

Nonradioactive Air Emissions Modification to the Notice of Construction for the 200 Area Effluent Treatment Facility

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Department of Energy

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Richland, Washington 99352

Approved for Public Release

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TERMS

1	
2	
3	
4	ASIL acceptable source impact level
5	
6	CFR <i>Code of Federal Regulations</i>
7	
8	EPA U.S. Environmental Protection Agency
9	
10	ETF Effluent Treatment Facility
11	
12	GAC granulated activated carbon
13	
14	HEPA high-efficiency particulate air
15	
16	LERF Liquid Effluent Retention Facility
17	
18	NOC notice of construction
19	
20	SALDS State-Approved Land Disposal Site
21	
22	SQE small quantity emission
23	
24	TAPs toxic air pollutants
25	
26	T-BACT Best Available Control Technology for Air Toxics
27	
28	VOC volatile organic compound
29	
30	VOG vessel off-gas
31	
32	WAC Washington Administrative Code
33	

METRIC CONVERSION CHART

The following conversion chart is provided to the reader as a tool to aid in conversion.

Into metric units

Out of metric units

Into metric units			Out of metric units		
If you know	Multiply by	To get	If you know	Multiply by	To get
Length			Length		
inches	25.40	millimeters	millimeters	0.0393	inches
inches	2.54	centimeters	centimeters	0.393	inches
feet	0.3048	meters	meters	3.2808	feet
yards	0.914	meters	meters	1.09	yards
miles	1.609	kilometers	kilometers	0.62	miles
Area			Area		
square inches	6.4516	square centimeters	square centimeters	0.155	square inches
square feet	0.092	square meters	square meters	10.7639	square feet
square yards	0.836	square meters	square meters	1.20	square yards
square miles	2.59	square kilometers	square kilometers	0.39	square miles
square miles	259	hectares	hectares	0.00391	square miles
acres	0.404	hectares	hectares	2.471	acres
Mass (weight)			Mass (weight)		
ounces	28.35	grams	grams	0.0352	ounces
pounds	0.453	kilograms	kilograms	2.2046	pounds
short ton	0.907	metric ton	metric ton	1.10	short ton
Volume			Volume		
fluid ounces	29.57	milliliters	milliliters	0.03	fluid ounces
quarts	0.95	liters	liters	1.057	quarts
gallons	3.79	liters	liters	0.26	gallons
cubic feet	0.03	cubic meters	cubic meters	35.3147	cubic feet
cubic feet per minute	0.02832	cubic meters per minute			
cubic yards	0.76	cubic meters	cubic meters	1.308	cubic yards
Temperature			Temperature		
BTU/hour	2.93 E-4	kilowatts			
Fahrenheit	subtract 32 then multiply by 5/9ths	Celsius	Celsius	multiply by 9/5ths, then add 32	Fahrenheit

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**NONRADIOACTIVE AIR EMISSIONS
MODIFICATION TO THE NOTICE OF CONSTRUCTION
FOR THE 200 AREA EFFLUENT TREATMENT FACILITY**

1.0 FACILITY IDENTIFICATION AND LOCATION

U.S. Department of Energy, Richland Operations Office
Hanford Site
200 Area Effluent Treatment Facility
Richland, Washington 99352

The responsible manager's name and address are as follows:

Mr. T. K. Teynor, Director
Waste Programs Division
U.S. Department of Energy, Richland Operations Office
P.O. Box 550
Richland, Washington 99352
(509) 376-1366.

The 200 Area Effluent Treatment Facility (ETF) is an industrial waste water treatment facility located in the 200 East Area on the Hanford Site. Associated with the ETF are the Liquid Effluent Retention Facility (LERF), also located in the 200 East Area, and the State-Approved Land Disposal Site (SALDS) located in the 200 West Area. Figure 1 shows the locations of the 200 East and 200 West Areas within the Hanford Site. Figure 2 shows the locations of ETF, LERF, and SALDS within the 200 Areas.

2.0 BACKGROUND INFORMATION

This document serves as a modification to Notice of Construction (NOC) (DOE-RL 1992) pursuant to the requirements of WAC 173-400-110 and 173-460-040 for the expansion of approved influent streams to the ETF.

The ETF has an integrated system designed to treat a combination of dilute liquid waste streams generated on the Hanford Site by removing organic, inorganic, and radioactive contaminants. The ETF was designed to handle a maximum flow of 150 gallons per minute. The three waste streams in the original application were the 242-A Evaporator process condensate, the PUREX Plant process distillate discharge, and the PUREX Plant ammonia scrubber distillate. Although included in the design, the two PUREX Plant streams no longer exist and were eliminated when the decision was made to shut down the PUREX Facility.

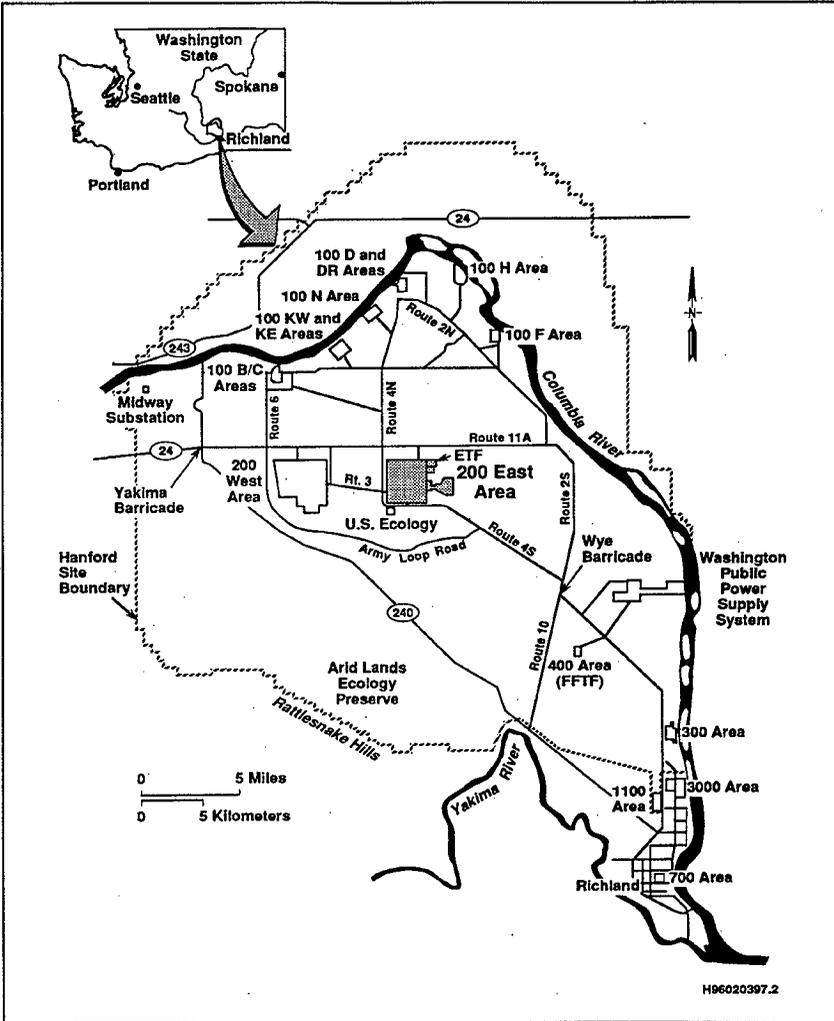


Figure 1. Hanford Site.

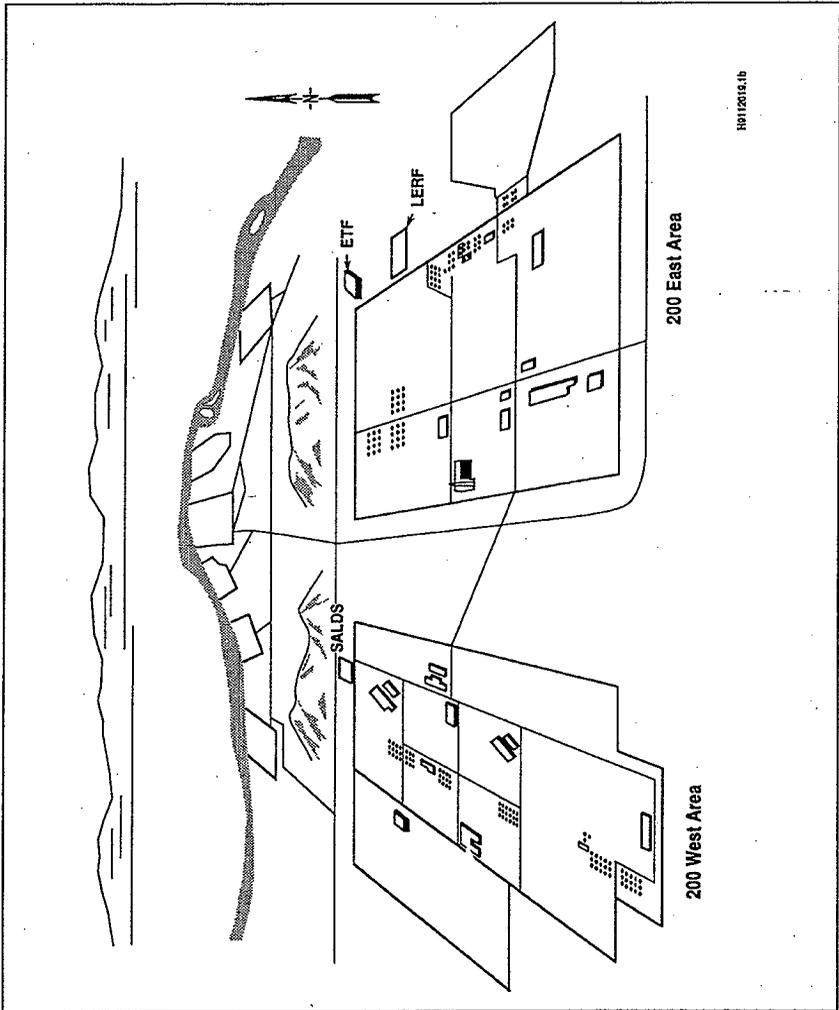


Figure 2. Locations of the 200 Area Effluent Treatment Facility, Liquid Effluent Retention Facility, and State-Approved Land Disposal Site in the 200 Areas.

1 The nonradioactive air emissions NOC application for ETF (DOE-RL 1992)
2 was submitted by the U.S. Department of Energy, Richland Operations Office
3 (DOE-RL) on February 4, 1993, and was approved by the Washington State
4 Department of Ecology (Ecology) (No. NOC-9393) on December 20, 1993. The
5 permit approval conditions for volatile organic compound (VOC) emissions were
6 limited to 0.50 gram per minute and 0.55 gram per cubic meter at standard
7 conditions, measured at stream number G6 of the ventilation offgas (VOG)
8 system. The initial feed stream was comprised of effluent from the
9 242-A Evaporator and the LERF. The approved NOC accepted the proposed
10 high-efficiency particulate air (HEPA) filters to control particulates.
11 Because of the very small emission levels, there were no controls proposed for
12 organic and inorganic vapors, which also were accepted. Ecology determined
13 that the proposal met best available control technology for air toxics
14 (T-BACT).

15
16 The State Waste Discharge Permit ST 4500, issued June 26, 1995, limited
17 the discharge to the SALDS to the effluent from the treatment of
18 242-A Evaporator process condensate. On June 14, 1996 (DOE-RL 1996a) the
19 DOE-RL requested Ecology to modify the permit to allow discharge by ETF to
20 SALDS of treated groundwater from the 200-UP-1 operable unit. Ecology made
21 modifications to the discharge permit to allow the 200-UP-1 groundwater as an
22 approved influent. Additional waste streams are being pursued in accordance
23 with Section G.4 of Permit ST 4500.

24
25 The Washington State Department of Health (DOH) regulates radionuclide
26 emissions under WAC 246-247. The addition of the 200-UP-1 groundwater and
27 N-Basin water waste streams to LERF and ETF was approved by DOH as a
28 streamlined NOC modification on June 11, 1996, which was later expanded to
29 include transfers from other locations.

30
31 This NOC modification involves a minor change in constituents, but no
32 change in treatment or T-BACT analysis. The LERF will not exceed acceptable
33 source impact levels (ASILS). The ETF will control VOC emissions to current
34 permit requirements. The ETF will use HEPA filters to control particulates,
35 as well as granulated activated carbon (GAC) filters to control VOC emissions.
36 The VOG filter unit includes a charcoal bed filter between the HEPA filters in
37 the VOG system; previously this was not included as VOC control equipment.

38
39 As an operational change, batch waste streams (e.g., minor changes in raw
40 material composition) from various locations on the Hanford Site will be
41 treated at ETF. The batches will be characterized and evaluated before
42 treatment to ensure that permit conditions are met. Following
43 characterization, the waste water will be transferred via truck from various
44 locations to the ETF truck unloading area, and accumulated at the LERF, if
45 necessary, before treatment at ETF. ETF has a treatment capacity of 216,000
46 gallons per day. The batch waste streams, anticipated to be a few thousand
47 gallons a few times a month, represent a small percentage of the approved
48 treatment capacity. The batch waste streams will meet the new source review
49 exemption found in WAC 173-460-040(2)(c).

50

1 The *State Environmental Policy Act of 1971* checklist that was prepared
2 for ETF in July 1992 was deemed adequate; no further information was required
3 for this NOC modification.
4
5

6 3.0 PROJECT INFORMATION

7
8
9 A description of the LERF and ETF processes, ventilation and emission
10 control systems, and monitoring is provided in the following sections.
11
12

13 3.1 PROCESS DESCRIPTION

14
15 The LERF was built before September 1991, for holding effluent from the
16 242-A Evaporator until ETF was constructed.
17

18 The LERF was built before the effective date of WAC 173-460, so an NOC
19 for nonradioactive emissions was not submitted. The LERF was included as part
20 of the process for 242-A Evaporator waste effluent to be treated at the ETF,
21 and is specifically listed as an approved effluent source for ETF in NOC-93-3.
22 The addition of new waste streams to LERF will not cause an increase in actual
23 toxic air pollutant (TAP) emissions. The design of the unit prevents TAP
24 emissions from exceeding the ASILS for any constituents, as discussed in
25 Section 4.2.1.
26

27 A detailed description of the ETF process is found in the original NOC
28 application (DOE-RL 1992). To summarize, the primary treatment train provides
29 for feed storage, suspended solids removal, ultraviolet/oxidation with
30 hydrogen peroxide, pH adjustment, degasification, reverse osmosis (RO),
31 ion-exchange polishing, final pH adjustment, and effluent storage. A
32 secondary treatment train provides evaporation of product solids (e.g. RO
33 reject and resin regenerating solutions) to dryness. All of the process
34 components contain vents that tie into the VOG (Figure 3).
35

36 As noted in the modification request for ST 4500 (DOE-RL 1996a),
37 inorganic compounds are treated at the ETF by a combination of reverse osmosis
38 and ion exchange with an overall removal efficiency between 99 and 99.9
39 percent for inorganic constituents of concern.
40

41 Organic compounds, such as carbon tetrachloride, are treated in several
42 locations at ETF. The majority are destroyed in the ultraviolet/oxidation
43 system. The VOC compounds not completely destroyed by the
44 ultraviolet/oxidation will be removed in the degasification system step and
45 captured on the VOG carbon filters. Finally, the RO unit is also effective in
46 treating organic compounds. As noted in the modification request for ST 4500
47 (DOE-RL 1996a), the ETF treatment systems should effectively treat the
48 expected concentration of carbon tetrachloride in the 200-UP-1 groundwater.
49
50

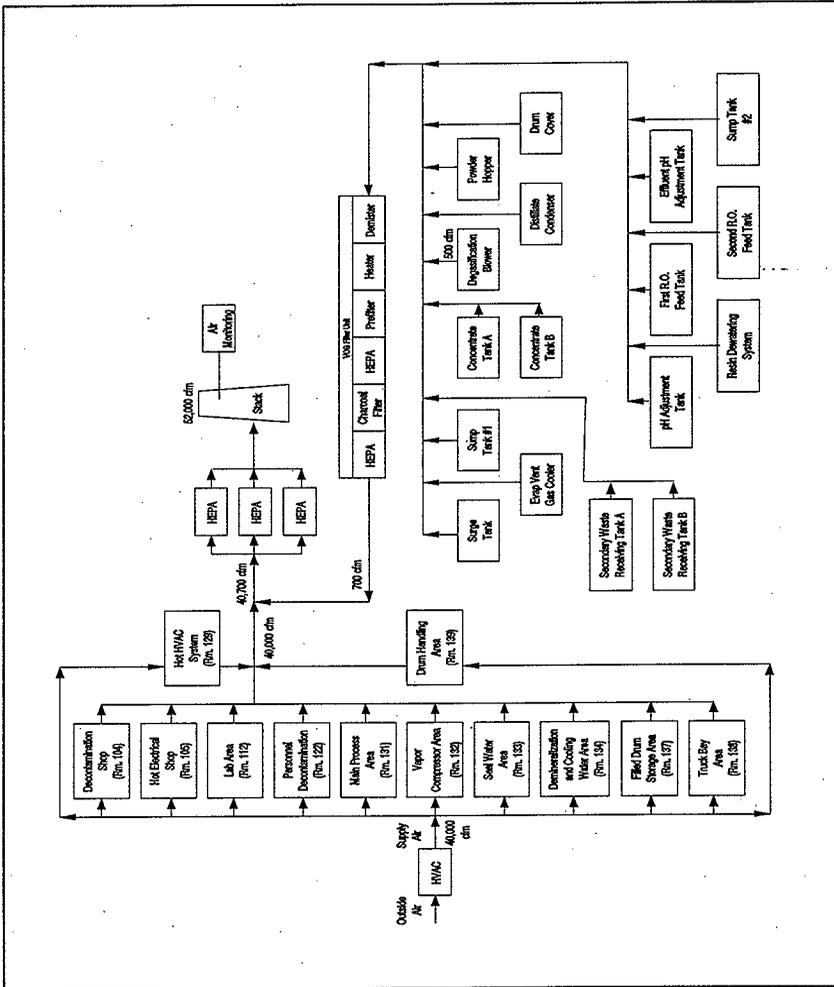


Figure 3. 200 Area Effluent Treatment Facility Ventilation and Emissions Control System Diagram.

1 **3.2 VENTILATION AND EMISSIONS CONTROL SYSTEM DESCRIPTION**
2

3 The LERF consists of three retention basins, each with a 6.5 million
4 gallon capacity. Each basin has a floating cover, with a relatively small,
5 passively vented breather space with intermittent use. The breather vents
6 operate at a maximum flow of 1 cubic foot per minute, whenever effluent is
7 transferred to the basins. Also, there are daily and seasonal cycles of
8 expansion and contraction that contribute to the passive ventilation at a
9 lower flow rate. Each breather vent is equipped with a drum containing
10 200 pounds of granulated activated carbon (GAC). The GAC canisters are
11 expected to last the life of the facility without requiring a changeout.
12

13 Gaseous emissions from ETF are controlled by the VOG system, which is
14 connected to each potential source of gaseous emissions. A slight negative
15 pressure in each tank and vessel where gaseous waste can be released prevents
16 any fugitive emissions. All collected emissions are treated before release.
17

18 The VOG system treats gaseous emissions through the VOG Filter Unit. The
19 filter unit contains a prefilter, a charcoal bed filter and two HEPA filters.
20 The VOG system is described in more detail in the original NOC application
21 (DOE-RL 1992).
22

23
24 **3.3 MONITORING DESCRIPTION**
25

26 Monitoring is performed at ETF within the VOG system after treatment and
27 before entry into the facility HVAC discharge system and before release from
28 the facility. The emissions from the VOG are monitored for temperature and
29 flow. Radioactivity is monitored continuously at the HVAC exhaust stack via a
30 paper filter sampler.
31

32 The performance tests for VOC emissions required by NOC-93-3 were
33 completed on January 23, 1996, and reported to Ecology (DOE-RL 1996b). Permit
34 conditions were met.
35

36
37 **4.0 EMISSIONS ESTIMATION**
38
39

40 The potential emissions for LERF and ETF are calculated by assuming the
41 entire volume of the two additional waste streams is at the highest
42 concentration found. Actual emissions are estimated for constituents of
43 concern based on removal efficiencies and transfer rates described in the
44 original NOC application (DOE-RL 1992) and the ST 4500 modification request
45 (DOE-RL 1996a). Emissions at either facility will not exceed ASILS for any
46 TAPs, so dispersion modeling will not be required.
47

48
49 **4.1 CRITERIA POLLUTANTS PER WAC 173-400-030**
50

51 Only one criteria pollutant, VOCs, has a potential to be emitted by LERF
52 or ETF. The increased potential to emit, based on total organic compound

1 concentrations in the proposed effluent waste streams, is less than 500
2 pounds, well below the Prevention of Significant Deterioration trigger level
3 of 40 tons per year specified in WAC 173-400-030.
4
5

6 4.2 TOXIC AIR POLLUTANTS PER WAC 173-460-080 7

8 The TAP emissions are anticipated to be in gaseous form. Tables 1 and 2
9 list the potential organic and inorganic TAP emissions from the proposed
10 200-UP-1 groundwater (26 million gallons) and the N-Basin water (1.4 million
11 gallons, including the emergency dump basin). The tables contain the list of
12 constituents, the maximum concentration in the untreated effluent, and whether
13 the constituent is a new TAP or an increase in concentration from a previously
14 listed TAP in the original NOC application (DOE/RL-92-69). If either
15 condition is true, the constituent's TAP class, ASIL, the corresponding small
16 quantity emissions (SQE) rate, and the potential mass inventory of each
17 constituent is also listed. The potential untreated mass of a constituent is
18 calculated by assuming all 27.4 million gallons of the untreated effluent was
19 at the highest concentration found in the 200-UP-1 groundwater, with the
20 exception of barium and lead. For these two constituents, which had a higher
21 concentration in the N-Basin water, a weighted average was used.
22

23 Constituents that have a mass in the untreated effluent that is less than
24 the SQE cannot exceed the SQE at the point of emission for either LERF or ETF,
25 and do not warrant further discussion. Constituents with a potential
26 inventory that could exceed the SQE, or if an SQE is not established, are
27 highlighted in the tables with shading, and are discussed in the following
28 section.
29
30

31 4.2.1 Toxic Air Pollutant Emissions from the Liquid Effluent 32 Retention Facility 33

34 Inorganic TAPs that potentially could exceed SQE rates (or where one
35 doesn't exist) include beryllium, cadmium, calcium, chromium, iron, lead,
36 nickel, and uranium. All of these constituents would exist as soluble salts,
37 with vapor pressures of zero. There is no potential for these constituents to
38 be released from LERF.
39

40 Organic TAPs that do not have SQE rates established include aldrin,
41 dieldrin, and heptachlor. Release fractions calculated from Henry's Law
42 constants are five to eight orders of magnitude lower than the potential
43 inventory release. Pesticides were detected only in one groundwater sample.
44 Even if the entire 27.4 million gallons of the two proposed waste streams had
45 the maximum concentration found, and assuming the breather vents operated at
46 1 cubic foot per minute continuously for an entire year, rather than

Table 1. Organic Toxic Air Pollutants Regulated Per WAC 170-460-080.

Constituent	Maximum concentration in untreated influent (ppb)	New or increased constituent on ETF TAPs NOC (yes/no)	Toxic Air Pollutant Class	ASIL (24 hour) (microgram per cubic meter)	SQE (lb/yr)	Untreated ETF mass 22.74 E-7 gal (lb/yr)
1,1,1-Trichloroethane	0.73	Yes	B	6400	43,748	0.167
1,1,2-Trichloroethane	0.31	Yes	B	180	22,750	0.0708
1,2-Dichloroethane	0.11	Yes	B	2700	10	0.0251
1,4-Dichlorobenzene	0.1	Yes	AI, AII	1.5	175	0.0228
4,4'-DDB	0.32	Yes	AI, AII	0.1	20	0.0731
4,4'-DDT	4.2	Yes	AI, AII	0.01	10	0.959
Acetone	100	No	N/A	N/A	N/A	N/A
Allyl in	1.8	Yes	AI, AIII	0.0002	None	0.411
Benzene	2	Yes	AI, AII	0.12	20	0.457
Carbon tetrachloride	440	Yes	AI, AII	0.067	10	161
Chloroform	6.8	No	N/A	N/A	N/A	N/A
m-Cresol	74	Yes	B	73	10,500	16.9
Dodecane	100,000	Yes	AI, AII	0.00022	None	0.845
Dibutyl in	4.4	Yes	N/A	N/A	N/A	N/A
Endrin	0.67	No	B	0.33	175	1.01
Endrin aldehyde	0.9	Yes	N/A	N/A	N/A	N/A
Ethyl benzene	1.7	Yes	B	1000	43,748	0.206
Heptachlor	2.5	Yes	AI, AII	0.00077	None	0.388
Methylene chloride	27	No	N/A	N/A	N/A	N/A
Pentachlorophenol	840	Yes	AI, AII	0.33	50	6.17
Phenol	0.62	Yes	B	63	10,500	192
Tetrachloroethane	180	Yes	AI, AII	1.1	500	0.142
Tetraedecane	0.6	No	N/A	N/A	N/A	N/A
Toluene	30,000	Yes	B	400	43,748	0.137
Tributyl phosphate	8	No	N/A	N/A	N/A	N/A
Trichloroethane	1.6	Yes	AI, AII	0.59	50	1.83
Xylenes (total)	1.7	Yes	B	1500	43,748	0.365
gamma-BHC (Lindane)	1.7	Yes	AI, AII	0.0026	0.5	0.388
Total organic carbon	2000	No				457
Total organic halogen	240	Yes				54.8

ETF = effluent treatment facility.

ppb = parts per billion.

TAPs = toxic air pollutants.

ASIL = acceptable source impact level.

SQE = small quantity emissions.

Table 2. Inorganic Toxic Air Pollutants Regulated Per WAC 170-460-080.

Constituent	Maximum concentration in untreated influent (ppb)	New or increased constituent on ETF TAPS NDC (Yes/no)	Toxic Air Pollutant Class	ASIL (24 hour) (microgram per cubic meter)	SOE (lb/yr)	Untreated ETF mass 82.7% E-7 gal (lb/yr)
Aluminum	240	No	N/A	N/A	N/A	N/A
Antimony	100	No	N/A	N/A	N/A	N/A
Barium (H-Basin @ 2590 ppb)	300	Yes	B	1.7	175	99.5
Beryllium	1.9	Yes	A1, A11	0.00042	None	0.232
Boron	70	No	N/A	N/A	N/A	N/A
Bromide	400	No	N/A	N/A	N/A	N/A
Cadmium	7.2	Yes	A1, A11	0.00056	None	1.64
Calcium	350,000	No	N/A	6.7	175	71,500
Chloride	59,000	No	N/A	N/A	N/A	N/A
Chromium	180	Yes	A1, A11	0.00083	None	4.1
Cobalt	5	No	N/A	N/A	N/A	N/A
Copper	790	No	N/A	N/A	N/A	N/A
Cyanide	10	No	N/A	N/A	N/A	N/A
Fluoride	4,000	No	N/A	N/A	N/A	N/A
Iron	9,400	Yes	B	3.3	175	2,153
Lead (H-Basin @ 3.3 ppb)	0.0	Yes	A1, A111	0.5	None	0.032
Magnesium	110,000	No	N/A	N/A	N/A	N/A
Manganese	33	No	N/A	N/A	N/A	N/A
Nickel	120	Yes	A1, A11	0.0021	0.5	26
Nitrate	1,700,000	No	N/A	N/A	N/A	N/A
Nitrite	12,000	No	N/A	N/A	N/A	N/A
Potassium	13,000	No	N/A	N/A-1	N/A	N/A
Silver	6.1	Yes	B	0.033	175	1.39
Sodium	59,000	No	N/A	N/A	N/A	N/A
Strontium	1,270	No	N/A	N/A	N/A	N/A
Sulfate	84,000	No	N/A	N/A	N/A	N/A
Sulfur	16,400	Yes	B	0.67	175	3,230
Vanadium	40	Yes	B	0.17	175	9.14
Zinc	330	Yes	B	0.033	175	75.4

ETF = effluent treatment facility.
 ppb = parts per billion.
 TAPS = toxic air pollutants.
 ASIL = acceptable source impact level.
 SOE = small quantity emissions.

1
2 intermittently for a shorter period, the total amount of pesticides that could
3 even challenge the GAC canisters is only about a gram. Releases of these
4 constituents are not considered feasible.
5

6 The only new constituent that has the potential to exceed an established
7 SQE is carbon tetrachloride. The 200-UP-1 groundwater has a potential
8 inventory of carbon tetrachloride of about 100 pounds. Most of this would
9 stay in the effluent that will be transferred to ETF, as it would not remain
10 at LERF long enough to escape. Even if the entire amount escaped through the
11 breather vents, the capacity of the GAC canisters is more than adequate to
12 capture all of it. The actual releases from LERF would be negligible. The
13 ASILS would not be exceeded for any TAP constituents for any waste stream
14 likely to be sent to LERF.
15

16 17 4.2.2 Toxic Air Pollutant Emissions from the 200 Area Effluent 18 Treatment Facility 19

20 Inorganic TAPs that could potentially exceed SQE rates (or where one
21 doesn't exist) include beryllium, cadmium, calcium, chromium, iron, lead,
22 nickel, and uranium. Calcium and chromium were discussed in Appendix B of the
23 original NOC application (DOE-RL 1992). Calculations for these two
24 constituents, present at 2,800 and 66 parts per billion, respectively, in the
25 242-A Evaporator process condensate, demonstrated that releases from ETF would
26 be below the ASILS or SQE rates. The ETF, processing this waste stream at a
27 maximum capacity of 150 gallons per minute for the entire year, would result
28 in a maximum concentration in the release of 2.8 E-6 micrograms per cubic
29 meter for calcium and 6.6 E-8 micrograms per cubic meter for chromium. With a
30 flowrate of 27,250 standard cubic feet per minute, this would correspond to an
31 annual release of 2.5 E-06 pounds per year for calcium and 5.9 E-08 pounds per
32 year for chromium. The maximum concentrations in the 200-UP-1 groundwater for
33 calcium and chromium were 330,000 parts per billion and 180 parts per billion,
34 respectively. Using the same transfer rate and mechanism, the maximum
35 concentration in the ETF release would be 3.3 E-04 micrograms per cubic meter
36 for calcium and 1.8 E-07 micrograms per cubic meter for chromium, both well
37 below the respective ASILS.
38

39 The same transfer rate (1 E-12 micrograms per cubic meter gaseous
40 effluent per parts per billion liquid effluent) applied to the other inorganic
41 constituents yields values well below ASILS.
42

43 Organic TAPs will be treated very effectively by ETF. The pesticides
44 (aldrin, dieldrin, and heptachlor) that do not have established SQE rates
45 should be destroyed completely by ultraviolet/oxidation. Because of the low
46 vapor pressures of these constituents, residual undestroyed levels would stay
47 in the water phase and be removed by the RO. It is unlikely that any
48 detectible amounts would even challenge the charcoal bed filter in the VOG
49 filter unit. Carbon tetrachloride also would be effectively treated. The
50 potential inventory from the 200-UP-1 groundwater is about 100 pounds. The
51 SQE rate for carbon tetrachloride is 10 pounds per year. The required removal
52 efficiency to stay under the SQE is 90 percent. As stated in the modification

1 request for ST 4500 (DOE-RL 1996a), the ETF treatment systems should remove
2 greater than 99.9 percent of the expected concentration of carbon
3 tetrachloride in the 200-UP-1 groundwater.
4
5

6 5.0 SCHEDULE

7
8
9 The piping changes needed to allow transfer of the 200-UP-1 groundwater
10 to LERF are scheduled to begin October 1, 1996 (no emission potential for this
11 phase). Treatment of the two new waste streams at ETF would begin as early as
12 January 1997.
13
14

15 6.0 REFERENCES

- 16
17
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