

1 Boosting Hydrogenation of CO₂ using Cationic Cu Atomically Dispersed on 2D γ -Al₂O₃**2 Nanosheets**

3 Ping Chen[†], Yifeng Zhu[†], Hailin Zhang[†], Micah P. Prange, Duo Song, Janos Szanyi, Yining Wang, Ying Chen,
4 Xiang Wang, Oliver Y. Gutiérrez, Zihua Zhu, Zheming Wang, Carolyn I. Pearce, Ping Li*, Kevin M. Rosso*,
5 Honghong Shi*, Xin Zhang*

6 Dedication [†] These authors contributed equally to this work.

7 [a] Dr. P. Chen, Dr. Y. Zhu, Dr. H. Zhang, Dr. M. P. Prange, Dr. D. Song, Dr. Y. Wang, Dr. Y. Chen, Dr. X.
8 Wang, Dr. Z. Wang, Dr. C. I. Pearce, Dr. K. M. Rosso and Dr. X. Zhang

9 Physical & Computational Science Directorate

10 Pacific Northwest National Laboratory

11 Richland, Washington 99354, United States

12 Email: xin.zhang@pnnl.gov and kevin.rosso@pnnl.gov

13 Dr. H. Zhang and Prof. P. Li

14 Institute of Process Engineering

15 Chinese Academy of Sciences

16 Beijing 100190, People's Republic of China

17 Email: lipinggnipil@ipe.ac.cn

18 Dr. J. Szanyi, Dr. O.Y. Gutiérrez and Dr. H. Shi

19 Institute of Integrated Catalysis

20 Pacific Northwest National Laboratory

21 Richland, WA 99354, United States

22 Email: crystal.shi@pnnl.gov

23 Dr. Z. Zhu

24 Environmental Molecular Sciences Laboratory

25 Pacific Northwest National Laboratory

26 Richland, Washington 99354, United States

27

28

29

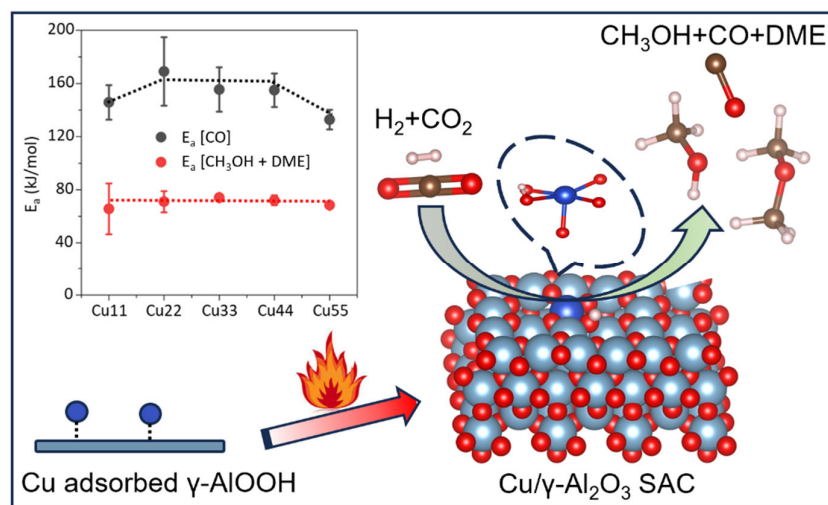
30

31

32

33

34 Graphical Abstract



35
36 A novel 2D single-atom catalyst featuring cationic Cu atomically dispersed on γ -Al₂O₃ nanosheets has been
37 developed, demonstrating exceptional thermal stability and catalytic activity for CO₂ hydrogenation. Compared to
38 traditional Cu/ZnO/Al₂O₃ systems, this catalyst achieves higher methanol (CH₃OH) and dimethyl ether (DME)
39 production rates, driven by the unique substitution of Cu for penta-coordinated Al sites. This innovative design
40 enhances H₂ activation and methanol synthesis, offering new insights into single-atom catalysis for sustainable CO₂
41 utilization.

42

43

44

45

46

47

48

49

50

51

52

53

COMMUNICATION

54 **Abstract:** The continuous development of novel catalytic approaches is crucial for advancing efficient CO₂
55 hydrogenation processes. Drawing inspiration from single-atom catalysis and two-dimensional (2D) materials, we
56 designed a new 2D single-atom catalyst with excellent thermal stability by thermally treating Cu-adsorbed γ -
57 AlOOH nanosheets, which yielded a Cu/ γ -Al₂O₃ catalyst with high activity in the hydrogenation of CO₂ yielding
58 methanol (CH₃OH), dimethyl ether (DME), and CO as products. The active Cu sites are monodispersed and highly
59 stable, due to their cationic oxidation state and their substitution for penta-coordinated aluminum (Al^P) sites on
60 particle surfaces. This study demonstrates an efficient approach for achieving a high CO₂ hydrogenation rate (30.45
61 mol/mol/h) using a catalyst system that lacks metallic Cu centers, traditionally considered essential for H₂
62 dissociation, and employs what was previously thought to be an inert metal oxide (γ -Al₂O₃) for CO and CH₃OH
63 production. Ongoing mechanistic studies aim to elucidate the synergy between cationic Cu single atoms and γ -
64 Al₂O₃, a Lewis acid support, in facilitating hydrogen (H₂) activation and methanol formation.

65 **Keywords:** CO₂ hydrogenation, CO₂ conversion, Cu/ γ -Al₂O₃ catalyst, single atoms, 2D catalyst.

66
67
68 The hydrogenation of CO₂ to methanol ($\text{CO}_2 + 3\text{H}_2 \rightarrow \text{CH}_3\text{OH} + \text{H}_2\text{O}$) is recognized as one of the most effective
69 and economical methods for fixing and utilizing large amounts of emitted CO₂. Optimizing the efficiency of this
70 reaction is an attractive route to sustainability because it converts CO₂, a cheap, nontoxic, and abundant C1
71 feedstock, into high-value-added chemicals and energy fuels as alternatives to petroleum.^[1] At present,
72 commercially recognized benchmark catalysts with the highest CH₃OH selectivity are Cu/ZnO₂/Al₂O₃ or
73 Cu/ZrO₂/Al₂O₃.^[2] In these systems, metallic Cu nanoparticles are typically considered the active sites for H₂
74 activation, while metal oxides such as ZnO₂ and ZrO₂ facilitate strong CO₂ adsorption. Al₂O₃ is generally viewed
75 as an inert support, playing a role in enhancing the physical stability and dispersion of ZnO or ZrO₂ species. The
76 specific role of Cu in these catalysts, whether in its metallic form (Cu⁰) or in cationic states (Cu⁺, Cu²⁺), as the
77 active site for methanol synthesis remains under debate. Previous studies suggest catalytic activity is proportional
78 to the surface area of exposed Cu⁰ produced by reduction prior to the reaction because H₂ dissociation cannot be
79 performed in efficient manner on Cu cations or on the oxide.^[3] In addition, deactivation studies of the
80 Cu/ZnO/Al₂O₃ catalyst >720 h on-stream have shown that deactivation is primarily due to the partial oxidation of

COMMUNICATION

81 Cu^0 to Cu^{2+} and the slight agglomeration of ZnO species during long-term operation,^[4] suggesting that Cu^{2+}
82 contributes reversely to hydrogenation of CO_2 compared with the Cu^0 .

83 Alternatively, other studies highlight the importance of the metal-oxide interface,^[5] suggesting that positively
84 charged Cu species (Cu-O-Zn) at the interface between Cu nanoparticles and the oxide are the true active sites for
85 CO_2 activation/hydrogenation, which favors the formation of methoxy species - the rate-determining step for CO_2 -
86 to- CH_3OH .^[6] In contrast to commercial, complex Cu metal particle systems that feature a mixture of metallic Cu,
87 peripheral copper cations, and Cu-Zn alloys,^[7] the single-atom Cu catalysts supported on a single oxide surface
88 provide a simpler, more uniform system of separated Cu cations.^[1a] They also offer an excellent model system for
89 studying a homogeneous metal-metal oxide interface and are particularly suited to providing fundamental insights
90 into the reaction of CO_2 hydrogenation.^[1a]

91 Considerable evidence suggests that the outstanding performance of single atom catalysts (SACs) stems from
92 a significant alteration in the electronic environment surrounding the central metal.^[8] For instance, the Cu SACs is
93 more efficient than copper clusters or nanoparticles in dissociating hydrogen and activating CO_2 to form HCOO^* ,
94 a key intermediate for CH_3OH synthesis, leading to high selectivity for CH_3OH .^[1a] In fact, the electronic
95 environment around the single atoms is not only determined by the choice of metal-support pair but also by the
96 morphology and homogeneity of the support.^[9] Changing the anchoring site of single atoms from terraces, steps,
97 vacancies, facets, and kinks should result in different surface energy, therefore affecting the catalyst's reactivity.^[10]
98 Doping metals onto the 3D-shaped materials usually results in a mixture of all these sites and the homogeneity of
99 the surface can hardly be realized. For this reason, the concept of 2D-material supported SACs emerged to maintain
100 the uniformity of the surface to the largest extent. These 2D material supports also offer large surface area, ease of
101 surface defect formation, and the possibility of uniformly controlled surface functionalization for tuning the spatial
102 confinement of SACs and the design of active sites on the surface. Although systematic research on 2D materials-
103 derived catalysts is still lacking, there have been reports about the superior catalytic properties of metal doping of
104 these 2D materials, especially in electrochemical or energy storage applications.^[11] So far, most single atom doped
105 low dimensional materials reported in literature use carbon nanomaterials such as 0D fullerene, 1D carbon
106 nanotubes, and graphene substrates.^[12] However, little work has been done on developing 2D-shaped metal oxide-
107 supported SACs. To establish this route, here we report a facile two-step synthesis method to obtain atomically
108 dispersed Cu on $\gamma\text{-Al}_2\text{O}_3$ nanosheets and evaluate its performance for CO_2 hydrogenation. $\gamma\text{-Al}_2\text{O}_3$ was selected as

COMMUNICATION

109 the support due to its high surface area (typically between 50~350 m²/g^[13]), excellent mechanical and thermal
110 stability (with no significant phase transformation below 700 °C^[14]), and its widespread use in industrial catalysts
111 as a structural promoter to enhance the dispersion of active metal or metal oxide species.^[15] The use of Cu-adsorbed
112 γ -AlOOH nanosheets enables controlled deposition of Cu species, promoting the formation of highly dispersed and
113 catalytically active Cu sites on the final γ -Al₂O₃ surface. This structural design aims to optimize catalytic
114 performance by improving both the dispersion and accessibility of the active Cu species.

115 Firstly, boehmite (γ -AlOOH) with a high specific surface area (375 m²/g, Table S1, Supporting Information)
116 and single-layered structure was prepared, which was conducive to improving the adsorption capacity of copper
117 ions. Varying amounts of Cu²⁺ cations were adsorbed onto boehmite particle surfaces via aqueous solution exposure
118 (initial concentration of Cu precursor solution: 0.5 to 10 wt%). Next, the Cu²⁺ adsorbed γ -AlOOH was converted
119 to Cu/ γ -Al₂O₃ by calcination in air at 600 °C. This led to various Cu/ γ -Al₂O₃ catalysts with Cu loading ranging
120 from 0.24 to 0.52 wt% based upon inductively coupled plasma (ICP) analyses. The prepared catalysts were
121 pretreated at 250 °C in 20 vol% H₂/N₂ for 30 minutes prior to catalytic testing. This pretreatment primarily increases
122 the surface concentration of hydrogen species, thereby preparing the surface for the subsequent catalytic reaction.
123 To avoid misinterpretation of the morphology or nature of the active Cu species under reaction conditions—such
124 as potential agglomeration of surface Cu species in H₂ at elevated temperatures—the catalysts (Cu/ γ -Al₂O₃) were
125 subjected to the same pretreatment protocol prior to characterization. After pretreatment, the catalysts were
126 evaluated in CO₂ hydrogenation in a fixed-bed flow reactor at commercial working conditions (250~350 °C and 32
127 bar), producing CO, CH₃OH, and DME as the main products. All the data were collected at CO₂ conversion
128 conditions far away from equilibrium (<5%), with the catalytic reaction being kinetically controlled. Since DME
129 is likely formed from the secondary reaction of CH₃OH dehydration on the Lewis-acid sites of the Al₂O₃ support,^[16]
130 we presented the CH₃OH formation rate on the combined formation rate of CH₃OH and DME, expressed in the
131 form of turn-over-frequency (TOF) with unit of h⁻¹ (Table S2 and Fig. S1, Supporting Information). The catalyst
132 that demonstrated the highest CH₃OH+DME rate was found to have Cu loading as 0.49 wt%; henceforth this sample
133 will be denoted as the Cu/ γ -Al₂O₃ with its precursor before calcination denoted as Cu/ γ -AlOOH and is the subject
134 of detailed characterization in the rest of this paper. The performance of the Cu/ γ -Al₂O₃ in this work is compared
135 with the Cu/ZnO/Al₂O₃ commercial catalyst tested on the same setup (as benchmark), and other reported Cu
136 nanoparticle and SACs from the literature as listed in Table 1. The CH₃OH+DME formation rate (TOF) of the

COMMUNICATION

137 Cu/ γ -Al₂O₃ catalyst developed in this work was found to be approximately one order of magnitude higher than that
 138 of the commercial Cu/ZnO/Al₂O₃ catalyst and three times higher than that of the state-of-the-art Cu₁/ZrO₂ SAC
 139 (CAZ-1). However, the CO selectivity remains significant (~82%), indicating that the reverse water-gas shift
 140 reaction (RWGSR) remains the predominant reaction pathway on the Cu/ γ -Al₂O₃ catalyst. And a detailed summary
 141 of the CO₂ hydrogenation performance of various catalysts has been reported in many references,^[17] which
 142 emphasizes the advantages of our catalyst in terms of performance, synthesis method, and cost.

143
 144 **Table 1.** Catalytic performance of metal oxides supported Cu nanoparticles and single atoms on the hydrogenation
 145 of CO₂

Catalysts	Conditions (T/°C, P/bar)	H ₂ /CO ₂	CO Rate (h ⁻¹)	CH ₃ OH+DME Rate (h ⁻¹)
Cu/ZnO/Al ₂ O ₃ ^{*[18]}	240, 96.5	3	n. a.	0.47
Cu/ZnO/Al ₂ O ₃ ^{*[19]}	240, 20	3	n. a.	0.65
Cu/ZnO/Al ₂ O ₃ [#] (<i>this work</i> ⁺)	250, 32	3	6.90	0.54
CAZ-1(Cu ₁ /ZrO ₂) ^{#[1a]}	180, 30	3	~ 0	1.4
Cu ₁ /ZnO ^{#[20]}	170, 30	3	0.014	0.16
Cu/ γ -Al ₂ O ₃ [#] (<i>this study</i> ⁺)	170, 32	3	0	0.25
	250, 32	3	25.10	5.35

146 “*” refers to Cu nanoparticle. “#” refers to Cu single atoms. “n. a.” refers to not available. “+” Reaction conditions:
 147 250 °C, 32 bar, CO₂/H₂/N₂ = 7/21/1 mL/min; the commercial Cu/ZnO/Al₂O₃ used as reference in this work are
 148 Johnson Matthey (JM) KATALCO 51 series.
 149

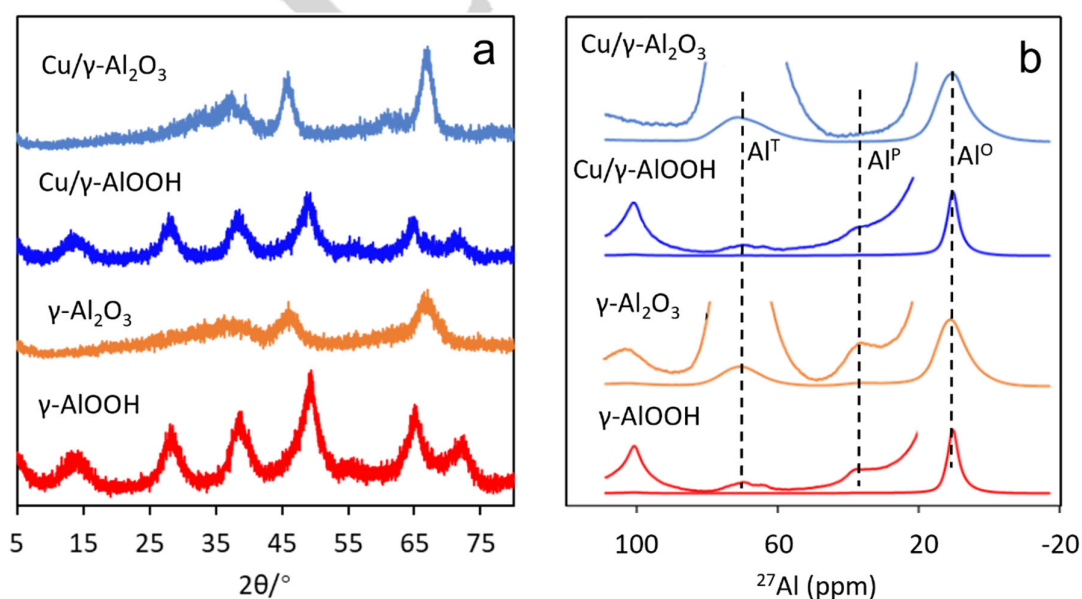
150 Powder X-ray diffraction (XRD) patterns (Fig. 1a) indicated that the synthesized γ -AlOOH precursor substrate
 151 exhibits peaks consistent with the boehmite phase, aligning well with the γ -AlOOH reference (JCPDS 21-1307).
 152 The broadening of the (002) peak suggests a low degree of crystallinity. After calcination, the pattern aligns with
 153 the γ -Al₂O₃ phase (JCPDS 00-010-0425), showing prominent peaks at 37.6°, 45.9°, and 67.0° corresponding to the
 154 (311), (400), and (440) planes. The crystal structure of γ -AlOOH remains unchanged upon copper adsorption (Cu/ γ -
 155 AlOOH), and the thermal transformation products (Cu/ γ -Al₂O₃) mirror those of pure γ -Al₂O₃, with no distinct Cu-
 156 related peaks observed. The BET results (Table S1, Supporting Information) indicate that the specific surface area
 157 of γ -AlOOH showed little change before and after Cu adsorption (from 349 to 332 m²/g). However, compared to
 158 the significant reduction in specific surface area after thermal calcination of the original γ -AlOOH (from 349 to
 159 185 m²/g), the specific surface area of Cu/ γ -AlOOH did not decrease significantly after heat treatment (from 332
 160 to 282 m²/g). This suggests that the surface-adsorbed Cu may undergo structural changes during the heat treatment

COMMUNICATION

161 process. This change helps mitigate the reduction in specific surface area, thereby facilitating the preparation of
 162 catalysts with high specific surface areas.

163 In ^{27}Al magic-angle spinning nuclear magnetic resonance (MAS NMR) spectra of $\gamma\text{-AlOOH}$ and $\gamma\text{-Al}_2\text{O}_3$
 164 samples (Fig. 1b), a major peak was located at about 10.8 ppm, and two low-intensity peaks located at 36.6 ppm
 165 and 70.1 ppm were observed. These peaks are assigned to octahedral aluminum coordination (Al^{O}) (10.8 ppm),
 166 pentahedral aluminum coordination (Al^{P}) (36.6 ppm), and tetrahedral aluminum coordination (Al^{T}) (70.1 ppm),^[21]
 167 respectively. Both Al^{P} and Al^{T} in $\gamma\text{-AlOOH}$, as well as Al^{P} in $\gamma\text{-Al}_2\text{O}_3$ represent structural incompleteness in the
 168 form of defects.^[21b, 22] The ratio (mol%) of Al^{O} , Al^{P} , and Al^{T} are quantified and listed in the Table S3, Supporting
 169 Information. Compared to the $\gamma\text{-AlOOH}$, the proportion of Al^{O} site decreased from 99.1% to 76.4%, while the Al^{T}
 170 sites increased from 0.4% to 22.9% in the $\gamma\text{-Al}_2\text{O}_3$, indicating a lattice structure transformation from Al^{O} to Al^{T} .^[23]
 171 It can be concluded that Cu adsorption does not affect the Al sites on the AlOOH significantly. However, as
 172 observed by comparing to the $\gamma\text{-Al}_2\text{O}_3$ sample, $\text{Cu}/\gamma\text{-Al}_2\text{O}_3$ catalyst showed a significantly decreased ratio of Al^{O}
 173 (from 76.4% to 70.5%) and Al^{P} (from 0.7% to 0.1%). Correspondingly, the ratio of Al^{T} sites increased from 22.9%
 174 to 29.4% in the Cu doped $\gamma\text{-Al}_2\text{O}_3$ sample. These changes suggest that thermal treatment at 600°C plays a crucial
 175 role in anchoring Cu atoms and modifying the surface Al species, where Cu atoms likely replaced the Al^{O} and/or
 176 Al^{P} sites.

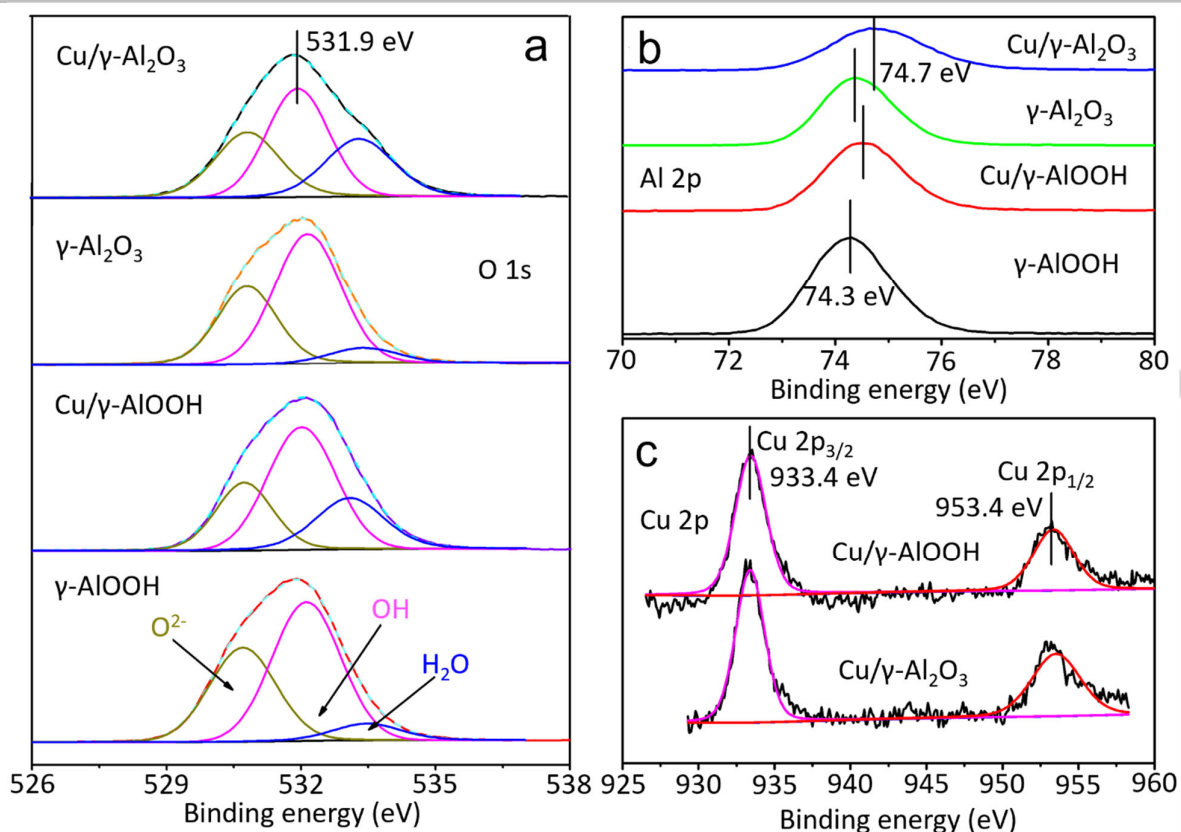
177



178
 179 **Fig. 1.** XRD patterns (a), and ^{27}Al MAS NMR spectra (b) of 2D $\gamma\text{-AlOOH}$, $\gamma\text{-Al}_2\text{O}_3$, $\text{Cu}/\gamma\text{-AlOOH}$, and $\text{Cu}/\gamma\text{-Al}_2\text{O}_3$

COMMUNICATION

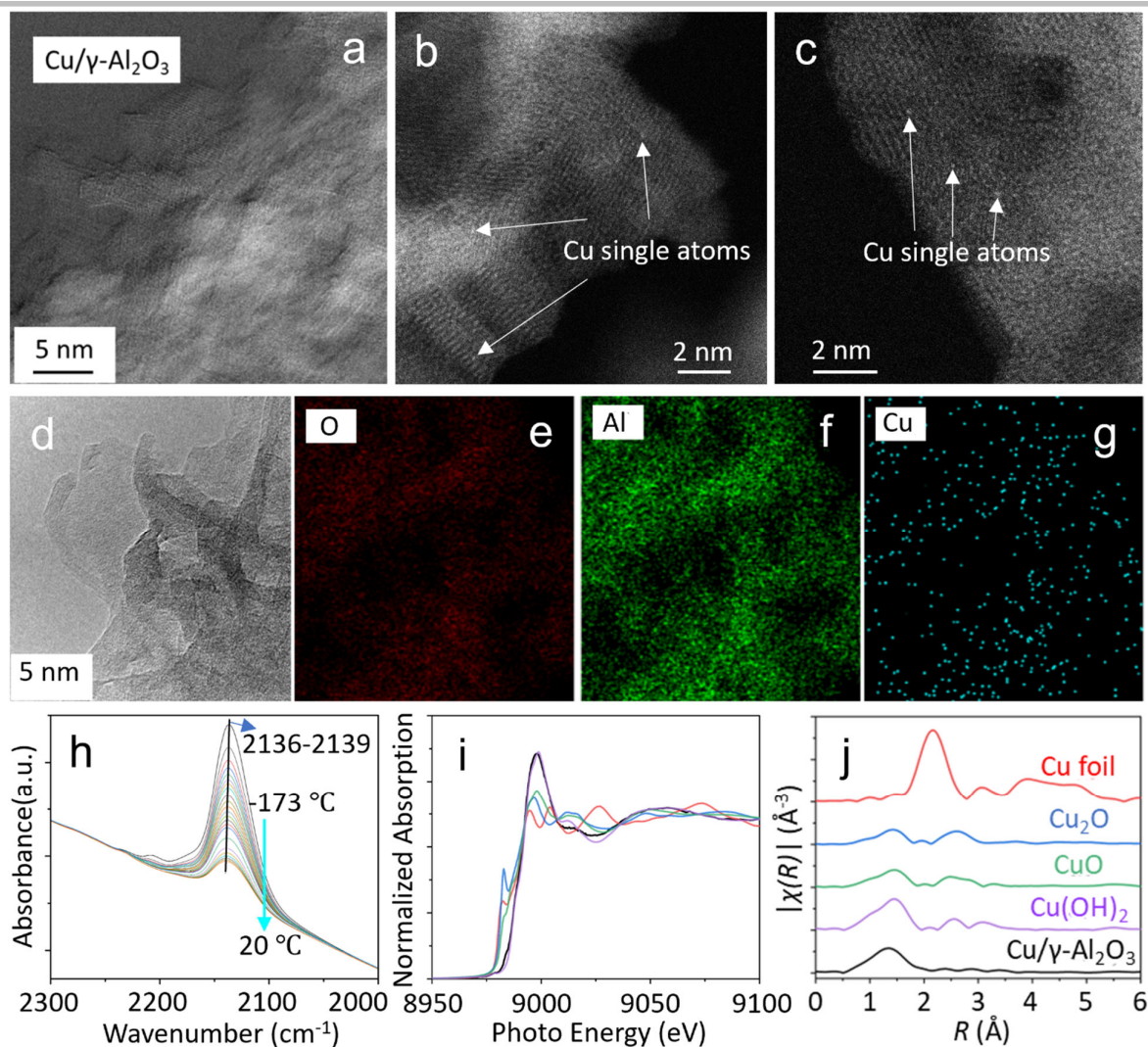
180 X-ray photoelectron spectroscopy (XPS) is widely used for studies of surface chemistry, offering a range of
181 useful information on depths, reasonable quantification, and chemically specific details for each detected element
182 through chemical shifts. The O 1s peaks (Fig. 2a, Table S4, Supporting Information) are composed of subpeaks
183 with peak energy ~ 530.7 eV, ~ 532.1 eV and 533.3 eV which can be designated as surface O^{2-} , -OH group and -
184 H_2O group,^[24] respectively. The most noticeable change is the sharp increase in the amount of adsorbed water on
185 samples containing Cu, indicating that copper enhances the surface activity. The binding energy of Al 2p (Fig. 2b)
186 shifted slightly from 74.3 to 74.7 eV^[25] and the peak shape was also affected due to the addition of Cu. This
187 indicates the coordination environment for Al atoms has been changed after the introduction of surface Cu species,
188 although the dominating chemical state of Al atoms in the Cu doped γ -AlOOH and γ -Al₂O₃ is still Al³⁺. The Cu 2p
189 spectrum (Fig. 2c) of Cu/ γ -AlOOH could be resolved to two peaks at 933.4 eV, and 953.4 eV, corresponding to
190 Cu²⁺ indicating that copper has been adsorbed onto the surface.^[26] And Cu 2p spectrum of Cu/ γ -Al₂O₃ was also
191 deconvoluted into two peaks at different binding energies of 933.4 eV and 953.4 eV, indicating that Cu²⁺ species
192 were not reduced, with no presence of Cu⁰ or Cu⁺ species on the catalyst.^[27] In addition, the nature of Cu²⁺ cannot
193 be classified as Cu(OH)₂, as evidenced by the absence of the two satellite peaks at 942.19 eV and 962.45 eV.^[28]
194



195
 196 **Fig. 2.** XPS spectra (a, O 1s. b, Al 2p. c, Cu 2p) of 2D γ -AlOOH, γ -Al₂O₃, Cu/ γ -AlOOH, and Cu/ γ -Al₂O₃
 197
 198 Transmission electron microscopy (TEM) images (Fig. S2a-b, Supporting Information) reveal that both γ -
 199 AlOOH and γ -Al₂O₃ exhibit thin sheet-like morphology with particle sizes ranging from 1 to 3 nm, and the addition
 200 of copper does not significantly alter these characteristics (Fig. 3a, and Fig. S2c, Supporting Information). Scanning
 201 transmission electron microscopy (STEM) of the Cu/ γ -Al₂O₃ in Fig. 3b, c and the Energy Dispersive X-ray (EDS)
 202 elemental mapping results in Fig. 3d-g demonstrated that a uniform distribution of Cu atoms across particle surfaces
 203 is maintained after thermal transformation. Consistent with this picture, in our time-of-flight secondary ion mass
 204 spectrometry (ToF-SIMS) observations (Fig. S3, Supporting Information), neither Cu/ γ -AlOOH nor Cu/ γ -Al₂O₃
 205 show a significant concentration of CuOCu⁺ species; instead, Cu exists primarily as CuOAl⁺ and Cu⁺, indicating
 206 that copper is predominantly in the form of single atoms. However, in Cu/ γ -Al₂O₃, the CuOAl⁺/Cu⁺ ratio changes
 207 significantly compared to Cu/AlOOH, increasing from the original 36.7% to 149.6%. This suggests that after the
 208 thermal phase transition from Cu/ γ -AlOOH to Cu/ γ -Al₂O₃, the coordination environment of Cu undergoes a
 209 fundamental transformation, shifting from an adsorbed state to a structurally steady state, which results in a much

COMMUNICATION

210 higher CuOAl⁺/Cu⁺ ratio. To further confirm the nature of surface Cu species and examine the atomic dispersion
211 of Cu atoms in the studied catalyst, IR spectroscopy of CO adsorption on Cu/ γ -Al₂O₃ was collected with results
212 shown in Fig. 3h and Fig. S4, Supporting Information. From the collected spectra, we didn't observe peaks
213 corresponding to *CO adsorbed on metallic Cu (Cu⁰), which typically shows peaks in the range of 2040~2120 cm⁻¹,
214 originating from the π -backdonation from Cu to the CO anti-bonding orbital. In the CO adsorption region, two
215 bands at ~2160 cm⁻¹ and ~2190 cm⁻¹ originated from the CO adsorption on the γ -Al₂O₃ support: the band at ~2190
216 cm⁻¹ is assigned to CO adsorbed on surface Lewis acid sites (Al³⁺), while the ~2160 cm⁻¹ band corresponds to CO
217 hydrogen-bonded to Al-OH groups.^[29] (Fig. S4, Supporting Information warming up from liquid N₂ temperature
218 to room temperature after CO adsorption). Both Cu⁺ and Cu⁰ sites form carbonyls that, when copper is highly
219 dispersed, show CO bands at similar frequency (~2136 cm⁻¹) as Cu⁺-CO or Cu⁰-CO carbonyls. However, the two
220 species can be distinguished by their stability: Cu⁰-CO species are easily decomposed during evacuation, whereas
221 CO remains strongly adsorbed on Cu⁺ sites.^[30] In this work, only a significant peak at 2136 cm⁻¹ was observed after
222 evacuation (Fig. 3h), corresponding to strong chemisorption of CO* adsorbed on the top of Cu cations (Cu⁺).
223 Notably, the absence of CO adsorption bands associated with Cu⁰ nanoparticles (2040-2120 cm⁻¹) confirms the
224 exclusive presence of cationic Cu species in our catalyst system. This observation provides direct spectroscopic
225 evidence for the unique metal-support interactions in our Cu/ γ -Al₂O₃ SAC, where the γ -Al₂O₃ nanosheets play a
226 crucial role in stabilizing the highly dispersed Cu atoms.
227



228

229 **Fig. 3.** (a) TEM image of Cu/γ-Al₂O₃. (b-d) HAADF-STEM image of Cu/γ-Al₂O₃. (e-g) STEM-EDS elemental
 230 mapping images Cu/γ-Al₂O₃. (h) FTIR spectra of evacuation on Cu/γ-Al₂O₃ at room temperature after CO
 231 adsorption at -173 °C (Fig. S4a) and heating to 9 °C (Fig. S4b). (i-j) Cu K-edge XANES spectra and Cu K-edge
 232 EXAFS spectra of Cu/γ-Al₂O₃, and Cu standards (Cu foil, Cu₂O, CuO, and Cu(OH)₂); fitting and wavelet transform
 233 analysis results are shown in the Supporting Information.
 234

235 Fig. 3i shows normalized Cu K-edge XANES spectra for the H₂ pretreated Cu/γ-Al₂O₃ sample and the different
 236 copper standard compounds. The pre-edge feature of Cu originates from the transition to spatially localized 3d
 237 states, and the shape of the pre-edge depends on the number of electrons in the d-shell and its intensity is
 238 proportional to the amount of 3d-4p hybridization.^[31] The sharp shoulder on the rising edge for Cu is known as
 239 indicative of a linear or square planar geometry with a lower energy of empty 4p orbitals perpendicular to the
 240 chemical bonds. This shoulder appears in the spectra of Cu₂O (linear, 2-coordinated) or CuO (planar, 4-coordinated)
 241 standards as expected (Fig. 3i), but not in the Cu/γ-Al₂O₃ sample. In addition, the absorption edge position, and the

COMMUNICATION

242 intensity of Cu/ γ -Al₂O₃ sample's white line are at nearly the same level of the Cu(OH)₂. Therefore, we can infer
243 that the Cu has coordination environment similar to Cu(OH)₂ that has the oxidation state around 2+, and a
244 pentahedral coordination with oxygen.

245 The Fourier Transforms (FTs) of the EXAFS (Extended X-ray Absorption Fine Structure) for the analyzed
246 Cu/ γ -Al₂O₃ catalyst and reference samples are presented in Fig. 3j, uncorrected for the phase change. It is apparent
247 that the Cu-O coordination is the dominant coordination environment in the first shell. Uniting these
248 characterization results we obtained from the XPS, Al-NMR, TOF-SIMS and XAS analysis of the H₂-pretreated
249 Cu/ γ -Al₂O₃, we arrive at a geometry model that the surface copper species replaced Al atoms at the pentahedral
250 sites on the surface (Al^P) for EXAFS fitting and this was supported by our DFT optimization results (Fig. 4a, b,
251 Table S6, Supporting Information). Further details regarding this fitting are available in the Fig. S5-S6 and Table
252 S5, Supporting Information. The attempts to replace Al^T or Al^O with Cu cations did not yield successful EXAFS
253 fitting results. Consequently, the data was fitted up to 3.4 Å at a satisfactory level and the results proved our
254 hypothesis on the surface structure. The fitting results revealed strong evidence that Cu atoms replaced the Al^P sites
255 that demonstrated a nearly 5-coordinated structure with Cu-O bond lengths of 2.0 Å (coordination number (CN) of
256 Cu-O: 3.3 ± 0.8 and Cu-O bond lengths of 2.3 Å (CN of Cu-O: 0.8 ± 0.2), respectively. There is one Cu-O bond
257 length longer than the other four Cu-O bonds, indicating the partial hydroxylation of the Cu site forming Cu-OH
258 after hydrogen pretreatment. Additionally, the Cu-O bond distance is slightly longer than the Al^T-O bond (~1.8
259 Å), and we observed the presence of Cu-O-Al at 2.8 Å with a CN of ~4. This value was derived from either the
260 Cu-O-Al^O distance or the Cu-O-Al^P distance. The Cu-O-O triangular path and Cu-Al^T path were also found in the
261 fitting of the higher shells.

262 To understand relationships between the atomic and electronic structure of these sites, we performed electronic
263 structure calculations using density functional theory (DFT). The projected density of states (PDOS) results (Fig.
264 4c) from our DFT calculations indicates that in the undoped γ -Al₂O₃, the Al-O bonds exhibit covalent
265 characteristics due to the strong overlap of O p orbitals with Al s and p orbitals. However, near the Fermi level
266 (around 0 eV), the density of states for O remains relatively high, while the contribution from Al is smaller. This
267 suggests a noticeable ionic character in Al-O bonds. Therefore, O-Al bonds in γ -Al₂O₃ are better described as ionic-
268 covalent rather than purely ionic.^[29a, 32] After Cu doping, the Cu d orbitals show significant contributions near the
269 Fermi level, but there is minimal overlap with the density of states of O22 and O23, suggesting limited electron

COMMUNICATION

270 sharing between Cu and O. This observation supports the conclusion that the Cu-O bond has a more ionic character.

271 The electron density difference in Fig. 4d shows that in undoped γ -Al₂O₃, there is a noticeable accumulation of
272 electron density along the Al-O bond direction. This accumulation indicates electron sharing between Al and O.

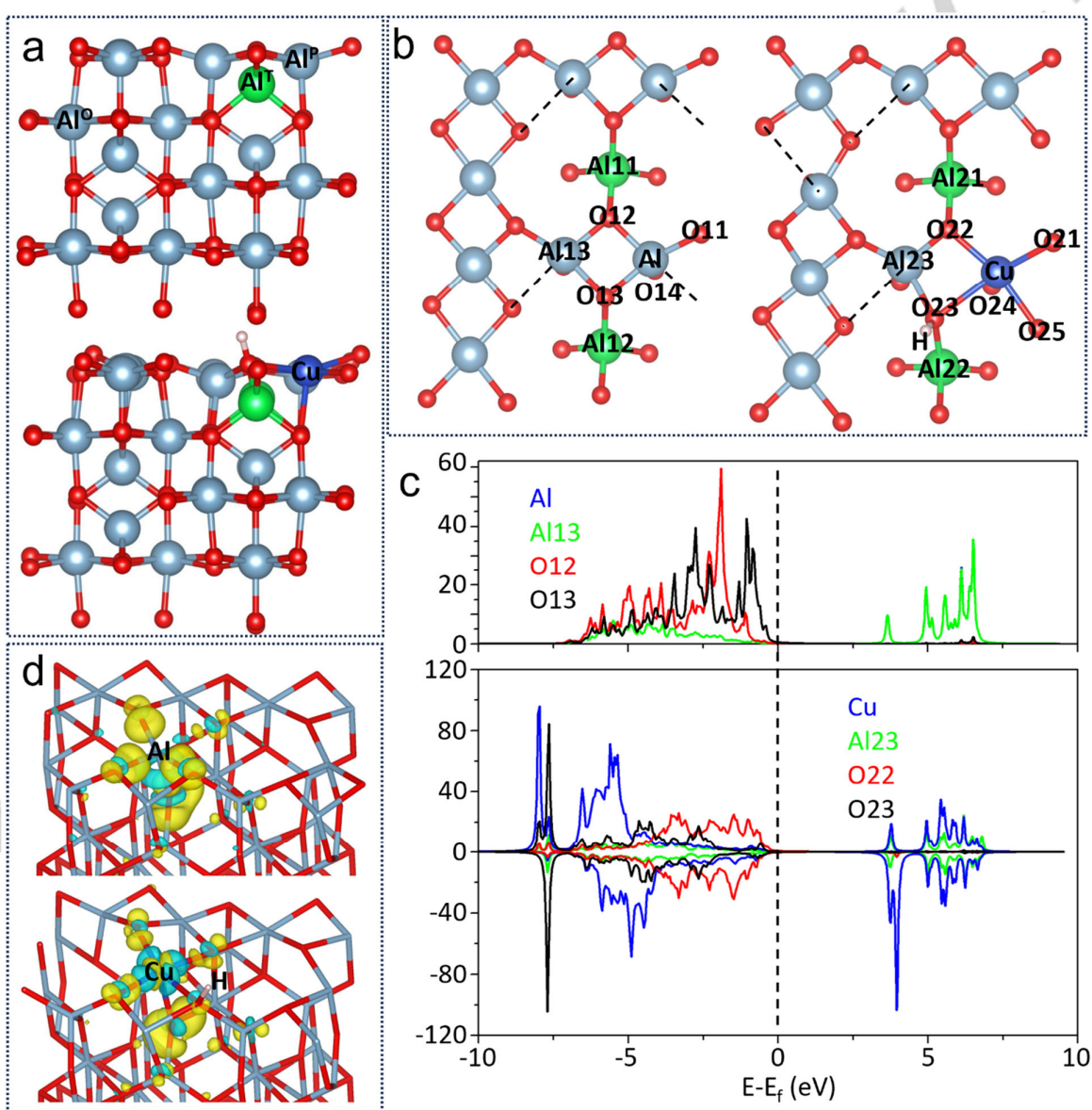
273 After Cu replaces Al, the electron density around Cu decreases (cyan regions), indicating electron transfer away

274 from Cu. This strengthens the ionic character of the Cu-O bond while weakening the covalent nature of the Al-O

275 bonds. This electron redistribution indicates that the unoccupied 4s and 3d orbital of Cu on the surface could act as

276 Lewis acid sites, exhibiting a stronger electron affinity and resulting in greater Lewis's acidity compared to Al.^[33]

277



278

COMMUNICATION

279 **Fig. 4.** Optimized γ -Al₂O₃ (100) surface and Cu-doped (100) surface (a, side view; b, top view), DOS projected
280 onto Al and O p orbitals and Cu d orbitals (c), and charge density differences as described in the text (d, cyan area:
281 losing electron; yellow area: gaining electron; isosurfaces drawn at +/- 0.01 a.u.).
282

283 To summarize the collective findings for the analyzed Cu/ γ -Al₂O₃ catalyst, no CuOCu⁺ peak is discernible from
284 the ToF-SIMS results, confirming the atomic-level dispersion as we observed in the S/TEM characterization, CO-
285 IR and XAS analysis. We conclude that the Cu/ γ -Al₂O₃ sample has pentahedral- and hydroxylated- Cu atoms doped
286 on the γ -Al₂O₃ surface atomically (single-atom catalyst). Additionally, the ToF-SIMS results (Fig. S3) showed that
287 the relative contents of CuOAl⁺/Cu⁺, and CuOCu⁺/Cu⁺ in the post-reaction catalyst did not change significantly,
288 indicating that its structure remains relatively stable with no formation of Cu clusters. This confirms our initial
289 hypothesis that a highly efficient stable 2D single-atom Cu catalyst could be developed through a simple thermal
290 treatment of Cu-adsorbed γ -AlOOH nanosheets. The core information we revealed in this work are: (1) Cu single
291 atoms substituting for Al^P sites on γ -Al₂O₃ exhibits high CO₂ hydrogenation activity, with 17.5% selectivity
292 towards CH₃OH. (2) the maximum capacity of anchoring single atoms on the alumina substrate is largely dependent
293 on the density of surface defects; optimizing the synthesis of γ -Al₂O₃ to increase Al^P defect density could thus be
294 a means to enhance Cu loading and catalytic activity even further.

295 Given that our catalyst lacks metallic Cu⁰ sites, it is important to further investigate the mechanism of H₂
296 activation. Recent work by N. Zheng et al. demonstrated that penta-coordinated Al³⁺-enriched amorphous Al₂O₃
297 facilitates the heterolytic activation of H₂,^[34] enabling the hydrogenation of substrates containing C=C and C=O
298 bonds. This defect-rich Al₂O₃ acts as a heterogeneous frustrated Lewis pair (FLP), capable of H₂ activation in the
299 absence of any transition metal species. Therefore, it remains to be determined whether similar heterolytic H₂
300 dissociation occurs on our cationic Cu SAC, forming O-H^{δ+} and Cu-H^{δ-} species as the initiation of hydrogenation.
301 In addition, activation of CO₂ molecule is also an important prerequisite. CO₂ molecules are known to be weakly
302 adsorbed on the γ -Al₂O₃ (110) surface with an E_{ads} = 0.45 eV and nearly linear configuration (\angle O-C-O = 176.5°),^[35]
303 and also interact with Cu⁰ weakly.^[36] We observed from the charge density analysis that Cu sites are significantly
304 electron deficient compared to Al cations, therefore the Cu-O-Al site is hypothesized to bend the adsorbed CO₂
305 molecule, thereby making it prone to receive electrons from surface H^{δ-}. Further investigations, including ²H-NMR
306 spectroscopy, chemisorption studies, and operando infrared experiments, coupled with DFT calculations are under-
307 way to elucidate the full hydrogenation mechanism in the reported Cu single atom catalyst.

308
309
310 **Acknowledgements**

311 This work is supported by the U.S. Department of Energy (DOE), Office of Science, Office of Basic Energy
312 Sciences, Division of Chemical Sciences, Geosciences and Biosciences through the Geosciences Program (FWP#
313 56674) and the Program of “Transdisciplinary Approaches to Realize Novel Catalytic Pathways to Energy Carriers”
314 (FWP 47319) at Pacific Northwest National Laboratory (PNNL). P. Chen, C. I. Pearce, and X. Zhang also
315 acknowledge the funding support from the Ion Dynamics in Radioactive Environments and Materials (IDREAM)
316 program, an Energy Frontier Research Center funded by the U.S. Department of Energy, Office of Science, Basic
317 Energy Sciences (FWP 68932). PNNL is operated for DOE by Battelle Memorial Institute under Contract DE-
318 AC05-76RL01830. Part of the research was performed with a user proposal #61223 (Award DOI:
319 10.46936/lser.proj.2024.61223/60012698) and 51922 (Award DOI: 10.46936/lser.proj.2021.51922/60000373) at
320 the William R. Wiley Environmental Molecular Sciences Laboratory (EMSL), a national scientific user facility
321 sponsored by the U.S. DOE’s Office of Biological and Environmental Research and located at PNNL in Richland,
322 WA. This research used the beamline 20-BM of the Advanced Photon Source, a U.S. Department of Energy (DOE)
323 Office of Science user facility at Argonne National Laboratory and is based on research supported by the U.S. DOE
324 Office of Science-Basic Energy Sciences, under Contract No. DE-AC02-06CH11357. We would like to
325 acknowledge Libor Kovarik for his valuable efforts in acquiring the HAADF-STEM images.

326 **Conflict of Interest**

327 The authors declare no conflict of interest.

328 **Data Availability Statement**

329 The data that support the findings of this study are available in the Supporting Information.

330 **Keywords:** 2D catalyst • Single-Atom Catalysis • Cu/ γ -Al₂O₃ • CO₂ Hydrogenation • Methanol

331 **References:**

- 332 [1] a) H. Zhao, R. Yu, S. Ma, K. Xu, Y. Chen, K. Jiang, Y. Fang, C. Zhu, X. Liu, Y. Tang, L. Wu, Y. Wu, Q. Jiang, P. He, Z. Liu, L. Tan, *Nat. Catal.* **2022**,
333 5, 818-831; b) R. P. Ye, J. Ding, W. Gong, M. D. Argyle, Q. Zhong, Y. Wang, C. K. Russell, Z. Xu, A. G. Russel, Q. Li, M. Fan, Y. G. Yao, *Nat.*
334 *Commun.* **2019**, 10, 5698; c) S. W. Lee, M. L. Luna, N. Berdunov, W. Wan, S. Kunze, S. Shaikhutdinov, B. R. Cuenya, *Nat. Commun.* **2023**, 14, 4649.

- [2] a) S. Kattel, P. J. Ramirez, J. G. Chen, J. A. Rodriguez, P. Liu, *Science* **2017**, *355*, 1296-1299; b) X. Dong, F. Li, N. Zhao, F. Xiao, J. Wang, Y. Tan, *Appl. Catal. B* **2016**, *191*, 8-17; c) T. Yang, X. Mao, Y. Zhang, X. Wu, L. Wang, M. Chu, C. W. Pao, S. Yang, Y. Xu, X. Huang, *Nat. Commun.* **2021**, *12*, 6022; d) Y. Wang, S. Kattel, W. Gao, K. Li, P. Liu, J. G. Chen, H. Wang, *Nat. Commun.* **2019**, *10*, 1166; e) P. Gao, F. Li, H. Zhan, N. Zhao, F. Xiao, W. Wei, L. Zhong, H. Wang, Y. Sun, *J. Catal.* **2013**, *298*, 51-60; f) O. Martin, C. Mondelli, D. Curulla-Ferré, C. Drouilly, R. Hauert, J. Pérez-Ramírez, *ACS Catal.* **2015**, *5*, 5607-5616; g) M. Bukhtiyarova, T. Lunkenbein, K. Kähler, R. Schlögl, *Catal. Lett.* **2017**, *147*, 416-427.
- [3] a) K. C. Waugh, *Catal. Today* **1992**, *15*, 51-75; b) T. Tagawab, G. Pleizier, Y. Amenomiya, *Appl. Catal.* **1985**, *18*, 285-293; c) G. J. Millar, C. H. Rochester, S. Bailey, K. C. Waugh, *J. Chem. Soc., Faraday Trans.* **1992**, *88*, 2085-2093.
- [4] B. Liang, J. Ma, X. Su, C. Yang, H. Duan, H. Zhou, S. Deng, L. Li, Y. Huang, *Ind. Eng. Chem. Res.* **2019**, *58*, 9030-9037.
- [5] a) E. Lam, J. J. Corral - Pérez, K. Larmier, G. Noh, P. Wolf, A. Comas - Vives, A. Urakawa, C. Copéret, *Angew. Chem. Int. Ed.* **2019**, *58*, 13989-13996; b) K. Samson, M. Sliwa, R. P. Socha, K. Góra-Marek, D. Mucha, D. Rutkowska-Zbik, J. Paul, M. Ruggiero-Mikołajczyk, R. Grabowski, J. Słoczynski, *ACS Catal.* **2014**, *4*, 3730-3741; c) A. Le Valant, C. Comminges, C. Tisseraud, C. Canaff, L. Pinard, Y. Pouilloux, *J. Catal.* **2015**, *324*, 41-49; d) S. Kattel, P. Liu, J. G. Chen, *J. Am. Chem. Soc.* **2017**, *139*, 9739-9754.
- [6] a) A. Gau, J. Hack, N. Maeda, D. M. Meier, *Energ. fuel.* **2021**, *35*, 15243-15246; b) Y. Zhu, J. Zheng, J. Ye, Y. Cui, K. Koh, L. Kovarik, D. M. Camaioni, J. L. Fulton, D. G. Truhlar, M. Neurock, C. J. Cramer, O. Y. Gutiérrez, J. A. Lercher, *Nat. Commun.* **2020**, *11*, 5849.
- [7] E. Frei, A. Gaur, H. Lichtenberg, L. Zwiener, M. Scherzer, F. Girgsdies, T. Lunkenbein, R. Schlögl, *ChemCatChem* **2020**, *12*, 4029-4033.
- [8] a) Y. Wang, H. Su, Y. He, L. Li, S. Zhu, H. Shen, P. Xie, X. Fu, G. Zhou, C. Feng, D. Zhao, F. Xiao, X. Zhu, Y. Zeng, M. Shao, S. Chen, G. Wu, J. Zeng, C. Wang, *Chem. Rev.* **2020**, *120*, 12217-12314; b) Y. Wang, D. Wang, Y. Li, *Adv. Mater.* **2021**, *33*, 2008151; c) Y. Zhao, W. J. Jiang, J. Zhang, E. C. Lovell, R. Amal, Z. Han, X. Lu, *Adv. Mater.* **2021**, *33*, 2102801.
- [9] a) J. Liu, *ACS Catal.* **2017**, *7*, 34-59; b) Y. Shi, Y. Zhou, Y. Lou, Z. Chen, H. Xiong, Y. Zhu, *Adv. Sci.* **2022**, *9*, 2201520.
- [10] a) D. Liu, Q. He, S. Ding, L. Song, *Adv. Energy Mater.* **2020**, *10*, 2001482; b) Y. Bo, C. Gao, Y. Xiong, *Nanoscale* **2020**, *12*, 12196-12209.
- [11] S. Zhao, G. Chen, G. Zhou, L. C. Yin, J. P. Veder, B. Johannessen, M. Saunders, S. Z. Yang, R. De Marco, C. Liu, S. P. Jiang, *Adv. Funct. Mater.* **2020**, *30*, 1906157.
- [12] R. Gusmão, M. Veselý, Z. k. Sofer, *ACS Catal.* **2020**, *10*, 9634-9648.
- [13] K. Wefers, *HARTLD & LENSE E* **1990**, 13-22.
- [14] Y. Rozita, R. Brydson, T. P. Comyn, A. J. Scott, C. Hammond, A. Brown, S. Chauruka, A. Hassanpour, N. P. Young, A. I. Kirkland, *ChemCatChem* **2013**, *5*, 2695-2706.
- [15] a) G. Pacchioni, *ACS Catal.* **2024**, *14*, 2730-2745; b) E. Cordi, J. L. Falconer, *J. Catal.* **1996**, *162*; c) M. Behrens, F. Studt, I. Kasatkin, S. Kühl, M. Hävecker, F. Abild-Pedersen, S. Zander, F. Girgsdies, P. Kurr, B. L. Knierp, M. Tovar, R. W. Fischer, J. K. Nørskov, R. Schlögl, *Science* **2012**, *336*, 893-897; d) C. Peng, R. Guo, X. Feng, X. Fang, *Chem. Eng. J.* **2019**, *377*, 119706; e) F. G. Botes, B. van Dyk, C. McGregor, *Ind. Eng. Chem. Res.* **2009**, *48*, 10439-10447.
- [16] S. S. Akarmazyan, P. Panagiotopoulou, A. Kambolis, C. Papadopoulou, D. I. Kondarides, *Appl. Catal. B* **2014**, *145*, 136-148.
- [17] a) Y. Zhu, R. Luo, H. Shi, K. Koh, L. Kovarik, J. L. Fulton, J. A. Lercher, Z. J. Zhao, J. Gong, O. Y. Gutiérrez, *ACS Catal.* **2024**, *14*, 10031-10039; b) Z. Xiao, L. Zhang, X. Tan, K. Sun, J. Li, L. Pan, J. J. Zou, G. Li, D. Wang, *Adv. Funct. Mater.* **2025**, 2500339; c) L. Wang, H. Wang, H. Huang, T. Yun, C. Song, C. Shi, *Adv. Funct. Mater.* **2024**, *34*, 2309850; d) B. Gao, Z. Wen, Y. Wang, D. Chen, B. Yang, T. Ishihara, L. Guo, *ChemCatChem* **2024**, *16*, e202400814; e) Z. Shi, L. Yang, Z. Lu, Q. Han, L. Wu, L. Wang, Y. Xiong, J. Ye, Z. Zou, Y. Zhou, *Adv. Funct. Mater.* **2024**, *34*, 2409904.
- [18] B. Doss, C. Ramos, S. Atkins, *Energ. fuel.* **2009**, *23*, 4647-4650.
- [19] S. Tada, K. Larmier, R. Büchel, C. Copéret, *Catal. Sci. Technol.* **2018**, *8*, 2056-2060.
- [20] W. Wu, Y. Wang, L. Luo, M. Wang, Z. Li, Y. Chen, Z. Wang, J. Chai, Z. Cen, Y. Shi, J. Zhao, J. Zeng, H. Li, *Angew. Chem. Int. Ed.* **2022**, *61*, e202213024.
- [21] a) J. H. Kwak, J. Hu, D. Mei, C. W. Yi, D. H. Kim, C. H. F. Peden, L. F. Allard, J. Szanyi, *Science* **2009**, *325*, 1670-1673; b) X. Zhang, W. Cui, J. Z. Hu, H. W. Wang, M. P. Prange, C. Wan, N. R. Jaegers, M. Zong, H. Zhang, C. I. Pearce, P. Li, Z. Wang, S. B. Clark, K. M. Rosso, *Cryst. Growth Des.* **2019**, *19*, 5557-5567.
- [22] J. Z. Hu, X. Zhang, N. R. Jaegers, C. Wan, T. R. Graham, M. Hu, C. I. Pearce, A. R. Felmy, S. B. Clark, K. M. Rosso, *J. Phys. Chem. C* **2017**, *121*, 27555-27562.
- [23] L. Kovarik, M. Bowden, K. Khivantsev, J. H. Kwak, J. Szanyi, *Acta Mater.* **2024**, *266*, 119639.
- [24] a) G. Zhu, Y. Jin, M. Ge, *Environ. Sci. Pollut. Res.* **2022**, *29*, 68636-68651; b) X. Yang, X. Ma, D. Han, M. Xiao, L. Ma, H. Sun, X. Yu, M. Ge, *Catal. Today* **2021**, *375*, 352-359.
- [25] L. Nie, A. Meng, J. Yu, M. Jaroniec, *Sci. Rep.* **2013**, *3*, 3215.
- [26] a) B. Xu, J. Qu, X. Wang, L. Wang, Y. Pu, P. Ning, Y. Xie, Y. Ma, Q. Ma, *J. Environ. Sci.* **2024**, *136*, 213-225; b) Y. Liu, B. Zhang, L. Luo, X. Chen, Z. Wang, E. Wu, D. Su, W. Huang, *Angew. Chem. Int. Ed.* **2015**, *127*, 15475-15480.
- [27] a) K. Liu, Z. Sun, W. Chen, X. Lang, X. Gao, P. Chen, *Adv. Funct. Mater.* **2024**, *34*, 2312589; b) K. Liu, Z. Sun, X. Peng, X. Liu, X. Zhang, B. Zhou, K. Yu, Z. Chen, Q. Zhou, F. Zhang, Y. Wang, X. Gao, W. Chen, P. Chen, *Nat. Commun.* **2025**, *16*, 2167.
- [28] R. P. Vasquez, *Surf. Sci. Spectra* **1998**, *5*, 267-272.
- [29] a) M. Digne, P. Sautet, P. Raybaud, P. Euzen, H. Toulhoat, *J. Catal.* **2004**, *226*, 54-68; b) C. Morterra, G. Magnacca, *Catal. Today* **1996**, *27*, 497-532; c) J. Szanyi, J. H. Kwak, *Phys. Chem. Chem. Phys.* **2014**, *16*, 15117-15125.
- [30] a) O. Dularent, X. Courtois, V. Perrichon, D. Bianchi, *J. Phys. Chem. B* **2000**, *104*, 6001-6011; b) A. Dandekar, M. A. Vannice, *J. Catal.* **1998**, *178*, 621-639; c) A. Martínez-Arias, M. Fernández-García, J. Soria, J. C. Conesa, *J. Catal.* **1999**, *182*, 367-377.
- [31] A. A. Guda, S. A. Guda, A. Martini, A. N. Kravtsova, A. Algasov, A. Bugaev, S. P. Kubrin, L. V. Guda, P. Šot, J. A. van Bokhoven, C. Copéret, A. V. Soldatov, *Npj Comput. Mater.* **2021**, *7*, 203.
- [32] L. Fu, X. Li, M. Liu, H. Yang, *J. Mater. Chem. A* **2013**, *1*, 14592-14605.
- [33] L. Shi, Y. Huang, Z. H. Lu, W. Cen, X. Yu, S. Qing, Z. Gao, R. Zhang, G. Feng, *Appl. Surf. Sci.* **2021**, *535*, 147651.
- [34] Q. Wu, R. Qin, M. Zhu, H. Shen, S. Yu, Y. Zhong, G. Fu, X. Yi, N. Zheng, *Chem. Sci.* **2024**, *15*, 3140-3147.
- [35] H. Zhou, H. Jin, Y. Li, Y. Li, S. Huang, W. Lin, W. Chen, Y. Zhang, *Catalysts* **2023**, *13*, 1244.
- [36] a) L. C. Grabow, M. Mavrikakis, *ACS Catal.* **2011**, *1*, 365-384; b) P. Liu, Y. Yang, J. Evans, J. A. Rodriguez, M. G. White, *Phys. Chem. Chem. Phys.* **2010**, *12*.