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Methyl Chloride Via Oxyhydrochlorination of Methane

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Contractor

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Contract Objective

The purpose of this contract is to develop a process for converting light alkane gases to methyl chloride via oxyhydrochlorination using highly selective, stable catalysts in fixed-bed reactors designed to remove the large amount of heat generated, so as to control the reaction temperature. Further, the objective is to obtain the engineering data base necessary for developing a commercially feasible process and to evaluate the economics of the process.

Task 1.0 Catalyst Definition and Separation Unit Operation Development

Task 2.0 Process Development Unit (PDU) Design Engineering

Task 3.0 PDU Construction and Procurement

Task 4.0 PDU Start-Up

Task 5.0 Evaluation of Packed Bed Technology

Task 6.0 Separation Optimization

Task 7.0 Process Optimization

Task 8.0 Economic Evaluation

Task 9.0 Preliminary Engineering Design Phase II

Task 10.0 Scale-Up Decision and Business Plan to Phase II

Summary of Technical Progress

Significant progress was made this quarter toward the development of a stable heterogenous packed bed catalyst for the oxyhydrochlorination of methane. The short term target for selectivity and conversion of the methane reactant is 80% MeCl selectivity and 20% methane conversion. This quarter's data shows a catalyst which gave an average 18% methane conversion and 78% MeCl selectivity for a 12 day period of time. This encouraging result, which was achieved using a $\text{CH}_4/\text{O}_2/\text{HCl}$ ratio of 100/23/30 with a fluid velocity of 9.0 cm/s and a residence time of about 3 seconds, puts the development on track to meet this short term target.

The development of the product separation system was moved forward a bit more slowly. The reduction to practice in the laboratory environment was plagued with a number of minor operational difficulties. Still, significant progress was made up the learning curve toward demonstration of this technology. Next quarter should bring significant results.

The PDU design engineering effort made significant progress this quarter. Two significant activities occurred. The first is that a bid on a modular unit by Xytel Corp. was received and evaluated. Xytel is a contract engineering firm that specializes in the design and construction of small scale modular processes for the chemical and petrochemical industry. This pre-engineering estimate showed that costs were considerably higher than the original project capital estimates. The primary driver for this cost increase was an increase in the cost of the recovery system. As a result of this work, a rigorous effort was made to eliminate all non-essential equipment and scope of work. A reduced scope was agreed upon and in the second round both Xytel and the Dow Corning in-house facilities engineering team were allowed to bid on the package. This work is in progress. Next quarter the new bids will be received and a design and construction partner will be chosen.

Technical Results

Task 1. Catalyst Definition and Separation Unit Operation Development.

Catalyst Definition-

The primary focus of this quarter's catalyst definition work was the evaluation of catalyst stability. The first "long" experiment for the quarter is reported in Data Set 1. The catalyst was a Cu_6Al cluster supported on silica. As shown on page 2 of this data set, this catalyst, #518, showed a rapid drop in activity from the 15-17% methane conversion range down to a steady 10-11% conversion that remained fairly stable for the 95 hour experiment. The selectivity for this 340 C experiment is plotted on page 3 of the data set and shows very good results, with 93% MeCl. However, due to the low activity the experiment was not extended longer. The initial development goal for this catalyst system is 20% methane conversion and 80% MeCl selectivity. This experiment, as well as all others performed this quarter, was performed at atmospheric pressure with a $\text{CH}_4/\text{O}_2/\text{HCl}$ feed ratio of 100/23/30. Most of the experiments were performed at a set point temperature of 340 C for the 3 zone tube furnace that is used to control temperature. Table 1 provides the average conversions and selectivities for this experiment and all others from this reporting period. In addition, the space velocities, temperatures and Cu loading for the catalyst are shown as well.

The next experiment was performed to serve as a baseline for the supported Cu catalyst stability testing. In this experiment a simple supported Cu salt catalyst was used. This catalyst, #511, was made from a CuCl₂.2H₂O salt and was not promoted in any fashion. More details on this catalyst and others used during this reporting period are found in appendix B. Focusing on the conversion vs time graph found on page 2 of Data Set 2, it is clear that this catalyst was fairly low in activity. In addition the activity dropped from 9-10% conversion to 6-7% conversion, or about 35% in the 140 hour experiment. This catalyst gave an average MeCl selectivity of 87% which is slightly lower at comparable conversion to the previous experiment on the Cu-Al supported cluster catalyst. Note the experimental noise on the selectivity vs time graph on page 3 of Data Set 2. This noise, due to a GC malfunction, was corrected at about 100 hours into the experiment. The apparent shift in selectivity at 100 hours is probably not real. However, the precipitous drop in selectivity at about 130 hours that was matched by a significant rise in the oxygenated by-products is apparently real. An explanation for this sudden shift is not available. This unexplained shift, combined with the low activity of the catalyst was a motivation to evaluate other, modified Cu catalysts for their stability.

Data Set 3 shows the results obtained in the evaluation of another simple Cu salt catalyst. Catalyst #516 was based on a Cu(I) salt. The results are very similar to those found in the above Cu(II) based catalyst. The average methane conversion was 12% and average MeCl selectivity 83%. The experimental record for conversion is found on page 2 of the data set and the selectivity record on page 3. A possible difference in this case is that while the activity is similar to that of the other simple Cu catalyst, there is not the same evidence of deactivation noted. It is possible this is due the increase in copper loading to 2.2% vs. the 1.0% found in catalyst #511.

While it is not immediately obvious from the preceding two experiments, the primary mode of catalyst deactivation in this system is most likely Cu loss from the catalyst surface. As such, one mechanism of coping with this issue would be to use a catalyst with a very high Cu loading to extend the lifetime of the catalyst. Catalyst 163C was evaluated to assess this strategy. This was a purchased catalyst with about 30% weight loading of Cu as CuO. Before use this catalyst was reduced in H₂ to remove the oxide coating and then dried in flowing dry N₂ for 1 hour at 340 C. During this experiment, because experiences from earlier evaluations of this catalyst, thermocouples were placed in the reactor and wired to the outside of the reactor to attempt to measure the exotherm that was expected. The results of this experiment were very interesting. On page 2 of Data Set 4 the conversion vs time graph for this experiment is shown. Note that the data is much more erratic than in most of the previous experiments in this system. While erratic, this data when combined with the selectivity data shown on page 3 of the same data set shows that the first 50 hours of this experiment gave results very close to the 20% conversion, 80% selectivity target. The conversion however, took steep drop at about 50 hours. In order to make some sense of this data the thermocouple profiles are shown on page 4 of the data set. They show the sporadic conversion data was quite understandable. The 3 traces show the furnace setpoint which holds steady at 340 C throughout the experiment. The next trace shows the outside reactor temperature which gives a spike to 400 C about 35 hours into the experiment. It is worth noting that the outside thermocouple was mounted about 2/3 of the way down the long axis of the reactor. The temperature measured in the bed gave two different exotherms, 460 C at 25 hours and 410 C at 45 hours. Clearly, this was not a steady state reactor during this experiment. A possible explanation for the drop in activity seen at 50 hours is that at this point the bed was not able to generate the exotherm needed for the higher conversions.

Another high Cu loading catalyst was evaluated to compare with the result just described. A PETC catalyst, received and pretreated in H₂ before use, was evaluated under our experimental conditions. This catalyst was a CuCl catalyst promoted with Li and La. The Cu weight loading was nominally 30 wt%. Data Set 5 contains our results. As in the experiment just described a thermocouple was put in the reactor bed. In this case, as shown on page 2 of the data set, the temperature at about 35 hours into the run was 560 C! This thermocouple was about 1/2 down the length of the bed. Note that at about 70 hours or twice the exotherm time, the conversion as reported on page 3 plummets. This drop from 25-30% to 11-13% methane conversion occurred over about a 1.5 hour time period. Note also on page 4 and page 1 that the selectivity abruptly changes at this point and the total oxygenate selectivity drops by about 20%, this is accompanied by a corresponding increase in the MeCl selectivity. This temperature impact seems to show very clearly that, in this case, the high initial conversion was caused by an exothermic wave moving through the bed that increase both methane conversion and combustion side reactions. When the wave left the bed both the conversion and the combustion dropped significantly. A similar signal was not seen in the experiment described in Data Set 3, presumably because the apparent existence of multiple exothermic waves confused the experiment.

The experiment described in Data Set 6 is an attempt to determine the 'initiation' temperature for the high metal loading catalysts. Catalyst 163C was used again. In this experiment the temperature was raised slowly by 10 C increments. Data included shows that the reaction was extraordinarily slow starting. A temperature of 340 C was maintained for a significant period of time with very low conversion. It was discovered later, that this oxide catalyst had not been reduced prior to reaction. As such the results are not surprising.

Data Set 7 shows the first experiment that evaluated the use of a copper tetrakis acetonitrile hexafluorophosphate salt as a precursor for the supported catalyst. Catalyst #535 uses this salt and is promoted with lanthanum and lithium salts. This catalyst, while using the PETC promoters, is a significantly different catalyst due to it's low metal loading (about 2% Cu) and the use of the fluorophosphate salt as a Cu source. Page 2 of the data set shows the conversion vs time profile for this experiment, note that much of the data prior to 35 hours was lost due to a computer malfunction on the CAMILE control system used for these experiments. The conversion data remaining shows a very flat profile with < 10% loss in conversion in the 140 hour experiment. Page 3 shows that the selectivity was fairly stable also, averaging 75% with some variation after 75 hours. This 21% conversion, 75% selectivity result that was sustained for 140 hours is a very encouraging result that is near the target for our PDU system. Note on page 4 that even with the 2% metal loading an exotherm was found by a thermocouple in the catalyst bed. This exotherm was only on the order of 10-20 C, but may still be significant. The differential between the 370 C outside reactor temperature and the 340 C furnace control temperature is real and is not a function of the heat of reaction. This condition remains constant throughout the work performed in this experimental apparatus.

Given the success of catalyst #535 in the 140 hour experiment, an extended trial was performed to see the impact of extended reaction time. Data Set 8 shows a 14 day experiment under the same conditions as the data found in Data Set 7. The page 2 conversion graph shows the catalyst increasing in conversion for the first 10-20 hours. After this the data shows a slow steady decline that is slightly more exaggerated than that seen in the previous experiment. The gap seen between 75 and 90 hours is again due to a computer malfunction. The deactivation of this catalyst is approximately 35% over the first 12 days. The average conversion during this period was 18% with a selectivity of 79%, another very encouraging result.

Separation Process Definition-

The primary emphasis of the separation process definition work undertaken this quarter focused on the startup of a laboratory absorber unit described in last quarter's report. This unit is a direct contact gas in liquid absorber column which is attached to a laboratory screening reactor. This will be used as a screening tool for process solvent selection and as an aid in PDU column design. The successful operation of a small column like this in a laboratory setting is quite challenging. Continuous work throughout the quarter made major progress toward successful operation, but at quarter's end it had still not successfully recovered a significant amount of MeCl due to an array of operational difficulties. Some of the operational problems will be briefly discussed here to illustrate the development of this laboratory experiment.

A key issue in the successful operation of this continuous liquid absorber is the delivery of a continuous, but extremely small, stream of a cooled process solvent to the absorber column. Work was performed with two different process solvents, Mobil SHC-624 oil and Multitherm 503. The target set temperature for solvent introduction to the column is -20 C. This created a number of problems associated with water freezing in the chiller reservoir and plugging the micropump being used for moving the solvent from the chiller to the column. The total delivery rate of solvent is in the 1-5 ml/min range, depending on desired L/G loading of the column.

An additional issue that proved to be very hard to solve was generating the appropriate pressure drops through the system. In order to get solvent flow down through the column and countercurrent gas flow up through the column the pressure drop across the column must be carefully coordinated with pressures downstream of the column. The basic problem is that the column sits above a phase separator where the processed solvent falls containing the absorbed MeCl. The gas flow enters the column above the phase separator. With this common design, the pressure in the phase separator must be slightly higher than the entering gas stream, this allows the gas to flow up through the column. To balance this and allow the liquid to flow down into the slightly higher pressure, the void volume of the column packing must be large. This problem was addressed by studying the flow dynamics via simple observation and observing which flow condition, packing combinations allowed appropriate flow. One additional problem was that the tubing from the column bottom to the phase separator was too small and solvent blockage of this line caused a vapor lock in the system. Replacement with a larger line solved this problem.

Work in the next quarter will continue on demonstrating this removal technology in the laboratory. Proper packing selection should allow this column to operate, and allow process solvents to be evaluated. In addition the plans for extensive solvent testing are in place for next quarter. Limited acid stability and thermal stability tests were completed this quarter, however the bulk of this work will occur next quarter and the few results from this quarter will be included in that report.

Task 2.0 Process Development Unit Design Engineering

Process Description and Definition-

The initial pre-engineering estimate from Xytel Corporation was received this quarter. The estimate for design and construction of a modular process unit to be built off-site and shipped to Carrollton was much higher than anticipated. The principal cost inflation as compared with historical estimates was the impact of the proposed absorber/stripper unit for MeCl recovery from the reactor effluent stream. Several decisions were made in light of this cost inflation. The first, as discussed at a March project management team meeting, was the elimination of the distillation column and associated equipment for the separation of a pure MeCl stream. This technology has been previously demonstrated, and the technological impact of this scope reduction was felt to be minimal. Several other small deletions were also made. After these changes in scope the process design package was sent again to Xytel for re-bidding. In addition DCC in house engineering was contacted and a bid on the process was requested for this internal option for design and construction. This limited the Process Development Unit (PDU) design engineering progress made during this period. Both estimates will be received next quarter and a decision will be made as to how to proceed with design, procurement and construction of the PDU.

List of Tables

Table 1 - Copper Based Catalysts for the Oxyhydrochlorination of Methane

Table 1 Copper Based Catalysts for the Oxyhydrochlorination of Methane

Catalyst Number	PETC	511	516	518	163C	535	535
%Cu on Catalyst	30	1.0	2.2	1.9	30	1.9	1.9
Temperature (C)	315	340	340	340	340	340	340
Space Velocity (cm/s)	9	9	9	9	9	9	9
CH ₄ Conversion	19	8	12	11	20	18	21
HCl Conversion	55	25	36	38	61	69	80
O ₂ Conversion	50	20	29	26	54	47	56
% CH ₃ Cl	74	87	83	93	77	79	75
%CH ₂ Cl ₂	7	2	4	5	6	14	18
%CHCl ₃	0	0	0	0	0	0	0
%CCl ₄	0	0	0	0	0	0	0
%CO	7	0	7	0	0	2	2
%CO ₂	12	11	6	2	16	4	4

*all data in this table taken at atmospheric pressure, CH₄/O₂/HCl : 100/22.8/29.6, HCl and O₂ conversions are calculated.

Data Appendices

Data Appendix A- Experimental Data Sets

Data Appendix B- Catalyst Synthesis Information

Data Appendix A
Experimental Data Sets

00006701 OPERATOR NAME: B. CRUM DATE: 31-DEC-82
 00006701 LOG BOOK #: 10346 PAGE # 128
 00006701 RUN #: 10346057 CATALYST #: 518

00006701 CATALYST NAME:

00006701 COMMENTS: CAT 518 RUN AT 340

00006701

00006701

00006701 MASS OF CATALYST (g): 3.09

00006701 REACTOR INSIDE DIAM (CM): 0.6

00006701 CATALYST BED HEIGHT (CM): 24

FLUID VELOCITY 9.0 CM/SEC
 RUNTIME 95 HRS

00006567 TEMPERATURE RAMPING EXPERIMENT FOR HOOD #6

	INITIAL TEMP (DEG C)	FINAL TEMP (DEG C)	ABSOLUTE RAMP RATE (DEG C / MIN)
BOTTOM	340	340	2
MIDDLE	340	340	2
TOP	340	340	2

(INITIAL TEMPERATURE CAN BE GREATER THAN FINAL TEMPERATURE)

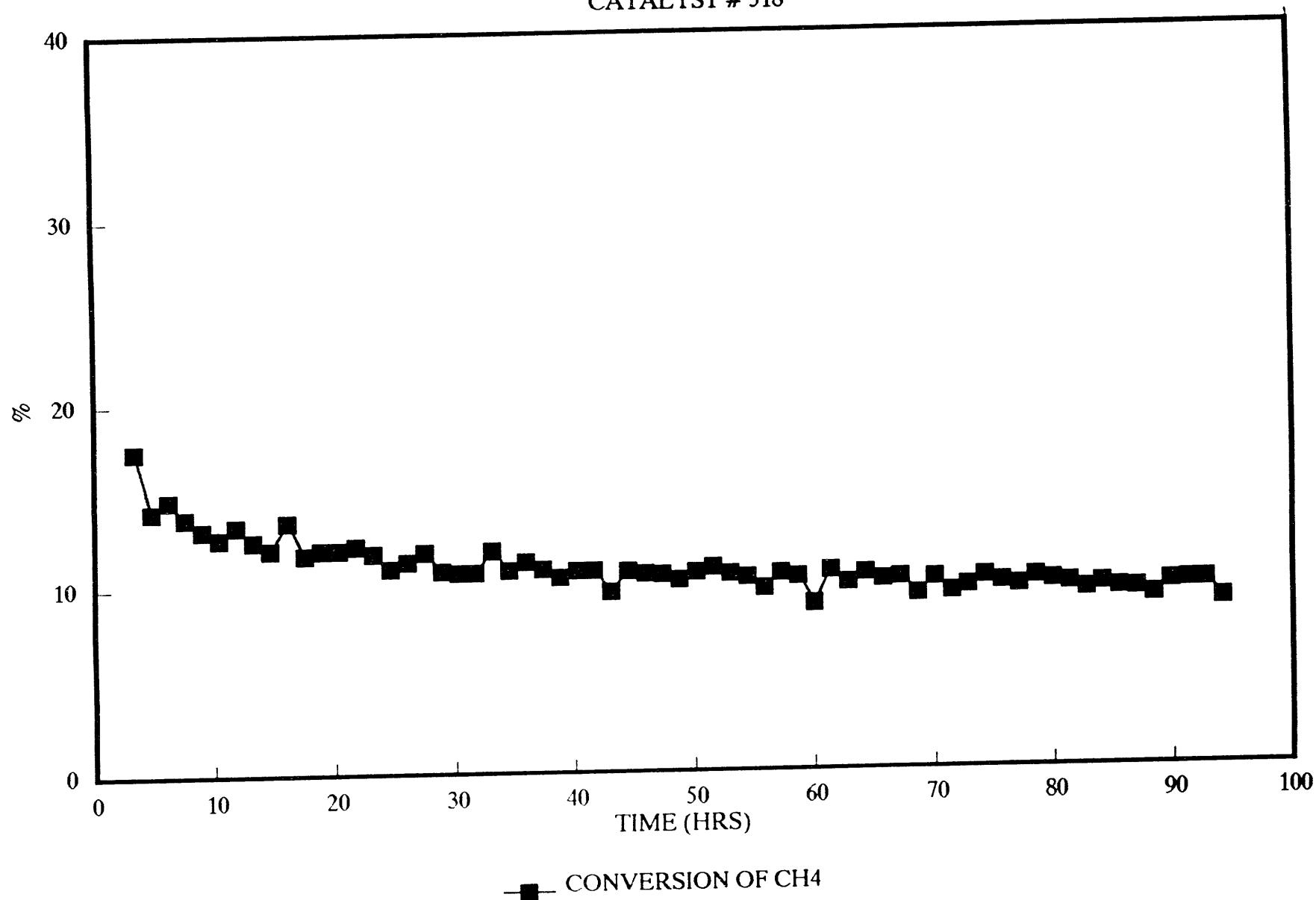
00006567 CH4 FLOW RATE (CC/MIN): 100 O2 FLOW RATE (CC/MIN): 22.8
 00006567 HCl FLOW RATE (CC/MIN): 29.6 AUX FLOW RATE (CC/MIN): 0

Time	A16CO	A16CO2	A16COX	A16M1	A16M2	A16M3	A16M4	ID6	MBC8	Q8CH4C	Q8HOLC	TQ1612
12063	0	26	26	74	0	0	0	1	100	17	44	340
17149	0	2	2	88	9	0	0	1	83	14	51	340
22248	0	1	1	91	7	0	0	1	82	15	53	340
27347	0	1	1	92	7	0	0	1	84	14	49	340
32447	0	1	1	92	7	0	0	1	85	13	47	340
37547	0	1	1	92	6	0	0	1	88	13	47	340
42641	0	1	1	92	6	0	0	1	87	13	45	340
47741	0	1	1	92	6	0	0	1	87	12	43	340
52848	0	1	1	93	6	0	0	1	87	14	48	340
57947	0	1	1	93	6	0	0	1	87	12	41	340
63084	0	1	1	93	6	0	0	1	87	12	43	340
68148	0	1	1	93	6	0	0	1	88	12	43	340
73248	0	1	1	93	6	0	0	1	88	12	43	340
78340	0	1	1	93	8	0	0	1	88	12	43	340
83448	0	1	1	93	5	0	0	1	88	12	42	340
88548	0	1	1	93	5	0	0	1	89	11	39	340
93840	0	1	1	94	6	0	0	1	89	11	40	340
98748	0	1	1	93	5	0	0	1	89	12	41	340
103848	0	1	1	93	5	0	0	1	89	11	38	340
108947	0	1	1	93	5	0	0	1	89	11	37	340
114047	0	1	1	93	5	0	0	1	89	11	38	340
119149	0	1	1	93	5	0	0	1	89	12	41	340
124248	0	1	1	93	5	0	0	1	89	11	38	340
129347	0	1	1	94	5	0	0	1	89	11	40	340
134447	0	1	1	94	5	0	0	1	89	11	38	340
139549	0	1	1	94	5	0	0	1	89	10	37	340
144648	0	1	1	93	5	0	0	1	90	11	38	340
149748	0	1	1	94	5	0	0	1	90	11	38	340
154865	0	1	1	94	5	0	0	1	91	10	34	340
159947	0	1	1	94	5	0	0	1	90	11	37	340
165047	0	1	1	94	5	0	0	1	90	11	37	340
170186	0	1	1	94	5	0	0	1	90	10	36	340
175272	0	1	1	94	5	0	0	1	90	11	37	340
180381	0	1	1	94	5	0	0	1	90	11	38	340
185507	0	1	1	94	4	0	0	1	91	11	37	340
190641	0	1	1	94	4	0	0	1	91	10	36	340
195780	0	1	1	94	4	0	0	1	91	10	34	340
200801	0	2	2	94	5	0	0	1	91	11	38	341
205044	0	1	1	94	5	0	0	1	91	10	36	340
211144	0	1	1	94	4	0	0	1	91	9	31	340
216228	0	1	1	95	4	0	0	1	92	11	37	340
221328	0	1	1	94	4	0	0	1	93	10	35	340
226445	0	2	2	94	5	0	0	1	91	10	36	340
231529	0	1	1	95	4	0	0	1	91	10	35	340
236629	0	1	1	94	4	0	0	1	91	10	36	340
241762	0	1	1	94	4	0	0	1	91	9	32	340
246669	0	1	1	95	4	0	0	1	92	10	36	340
251969	0	1	1	95	4	0	0	1	92	9	33	340
257086	0	1	1	95	4	0	0	1	92	10	34	340
262186	0	1	1	95	4	0	0	1	91	10	35	340
267288	0	1	1	95	4	0	0	1	91	10	34	341
272388	0	1	1	95	4	0	0	1	91	10	34	340
277488	0	1	1	95	4	0	0	1	91	10	35	340
282580	0	1	1	95	4	0	0	1	91	10	35	340
287681	0	1	1	95	4	0	0	1	91	10	34	341
292788	0	1	1	95	4	0	0	1	91	9	33	340
297888	0	1	1	95	4	0	0	1	91	10	34	340
302988	0	1	1	95	4	0	0	1	91	10	33	340
308089	0	2	2	94	4	0	0	1	93	10	33	340
313189	0	1	1	95	4	0	0	1	91	9	32	340
318289	0	1	1	95	4	0	0	1	91	10	34	340
323386	0	1	1	95	4	0	0	1	92	10	34	340
328489	0	1	1	95	4	0	0	1	92	10	34	340
333581	0	1	1	95	4	0	0	1	91	9	30	340
338687	0	1	1	95	3	0	0	1	91	9	30	340

Time	A16CO	A16CO2	A16COX	A16M1	A16M2	A16M3	A16M4	ID6	MBC8	Q8CH4C	Q8HOLC	TQ1612
AVG	0	2	2	93	5	0	0	1	90	11	38	340
STD	0	3	3	3	1	0	0	0	3	2	5	340

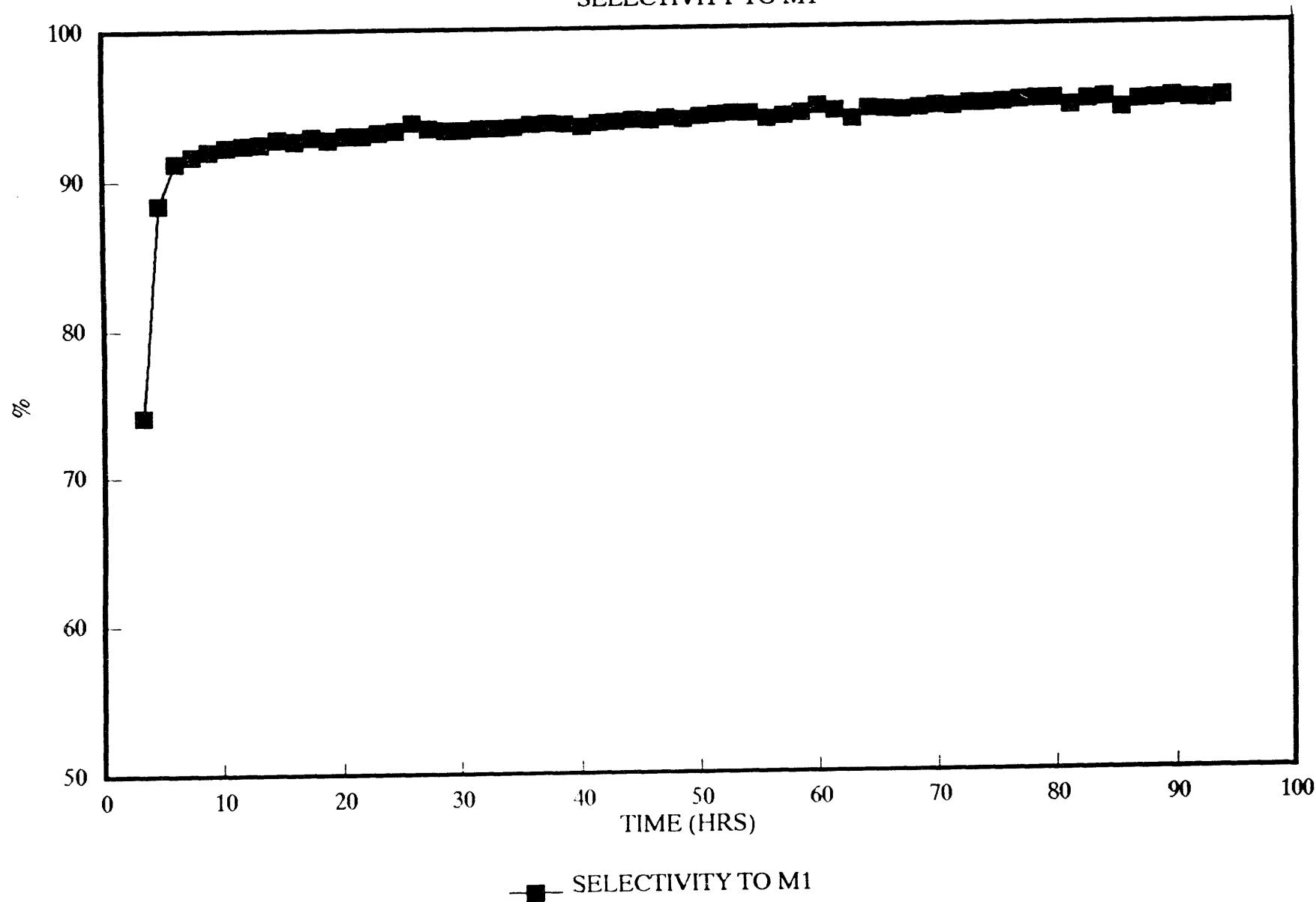
RUN 10346057 CONVERSION

CATALYST # 518



RUN 10346057 SELECTIVITY

SELECTIVITY TO M1



0000048 OPERATOR NAME: B. CRUM DATE: 08-JAN-83

0000048 LOG BOOK #: 10446 PAGE #: 132

0000048 RUN #: 1044699 CATALYST #: 611

0000048 CATALYST NAME: Duricat on 08 10446

0000048 COMMENTS: SINGLE TEMP 1440 LONG RUN

0000048

0000048

0000048 MASS OF CATALYST (G): 2.04

FLUID VELOCITY: 8.0 CM/SEC

0000048 REACTOR INSIDE DIAM (CM): 0.6

RUN TIME: 140 HRS

0000048 CATALYST BED HEIGHT (CM): 94

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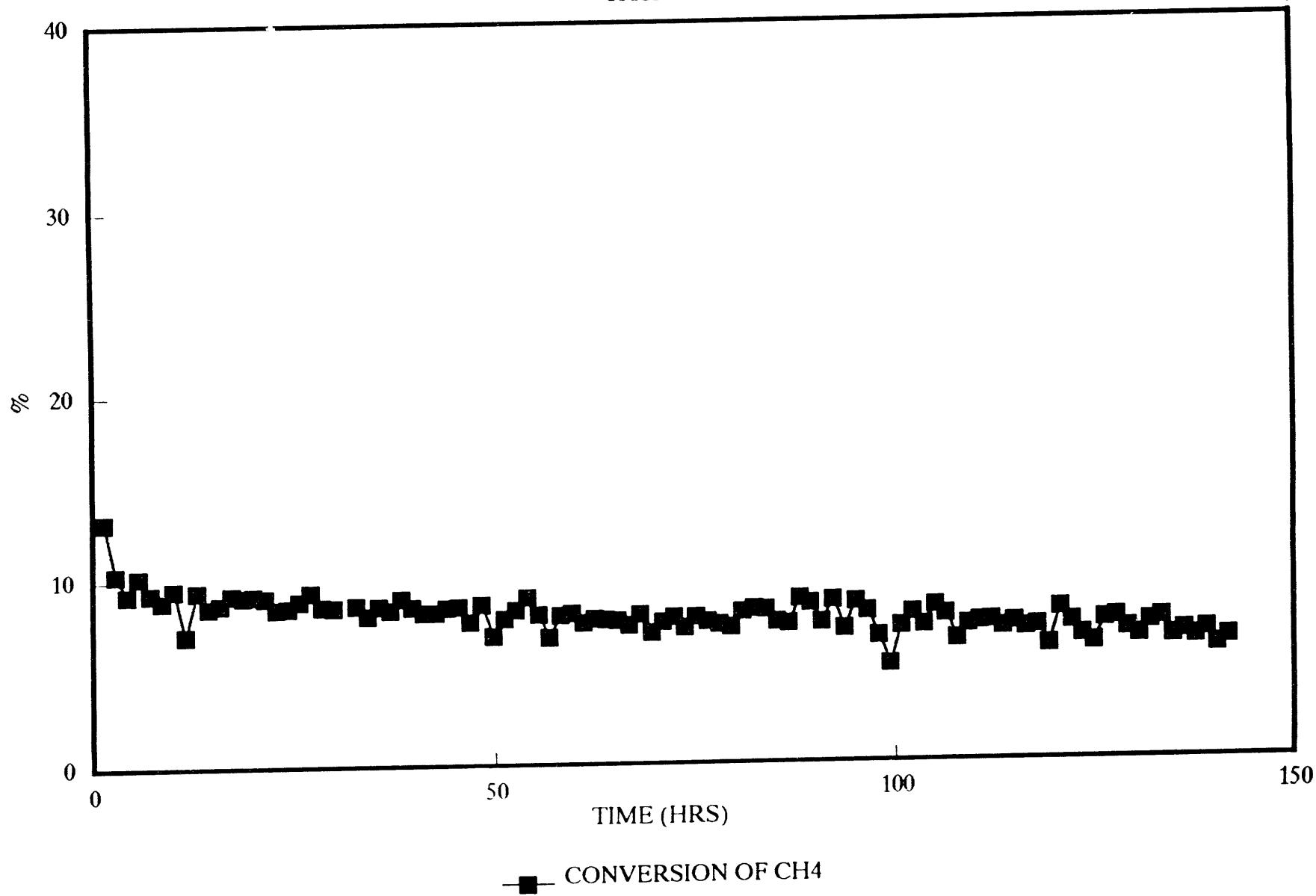
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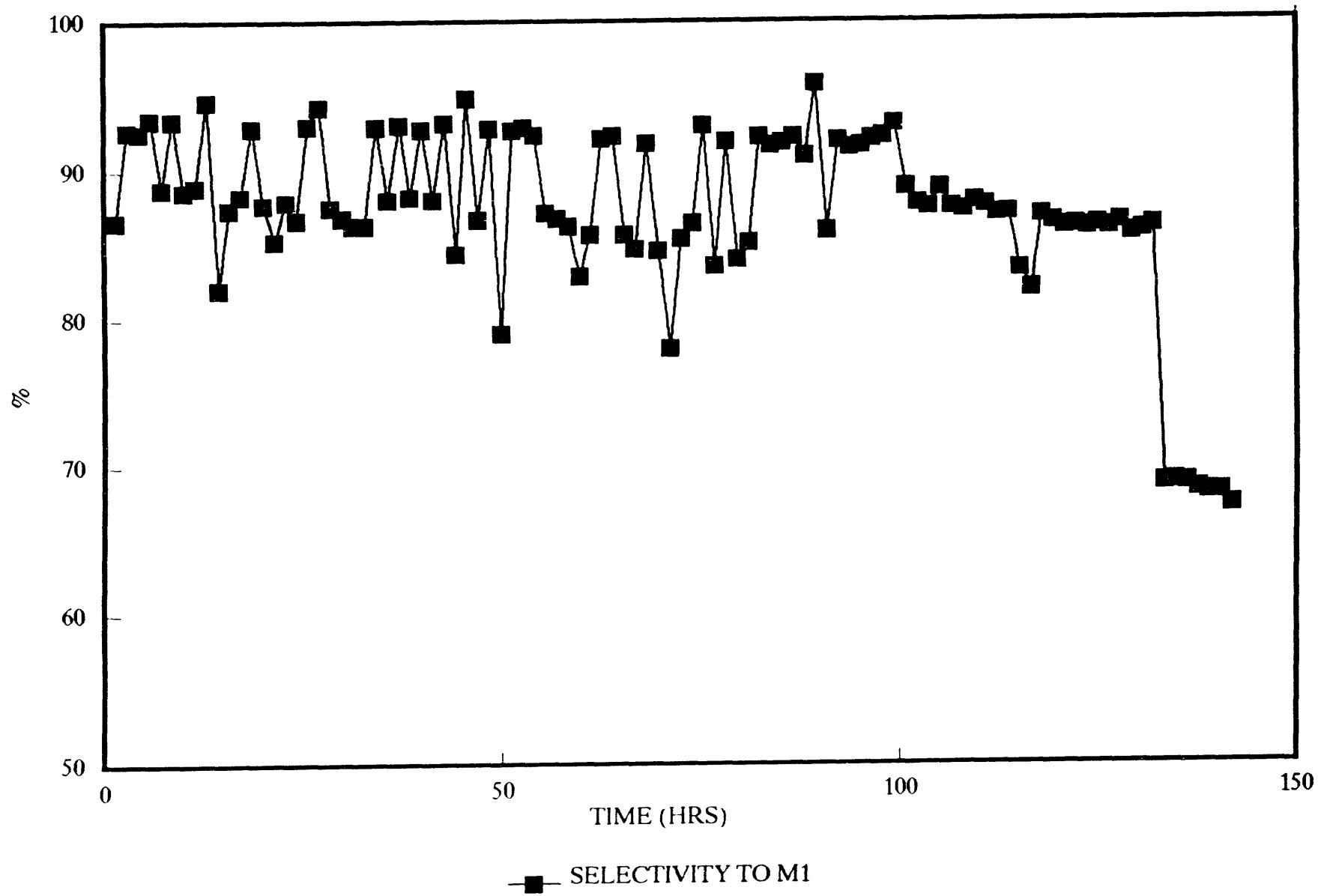
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RUN10346059
CATALYST 511



RUN 10346059

CATALYST 511



■ SELECTIVITY TO M1

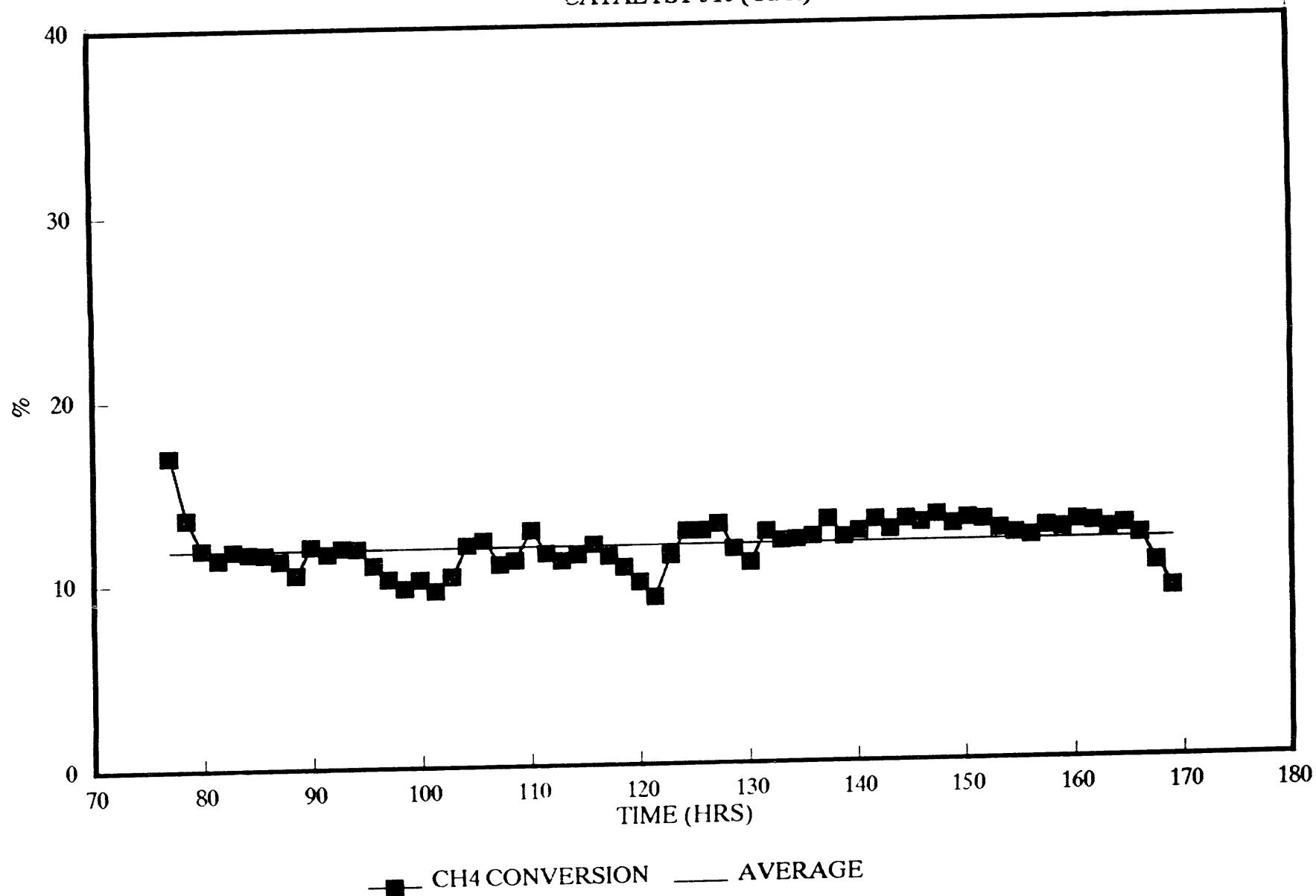
00003970 HOOD #6 RAMPING EXPERIMENT DEFINITION
 00003970
 00003970
 00003970 OPERATOR NAME: B. CRUM DATE 05-MAR-93
 00003970 LOG BOOK #: 10348 PAGE #: 148
 00003970 RUN #: 10348066 CATALYST #: 516
 00003970 CATALYST NAME: CuCl on Silica
 00003970 COMMENTS: Repeat of run 063 conditions with this cat. 2nd try
 00003970
 00003970
 00003970 MASS OF CATALYST (g) 30
 00003970 REACTOR INSIDE DIAM (CM): 0.6
 00003970 CATALYST BED HEIGHT (CM): 25.4
 00003951 TEMPERATURE RAMPING EXPERIMENT FOR HOOD #6
 00003951
 00003951 INITIAL FINAL ABSOLUTE
 00003951 TEMP TEMP RAMP RATE
 00003951 (DEG C) (DEG C) (DEG C / MIN)
 00003951
 00003951 BOTTOM: 340 340 5 FLUID VELOCITY 9.0 CM/SEC
 00003951 MIDDLE: 340 340 5 RUN TIME 170 HRS
 00003951 TOP: 340 340 5
 00003951
 00003951 (INITIAL TEMPERATURE CAN BE GREATER THAN FINAL TEMPERATURE)
 00003951
 00003951 CH4 FLOW RATE (CC/MIN): 100 O2 FLOW RATE (CC/MIN): 22.8
 00003951 HCl FLOW RATE (CC/MIN): 29.6 AUX FLOW RATE (CC/MIN): 0

Time	A16CO	A16CO2	A16COX	A16M1	A16M2	A16M3	A16M4	IDB	MBC6	Q6CH4C	Q6HCLC	TQ1612
277013	4	5	9	81	10	0	0	1	78	17	58	341
282172	4	3	7	86	7	0	0	1	85	14	46	341
287330	3	1	4	88	8	0	0	1	86	12	42	340
292492	5	3	8	86	6	0	0	1	89	11	37	340
297852	5	3	9	86	5	0	0	1	91	12	38	340
302811	5	4	9	87	3	0	0	1	91	12	37	340
307973	5	3	9	88	3	0	0	1	88	12	37	340
313132	6	4	10	87	4	0	0	1	91	11	36	340
318291	5	4	9	87	5	0	0	1	88	10	34	341
323453	7	5	11	89	0	0	0	1	82	12	36	341
328586	5	5	10	85	5	0	0	1	88	12	37	340
333711	7	6	13	87	0	0	0	1	92	12	35	340
338872	6	4	11	84	5	0	0	1	91	12	38	340
344030	7	5	11	84	5	0	0	1	90	11	34	340
349188	8	4	10	84	6	0	0	1	88	10	33	341
354292	7	6	14	80	6	0	0	1	91	10	30	340
358452	6	4	10	85	5	0	0	1	88	10	33	340
364811	7	5	12	83	4	0	1	1	90	9	30	340
369773	6	5	11	85	4	0	0	1	89	10	32	340
374884	7	5	12	82	6	0	0	1	91	12	38	341
380210	7	5	12	82	6	0	0	1	91	12	38	340
385371	7	6	13	82	5	0	0	1	91	11	34	340
390532	7	5	11	84	4	0	0	1	87	11	34	340
395752	8	6	14	80	6	0	0	1	91	13	39	340
400912	7	5	13	87	0	0	0	1	90	11	34	340
406073	7	6	13	81	6	0	0	1	88	11	34	340
411232	9	6	15	85	0	0	0	1	92	11	32	340
416451	8	6	14	81	4	0	0	1	90	12	36	340
421612	7	5	13	84	3	0	0	1	91	11	34	341
426772	8	6	14	82	4	0	0	1	91	11	32	340
431930	8	7	15	85	0	0	0	1	93	10	28	340
437092	7	6	13	87	0	0	0	1	91	9	26	340
442313	7	6	13	83	4	0	0	1	89	11	35	340
447533	8	7	14	80	5	0	0	1	88	13	39	340
452753	0	7	7	87	6	0	0	1	88	12	42	340
457972	9	8	17	83	0	0	0	1	92	13	37	339
483130	7	4	12	88	0	0	0	1	90	11	34	340
488350	7	6	14	82	4	0	0	1	89	11	33	340
473571	9	8	17	79	4	0	0	1	90	12	37	340
478701	8	6	14	81	5	0	0	1	87	12	37	340
483881	6	7	15	80	5	0	0	1	90	12	36	340
489052	9	7	16	78	6	0	0	1	88	12	37	339
494212	9	7	16	79	5	0	0	1	85	13	39	340
499372	9	8	17	77	6	0	0	1	89	12	36	340
504532	9	7	16	78	5	0	0	1	88	12	37	341
509752	9	7	16	81	4	0	0	1	88	13	38	340
514889	8	7	16	82	2	0	0	1	87	12	38	340
520070	9	7	16	78	5	0	0	1	88	13	39	340
525292	9	7	17	78	5	0	0	1	90	13	39	340
530511	8	6	14	80	8	0	0	1	83	13	41	340
535732	10	8	18	81	0	1	0	1	90	13	38	340
540929	9	8	17	79	4	0	0	1	85	13	38	340
546052	10	8	18	78	4	0	0	1	87	13	38	340
551248	8	7	15	80	5	0	0	1	87	12	38	341
558409	8	7	16	81	3	0	0	1	86	12	38	340
561592	10	8	17	78	4	0	0	1	90	12	35	340
566750	10	8	18	78	4	0	0	1	90	12	37	340
571972	8	7	15	80	5	0	0	1	87	12	38	340
577131	9	8	18	77	5	0	0	1	89	13	38	341
582291	9	7	16	80	3	0	0	1	88	13	37	340
587451	9	8	18	82	0	0	0	1	89	12	34	340
592611	9	8	17	78	5	0	0	1	87	13	37	340
597832	10	8	18	79	3	0	0	1	87	12	34	340
603054	0	6	8	88	8	0	0	1	86	10	35	340
608271	9	8	17	75	5	3	0	1	89	9	28	340

Time	A16CO	A16CO2	A16COX	A16M1	A16M2	A16M3	A16M4	IDB	MBC6	Q6CH4C	Q6HCLC	TQ1612
AVERAGES	7	6	13	83	4	0	0	1	89	12	36	340
	2	2	3	3	2	0	0	0	2	1	4	

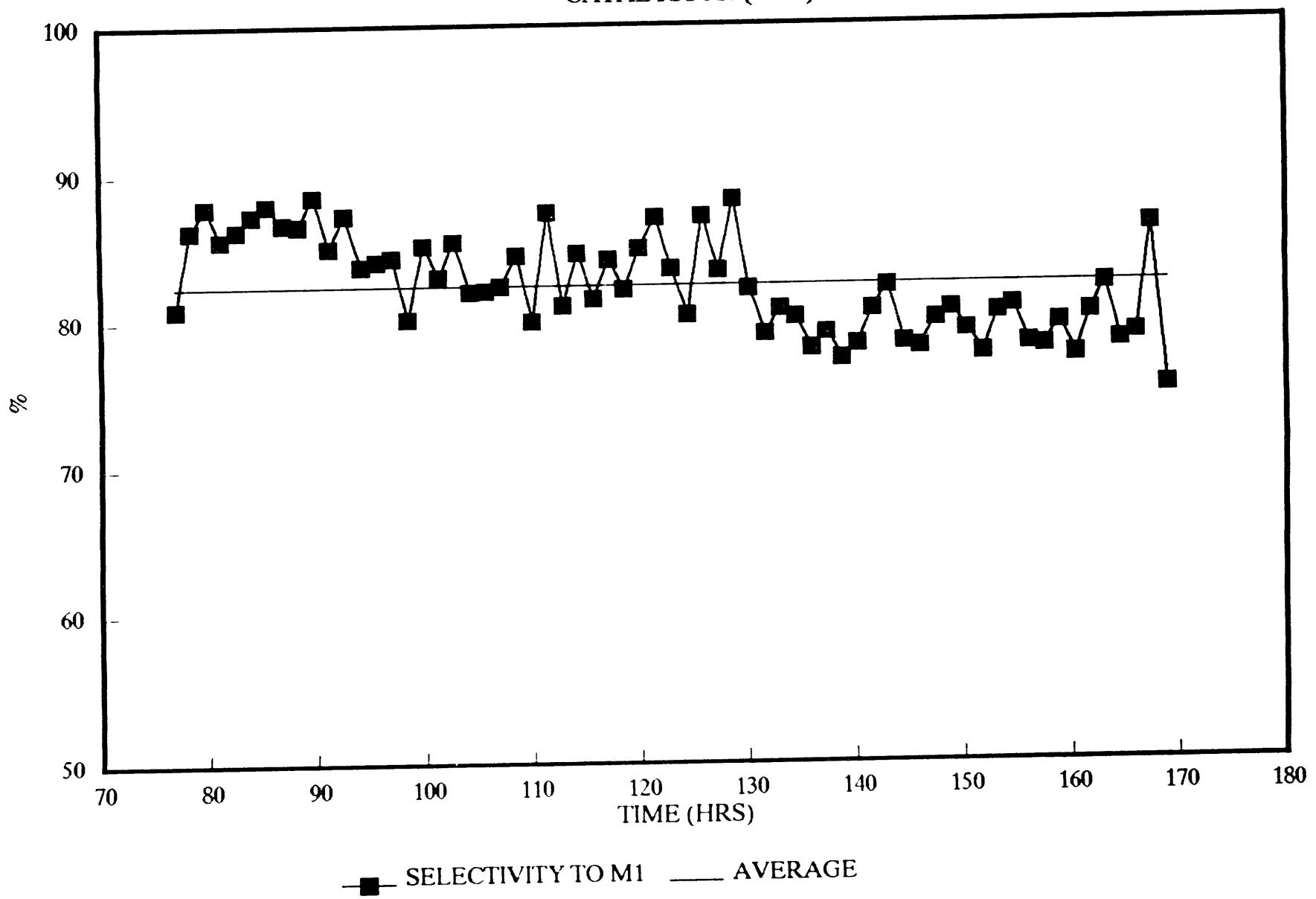
RUN 10346066

CATALYST 516 (CuCl)



RUN 10346066

CATALYST 516 (CuCl)



00016083 HOOD #6 RAMPING EXPERIMENT DEFINITION
 00016083
 00016083
 00016083 OPERATOR NAME: B. CRUM DATE: 22-JAN-93
 00016083 LOG BOOK #: 10346 PAGE #: 134
 00016083 RUN #: 10346060 CATALYST #: 163c
 00016083 CATALYST NAME: PURCHASED CUO CRUSHED
 00016083 COMMENTS: SEE RUNSHEET - REDUCED CAT W H2 2HR 300C THEN 1HR N2 340
 00016083 SEE TEMP DATA WHEN LOOKING AT RESULTS
 00016083

00016083 MASS OF CATALYST (g): 6.36

00016083 REACTOR INSIDE DIAM (CM): 6

00016083 CATALYST BED HEIGHT (CM): 25.4

00015710 TEMPERATURE RAMPING EXPERIMENT FOR HOOD #6

00015710 =====

00015710 INITIAL FINAL ABSOLUTE
 00015710 TEMP TEMP RAMP RATE
 00015710 (DEG C) (DEG C) (DEG C / MIN)

00015710 =====

00015710 BOTTOM: 340 340 2 SPACE VELOCITY 9.0 CM/SEC
 00015710 MIDDLE: 340 340 2 RUN TIME 70 HRS

00015710 TOP: 340 340 2

00015710

(INITIAL TEMPERATURE CAN BE GREATER THAN FINAL TEMPERATURE)

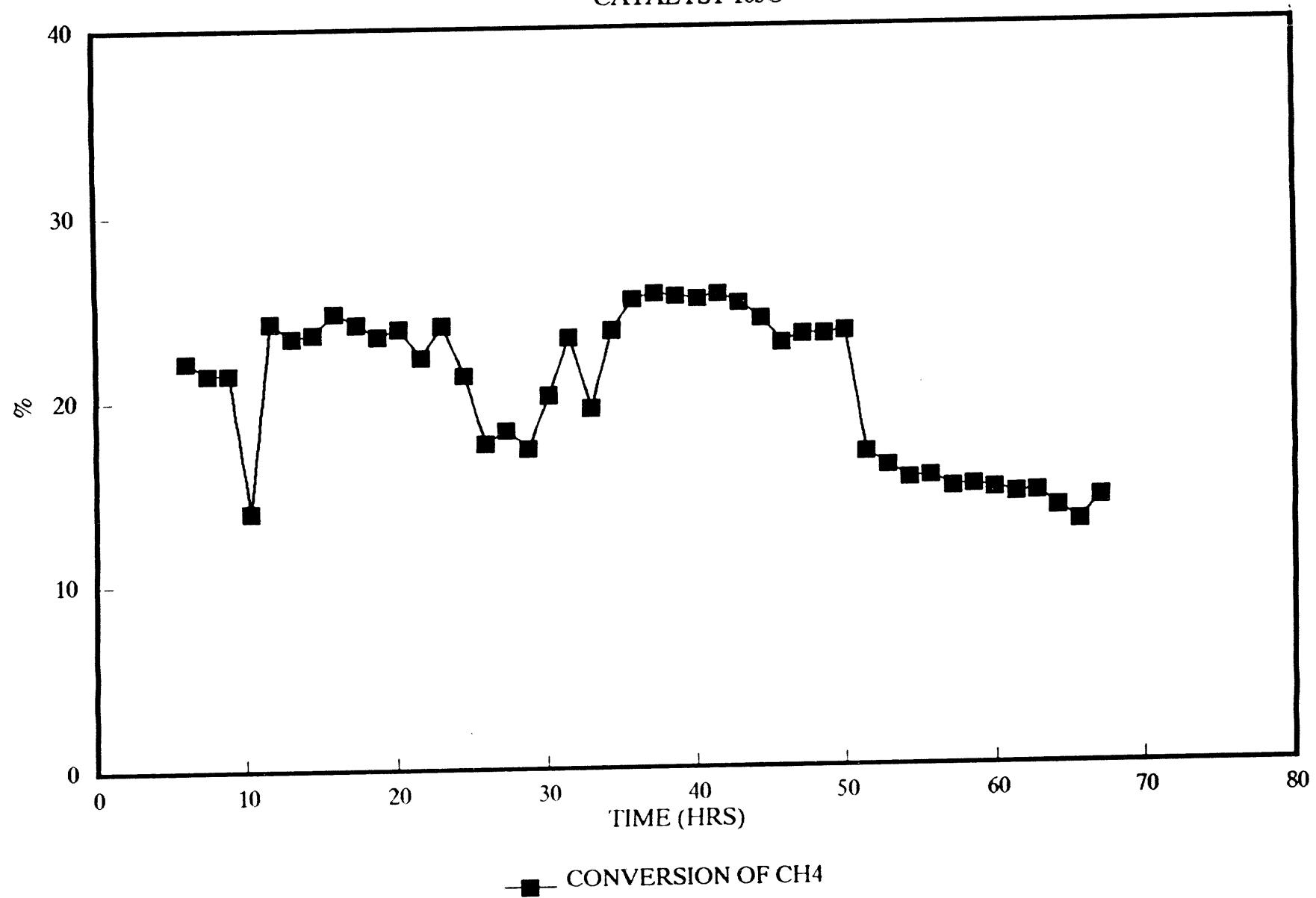
00015710

00015710 CH4 FLOW RATE (CC/MIN): 100 O2 FLOW RATE (CC/MIN): 22.8

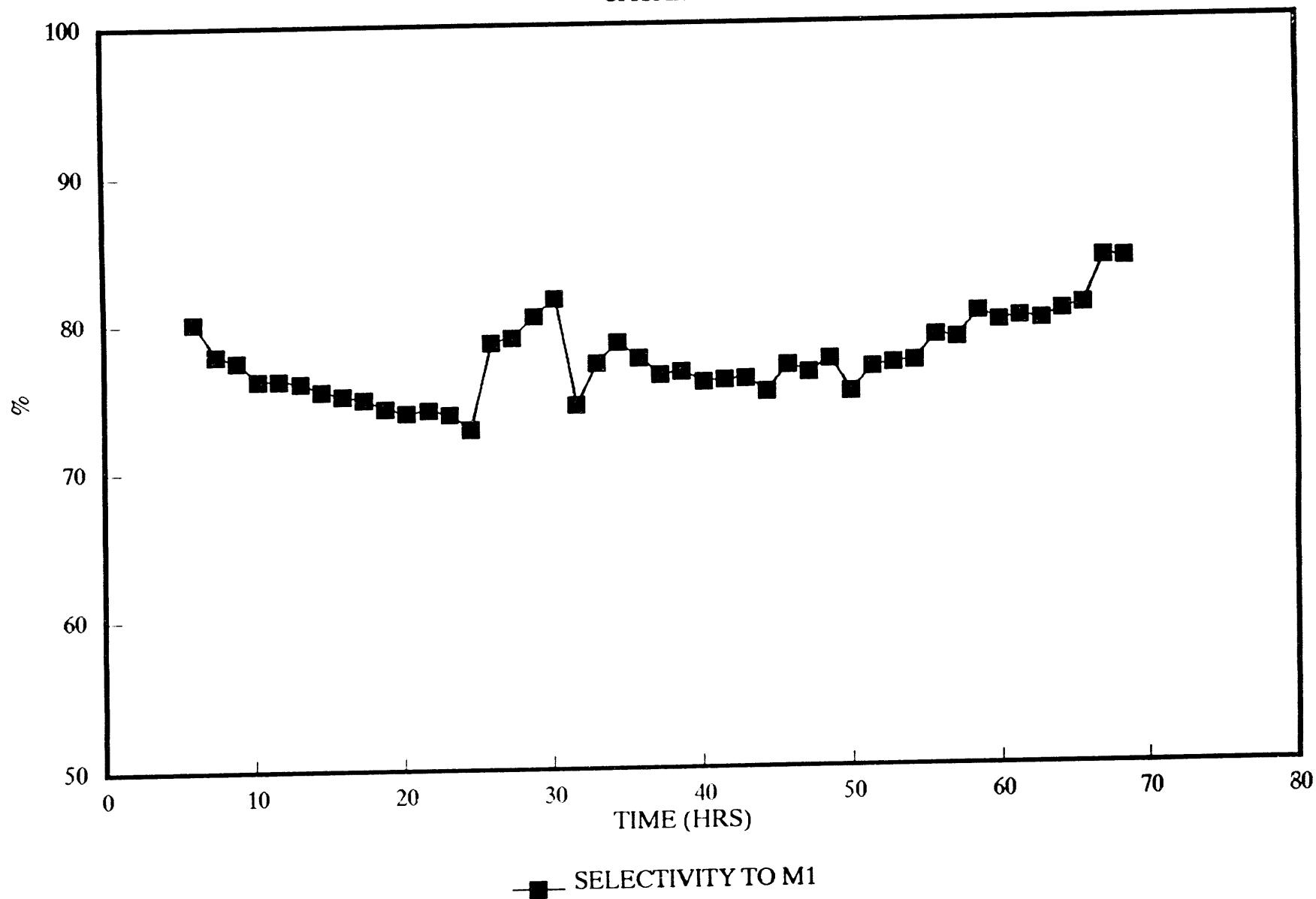
00015710 HCI FLOW RATE (CC/MIN): 29.6 AUX FLOW RATE (CC/MIN): 0

Time	AI6CO	AI6CO2	AI6COX	AI6M1	AI6M2	AI6M3	AI6M4	ID6	MBC6	Q6CH4C	Q6HCLC	TQ1612
26724	0	15	15	80	4	0	0	1	69	22	66	
31868	0	15	15	78	7	0	0	1	67	21	66	
38985	0	15	15	78	7	0	0	1	74	21	67	
42128	0	16	16	76	8	0	0	1	69	14	43	
47229	0	16	16	76	8	0	0	1	67	24	76	
52334	0	16	16	76	8	0	0	1	66	23	72	
57416	0	16	16	75	8	0	0	1	68	24	74	
62533	0	17	17	75	8	0	0	1	68	25	77	
67636	0	17	17	75	8	0	0	1	66	24	74	
72742	0	18	18	74	8	0	0	1	70	23	71	
77877	0	18	18	74	8	0	0	1	68	24	72	
82977	0	18	18	74	8	0	0	1	70	22	68	
88096	0	19	19	74	8	0	0	1	70	24	73	
93194	0	19	19	73	8	0	0	1	70	21	64	
98295	0	17	17	79	5	0	0	1	71	18	52	
103454	0	15	15	79	6	0	0	1	72	18	56	
108548	0	13	13	80	6	0	0	1	73	17	54	
113648	0	12	12	82	6	0	0	1	72	20	63	
118749	0	16	16	74	10	0	0	1	59	23	61	
123832	0	15	15	77	8	0	0	1	83	19	62	
128948	0	14	14	79	7	0	0	1	69	24	75	
134049	0	14	14	77	8	0	0	1	68	25	81	
139131	0	15	15	76	9	0	0	1	65	26	82	
144250	0	15	15	77	9	0	0	1	65	26	81	
149347	0	16	16	78	9	0	0	1	68	25	79	
154449	0	16	16	78	8	0	0	1	66	26	81	
159549	0	16	16	78	8	0	0	1	68	25	79	
164650	0	16	16	75	8	0	0	1	68	24	76	
169747	0	15	15	77	8	0	0	1	68	23	72	
174848	0	15	15	76	8	0	0	1	70	23	72	
179948	0	14	14	77	8	0	0	1	68	23	74	
185048	0	16	16	75	9	0	0	1	70	24	74	
190149	0	19	19	77	4	0	0	1	74	17	48	
195249	0	20	20	77	3	0	0	1	73	16	45	
200332	0	20	20	77	3	0	0	1	73	15	44	
205450	0	18	18	79	3	0	0	1	73	16	44	
210547	0	18	18	79	4	0	0	1	77	15	43	
215649	0	17	17	80	3	0	0	1	72	15	44	
220748	0	17	17	80	3	0	0	1	73	15	43	
225849	0	17	17	80	3	0	0	1	73	15	42	
230947	0	18	18	80	3	0	0	1	73	15	42	
236048	0	17	17	80	2	0	0	1	72	14	40	
241174	0	17	17	81	2	0	0	1	75	13	37	
246309	0	15	15	84	1	0	0	1	71	14	39	
254367	0	14	14	84	2	0	0	1	750	0	0	
Time	AI6CO	AI6CO2	AI6COX	AI6M1	AI6M2	AI6M3	AI6M4	ID6	MBC6	Q6CH4C	Q6HCLC	TQ1612
Avg	0	16	16	77	6	0	0	1	85	20	61	
STD	0	2	2	3	2	0	0	0	100	5	17	

RUN 10346060
CATALYST 163C

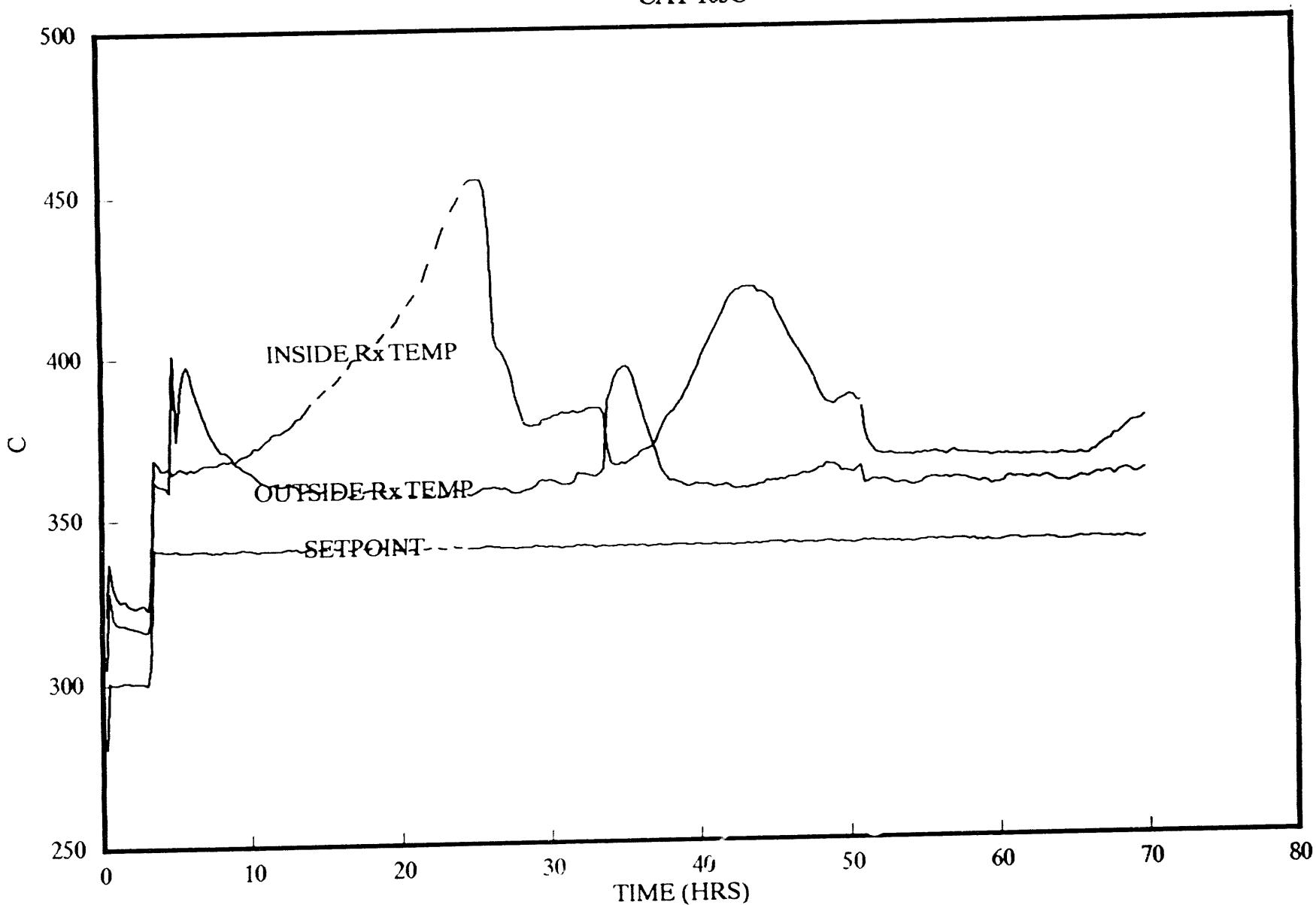


RUN 10346060
CATALYST 163C



RUN 10346060

CAT 163C



00081123 OPERATOR NAME: B CRUM DATE 23-FEB-93
 00081123 LOG BOOK #: 10346 PAGE #: 144
 00081123 RUN #: 10348065 CATALYST #: 158
 00081123 CATALYST NAME: pet catalyst
 00081123 COMMENTS CAT SCREENED BETWEEN 18 & 35 MESH PRETREAT 1 hr with H2 AT 290C.
 00081123 CAMILE SHUT DOWN 3 TIMES DURING THIS RUN SEE BOOK FOR DETAILS
 00081123

00081123 MASS OF CATALYST (g) 42

00081123 REACTOR INSIDE DIAM (CM) 6

00081123 CATALYST BED HEIGHT (CM) 25.4

00080777 TEMPERATURE RAMPING EXPERIMENT FOR HOOD #6

00080777 -----

00080777 INITIAL FINAL ABSOLUTE
 00080777 TEMP TEMP RAMP RATE
 00080777 (DEG C) (DEG C) (DEG C / MIN)

00080777 -----
 00080777 BOTTOM 315 315 1 FLUID VELOCITY 9.0 CM/SEC
 00080777 MIDDLE 315 315 1 RUN TIME 135 HRS
 00080777 TOP 315 315 1

00080777 (INITIAL TEMPERATURE CAN BE GREATER THAN FINAL TEMPERATURE)

00080777

00080777 CH4 FLOW RATE (CC/MIN) 100 O2 FLOW RATE (CC/MIN) 22.8

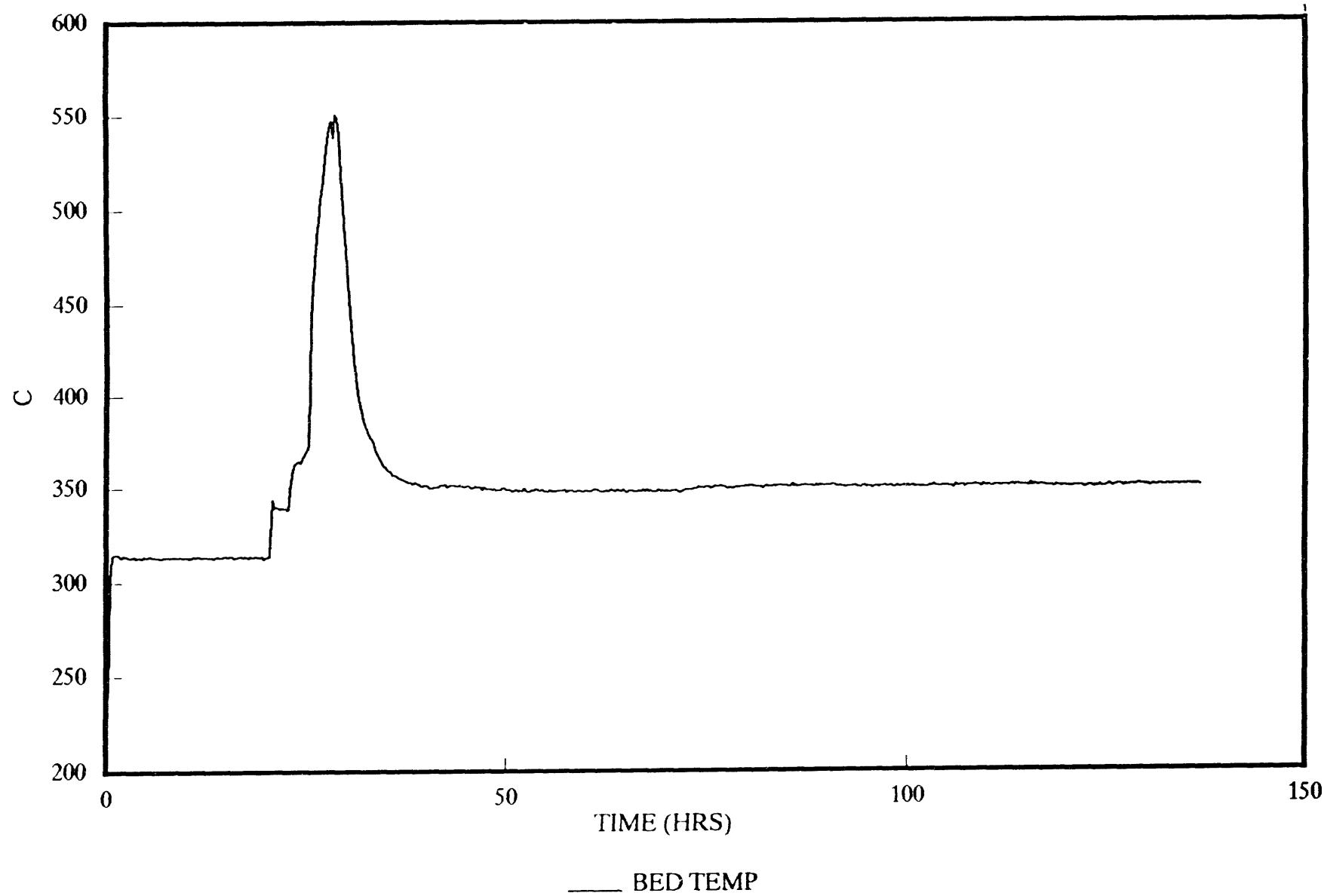
00080777 HCl FLOW RATE (CC/MIN) 29.6 AUX FLOW RATE (CC/MIN) 0

Time A16CO A16CO2 A16COX A16M1 A16M2 A16M3 A16M4 ID6 MBC6 Q6CH4C Q6HCLC TQ1612

91847	11	17	28	64	8	0	0	1	64	29	79	321
92884	9	20	29	59	12	0	0	1	56	28	78	315
102148	9	23	32	57	12	0	0	1	62	29	77	315
107309	10	20	30	60	10	0	0	1	74	28	76	315
112471	13	21	34	57	9	0	0	1	65	28	71	315
117629	14	21	35	56	10	0	0	1	99	26	65	315
122791	16	19	35	56	9	0	0	1	93	26	66	315
127851	14	15	29	85	7	0	0	1	67	28	72	316
133110	16	20	36	57	8	0	0	1	68	27	87	315
138269	16	20	36	57	7	0	0	1	70	26	64	315
143431	14	20	33	59	8	0	0	1	80	26	65	315
148588	13	15	28	67	6	0	0	1	56	28	71	315
153690	16	20	36	56	8	0	0	1	93	27	66	315
158648	18	20	38	53	9	0	0	0	122	25	59	315
167190	14	21	35	55	10	0	0	1	56	28	71	315
172351	15	21	36	55	9	0	0	1	83	28	68	315
177510	14	20	34	57	9	0	0	1	57	28	71	315
182871	14	21	35	55	9	0	0	1	59	28	71	314
187829	14	20	34	57	9	0	0	1	80	29	73	315
192992	13	19	32	59	9	0	0	1	61	28	73	316
198150	12	17	28	64	7	0	0	1	62	29	77	315
203309	13	18	31	61	8	0	0	1	64	29	74	315
208470	13	19	32	59	9	0	0	1	58	28	72	315
213630	9	14	23	71	5	0	0	1	61	28	78	315
218791	13	21	33	58	9	0	0	1	77	26	87	315
223949	13	20	33	57	10	0	0	1	66	27	70	316
229108	9	24	33	58	11	0	0	1	115	22	58	316
234270	14	22	36	53	10	0	0	1	82	28	66	315
239431	15	20	35	55	9	0	0	1	83	27	69	315
244590	12	21	33	57	10	0	0	1	100	25	66	315
249748	13	20	33	58	10	0	0	1	95	25	65	315
254911	12	19	31	60	9	0	0	1	69	28	72	315
260069	15	23	38	52	11	0	0	1	85	27	66	315
265220	13	20	34	57	9	0	0	1	123	30	78	316
270389	10	19	29	82	4	0	0	1	78	26	70	315
275549	8	18	26	63	10	0	0	1	105	21	61	315
280708	1	9	9	86	5	0	0	1	102	9	28	315
285870	2	7	9	33	8	0	0	1	92	12	41	315
291029	1	3	4	92	4	0	0	1	108	11	37	315
298188	1	2	3	96	1	0	0	1	74	13	43	315
301351	1	3	4	94	1	0	0	1	123	11	36	315
308510	2	6	8	85	7	0	0	1	83	13	44	315
311668	1	5	6	88	6	0	0	1	81	13	43	315
316824	0	3	3	95	2	0	0	1	123	10	34	315
321988	5	8	13	77	10	0	0	1	147	15	48	315
327150	3	8	11	78	11	0	0	1	102	13	44	315
332311	2	8	11	78	11	0	0	1	85	13	46	315
337469	2	9	11	78	11	0	0	1	88	13	43	315
342629	1	3	4	92	4	0	0	1	108	12	30	315
347790	2	6	8	86	7	0	0	1	110	11	36	315
352048	1	5	6	88	5	0	0	1	93	12	40	316
358110	1	4	5	91	4	0	0	1	98	11	38	315
363269	1	3	3	94	3	0	0	1	87	12	39	315
368429	1	3	4	95	2	0	0	1	122	12	39	315
373588	1	3	4	95	2	0	0	1	95	13	44	315
378748	1	3	4	93	3	0	0	1	108	12	42	315
383909	1	4	5	90	5	0	0	1	93	13	43	315
389071	1	4	5	91	4	0	0	1	76	13	44	315
394236	1	4	5	91	4	0	0	1	83	13	43	316
398998	1	6	7	85	7	0	0	1	88	13	44	315
404658	1	5	7	87	7	0	0	1	86	11	46	316
409718	1	4	5	90	5	0	0	1	84	13	45	315
414879	1	6	7	87	6	0	0	1	90	14	47	315
420031	1	5	8	89	5	0	0	1	88	13	45	315
425189	1	4	5	91	4	0	0	1	98	13	42	315
430356	1	4	5	91	4	0	0	1	84	13	43	316
435515	1	5	6	88	6	0	0	1	88	12	42	315
440678	1	3	4	94	2	0	0	1	85	13	43	315
445830	1	4	6	90	5	0	0	1	98	11	38	315
450997	1	4	5	91	4	0	0	1	90	12	39	315
456149	1	4	5	91	4	0	0	1	92	13	44	315
461311	2	7	9	82	9	0	0	1	102	14	46	315
466469	2	6	8	85	7	0	0	1	102	12	41	315
471630	2	6	7	85	7	0	0	1	107	13	44	316
476788	1	4	5	89	6	0	0	1	103	13	44	315
487111	1	5	7	87	6	0	0	1	99	12	42	315
492277	1	6	7	86	7	0	0	1	90	13	45	315
AVG	8	A16CO	A16CO2	A16COX	A16M1	A16M2	A16M3	A16M4	MBC6	Q6CH4C	Q6HCLC	TQ1612
AVG	7		12	19	74	7	0	0	88	19	55	315
STD	6		6	13	16	3	0	0	10	7	15	

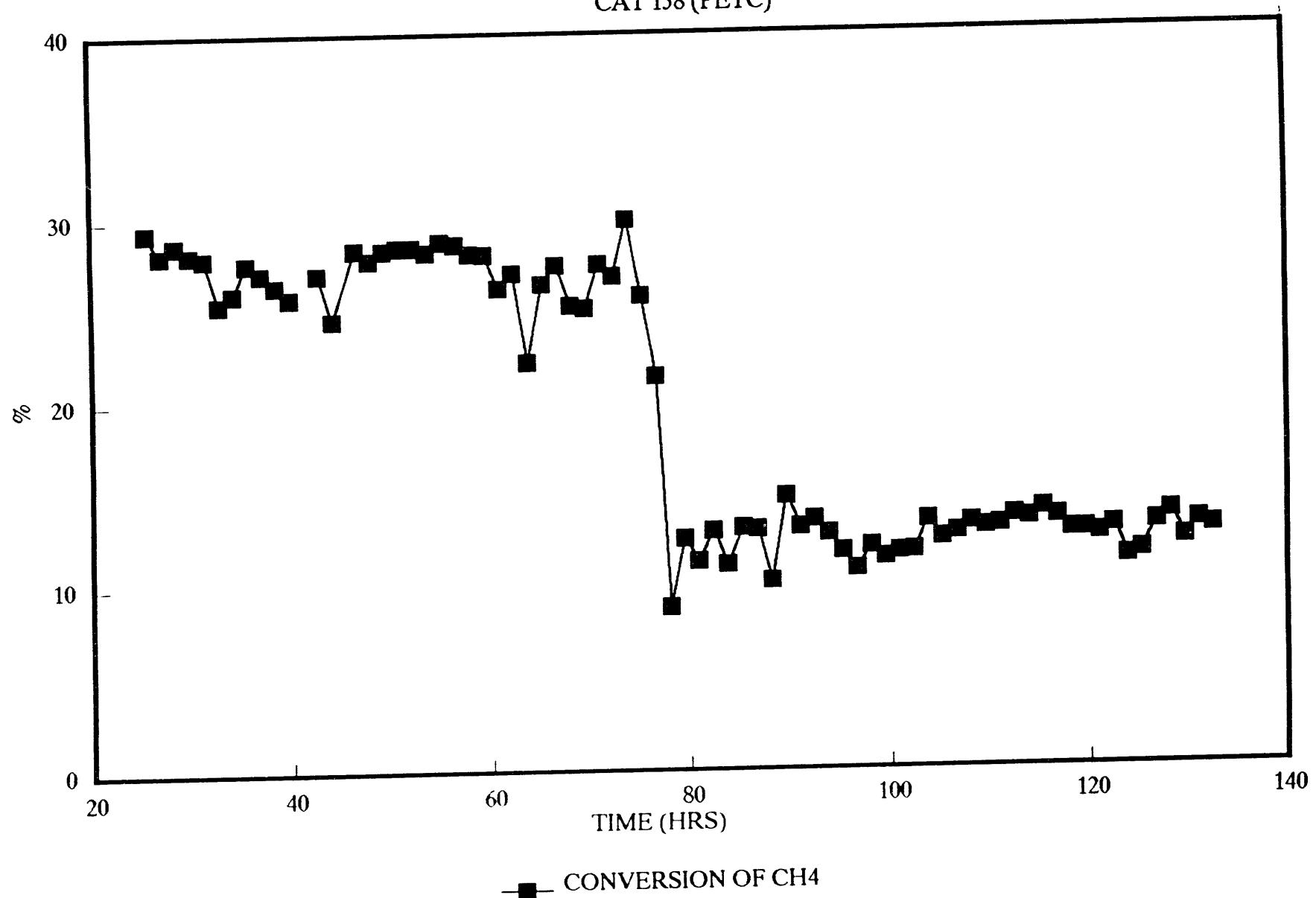
RUN 10346065

CAT 158

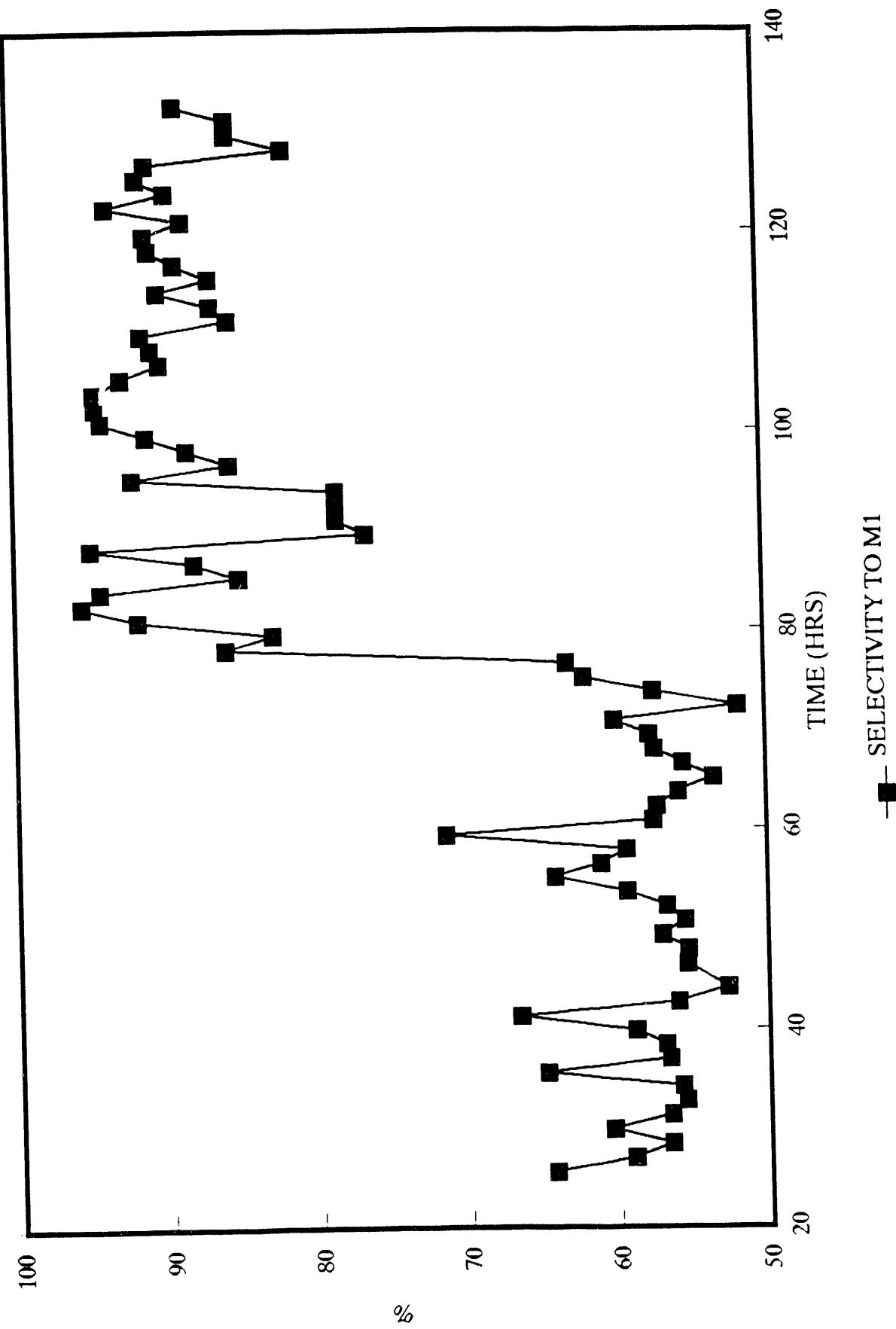


RUN 10346065

CAT 158 (PETC)



RUN 10346065
CAT 158 (PETC)



00003294 OPERATOR NAME: B. CRUM DATE: 19-MAR-93
 00003294 LOG BOOK #: 10346 PAGE #: 150
 00003294 RUN #: 10346067 CATALYST #: 163c
 00003294 CATALYST NAME: PURCHASED Cu CATALYST
 00003294 COMMENTS: START AT LOW TEMP 10 DEG C INCREMENTS
 00003294 Rx PLUGGED AT END OF RUN
 00003294

00003294 MASS OF CATALYST (g): 6.45

00003294 REACTOR INSIDE DIAM (CM): .6

00003294 CATALYST BED HEIGHT (CM): 25.4

00003308 TEMPERATURE RAMPING EXPERIMENT FOR HOOD #6

00003308 =====

INITIAL TEMP (DEG C)	FINAL TEMP (DEG C)	ABSOLUTE RAMP RATE (DEG C / MIN)
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00003308 =====

BOTTOM: 250	260	2	FLUID VELOCITY 9.0 CM/SEC
MIDDLE: 250	260	2	RUN TIME 160 HRS
TOP : 250	260	2	

00003308 (INITIAL TEMPERATURE CAN BE GREATER THAN FINAL TEMPERATURE)

00003308 CH4 FLOW RATE (CC/MIN): 100 O2 FLOW RATE (CC/MIN): 22.8

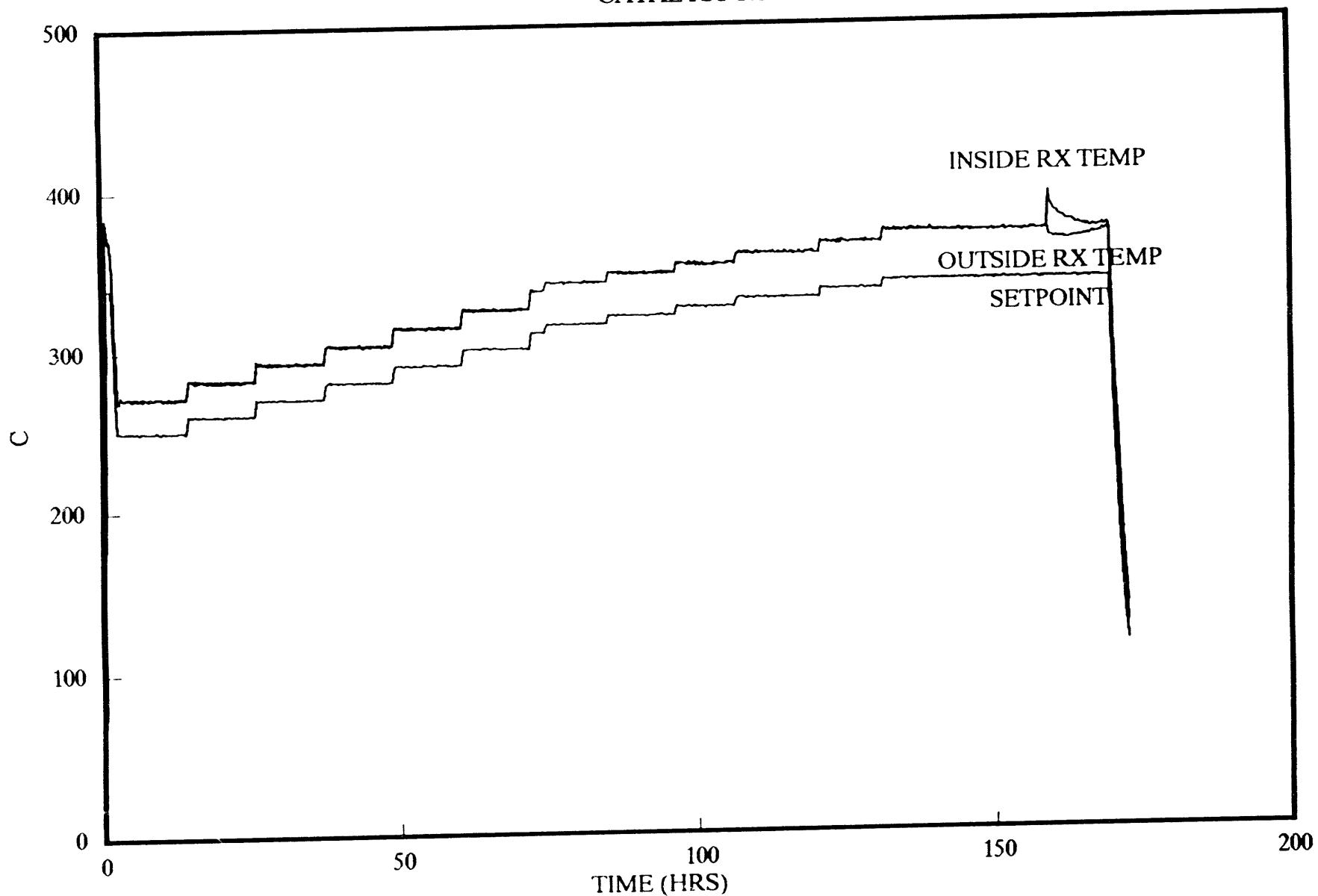
00003308 HCl FLOW RATE (CC/MIN): 29.6 AUX FLOW RATE (CC/MIN): 0

Time	AI6CO	AI6CO2	AI6COX	AI6M1	AI6M2	AI6M3	AI6M4	ID6	MBC6	Q6 CH4C	Q6 H CLC	TQI612
15266	0	0	0	0	0	0	0	1	200	0	0	250
20428	0	0	0	0	0	0	0	1	200	0	0	250
25570	0	0	0	0	0	0	0	1	200	0	0	250
30664	0	0	0	0	0	0	0	1	200	0	0	250
35840	0	0	0	0	0	0	0	1	102	0	0	250
40942	0	0	0	0	0	0	0	1	200	0	0	250
46021	0	0	0	0	0	0	0	1	200	0	0	250
51167	0	0	0	0	0	0	0	2	102	0	0	253
57043	0	0	0	0	0	0	0	2	102	0	0	260
62101	0	0	0	0	0	0	0	2	200	0	0	260
67232	0	0	0	0	0	0	0	2	102	0	0	260
72388	0	0	0	0	0	0	0	2	102	0	0	260
77507	0	0	0	0	0	0	0	2	102	0	0	260
82607	0	0	0	0	0	0	0	2	102	0	0	260
87693	0	0	0	0	0	0	0	2	102	0	0	259
92805	0	0	0	0	0	0	0	3	102	0	0	263
98652	0	0	0	0	0	0	0	3	102	0	0	270
103788	0	0	0	0	0	0	0	3	102	0	0	270
108889	0	0	0	0	0	0	0	3	102	0	0	271
114012	0	0	0	0	0	0	0	3	102	0	0	270
119102	0	0	0	0	0	0	0	3	200	0	0	270
124159	0	0	0	0	0	0	0	3	200	0	0	270
129271	0	0	0	0	0	0	0	3	199	0	0	270
134379	0	0	0	0	0	0	0	4	199	0	0	273
140224	0	0	0	0	0	0	0	4	200	0	0	280
145293	0	0	0	0	0	0	0	4	200	0	0	280
150401	0	0	0	0	0	0	0	4	200	0	0	280
155508	0	0	0	0	0	0	0	4	102	0	0	280
160598	0	0	0	0	0	0	0	4	198	0	0	281
165641	0	0	0	0	0	0	0	4	199	0	0	280
170740	0	0	0	0	0	0	0	4	196	0	0	280
175786	0	0	0	0	0	0	0	5	188	0	0	283
181599	0	0	0	0	0	0	0	5	198	0	0	290
186706	0	0	0	0	0	0	0	5	165	0	0	290
191807	0	0	0	100	0	0	0	5	102	0	0	290
196905	0	0	0	100	0	0	0	5	102	0	0	290
202000	0	0	0	0	0	0	0	5	197	0	0	290
207099	0	0	0	0	0	0	0	5	199	0	0	290
212142	0	0	0	0	0	0	0	5	199	0	0	290
217239	0	0	0	0	0	0	0	6	198	0	0	293
223065	0	0	0	100	0	0	0	6	102	0	0	300
228168	0	0	0	100	0	0	0	6	102	0	0	301
233266	0	0	0	100	0	0	0	6	102	0	0	300
238367	0	0	0	100	0	0	0	6	102	0	0	300
243466	0	0	0	0	0	0	0	6	197	0	0	300
248560	0	0	0	0	0	0	0	6	199	0	0	300
253685	0	0	0	0	0	0	0	6	102	0	0	300
258772	0	0	0	100	0	0	0	7	199	0	0	303
264585	0	0	0	100	0	0	0	7	101	0	0	310
269706	0	0	0	100	0	0	0	1	100	0	0	315
274848	0	0	0	100	0	0	0	1	102	0	0	315
279938	0	0	0	100	0	0	0	1	101	0	0	315
285045	0	0	0	100	0	0	0	1	108	0	0	315
290153	0	0	0	100	0	0	0	1	198	0	0	315
295273	0	0	0	100	0	0	0	1	101	0	0	315
300424	0	0	0	100	0	0	0	1	96	0	0	315

Time	AI6CO	AI6CO2	AI6COX	AI6M1	AI6M2	AI6M3	AI6M4	ID6	MBC6	Q6CH4C	Q6HCLC	TQI612
305593	0	0	0	100	0	0	0	2	83	0	3	318
310999	0	0	0	100	0	0	0	2	101	0	2	320
316125	0	0	0	100	0	0	0	2	101	0	0	320
321228	0	0	0	100	0	0	0	2	102	0	0	320
326326	0	0	0	100	0	0	0	2	102	0	0	320
331444	2	0	2	98	0	0	0	2	84	2	5	320
336585	7	0	7	93	0	0	0	2	93	3	10	320
341720	0	0	0	100	0	0	0	2	100	2	6	320
346865	0	0	0	100	0	0	0	3	101	2	7	322
352203	6	0	6	89	5	0	0	3	96	3	8	325
357363	1	0	1	99	0	0	0	3	72	3	11	325
362523	2	0	2	98	0	0	0	3	88	2	7	325
367682	8	0	8	92	0	0	0	3	100	3	9	325
372842	7	0	7	93	0	0	0	3	101	3	9	325
378004	7	0	7	93	0	0	0	3	100	3	10	325
383162	4	0	4	96	0	0	0	4	98	2	7	325
388743	6	3	9	85	6	0	0	4	99	6	19	330
393903	6	2	9	86	6	0	0	4	101	5	16	330
399065	6	2	9	85	6	0	0	4	100	6	20	330
404161	0	2	2	94	4	0	0	4	192	0	0	330
409323	6	3	9	85	6	0	0	4	99	6	20	330
414483	5	2	7	88	5	0	0	4	99	7	22	330
419625	0	3	3	90	7	0	0	4	157	2	6	330
440649	5	2	6	89	5	0	0	1	84	10	34	335
445812	4	1	5	91	4	0	0	1	89	9	30	336
450964	4	1	5	91	4	0	0	1	83	11	35	335
456123	4	2	5	90	4	0	0	1	88	9	30	335
461282	3	2	5	90	5	0	0	1	87	8	25	336
466444	2	1	3	94	3	0	0	1	79	8	26	335
471602	7	3	10	82	8	0	0	2	94	8	27	336
477184	7	4	11	78	11	0	0	2	117	12	41	340
482343	5	4	10	78	12	0	0	2	83	14	48	340
487509	6	4	10	79	11	0	0	2	87	13	45	340
492671	6	4	10	78	12	0	0	2	85	13	46	340
497834	6	4	10	78	12	0	0	2	85	15	53	340
502991	1	1	3	94	3	0	0	2	70	16	54	340
508151	6	4	10	79	11	0	0	1	94	14	48	340
513312	6	4	10	78	12	0	0	1	83	14	50	340
518470	3	2	5	89	6	0	0	1	76	14	49	340
523631	6	4	10	79	11	0	0	1	84	11	37	339
528784	4	3	6	87	7	0	0	1	78	14	48	340
533951	6	3	10	79	11	0	0	1	86	12	42	340
539112	6	4	10	79	11	0	0	1	86	12	41	340
544272	6	4	10	79	11	0	0	1	86	13	45	340
549423	6	4	10	80	10	0	0	1	84	11	39	340
554590	1	1	2	98	0	0	0	1	62	13	43	341
559742	7	4	11	77	12	0	0	1	82	15	50	341
564904	6	4	10	78	11	0	0	1	83	14	46	340
570040	1	1	2	98	0	0	0	1	67	14	45	340
575170	32	4	36	53	11	0	0	1	137	17	43	340
580332	17	28	46	45	9	0	0	1	52	27	59	340
585490	16	28	45	44	11	0	0	1	68	27	61	341
590651	13	21	34	57	9	0	0	1	41	29	73	340
595813	17	26	43	47	11	0	0	1	58	28	65	340
600970	18	25	43	46	11	0	0	1	50	26	59	340
606129	12	15	27	65	8	0	0	1	81	27	73	340
611292	10	14	23	69	8	0	0	1	25	0	0	250
AVG & STD AI6CO		AI6CO2	AI6COX	AI6M1	AI6M2	AI6M3	AI6M4	ID6	MBC6	Q6CH4C	Q6HCLC	TQI612
AVG 250	0	0	0	0	0	0	0	0	1	186	0	0
AVG 260	0	0	0	0	0	0	0	0	0	34	0	0
AVG 270	0	0	0	0	0	0	0	0	2	114	0	0
AVG 280	0	0	0	0	0	0	0	0	0	32	0	0
AVG 290	0	0	0	0	0	0	0	0	3	151	0	0
AVG 300	0	0	0	100	0	0	0	0	0	49	0	0
AVG 315	0	0	0	100	0	0	0	0	0	195	0	0
AVG 320	1	0	1	99	0	0	0	0	1	111	0	1
AVG 325	2	0	2	4	2	0	0	0	2	98	1	4
AVG 330	5	0	6	93	1	0	0	0	3	94	3	2
AVG 335	3	1	3	4	2	0	0	0	0	9	1	4
AVG 340	5	2	7	88	5	0	0	0	4	115	5	18
AVG 340	2	0	3	3	1	0	0	0	0	34	2	8
AVG 340	4	2	6	89	5	0	0	0	1	87	9	30
AVG 340	1	1	2	4	2	0	0	0	0	5	1	4
AVG 340	9	8	17	74	9	0	0	0	1	79	17	48
AVG 340	7	9	14	15	3	0	0	0	0	19	6	13

RUN 10346067

CATALYST 163C



00010468 HOOD #6 RAMPING EXPERIMENT DEFINITION
 00010468
 00010468

00010468 OPERATOR NAME B CRUM DATE 27-JAN-83
 00010468 LOG BOOK # 10346 PAGE # 136
 00010468 RUN # 10346061 CATALYST # 535

00010468 CATALYST NAME
 00010468 COMMENTS TC IN BED

00010468

00010468 MASS OF CATALYST (g) 3.75

00010468 REACTOR INSIDE DIAM (CM) 6

00010468 CATALYST BED HEIGHT (CM) 25.4

00010262 TEMPERATURE RAMPING EXPERIMENT FOR HOOD #6

00010262 -----
 00010262 INITIAL FINAL ABSOLUTE
 00010262 TEMP TEMP RAMP RATE
 00010262 (DEG C) (DEG C) (DEG C/ MIN)

00010262 -----
 00010262 BOTTOM 340 340 2
 00010262 MIDDLE 340 340 2
 00010262 TOP 340 340 2

SPACE VELOCITY 9.0 CM/SEC
 RUN TIME 140 HRS

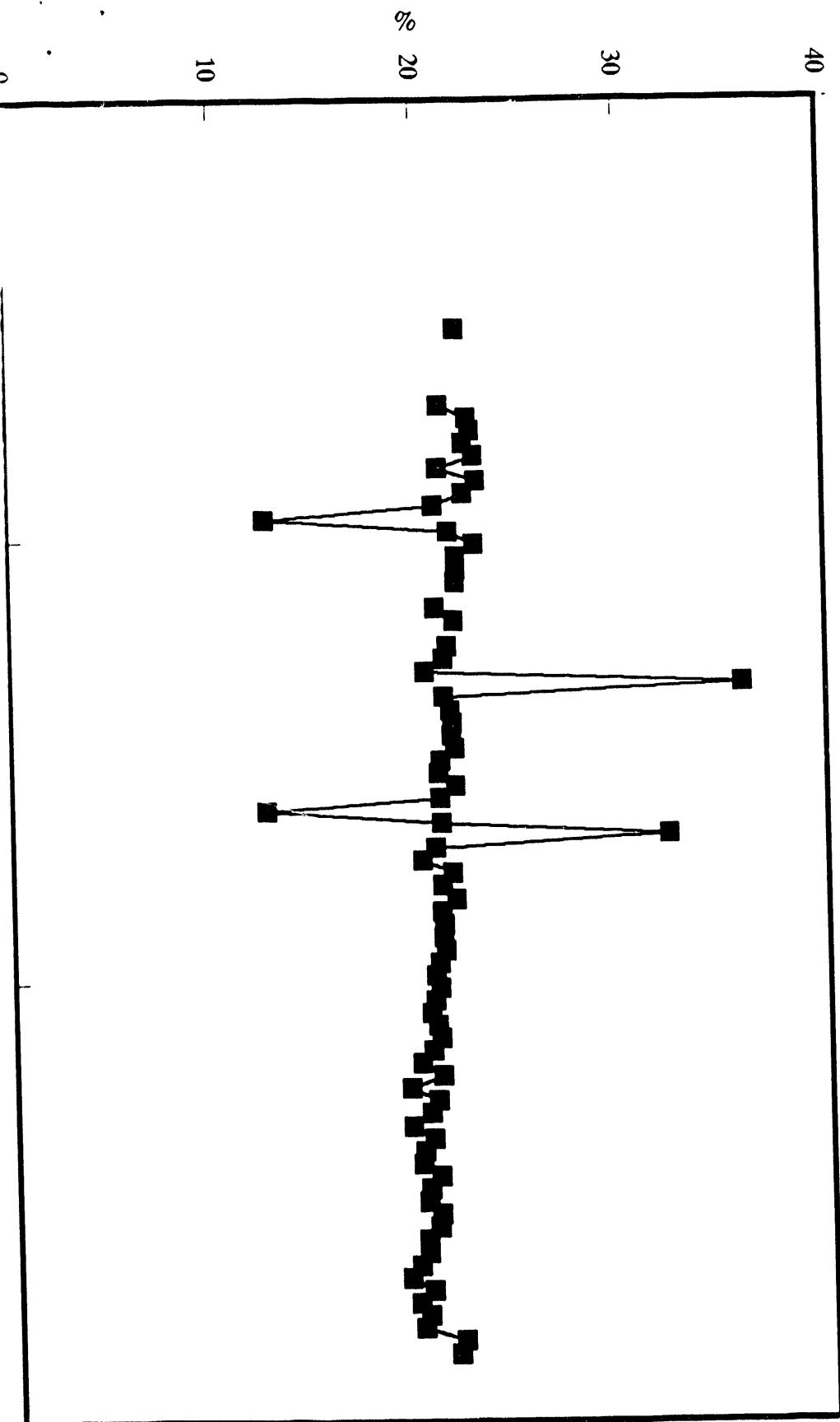
00010262 (INITIAL TEMPERATURE CAN BE GREATER THAN FINAL TEMPERATURE)

00010262 CH4 FLOW RATE (CC/MIN) 100 O2 FLOW RATE (CC/MIN) 22.8
 00010262 HCl FLOW RATE (CC/MIN) 29.6 ALK FLOW RATE (CC/MIN) 0

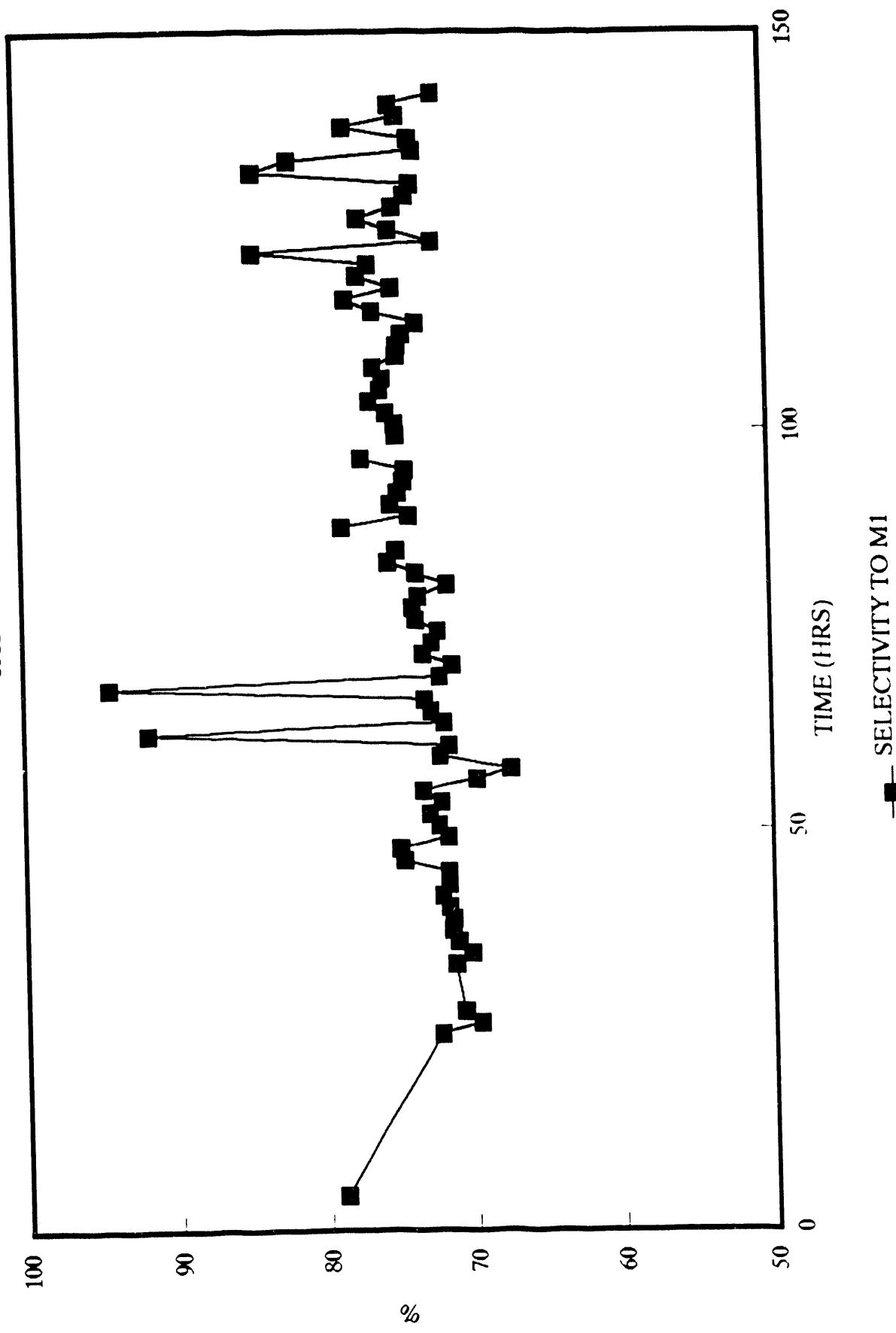
Time	A16CO	A16CO2	A16COX	A16M1	A16M2	A16M3	A16M4	ID6	MBC6	Q6CH4C	Q6HCLC	TQ1612
15405	0	3	3	79	18	0	0	1		0	0	340
88003	0	6	6	72	19	3	0	1	62	22	90	340
93276	0	7	7	70	21	3	0	1		0	0	340
98380	0	6	6	71	20	3	0	1		0	0	340
119482	0	6	6	71	20	3	0	1		0	0	340
124706	0	6	6	70	21	3	0	1	94	21	87	340
129878	1	6	6	71	20	3	0	1	68	23	91	340
135057	1	6	7	71	19	3	0	1	73	23	91	340
140234	1	6	6	71	20	3	0	1	68	22	91	340
145361	1	5	6	72	19	3	0	1	72	23	92	340
150477	0	5	5	72	20	3	0	1	94	21	88	340
155646	1	5	6	72	19	3	0	1	74	23	92	340
160836	1	5	6	72	19	3	0	1	71	22	91	340
165976	0	5	5	75	18	2	0	1	21	394	340	
171168	0	5	5	75	18	2	0	1	12	398	340	
176366	1	6	7	72	19	3	0	1	70	22	87	340
181555	1	5	6	72	19	3	0	1	72	23	90	340
186741	1	5	6	73	19	2	0	1	72	22	87	340
191900	1	5	6	72	19	3	0	1	70	22	87	341
197077	1	5	6	73	18	2	0	1	71	22	86	340
202246	0	7	8	70	17	6	0	1		334	341	
207364	0	7	7	67	19	7	0	1	75	21	87	339
212556	1	5	6	72	19	3	0	1	67	22	87	340
217692	2	5	7	71	19	3	0	1	74		304	340
222854	1	2	3	92	6	0	0	1	98	21	99	340
228023	1	5	6	72	19	3	0	1	68	21	84	340
233174	1	5	6	73	19	2	0	1	82	20	80	340
238518	0	5	5	73	19	3	0	1	36	209	340	
243486	1	2	2	94	3	0	0	1	102	21	83	340
248653	1	5	6	72	19	3	0	1	93	21	120	340
253808	1	5	6	71	20	3	0	1	93	22	122	340
258865	1	5	6	73	18	2	0	1	96	22	119	340
264134	1	5	6	73	19	2	0	1	93	22	120	340
269265	1	5	6	72	19	3	0	1	90	21	118	340
274445	1	5	6	74	20	0	0	1	94	21	107	340
279606	2	5	6	74	20	0	0	1	90	22	104	340
284767	1	5	6	73	20	0	0	1	101	21	108	340
289919	0	5	5	71	21	3	0	1	143	12	72	340
295093	2	5	6	74	20	0	0	1	90	21	102	340
300257	0	5	5	75	20	0	0	1		32	175	339
305406	2	5	6	75	19	0	0	1	92	21	105	340
310566								1	109	20	96	340
315777	1	4	5	79	17	0	0	1	94	21	114	340
320953	2	5	6	74	20	0	0	1	93	21	101	340
326106	2	4	5	75	19	0	0	1	92	22	111	340
331260	2	4	6	75	20	0	0	1	95	21	110	340
336418	2	4	6	74	19	0	0	1	91	21	102	340
341584	2	4	6	74	20	0	0	1	92	21	101	340
346746	2	4	6	77	17	0	0	1	94	21	107	340
351907								1	95	21	105	340
357066	2	4	6	75	19	0	0	1	99	21	106	340
362226	2	4	6	75	19	0	0	1	95	21	106	340
367367	2	4	6	75	19	0	0	1	94	21	105	340
372547	2	4	6	77	18	0	0	1	103	20	104	340
377706	2	4	6	78	18	0	0	1	94	21	105	340
382866	2	4	6	78	18	0	0	1	100	21	105	340
388026	2	4	6	78	18	0	0	1	94	20	103	340
393186	2	4	6	75	19	0	0	1	102	20	95	340
398345	2	4	6	75	19	0	0	1	91	21	99	340
403506	2	4	6	74	20	0	0	1	103	19	100	340
408674	2	4	7	73	20	0	0	1	98	21	104	340
413826	2	4	6	78	18	0	0	1	102	20	103	340
418866	2	4	6	78	18	0	0	1	105	19	97	340
424147	2	4	6	75	19	0	0	1	97	20	103	340
429301	0	4	4	77	19	0	0	1	105	20	111	340
434466	2	4	5	78	18	2	0	1	90	20	76	340
438625	2	3	4	84	11	0	0	1	90	21	74	340
444765	2	4	6	72	19	2	0	1	70	20	80	340
449846	2	4	6	75	17	2	0	1	79	20	78	340
455106	2	0	2	77	18	2	0	1	74	21	64	340
460265	2	3	6	75	17	2	0	1	76	21	61	340
465426	2	4	6	74	18	2	0	1	63	20	79	340
470584	2	4	6	73	18	2	0	1	75	20	79	340
475745	2	3	4	84	11	0	0	1	91	20	71	340
480607	2	3	5	82	13	0	0	1	105	19	70	340
486067	2	4	6	73	18	2	0	1	72	20	79	340
491227	2	4	6	74	18	2	0	1	87	20	77	340
496386	2	3	5	78	15	2	0	1	81	20	76	340
501547	3	3	6	74	18	2	0	1	88	20	77	340
506705	2	4	6	75	17	2	0	1	68	22	64	340
511866	3	4	6	72	19	2	0	1	75	21	66	341

Time	A16CO	A16CO2	A16COX	A16M1	A16M2	A16M3	A16M4	ID6	MBC6	Q6CH4C	Q6HCLC	TQ1612
AVG	1	4	6	75	18	1	0	1	88	21	105	340
STD	1	1	1	4	3	1	0	0	14	3	65	

RUN 10346061
CAT 535

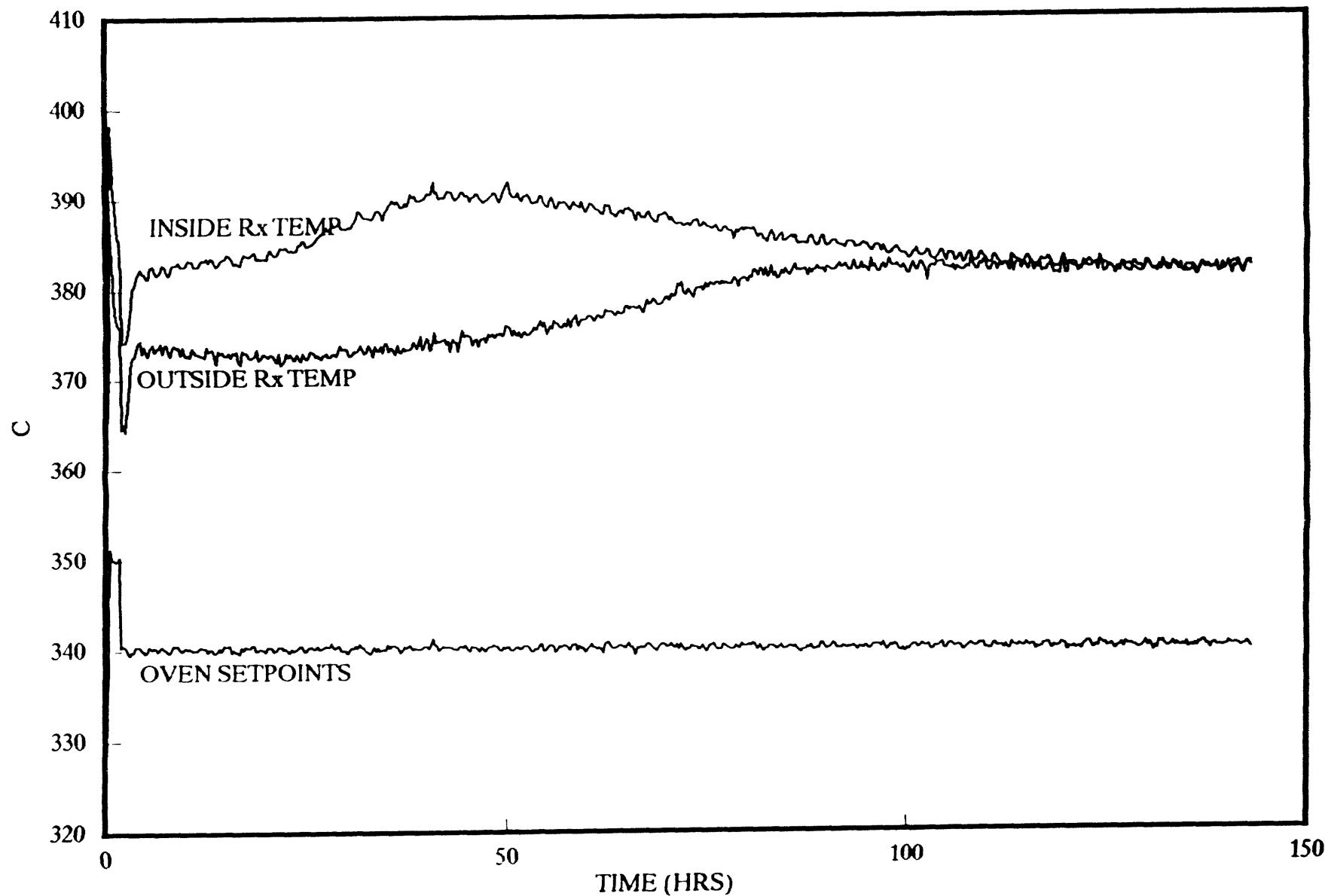


RUN 10346061
CAT 535



RUN 10346061

CATALYST 535



OPERATOR NAME BRUCE CRUM
 LOGBOOK # 10348 PAGE 140
 RUN # 10348003 CATALYST # 536
 CATALYST NAME

COMMENTS: 2 WEEK RUN. TEMPERATURE RAISED NEAR END
 TEMPERATURE PROFILE AND HEADER DATA LOST DUE TO
 GAMBLE CLUTCH. GAMBLE SHUT DOWN ON CALC ERROR AT BEGINNING OF RUN -- RESTARTED NEXT DAY

MASS OF CATALYST 3.60
 REACTOR INSIDE DIAM (IN) 8
 CATALYST BED HT (CM) 26.4
 TEMPERATURE PROBE INSIDE BED

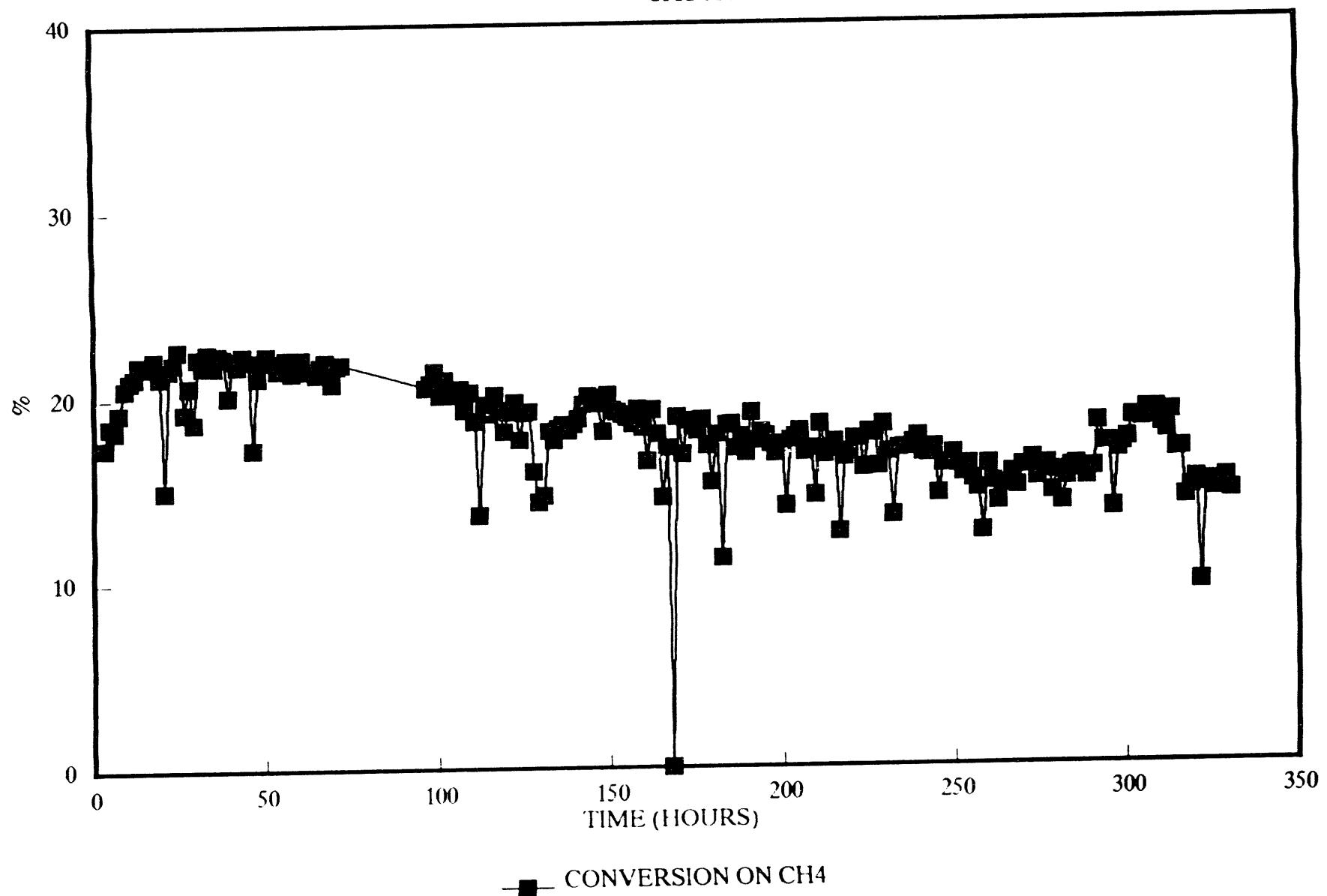
CH4 FLOW 100
 O2 FLOW 22.8
 HCl FLOW 29.6

Time	A1CO	A1CO2	A1COX	A1M1	A1M2	A1M3	A1M4	ID6	MBC6	Q8CHAC	Q8HCLC	TQ1612
11230	3	0	3	83	14	0	0	1	88	17	65	340
16410	3	3	5	78	15	2	0	1	87	19	71	340
21560	2	3	6	76	16	2	0	1	94	18	71	340
26721	2	4	6	75	17	2	0	1	94	19	75	340
31870	1	5	6	73	18	3	0	1	89	21	61	340
37038	1	6	7	73	18	2	0	1	83	21	61	340
42193	0	7	7	72	18	3	0	1	89	21	83	340
47364	0	7	7	71	19	3	0	1	82	22	67	340
52514	0	7	7	71	19	3	0	1	80	22	85	340
57673	0	7	7	72	18	3	0	1	83	22	86	340
62833	0	7	7	71	19	3	0	1	84	22	87	340
67991	0	7	7	71	19	2	0	1	86	21	84	340
73153	0	7	7	71	19	3	0	1	130	19	60	340
78313	0	7	7	72	19	3	0	1	83	22	85	340
83473	0	7	7	71	20	2	0	1	79	22	87	340
88633	0	7	7	70	20	3	0	1	72	23	91	340
93783	0	5	5	78	15	2	0	1	116	19	74	340
98863	0	6	6	71	19	3	0	1	85	21	83	340
104112	0	5	5	72	20	3	0	1	116	19	76	340
109282	1	6	7	71	20	3	0	1	73	22	89	340
114440	1	6	7	72	19	3	0	1	86	22	87	340
119601	0	6	6	72	19	3	0	1	72	23	91	340
124762	0	6	6	71	20	3	0	1	71	22	88	340
129918	0	6	6	72	19	3	0	1	79	22	90	340
135082	0	6	6	72	19	3	0	1	71	22	89	340
140238	1	4	5	83	12	0	0	1	111	20	73	340
145401	0	5	5	74	18	2	0	1	75	22	88	340
150642	0	5	5	79	15	2	0	1	84	22	84	340
158720	0	6	6	72	19	3	0	1	74	22	90	340
160682	0	6	6	72	20	3	0	1	72	22	89	340
166033	0	8	8	66	26	0	0	1	146	17	89	339
171182	0	5	5	72	20	3	0	1	78	21	88	340
176342	0	5	5	72	20	3	0	1	73	22	89	340
181821	0	5	5	77	18	2	0	1	81	22	87	340
186601	0	5	5	73	19	3	0	1	73	22	88	340
191841	0	5	5	72	20	3	0	1	72	22	88	340
197000	0	5	5	74	19	2	0	1	78	22	86	340
202161	0	5	5	73	20	3	0	1	81	22	89	340
207320	0	5	5	73	19	1	0	1	73	21	87	340
212480	0	5	5	74	19	3	0	1	74	22	89	340
217843	0	1	3	89	8	0	0	1	88	22	79	340
222002	0	5	5	73	20	3	0	1	77	21	87	340
227981	0	5	5	73	19	3	0	1	83	21	87	340
233112	0	5	5	74	19	3	0	1	79	21	86	340
238272	0	3	1	83	13	1	0	1	86	22	82	340
243431	0	5	5	74	19	2	0	1	72	22	88	340
248802	2	5	6	73	18	2	0	1	85	21	83	341
253753	2	4	8	75	19	0	0	1	75	22	82	340
258820	2	5	9	75	19	0	0	1	72	22	83	340
348447	2	4	6	73	19	2	0	1	78	20	81	340
350898	2	4	6	75	19	2	0	1	71	21	82	340
358760	2	4	6	73	18	2	0	1	73	21	84	340
360812	2	4	6	73	18	2	0	1	74	20	79	340
366140	1	4	5	77	14	3	0	1	80	21	83	340
371301	2	4	6	74	18	2	0	1	71	20	79	340
378482	2	4	6	75	18	2	0	1	77	20	79	340
381611	2	4	6	74	18	2	0	1	72	20	81	340
386771	2	4	6	74	18	2	0	1	84	19	76	340
391832	2	4	6	75	17	2	0	1	72	20	79	340
397099	2	3	6	75	17	2	0	1	95	19	73	340
402268	3	3	6	76	17	2	0	1	97	14	52	340
407420	2	3	6	75	17	2	0	1	78	20	77	341
412578	2	3	6	74	18	2	0	1	75	19	75	340
417741	2	3	5	79	14	2	0	1	70	20	77	340
422800	3	3	6	74	18	2	0	1	74	19	78	340
429080	1	1	2	88	10	0	0	1	82	18	86	340
433221	2	3	6	77	18	2	0	1	78	19	73	341
436380	2	3	6	75	17	2	0	1	77	20	78	340
443640	2	3	6	82	13	0	0	1	98	16	84	340
448701	3	3	6	77	16	2	0	1	75	19	73	340
451848	3	3	6	77	16	2	0	1	83	19	73	340
458021	3	3	6	78	16	2	0	1	114	16	61	340
464180	3	3	6	76	16	2	0	1	122	14	56	340
469340	3	3	6	78	16	2	0	1	115	15	57	340
474801	3	3	6	78	16	2	0	1	89	18	70	340
479861	3	3	6	77	16	2	0	1	86	18	87	340
484819	3	3	6	76	16	2	0	1	78	18	71	340
488861	3	3	6	78	15	2	0	1	82	18	70	340
496142	2	3	5	83	12	0	0	1	96	18	65	340
500308	4	3	6	78	14	2	0	1	128	18	69	340
506440	3	3	6	76	16	2	0	1	85	19	72	340
510628	3	3	6	75	17	2	0	1	84	20	75	340
515779	3	3	6	77	16	2	0	1	80	20	76	340
520838	3	3	6	75	17	2	0	1	77	20	77	340
526098	3	3	5	78	16	2	0	1	70	20	74	340
531268	3	3	6	78	14	1	0	1	112	18	66	340
536420	3	3	6	78	16	2	0	1	81	20	76	340
541840	3	3	6	77	15	2	0	1	82	19	74	340
546738	3	3	6	77	16	2	0	1	84	18	73	340
551900	3	3	6	77	15	2	0	1	81	19	72	340
557080	3	3	5	77	15	2	0	1	78	19	72	340
562220	3	3	6	77	16	2	0	1	79	18	70	340
567361	3	3	5	77	16	2	0	1	75	19	74	340
572540	3	3	6	77	16	2	0	1	83	18	71	340
577699	3	3	6	77	15	2	0	1	107	16	62	340
582659	3	3	6	78	15	2	0	1	78	19	74	340
588027	3	3	5	78	15	2	0	1	88	18	68	340
593179	4	3	6	77	15	1	0	1	127	14	55	340
598333	3	2	6	78	16	1	0	1	86	17	65	340

Time	A16CO	A16CO2	A16COX	A16M1	A16M2	A16M3	A16M4	ID6	MBC6	Q8CH4C	Q8HCLC	TQ1612
603602	3	3	6	77	16	2	0	1	80	19	12	340
604660	1	1	2	91	8	0	0	1	109	17	60	340
613621	3	3	5	78	15	2	0	1	78	19	71	340
618661	1	1	2	88	12	0	0	1	81	18	68	340
624140	3	3	6	79	14	1	0	1	84	18	67	340
626266	3	3	6	77	16	1	0	1	77	19	70	340
634488	3	2	6	78	15	2	0	1	91	17	66	340
636619	4	3	6	77	15	2	0	1	109	15	58	340
644782	3	3	6	77	15	1	0	1	83	18	67	341
649833	0	2	2	86	12	0	0	1	165	11	42	340
655100	3	2	6	80	14	0	0	1	81	18	68	340
660288	3	3	6	77	15	2	0	1	78	18	70	340
665418	3	2	5	79	14	1	0	1	84	17	63	340
670680	3	2	5	82	13	0	0	1	83	18	65	340
676740	4	3	6	77	16	1	0	1	92	17	63	340
680898	3	2	6	80	15	0	0	1	80	18	71	340
686090	3	2	6	81	14	0	0	1	86	18	64	340
691220	3	2	6	81	14	0	0	1	79	18	66	340
696379	3	2	5	82	12	0	0	1	84	18	64	340
701538	3	2	6	79	14	1	0	1	89	17	66	340
706700	3	2	6	80	14	0	0	1	88	17	62	340
711862	4	2	6	79	15	0	0	1	133	14	49	340
717019	3	2	5	85	10	0	0	1	84	18	83	340
722180	2	2	6	82	13	0	0	1	84	18	83	340
727341	4	2	6	80	14	0	0	1	89	18	64	340
732602	3	2	6	81	14	0	0	1	80	18	85	340
737674	3	2	5	83	12	0	0	1	92	17	60	340
742820	4	2	5	81	13	0	0	1	93	17	62	341
747978	4	2	6	82	12	0	0	1	115	14	53	341
753140	3	2	6	82	13	0	0	1	77	18	66	340
758292	2	2	4	88	8	0	0	1	85	17	58	340
763468	3	2	5	80	16	0	0	1	92	17	64	340
768619	4	2	6	79	14	0	0	1	85	17	83	340
773780	4	2	6	82	12	0	0	1	130	13	45	340
778830	4	2	6	83	12	0	0	1	92	17	59	340
784098	3	2	5	84	11	0	0	1	78	17	61	340
789261	4	2	6	79	15	0	0	1	78	18	64	340
794420	3	2	5	84	11	0	0	1	78	18	63	340
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804741	4	2	6	81	13	0	0	1	78	18	65	340
809889	4	2	6	79	14	0	0	1	80	18	64	340
815060	4	2	6	82	13	0	0	1	106	16	58	340
820228	2	2	4	88	8	0	0	1	80	18	65	340
825380	3	2	5	83	12	0	0	1	86	17	61	340
830641	5	2	7	78	15	0	0	1	120	13	49	340
835699	4	2	7	78	15	0	0	1	78	17	62	340
840888	3	2	5	83	12	0	0	1	80	17	62	340
846020	4	2	6	82	12	0	0	1	88	17	62	340
851180	4	2	6	82	13	0	0	1	77	17	63	340
858339	3	2	5	84	11	0	0	1	79	18	63	340
861699	3	2	5	83	12	0	0	1	84	17	60	340
866661	4	2	6	82	13	0	0	1	82	17	60	340
871819	4	2	6	80	14	0	0	1	78	17	62	340
876879	4	2	6	83	11	0	0	1	118	15	52	340
882141	4	2	6	79	14	0	0	1	90	18	58	340
887300	4	2	6	83	12	0	0	1	98	16	58	340
892468	4	2	6	79	14	0	0	1	88	17	61	340
897820	4	2	5	82	12	0	0	1	88	16	58	340
902782	4	2	6	80	13	0	0	1	94	18	57	340
907839	3	2	5	84	11	0	0	1	88	18	58	340
913089	4	2	6	81	13	0	0	1	98	15	55	340
918266	4	2	7	80	14	0	0	1	103	15	53	340
923435	4	2	6	83	11	0	0	1	118	12	44	340
928840	4	2	6	81	13	0	0	1	84	18	58	340
933738	4	2	6	82	12	0	0	1	99	15	54	340
938889	3	2	5	86	9	0	0	1	109	14	49	340
944069	4	2	6	83	11	0	0	1	89	15	53	340
949221	3	2	5	83	11	0	0	1	84	16	58	340
958421	4	2	6	81	13	0	0	1	95	15	53	340
964581	4	2	5	83	11	0	0	1	78	16	57	340
968741	3	2	5	95	0	0	0	1	80	16	51	340
974800	4	2	6	94	0	0	0	1	82	16	52	340
980061	5	3	8	92	0	0	0	1	88	15	47	340
985220	5	3	8	92	0	0	0	1	88	16	49	340
990379	4	2	6	94	0	0	0	1	79	16	51	341
996638	7	3	9	91	0	0	0	1	124	18	44	340
1000899	4	2	6	94	0	0	0	1	90	18	50	340
1005883	6	2	7	93	0	0	0	1	108	14	43	341
1011018	4	2	6	94	0	0	0	1	79	15	48	340
1016178	4	2	6	94	0	0	0	1	84	18	50	340
1021341	5	3	8	92	0	0	0	1	90	18	49	340
1026490	5	2	7	79	14	0	0	1	92	16	56	340
1031660	4	2	6	80	13	0	0	1	80	15	56	340
1036819	4	2	7	80	13	0	0	1	80	18	67	346
1044321	4	2	6	81	13	0	0	1	84	17	66	346
1048480	6	3	8	75	16	1	0	1	80	17	63	346
1064460	4	2	7	79	13	1	0	1	123	14	48	346
1068799	4	2	6	85	9	0	0	1	70	17	60	346
1069490	4	2	6	82	12	0	0	1	77	17	65	346
1070119	5	3	8	75	16	2	0	1	78	17	63	346
1078279	4	2	6	82	12	0	0	1	75	19	67	346
1080455	4	2	6	81	13	0	0	1	79	19	67	346
1086582	0	3	3	84	13	0	0	1	79	19	67	346
1090759	5	3	7	78	15	0	0	1	93	18	68	348
1098820	4	2	6	83	11	0	0	1	82	19	67	348
1101062	4	2	6	83	11	0	0	1	82	19	68	348
1106240	4	2	6	83	12	0	0	1	72	19	68	348
1111396	5	3	8	77	15	0	0	1	94	18	66	348
1116859	4	2	6	83	11	0	0	1	80	18	63	348
1121721	4	2	7	81	12	0	0	1	103	19	60	348
1126560	4	2	6	82	12	0	0	1	74	17	60	348
1132041	3	2	5	86	9	0	0	1	81	17	60	348
1137196	6	2	7	80	13	0	0	1	102	14	50	348
1142262	6	2	7	81	13	0	0	1	96	15	53	348
1147620	5	3	8	79	14	0	0	1	86	18	64	348
1152678	7	3	9	78	14	0	0	1	133	10	34	348
1157842	6	2	7	80	13	0	0	1	84	15	62	348
1163008	4	2	6	84	10	0	0	1	88	15	52	348
1168158	4	2	6	83	11	0	0	1	95	15	52	348
1173319	3	2	5	87	8	0	0	1	86	15	51	348
1178479	2	1	3	92	5	0	0	1	71	15	63	348
1183840	6	2	8	79	13	0	0	1	99	14	52	348
1188802	3	2	5	87	8	0	0	1	78	15	53	348
Time												

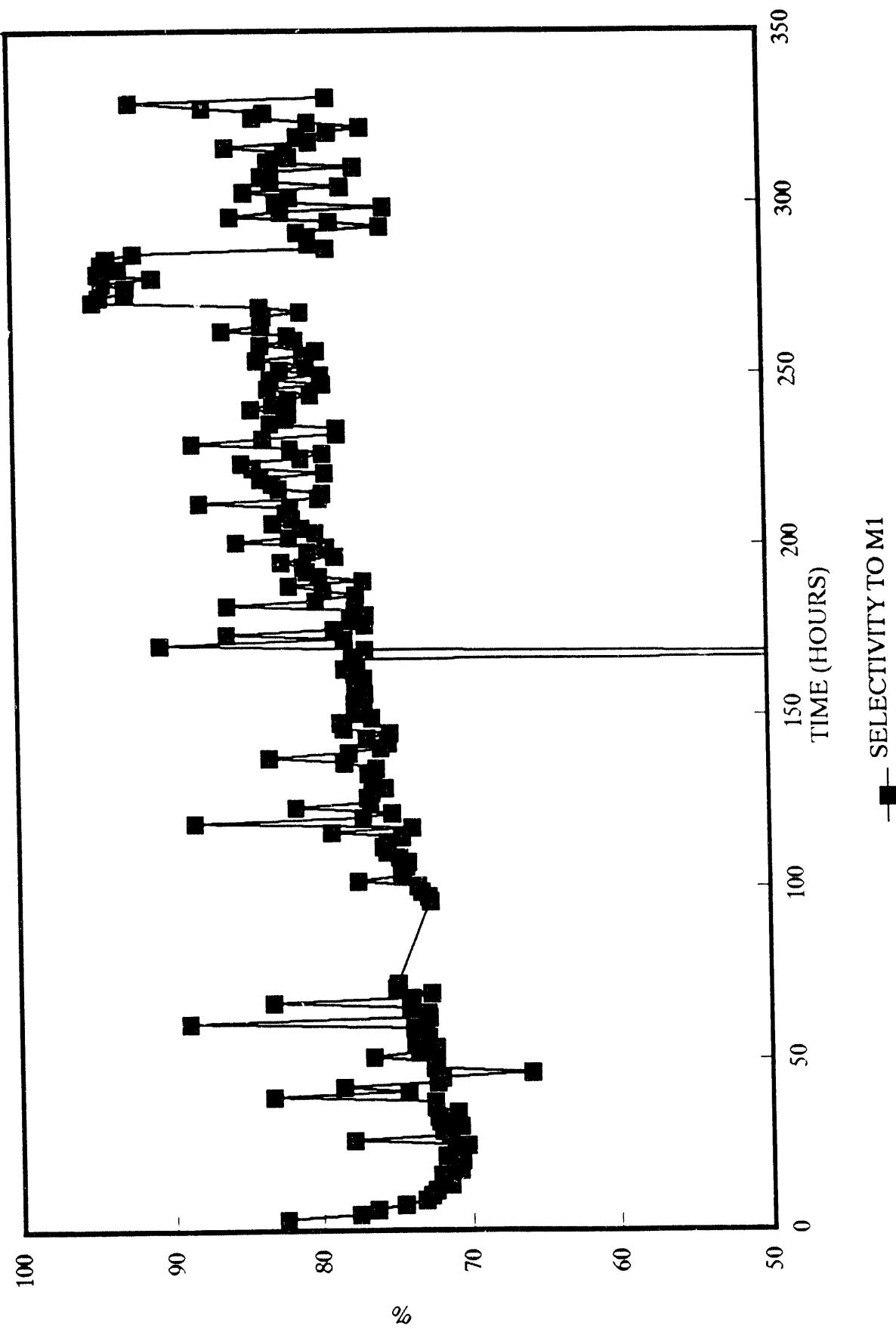
RUN 10346063

CAT 535



RUN 10346063

CAT 535



Data Appendix B
Catalyst Synthesis and Composition Information

CATALYST 511

SUPPORT	Silica CS-1040, PQ Corp. Lot #1229-2201
SOURCE	$\text{CuCl}_2 \cdot 2\text{H}_2\text{O}$. 9947 lab-book page 34.
LOADING	0.992% Cu, 1.34% Cl.
IMPREGNATION METHOD	Very short impregnation period. While heating the solvent was evaporated using a nitrogen flow.
PRETREATMENT	Under vacuum for 3 hours at 140 °C, and R.T. overnight under static vacuum.
COLOR	Green.

CATALYST 516

SUPPORT	Silica (CS-1040)
SOURCE	CuCl. 9947 lab-book page 46.
LOADING	2.23% Cu, 1.29% Cl.
IMPREGNATION METHOD	The pale yellow acetonitrile solution of the pure salt was added to the support for impregnation overnight. Solvent removed while heating at 50 C for 1.5 hours under vacuum.
PRETREATMENT	Under full vacuum at 350 °C for 2 hours
COLOR	White

CATALYST 518

Silica (CS-1040)

"Cu₆Al" cluster. 9947 lab-book page 43 and 54.

1.86% Cu, 0.14% Al.

METHOD

The acetonitrile solution of the cluster was left with the support overnight. The pale blue color of the solution was decanted and the catalyst was dried (see pretreatment).

Under full vacuum

- A. 50-60 °C for 1 hour
- B. 200 °C for 2 hours
- C. 350 °C for 2 hours

Black

CATALYST 535

Silica CS-1040, PQ Corp. Lot #1229-2201

[Cu(NCCH₃)₄PF₆. 9947 lab-book page 89.

1.94% Cu, 12.1% Cl, 1.16% Li, 19.5% Li, and 1.02% P.

METHOD

The colorless acetonitrile solution of the salt was added to the support for impregnation over the weekend. The solvent was removed under vacuum. A solution in water was made from LaCl₃ and LiCl and was added to the catalyst preparation. The water was removed with a dry nitrogen purge.

Under vacuum for 30 minutes at 110 °C.

CATALYST 163C
(Purchased G-108 SUD-CHEMIE)

SUPPORT Silica

SOURCE Unknown

LOADING Cu = 30%

IMPREGNATION METHOD Unknown

PRETREATMENT Under flowing dry nitrogen for 60 minutes at 350 °C.. Crushed and sieved between 18 an 35 mesh.

July 1974

DATE
REMOVED

1974

