

# A geospatial environmental and techno-economic framework for sustainable phosphorus management at livestock facilities

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## Abstract

Nutrient pollution of waterbodies is a major worldwide water quality problem. Excessive use and discharge of nutrients can lead to eutrophication and algal blooms in fresh and marine waters, resulting in environmental problems associated with hypoxia, public health issues related to the release of toxins and freshwater scarcity. A promising option to address this problem is the recovery of nutrient releases prior to being discharged into the environment. Driven by the sustainable materials management concept, the COW2NUTRIENT (Cattle Organic Waste to NUTRIent and ENergy Technologies) framework is developed for the techno-economic evaluation and selection of nutrient recovery systems at livestock facilities. Environmental vulnerability to nutrient pollution determined through a geographic information system (GIS)-based model and techno-economic information of different state-of-the-art nutrient management technologies are combined in a multi-criteria decision analysis (MCDA) model, resulting in the selection and economic analysis of the most suitable process for each studied livestock facility. This framework has been employed for studying the implementation of sustainable phosphorus management systems at 2,217 livestock facilities in the Great Lakes area, resulting in capital expenses of 2.5 billion USD if only phosphorus recovery technologies are installed, and up to 5.2 billion USD if nutrient management is combined with biogas and power production. However, considering potential economic incentives for the recovery of phosphorus, net revenues up to 230 million USD per year can be achieved. Therefore, the framework presented reveals the potential of implementing nutrient management systems at

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28 regional scale for the abatement of phosphorus releases from livestock facilities.

29 *Keywords:* Organic Waste, Harmful Algal Blooms, Nutrient Pollution, Livestock Waste,

30 Phosphorus Recovery

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## 31 **1. Introduction**

32 Phosphorus is a source of concern for modern societies. On the one hand, nutrient pollution of  
33 waterbodies is one of the major water quality problems worldwide, resulting in environmental issues  
34 as a consequence of the eutrophication of waterbodies, and the occurrence of cyanobacteria and  
35 harmful algal blooms (HABs). Surveys reveal that eutrophication is a global problem, reporting  
36 that 54% of lakes in Asia, 53% in Europe, 48% in North America, 41% in South America, and 28%  
37 in Africa are eutrophic (Ansari, 2010). In addition to eutrophication, hypoxia of aquatic ecosystems  
38 is associated with the aerobic degradation of the algal biomass by bacteria, shifting the distribution  
39 of aquatic species and releasing toxins in drinking water sources (Sampat et al., 2018). Although  
40 eutrophication is affected by several factors, such as temperature and the self-purification capacity  
41 of waterbodies, the primary limiting factor for eutrophication is often the phosphate concentration  
42 (Werner, 2009). Aside from disturbing aquatic ecosystems, eutrophication also contributes to cli-  
43 mate change, emitting large amounts of strong greenhouse gases as a consequence of the biomass  
44 degradation, such as  $\text{CH}_4$  and  $\text{N}_2\text{O}$  (Beaulieu et al., 2019). On the other hand, phosphorus is an  
45 essential nutrient for living organisms, and a key element for maintaining agricultural productivity.  
46 However, phosphorus is a resource very sensitive to depletion, since extractable deposits of phos-  
47 phorus rock are limited and there is no known substitute or synthetic replacement. Projections  
48 estimate limited availability of phosphate over the next century (Cordell et al., 2009). Therefore, in  
49 addition to the environmental perspective, the search for phosphorus recycling processes is a major  
50 driving force for the development of nutrient recovery systems (Reijnders, 2014).

51 Agricultural activities are one of the main contributors to human-based phosphorus releases  
52 (Dzombak, 2011), including non-point source releases by over-use of fertilizers in croplands, point  
53 source releases originated from the disposal of livestock waste, and nutrient legacy that have accu-  
54 mulated in watersheds due to historical phosphorus releases. Focusing on the point source releases

55 generated by the cattle industry, these result from the production of large amounts of livestock  
56 organic waste, containing substantial amounts of phosphate and ammonia. Sampat et al. (2017)  
57 presented the link between the presence of livestock facilities and higher concentrations of phos-  
58 phorus in soil, resulting in increased nutrient runoff to waterbodies. While for animals on pasture,  
59 organic waste should not be a source of concern if stocking rates are not excessive, for concentrated  
60 animal feeding operations (CAFOs) manure should be properly managed due to the high rates and  
61 spatial concentration of the organic waste generated. A common practice to recycle the nutrients  
62 contained in the organic waste is the land application of the manure. However, since the high-water  
63 content of manure makes its transportation to nutrient deficient locations difficult and expensive,  
64 it is usually spread in the surroundings of the CAFOs, leading to surplus of nutrients in soils and  
65 phosphorus runoff to waterbodies (United States Department of Agriculture, 2009).

66 The implementation of nutrient recovery technologies at livestock facilities to recover phosphorus  
67 from cattle manure is a promising approach to recycle and leverage nutrients more efficiently,  
68 mitigating the nutrient pollution of waterbodies (Li et al., 2021). However, the technologies that  
69 can be implemented at CAFOs differ widely in aspects such as phosphorus recovery performance,  
70 final products obtained, capital expenses, and operational costs. Additionally, different levels of  
71 environmental vulnerability to eutrophication may require the use of different P recovery processes,  
72 searching for the most effective balance between P recovery efficiency and cost. Previous efforts for  
73 the technical evaluation of different phosphorus recovery technology have been performed, resulting  
74 in processes with proven technical feasibility for phosphorus recovery. Particularly, there exists  
75 a considerable body of literature on the production of struvite (Muhmood et al., 2019). Other  
76 mature processes for the recovery of phosphorus are the formation of calcium precipitates (Berg  
77 et al., 2006), and systems based on physical separations (Church et al., 2016). Additionally, novel  
78 processes are currently under development, such as membrane separation processes (Li et al., 2020),  
79 microalgae-based processes (Robles et al., 2020), adsorption using biochar (Wang et al., 2020), and  
80 electrochemical processes (Belarbi et al., 2020). Moreover, a decision-making framework has been  
81 developed for the selection and implementation of phosphorus recovery systems in urban areas  
82 (Pearce, 2015). However, to the best of the authors knowledge, there are no specific frameworks

83 to study the implementation of phosphorus recovery systems at livestock facilities considering GIS  
84 environmental and techno-economic dimensions.

85 In this work, we propose a novel framework, COW2NUTRIENT (Cattle Organic Waste to  
86 NUTRIent and ENergy Technologies), for the assessment and selection of phosphorus recovery  
87 technologies at CAFOs based on environmental and techno-economic criteria. This framework  
88 combines eutrophication risk data at subbasin level and the techno-economic assessment of six  
89 state-of-the-art phosphorus recovery processes in a multi-criteria decision analysis (MCDA) model.  
90 This information is normalized and aggregated for the selection of the most suitable technology for  
91 each analyzed CAFO. The goal is to develop a flexible framework able to balance the operating  
92 cost of the systems and P recovery efficiency as a function of the environmental vulnerability to  
93 eutrophication of each region. The minimization of operating costs is prioritized in regions with low  
94 eutrophication risk, while the efficiency of P recovery is the most relevant criteria in regions affected  
95 by nutrient pollution. Also, COW2NUTRIENT aims to provide a useful framework for designing  
96 and evaluating effective GIS-based incentives and regulatory policies to control and mitigate nutrient  
97 pollution of waterbodies. The practicability of the proposed framework is assessed by studying and  
98 designing the implementation of P recovery systems at 2,217 current livestock facilities in the Great  
99 Lakes area.

## 100 **2. Methods**

101 COW2NUTRIENT framework is comprised by three models, i.e. environmental geographic in-  
102 formation, techno-economic, and multi-criteria decision analysis models, in order to integrate the  
103 geographic data on vulnerability to nutrient pollution, and the technical and economic information  
104 of the nutrient recovery systems through an MCDA model, as shown in Figure 1. First, the geo-  
105 graphic location of the individual facilities (longitude and latitude) is supplied to the environmental  
106 GIS model to determine the vulnerability level to nutrient pollution of the region where the stud-  
107 ied CAFOs are located. Secondly, data regarding the number and type of animals at the facility  
108 (i.e., beef and dairy cattle, adult animals, heifers, and calves) are entered into the techno-economic  
109 model to capture the characteristics of the livestock facility evaluated. Data reported by the US

110 Department of Agriculture were considered for manure generation ratios (Kellogg et al., 2000) and  
 111 composition (United States Department of Agriculture, 2009). These values are collected in Table  
 112 3S of the Supplementary Material. In addition, economic data are fed into the techno-economic  
 113 model for economic performance evaluation purposes, including the value of incentives received for  
 114 phosphorus recovery (in the form of P credits), and for the generation of bio-based methane or  
 115 electricity (in form of Renewable Energy Certificate (REC) and Renewable Identification Number  
 116 (RIN) respectively). The output data from the techno-economic and environmental geographic  
 117 information models are imported in the MCDA model. In this module, the data is normalized  
 118 and aggregated, returning a composite index for each technology. This composite index is used to  
 119 score and rank the nutrient recovery systems based on their performance. All models have been  
 120 developed using Python (van Rossum, 1995).

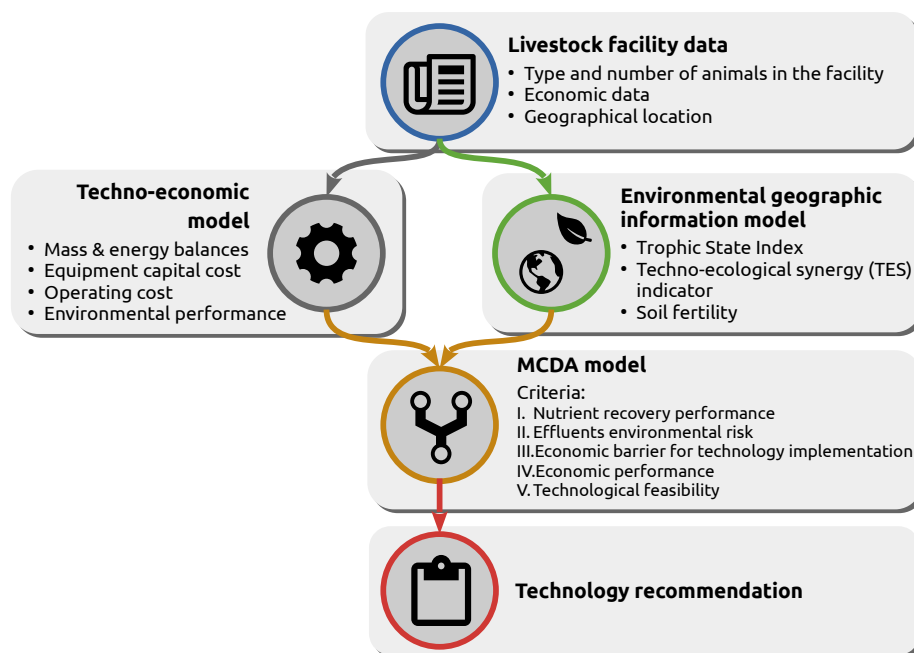


Figure 1: Structure of the COW2NUTRIENT decision support framework for the assessment and selection of phosphorus recovery systems.

121 *2.1. Environmental geographic information model*

122 The environmental vulnerability to nutrient pollution of the area where the livestock facilities  
123 are located determines the preference (i.e., ranks the importance) of each criterion. Three indicators  
124 are used to evaluate the eutrophication risk of each region studied at subbasin spatial resolution.  
125 The trophic state of waterbodies is evaluated through the Trophic State Index (Carlson, 1977),  
126 determining their eutrophication level. The phosphorus saturation of soils, which can result in  
127 the transport of phosphorus to waterbodies by run-off, is evaluated through Mehlich 3 phosphorus  
128 concentration (Espinoza et al., 2006). Finally, the balance between phosphorus releases and uptakes  
129 from anthropogenic activities is assessed through the techno-ecological synergy metric (Bakshi et al.,  
130 2015), determining if there is a net accumulation or depletion of phosphorus in a region over time.  
131 The use of these three indicators makes it possible to determine if there exist an immediate risk of  
132 eutrophication in the region studied (eutrophized waterbodies), a long-term risk (moderate value  
133 of TSI, soils saturated by phosphorus, or phosphorus releases and uptakes from anthropogenic  
134 activities unbalanced), or if there is no risk of eutrophication (phosphorus uptakes and releases are  
135 balanced). Detailed descriptions of the performed data analysis, and maps for the contiguous US  
136 are provided in Section 1 of the Supplementary Material.

137 *2.1.1. Spatial resolution*

138 A watershed is defined as the region draining all the streams and rainfall to a common waterbody,  
139 defining the geographic limits for the collection of runoff elements. US watersheds are designated  
140 by the US Geological Survey through the Hydrologic Unit Code (HUC) system. The HUC system  
141 divides the US into regions, subregions, basins, subbasins, watersheds, and subwatersheds. Each  
142 hydrologic unit of these six levels is identified hierarchically by a unique numeric code from 2 to 12  
143 digits (i.e., HUC2 to HUC12). The spatial resolution of this study is the contiguous United States  
144 at the subbasin level, defined by the HUC system at 8 digits (HUC8) (U.S. Geological Survey,  
145 2013).

146 *2.1.2. Trophic State Index*

147 The Trophic State Index (TSI) is a metric proposed by Carlson (1977) to determine the trophic  
 148 status of waterbodies (U.S. Environmental Protection Agency, 2012a). The TSI of a waterbody is  
 149 scored in a range from 0 to 100 representing its throphic state, as shown in Table 1. Oligotrophic  
 150 and mesotrophic states denote low and intermediate biomass productivities, while eutrophic and  
 151 hypereutrophic states are referred to waterbodies with high biological productivity and frequent  
 152 algal blooms. Combined data for chl- $\alpha$  and total phosphorus concentrations retrieved from the  
 153 National Lakes Assessments conducted by the US EPA in 2007 and 2012 (U.S. Environmental  
 154 Protection Agency, 2012b, 2007) is used to determine the Trophic State Index of lentic waters in the  
 155 contiguous US. No TSI values were assigned to the watersheds without reported data. Correlations  
 156 to estimate the TSI from chlorophyll- $\alpha$  and total phosphorus concentrations are collected in Section  
 157 1 of Supplementary Material.

Table 1: Relation between TSI value and trophic class.

TSI	<40	40-50	50-70	>70
Trophic Class	Oligotrophic	Mesotrophic	Eutrophic	Hypereutrophic

158 *2.1.3. Techno-ecological synergy sustainability metric*

159 The techno-ecological synergy sustainability metric (TES) is an indicator proposed by Bakshi  
 160 et al. (2015) to evaluate the fraction of net anthropogenic phosphorus releases, Eq. 1.

$$V_x = \frac{(U_x - E_x)}{E_x} \quad (1)$$

161 A negative value for TES indicator ( $V_x$ ) indicates that the releases ( $E_x$ ) are larger than the  
 162 uptake capacity of the evaluated system, ( $U_x$ ), and thus impacting in the ecosystems; while positive  
 163 values reflects that the releases can be absorbed by the system without any harm.

164 Phosphorus releases from agricultural activities have been estimated from data reported by the  
 165 Nutrient Use Geographic Information System project. Since this work is limited to the assessment

166 of agricultural phosphorus releases, other possible sources of phosphorus releases are not considered.  
 167 Further information about the methodology used for the estimation of human-based phosphorus  
 168 releases can be found in International Plant Nutrition Institute (IPNI) (2012). Anthropogenic  
 169 phosphorus uptakes are those due to the crops grown in each watershed, including corn, soybeans,  
 170 small grains, cotton, rice, vegetables, orchards, greenhouse and other crops (i.e., fruits, sugar crops,  
 171 and oil crops). The estimation of the phosphorus uptakes is performed considering the different  
 172 phosphorus requirements and yield rates of each crop, as well as the land cover and the crops  
 173 distribution in each watershed. Data retrieved from United States Department of Agriculture  
 174 (2019), United States Department of Agriculture (2009), and Pickard et al. (2015) is used for this  
 175 purpose.

#### 176 *2.1.4. Phosphorus saturation of soils*

177 Phosphorus concentration in soil is used for the evaluation of the phosphorus legacy that is  
 178 continuously built up in soils, providing a metric of soil quality. However, only a fraction of  
 179 phosphorus is available for plants. To measure this phosphorus fraction available for plants, several  
 180 standardized phosphorus soil tests have been proposed, including Olsen, Bray 1, and Mehlich 3  
 181 tests. Among them, Mehlich 3 (M3P) has been selected as a measure of the concentration of P in  
 182 soils since it is a widely used metric, and it is the P soil test least affected by changes in soil pH. To  
 183 estimate the fraction of phosphorus available for plants from total phosphorus concentration data,  
 184 a correlation developed by Allen and Mallarino (2006) has been used, Eq. 2. It must be noted that  
 185 this correlation has been developed for agricultural soils in Iowa, but due to the lack of studies in  
 186 this topic, it has been used for soils throughout the contiguous US. Therefore, it must be considered  
 187 as an exploratory effort to determine the phosphorus saturation in the US soils. Data reported by  
 188 Smith et al. (2013) is used to evaluate the concentration of total phosphorus along the contiguous  
 189 US.

$$\text{M3P (\% over TP)} = \frac{4.698 \cdot 10^{-1}}{1 + (\text{TotalP (mg/kg)} \cdot 1.336 \cdot 10^{-3})^{-2.148}} \quad (2)$$

190 The relationship between M3P test value and the quality of soil is shown in Table 2. Soil fertility  
 191 levels below optimum indicate that nutrient supplementation is needed to enhance the yield of crops,  
 192 optimum values indicates that no nutrient supplementation is needed, and excessive soil fertility  
 193 level indicate over-saturation of phosphorus in soil that can reach waterbodies by runoff (Espinoza  
 194 et al., 2006).

Table 2: Relationship between Mehlich 3 phosphorus and soil fertility level (Espinoza et al., 2006).

Soil Fertility Level	M3P soil phosphorus concentration (ppm)
Very Low	<16
Low	16-25
Medium	26-35
Optimum	36-50
Excessive	>50

## 195 2.2. Techno-economic model

196 COW2NUTRIENT framework evaluates all the stages involved in the processing of manure for  
 197 P recovery, from organic waste collection to the recovery of nutrients and other by-products such  
 198 as electricity or biomethane, as represented in Fig 2. In addition to the assessment of nutrient  
 199 recovery systems, the framework is flexible to include anaerobic digestion, and the subsequent  
 200 biogas valorization, for the production of methane or electricity. The techno-economic model is  
 201 based on mass balances, thermodynamics, and chemical equilibria for each possible stage of the  
 202 manure treatment process, i.e. manure conditioning, anaerobic digestion, biogas purification, biogas  
 203 valorization, and phosphorus recovery. Preliminary design and sizing of equipment is performed to  
 204 estimate the capital and operating expenses when no specific costs data are available. A detailed  
 205 description of equipment design and sizing, as well as the correlations used for costs estimation,  
 206 can be found in Section 2 of the Supplementary Material.

### 207 2.2.1. Manure conditioning

208 It is considered that the collection of manure does not involve any cost, since CAFOs have  
 209 manure collection systems already installed. All manure produced is assumed to be collected. If  
 210 the anaerobic digestion (AD) stage is implemented, a preconditioning stage is considered to adjust

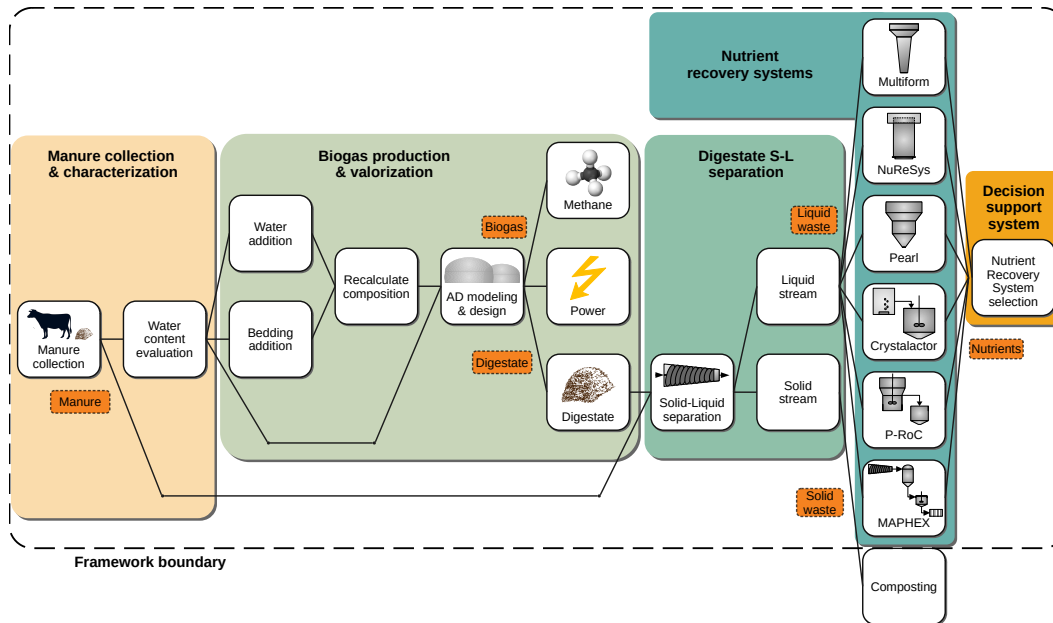


Figure 2: Process flowsheet for manure management and phosphorus recovery stages included in COW2NUTRIENT.

211 the water content of the waste. US EPA determines that the content of total solids in manure  
 212 should be less than 15% (U.S. Environmental Protection Agency, 2004), as shown in Figure 6S of  
 213 the Supplementary Material. Therefore, additional water may be added to reduce the solids content  
 214 in manure before the AD stage.

### 215 2.2.2. Anaerobic digestion

216 Anaerobic digestion is a microbiological process that breaks down organic matter in the ab-  
 217 sence of oxygen. It involves four stages, hydrolysis, acidogenesis, acetogenesis, and methanogenesis;  
 218 producing a mixture of gases mainly composed of methane and carbon dioxide (biogas), and a de-  
 219 composed organic substrate (digestate). The model of the anaerobic digester is formulated through  
 220 the mass balances of the species involved in the production of biogas and digestate. A detailed  
 221 description of the digester modeling can be found in León and Martín (2016). As a result of the  
 222 AD process, a fraction of organic phosphorus and nitrogen are transformed in their inorganic forms.  
 223 To evaluate the amount of organic nutrients transformed into inorganic phosphorus and nitrogen,

224 data available in literature was considered, resulting in an increase of 24% and 16% over the orig-  
225 inal inorganic ammonia and phosphate respectively, as shown in Table 5S of the Supplementary  
226 Material. Correlations to estimate the capital cost and operating and management costs (O&M)  
227 as a function of the animal population of CAFOs were developed using data from the US EPA  
228 AgSTAR program (U.S. Environmental Protection Agency, 2003) and the USDA (Beddoes et al.,  
229 2007) respectively. We refer the reader to the Supplementary Material for further information.

### 230 *2.2.3. Biogas purification*

231 Before transforming biogas into marketable products, a purification stage has to be carried out  
232 to remove  $H_2S$ ,  $H_2O$ , and  $NH_3$ . The removal of  $H_2S$  is performed in a bed of ferric oxide through the  
233 production of  $Fe_2S_3$  operating at a temperature range of 25-50°C. The bed regeneration is carried  
234 out using oxygen to produce elemental sulfur and ferric oxide ( $Fe_2O_3$ ). Water and ammonia are  
235 adsorbed using a pressure swing adsorption system (PSA) with zeolite 5A as adsorbent material,  
236 operating at low temperature (25°C) and moderate pressure (4.5 bar). The assumed recovery for  
237  $NH_3$  and  $H_2O$  is 100%. For further details about the modeling of the biogas purification stage, we  
238 refer the reader to previous works (León and Martín, 2016; Martín-Hernández et al., 2018).

### 239 *2.2.4. Biogas valorization*

240 Two final added value products have been considered, methane and electricity, since they can  
241 be obtained through relatively simple processes and there exists developed markets for them.

242 *Methane production.* The process considered for methane production is the removal of  $CO_2$  using  
243 a PSA system with a bed of zeolite 5A, since this process was demonstrated as the optimal biogas  
244 upgrading process by Martín-Hernández et al. (2020a), where further details about the modeling  
245 of the PSA system can be found.

246 *Electricity production.* Electricity is produced from biogas through a gas turbine. A Brayton cycle  
247 consisting of double-stage compression system, one for the air stream and one for the biogas stream,  
248 is considered. Polytropic compression is assumed, with a polytropic index of 1.4 and an efficiency of  
249 85% (Moran et al., 2010). The adiabatic combustion of methane contained in the biogas is assumed,

250 with a pre-heating of the biogas-air mixture, considering the combustion chamber as an adiabatic  
251 furnace. An air excess of 20% with respect to the stoichiometric needs, and 100% conversion of the  
252 reaction are assumed. Further details for electricity production can be found in Martín-Hernández  
253 et al. (2018).

#### 254 *2.2.5. Solid-liquid separation*

255 Nutrients contained in organic waste (manure or digestate, depending on whether AD is carried  
256 out or not) are present in both organic and inorganic forms. Organic nutrients are chemically bonded  
257 to carbon, and they have to be converted into their inorganic forms through a mineralization process  
258 to be available for the vegetation to grow. Organic nutrients are mainly contained in the solid phase  
259 of organic waste. Inorganic nutrients are water soluble, and they are mostly present in the liquid  
260 phase, or bounded to soluble minerals. They are immediately available to plants, including algae  
261 involved during the occurrence of HABs. To recover the inorganic fraction of nutrients, a solid-  
262 liquid separation stage is implemented, keeping the inorganic nutrients in the liquid stage, which  
263 will be further processed, and the organic nutrients in the solid phase, which can be composted to  
264 mineralize nitrogen and phosphorus and be further used as fertilizers. The study of organic waste  
265 composting is out of the scope of this work.

266 Based on the evaluation reported by Møller et al. (2000), a screw press is the technology selected  
267 to carry out the solid-liquid separation stage since it is the most cost-efficient equipment. The  
268 partition coefficients for the different components are shown in Table 6S of the Supplementary  
269 Material. Assuming the discretization of units due to the commercial sizes available, the investment  
270 and operating costs for the screw press equipment are presented in Figure 9S of the Supplementary  
271 Material.

#### 272 *2.2.6. Phosphorus recovery*

273 The technologies to recover inorganic phosphorus can be classified in three categories: struvite-  
274 based phosphorus recovery, calcium precipitates-based phosphorus recovery, and physical separation  
275 systems. Table 3 shows the classification and characteristics of the evaluated technologies. Regard-  
276 ing struvite-based systems, the formation of struvite has been widely described in the literature,

277 mainly focused on phosphorus recovery from wastewater (Rahaman et al., 2014; Battistoni et al.,  
278 2001). However, cattle organic waste shows some characteristics that hinder struvite formation,  
279 including high ionic strength, which reduces the effective concentration of ions; and the presence of  
280 calcium ions competing for phosphate ions (Yan and Shih, 2016), which inhibits a selective recovery  
281 by phosphorus precipitation. The high variability in the manure composition, as a function of the  
282 geographic area, the animal feed, etc., represents an additional challenge for nutrient recovery (Tao  
283 et al., 2016). Therefore, specific correlations for livestock waste to estimate the molar fraction of  
284  $\text{PO}_4^{3-}$  and  $\text{Ca}^{2+}$  recovered as struvite as a function of the amount of calcium contained in the waste  
285 were developed in a previous work (Martín-Hernández et al., 2020b).

286 Among the different products obtained by the different processes, only struvite generates in-  
287 come. Calcium precipitates lacks of a well-established market as fertilizer, and therefore no sales  
288 of this product are considered. MAPHEX produces an organic solid rich in nutrients, but with  
289 a lower nutrient density compared with struvite, hindering transportation of this product and  
290 decreasing its market value. Therefore, we have assumed that no income is obtained from this  
291 product. Nevertheless, the recovered products allow phosphorus distribution from CAFO releases  
292 to phosphorus-deficient areas.

293 All technologies considered are at or near commercial stage. We note that, for all the technologies  
294 evaluated, the installation of several P recovery units in parallel arrangement is considered if the  
295 amount of waste to be processed exceeds the treatment capacity of the system. The description  
296 of the processes, and the correlations used to estimate the struvite formed, equipment cost, and  
297 operating costs are collected in the Section 2.2.4 of the Supplementary Material.

### 298 *2.2.7. Incentives for the installation of nutrient recovery systems*

299 COW2NUTRIENT can evaluate the effect of different kinds of incentives on the economic perfor-  
300 mance of the nutrient recovery systems. These incentives can be received as a result of the recovery  
301 of phosphorus, in the form of P-credits, or for the generation of electricity or biomethane, in form of  
302 Renewable Energy Certificates (REC) and Renewable Identification Numbers (RIN) respectively.  
303 Renewable Energy Credits are a mechanism implemented in the US which guarantees that energy

Table 3: Description of phosphorus recovery technologies systems by COW2NUTRIENT framework.  $x_{Ca^{2+};PO_4^{3-}}$  refers to the  $Ca^{2+}/PO_4^{3-}$  molar ratio.  $n_i$  denotes the number of units of the technology  $i$  installed.

Technology	Company	Technology type	Technology readiness level	Phosphorus recovery efficiency (%)	Treatment capacity ( $\frac{kg-P_{2O_5}}{day-unit}$ )	CAPEX ( $\frac{MM USD}{unit}$ )	OPEX ( $\frac{USD}{kg-P_{2O_5}}$ )	Reference
Multiform	Multiform Harvest	Struvite-based	9	$\frac{0.798 \cdot 100}{1 + (x_{Ca^{2+};PO_4^{3-}} - 0.576)^{2.113}}$	38.5	1.1	15.42	1
Crystalactor	Royal Haskoning DHV	Struvite-based	9	$\frac{0.798 \cdot 100}{1 + (x_{Ca^{2+};PO_4^{3-}} - 0.576)^{2.113}}$	137.7	$2.3 + 0.71 \cdot n_{Crystalactor}$	2.12	2
NuReSys	Nutrient Recovery Systems	Struvite-based	9	$\frac{0.798 \cdot 100}{1 + (x_{Ca^{2+};PO_4^{3-}} - 0.576)^{2.113}}$	204.0	1.38	6.22	1
Pearl 500	Ostara	Struvite-based	9	$\frac{0.798 \cdot 100}{1 + (x_{Ca^{2+};PO_4^{3-}} - 0.576)^{2.113}}$	65.0	2.3	7.54	3
Pearl 2K	Ostara	Struvite-based	9	$\frac{0.798 \cdot 100}{1 + (x_{Ca^{2+};PO_4^{3-}} - 0.576)^{2.113}}$	250.0	3.1	7.54	1
Pearl 10K	Ostara	Struvite-based	9	$\frac{0.798 \cdot 100}{1 + (x_{Ca^{2+};PO_4^{3-}} - 0.576)^{2.113}}$	1250.0	10.0	7.54	4
P-RoC	Karlsruhe Institute of Technology	Calcium precipitates-based	6	60	24.3	Tailored design based on waste flow processed. See Section 2.2.4.4 of Supplementary Material.	23.22 - 167.8	5
MAPHEX	University of Pennsylvania and USDA	Modular phases separation system	7	90	18.5	0.3	110.8	6, 7

- 1: Australian Meat Processor Corporation (2018)
- 2: Egle et al. (2016)
- 3: County of Napa (2013)
- 4: American Society of Civil Engineers (ASCE) (2013)
- 5: Ehbrecht et al. (2011)
- 6: Church et al. (2016)
- 7: Church et al. (2018)

304 is generated from renewable sources, providing a system for trading produced renewable electricity.  
305 Each produced renewable megawatt-hour generates one REC, that can be sold separately from the  
306 electricity commodity itself and can be used to meet regulatory requirements by generators, trades,  
307 or end-users. On the other hand, RINs are identification numbers assigned to batches of biofuel,  
308 allowing their tracking through the production, purchase, and final usage. The allocation of RINs  
309 is associated with the allocation of incentives for the generation bio-fuels. The considered values  
310 for the different incentives are listed in Table 4S of the Supplementary Material.

### 311 *2.3. Multi-criteria decision model*

312 The determination of the most suitable nutrient management process is not a trivial procedure  
313 since multiple criteria play a critical role at the decision-making stage. COW2NUTRIENT per-  
314 forms the selection of P recovery technologies considering information concerning environmental,  
315 economic, and technology readiness dimensions. The integration of these dimensions is justified  
316 by the need to find the most suitable system for each CAFO by balancing operating cost and ef-  
317 ficiency in the mitigation of nutrient pollution according to the local environmental vulnerability  
318 to eutrophication. Finally, the technical maturity of each system is also considered to assess the  
319 development level of the different processes. Therefore, a multi-criteria decision analysis (MCDA)  
320 model was developed to address the selection of the most suitable phosphorus recovery systems for  
321 each studied CAFO. The workflow of the MCDA model is summarized in Figure 3.

322 Five criteria are combined in a composite index for the assessment of the environmental, eco-  
323 nomic, and technology maturity dimensions of the different technologies. Two environmental crite-  
324 ria are studied to assess the performance of the different technologies to mitigate phosphorus releases  
325 from CAFOs, i.e., the fraction of phosphorus recovered, and the potential environmental threat for  
326 the local ecosystem of the effluents containing the non-recovered phosphorus evaluated through  
327 the eutrophication potential of the effluents. The economic aspect is considered by means of two  
328 criteria, the economic barrier for the implementation of P recovery processes, measured in terms  
329 of capital cost, and the overall economic performance of the systems, which is evaluated through  
330 the net present value (NPV) (Sinnott, 2014). Finally, the technological maturity of the different

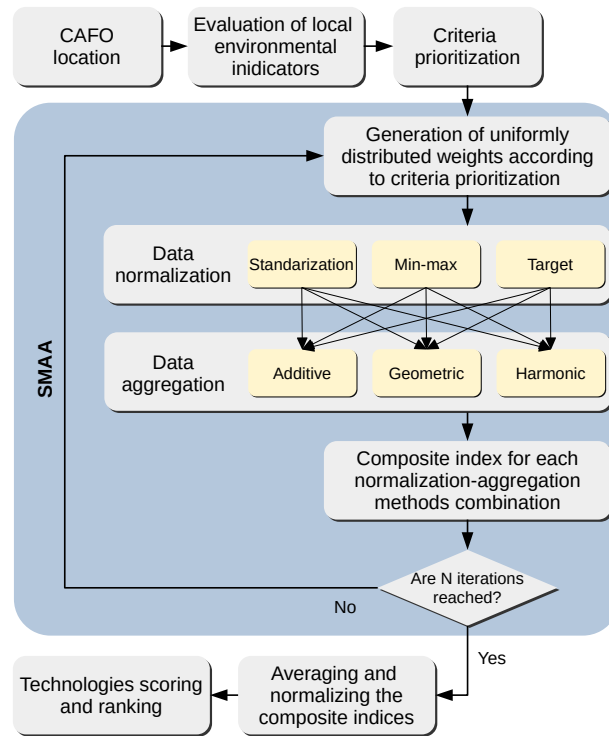


Figure 3: Flowsheet for the MCDA model.

331 technologies is considered through the technology readiness level (TRL) index. The construction  
 332 of a composite index integrating these criteria is composed of three steps: criteria normalization,  
 333 weighting, and aggregation (Gasser et al., 2020).

### 334 2.3.1. Data normalization

335 Since each criteria has a different range of potential values, they must be normalized to a  
 336 common scale to allow each criteria to be compared with the others. However, the composite  
 337 index can be affected by the normalization technique used. In order to study the robustness of  
 338 the composite index obtained, and to address the uncertainty originated by data normalization,  
 339 normalized data using standardization, min-max, and target normalization methods is calculated  
 340 (OECD and European Commission, 2008).

Table 4: Criteria preference as a function of the GIS-based environmental indicators for nutrient pollution.

Local environmental indicators values	Criteria ranking	Description
<p>Condition 1:  <math>TES &gt; TSI</math> and  <math>TES &gt; \text{Soil fertility}</math></p> <p>Condition 2:  <math>TES = \text{Unbalanced}</math></p>	$TRL > NPV >$ $\text{Capital cost} > TP \text{ recovered} >$ $\text{Eutrophication potential}$	<p>Unbalanced phosphorus releases but no immediate threat to soil and water bodies.</p> <p>Prevalence of economic criteria for nutrient recovery system selection.</p>
<p>Condition 1:  <math>TSI \geq TES</math> or  <math>TSI \geq \text{Soil fertility}</math></p> <p>Condition 2:  <math>TSI = \text{Eutrophic}</math> or  <math>\text{Hypereutrophic}</math></p>	$TRL >$ $\text{Eutrophication potential} > NPV >$ $TP \text{ recovered} > \text{Capital cost}$	<p>High Trophic State Index.</p> <p>Immediate environmental risk due to potential algal blooms.</p> <p>Prevalence of environmental criteria for nutrient recovery system selection.</p>
<p>Condition 1:  <math>\text{Soil fertility} \geq TES</math> and  <math>\text{Soil fertility} &gt; TSI</math></p> <p>Condition 2:  <math>\text{Soil fertility} = \text{Excessive}</math></p>	$TRL > TP \text{ recovered} >$ $NPV > \text{Eutrophication potential} >$ $\text{Capital cost}$	<p>Excessive P in soil.</p> <p>Immediate environmental risk due to potential P runoff.</p> <p>Prevalence of environmental criteria for nutrient recovery system selection.</p>
<p>Condition:  <math>TES \neq \text{Saturated}</math>  and  <math>TSI \neq \text{Eutrophic}</math> or  <math>\text{Hypereutrophic}</math>  and  <math>\text{Soil fertility} \neq \text{Excessive}</math></p>	$TRL > NPV >$ $\text{Capital cost} > TP \text{ recovered} >$ $\text{Eutrophication potential}$	<p>No environmental risk.</p> <p>Prevalence of economic criteria for nutrient recovery system selection.</p>

TRL: Technology Readiness Level  
 TSI: Trophic State Index  
 TES: Techno-Ecological Synergy sustainability metric  
 NPV: Net Present Value  
 TP: Total Phosphorus

341 *2.3.2. Criteria weighting*

342 The normalized criteria are weighted to set the relative importance of each criterion, prioritizing  
343 some criteria over others. This is needed in order to obtain a flexible decision method able to balance  
344 the operating cost of the systems and the P recovery efficiency as a function of the environmental  
345 vulnerability to eutrophication of each region. The minimization of the operating costs is prioritized  
346 in regions with low eutrophication risk, while the efficiency of P recovery is more relevant in regions  
347 affected by nutrient pollution. Therefore, the criteria are dynamically weighted according to the  
348 values of TSI, TES and Mehlich 3 phosphorus concentration in each region studied. The preference  
349 of criteria as a function of the environmental vulnerability to eutrophication is shown in Table 4.  
350 On the one hand, if there is immediate environmental risk by nutrient pollution (i.e., high values  
351 for TSI or soil fertility), phosphorus recovery efficiency is prioritized over economic performance.  
352 Conversely, if there is environmental risk in the long run due to the unbalance between anthro-  
353 pogenic phosphorus releases and uptakes (negative value of TES indicator), or there is no potential  
354 environmental risk, the economic performance is prioritized over the phosphorus recovery efficiency.  
355 Finally, since the objective of this framework is to select P recovery systems that are feasible to  
356 install and operate in CAFOs, the TRL index is set as the criteria with highest preference in all  
357 cases in order to minimize the risk of selecting non-full-scale processes. As a result, the selection  
358 of processes with low TRL will be hampered unless they have good economic or environmental  
359 performance.

360 The procedure described above sets the prioritization of criteria, i.e., they can be sorted in  
361 order of importance. However, it does not provide an specific value for the weights, which values  
362 are unknown. In order to avoid the risk of biasing the decision-making procedure setting arbitrary  
363 values for the weights, a stochastic multi-criteria acceptability analysis (SMAA) is used to explore  
364 the weights space (Tervonen and Lahdelma, 2007). Through this approach, the feasible space of each  
365 weight (i.e., the space delimited by the previous and the subsequent weights) is explored through  
366 the Monte Carlo method, retrieving a set of weights for all criteria according to the assigned order.  
367 The SMAA is formulated by defining the set of  $n$  weights ( $\omega$ ) as a non-negative set which elements  
368 must sum 1, as shown in Eqs. 3 and 4.

$$\omega_j \geq 0 \quad \forall j \in n \quad (3)$$

$$\sum_{j=1}^n \omega_j = 1 \quad (4)$$

$$\omega_{j1} \geq \omega_{j2} \geq \dots \geq \omega_{jn} \quad (5)$$

369 The preference information of the criteria, defined through the ranking of the criteria shown  
 370 in Table 4, is expressed as a sequence of inequality constraints, Eq. 5. A detailed description of  
 371 the SMAA method can be found in Tervonen and Lahdelma (2007). A number of Monte-Carlo  
 372 simulations ( $N$ ) of 100 is assumed as a trade-off between computational cost and MCDA model  
 373 performance.

### 374 2.3.3. Criteria aggregation

375 The aggregation stage merges the weighted criteria, resulting in the composite index. Similarly  
 376 to the normalization stage, different aggregation methods are evaluated to improve the robustness  
 377 of the solutions retrieved by the framework. Different aggregation schemes denote different degrees  
 378 of compensability between indicators, i.e. a deficit in one criteria can be fully, partially, or not  
 379 compensated by a surplus in other criteria (Gasser et al., 2020). Three aggregation functions are  
 380 evaluated including full compensation (additive aggregation) and partial compensation schemes  
 381 (geometric and harmonic aggregation methods). Nine composite indexes are obtained for each P  
 382 recovery technology combining normalization and aggregation techniques, as shown in Figure 3.  
 383 Finally, the composites indexes are normalized in a range from 0 to 1 and ranked to determine the  
 384 most suitable P recovery process for the CAFO under study.

### 385 2.4. Framework limitations

386 The main limitations of the proposed framework lie in the uncertainty of the input data. On the  
 387 one hand, since the data regarding the animal number, type of animals, and location of CAFOs are  
 388 reported by the state environmental protection agencies of each state, they are considered reliable.

389 On the other hand, to estimate the local vulnerability to phosphorus pollution throughout the  
390 contiguous US, HUC8 spatial resolution has been chosen as a trade-off solution between spatial  
391 accuracy and data uncertainty. However, more accurate results can be obtained if reliable data for  
392 phosphorus level in soils, fertilizer application rates, etc. are available for higher spatial resolution.  
393 Particularly, further studies for developing more accurate correlations to estimate the fraction of  
394 phosphorus available to plants based on soil type and climate conditions in each region would  
395 improve the accuracy of the assessment of local risk to phosphorus pollution. Additionally, since the  
396 proposed framework is focused on phosphorus recovery for freshwater nutrient pollution prevention  
397 and control, the recovery of other resources contained in livestock manure (such as organic carbon  
398 and nitrogen) is not considered in this study.

## 399 *2.5. Case study*

### 400 *2.5.1. Study region*

401 The Great Lakes area, located in North America, is selected in order to demonstrate the im-  
402 plementation of nutrient management systems at CAFOs using the COW2NUTRIENT framework.  
403 This region is selected because its high concentration of CAFO facilities, resulting in significant  
404 nutrient releases that contribute to frequent HABs and eutrophication episodes, as well as to the  
405 nutrient legacy accumulated over time (Sayers et al., 2019; Han et al., 2012). The evaluation  
406 and implementation of phosphorus recovery systems at CAFOs already in operation at the US  
407 states of Pennsylvania (Pennsylvania Department of Environmental Protection, 2019), Ohio (Ohio  
408 Department of Agriculture, 2019), Indiana (Indiana Department of Environmental Management,  
409 2019), Michigan (Michigan Department of Environment, Great Lakes, and Energy, 2019), Wis-  
410 consin (Wisconsin Department of Natural Resources, 2019), and Minnesota (Minnesota Center for  
411 Environmental Advocacy, 2019) are performed using the criteria prioritization based on the GIS  
412 indicators describing the environmental impact of nutrient pollution shown in Table 4. The states  
413 of Illinois and New York, and the Canadian province of Ontario, which are also part of the Great  
414 Lakes area, are not included due to the unavailability of reliable information about their CAFOs.  
415 A description of the studied states listing the animal units, annual manure generation, and annual

416 phosphorus releases by the year 2019, disaggregated for dairy and beef cattle, is collected in Table  
417 10S of the Supplementary Material.

418 It should be noted that, accordingly to the US regulatory definition of CAFOs, only intensive  
419 livestock facilities with 300 animal units or more are considered in this study (U.S. Environmental  
420 Protection Agency, 2012c), resulting in the evaluation of 2,217 CAFOs. An animal unit is defined  
421 as an animal equivalent of 1,000 pounds (453.6 kg) live weight (U.S. Department of Agriculture,  
422 2011). Animal units is used as a unit to measure the size of CAFOs due to the presence of different  
423 types of animals in the CAFOs, i.e. beef or dairy cows, and animals of different age, including  
424 heifers, calves, and adult animals. Different types of animals result in different manure generation  
425 rates and composition. Therefore, the different types of animals within each studied CAFO are  
426 normalized using the definition of animal units to estimate the amount and composition of the  
427 manure generated.

#### 428 *2.5.2. Scenarios description*

429 Two scenarios have been evaluated, the deployment of only phosphorus recovery systems, and  
430 the integration of these processes with AD and electricity production processes. Incentives for  
431 the recovery of phosphorus based on the work of Sampat et al. (2018) are considered, assuming  
432 a phosphorus credit value of 22 USD/kg<sub>P recovered</sub> for both scenarios. We note that this value  
433 is significantly lower than the economic impact of P release from livestock waste, valued in 74.5  
434 USD/kg<sub>P released</sub> (Sampat et al., 2021). Additionally, in the scenario considering the production  
435 biogas-based electricity, a value of Renewable Energy Certificates (fixed electricity selling price)  
436 of 60 USD per MWh generated is assumed. Finally, a discount rate of 7% is considered in both  
437 scenarios.

### 438 **3. Results**

#### 439 *3.1. Implementation of phosphorus recovery systems in the Great Lakes area*

440 Table 5 summarizes the results of the phosphorus recovery process selection in the Great Lakes  
441 area. It can be observed that only three out of the six commercial processes evaluated are selected to

442 be installed. All selected processes recover P in the form of struvite, which is a valued product that  
443 can be sold, generating income. Although the Ostara Pearl process also produces struvite, it results  
444 in larger operating costs than the technologies selected. Conversely, P-RoC recovers phosphorus in  
445 the form of calcium-based precipitates. This product lacks a well-established market, and therefore  
446 it does not generate income. In addition, P-RoC is the technology with the lowest TRL, which  
447 hampers the selection of this process. The selection of modular phosphorus recovery systems, such  
448 as MAPHEX, which due to economies of scale are especially suitable for small livestock facilities, is  
449 largely prevented by the absence of small-scale CAFOs. Therefore, a sub-set of three technologies  
450 is obtained. Therefore, it can be concluded that the selection of this pool of three technologies  
451 amongst the six systems evaluated is mainly driven by economic factors. Additionally, the low  
452 TRL of P-RoC also hampers the selection of this process.

453 The selection of the most suitable technology for each studied CAFO among the sub-set com-  
454 prised by Multiform, Nuresys, and Crystalactor systems is based on the CAFO scale and local  
455 eutrophication risk, as it is discussed in the following sections.

Table 5: Distribution and characteristics studied CAFOs, and phosphorus recovery processes selected. Only selected technologies are included in the table.

State	CAFO average size (animal units)	Number of CAFOs	Manure generated (ton/year)	P recovered (ton/year, (%))	Number of phosphorus recovery systems installed					
					Multiform		NuReSys		Crystalactor	
					S1	S2	S1	S2	S1	S2
Indiana	1,574.41	119	$2.48 \cdot 10^6$	1558.8 (78.7)	116	113	0	0	3	6
Michigan	2,461.52	144	$4.76 \cdot 10^6$	3004.4 (79.0)	127	113	16	30	1	1
Minnesota	634.23	1,487	$1.13 \cdot 10^7$	6938.1 (76.9)	1,477	1,476	0	0	10	11
Ohio	2,415.24	53	$1.68 \cdot 10^6$	1055.8 (78.6)	50	47	1	3	2	3
Pennsylvania	1,495.94	131	$2.59 \cdot 10^6$	1633.2 (78.9)	124	119	6	11	1	1
Wisconsin	2,628.19	283	$1.02 \cdot 10^7$	6510.5 (79.4)	262	255	6	7	15	21

S1: Phosphorus recovery systems only.

S2: Phosphorus recovery systems coupled with AD and electricity production.

### 456 3.1.1. Effect of CAFOs scale on selecting P recovery systems

457 A relationship between CAFOs size and the selected technologies can be observed in Table 5.  
458 This relationship is also observed in Figures 4 and 5. Multiform is the predominant phosphorus  
459 recovery process. Furthermore, we observe that in those states with smaller CAFOs (Minnesota

460 and Indiana) the selection of Multiform is more predominant than in states with larger CAFOs.  
 461 On the contrary, in the states with large CAFOs or with outliers representing large facilities, (such  
 462 as Ohio and Wisconsin) Crystalactor is selected for some facilities. Additionally, NuReSys is a  
 463 technology also selected for medium-size CAFOs.

464 The integration of biogas production and upgrading affects the selection of P recovery processes  
 465 as a consequence of the high investment expenditures associated to the installation of AD processes.  
 466 These large costs blur the capital investment differences between different P recovery processes. As  
 467 a result, the MDCA model promotes the implementation of technologies with better long-term  
 468 economic performance (lower operating costs), such as NuReSys and Crystalactor, in spite of the  
 469 fact that they involve larger investments costs than other technologies like Multiform, as shown in  
 470 Figure 4b.

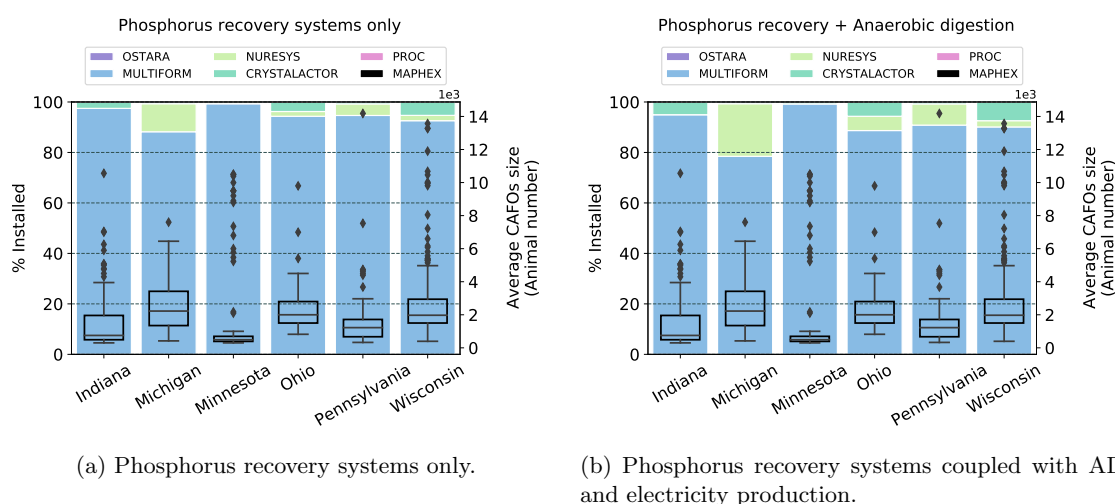


Figure 4: Distribution of the phosphorus recovery systems selected for the CAFOs in the Great Lakes area. The boxplots represent the distribution of CAFO sizes in each studied state.

471 Based on the data illustrated in Figures 5 to 7, a preliminary screening of P recovery systems can  
 472 be performed based on the size of the CAFOs. If the installation of only nutrient recovery systems  
 473 is considered, Multiform can be selected for CAFOs with sizes up to 5,000 animal units, NuReSys  
 474 can be selected for CAFOs with a size between 2,000 and 5,000 animal units, and Crystalactor is  
 475 selected for CAFOs larger than 5,000 animal units. For the scenario integrating anaerobic digestion

476 and phosphorus recovery processes, Multiform is mostly selected for CAFOs up to 4,000 animal  
477 units, although it is also selected in some larger CAFOs, NuReSys are mostly selected for CAFOs  
478 between 2,000 and 6,000 animal units, while the size range for the selection of Crystalactor is  
479 similar to the previous case. The operating costs are shown in Figure 6. It can be observed that  
480 the operating cost of Multiform is larger than NuReSys, and in turn the operating cost of this one  
481 is larger than Crystalactor, showing an opposite pattern than capital costs.

### 482 *3.1.2. Effect of local eutrophication risk on the selection of P recovery systems*

483 The results obtained reveal that CAFOs scale is the main driver for the selection of phosphorus  
484 recovery technologies. However, the role of the environmental vulnerability to eutrophication can  
485 be appreciated in those CAFOs where two different systems show similar economic performance.  
486 From the results illustrated in Figure 7, it can be observed that Multiform and NuReSys technolo-  
487 gies are selected for CAFOs with similar size. However, the economic performance of the second  
488 technology is better as consequence of the lower operating expenses and larger net revenues of this  
489 technology. Although both technologies have similar phosphorus recovery yield, Multiform shows  
490 better environmental performance since the eutrophication potential of its output streams is lower  
491 than NuReSys effluents. This difference in eutrophication potential between both technologies is  
492 mainly driven by the higher nitrogen recovery of Multiform. Therefore, in those locations that are  
493 highly vulnerable to nutrient pollution, the solution proposed by the COW2NUTRIENT framework  
494 is driven more by environmental criteria than by economic criteria, resulting in the selection of the  
495 Multiform process.

### 496 *3.2. Economic results*

497 The capital expenditures (CAPEX), operating expenses (OPEX), and net revenues (difference  
498 between incomes and operating expenses) associated with the deployment of the nutrient manage-  
499 ment systems are listed per state in Table 6. For the scenario considering the installation of only  
500 phosphorus recovery processes, the CAPEX and OPEX are 2,540.77 MM USD and 185.65 MM  
501 USD per year respectively. If the integration of biogas production and upgrading to power with  
502 phosphorus management is considered, the CAPEX and OPEX increase up to 5,192.29 MM USD

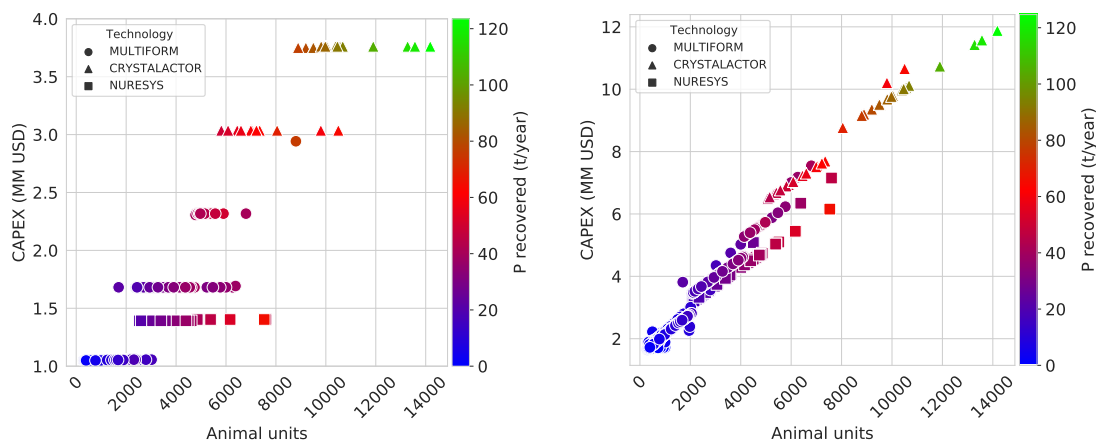
503 and 267.51 MM USD per year respectively. It can be observed that, due to the high CAPEX of  
 504 biogas production and upgrading stages, the net revenues decrease from 230.65 MM USD per year  
 505 for the scenario considering only phosphorus recovery systems to 95.77 MM USD per year if the  
 506 processes for phosphorus recovery and AD are combined.

Table 6: Economic results per state for installing phosphorus recovery systems in the studied states of the Great Lakes area.

State	CAPEX (MM USD)		OPEX (MM USD/year)		Net revenue (MM USD/year)	
	S1	S2	S1	S2	S1	S2
Indiana	145.58	325.00	21.18	34.16	19.32	11.88
Michigan	191.09	480.19	36.74	55.92	41.00	32.15
Minnesota	1,591.40	2,866.31	140.74	251.58	39.61	-46.15
Ohio	68.30	179.29	12.95	20.32	14.46	10.80
Pennsylvania	148.16	332.03	21.46	35.03	20.82	12.95
Wisconsin	396.24	1,009.47	73.55	117.80	95.44	74.14

S1: Phosphorus recovery systems only.

S2: Phosphorus recovery systems coupled with AD and electricity production.



(a) Phosphorus recovery systems only.

(b) Phosphorus recovery systems coupled with AD and electricity production.

Figure 5: Capital expenses for deploying phosphorus recovery systems in the studied CAFOs. The dots represent the P recovery technologies installed in the studied CAFOs.

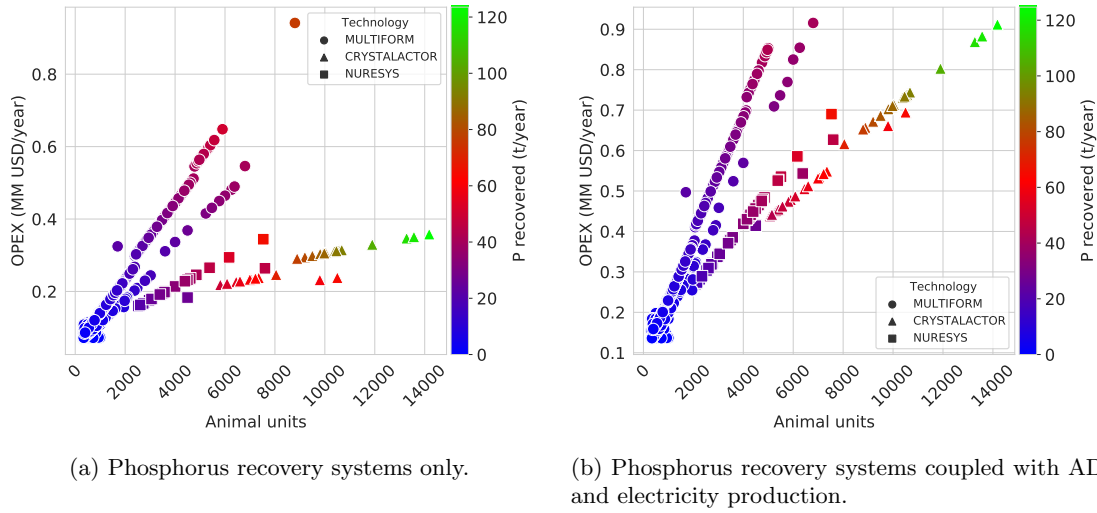
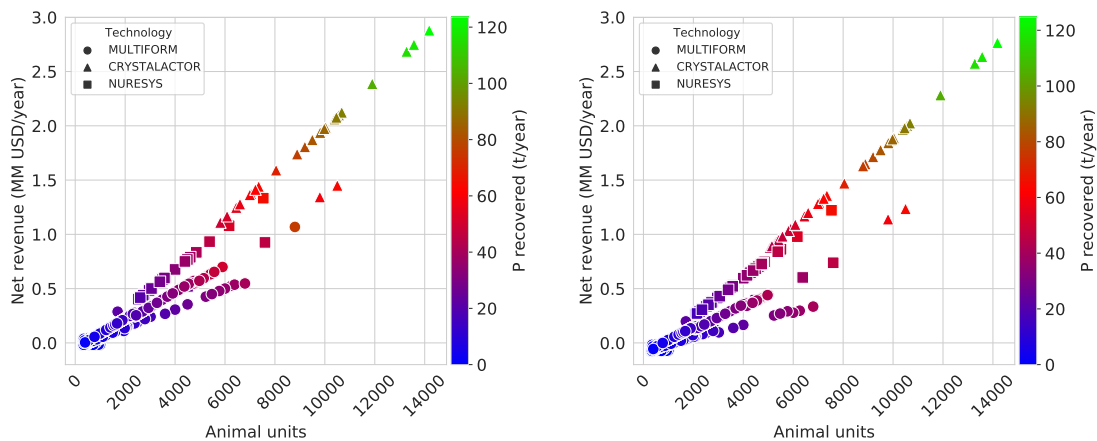


Figure 6: Operating expenses for deploying phosphorus recovery processes in the studied CAFOs. The dots represent the P recovery technologies installed in the studied CAFOs.

507 Figures 5 and 6 show the evolution of CAPEX and OPEX of the P recovery technologies installed  
 508 at the livestock facilities studied as a function of CAFOs scale. Figure 5a shows the CAPEX when  
 509 the implementation of only P recovery systems is considered. We observe that CAFOs are grouped  
 510 in sets selecting the same P recovery technology. This is because the manufacturers standardize  
 511 the size of each P recovery technology, which in turn determines the maximum waste processing  
 512 capacity of each technology (as shown in Table 3). This results in the use of the same P recovery  
 513 equipment, and thus the same CAPEX, for all the CAFOs generating waste below the maximum  
 514 processing capacity. Likewise, we note different CAPEX values for the implementation of the same  
 515 P recovery technology. This is a consequence of installing of multiple in-parallel P recovery units  
 516 to increase the processing capacity of such technology, since the waste generated in that CAFO  
 517 exceeds its maximum processing capacity. It can also be appreciated that CAFOs with similar  
 518 size might result in the installation of different technologies, or a different number of units of the  
 519 same technology. This is because, although CAFOs can have a similar number of animal units, the  
 520 type of the animals can be different, resulting in the generation of different amounts of manure.  
 521 In the case of considering biogas production and upgrading, illustrated in Figure 5b, the required

522 CAPEX increases significantly, blurring the differences in the capital investment between different  
 523 P recovery processes observed in Figure 5a into the cost of the whole system. The integration of  
 524 AD and electricity production also results in the increase of the OPEX, as shown in Figure 6.



(a) Phosphorus recovery systems only.

(b) Phosphorus recovery systems coupled with anaerobic digestion and electricity production.

Figure 7: Net revenue from the phosphorus recovery processes selected in the studied CAFOs. The dots represent the P recovery technologies installed in the studied CAFOs.

525 The net revenue of the installed nutrient management systems according with the economic  
 526 parameters described at the beginning of the section is shown in Figure 7. We observe a pattern  
 527 characterized by the increase of the net revenues with the increase of CAFOs size. However, the  
 528 implementation of P recovery technologies in CAFOs below 1,000 animal units, and below 2,000  
 529 animal units if biogas production and upgrading is also considered, result in economic losses.  
 530 Additionally, the integration of these processes slightly decreases the net revenues of the systems  
 531 installed for phosphorus recovery.

## 532 4. Discussion

### 533 4.1. Economic implications

534 In this work, fixed incentives for P recovery and biogas-based electricity generation have been  
 535 considered as starting point to explore the effect of the application of incentives in the imple-

536 mentation of P recovery technologies, either standalone or integrated with biogas production and  
537 upgrading processes. The results shown in Figure 7 reveal the effect of the economies of scale in  
538 the net revenues from the implementation of P recovery technologies in the Great Lakes area are  
539 highly dependent on the economies of scale, i.e., the larger the amount of waste to be treated,  
540 the larger the net revenues obtained. However, while for the largest CAFOs significant profits are  
541 obtained, negative revenues (i.e., economic losses) are obtained for the smallest CAFOs, even for  
542 large P credits prices such as 22 USD/kg<sub>P recovered</sub>. This suggests that the implementation of fixed  
543 incentives is not a fair policy, since the small CAFOs are not profitable while they increase the  
544 profits of the largest CAFOs. Therefore, alternative incentive policies must be explored. Sampat  
545 et al. (2019) studied the development of a coordinated management system for the treatment of  
546 cattle manure and P recovery. That framework captures the geographical phosphorus imbalance by  
547 proposing different prices for manure treatment that capture the regional remediation cost caused  
548 by P releases. They found that economic drivers are needed for a cost-effective recovery and re-  
549 distribution of phosphorus, considering fixed incentives for P recovery up to 50 USD/kg<sub>P</sub> for this  
550 purpose. Therefore, further research about the effect of implementing dynamic incentives for P  
551 recovery is needed. These incentive policies can follow different schemes, such as progressive in-  
552 centives for P recovery based on the amount of manure treated, or cooperative schemes where the  
553 profits from P recovery obtained by the largest livestock facilities are redistributed to the smallest  
554 CAFOs. This is a concept that has been studied for minimizing the costs of meeting greenhouse  
555 gases emission targets (Galán-Martín et al., 2018), and could be adopted for the reduction of P  
556 releases.

557 Furthermore, consideration should be given to the fair allocation of incentives in those scenarios  
558 where the available incentives budget is not enough to avoid economic losses in all CAFOs. In this  
559 regard, the fairness measure considered for budget allocation must be carefully selected among the  
560 existing schemes (Sampat and Zavala, 2019).

#### 561 4.2. Phosphorus use efficiency

562 Currently, manure or digestate in liquid phase is usually supplied as nutrient supplementation  
563 in croplands, or it is treated in either aerobic or anaerobic ponds. Solid phase processing is based on  
564 composting or drying. However, the high density of manure and digestate and low concentration of  
565 nutrient prevent an efficient redistribution of the phosphorus released from CAFOs to phosphorus-  
566 deficient areas (Burns and Moody, 2002). Therefore, the implementation of phosphorus recovery  
567 processes is a desirable measure for sustainable phosphorus management. We find that implement-  
568 ing struvite production processes considering incentives for P recovery of 22 USD/kg<sub>P recovered</sub> is  
569 economically feasible for CAFOs larger than 1,000 animal units if standalone P recovery technologies  
570 are implemented, and for CAFOs larger than 2,000 animal units if they are integrated with biogas  
571 production and upgrading processes. The requirement of large incentives to produce profit in most  
572 of the P recovery systems installed at CAFOs might raise the debate of whether it is worthwhile  
573 to implement P recovery systems; or if the economic resources should be allocated to simpler phos-  
574 phorus management alternatives, such as the redistribution of either raw or pond-stored manure.  
575 In this regard, Sampat et al. (2019) studied the separation of manure in liquid and solid phases,  
576 and their further transport to demanding allocations, considering a coordinated management sys-  
577 tem in Upper Yahara watershed (Wisconsin, United States). In addition, that study considered  
578 the implementation of economic incentives from 0 to 50 USD/kg<sub>P</sub>. However, the results showed  
579 that manure redistribution is not an economically viable technique for phosphorus recycling in this  
580 range of incentives. The main drawback of manure redistribution is the large transportation cost  
581 of both liquid and solid raw manure because of the high volume of these materials and their low  
582 phosphorus concentration. Therefore, the results reveal that on-site manure processing to generate  
583 valuable products (struvite) is more beneficial than manure redistribution.

584 The replacement of phosphorus from synthetic fertilizers by the recovered P, mitigating the  
585 dependency on fertilizers from non-renewable resources (phosphate rock), is an interesting alterna-  
586 tive towards the sustainability of the agri-food sector. However, phosphorus availability for plants  
587 depends on several factors, including the P product used as fertilizer and soil pH level. Since stru-  
588 vite is the product recovered in all studied CAFOs, we will focus the discussion on this product.

589 Vaneeckhaute et al. (2015) compared the bio-availability of several bio-based fertilizers, including  
590 struvite, to synthetic triple super phosphate (TSP). This study shows that P available in soil (mea-  
591 sured as Prhizon) was a 45% higher than TSP in acidic soils (pH=5.0), but 60% lower in slightly  
592 basic soils (pH=7.9). Based on these data, one kilogram of manure processed for P recovery by  
593 struvite production can replace from  $1.53 \cdot 10^{-3}$  to  $3.71 \cdot 10^{-3}$  kg of TSP ( $5.02 \cdot 10^{-3}$  kg of struvite  
594 are recovered per kilogram of manure processed). However, it must be noted that currently the  
595 cost of recovered P from manure (2.12-15.42 USD/kg<sub>P<sub>recovered</sub></sub>, see Table 3) is considerable larger  
596 than the cost of phosphorus from synthetic TSP (1.23 USD/kg<sub>P</sub>) (Index Mundi, 2020). As a result,  
597 from an economic perspective the complete substitution of phosphate rock is currently hindered  
598 by the large recovery costs, in addition to a limited availability of resources recovered from waste,  
599 and henceforth further exploration on resource recovery from different wastes is required to achieve  
600 P circularity reducing the recovery costs, and increasing the amount of phosphorus from organic  
601 waste, including but not limited to livestock manure.

## 602 5. Conclusion

603 We presented a framework for the techno-economic evaluation and selection of phosphorus re-  
604 covery systems considering the local vulnerability to phosphorus pollution through a GIS environ-  
605 mental model. A multi-criteria decision analysis model is used for the comparison and section of  
606 phosphorus recovery systems based on the economic performance and technological readiness level  
607 of the processes, and the eutrophication risk of the watershed where the studied CAFOs are located.  
608 Technologies for P recovery in the form of struvite are selected in all CAFOs studied. The selection  
609 of P recovery technologies is mainly driven by economic criteria, and the effect of the economies  
610 of scale is very significant. However, environmental criteria (P recovery efficiency, eutrophication  
611 potential of process effluents) are the decision criteria at some CAFOs where different technologies  
612 show similar economic performances. The results show that a preliminary screening of P recovery  
613 systems can be performed based on the size of CAFOs. Multifarm can be selected for CAFOs with  
614 sizes up to 5,000 animal units, NuReSys can be selected for CAFOs with a size between 2,000 and  
615 5,000 animal units, and Crystalactor is selected for CAFOs larger than 5,000 animal units. The

616 implementation of these systems in the Great Lakes area involves capital expenditures of 2.5 billion  
617 USD and operating costs of 186 million USD per year if only phosphorus recovery technologies  
618 are installed, and 5.2 billion USD and 268 million USD per year respectively if biogas production  
619 and upgrading are also considered. The implementation of fixed incentives of 22 USD/kg<sub>P recovered</sub>  
620 is considered to avoid economic losses due to P recovery costs impact in the economy of CAFOs.  
621 However, we find that that the implementation of fixed incentives is not a fair policy, since the small  
622 CAFOs are not profitable while they increase the profits of the largest CAFOs. The phosphorus  
623 recovered in the form of struvite from one kilogram of manure processed can replace from  $1.53 \cdot 10^{-3}$   
624 to  $3.71 \cdot 10^{-3}$  kg of synthetic triple super phosphate, but incurring in significantly larger production  
625 costs (2.12-15.42 USD/kg<sub>P recovered</sub>) than synthetic fertilizer (1.23 USD/kg<sub>P</sub>).

626 As part of future work, customized incentive policies adapted to the particularities of each live-  
627 stock facility can be proposed in order to optimize the allocation of limited monetary resources.  
628 Additionally, it would be interesting to analyze the potential of crop-livestock integration as an al-  
629 ternative for phosphorus recycling to the implementation of physicochemical P recovery processes.  
630 Another interesting research line is the integration of multiple processes in order to recover addi-  
631 tional valuable products from organic waste (such as biochar), adapting the concept of refinery to  
632 resource recovery from organic waste.

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**Declaration of interests**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

## **CRedit Authorship Contribution Statement**

**Edgar Martín-Hernández:** Conceptualization, Methodology, Software, Writing - Original Draft, Writing - review & editing, Visualization

**Mariano Martín:** Conceptualization, Supervision, Writing – Review & Editing, Funding acquisition

**Gerardo J. Ruiz-Mercado:** Conceptualization, Supervision, Writing – Review & Editing, Funding acquisition

