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Hot Oiling Spreadsheet

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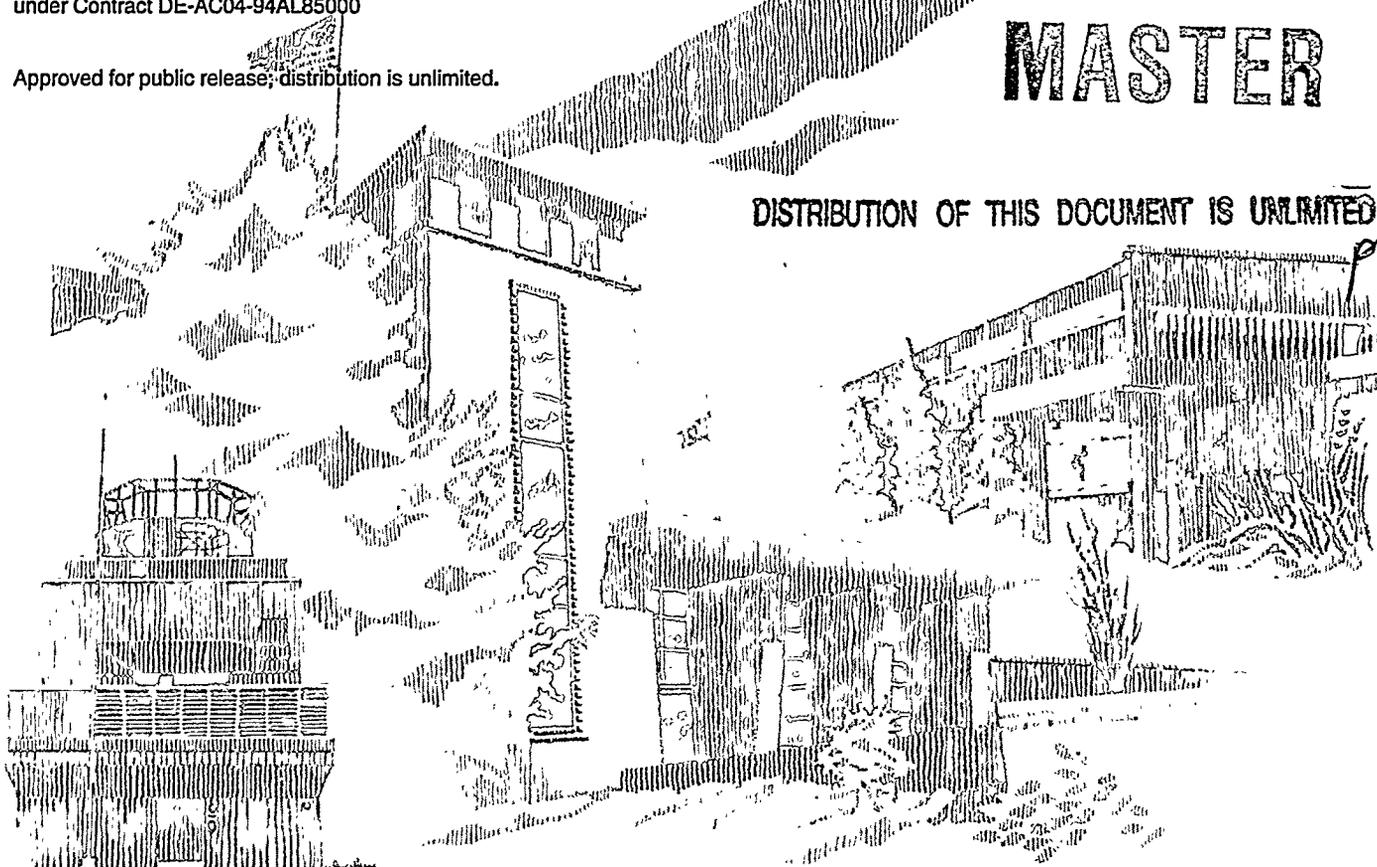
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under Contract DE-AC04-94AL85000

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SAND96-2247
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Hot Oiling Spreadsheet

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Abstract

One of the most common oil-field treatments is hot oiling to remove paraffin from wells. Even though the practice is common, the thermal effectiveness of the process is not commonly understood. In order for producers to easily understand the thermodynamics of hot oiling, a simple tool is needed for estimating downhole temperatures. Such a tool has been developed that was distributed as a compiled, public-domain-software spreadsheet. That spreadsheet has evolved into a interactive from on the World Wide Web (<http://www.sandia.gov/apt/>) and has been adapted into a Windows™ program by Petrolite, St. Louis MO. The development of such a tools was facilitated by expressing downhole temperatures in terms of analytic formulas. Considerable algebraic work is required to develop such formulas. Also, the data describing hot oiling is customarily a mixture of practical units that must be converted to a consistent set of units. To facilitate the algebraic manipulations and to assure unit conversions are correct, during development parallel calculations were made using the spreadsheet and a symbolic mathematics program. Derivation of the formulas considered falling film flow in the annulus and started from the transient differential equations so that the effects of the heat capacity of the tubing and casing could be included. While this approach to developing a software product does not have the power and sophistication of a finite element or difference code, it produces a user friendly product that implements the equations solved with a minimum potential for bugs. This allows emphasis in development of the product to be placed on the physics.

ACKNOWLEDGMENTS

This work performed at Sandia National Laboratories supported by the U.S. Department of Energy (DOE) under contract DE-AC04-76DP00789. The paraffin control study at Sandia, which the development of the Hot Oiling Spreadsheet was a part, was sponsored by the Natural Gas and Oil Technology Partnership, a DOE program of cooperative work between the national labs and industry. The industrial partner that worked with Sandia on the paraffin control work was Petrolite of St. Louis, Mo. The contributions of Ken Barker, the principal investigator at Petrolite, are gratefully acknowledged for his identification of the physical processes that control the effectiveness of hot oiling jobs.

INTRODUCTION

While hot oiling is a common oil field practice there is little appreciation of the thermal effectiveness of hot oiling. To change this situation a spreadsheet has been developed to estimate downhole temperatures during hot oiling. The spreadsheet was developed as an educational tool and makes a number of simplifying assumptions. If accurate predictions of downhole temperature are required, a more sophisticated code should be used.¹ The challenge was to develop user-friendly, interactive, public-domain software that will run on any PC. However, it is also important that the code be as physically accurate as possible. While there are a number of simple analytic models that have been used for predicting downhole temperatures during injection, drilling, or production,^{2,3} they make assumptions that are not valid for hot oiling. There are of course finite element or finite difference codes that could be adapted for the calculations, but this approach was not deemed to meet the user-friendly, interactive, and public-domain goals. A significant challenge in the development of this tool was insuring that the equations and unit conversions were correctly input into the spreadsheet. Spreadsheets while being user friendly to use are difficult to debug. Thus, as part of the verification of the spreadsheet, the equations were solved, including units, with a symbolic logic program (Mathematica, <http://www.wri.com/>) and the results were shown to be the same as the spreadsheet to three significant figures.

Initially the tool developed to satisfy these requirements was a DOS based compiled spreadsheet that executes as a stand-alone program (Figure 1). When World Wide Web technology became available, the spreadsheet was converted to a interactive form that can be accessed over the INTERNET at <http://www.sandia.gov/apt/> (Figure 2). The form launches a Visual Basic™ program that does the calculations based on the user's inputs and creates the hypertext document that is served back to the user. Petrolite of St. Louis MO has developed a Windows™ program based on the original DOS spreadsheet (Figure 3). All three of these tools allow the user to interactively input data and receive the results of the calculations either as a table or graph (Figure 4.).

The intent of this report is to document the assumptions, empirical formulas used, and other information about the spreadsheet. As such it is a collection of separate topics written to document various aspects of the spreadsheet. While it lacks completeness or flow from one topic to the next, its value to those who are already using the spreadsheet makes it important to publish it as rather than let the work go undocumented.

In a "hot oiling" job oil or water is injected down the annulus of an oil well in an attempt to melt paraffin that has deposited in the tubing. The heat capacity of the fluid injected is smaller than the heat capacity of the casing and tubing and there is heat loss to the surrounding rock. Thus the oil injected cools rapidly. The effectiveness of hot oil/watering depends on the depth to

which the tubing is raised above the melting point of the paraffin. Because of this rapid cooling of the injected fluid, the assumption of quasi-static equilibrium assumed in previous work needed to be investigated, thus the development of the spreadsheet started with the transient differential equations.

Sometimes Joule-Thomson cooling during production can cool the production interval enough to drop the temperature below the cloud point and cause paraffin to precipitate at the production interval. Being able to calculate if this happens can be important in analyzing paraffin problems and thus such calculations have been included in the spreadsheet.

The development of a practical approach to estimating hot oiling temperatures has involved a number of various investigations which constitute the sections of this document:

- **SPREADSHEET EMPIRICAL FORMULAS:** establishing empirical formulas for fluid properties, falling film flow, heat transfer coefficients, and heat loss to the earth,
- **QUASI-STATIC APPROXIMATION:** investigation of quasi-static equilibrium assumption for case of no flow in the tubing,
- **DERIVATION COUNTER-FLOW EQUATIONS:** derivation of counter flow equations assuming quasi-static equilibrium, but accounting for the depth the thermal transient penetrates the well from the surface,
- **JOULE-THOMSON COOLING:** development of approach for calculating the temperature of gas flow up the annulus during production.
- **VERIFICATION OF HOT OILING SPREADSHEET:** verification of hot oiling and hot watering calculations with field data.

SPREADSHEET EMPIRICAL FORMULAS

Average Fluid Temperature

The average fluid temperature is used to calculate fluid viscosity and density. It thus has an effect on the thermal properties, such as, heat transfer coefficients. The user can replace the formula with a numerical value iteratively to assure calculations are self consistent. It is important, however, to recognize that once a formula in a cell is replaced by a numerical value input, the formula is gone and the spreadsheet must be reloaded to recover the formula. The value assumed is (nomenclature defined at end of report)

$$T_{avg} = T_{ho} / 2 + T_s / 4 + T_{bh} / 4 .$$

Oil Viscosity

The spreadsheet calculates oil viscosity in two steps: first, oil viscosity at 60 °F, and then, oil viscosity at "average fluid temperature." This allows the user to change the oil viscosity at 60 °F, while still using the formula to correct viscosity for temperature. The oil viscosity at 60 °F is calculated from the oil gravity using the Beggs and Robinson⁴ correlation. The oil viscosity at average fluid temperature is calculate as

$$\mu_o = \frac{(\text{oil viscosity @ 60 }^\circ\text{F}) * (\text{oil viscosity as per Beggs and Robinson})}{(\text{oil viscosity @ 60 }^\circ\text{F as per Beggs and Robinson})}$$

Thus, if the user does not alter the cell for oil viscosity at 60 °F, the denominator and first factor in the numerator in the above formula cancel and the oil viscosity at average fluid temperature is merely that of Beggs and Robinson's correlation. If the spreadsheet user enters a numerical value for viscosity at 60 °F, then the oil viscosity at average fluid temperature becomes Beggs and Robinson's correlation times the ratio of the oil viscosity at 60 °F entered by the user to the oil viscosity predicted by Beggs and Robinson's correlation at 60 °F.

Beggs and Robinson's correlation calculates oil viscosity from oil gravity and temperature. For gas-free oil their correlation is:

$$\mu_o = -1 + 10^{\left(1077.46 * 10^{-0.02023 \gamma_o T^{-1.163}}\right)} .$$

Water Viscosity

The viscosity of water can be estimated from a formula of Hawkins et al.:⁵

$$\mu_w = \frac{2.185}{0.04012 T_{avg} + 0.000005111547 T_{avg}^2 - 1} .$$

Oil Density

The density of oil is calculated from the oil gravity using a value for the coefficient of thermal expansion recommended by Farouq Ali:⁶

$$r_o = \left(\frac{62.36 \text{ lb} / \text{ft}^3 141.5}{131.5 + g_o} \right) \left(1 - \frac{0.0005}{^\circ F} (T_{avg} - 60^\circ F) \right) .$$

Water Density

The density of water is calculated from the average temperature using the following formula by Farouq Ali:⁶

$$r_w = \frac{1}{0.01602 + 0.000023 * (-6.6 + 0.0325 * T_{avg} + 0.000657 * T_{avg}^2)} .$$

Thermal Conductivity of Oil

The thermal conductivity of oil was calculated as proposed by Cragoe:⁷

$$k_o = 1.62(1 - 0.0003(T_{avg} - 32^\circ F)) / \gamma_o .$$

Heat Capacity of Oil

The heat capacity of oil was calculated from Gambill's⁸ relation:

$$C_o = (0.388 + 0.00045 T_{avg}) \rho_o / \sqrt{\gamma_o} .$$

Heat Capacity of Water

The heat capacity of water was calculated from Farouq Ali 's formula⁶

$$C_w = r_w * (1.0504 - 0.000605 * T_{avg} + 1.79 * 10^{-6} * T_{avg}^2) .$$

Approximate Area and Wetted Perimeter for Fluid Falling in Annulus

It is assumed that at the beginning of a hot oil/watering job that the annulus is filled with gas and that the fluid injected falls down the annulus. The tubing is assumed to be against the side of the casing as shown on Figure 5.

The wetted perimeter in Figure 5 is approximately proportional to the square root of the area occupied by the fluid:

$$P \approx \beta \sqrt{A_1}, \quad \text{where} \quad \beta = \sqrt{4\pi \frac{R_{ci} + R_{to}}{R_{ci} - R_{to}}}$$

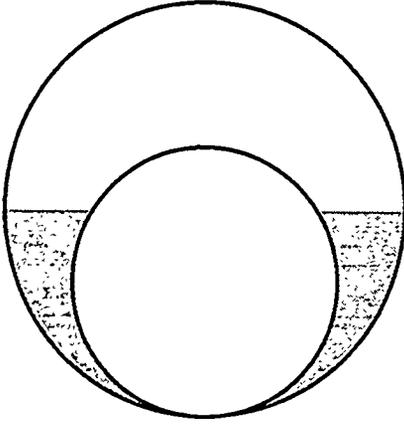


Figure 5: Position of tubing within casing showing area (shaded region) occupied by fluid.

For channel flow the Chézy formula⁹ relates velocity, friction factor, wetted perimeter, and area:

$$v^2 / \left(\frac{8g}{f} \right) = A_1 / P$$

The Reynolds number and friction factor can be written in terms of the area as

$$\text{Re} = \frac{4\rho Q_1}{\mu\beta\sqrt{A_1}} \quad \text{and} \quad f = 0.184 \text{Re}^{-0.2} = 0.184 \left(\frac{4\rho Q_1}{\mu\beta\sqrt{A_1}} \right)^{-0.2}$$

These equations can be combined and solved for the area to get

$$A_1 = 2.4 \sqrt{Q_1^2 \left(\frac{0.184\beta}{8g} \right) \left(\frac{4\rho Q_1}{\mu\beta} \right)^{-0.2}}$$

Annular Heat Transfer Coefficient

The annular heat transfer coefficient can be calculated using the following formulas:¹⁰

$$D_h = 4A_1 / P$$

$$\text{Re} = D_h \langle v \rangle \rho / \mu$$

$$\langle v \rangle = Q_1 / A_1$$

$$P_r = C\mu / k$$

$$\text{Nu}_d = 0.0296 \text{Re}^{0.8} \text{Pr}^{1/3}$$

$$h = \text{Nu}_d k / D_h$$

Heat Loss to the Earth

Ramey² showed how the heat lost to the earth can be approximated by a parameter

$$A[t] = \frac{Q_1 C [k + R_{co} U_{co} f(t)]}{2\pi R_{co} k}$$

where C is the heat capacity of the fluid in the annulus, k is the conductivity of the surrounding earth, and U is the overall heat transfer coefficient as discussed by Willhite.¹¹ For hot oil/watering jobs, U is typically large enough that $f(t)$ is closer to a constant temperature than constant flux boundary condition. The analytic solution for this boundary condition is¹²

$$f(y) = -\left(\frac{4}{\pi^2}\right) \int_0^\infty e^{-y^2 z^2} \frac{dz}{z [J_0^2(z) + Y_0^2(z)]},$$

which can be approximated as ($y < 5$):

$$f(y) \cong \frac{1}{(\pi y)^{-1/2} + 0.35 - 0.067(y/\pi)^{1/2}}$$

For hot oil/watering jobs the time of heat transfer is short enough that the difference in thermal conductivity of the "cement" surrounding casing and the earth can be important. This can be corrected for using the following empirical equation:

$$f(y) \rightarrow f(y) \frac{m + (k_c / k_e) f^2(y) \cdot (1 - k_c / k_e)}{m + f^2(y) \cdot (1 - k_c / k_e)}$$

where k_c is the conductivity of the cement, k_e is the conductivity of the earth, and

$$m = (1.976 - 1.69 R_{co} / R_h) \ln [R_h / R_{co}] .$$

Joule-Thomson Cooling

For oil and water free gas expanding from a high formation pressure to a low flow-line pressure the Joule-Thomson cooling can be approximated as

$$\Delta T_{J-T} = (0.048^\circ F / \text{psi}) \Delta P .$$

QUASI-STATIC APPROXIMATION

Including the effects of the heat capacity of the fluid in the annulus results in the following time dependent generalization of Ramey's differential equation:

$$\frac{\partial T}{\partial z} + \varepsilon \frac{\partial T}{\partial t} + \frac{\text{sign}}{J \cdot C} + \frac{T - T_e}{A[t]} = 0$$

where Q is positive for flow down the well and negative for flow up the well, $\text{sign} = 0$ for liquid flow in the well, $\text{sign} = -1$ for gas flow down the well, $\text{sign} = +1$ for gas flow up the well, and

$$\varepsilon = A_1 / Q_1$$

$$T_e = a \cdot z + T_s$$

Let

$$T = a \cdot z + T_s + F_0[t] + B[z, t]$$

where $B[z, t]$ is a function that goes to zero far from where fluid enters the well and $F_0[t]$ is a function governing the shift in temperature of a flowing well with no fluid injection, thus

$$F_0[0] = 0$$

$$T|_{z=0} = T_{ho}$$

The equation can be solved by Laplace transform techniques to give

$$F_0[t] = -\left(\frac{a}{\varepsilon} + \frac{\text{sign}}{C\varepsilon J}\right) \frac{\int_0^t e^{\int_0^{t'} 1/(\varepsilon A[t']) dt'} dt'}{e^{\int_0^t 1/(\varepsilon A[t]) dt}} \quad \text{and}$$

$$B[z, t] = \frac{T_{ho} - T_s - F_0[t - \varepsilon \cdot z]}{e^{\int_{t-\varepsilon z}^t 1/(\varepsilon A[t]) dt}}$$

Unfortunately these integrals can not be solved in closed form. In the quasi-static approximation, these integrals are solved assuming that $A[t]$ is a constant independent of time and then the appropriate time dependent value of $A[t]$ is plugged into the approximate solutions. For constant $A[t]$ or the quasi-static approximation, the above expressions become

$$F_{0qs}[t] \rightarrow -\left(\frac{a}{\varepsilon} + \frac{\text{sign}}{C\varepsilon J}\right) A\varepsilon [1 - e^{-t/(A\varepsilon)}] \quad \text{and}$$

$$B_{qs}[z, t] \rightarrow \frac{T_{ho} - T_s - F_{0qs}[t - \varepsilon \cdot z]}{e^{-(z/A)}}$$

for $z < t/\varepsilon$ and zero for $z > t/\varepsilon$. The depth t/ε is the depth the transient solution has propagated

down the well. Note: if the quasi-static approximation is made to the differential equation (Ramey's formulation) the temperature disturbance continues to infinity. Thus, one important addition to Ramey's solution is to cut it off at t/ϵ .

To test the adequacy of this approximation the integral solution was numerically integrated using the following approximation for $A[y]$:

$$A_{approx.}[y] = 33.2(Ln[874y + \pi])^2 .$$

In order to do the numerical integration it is necessary to assume a value for ϵ . The value assumed was 0.0004. The conclusion is not significantly dependent upon the ϵ assumed as was demonstrated by varying the value of ϵ . Figure 6 compares numerically integrated solution with the quasi-static approximation. The figure shows discrepancies, but $F_o[t]$ appears quite good for small times -- hot oil/watering jobs typically have $t < 1$. The plot of the quasi-static $B[z,t]$ shows a square shoulder at the cutoff depth, where as, the numerically integrated solution is rounded. Fortunately, the depth the spreadsheet needs to be accurate is back up the well above the "thermal front" (~500 ft) where the increase in temperature is high enough to be above the wax melting point. At these depths the error in the quasi-static solution is only a few percent.

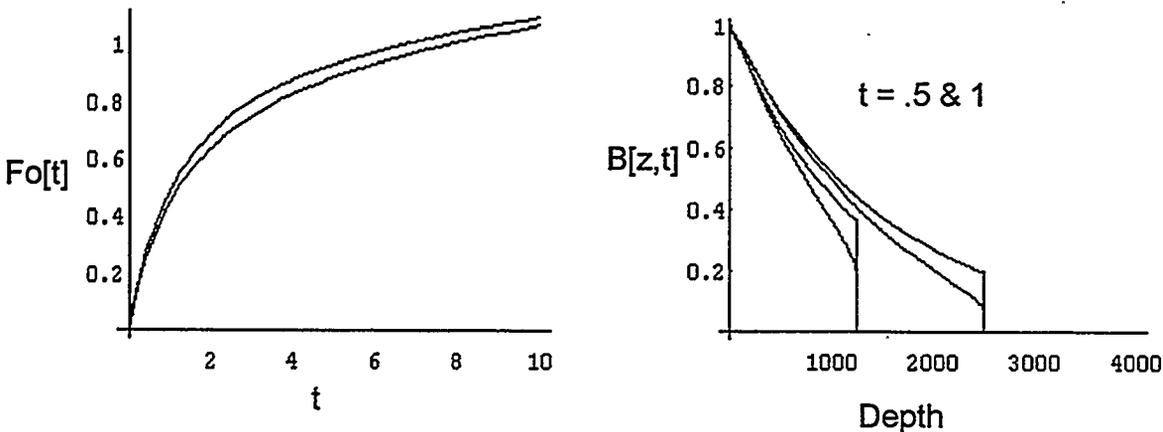


Figure 6: Comparison of quasi-static solution and numerically integrated solution.

The above equations apply when the annulus has fluid in it. At the beginning of a hot oil/watering job the annulus is typically empty. Clearly below the depth the fluid has fallen or reached, there will be no change in temperature. The depth t/ϵ is the depth to which the thermal front has advanced down the well. This depth will be less than the depth the fluid has fallen.

The case considered here is for a single flow stream, down the annulus only. When there is flow down the annulus and up the tubing the problem becomes more complex and the time dependent equations can not be solved in integral form. However, the evaluation of the quasi-static solution above indicates that it can be used, provided that the transient solution is cutoff at the right depth.

DERIVATION OF COUNTER-FLOW EQUATIONS

During a hot oil/watering job, fluid flows down the annulus and up the tubing; thus the well acts like a counter-flow heat exchanger. The thermal effectiveness of a hot oil/watering job can be analyzed using the temperature of the fluid in the tubing-casing annulus, T_1 , and rod-tubing annulus, T_0 , and the temperature of the earth, T_e (see Figure 7). The importance of the steel in the rods, tubing, and casing is that the steel absorbs heat from the fluid or changes the heat capacity of the system. The rate of heat flow up or down the well, for example $-Q_1 C \frac{\partial T_1}{\partial z}$ for the tubing-casing annulus, is unaffected by the steel, but the rate a given volume of fluid cools, for example $-A_1 C \frac{dT_1}{dt}$ for the tubing-casing annulus, needs of be adjusted to account for the heat absorbed by the steel, i.e., $A_1 C \rightarrow \sum (A_s C_s + A_1 C)$. The discussion of the quasi-static approximation for a single-flow stream showed that this adjustment affects the depth the thermal transient penetrates the well, but not the curvature of the profile above the cutoff. For counter flow, the depth the thermal transient in the tubing-casing annulus penetrates the well affects the lower boundary condition of the fluid in the rod-tubing annulus, but this effect is minor.

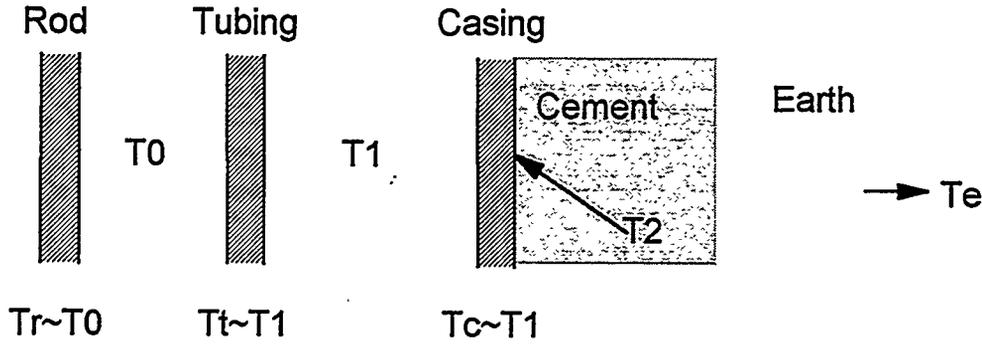


Figure 7: Temperatures important in analyzing thermal effectiveness of a hot oil/watering.

The time dependent equations governing the balance between radial transport of heat and flow of heat up and down the well are

$$-Q_1 C \left(\frac{\partial T_1}{\partial z} - \varepsilon_1 \frac{\partial T_1}{\partial t} \right) = 2\pi R_{co} U_{co} (T_1 - T_2) + 2\pi R_u U_u (T_1 - T_0)$$

$$-Q_0 C \left(\frac{\partial T_0}{\partial z} + \varepsilon_0 \frac{\partial T_0}{\partial t} \right) = 2\pi R_u U_u (T_0 - T_1)$$

where the heat capacity terms combine the capacity of the fluid and steel

$$-Q_1 C \varepsilon_1 = \sum (A_s C_s + A_1 C)$$

$$-Q_0 C \varepsilon_0 = \sum (A_r C_r + A_t C)$$

According to Ramey the heat flux at the outside of the casing can be prescribed as

$$2\pi R_{co} U_{co} (T_1 - T_2) = \frac{2\pi k_e}{f(t)} (T_2 - T_e) .$$

k_e is the conductivity outside the casing assuming homogeneity, i.e., no contrast in thermal properties between the cement and the earth. The section on empirical formulas gives a correction for the effect of the cement. This correction is important because at the beginning of a hot oil/watering job the radial thermal disturbance only penetrates the cement where as at the end of the job it penetrates out into the earth. The correction was determined by solving the inhomogeneous radial heat flow equation using a finite difference method. Solving this last equation for T_2 , the temperature at the casing cement boundary, and substituting in the first two equations gives

$$\frac{\partial T_1}{\partial z} + \varepsilon_1 \frac{\partial T_1}{\partial t} + \frac{T_1 - T_e}{A[t]} + g_1 (T_1 - T_e) = 0$$

$$\frac{\partial T_0}{\partial z} + \varepsilon_0 \frac{\partial T_0}{\partial t} + g_0 (T_0 - T_1) = 0$$

where

$$A[t] = \frac{Q_0 C (k_e + R_{co} U_{co} f(t))}{2\pi R_{co} U_{co} k_e}$$

$$g_1 = 2\pi R_{ci} U_{ci} / Q_1 C$$

$$g_0 = 2\pi R_{ci} U_{ci} / Q_0 C$$

In the quasi-static approximation these equations are solved assuming A is a constant and then the appropriate time dependent value of $A[t]$ is plugged back into this solution. The determination of $A[t]$ involves particular assumptions about the boundary condition for heat flow into the formation. Of course to solve the real problem properly and avoid the a priori assumed boundary condition for $A[t]$, one should include the radial heat flow equation in the above set. The solution to that equation involves Bessel functions and the problem becomes very complex. To address the issue of whether the radial heat flow equation can be solved separate from the above equations, the results of this work were compared with finite difference code calculations.

The quasi-static assumption can be used to reduce the above equations to static equations provided the solution is cutoff at the right point. It is assumed that the down hole pump does not

introduce any thermal transients and that below the heat-front propagating down the well from the surface, temperatures are in equilibrium with the earth, i.e. for $z^* \varepsilon_1 > t$ that $T_1 = T_0 = T_e$. With these assumptions the differential equations reduce to

$$\frac{\partial T_1}{\partial z} + \frac{T_1 - T_e}{A[t]} + g_1(T_1 - T_0) = 0$$

$$\frac{\partial T_0}{\partial z} + g_0(T_0 - T_1) = 0$$

subject to the boundary conditions $T_1|_{z=0} = T_{h0}$ and $T_0|_{z=t/\varepsilon} = T_e$. There is thus a moving boundary condition for the fluid in the tubing. The solution to the above set of equations is conceptually straight forward but algebraically complex. They are most readily solved by assuming functions of the right algebraic form and using a symbolic mathematics program to solve the resulting equations for the coefficients and boundary conditions. Below the cutoff point $T_1 = T_2 = T_e$. Above the cutoff point t/ε

$$T_1 = T_e + c_1 \cdot e^{-d \cdot z} + c_2 \cdot e^{-j \cdot z} - A[t] \cdot a(1 + g_1 / g_0)$$

$$T_0 = T_e + e_1 c_1 \cdot e^{-d \cdot z} + e_2 c_2 \cdot e^{-j \cdot z} - A[t] \cdot a(1 + g_1 / g_0) - a / g_0$$

where

$$d = \frac{1}{2} \left(\frac{1}{A[t]} + g_0 + g_1 - \frac{Y^{1/2}}{A[t]} \right)$$

$$j = \frac{1}{2} \left(\frac{1}{A[t]} + g_0 + g_1 + \frac{Y^{1/2}}{A[t]} \right)$$

$$e_1 = \frac{1}{2} \left(1 + \frac{1}{A[t]g_1} - \frac{g_0}{g_1} + \frac{Y^{1/2}}{A[t]g_1} \right)$$

$$e_2 = \frac{1}{2} \left(1 + \frac{1}{A[t]g_1} - \frac{g_0}{g_1} - \frac{Y^{1/2}}{A[t]g_1} \right)$$

$$c_1 = - \frac{-ae^{\left(\frac{dt}{\varepsilon} + \frac{jt}{\varepsilon}\right)} - ag_0 A[t] e^{\left(\frac{dt}{\varepsilon} + \frac{jt}{\varepsilon}\right)} + ae_2 g_0 A[t] e^{\frac{dt}{\varepsilon}} - ag_1 A[t] e^{\left(\frac{dt}{\varepsilon} + \frac{jt}{\varepsilon}\right)}}{\left(e_1 g_0 e^{\frac{jt}{\varepsilon}} - e_2 g_0 e^{\frac{dt}{\varepsilon}} \right)}$$

$$+ \frac{-ag_1 A[t] e^{\left(\frac{dt}{\varepsilon} + \frac{jt}{\varepsilon}\right)} + ae_2 g_1 A[t] e^{\frac{dt}{\varepsilon}} + e_2 g_0 T_{ho} e^{\frac{dt}{\varepsilon}} - e_2 g_0 T_s e^{\frac{dt}{\varepsilon}}}{\left(e_1 g_0 e^{\frac{jt}{\varepsilon}} - e_2 g_0 e^{\frac{dt}{\varepsilon}} \right)}$$

$$c_2 = aA[t] - c_1 + \frac{aA[t]g_1}{g_0} + T_{ho} - T_s$$

$$Y = 1 - 2A[t]g_0 + A[t]^2 g_0^2 + 2A[t]g_1 + 2A[t]^2 g_0 g_1 + A[t]^2 g_1^2$$

JOULE-THOMSON COOLING

The quasi-steady state heat balance for the production interval, Δz , accounting for Joule-Thomson cooling of gas as it expands from the formation into the tubing-casing annulus is

$$\left\{ -2\pi R_{co} k_e \frac{dT}{dr} \Delta z + T_2 \sum QC \right\} + \left\{ -T_1 \sum QC \right\} = \left\{ (QC)_{gas} \Delta T_{J-T} \right\}$$

{radial heat flow into the well}
+ {heat flow up the well} =
{J-T cooling}

where

$$\sum QC = (QC)_{oil} + (QC)_{gas} + (QC)_{water}$$

According to Ramey¹

$$-2\pi R_{co} k_e \frac{dT}{dr} = \frac{2\pi k_e \Delta T}{f(t)}$$

Substituting the last equation into the first and solving for ΔT , the observed temperature change or $T_2 - T_1$ gives

$$\Delta T = \frac{(QC)_{gas} \Delta T_{J-T}}{\sum (QC) + \frac{2\pi k_e \Delta z}{f(t)}}$$

After a day of production the second term in the denominator typically becomes small. That is, after a day, the observed cooling ΔT levels off and

$$\Delta T \rightarrow \frac{(QC)_{gas} \Delta T_{J-T}}{\sum (QC)}$$

When a well is produced with oil and water pumped up the tubing and gas flowing up the tubing-casing annulus, heat transfers across the tubing much easier than from the casing to the earth. Thus the oil, water, and gas can be assumed to be in thermal equilibrium with each other, but may be at a temperature different than that of the earth. The equations governing heat lost to the earth are thus

$$-\sum (-QC) \frac{\partial T_1}{\partial z} - \frac{Q_{gas}}{J} = 2\pi R_{co} U_{co} (T_1 - T_2) \quad \text{and}$$

$$2\pi R_{co} U_{co} (T_1 - T_2) = \frac{2\pi k_e}{f(t)} (T_2 - T_e)$$

Solving the second for T_2 and substituting in the first gives

$$\frac{dT}{dz} + \frac{Q_{gas}}{\sum (QC) J} + \frac{T - T_e}{A_g [t]} = 0$$

where

$$A_g [t] = \frac{\sum (QC) (k_e + R_{co} U_{co} f(t))}{2\pi R_{co} U_{co} k_e}$$

For production with Joule-Thomson cooling at the formation the boundary condition is

$$T|_{z=D} = T_e|_{z=D} - \Delta T_{J-T} .$$

The solution to the differential equation with this boundary condition is

$$T_g = a \cdot z + T_s - a \cdot A_g[t] - \frac{A_g[t] Q_g}{J \sum(QC)} + \left(a \cdot A_g[t] + \frac{A_g[t] Q_g}{J \sum(QC)} - \Delta T_{J-T} \right) e^{(D-z)/A_g[t]}$$

VERIFICATION OF HOT OILING SPREADSHEET

While the physics included in the calculations done by the Hot Oiling Spreadsheet is basic, there is always questions as to whether a set of calculations includes the right physics and is the physics coded correctly. To address these questions, a series of field tests were done in attempt to verify the Hot Oiling Spreadsheet. At the time these field tests were started, there was no practical way to measure downhole temperatures during hot oiling. Hence, a parallel effort to develop downhole rod coupling temperature monitors was initiated. The development of these is documented as part of the Applied Production Technology home page on the INTERNET (<http://www.sandia.gov/apt/>). These were only available for limited use during the verification of the spreadsheet. Unfortunately, no verification has been done of the Joule-Thomson cooling calculations.

Field tests of the heat transfer that occurs during hot oiling or hot watering were made by setting a bridge plug between the perforations and bottom of the tubing so that fluid could be circulated without entering the formation. The temperature was logged before the experiment to determine the geothermal temperature. Temperature was recorded inside the tubing at 300 feet while hot fluid was circulated and immediately after circulation was stopped the temperature in the tubing was logged. Before the test, the well was filled with oil, circulated, and allowed to equilibrate. At the end of the first day the oil was displaced with water. The next day hot water was circulated. Thus, the thermal disturbance from circulating the oil had a day to dissipate before hot water was circulated. Radial heat flow calculations indicate that the temperature increase due to the hot oil should be down to ~ 5% the next day.

Figure 8 shows the geothermal temperature measured before the work began (squares with an x). It was winter, hence the cooling of the first 100 feet near the surface. Note, however, there also is a change in gradient near 2000 feet. Thus assuming a constant geothermal gradient introduces some error in the calculations. The assumed geothermal temperatures are shown by the straight line on the figure.

Figure 9 compares the temperature logged immediately after circulating oil with that predicted by the spreadsheet. The curves marked Tubing and Annulus were calculated by the spreadsheet. The curve marked 1 BPM is that measured. The calculations were done using Version 2 of the spreadsheet with one change: the equations were modified so that the annulus was full of fluid at the beginning of the job. The figure shows that the temperature measured inside the tubing at the end of the job is close to what the spreadsheet predicts for the tubing temperature, but is systematically less. In making this calculation, none of the typical input parameters (thermal properties of the earth, etc.) were changed from the defaults in the spreadsheet. While the discrepancy is no more than expected due to uncertainties in the typical

input parameters, the nature of the discrepancy suggests that it may be due to ignoring the surface casing. Overall, the maximum discrepancy, at the end of this long job, is only about 10 °F, which is within the uncertainty due to the typical input parameters or within the accuracy the spreadsheet was designed to give.

Figure 10 shows temperature as a function of time 300 feet down the tubing taken with a downhole rod coupling temperature monitor. The agreement between the spreadsheet and measured data is quite good. As before, the typical input parameters were not changed from the defaults in the spreadsheet. The calculations shown do not consider the surface casing which is set at 341 feet or below the depth of the measurement. Including surface casing improves agreement. The figure assumes that the process began when the first measurement was taken. However, since heat had already reached 300 feet the hot oiling truck must have been started some time earlier. Accounting for this will shift the measured data to the right improving the agreement.

Figure 11 compares the temperature logged immediately after circulating water with that predicted by the spreadsheet. One additional change in the spreadsheet was made for these calculations: the fluid in the tubing was assumed to be water rather than oil. At first glance the agreement does not appear to be as good as for oil circulation; if, however, the surface temperature is raised 5°F to account for the heat left over from the day before, the agreement for hot watering is just as good as for hot oiling.

In conclusion, the spreadsheet has been shown to be a reasonable tool for estimating hot oiling and hot watering downhole temperatures.

CONCLUSIONS

The goal in developing the Hot Oiling Spreadsheet was to provide a public-domain, user-friendly program for evaluating the effectiveness of hot oiling jobs. The success in meeting such a goal is determined by how much the program is used by the customer, the oil patch. Sandia has received over 200 requests for copies of the spreadsheet. Further, a number of companies have written indicating they make their own copies and distribute them as part of in-house training. Recognition of the value of the spreadsheet as an educational tool resulted in requests from industry to place the hot oiling spreadsheet on the INTERNET. Petrolite, St. Louis MO, has used the physics documented here to develop a Windows™ version of the spreadsheet for use in their paraffin control schools. Short articles on the Sandia's work on paraffin control including the spreadsheet have appeared in the Oil & Gas Journal, World Oil, and The American Oil & Gas Reporter. Thus there has been a high recognition of the value of the spreadsheet by the customer and the goals set in developing the spreadsheet have been met. This recognition of the value of the spreadsheet has been the impetus to document the physics of the spreadsheet in this report.

NOMENCLATURE

a	Geothermal gradient, °F/ft,
A[t]	A function governing heat transfer to the earth,
A _g [t]	A function governing heat transfer to the earth during production,
A ₀	Area of fluid in the rod-tubing annulus, ft ² ,
A ₁	Area of fluid in the tubing-casing annulus, ft ² ,
A _s	Area of steel in the tubing and casing, ft ² ,
A _r	Area of fluid in the rods, ft ² ,
C	Heat capacity of fluid, Btu/lb-°F,
C _s	Heat capacity of steel, Btu/lb-°F,
D _h	Hydraulic diameter, ft,
f	Friction factor (Moody or Darcy),
g	Acceleration of gravity, ft/sec ² ,
J	Mechanical equivalent of heat, 777.97 lb-ft/Btu,
k	Fluid thermal conductivity, Btu/ft-hr-°F,
h	Heat transfer Coefficient, Btu/ft ² -hr,
k _c	Cement thermal conductivity, Btu/ft-hr-°F,
k _e	Earth thermal conductivity, Btu/ft-hr-°F,
Nu _d	Nusselt number,
P	Wetted Perimeter, ft ² ,
P _r	Prandtl number,
Q _g	Gas production rate, lb ³ /min,
Q ₀	Rod-tubing annulus volume flow rate, lb/min,
Q ₁	Tubing-casing annulus volume flow rate, lb/min,
R _{ci}	Casing inside radius, ft,
R _{co}	Casing outside radius, ft,
Re	Reynolds number,
R _h	Radius of hole, ft,
R _{ti}	Tubing inside radius, ft,
R _{to}	Tubing outside radius, ft,
r	radial distance, ft,
t	Time, hr,
T	Temperature, °F,
T _{avg}	Average fluid temperature, °F,
T _e	Temperature of the Earth, °F,
T _g	Gas temperature during production, °F,
T _{ho}	Temperature of injected fluid, °F,
T _r	Mean rod temperature, °F,
T _s	Mean surface temperature, °F,
T _t	Mean tubing temperature, °F,
T _c	Mean casing temperature, °F,
T _{bh}	Bottomhole temperature, °F,
T ₁	Temperature of the oil in the annulus between the casing and the tubing, °F,

T_0	Temperature of the oil inside the tubing, °F,
T_2	Temperature at the outside of the casing, °F,
U_{ti}	Overall heat-transfer coefficient at inside of tubing, Btu/day-ft ² -°F,
U_{co}	Overall heat-transfer coefficient at outside of casing, Btu/day-ft ² -°F,
z	Depth, ft,
v	Velocity, ft/min,
α	Thermal diffusivity, ft ² /day ($\alpha = k/\rho C$),
ΔT	Observed temperature change, °F,
ΔT_{J-T}	Joule-Thomson cooling, °F,
Δz	Production interval, ft,
μ	Viscosity, CP,
ρ	Density, lb/ft ³ , and
γ_o	Oil gravity, °API.

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Hotoil		
File Print Video Quit		
WELL NAME:	Example Data	
Process (Hot Oiling=1; Production=0)	1	
INPUT DATA HOTOILING (well specific):		
Injected Fluid (Oil = 1; H2O = 0)	1	UNITS none
Hot Oiling Time	1.25	hr
Bottom Hole Depth	4920	ft
Bottom Hole Temperature	113	F
Surface Temperature	50	F
Injection Temperature	257	F
Injection Rate	90	BBL/hr
Pump Rate	68	BBL/hr
Rod OD	0.875	in
Tubing ID	2.44	in
Tubing OD	2.87	in
Casing ID	4.95	in
Casing OD	5.50	in
Hole Diameter	7.88	in
Oil Gravity	32	API
Cloud Point	80	F
Wax Melting Point	183	F

Figure 1: DOS based compiled spreadsheet.

Netscape - [Hot Oiling Spreadsheet Demo]

File Edit View Go Bookmarks Options Directory Help

 Sandia National Laboratories

Hot Oiling Spreadsheet Demo

Fluid Injected Oil Water

Injection Time hrs

Bottom Hole Depth feet

Bottom Hole Temperature deg F

Surface Temperature deg F

Injection Temperature deg F

Injection Rate BBL/hr

Figure 2: Interactive form on the INTERNET.

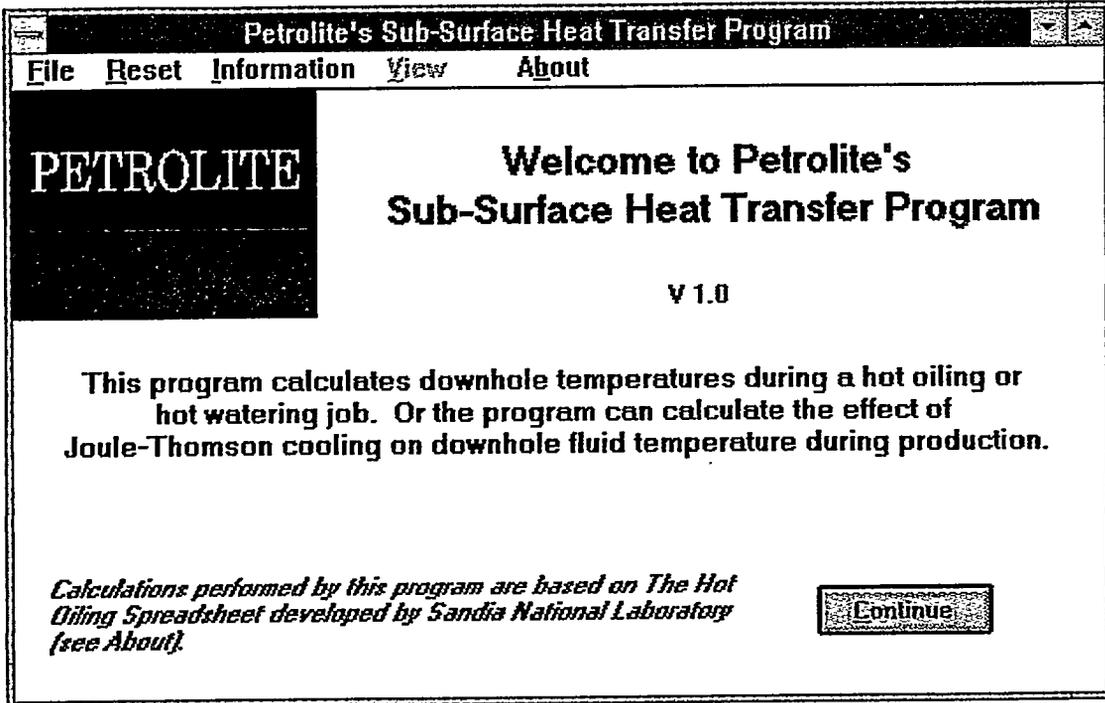
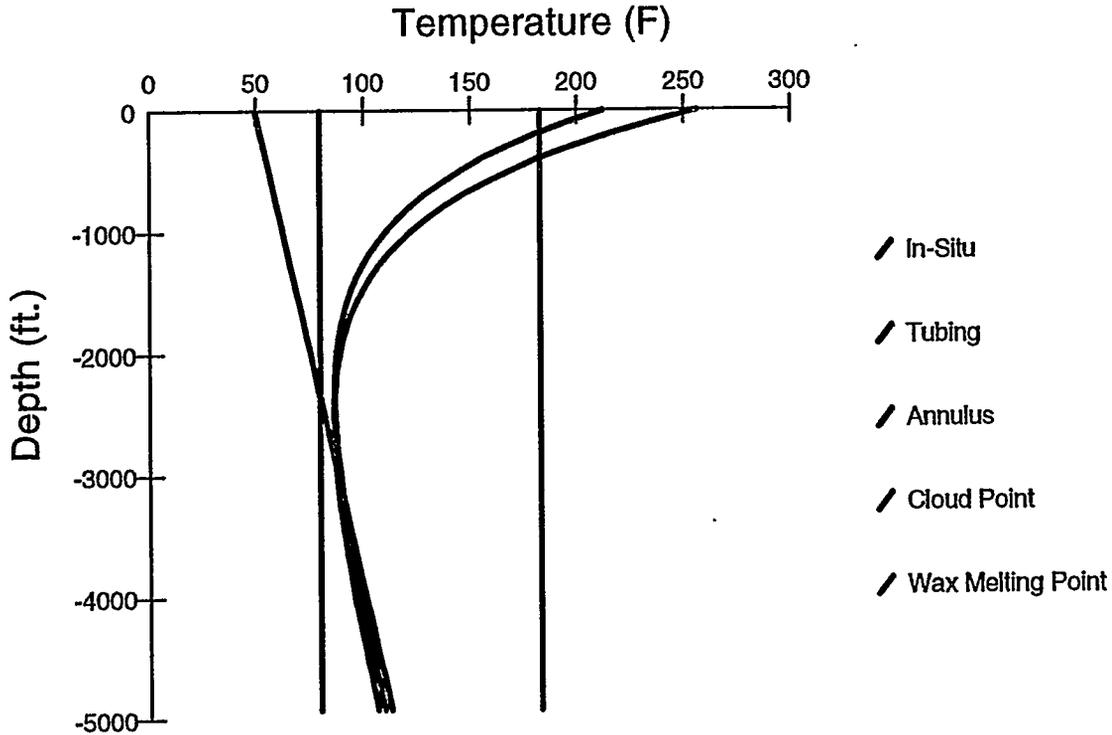


Figure 3: Petrolite's Windows™ program.



Example Well Data

Figure 4: Graphical output.

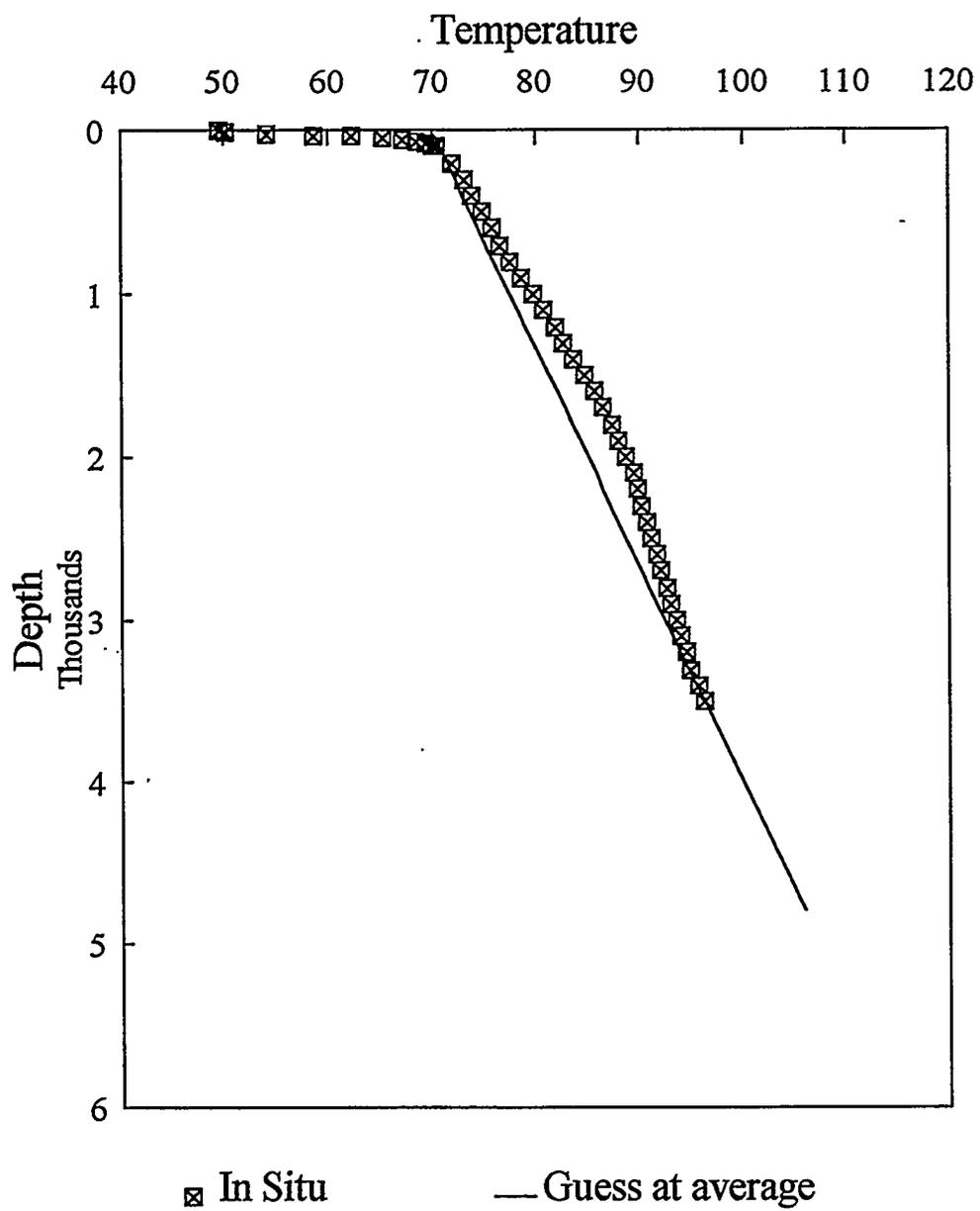


Figure 8: Measured and assumed geothermal temperatures.

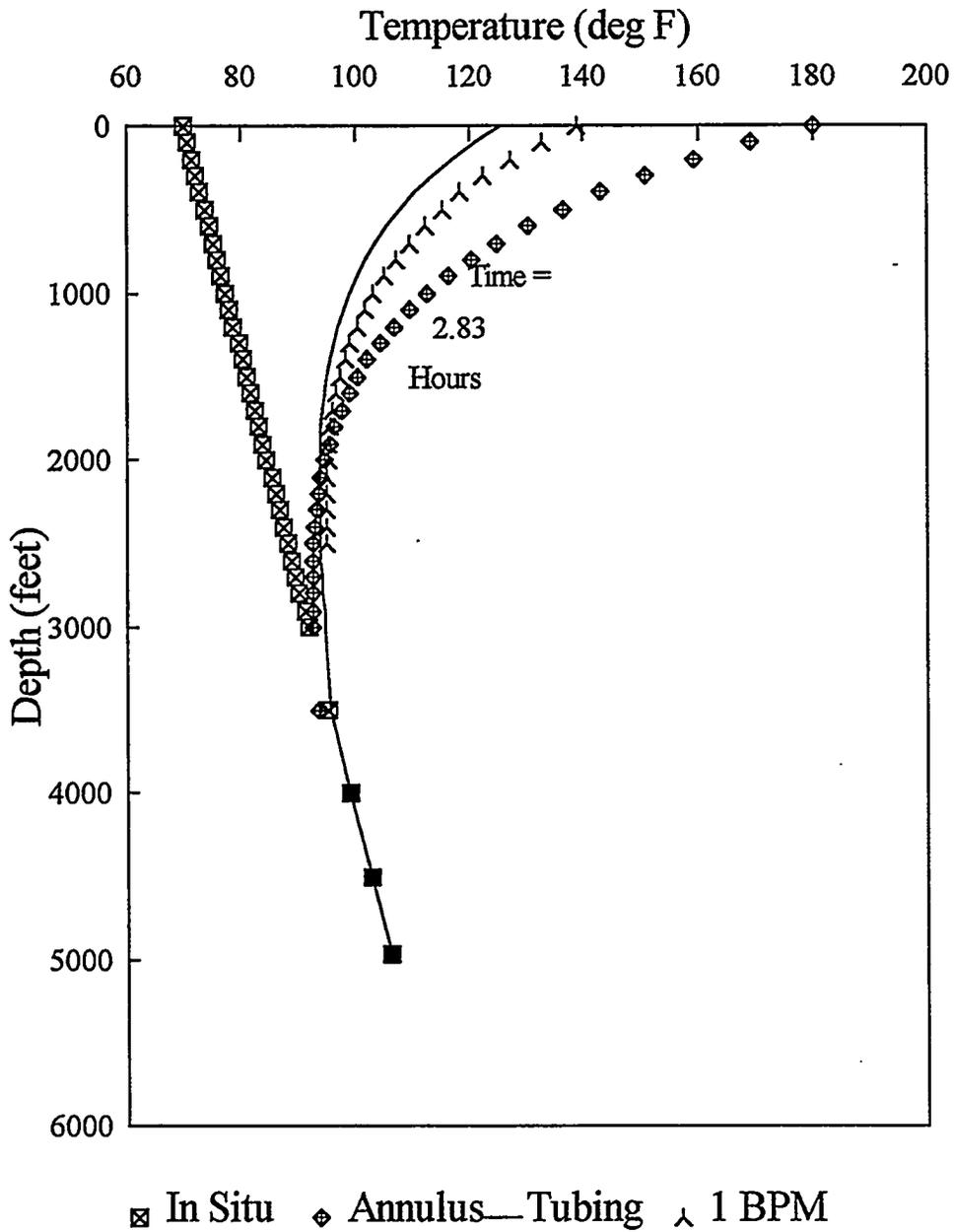


Figure 9: Temperature after circulating oil at 180°F for 2.83 hours at 1.12 BPM.

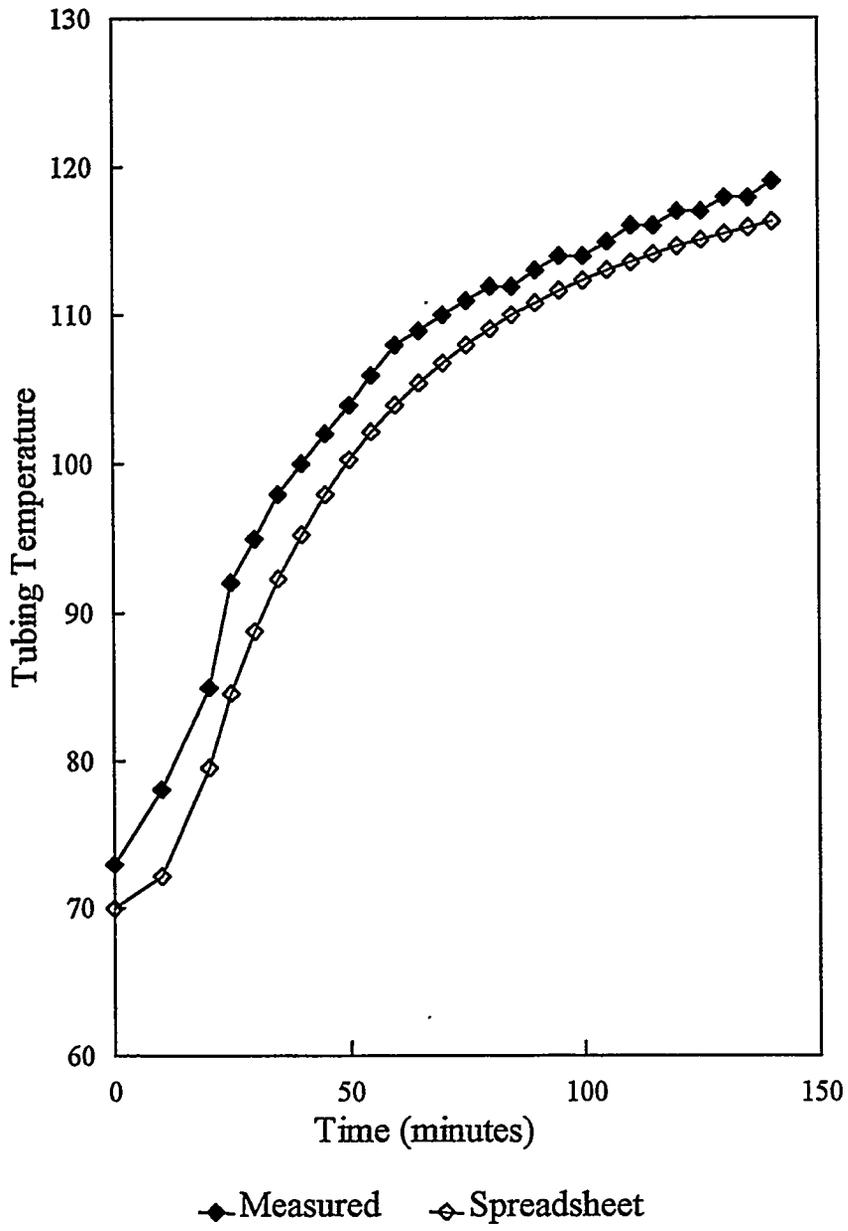


Figure 10: Temperature at 300 feet as a function of oil circulation time.

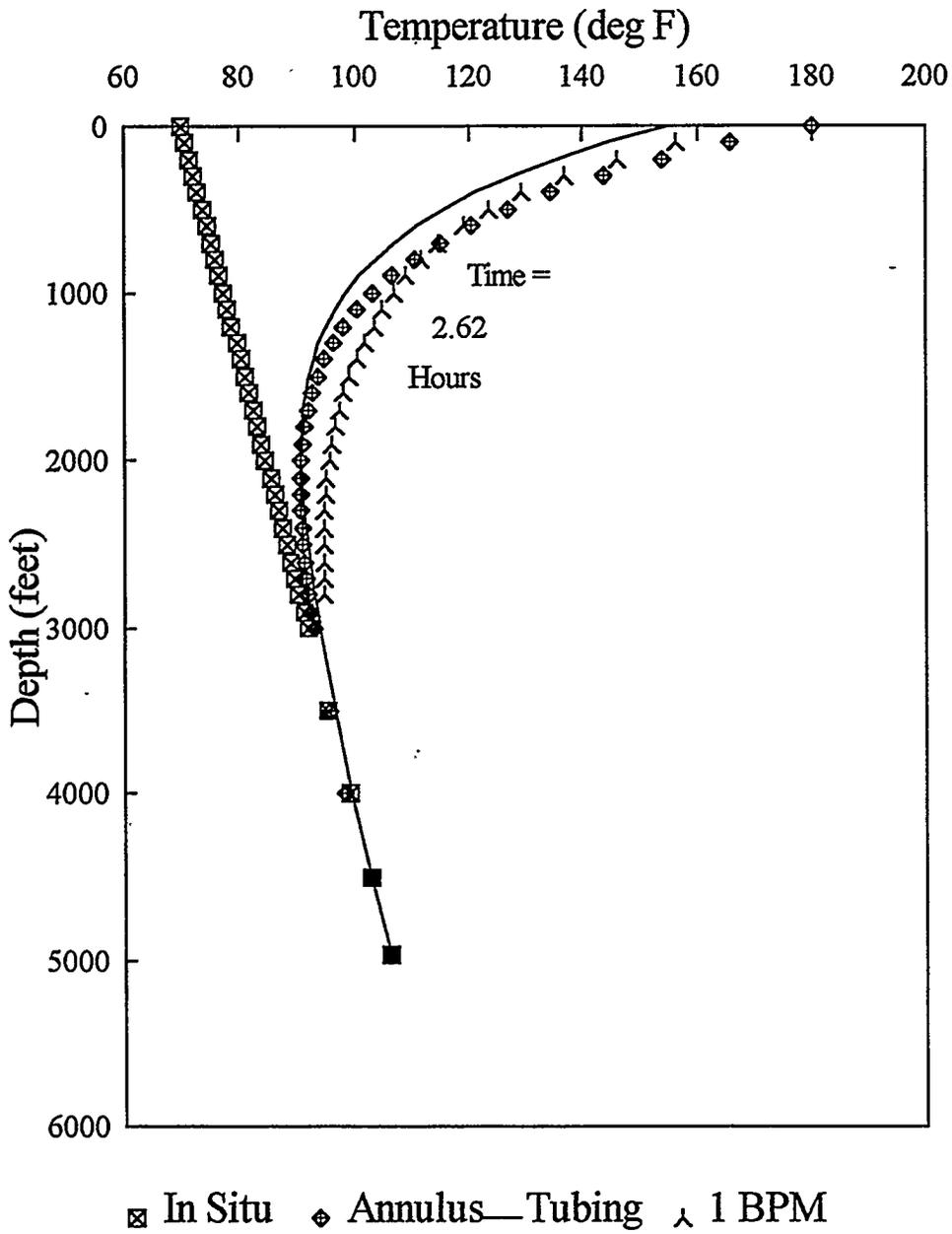


Figure11: Temperature after circulating water at 180°F for 2.62 hours at 1.08 BPM.

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