

# ***CO<sub>2</sub> Capture with Enzyme Synthetic Analogue***

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**Funded by:**



**arpa-e**

# Program Team

- Hamilton Sundstrand  
*Review of CO<sub>2</sub> separations system testing*
- Columbia University  
*Modification of Synthetic Analogue  
(Prof. Gerard Parkin's group)*
- WorleyParsons, LLC  
*Review of power plant -coupled system performance and cost models*
- CM-Tec, Inc.  
*Custom Chemical Synthesis*
- GL Chemtec Int'l, Ltd.  
*Custom Chemical Synthesis*
- Consultants:



Prof. Benny Freeman  
University of Texas



Prof. William Koros  
Georgia Tech



Prof. Don Paul  
University of Texas

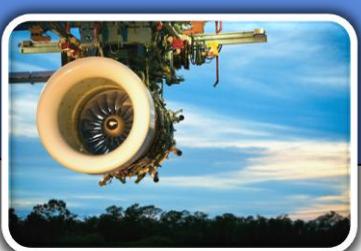
# Program Team (Cont'd): UTRC

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<b>Bart Van Hassel</b> , PhD	Membrane Science
<b>George Zafiris</b> , PhD	Chemical Engineering

# United Technologies

## *Business units*

### Pratt & Whitney



*2009 Revenues  
\$52.9 billion*

### aerospace systems

#### Sikorsky



#### Carrier



### power solutions

#### UTC Power



### Hamilton Sundstrand



### UTC Fire & Security



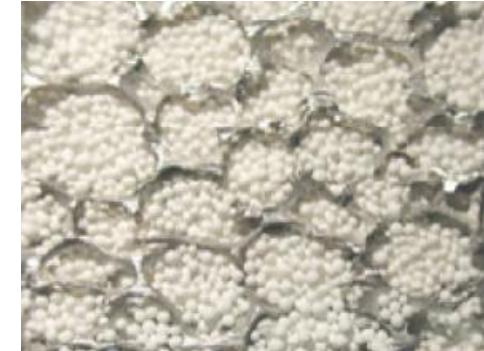
### building systems

#### Otis



# Hamilton Sundstrand: CO<sub>2</sub> Capture for Space Applications

- CAMRAS: CO<sub>2</sub> And Moisture Removal Amine Swing bed
- Prototype delivered to NASA JSC (currently TRL6)
- Baseline for Orion; Lunar Lander; and new space suit
- Regeneration by space vacuum  
(heat for Mars environment)
- Heat exchange between adsorption/desorption  
maintains system isothermal



HS solid amine sorbent  
in metal foam



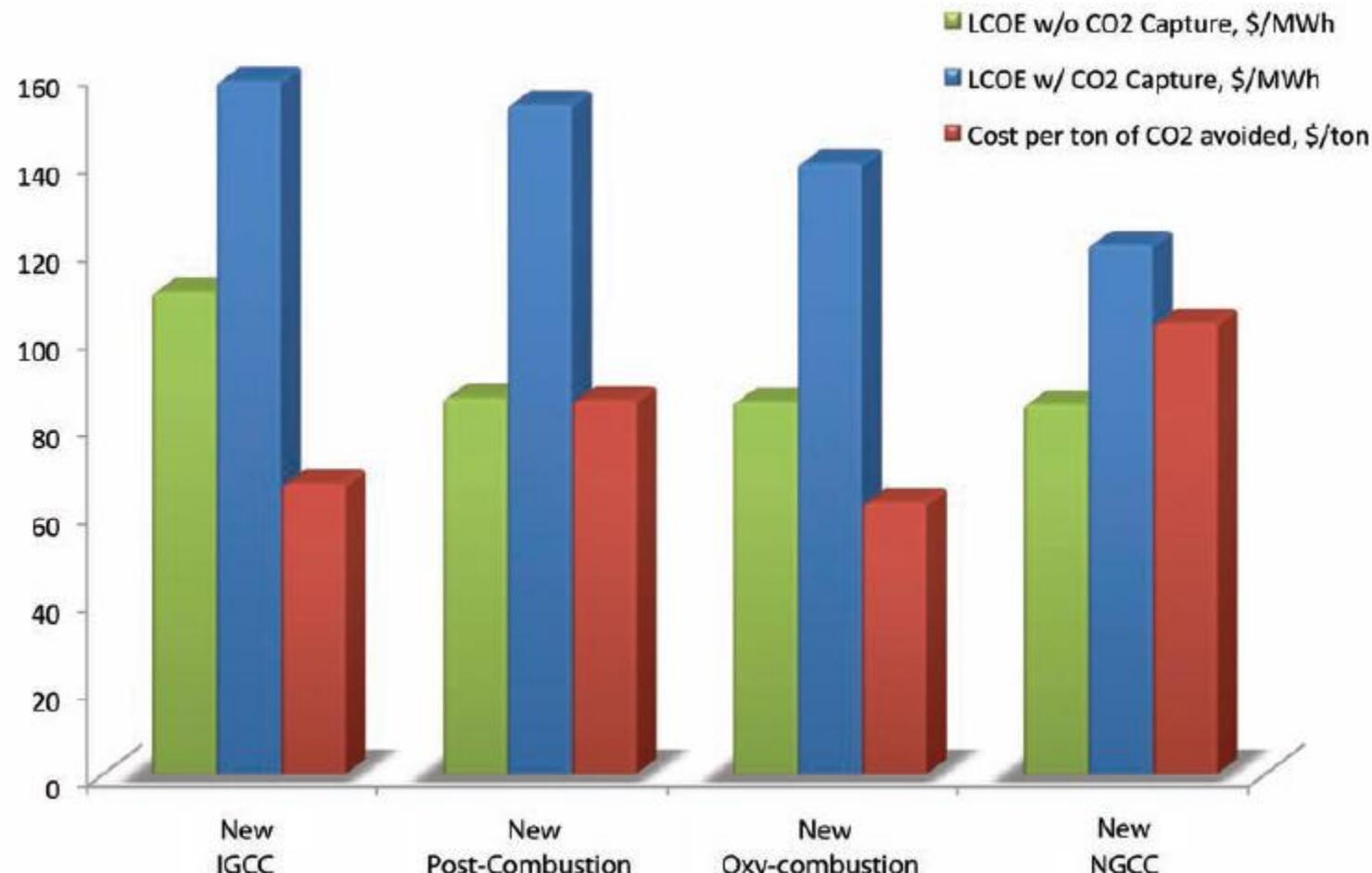
Volunteers and NASA JSC scientists testing the CAMRAS system



Prototype CAMRAS system

# Post-Combustion CO<sub>2</sub> Capture from Power Plants

*Technologies exist, but COE would almost double*

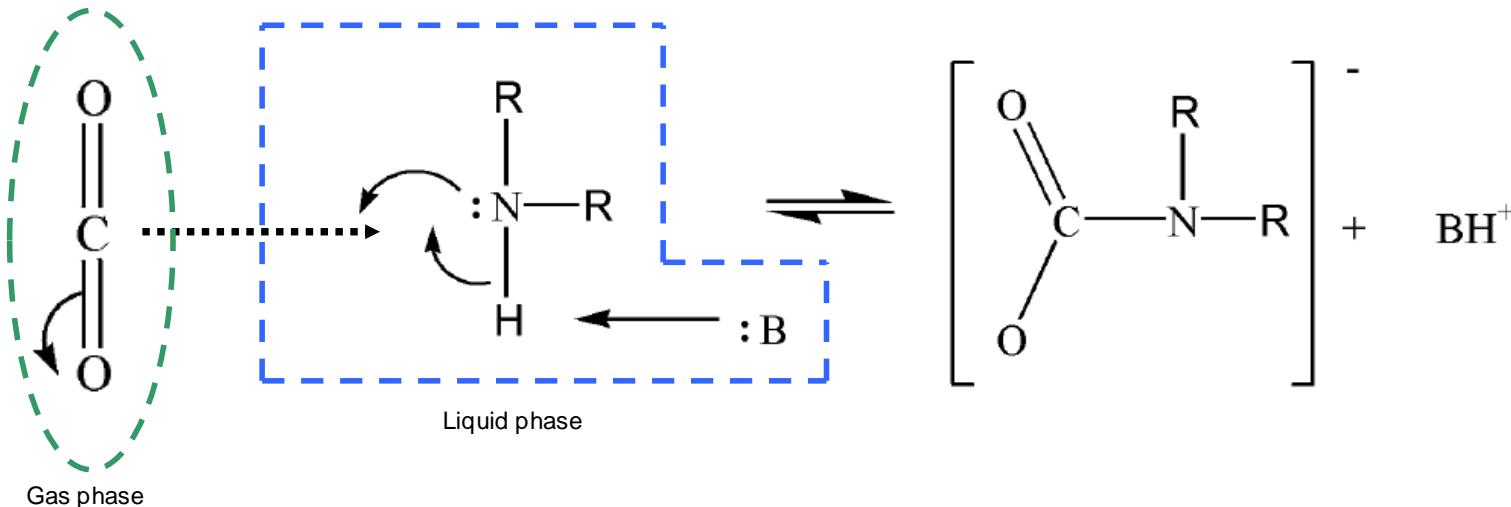


Source:

DOE/NETL Advanced CO<sub>2</sub> Capture R&D Program  
Technology Update: September 2010

# Existing technology: Reaction between Liquid Amines and CO<sub>2</sub>

*High cost can be traced to limitations in chemistry*



	Pulverized Coal Boiler			
	PC Subcritical		PC Supercritical	
	Case 9	Case 10	Case 11	Case 12
CO <sub>2</sub> Capture	No	Yes	No	Yes
Gross Power Output (kW <sub>e</sub> )	583,315	679,923	580,260	663,445
Auxiliary Power Requirement (kW <sub>e</sub> )	32,870	130,310	30,110	117,450
Net Power Output (kW <sub>e</sub> )	550,445	549,613	550,150	545,995
Coal Flowrate (lb/hr)	437,699	646,589	411,282	586,627
Natural Gas Flowrate (lb/hr)	N/A	N/A	N/A	N/A
HHV Thermal Input (kW <sub>th</sub> )	1,496,479	2,210,668	1,406,161	2,005,660
Net Plant HHV Efficiency (%)	36.8%	24.9%	39.1%	27.2%
Net Plant HHV Heat Rate (Btu/kW-hr)	9,276	13,724	8,721	12,534
Raw Water Usage, gpm	6,212	12,187	5,441	10,444
Total Plant Cost (\$ x 1,000)	852,612	1,591,277	866,391	1,567,073
Total Plant Cost (\$/kW)	1,549	2,895	1,575	2,870
LCOE (cents/kWh) <sup>1</sup>	64.0	118.8	63.3	114.8

(Exhibit 4-46, DOE/NETL - 2007 / 1281)

## High regeneration energy:

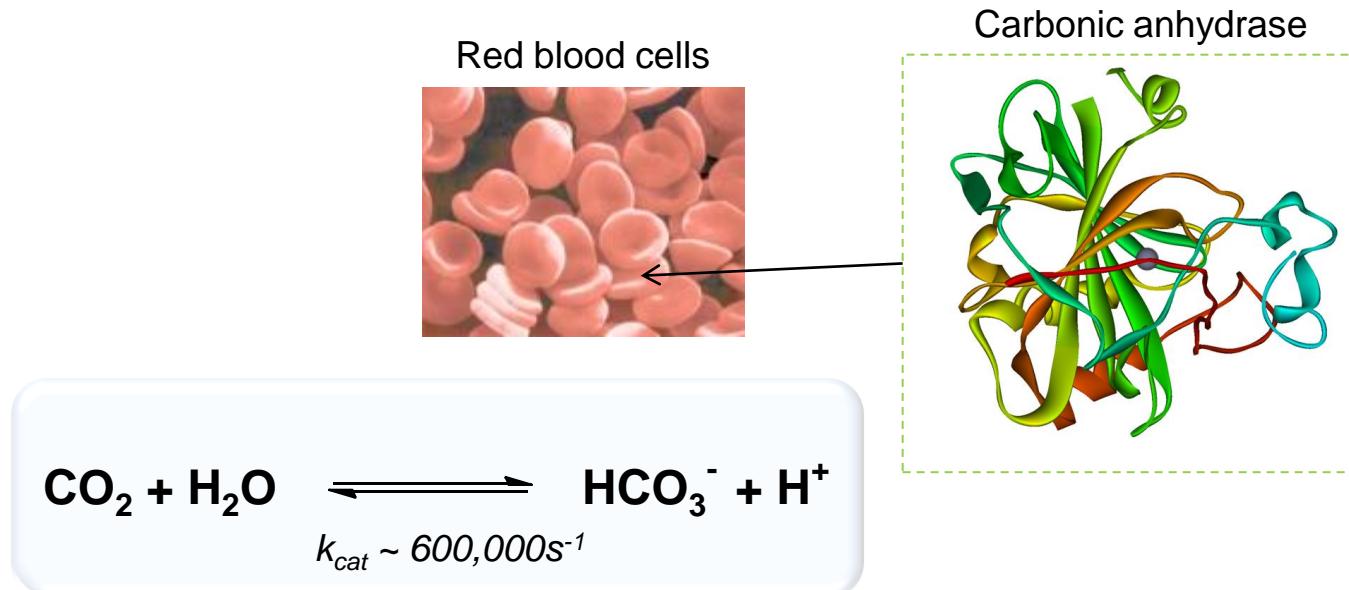
- 1) Reaction forms stable compound
- 2) ~70% of total mass is water

## Slow kinetics:

- 1) CO<sub>2</sub> diffusion through liquid phase
- 2) Alignment with base and amine  
(low probability for reaction)

# Nature's Solution: Carbonic Anhydrase

*One of the fastest enzymes known; ancient and ubiquitous*

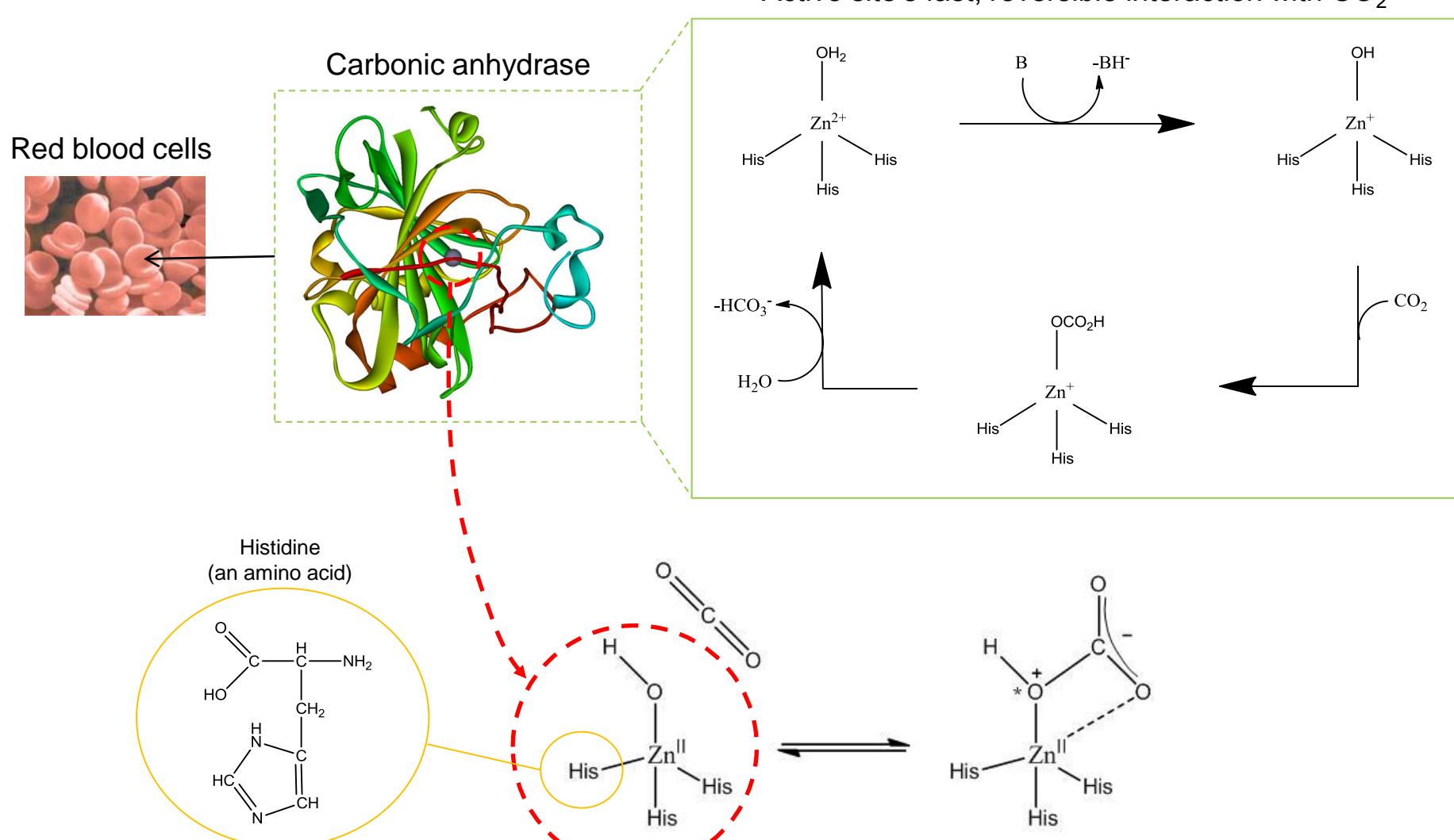


Limitations with using CA directly:

*Not “designed” for harsh environments*  
*Thermodynamically unstable, sensitive to pH*  
*High cost*

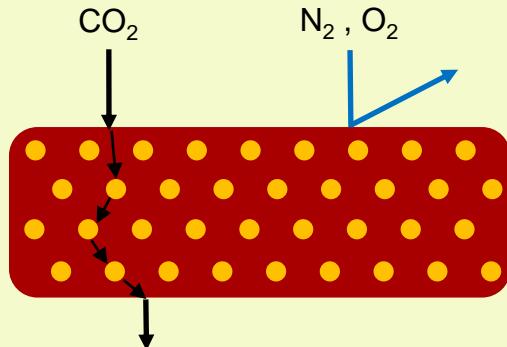
# Overview of CA Structure & Function

*Active site stereochemistry key for fast, reversible interaction with CO<sub>2</sub>*



# Proposed Approach: Membrane-based Separation

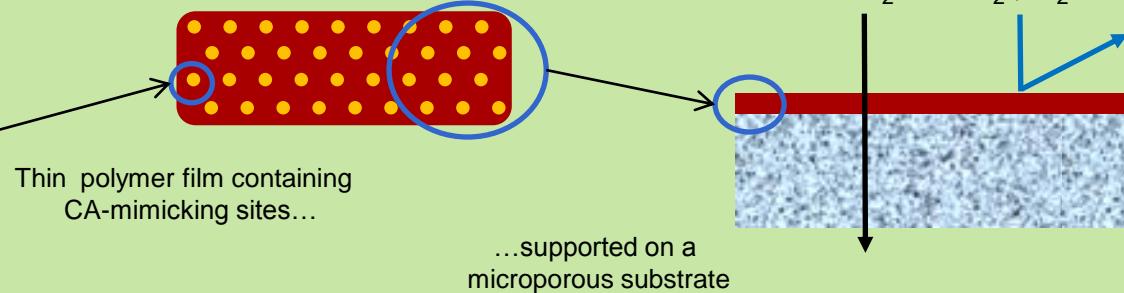
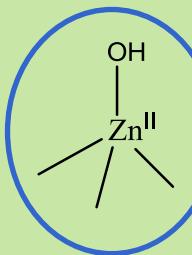
*CO<sub>2</sub> transport facilitated by carriers mimicking enzyme active site*



“Ideal” membrane:

- CO<sub>2</sub> transport is facilitated by specialized “carriers” within a barrier film
- Requires sites exhibiting fast and reversible interaction with CO<sub>2</sub>

Proposed approach:



- ~30% lower CO<sub>2</sub> capture cost compared to liquid amines
- ~2 billion tons/yr CO<sub>2</sub> from existing coal-fired power plants
- Modular, skid-mounted configurations; no moving parts
- Flexibility to start with smaller system, gradually increase to 90% CO<sub>2</sub> capture

# Key Questions

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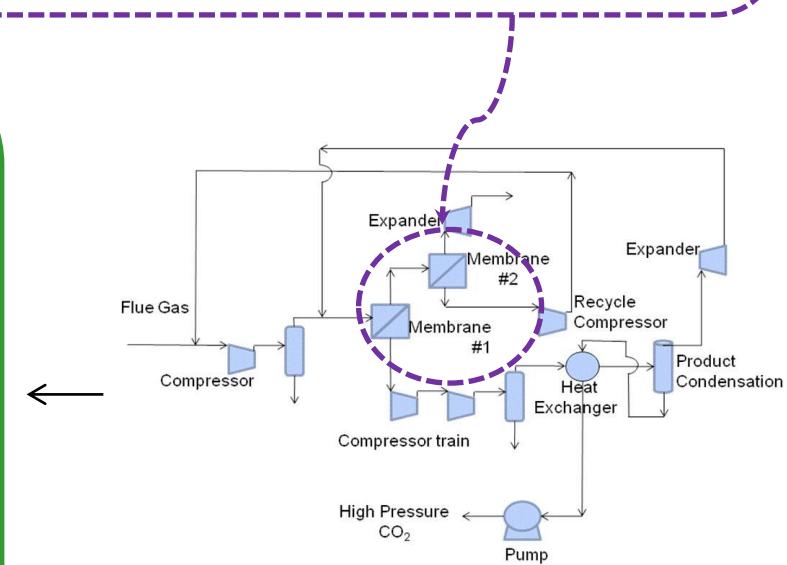
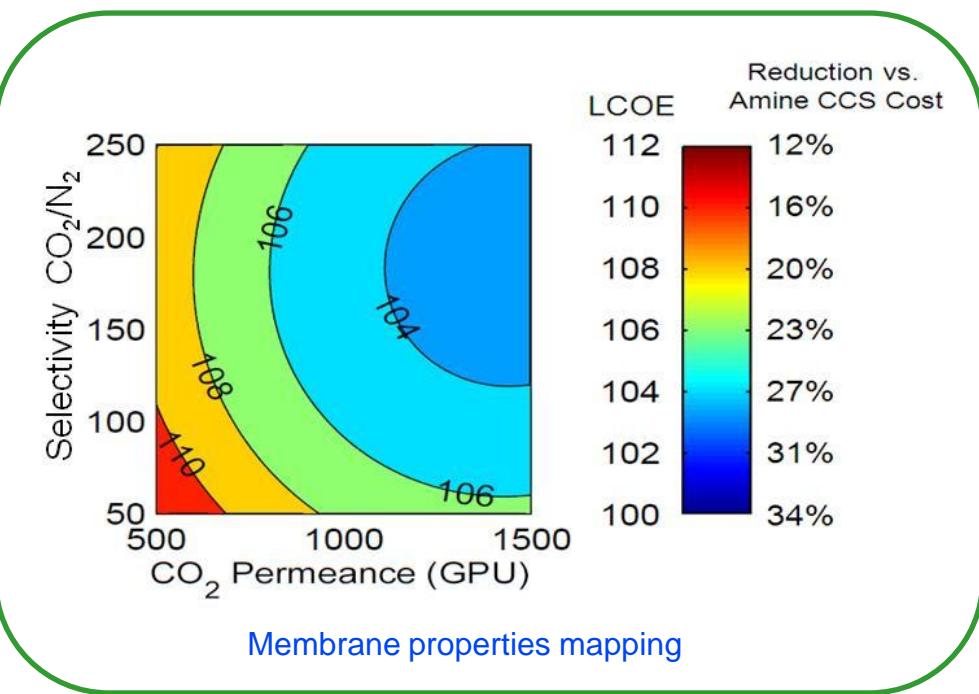
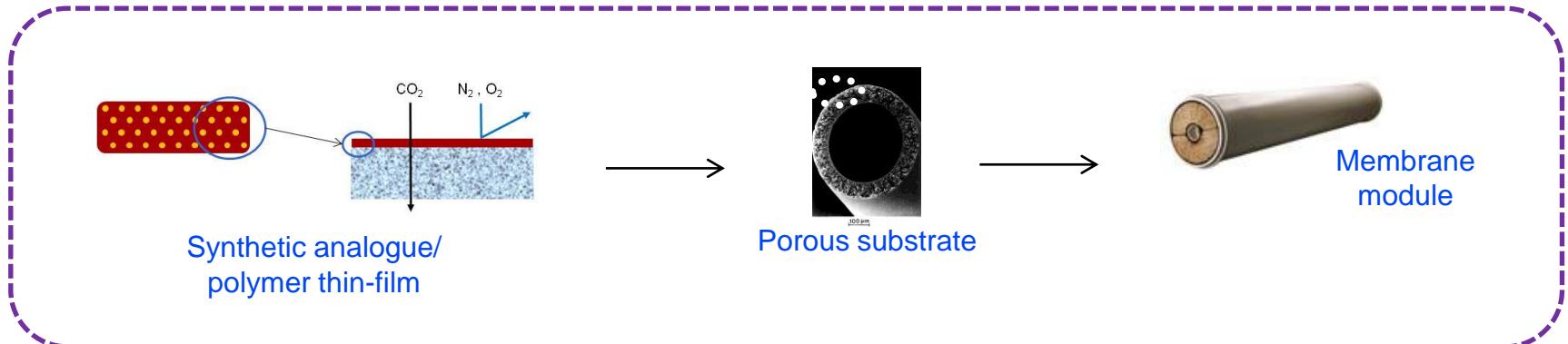
How does a membrane-based separation system compare to current benchmark (liquid amines)?

How do we maintain Zn-OH in tetrahedral coordination within a polymer matrix?

What is the effect of flue gas contaminants?

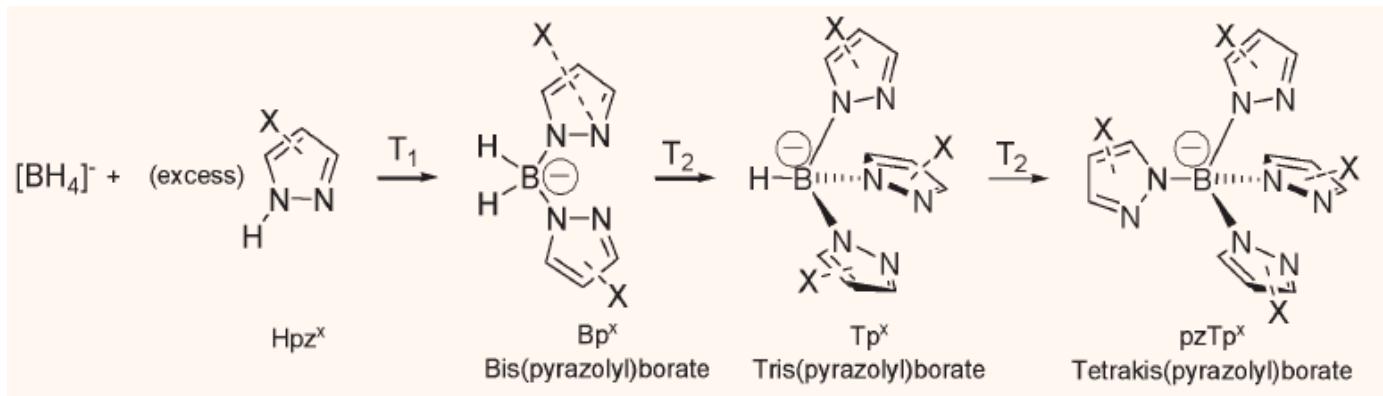
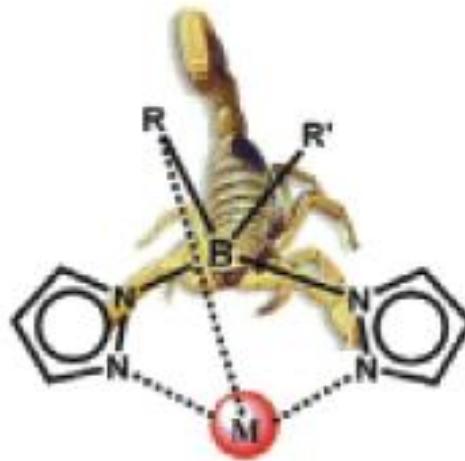
# First Task: Separation System Feasibility Study

*Simulation compares membrane vs. benchmark amine system*



# “Scorpionates” (Poly-Pyrazolyl-Borates)

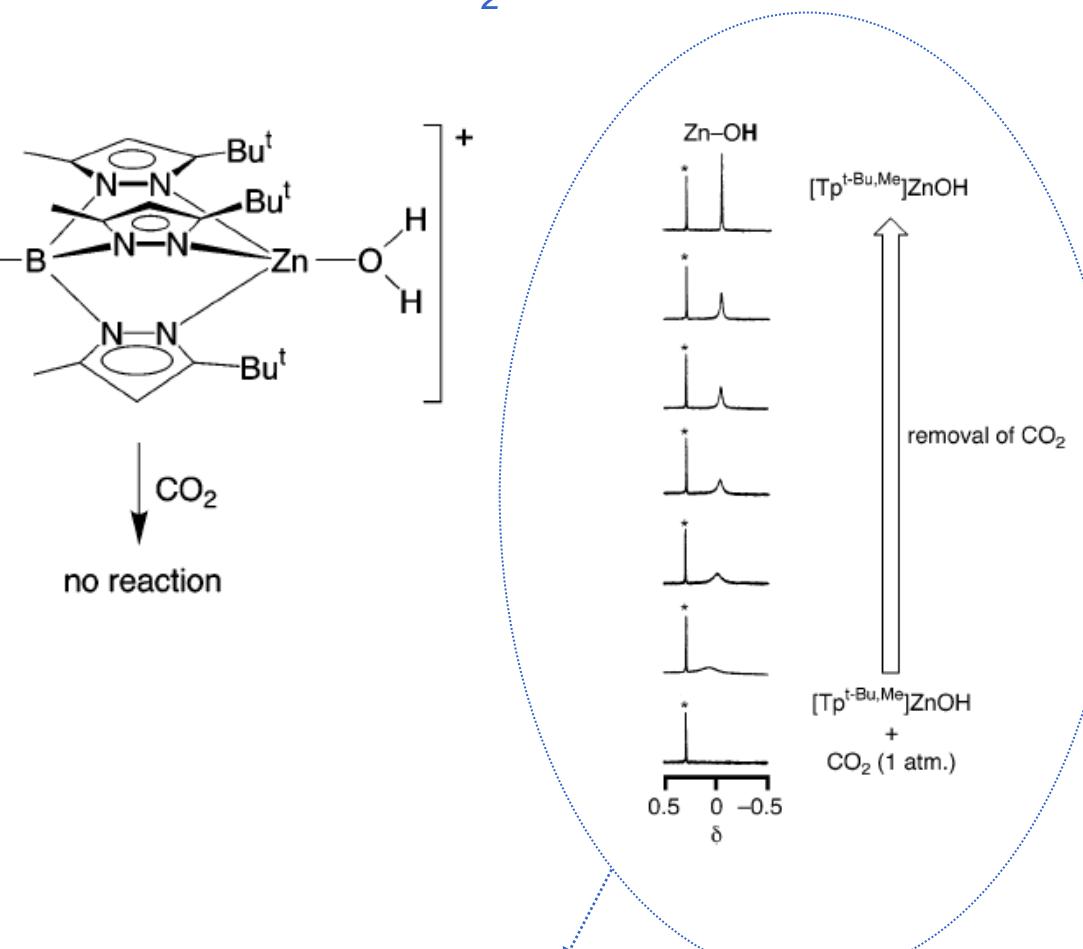
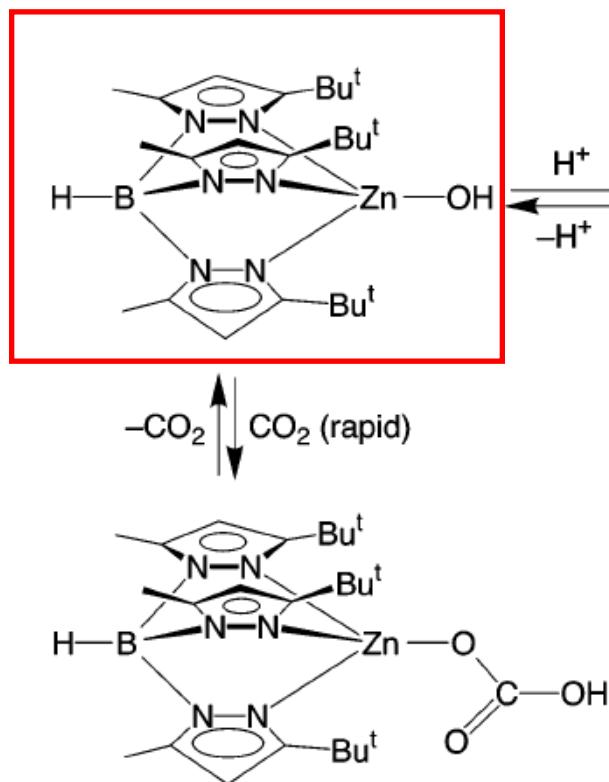
*Modern tripodal ligants “force” metals into tetrahedral coordination*



Trofimenko, S. “Scorpionates: The Coordination Chemistry of Polypyrazolylborate Ligants”, Imperial College Press, London 1999

# $[\text{Tp}^{\text{t-Bu,Me}}]\text{ZnOH}$ : a “Scorpionate” Synthetic Analogue for CA

Demonstrated fast & reversible interaction with  $\text{CO}_2$



G. Parkin, Chem. Rev. 2004, 104, 699-767

Stable molecule;  
Fast reaction in NMR time scale

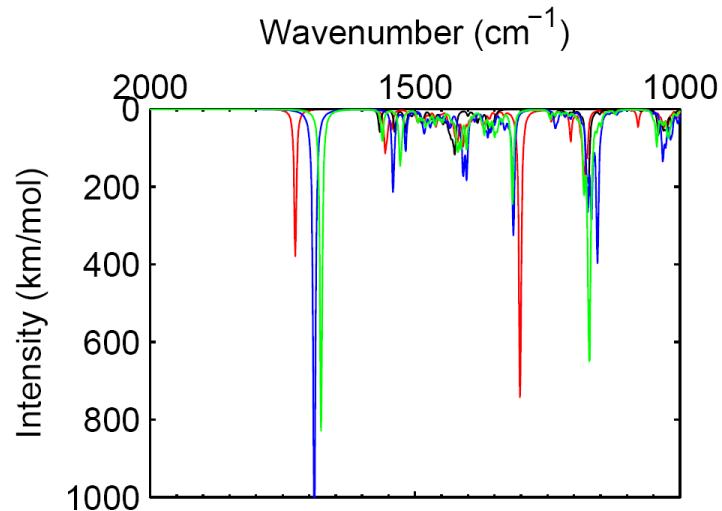
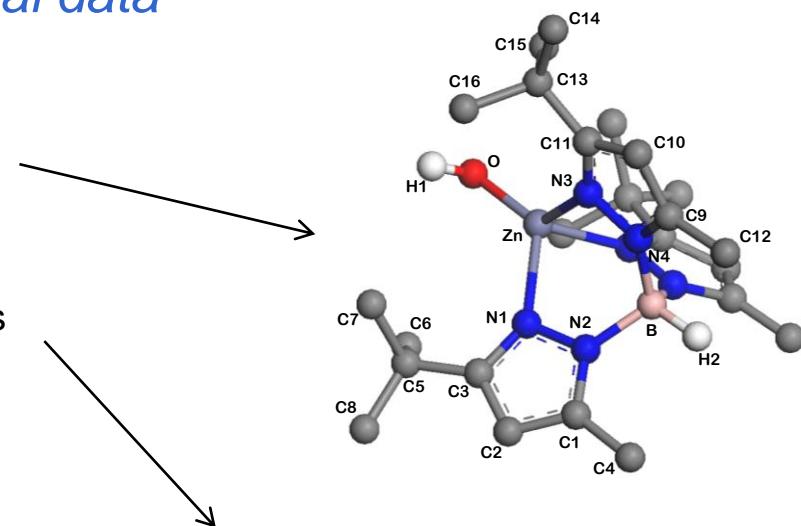
# Synthetic Analogue Structure Analysis via Atomistic Modeling

*DMoL<sup>3</sup> model validated with experimental data*

- Calculated structure predicts bond lengths & angles observed experimentally (XRD)
- Similar IR bicarbonate peaks observed in simulations and experiments
- Reasonable comparison between experimental and calculated analogue NMR

<sup>1</sup>H

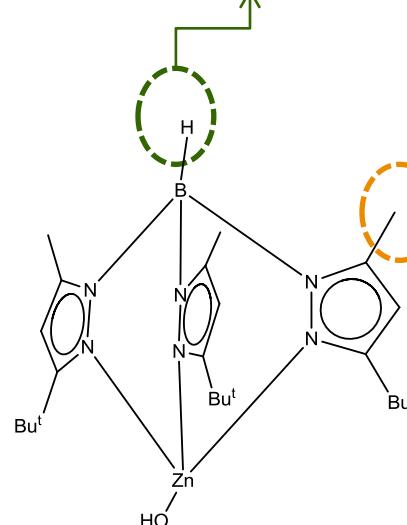
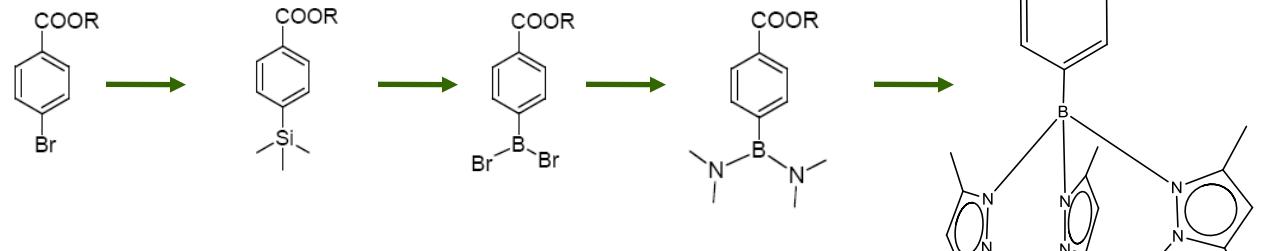
Atom	Vacuum	Chloroform	Benzene	Experimental
H1	-1.0	-0.7	-0.8	-0.3
H2	4.8	4.8	4.8	*
H(C2)	5.8	6.0	5.9	5.7
H(C4)	2.5	2.6	2.6	2.1
H(C6)	1.5	1.4	1.5	1.6



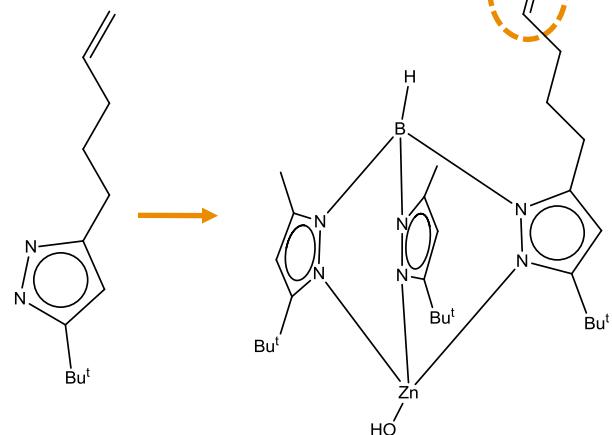
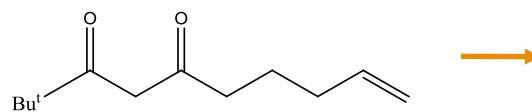
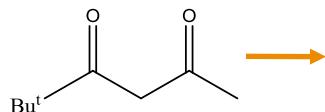
# Synthetic Analogue Modification Example

*Incorporate functional units for grafting or (co)polymerization*

**Path 1:**  
Replace -H with -COOH

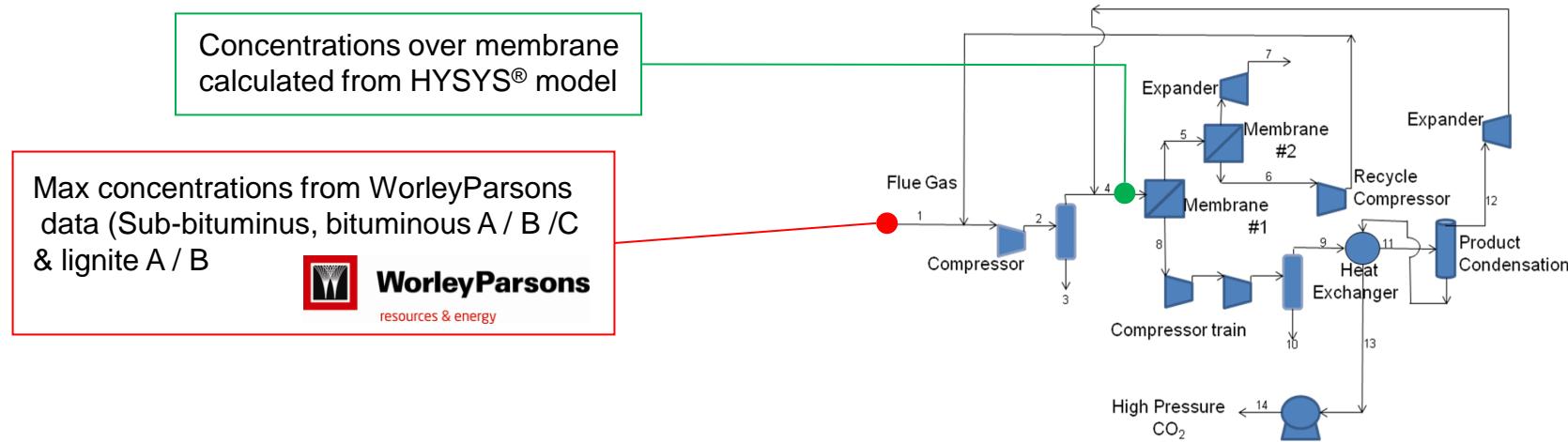


**Path 2:**  
Replace Me with double bond

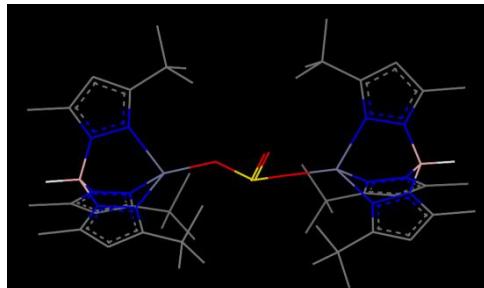


# Resistance to Flue Gas Contaminants

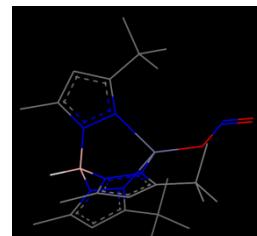
No unrecoverable analogue poisoning (go/no go milestone)



Example possible structures  
(predicted by DMol<sup>3</sup>)



?



	mol %
Water	1.70
Oxygen	2.83
Nitrogen	78.61
Argon	0.94
CO <sub>2</sub>	15.92
HCl	0.00115287
SO <sub>2</sub>	0.00430116
SO <sub>3</sub>	0.00004346
NO <sub>2</sub>	0.00035149
HF	0.00005983

# Program Summary

