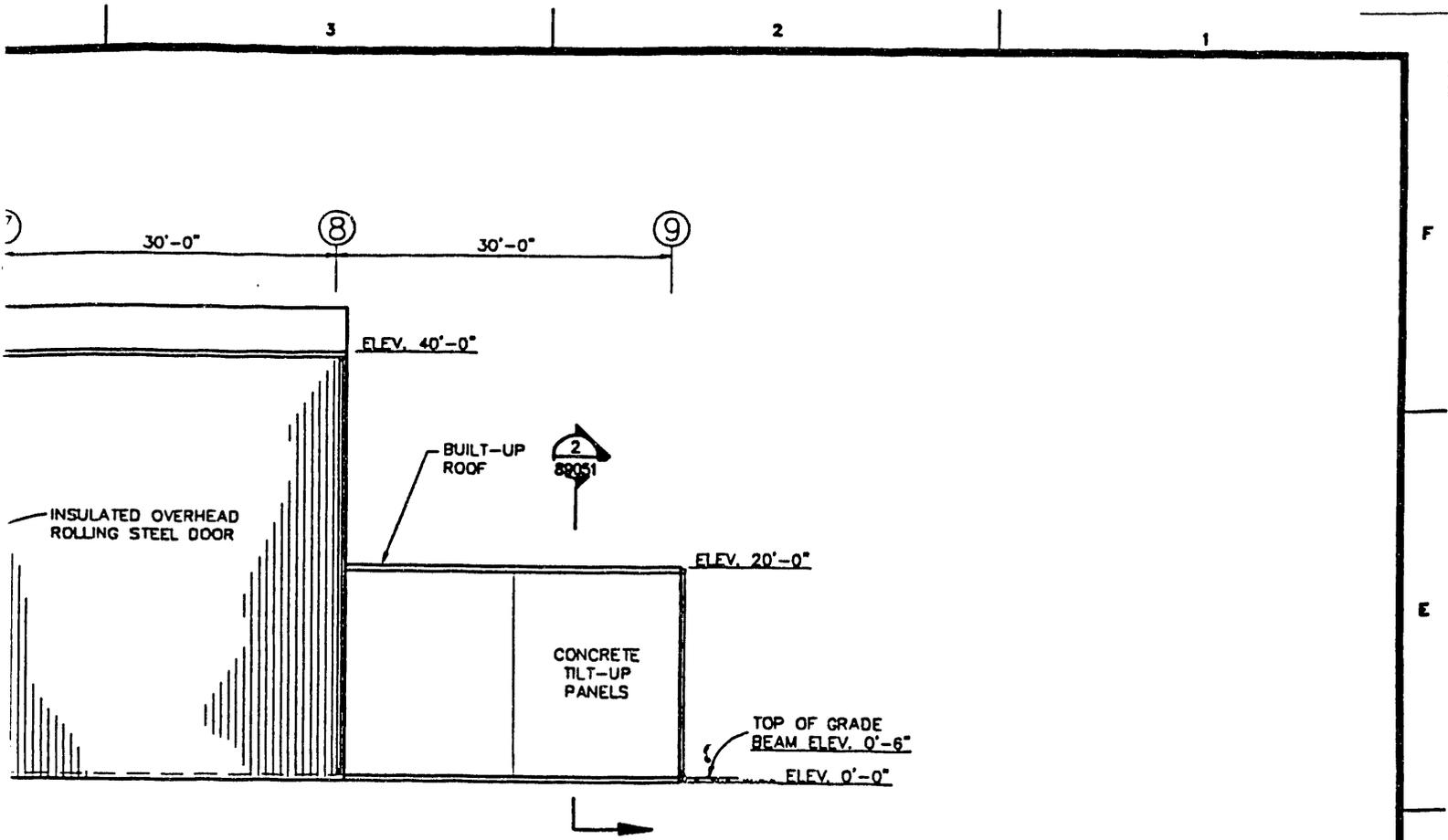
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NUMBER	TITLE	NAME
	DRAWING TRACEABILITY LIST	

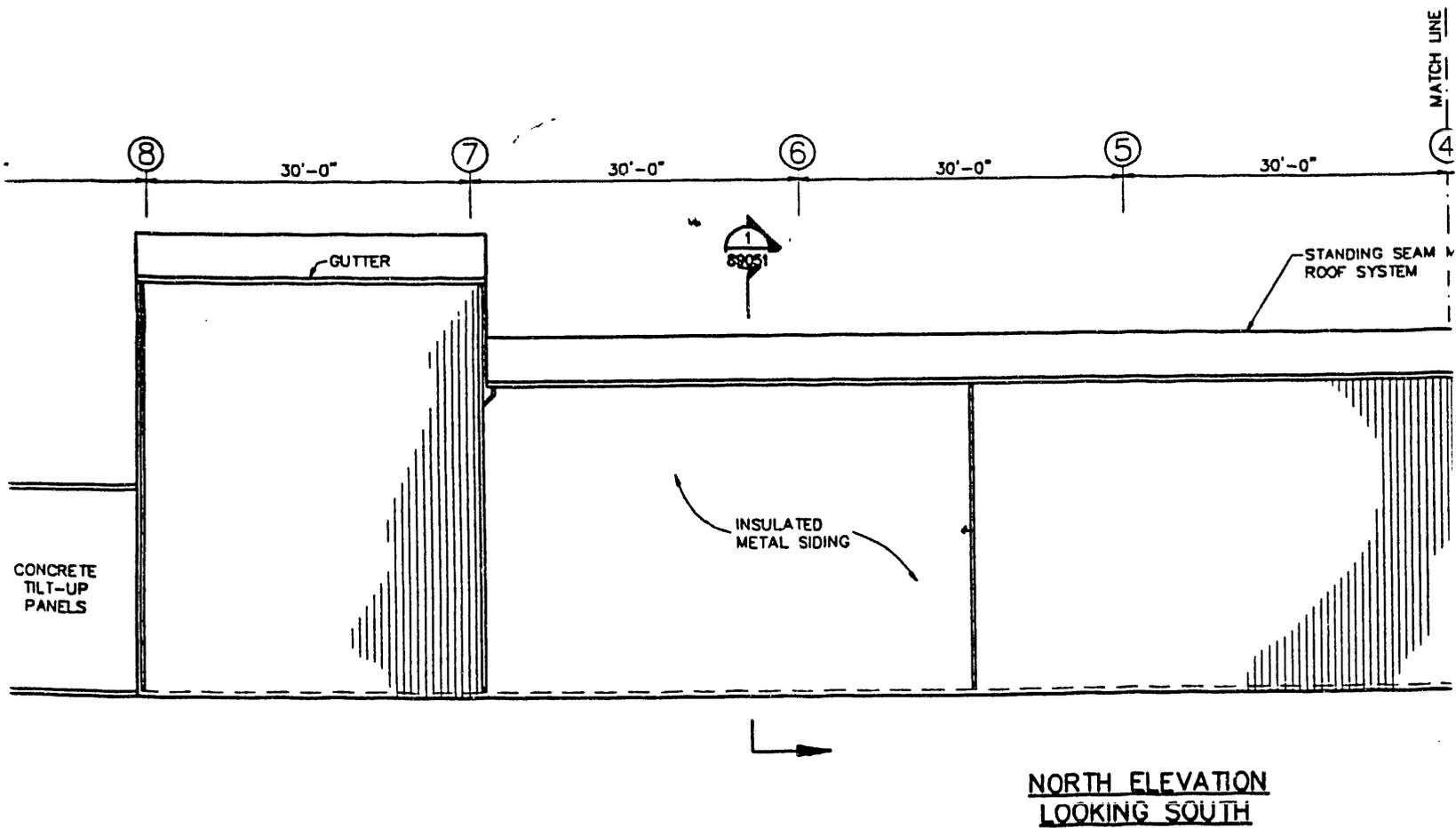
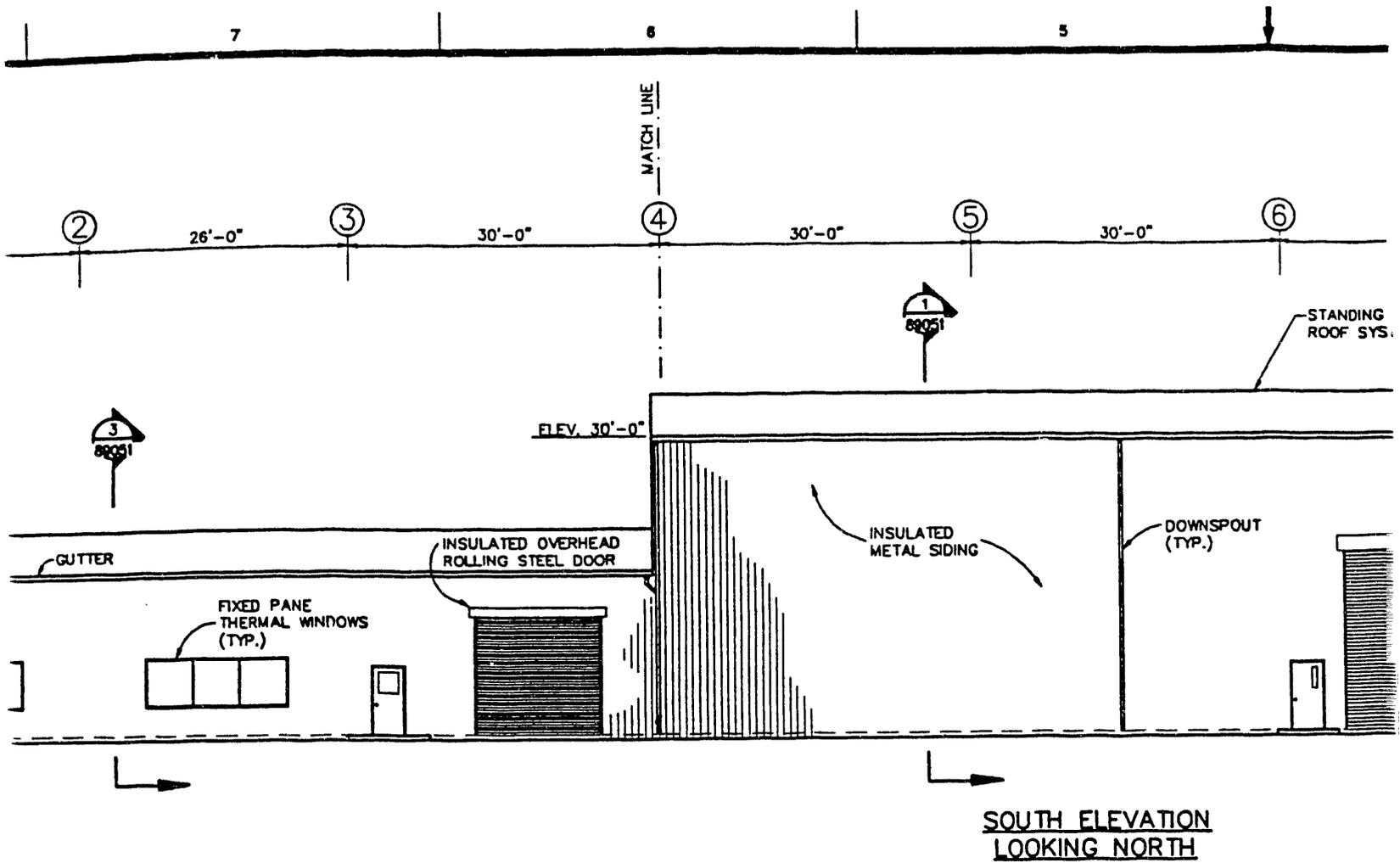


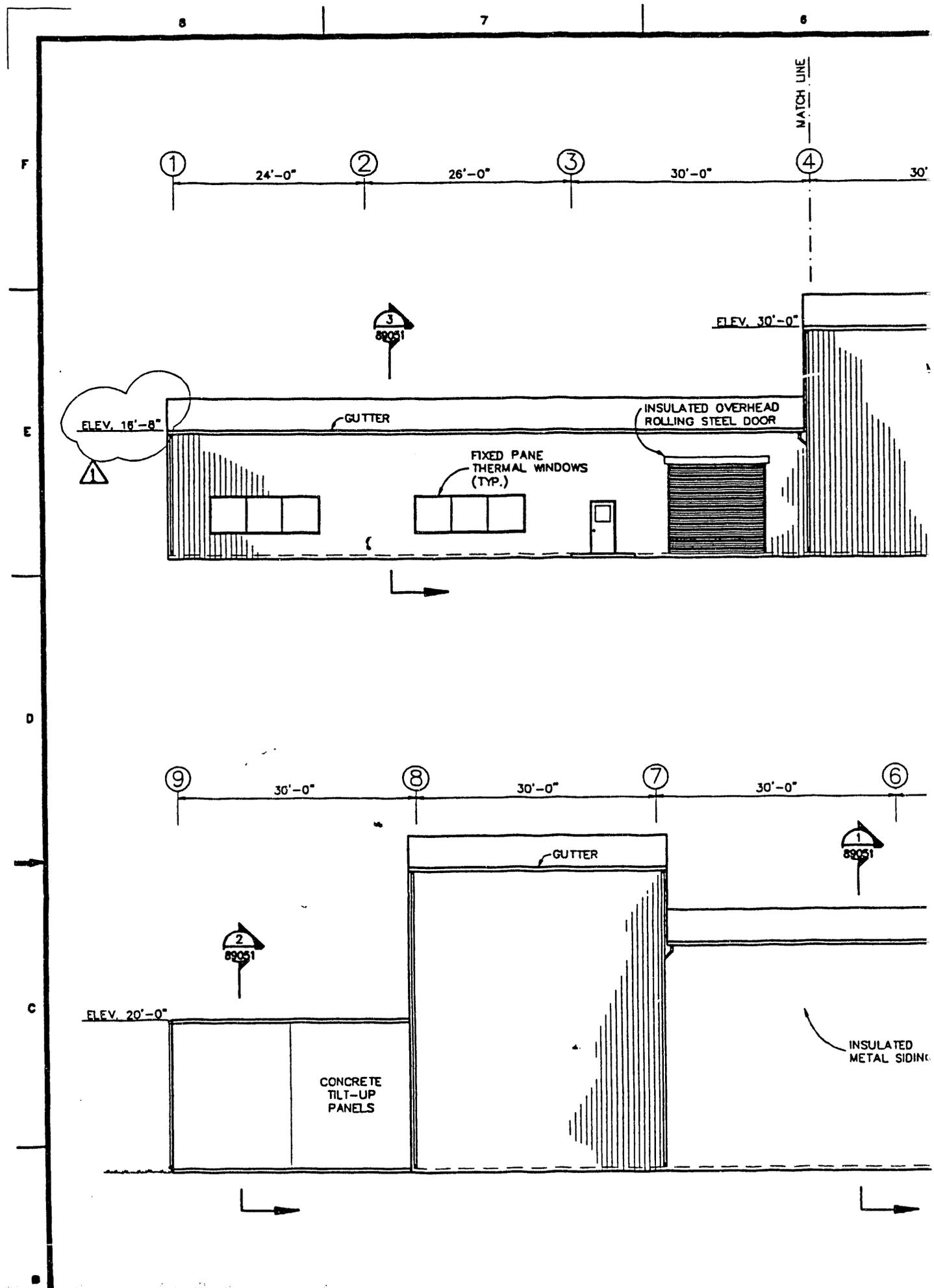


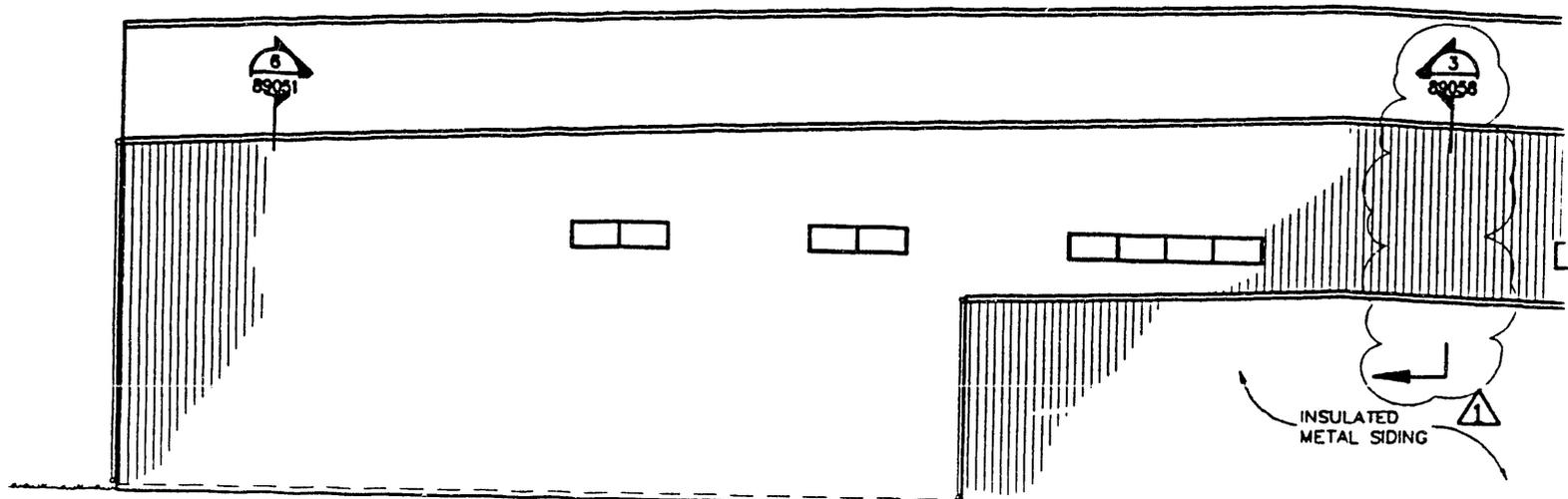
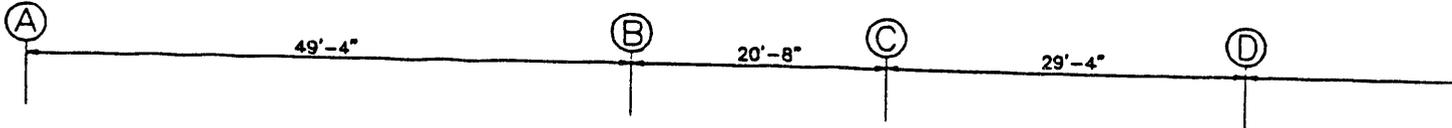
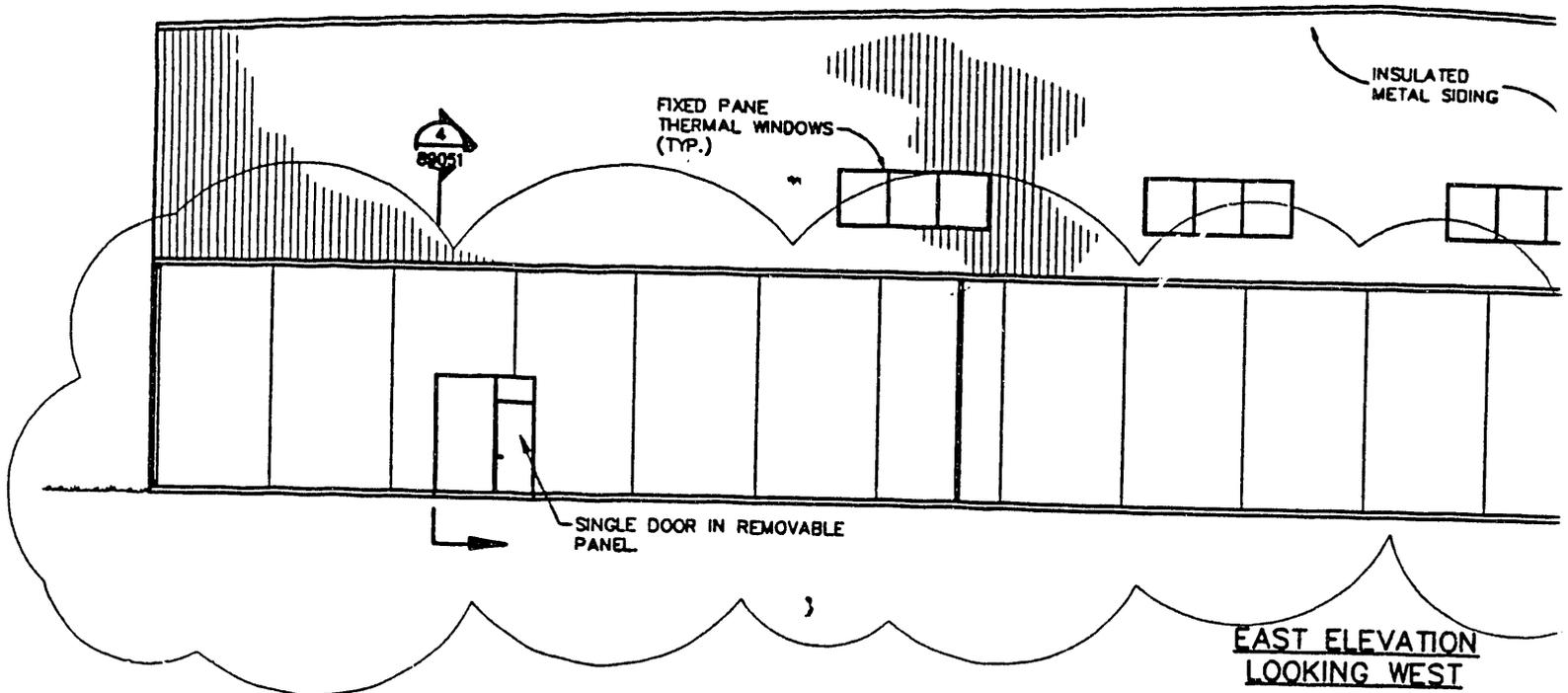
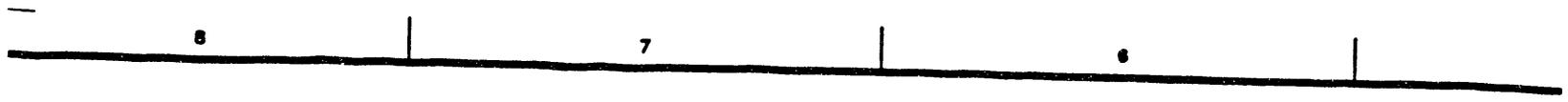


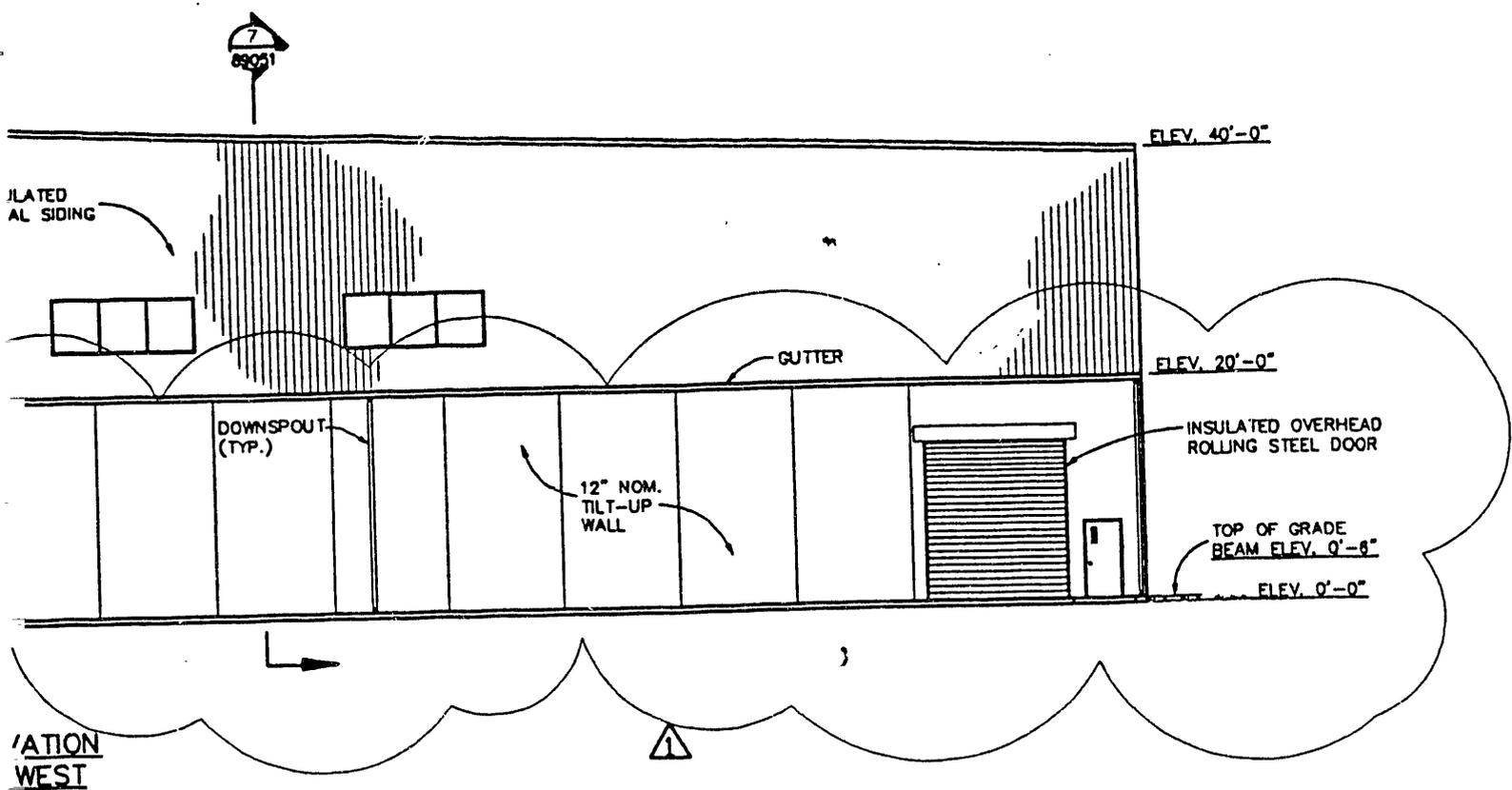
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 H-2-89047 AND 89048

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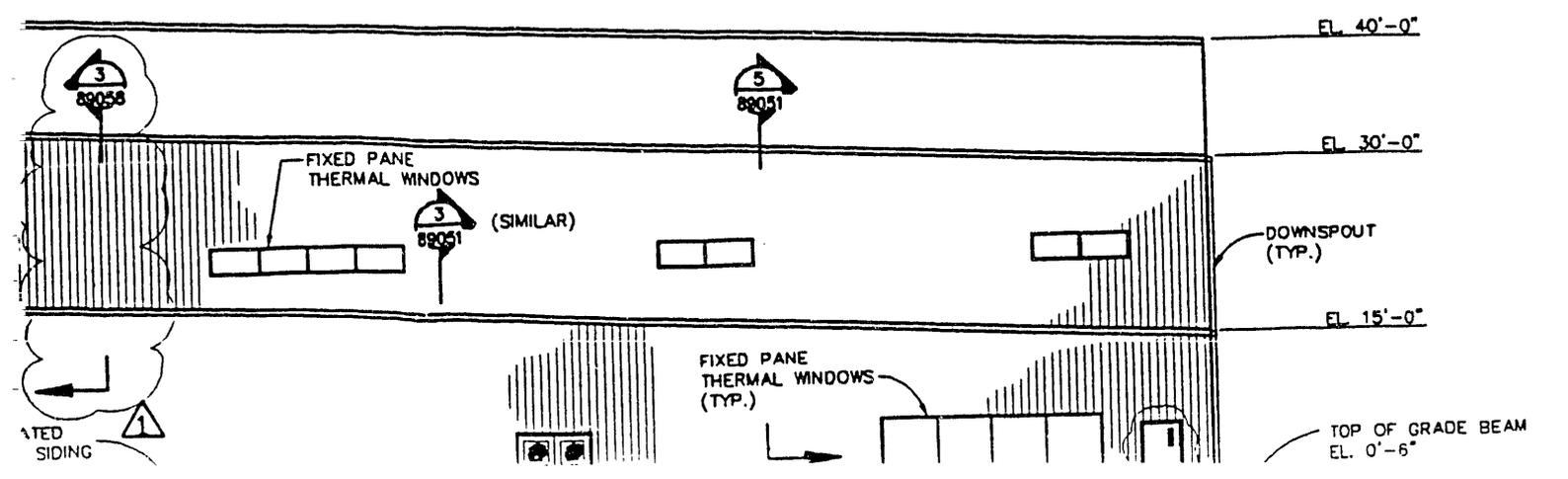




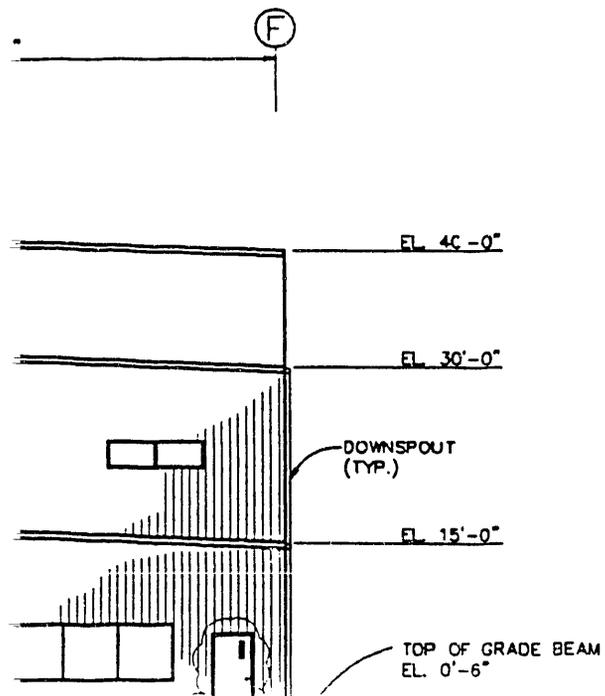
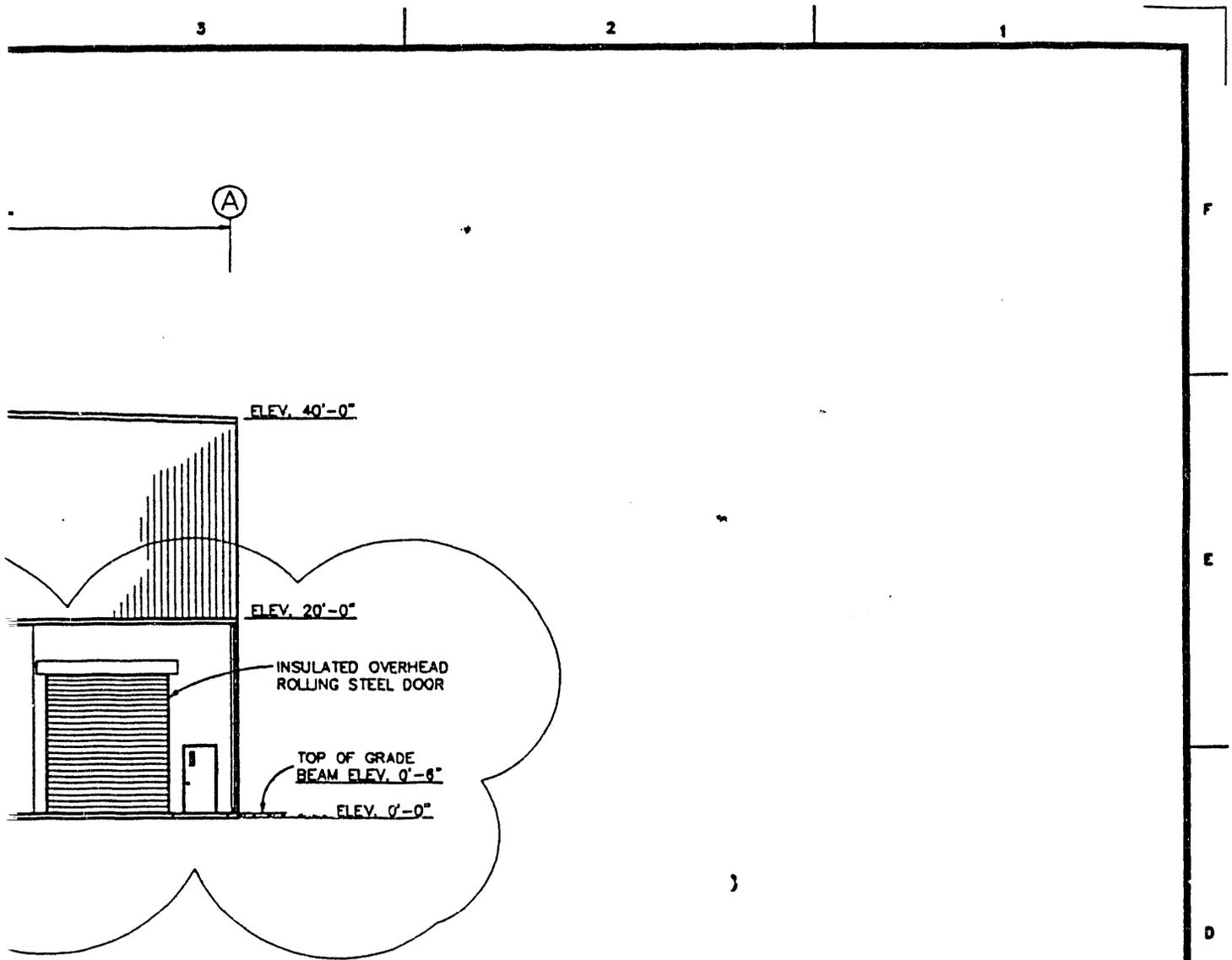




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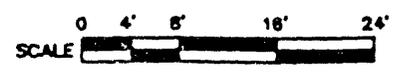
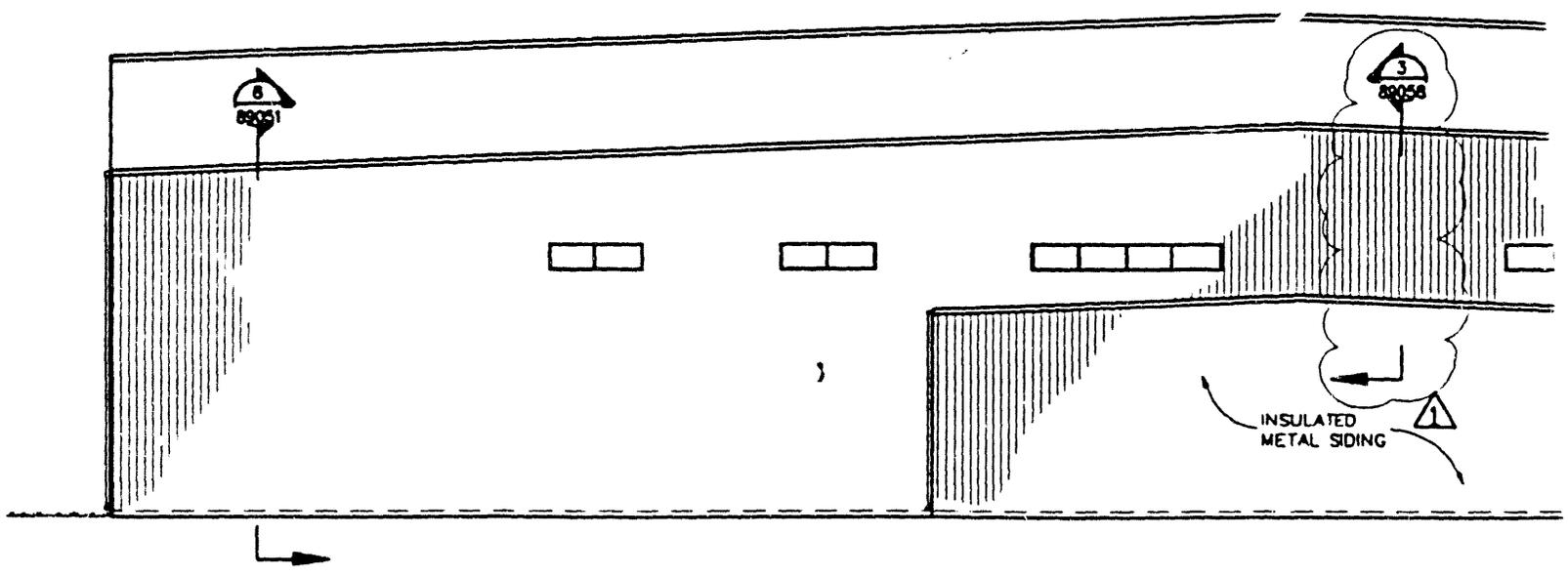
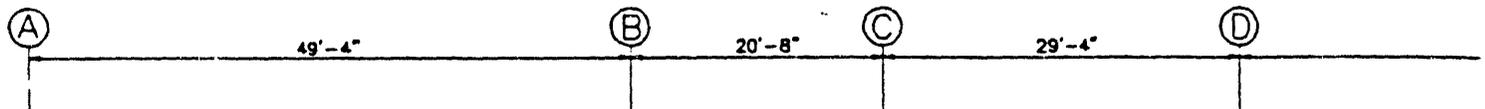
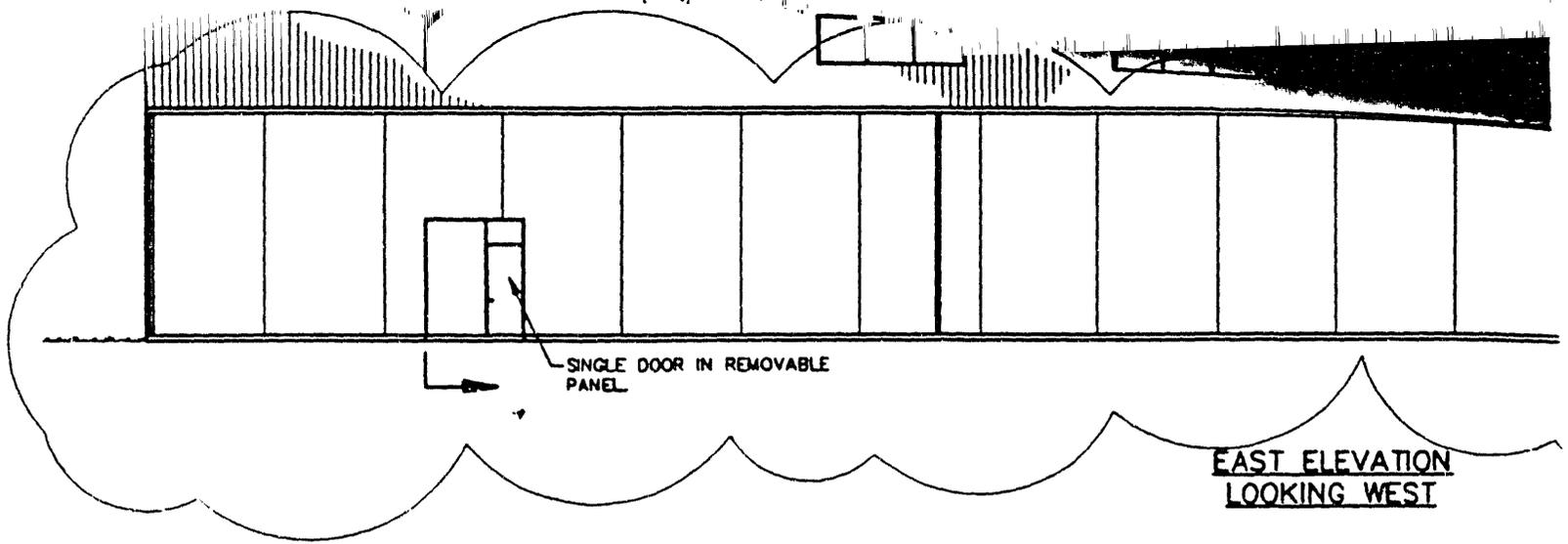


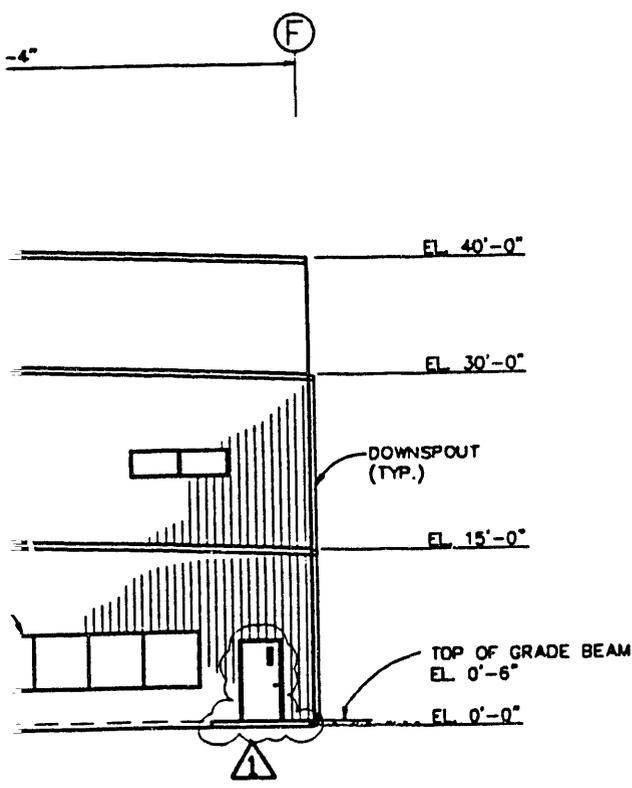
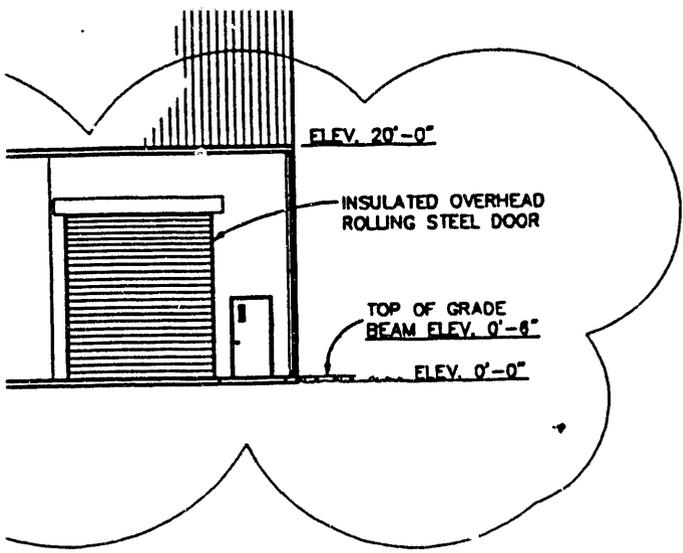
SECTION WEST



NOTES:

1. SEE DRAWINGS H-2-89047 AND H-2-89048
2. GENERAL ARRANGEMENT DRAWINGS. SEE H-2-89029 AND H-2-89030.





NOTES:

1. SEE DRAWINGS H-2-89047 AND H-2-89048
2. GENERAL ARRANGEMENT DRAWINGS. SEE H-2-89029 AND H-2-89030.

[Handwritten signature]
 3/18/93

DATE: 4/10/93

1	ISSUED FOR CONSTRUCTION	MM	EDH	EPH
2	ISSUED FOR DOE DESIGN REVIEW	MM	EDH	EPH
3	ISSUED FOR INTERNAL REVIEW	MM	EDH	EPH
4	ISSUED FOR INTERNAL REVIEW	MAC	EDH	EPH

PROJECT: 0-0001, 0-0001-A, 0-0001-B, 0-0001-C, 0-0001-D, 0-0001-E, 0-0001-F, 0-0001-G, 0-0001-H, 0-0001-I, 0-0001-J, 0-0001-K, 0-0001-L, 0-0001-M, 0-0001-N, 0-0001-O, 0-0001-P, 0-0001-Q, 0-0001-R, 0-0001-S, 0-0001-T, 0-0001-U, 0-0001-V, 0-0001-W, 0-0001-X, 0-0001-Y, 0-0001-Z

U.S. DEPARTMENT OF ENERGY
 DOE FIELD OFFICE, RICHLAND
 JOC CORPORATION

ARCHITECTURAL
 EAST AND WEST ELEVATIONS

DATE: 4/10/93

NO. 2025E

H-2-89050

1/8"-1'-0"

0-1302-004

NUMBER	TITLE	REFERENCES
1		
2		
3		

19930317 • LYNN M. • 89050

ATTACHMENT E

REFERENCES

ATTACHMENT E

REFERENCES

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