Theoretical Studies of Aqueous Systems above 25°C. 1. Fundamental Concepts for Equilibrium Diagrams and some General Features of the Water System.

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THEORETICAL STUDIES OF AQUEOUS SYSTEMS ABOVE 25°C. 1. FUNDAMENTAL CONCEPTS FOR EQUILIBRIUM DIAGRAMS AND SOME GENERAL FEATURES OF THE WATER SYSTEM.

Derek Lewis

SUMMARY

The illustration of thermodynamic data on aqueous systems is discussed and diagrams are described that are useful for bringing together the large numbers of data that are relevant to technological problems such as corrosion, mass-transport and deposition.

Two kinds of logarithmic equilibrium diagram are particularly useful, namely, diagrams depicting the variation with pH or pe of the concentrations of ionic species relative to that of a chosen reference ion and diagrams depicting the fields of conditions of pH and pe in which the various species in any given system predominate or are stable. Such diagrams clearly and concisely illustrate the data and greatly simplify the comparison of the states of a system at different temperatures.

Estimates of the equilibrium constants for the redox and the acid - base dissociation of water up to 375 °C are reported and some general features of aqueous systems at elevated temperatures are discussed

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INTRODUCTION

Only slow progress is being made in the experimental study of aqueous systems at elevated temperatures, partly because of difficulties that arise in the construction of apparatus such as autoclaves and electrode systems. For this reason, and because it is probably not practicable to study experimentally each of the very large number of systems and reactions of practical interest, it is important to develop theoretical methods for characterizing these systems.

A method has been described elsewhere [1] which enables reasonable estimates to be made of the equilibrium constants for reactions in aqueous systems at temperatures up to close to the critical temperature. It is based on the relations of classical thermodynamics and empirical equations for the variation with temperature of ionic heat capacity, derived from those for ionic entropy obtained by Criss and Cobble [2, 3]. The data that are needed are the standard entropies of the constituents at the reference temperature, the coefficients in the equations for their molar heats, and the value of the equilibrium constant at the reference temperature. These quantities have been determined experimentally for many species and reactions. Those that have not yet been so determined can often be estimated by means of thermodynamic or quasi-thermodynamic relationships [1, 4, 5].

Large numbers of equilibrium data must be considered together in the characterisation of most chemical systems and, especially in the definition of the conditions for the stability or the corrosion of different materials in various milieu, increasing attention is being paid to the construction of diagrams that concisely and clearly illustrate them [6 - 14]. The concept of the potential - pH diagram developed by Pourbaix [6] forms the basis of most of this work but other kinds of diagram, especially the logarithmic (double) activity or concentration diagrams extensively treated by Sillén [7] are also very useful, especially when the primary interest is in the relative concentrations of dissolved species. Only a little of the work on equilibrium diagrams for aqueous systems so far reported has related to temperatures above $100^{\circ}C$. In the studies to be described in this series of reports, work on the estimation of thermodynamic quantities for a number of aqueous systems at elevated temperatures and on their representation has been brought together and further developed. Diagrams are presented that clearly illustrate the equilibrium characteristics of the systems in a way that is useful in investigations of corrosion, mass-transport and deposition in power-plant working on the water-cycle. In this first report, the fundamental concepts used in the series are described and equilibrium data and diagrams for water up to 350°C are presented.

1. FUNDAMENTAL CONCEPTS FOR EQUILIBRIUM DIAGRAMS FOR AQUEOUS SYSTEMS.

Equilibria in aqueous media involving an oxidised species, A, and the conjugate reduced species, B, may be described generally by the formula:

$$aA + hH^{\dagger} + e^{-} = bB + wH_{2}O$$
 (r)

and the equilibrium constant at T^OK:

$$T_{r}^{K} = \{B\}^{b} \{H_{2}O\}^{w} \{A\}^{-a} \{H^{+}\}^{-h} \{e^{-}\}^{-1}$$

For dilute solutions in which the activity of water is likely to be close to unity a reasonable approximation is obtained when the concentrations of ionic species, [], are substituted for their activities, {}, so that

$$\log_{T} k_{r} = pe + hpH - \log[A]^{a} \cdot [B]^{b}$$
(1.1)

The quantity pe, a measure of "tension" [8], may conveniently be defined by means of the standard hydrogen electrode, like pH.

It follows from equation (1.1) that if the activities or concentrations of two of the species are fixed then a graph of corresponding values of the logarithms of the activities or concentrations of the other two species will describe a straight line. Quite generally, the several chemical equilibria in which a metal or other central species may be involved can be represented by a system of lines on one or another kind of logarithmic diagram [7].

1.1. Tension - concentration diagrams.

The tension - pH diagrams developed on the basis of the work of Pourbaix [6] on the illustration of equilibrium data relating to corrosion have hitherto been constructed with redox potential (volt) or some partial pressure parameter such as rH or $P(O_2)$ as the ordinate. A better method, particularly for treating and comparing systems at widely different temperatures, is to use pe as the conjugate of pH.

A number of benefits are obtained when chemical equilibria are formulated in terms of electron activity [15, 16, 17] instead of an electrical volt. Thus, for example, the elimination of the factor $RTF^{-1}\ln 10$ appearing in the Nernst relation simplifies equilibrium calculations and permits the construction of equilibrium diagrams in which the slopes of the lines depend only on the stoichiometry of the reactions they represent, and not also on the temperature. When it is necessary to evaluate the voltage, on any one of the several scales of potential now commonly used, that corresponds to a given value of pe use may be made of the relation

$$_{\rm T}\mathbf{\mathfrak{E}} = \mathrm{RTF}^{-1} \ln 10.\,\mathrm{pe}$$

where $_{T}$ is the potential (volt) relative to the standard hydrogen electrode. Some values for the factor $RTF^{-1}\ln 10$ in the range of temperature of concern here are given in the table below.

t^oC 50 100 150 200 250 300 350 (RTF⁻¹ln10)mV 64.12 74.04 83.96 93.88 103.8 113.7 123.6

Because of these benefits, and because the usage may assist in the development of a uniform description of electrochemical equilibria in media varying from dilute aqueous solution to molten salts [14], here, and in the similar publications that follow, tension - pH diagrams are constructed with pe as the ordinate. The diagrams so obtained are otherwise similar in principle to those first introduced by Pourbaix and his name is used to designate them. Thus, the field of the diagram is divided by lines describing equilibria into areas corresponding to the fields of conditions (domains) in which the several species in question are stable or otherwise, such as those in which a metal is immune or passive or subject to corrosion. A diagram of this kind illustrating data for the iron - water system at $25^{\circ}C$ [15] is shown in figure 1.

1.2. Relative concentration diagrams.

Other kinds of diagrams, such as those illustrating the concentrations of ionic species as a function of pH or pe, may often be a valuable complement to the Pourbaix diagram. Each such diagram might be regarded as a section of a three-dimensional figure showing the relations between the log concentrations of the species concerned, say log [i], and pe and pH, in a plane parallel to that containing the axes of log [i] and pH and intersecting the line pe = 0. The Pourbaix diagram then corresponds to the section (pe, pH)_{log [i]} = -6. Clearly this concept is of only limited usefulness in studies of systems at more than one temperature.

In the present work particular use will be made of relative concentration diagrams showing the variation with pH or pe of the concentrations of ions relative to that of a given reference species, $\log [i]/[ref]$. Figure 2. shows one such relative concentration diagram for the characterised species of iron in dilute aqueous solution at 25°C. It illustrates the variation with pH of the log ratio of the concentrations relative to that of Fe(OH)⁺ of Fe(VI), Fe(III) and Fe(II) species in oxidising milieu, under conditions of redox neutrality, and in reducing milieu.

1.3. Approximations in equilibrium diagrams.

In parts of the fields represented in equilibrium diagrams for a given system several aqueous species may coexist in similar concentrations. This has the result that ion-solid and ion-ion equilibria in these parts cannot strictly be represented by straight lines on the Pourbaix diagram or other logarithmic equilibrium diagram. Rectilinearity depends on the assumption that the total concentration of dissolved metal is the same as the concentration of the reacting ion, $[M]_{tot} = [i]$. When several mononuclear species coexist, as in a simple alternative to the presence of only a single ion, the total concentration of metal will be given by an expression of the form [7]:-

$$[M]_{tot} = [i](1 + \sum_{\beta_p} [H^{\dagger}]^{-p})$$

It seems likely that the application of corrections for the presence of more than one species in solution would make the construction of Pourbaix diagrams very much more complicated; the more so because the concentrations of individual ions in a mixture usually cannot be expressed explicitly in terms of total concentration and must be evaluated by iterative procedures.

One reasonable solution to this difficulty is to construct the Pourbaix diagram on the assumption that the concentration of the predominant species is equal to the conventional corrosion limit, 10⁻⁶ molal, and then to complement the Pourbaix diagram with a relative concentration diagram constructed assuming linearity. This scheme has been followed here.

Another usual assumption in the construction of equilibrium diagrams is that, as in the derivation of equation (1.1), the concentrations of ions can be taken instead of their activities. Clearly this is invalid for concentrated solutions such as those to which very high or very low pH numbers are assigned. In such solutions activity coefficients are likely to be so large, and to change so rapidly with pH, that concentration quotients will differ greatly from the corresponding equilibrium constants. For this reason no significance is attached here to lines in equilibrium diagrams based on concentration quotients when these lines extend beyond the limits pH = 1 and pH = 13. In the diagrams presented in this work such parts of lines beyond these limits as may be included for construction purposes are drawn dotted.

2.1. The stability domain of water.

The thermodynamic stability of aqueous systems is limited by the dissociation of water and by its reduction and its oxidation according to the reactions

$$H_{2}O(1) = H^{+} + OH^{-}$$
(W3)

$$\log_{298}k_{W3} = -14.00 [15]$$

$$H^{+} + e^{-} = \frac{1}{2}H_{2}(g)$$
(H1)

$$\log_{298}k_{H1} = zero$$

$$\frac{1}{4}O_2(g) + H^+ + e^- = \frac{1}{2}H_2O(1)$$
(O1)
$$\log_{298}k_{O1} = 20.79 \ [15]$$

Thus, for example, in a system containing no other oxidising agent the introduction of a metal with an equilibrium potential below that corresponding to a reversible hydrogen electrode in the same system leads to the reduction of water (and the oxidation of the metal) according to W3 and H1.

Corresponding to the reactions H1 and O1 the stability domain of water on a Pourbaix diagram is bounded by the lines

$$pe = \log_{T} k_{H1} - pH - \frac{1}{2} \log P(H_2)$$
 (a)

$$pe = \log_{T} k_{O1} - pH + \frac{1}{4} \log P(O_2)$$
 (b)

where $P(H_2)$ and $P(O_2)$ are the partial pressures of hydrogen and of oxygen, respectively. Thus the stability domain of water at 25°C corresponding to an equilibrium pressure of hydrogen or of oxygen of one atmosphere extends between the lines

$$pe = -pH$$
 and $pe = 20.79 - pH$

At any other temperature than 25°C, for a given equilibrium

pressure of hydrogen and of oxygen, the extent of the stability domain is determined by the magnitudes of k_{H1} and k_{O1} . Estimates of these quantities for temperatures up to 375°C have been obtained in this study from the data in table 1 by the method described previously [1]. They are given in tables 2 and 3. Table 4 gives estimates of $\log_T k_{W3}$ obtained in the same way (GIBBS K), together with estimates of this quantity obtained by interpolation between the values reported by Noyes [31]. The Pourbaix diagrams (incomplete) for the oxygen - water hydrogen system illustrating the results for 50°, 150°, 250° and 350°C are shown in figure 3.

The calculations leading to the estimates of equilibrium constants given here and in the following publications in this series have been performed by a computer with a simple program (TEMCON) giving tabulations of related equilibrium quantities for the reaction in question such as those reproduced in tables 2 and 3. The quantities under the column headings are:-

> 10 E 3 = $10^{3} T^{-1}$, VHOFF K = estimate of $\log_{T} k$ formed using the Van't Hoff isobar, HEAT H = 10^{-3} . $\int_{298}^{T} \Delta_{T} C_{P}^{o}$. dT, SIG TH = $10^{-3} (\Delta_{298} H^{o} + \int_{298}^{T} \Delta_{T} C_{P}^{o}$. dT), HEAT S = $\int_{298}^{T} \Delta_{T} C_{P}^{o} d \ln T$, TSIG TS = $10^{-3} T (\Delta_{298} S^{o} + \int_{298}^{T} \Delta_{T} C_{P}^{o} d \ln T)$, GIBBS K = estimate of $\log_{T} k$ formed using equation (1.1) E ZERO = $RF^{-1} \ln_{T} k$ (GIBBS K) x number of electrons involved

When the standard heat of formation has not been known for all the constituents the data for one constituent (usually $\Delta_{298}H_f^o(e^-)$) have been adjusted so that $\Delta_T H_r^o = 0$. In such cases a single value, $\log_{298}k$, appears repeatedly under VHOFF K.

For a partial pressure of one atmosphere of hydrogen or oxygen, the results obtained in this study indicate that the limits of the domain of stability of water are as follows

t ^o C	50	150	250	350
		pe l	· pH	
<u>reduction</u>	0.33	1.00	1.06	0.80
oxidation	19.18	14.43	11.18	8.70

Clearly, any physically significant partial pressure may be chosen in this connection and lower values than one atmosphere may be more relevant to discussions of corrosion in high-temperature systems such as, for example, those existing in water-cycle power-plant. Here, partial pressures of hydrogen and of oxygen have been chosen that, according to recently published solubility data [18], correspond to mole fractions of gas in the aqueous phase of, respectively, 0.8×10^{-6} and 8.0×10^{-6} . These concentrations represent the conditions that might exist in a 500 MWt boiler. For the temperatures here taken in illustration, the limiting partial pressures corresponding to the boundaries of the water domain, indicated by the broken lines on the Pourbaix diagrams in figure 2 and the similar figures that follow, are:

t ^o C	50	150	250	350
Р(Н ₂)	0.727	0.384	0.172	0.028
P(0 ₂)	0.885	0.468	0.211	0.035

2.2. The acid - base dissociation of water.

Regardless of the differences between the numerical values in table 4 for the dissociation constant of water, $T^{k}W_{3}$, obtained experimentally (Noyes) and theoretically (GIBBS K), it is well-established that this constant, like the dissociation constants of many weak acids and bases, passes through a maximum as the temperature increases. To the extent that the temperature coefficient of the dissociation constant differs for different substances the orders of acid and base strengths may change with temperature.

The condition for acid - base neutrality in aqueous solution, defined by equal concentrations of H^+ -ion and OH^- -ion, changes with temperature in accordance with the dissociation of water. In the Pourbaix diagram it corresponds to the line

$$pH_n = -\frac{1}{2}\log_T k_{W3}$$
 (d)

which, according to the data used here (GIBBS K), moves from pH 7.00 at 25° C through pH 5.57 at 275° C to pH 5.65 at 375° C.

Gurney [19] and, more recently, Helgeson [20] have shown how such maxima might arise as the resultant of opposed electrostatic and non-electrostatic contributions to the free-energy of dissociation. The electrostatic contribution may be related to the dielectric constant of water on the basis of the Born equation, and this constant decreases non-linearly with increasing temperature. Dissociation constants must then have a maximum value if, as is assumed, the non-electrostatic contribution does not vary with temperature or increases nearly linearly. The maximum would be expected to occur at different temperatures for different acids or bases, depending on the different relative magnitudes of the two contributions in different substances. For the dissociation of water the maximum might be expected to occur about 250°C because the temperature coefficient of the dielectric constant begins to increase rapidly above this temperature. Because of, among other things, the inadequacies of the Born model of ionic free energy [cf., 21 22 and the references therein] it is not clear to what extent this quasi-thermodynamic approach to dissociation in aqueous systems at elevated temperatures is valid.

2.3. The redox dissociation of water.

In some contexts it may be convenient to consider the conditions for redox neutrality as well as dissociative neutrality. For any system at equilibrium the pe of a reversible hydrogen electrode in the system is the same as that of a reversible oxygen electrode. Thus, from equations (a) and (b).

$$\log_{\mathrm{T}^{k}O1} + \frac{1}{4}\log P(O_{2}) = \log_{\mathrm{T}^{k}H1} - \frac{1}{2}\log P(H_{2})$$

and so, with the stoichiometric condition for redox neutrality $P(H_2) = 2 P(O_2)$,

$$\log P(O_2) = \frac{4}{3} (\log_T k_{H1} - \log_T k_{O1}) - \frac{2}{3} \log 2$$

Substitution for log $P(O_2)$ in equation (b) leads to the line described by pe at redox neutrality, viz,

pe =
$$\frac{2}{3} \log_{T} k_{O1} + \frac{1}{3} \log_{T} k_{H1} - 0.05 - pH$$
 (c)

Thus, according to the values for k_{H1} and k_{O1} obtained here, redox neutrality in dilute aqueous solutions corresponds to the conditions

t [°] C	25	50	150	250	350
pe+pH	13.80	12.85	9.90	7.75	6.02

Both tension (pe) and hydrogen-ion activity (pH) must usually be specified in comparisons of redox systems. In an attempt to simplify these comparisons Clarke and his coworkers introduced a single parameter, $rH = -\log P(H_2)$, as a measure of relative redox activity. It was intended that each and every potential on the line ε vs pH (cf. (a)) defined by the reversible hydrogen electrode should be designated by the single value of rH corresponding to the partial pressure of hydrogen determining the intercept of the line on the potential axis. Subsequently, other authors, recently including Robins [23], have more often used rH as a symbol for $-\log P(H_2)$ analogous to pH (and similarly rO for $-\log P(O_2)$). Clarke has himself pointed out the several undesirable consequences to which this misunderstanding leads, and has concluded [24] "In brief, rH has become an unmitigated nuisance".

2.4. Absolute neutrality in water.

Complete electrochemical neutrality or absolute neutrality in water corresponds to the point of intersection of the lines, (d) and

(c), describing acid - base neutrality and redox neutrality at the temperature in question. According to the results presented here, absolute neutrality prevails at the points

t ^o C	25	50	150	250	350
pH	7.00	6.64	5.83	5.58	5.62
pen	6.80	6.21	4.07	2.17	0.40

As Pourbaix has pointed out, the lines describing acid - base and redox neutrality divide the field of the general Pourbaix diagram into four regions corresponding to

I.	Oxidising acid media.	II.	Reducing acid media
III.	Reducing alkaline media.	IV.	Oxidising alkaline media

2.5. The principle features of the system.

For the present purpose it has not been necessary to consider the formation of other species in the oxygen - water - hydrogen system than H_2O , H^+ and OH^- , and such species as O_3 (aq), H_2O_2 (aq) and HO_2^- have been neglected.

The analysis presented here, although incomplete, gives useful information on the extent of the stability domain of H_2O , as well as on the conditions for acid - base dissociation and redox neutrality. As seen from figure 3., the extent of this domain decreases rapidly with temperature, being at 50°, 150° , 250° and $350^{\circ}C$, respectively, about 90%, 60%, 50% and 35% of its extent at $25^{\circ}C$. Clearly the stability domains of other substances in aqueous systems, such as metals and metal oxides, must decrease correspondingly.

CONCLUSION

Data on equilibria in aqueous systems at elevated temperatures, such as estimates of equilibrium constants obtained by a method based on the Criss and Cobble correspondence principle, can conveniently be illustrated by diagrams showing the relations between pe and pH, and between relative ionic concentration and pH, obtaining at equilibrium.

A marked feature of the oxygen - water - hydrogen system is the rapid decrease in the extent of the stability domain of liquid water with increasing temperature.

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			on water	<u> </u>	ogen byb	
Species	- ^A 298 ^G f cal.mol	$-\Delta_{298}H_{f}^{o}$ 1×10^{-3}	298 ^{5°}	a cal.m	$b \ge 10^3$ $co1^{-1}.deg^{-1}$	$c \ge 10^{-4}$
H ₂ (g)	0	0	31.2	6.52	0.8	1.2
H+	0	0	-5.0	0	92.25	0
OH-	37.6	55.0	2.5	0	-172.7	-
н ₂ 0(1)	56.7	68.3	16.7	18.03		-
H ₂ O ₂ (aq)	31.5	45.7	41.3 ^f	12.50	2.84	- 2.84 [†]
но <mark>-</mark>	15.6	-	25. 3 [*]	-	-114.4	-
0 ₂ (aq)	0	3.8	-	-	-	-
0 ₂ (g)	0	0	49.0	7.16	1.0	-4.0
0 ₃ (aq)	-	32.2	-	-	-	-
0 ₃ (g)	39.1	34.0	56.8	_	-	-

Table 1. <u>Thermodynamic constants and heat capacity parameters</u> for species in the oxygen - water - hydrogen system.

In this and the similar tables in following reports in the series, data for gases and solids have been taken from Kubaschewski and Evans [4]and for dissolved species from Latimer [5]. Exceptions are the b - parameters for ions which have been estimated as described in [1], and those indicated as follows:

- a. From N.B.S. 500 [25].
- b. From Latimer [5].
- c. Estimated using the equation of Couture and Laidler [26].
- d. Estimated using the equation of Powell and Latimer [27].
- e. Estimated using the equation of Latimer [28].
- f. Estimated using the equation of Cobble [29].
- g. From Pourbaix et al. [8].
- h. Estimated from the corresponding equilibrium constant and ΔG .
- † Data for $H_2O_2(g)$.
- * Estimated from $298\overline{S}^{\circ}(H_2O_2)$ by Pitzer's rule [5, 30].

REDN HYDROGEN ION

.

H+1 + E-1 = 0.5H2(9)

LOG298K =	0•0	SIGMA2985	=	20.60 S	IGMA298H =	0.0			
TEMP C	ТЕМР К	10E3/T	VHCFF	K HEAT H	SIG TH	HEAT S	T*SIGTS	GIBBS K	E ZERO
50.00	323.15	3.0945	0•0	-0.630	-0.630	-2.029	6.003	0.331	0.0212
75.00	348.15	2.8723	0.0	-1.318	-1.318	-4.079	5.754	0.583	0.0403
100.00	373.15	2.6799	0.0	-2.064	-2.064	-6.146	5.395	0.771	0.0571
125.00	398.15	2.5116	0.0	-2.867	-2.867	-8.228	4.928	0.906	0.0716
150.00	423.15	2.3632	0.0	-3.728	-3.728	-10.324	4.350	0.999	0.0839
175.00	448.15	2.2314	0.0	-4.646	-4.646	-12.432	3.663	1.056	0.0939
200.00	473.15	2.1135	0.0	-5.622	-5.622	-14.550	2.865	1.082	0.1016
225.00	498.15	2.0074	0.0	-6.655	-6.655	-16.677	1.957	1.083	0.1070
250.00	523.15	1.9115	0.0	-7.745	-7.745	-18.813	0.938	1.061	0.1101
275.00	548.15	1.8243	0.0	-8.893	-8.893	-20.956	-0.192	1.020	0.1109
300.00	573.15	1.7447	0.0	-10.099	-10.099	-23.106	-1.434	0.962	0.1094
325.00	598.15	1.6718	0.0	-11.362	-11.362	-25.263	-2.786	0.889	0.1055
350.00	623.15	1.6047	0.0	-12.682	-12.682	-27.425	-4.250	0.803	0.0993
375.00	648.15	1.5429	0.0	-14.060	-14.060	-29.593	-5.825	0.705	0.0907

0.2502(G)	+ H+1 +	- 5-1 =	0.5H20						
LOG298K =	20.788	SIGMA 298	S =	1.10 SIC	GMA298H = -	-34160.00			
TEMP C	TEMP K	10E3/T	VHCFF K	HEAT H	SIG TH	HEAT S	T*SIGTS	GIBBS K	E ZERO
50.00	323.15	3,0945	18.851	-0.535	-34.695	-1.722	-0.200	19.184	1.2300
75.CO	348.15	2.8723	17.192	-1.128	-35.288	-3.490	-0.830	17.783	1.2284
100.00	373.15	2.6799	15.755	-1.780	-35.940	-5.296	-1.564	16.543	1.2248
125.00	398.15	2.5116	14.499	-2.489	-36.649	-7.136	-2.401	15.435	1.2193
150.00	423.15	2.3632	13.391	-3.257	-37.417	-9.004	-3.343	14.433	1.2117
175.00	448.15	2.2314	12.407	-4.082	-38.242	-10.899	-4.389	13.520	1.2021
200.00	473.15	2.1135	11,527	-4.966	-39.126	-12.817	-5.542	12.681	1.1905
225.00	498.15	2.0074	10,735	-5,907	-40.067	-14.755	-6.800	11.906	1.1767
250.00	523.15	1.9115	10.019	-6.907	-41.067	-16.712	-8.165	11.184	1.1609
275.00	548.15	1.8243	9.368	-7.964	-42.124	-18.686	-9.637	10.509	1.1429
300.00	573.15	1.7447	8.774	-9.079	-43.239	-20.675	-11.216	9.873	1.1228
325.00	598.15	1.6718	8.230	-10.252	-44.412	-22.677	-12.903	9.273	1.1005
350.00	623.15	1.6047	7.729	-11.483	-45.643	-24.693	-14.699	8.703	1.0760
375.00	648.15	1.5429	7.267	-12.771	-46.931	-26.720	-16.602	8.160	1.0493

REDN OXYGEN

Table 3. TEMCON output. Estimates of the equilibrium constant and standard potential for the reduction of oxygen.

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<u>Table 4</u> .	. Values for the dissociation constant of water obtained									
	experimentally (Noyes) and by calculations (GIBBS K)									
	using thermodynamic data.									
t ^o C	25	50	150	250	350					
			$-\log T^k W3$							
Noyes	14.09	13.25	11.82	11.32	12.38					
GIBB S K	14.00	13.27	11.65	11.16	11.23					

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Figure 1. Tension - pH diagram for the Fe - H_2O system at 25°C.



Figure 2. Relative concentration diagram showing the concentrations relative to Fe(OH)⁺ of aqueous Fe(II), Fe(III) and Fe(VI) species in oxidising, redox neutral and reducing media at 25°C.



Figure 3. Pourbaix diagrams for the water system above 25° C.

1-360 (See back cover earlier reports.)

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