

DOE/PC/91292--T4

RHEOLOGICAL PROPERTIES ESSENTIAL FOR THE ATOMIZATION OF
COAL WATER SLURRIES (CWS).

Quarterly Progress Report
June 15, 1992-September 15, 1992

DOE/PC/91292--T4

DE93 006004

FRANK OHENE
Department of Chemistry
Grambling State University
Grambling, LA 71245

Technical Project Officer
U. S. Department of Energy
Pittsburgh Technology Energy Center
P. O. Box 10940
Pittsburgh, PA 15236

Work Performed for the Department of Energy Under
Contract #DE-FG22-91PC91292

DISCLAIMER

"This report was prepared as an account of work sponsored by an agency of the United States Government. Neither the United States Government nor any agency thereof, nor any of their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference therein to any specific commercial product, process or service by tradename, trademark, manufacturer, or otherwise, does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof. The views and opinions of the author expressed herein do not necessarily state or reflect those of the United States or Government or any agency thereof."

MASTER

EB

REPRODUCTION OF THIS DOCUMENT IS UNLIMITED

OCT 15 1992

OVERALL OBJECTIVE:

The overall objective of this project is to perform experiments to understand the effect of high shear and extensional properties on the atomization of coal-water slurries (CWS). In the atomization studies, the mean drop size of the CWS sprays will be determined at various air-to CWS. A correlation between the extensional and high shear properties, particle size distributions and the atomization will be made in order to determine the influence of these parameters on the atomization of CWS.

Work Done

During the past quarter, several experimental studies on pressure dependent atomization of Coal-water slurries and simulated fluids were performed. Also surface tension, elastic, high and low shear viscosities were performed. These tests were performed to initiate the understanding of the fundamental parameters that govern the atomization process of CWS.

Surface Tension

The influence of surface tension on Sauter mean Diameter (SMD) has been discussed by Lefebvre [1]. Thus, to test the significance of this parameter on atomization, the surface tension of several diluted concentrations of corn syrup were measured using Fisher model du-Nuoy Tensiomat, model 21. The tensiomat's performance was initially verified by determining the surface tension of distilled water. Excellent agreement was obtained between the measured value and the literature value of 72 dynes/cm. The results of the surface tension measurements as well as, the viscosity and the densities

are as shown in Table 1.

Rheological Properties

The Rheological properties of the corn syrup solutions were determined using a Haake RV-20 rheometer. The corn syrup solutions were found to be Newtonian and the viscosities ranged from 709 mPas.s to 120 mPas.s, depending on the concentration. The flow curves for 100% and 80% corn syrup solutions are as shown in Figures 3 and 4. The densities of these solutions were found to be in the range of 1.37 to 1.02 gm/mL (Table 1). The density of the coal-water slurries used had densities of between 1.12gm/mL and 1.26 gm /ml.

In order to understand the CWS atomization behavior, it is necessary to understand the flow behavior of the CWS. A low shear flow behavior of 66% and 61 % CWS (PSOC-1527) containing 0.5% A-23 coal weight as additive, and high shear flow behavior of 61% (PSOC-1527) slurry used in the atomization studied are as shown in Figures 5-8. The high shear was run on Pen-Kem HVA-6 capillary rheometer (Figure 8). This instrument was evaluated and found to be excellent in the study of high shear behavior of the CWS. Also, a viscoelastic measurements of the CWS was made (Figure 7). The slurry exhibited a Newtonian flow in the shear rate region of between 8.89×10^3 1/s and 1.29×10^5 1/s (Figure 7 and Table 2.) The viscoelastic measurement show that the slurry has a considerable elastic component (Figure 8).

Several experiments on the high shear and the viscoelastic behavior will be performed during the next quarter in order to

relate the data to the Sauter Mean Diameter (SMD).

Atomization Studies

Atomization studies were performed at Adelphi University. The initial tests were performed to compare and optimize conditions necessary for the CWS atomization. A video camera system and a Malvern 2600 particle size analyzer and a Dalvan Airo Nozzle were used to provide information about the spray characteristics, including drop size distribution, mean median size distribution and spray velocity. The source of atomizing air used was the house air system, which delivers air at pressures up to a maximum of 85 psig. The atomizing air passes through a filter and a flowmeter before it enters the atomizer.

The atomization results of the corn syrup solutions and the CWS are as shown in Figures 1 and 2. The Sauter Mean Diameter (SMD) obtained for each concentration is as listed in Figures 1 and 2. In the corn syrup atomization studies, the SMD was found to decrease with decrease in the corn syrup concentration. The A/F ratio was maintained at 0.2 in this studies. The density and surface tension of the solution were also found to decrease with concentration. In the CWS atomization studies, the A/F ratio was increased to 0.4 due to initial clogging of the nozzle at the low A/F ratio. This increase was necessary to effect a constant stream of fine spray production. This is an indication that the atomization of the CWS is dependent on the A/F ratio.

The CWS used exhibited a pseudoplastic with yield flow behavior in the low shear regime, whereas the Corn syrup solutions

exhibited a Newtonian flow behavior (Figure 3-6). The observed differences in fine spray obtained for the CWS and the corn syrup solutions at A/F ratio of 0.2 , is probably due to differences in their flow behaviors.

Further experiments on corn syrup solutions containing polymer additives, will be performed in the subsequent quarters to determine the effect of the flow behavior (consistency index, density, A/F ratio and surface tension) of the corn syrup solutions on atomization. Varying concentrations of xantham gum will be added to the corn syrup solutions and changes in the flow consistency index noted as a function of Xantham gum concentration.

Table 1

Corn Syrup Concentration(%)	Density (gm/mL)	Surface Tension (dynes/cm)	Viscosity (mPa.S)
100	1.37	80.64	750
90	1.31	76.1	234
80	1.26	73.8	196
70	1.23	70.9	103
60	1.19	59.8	72.4
50	1.14	53.4	45.2
30	1.08	51.2	34.2

TABLE 2

HIGH SHEAR RHEOLOGY DATA

A P P A A R

H V A - 6

R E S U L T S

from

05/08/1992

Operator : Hancy
 Sample : Slurry 2
 Solvent : 1000
 Density (kg/m³) : 1200
 Capillary-length (mm) : 100.00

File : SLUR2
 Number : ms980b
 Temperature(°C) : 20
 Capillary-diameter (mm) : 0.800

HVA 6 - Table lin (measured)

No.	τ_{AO} (Pa)	τ_{AO} corr (Pa)	D (1/s)	EIA (Pa.s)	Reynolds	t_v (s)
1	2.600E+02	2.579E+02	8.890E+03	0.0290	27	0.1125
2	3.600E+02	3.559E+02	1.242E+04	0.0286	42	0.0805
3	5.600E+02	5.464E+02	2.248E+04	0.0243	87	0.0445
4	8.200E+02	7.964E+02	2.564E+04	0.0267	106	0.0337
5	1.160E+03	1.112E+03	4.211E+04	0.0264	153	0.0237
6	1.560E+03	1.474E+03	5.672E+04	0.0260	210	0.0176
7	1.880E+03	1.751E+03	6.921E+04	0.0253	263	0.0144
8	2.380E+03	2.183E+03	8.567E+04	0.0255	323	0.0117
9	3.120E+03	2.830E+03	1.038E+05	0.0273	366	0.0096
10	3.880E+03	3.433E+03	1.290E+05	0.0266	465	0.0078

Reference

1. Lefebvre, A. H., Atomization and Spray Technology, **3**, (1987), 37-31.

Fig. 2. Particle Size Distribution of Varying Concentrations of CWS (PSOC-1527).

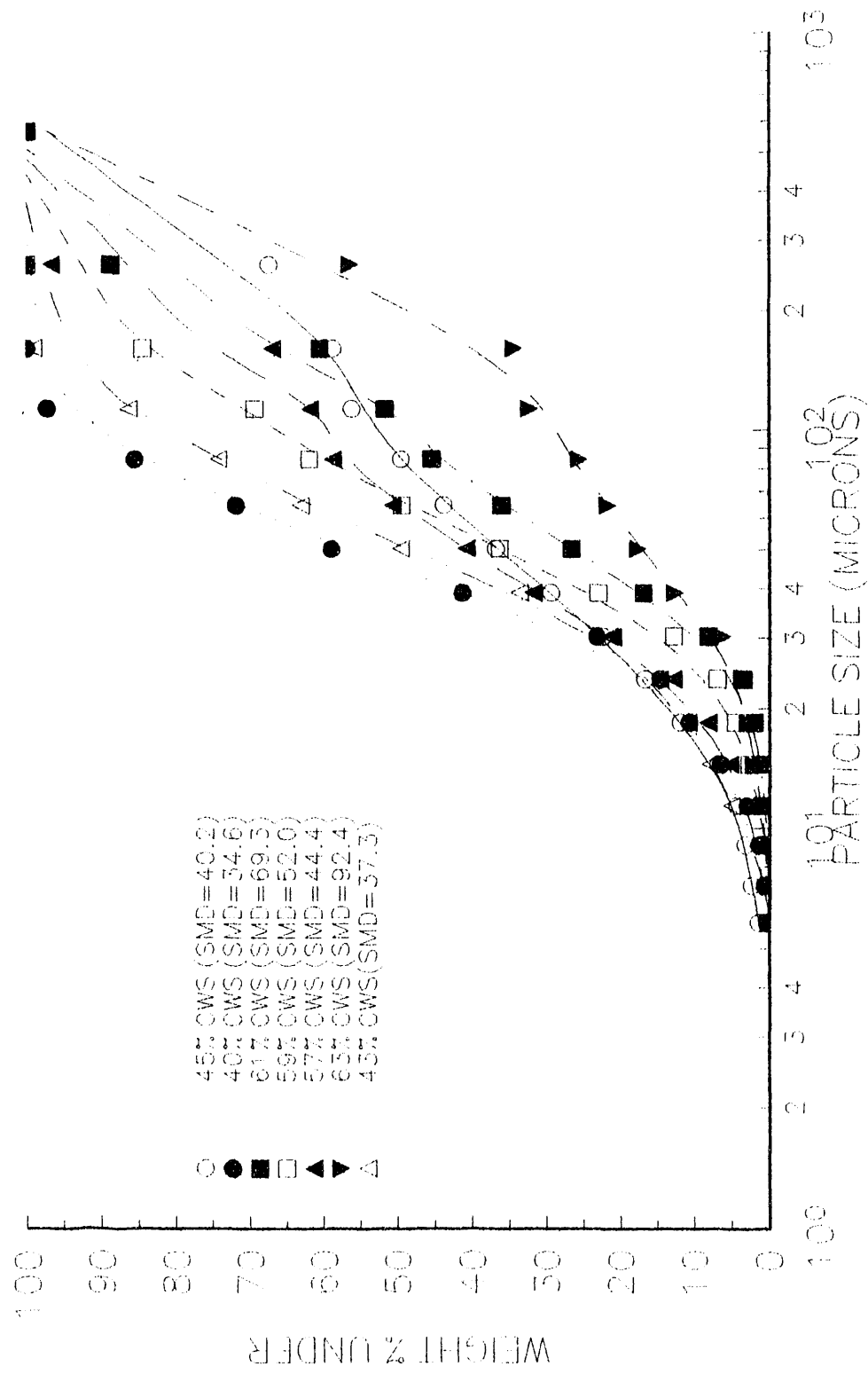


Fig. 1. Particle Size Distribution of Varying Concentrations of Corn Syrup.

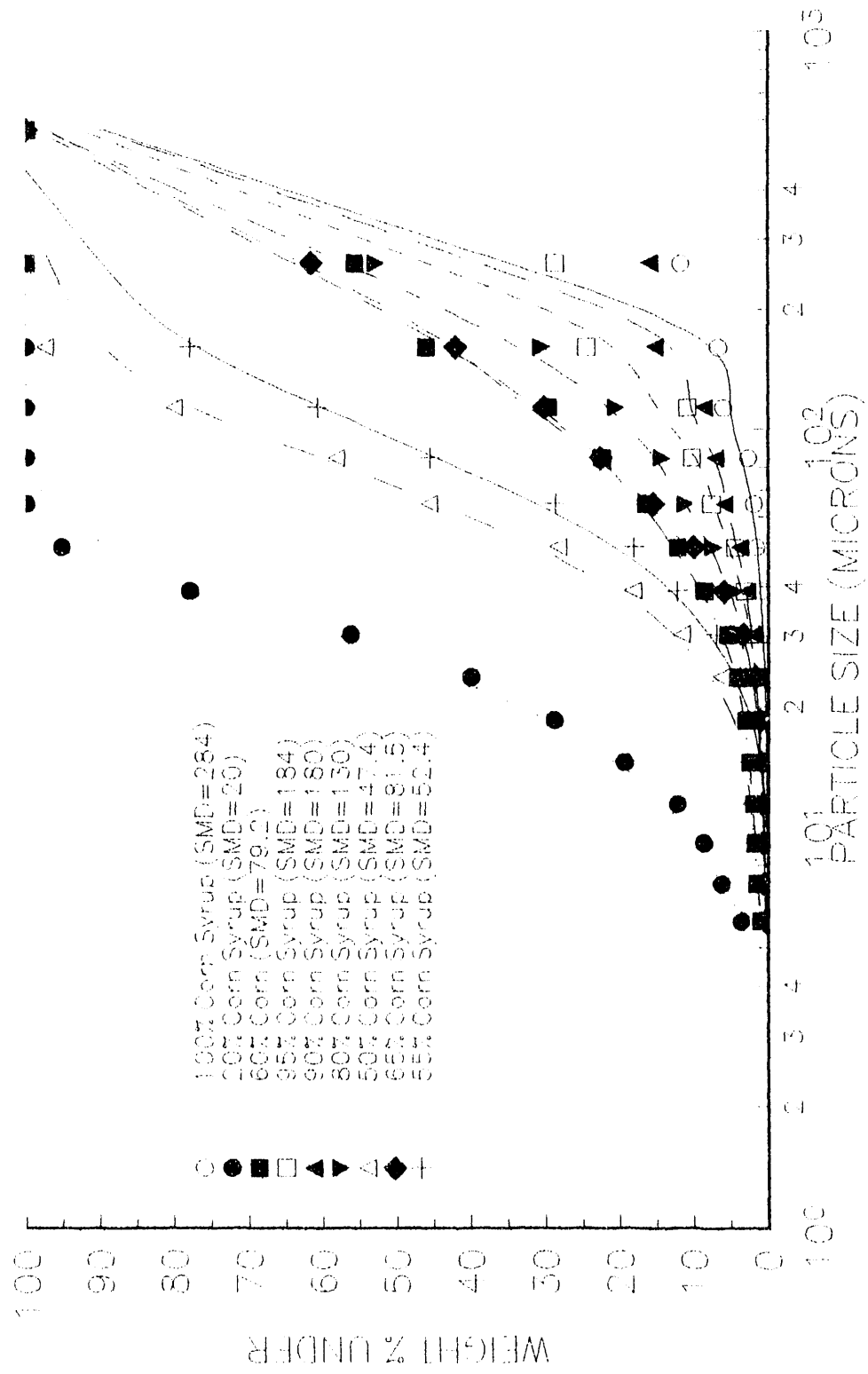


FIGURE 3: FLOW BEHAVIOR OF 100% CORN SYRUP

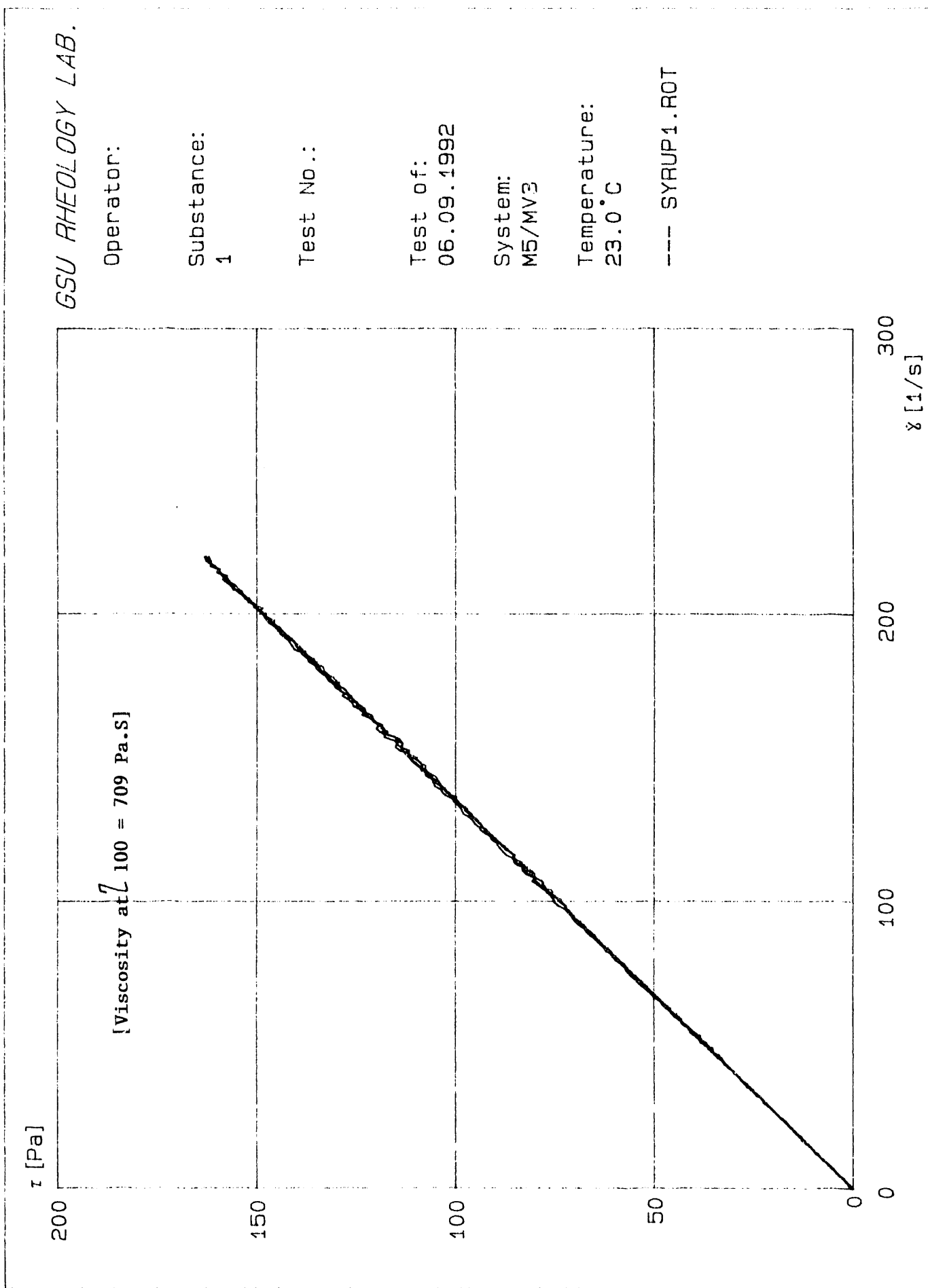
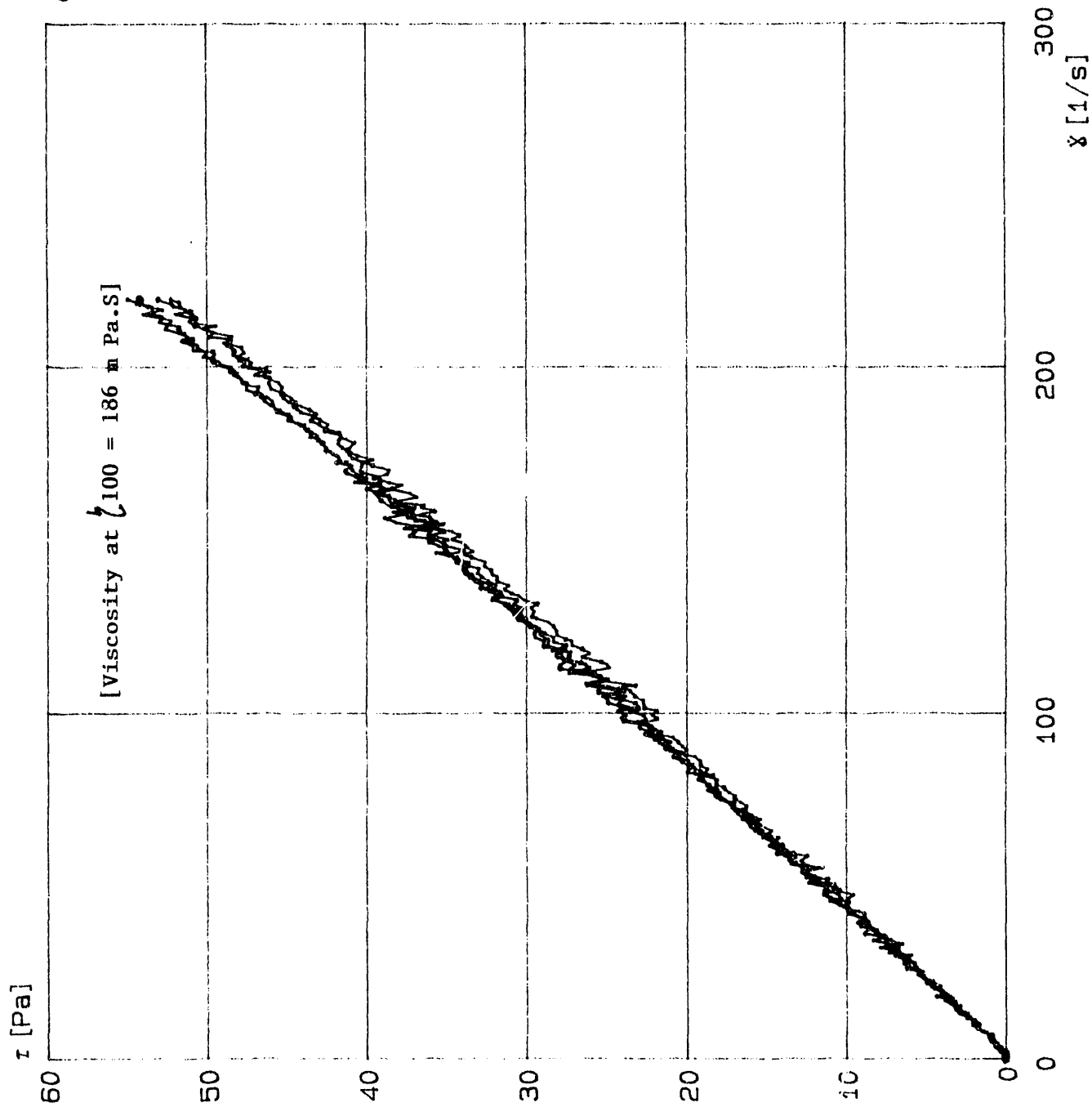


FIGURE 4: FLOW BEHAVIOR OF 80% CORN SYRUP SOLUTION



GSU RHEOLOGY LAB.

Operator:

Substance:
80% syrup

Test No.:

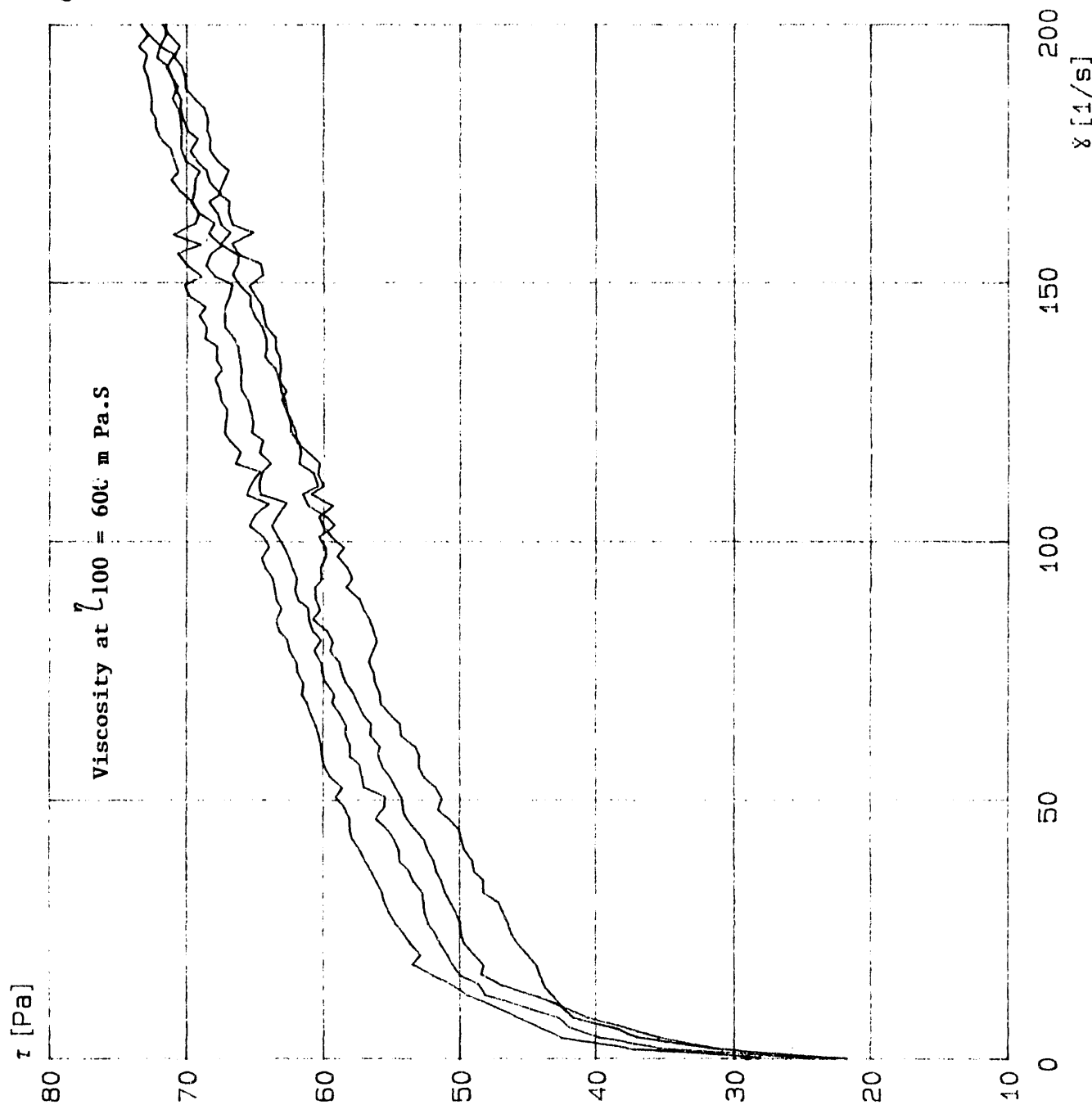
Test of:
16.09.1992

System:
M5/MV3

Temperature:
23.0 °C

---- 8SYRUP.ROT

FIGURE 5: LOW SHEAR FLOW BEHAVIOR OF 66Z CWS (PSOC-1527)



GSU RHEOLOGY LAB.

Operator:
Urelaine

Substance:
1527 unsieved A-2
3

Test No.:
2

Test of:
08.07.1992

System:
M5/MV3

Temperature:
23.0 °C

--- U15272.R0T

FIGURE 6: LOW SHEAR FLOW BEHAVIOR OF 61Z CWS (2S0C-1527)

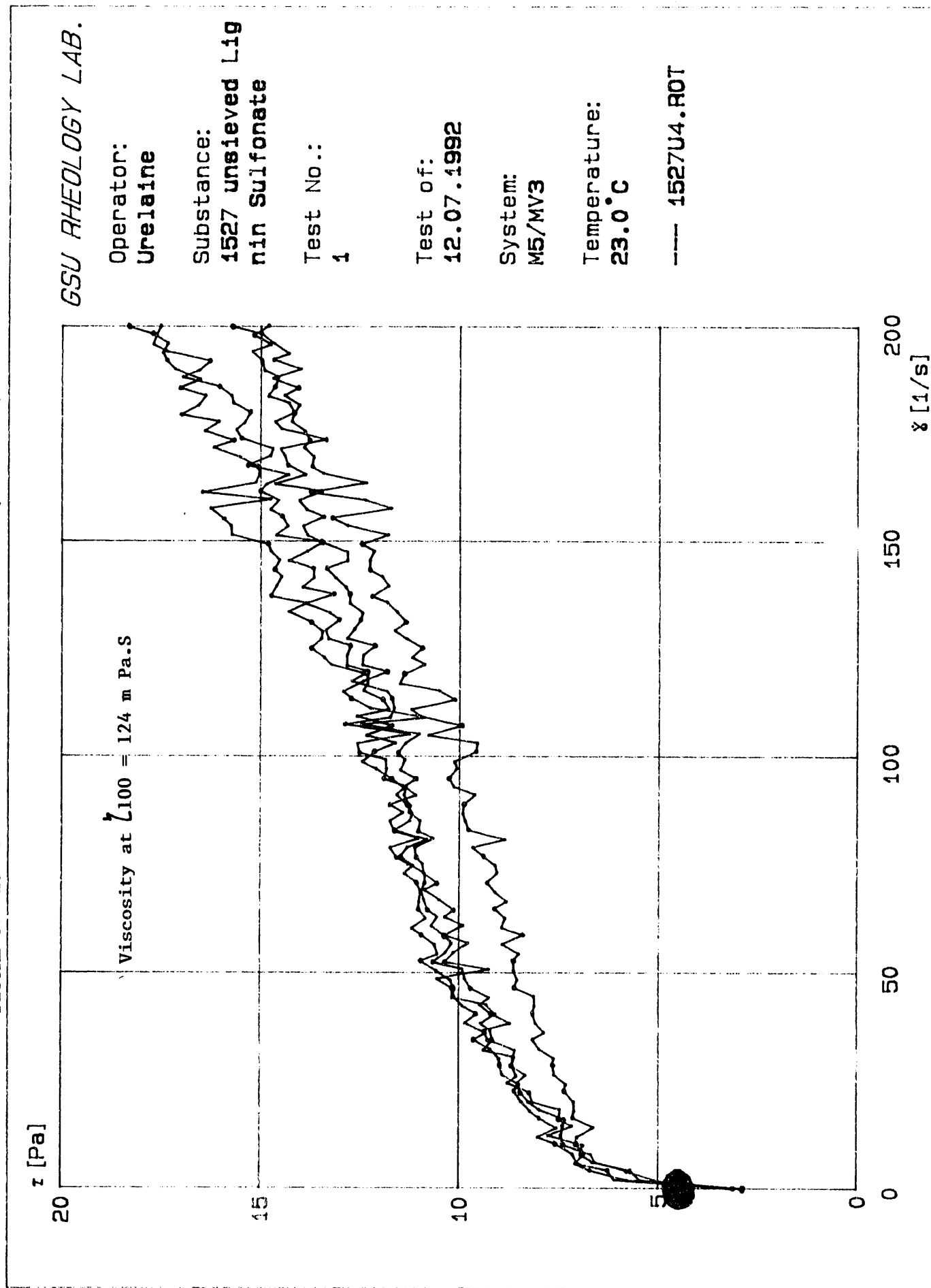


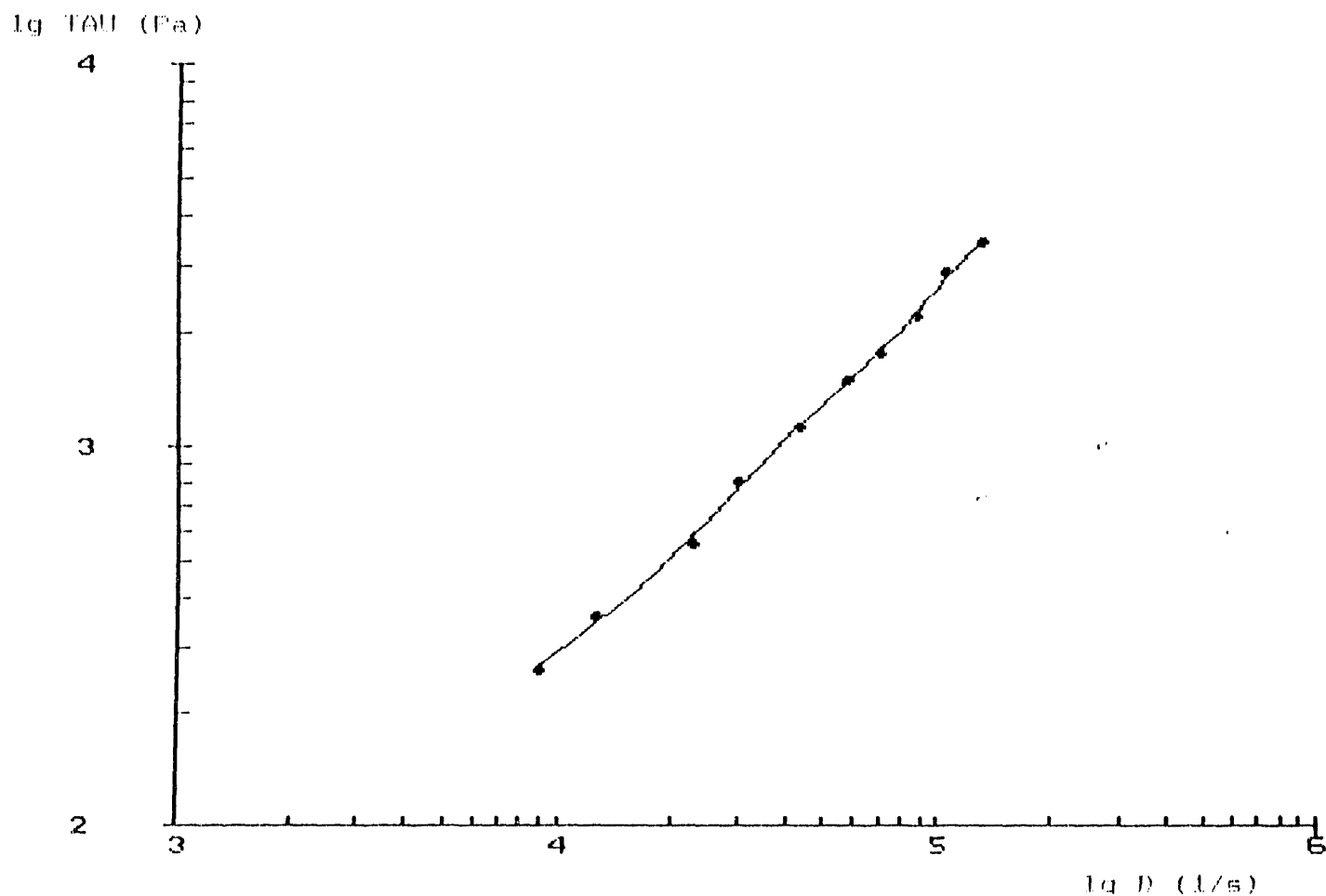
FIGURE 7: HIGH SHEAR FLOW BEHAVIOR OF 61% CWS (PSOC - 1527)

A P P A R

H V A - 6

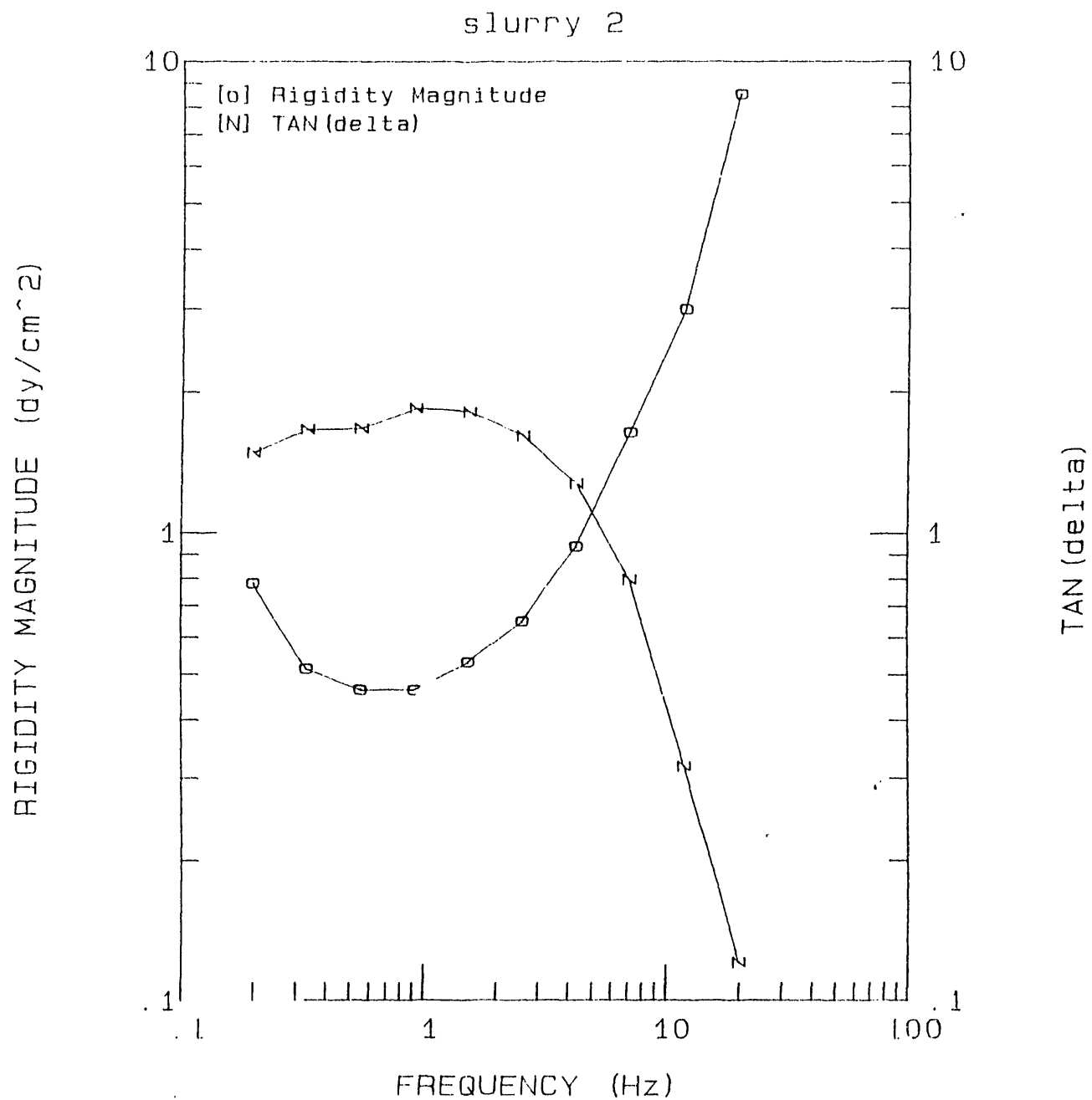
R E S U L T S from 05/08/1992

Operator	: Hancy	File	: SLUR2
Sample	: Slurry 2	Number	: ms980b
Solvent	: 1000		
Density (kg/m ³)	: 1200	Temperature (°C)	: 20
Capillary length (mm)	: 100.00	Capillary-diameter (mm)	: 0.800



VISCOELASTIC MEASUREMENT OF 61% CWS (PSOC - 1527)

Frequency (Hz) [.2- 20] Den. (g/ml) =1.2 Temp. (°C) =25.8
 Tube: Radius (cm) =.0523 Length (cm) =8



**DATE
FILMED**

2 / 3 / 93

